

# Investigation of the limonene photooxidation by OH at different NO concentrations in the atmospheric simulation chamber SAPHIR

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**Abstract.** The oxidation of limonene by the hydroxyl (OH) radical and ozone (O<sub>3</sub>) was investigated in the atmospheric simulation chamber SAPHIR in experiments performed at different nitric oxide (NO) mixing ratios from nearly zero up to 10 ppbv. For the experiments dominated by OH oxidation the formaldehyde (HCHO) yield was experimentally determined and found to be (12±3), (13±3), and (32±5) % for experiments with low (~0.1 ppbv), medium (~0.3 ppbv), and high NO (5 to 10 ppbv), respectively. The yield in an ozonolysis-only experiment was (10±1)%, which agrees with previous laboratory studies. The experimental yield of the first generation organic nitrates from limonene-OH oxidation is calculated as (34±5)%, about 11% higher than the value in the Master Chemical Mechanism (MCM), which is derived from structure-activity-relationships (SAR). Time series of measured radicals, trace-gas concentrations, and OH reactivity are compared to results from zero-dimensional chemical box model calculations applying the MCM v3.3.1. Modelled OH reactivity is 5 to 10 s<sup>-1</sup> (25% to 33% of the OH reactivity at the start of the experiment) higher than measured values at the end of the experiments at all chemical conditions investigated, suggesting either that there are unaccounted loss processes of limonene oxidation products or that products are less reactive toward OH. In addition, model calculations underestimate measured hydroperoxyl radical (HO<sub>2</sub>) concentrations by 20% to 90% and overestimate organic peroxy radical (RO<sub>2</sub>) concentrations by 50% to 300%. Largest deviations are found in low-NO experiments and in the ozonolysis experiment. An OH radical budget analysis, which uses

only measured quantities, shows that the budget is closed in most of the experiments. A similar budget analysis for RO<sub>2</sub> radicals suggests that an additional RO<sub>2</sub> loss rate constant of about  $(1 - 6) \times 10^{-2} \text{ s}^{-1}$  for first-generation RO<sub>2</sub> is required to match the measured RO<sub>2</sub> concentrations in all experiments. Sensitivity model runs indicate that additional reactions converting RO<sub>2</sub> to HO<sub>2</sub> at a rate constant of about  $(1.7 - 3.0) \times 10^{-2} \text{ s}^{-1}$  would improve the model-measurement agreement of NO<sub>x</sub>, HO<sub>2</sub>, RO<sub>2</sub> concentrations, and OH reactivity. Reaction pathways that could lead to the production of additional OH and HO<sub>2</sub> are discussed, which include isomerisation reactions of RO<sub>2</sub> from the oxidation of limonene, different branching ratios for the reaction of RO<sub>2</sub> with HO<sub>2</sub>, and a faster rate constant for RO<sub>2</sub> recombination reactions. As the exact chemical mechanisms of the additional HO<sub>2</sub> and OH sources could not be identified, further work needs to focus on quantifying organic product species and organic peroxy radicals from limonene oxidation.

## 1 Introduction

About 1000 Tg of biogenic volatile organic compounds (BVOCs) are emitted into the atmosphere every year. Approximately half of the emissions comprise isoprene while 15% consist of monoterpene species (Guenther et al., 2012). Among monoterpenes, limonene is the fourth most abundant species, which comprises about 10% of the total monoterpene emissions (Sindelarova et al., 2014). Apart from biogenic sources, limonene is also emitted from anthropogenic sources such as air fresheners and cleaning products (Liu et al., 2004; Nazaroff and Weschler, 2004; McDonald et al., 2018; Gkatzelis et al., 2021a, b). Limonene has two carbon-carbon double bonds, which make it reactive towards atmospheric oxidants such as ozone (O<sub>3</sub>), hydroxyl radicals (OH), and nitrate radicals (NO<sub>3</sub>) (Calogirou et al., 1999; Atkinson and Arey, 2003).

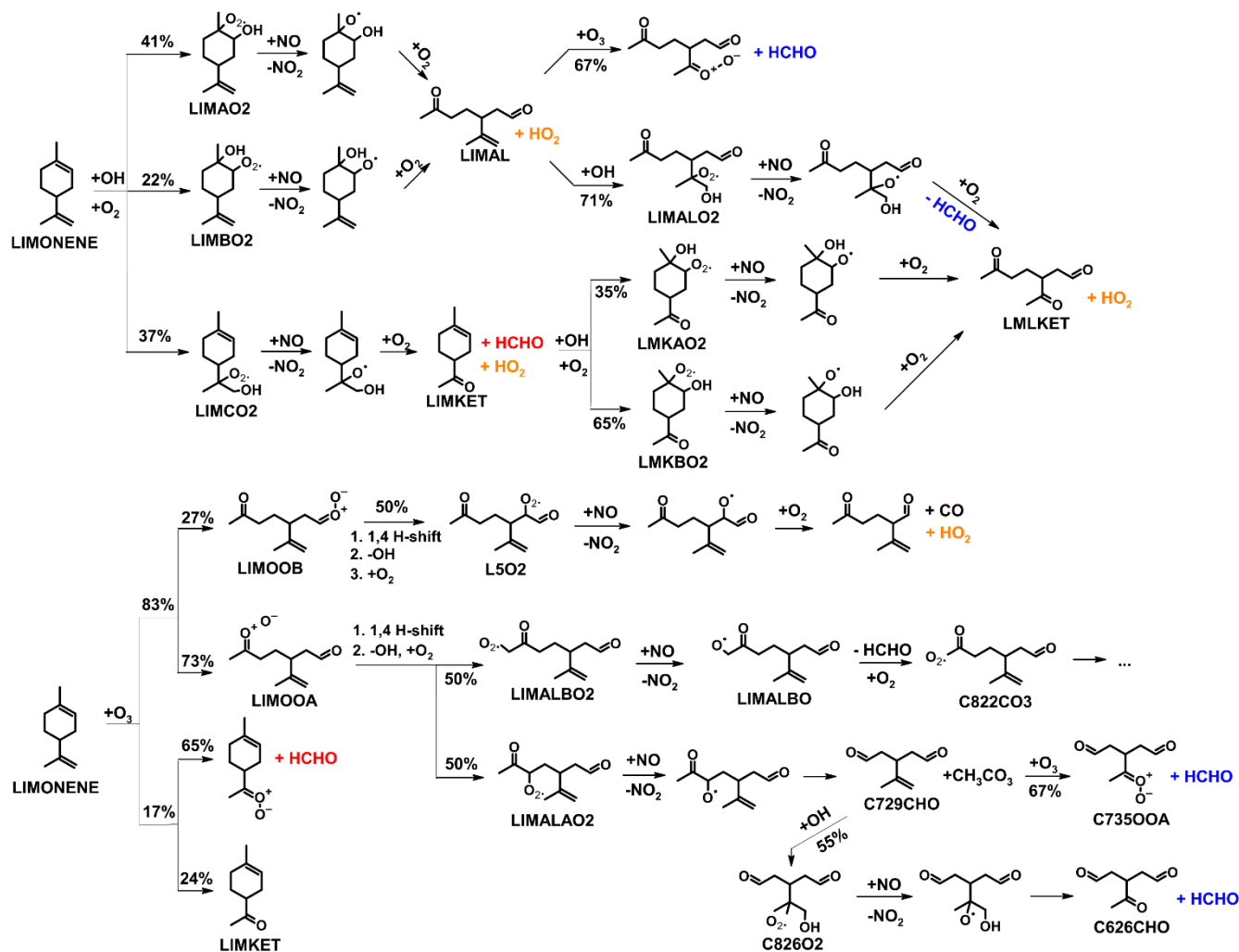
During daytime, the most important oxidant is the hydroxyl radical (OH). The reaction between the olefin group and the OH radical yields a β-hydroxyalkyl radical, which subsequently reacts with an oxygen molecule (O<sub>2</sub>) under atmospheric conditions to form an organic peroxy radical (RO<sub>2</sub>) (Fig. 1). In the presence of nitric oxide (NO), RO<sub>2</sub> is converted to an alkoxy radical (RO) and thereby NO is oxidized to nitrogen dioxide (NO<sub>2</sub>). NO<sub>2</sub> can be photolyzed back to NO together with an oxygen atom, which then reacts with an oxygen molecule producing ozone. This mechanism is the most relevant source for tropospheric ozone. Alkoxy radicals are very reactive and they often quickly decompose forming carbonyl products and a hydroperoxyl radical (HO<sub>2</sub>) or further organic radicals (Orlando et al., 2003). OH is then regenerated through the reaction between HO<sub>2</sub> and NO, closing the radical reaction cycle and producing another ozone molecule from the photolysis of nitrogen dioxide. In polluted environments with high NO<sub>x</sub> (=NO+NO<sub>2</sub>) emissions such as in urban areas (NO concentration > 1000 pptv; e.g., Dusanter et al. (2009) and Lu et al. (2017)), the reaction between RO<sub>2</sub> and NO is often the dominant pathway, through which OH is regenerated. In remote regions with low NO mixing ratios (< 200 pptv; e.g., Ren et al. (2006) and Whalley et al. (2011)), RO<sub>2</sub> predominantly reacts with HO<sub>2</sub> and forms an organic peroxide molecule. This process terminates the radical chain. The organic peroxide produced during this process can potentially add to secondary organic aerosols (SOA) (Surratt et al., 2006). RO<sub>2</sub> radicals can also react with other RO<sub>2</sub> radicals. The reaction rate constant is usually low ( $k$  ranges from  $10^{-15}$  to  $10^{-11} \text{ cm}^3 \text{ s}^{-1}$ ; (Tyndall et al. (2001); Jenkin et al. (2019)) and the RO<sub>2</sub> loss rate is often small for atmospheric RO<sub>2</sub> concentrations (RO<sub>2</sub>

65  $\sim 10^8 \text{ cm}^{-3}$ ; Tan et al. (2018)). Products of the  $\text{RO}_2$  recombination reactions are either alkoxy radicals or oxidized organic compounds containing alcohol or carbonyl functional groups, which terminate the radical reaction chain.

During the last decade, there has been increasing evidence from laboratory studies as well as theoretical studies that also unimolecular reactions of  $\text{RO}_2$  can be of importance in the atmosphere. Unimolecular H-shift reactions of  $\text{RO}_2$  can promote the formation of low volatility organic compounds as the number of oxygen atoms in the molecule quickly increases during the process (Jokinen et al., 2014). In some of the unimolecular reactions,  $\text{HO}_x (= \text{OH} + \text{HO}_2)$  radicals can be regenerated, so that this reaction pathway becomes a radical propagation reaction that does not require the presence of NO. This has been, for example, shown for isoprene (Peeters and Müller, 2010; Crounse et al., 2011; Peeters et al., 2014; Berndt et al., 2019; Novelli et al., 2020) and methacrolein (Crounse et al. 2012, Fuchs et al., 2014). The reaction rate constant of H-shift unimolecular reactions depends on the position of the H-atom relative to the peroxy group, the position of other functional groups to the H-atom, and temperature (Crounse et al., 2013; Vereecken and Nozière, 2020). H-shift reactions are very slow ( $k < 10^{-3} \text{ s}^{-1}$  at 298 K) in an aliphatic peroxy radical without an oxygenated function group (e.g., carbonyl, hydroxyl, alkoxy) attached to the carbon atom, from which the hydrogen is abstracted ~~nearby electron drawing functional group for atmospheric conditions~~ (Otkjær et al., 2018; Praske et al., 2019), ~~so that~~ Therefore, they H-shift reactions typically cannot compete with bimolecular reactions under atmospheric conditions ( $k_{\text{bi}} \sim 10^{-2} \text{ s}^{-1}$ , for 50 pptv of NO and  $5 \times 10^8 \text{ cm}^{-3}$  of  $\text{HO}_2$ ). Even if the  $\text{RO}_2$  radical contains a hydroxyl group, rate constants for H-shift reactions from the hydroxyl group are still low ( $k \sim 10^{-2}$  to  $10^{-1} \text{ s}^{-1}$ ) (Vereecken and Nozière, 2020) and can only compete with bimolecular reactions in the atmosphere in remote areas or suburban regions with low to moderate NO concentrations (50 – 500 pptv). However, there are also fast H-shift reaction pathways that could compete with bimolecular reactions even in moderately or heavily polluted scenario such as allylic-H shift ( $k \sim 1 \text{ s}^{-1}$ ) or aldehydic H-shift ( $k \sim 1 - 100 \text{ s}^{-1}$ ) reactions, in which the radical is stabilized by delocalized electrons or the carbonyl group, respectively (Otkjær et al., 2018; Zhang and Dibble, 2011; Vereecken and Nozière, 2020). Concerning limonene, which contains two carbon-carbon double bonds (Fig. 1), recent theoretical studies suggest that the  $\text{RO}_2$  radical formed after the reaction with OH or  $\text{O}_3$  undergoes rapid unimolecular reactions (reaction rate constants range from 1 to  $10^2 \text{ s}^{-1}$ ; Møller et al., 2020; Chen et al., 2021), which would be competitive with bimolecular reactions even in polluted environments. In this study, the atmospheric degradation of limonene was investigated in the atmospheric simulation chamber SAPHIR (Simulation of Atmospheric PHotochemistry In a large Reaction Chamber) at Forschungszentrum Jülich, Germany. Experiments were performed at three atmospherically relevant NO concentrations ranging from 0.1 to 10 ppbv. In addition, one ozonolysis experiment was conducted without the presence of  $\text{NO}_x$ . Radiation and relative humidity during the experiments were also relevant to the conditions that are typically found in the atmosphere, which was an improvement compared to previous experiments that typically used artificial light sources or were conducted under very dry conditions (e.g., (Larsen et al., (2001) and; Librando and Tringali, (2005)).

The main objective of this work is to evaluate the performance of the current chemical model (Master Chemical Mechanism version 3.3.1, <http://mcm.leeds.ac.uk/MCM>) by comparing observations of trace gas and radical concentrations with model

results. In particular, the question of whether the regeneration of OH from the radical cycle can be described by model calculations is investigated.



**Figure 1.** Simplified mechanism of the limonene oxidation by OH and O<sub>3</sub>. If available, names of the species as they appear in the MCM v3.3.1 are given. For simplicity the stereo-specificity of the intermediates, RO<sub>2</sub> reactions with HO<sub>2</sub> and other RO<sub>2</sub>, as well as the formation of organic nitrates are not shown here. Production of HCHO from the first oxidation step of limonene is labelled in red; HCHO production from the second oxidation step is labelled in blue; production of a HO<sub>2</sub> radical is labelled in orange. The production of HCHO from the decomposition of LIMALBO is not classified as it is not produced from the oxidation of the terminal C=C double bond. Most of the mechanism and branching ratios are taken from the MCM v3.3.1, except for the branching ratios of the O<sub>3</sub> addition at the external C=C bond of limonene (Wang and Wang, 2021) and the decomposition of LIMOOB to L5O<sub>2</sub>.

## 2 Methods

### 2.1 Atmospheric simulation chamber SAPHIR

SAPHIR is a large outdoor chamber located at Forschungszentrum Jülich, Germany. The cylindrical-shaped chamber (18 m length, 5 m diameter, volume 270 m<sup>3</sup>) is made of a double-wall Teflon (FEP) film, which minimizes wall loss and allows the transmission of the entire spectrum of solar radiation. A shutter system can be opened and closed to allow experiments in illuminated or dark conditions. All experiments are performed in synthetic air produced by evaporating ultrapure liquid oxygen and nitrogen (Linde, purity > 99.9999%). The air pressure inside the SAPHIR chamber is kept above the atmospheric pressure by 35 Pa to ensure that air outside the chamber cannot leak into the chamber, resulting in a typical dilution rate of trace gases of approximately 4 % h<sup>-1</sup>. The temperature in the chamber is similar to the ambient temperature. More details of the chamber can be found in previous publications Rohrer et al. (2005) and Kaminski et al. (2017).

### 2.2 Instrumentation

Table 1 provides an overview of the quantities that were measured and the corresponding instruments. NO and NO<sub>2</sub> concentrations were monitored with a chemiluminescence instrument (Eco Physics) with a blue-light photolytic converter that converts NO<sub>2</sub> to NO. In some experiments, the zero value of the instrument was not accurately determined as could be seen by a significant NO and NO<sub>2</sub> mixing ratio (NO < 0.02 ppbv, NO<sub>2</sub> < 0.5 ppbv) that was measured in the dark, clean chamber. For these experiments, the instrumental zero was subtracted for the analysis of data in this work. Nitrous acid was measured in some experiments by a long-path absorption photometer (Li et al., 2014). Similar as for the NO<sub>x</sub> instruments, non-zero HONO (< 100 pptv) was measured in the clean dark chamber in some experiments. This value was attributed to an unaccounted instrumental zero value and subtracted from the data.

O<sub>3</sub> was measured with a UV absorption instrument (AnsycO). Photolysis frequencies were calculated from solar actinic flux densities measured by a spectroradiometer outside the chamber (Bohn et al., 2005; Bohn and Zilken, 2005).

OH was measured with a laser-induced fluorescence (LIF) instrument, in which OH is excited by laser light at a wavelength of 308 nm in a low-pressure cell (3.5 hPa) (Holland et al., 1995). HO<sub>2</sub> was measured by the LIF instrument in a separate detection cell (HO<sub>x</sub>-cell), in which HO<sub>2</sub> is first converted to OH in the reaction with NO and the sum of OH and HO<sub>2</sub> (=HO<sub>x</sub>) is detected by OH fluorescence. The HO<sub>2</sub> concentration is then calculated by subtracting the OH concentration measured in the OH-cell from the signal obtained in the HO<sub>x</sub>-cell. Organic peroxy radicals (RO<sub>2</sub>) can potentially interfere in the measurement of HO<sub>2</sub> due to the concurrent conversion of RO<sub>2</sub> to HO<sub>2</sub> after the reaction with NO. This interference is usually

less than 5% for simple alkoxy radicals ( $C_1$ - $C_4$ ) because of the slow conversion rate of the alkoxy radical produced in the reaction of  $RO_2$  with NO at the reduced  $O_2$  concentration in the low-pressure cell. However,  $\beta$ -hydroxy alkoxy radicals formed from the OH-initiated oxidation of larger alkene species (e.g., isoprene) could rapidly decompose and then react with  $O_2$  to form  $HO_2$ , which adds to the sampled  $HO_2$  radical concentration (Fuchs et al., 2011; Lu et al., 2012). During the experiments in this work, the  $HO_2$  cell was operated with low NO concentrations to minimize the conversion of  $RO_2$  to  $HO_2$  radicals, but it cannot be excluded that a small fraction of limonene  $RO_2$  acted as interference. -The upper limit of such an interference would be around 15% as indicated by characterization experiments, which unfortunately did not allow to determine an accurate number due to the limited precision of results.

$RO_2$  was measured in the  $RO_x$ -LIF system, which consists of a converter mounted on top of a fluorescence detection cell. In the converter,  $RO_2$  is converted to  $HO_2$  in the presence of added CO and NO at low total pressure ( $\sim 25$  hPa). The  $HO_2$  is then passed into a low-pressure detection cell (3.5 hPa) where  $HO_2$  is converted into OH by reaction with a large excess of added NO. The  $RO_2$  concentration is calculated by subtracting the  $HO_x$  concentration from the measured signal (Fuchs et al., 2008, 2011). The sensitivity of the LIF instrument to  $RO_2$  is regularly calibrated for methylperoxy radicals. Laboratory tests show that the instrument's sensitivity for  $RO_2$  radicals from limonene might be slightly reduced compared to the sensitivity for methylperoxy radicals ( $0.85 \pm 0.05$ ).

Apart from the detection by the LIF instrument, OH radical concentrations were measured by differential optical absorption spectroscopy (DOAS) (Dorn et al., 1995) in the experiments in 2015. The mean differences between the LIF-measured OH and DOAS-measured OH concentrations in the two experiments in 2015 were -13 % and +39 %. The difference between measurements on the latter experiment was higher than the combined accuracies of the measurements. Because DOAS is inherently a calibration-free method and it is regarded as a reference method (Schlosser et al., 2007, 2009), OH concentrations from this instrument are used for the evaluation of experiments in 2015.

Measurements of the OH reactivity ( $k_{OH}$ ), the inverse chemical lifetime of the OH radical, were achieved by an instrument making use of laser flash-photolysis combined with the OH detection by LIF (Lou et al., 2010; Fuchs et al., 2017). In this instrument, air is sampled through a flow tube. A high concentration of OH is generated by ozone photolysis in the presence of water vapour using a short laser pulse at 266 nm, followed by the time-resolved measurement of the OH concentration while the OH is consumed by OH reactants contained in the sampled air. The pseudo-first-order loss rate ~~loss~~-constant of the decay of the OH concentration gives the OH reactivity value.

Limonene concentrations were measured by gas chromatography coupled with a flame ionization detector (GC-FID, Kaminski (2014)), as well as by a proton-transfer-reaction time-of-flight mass spectrometer (PTR-TOF-MS) (Lindinger et al., 1998; Jordan et al., 2009). Two GC-FIDs were used in the experiments in 2012. The differences between measurements by the 2 GC-derived measurements for limonene concentrations were about 12%. Discrepancies between the limonene concentrations measured by GC-FID and PTR-MS were about 12% depending on which GC-FID measurement is used.

The amount of injected limonene can also be derived from the rapid increase of OH reactivity, when limonene is injected. The injected limonene concentrations derived from the increase of OH reactivity agree with the PTRMS measurements within 15% in three experiments (08 August 2012, 10 August 2012, and 13 June 2015), but discrepancies were between 20 – 55% in the other experiments. For the analysis in this work, PTR-MS measurements were scaled in some experiments to match the  
175 limonene injections assuming that the measurement of OH reactivity is more accurate than PTR-MS measurements because no calibration of the instrument is required.

A time-of-flight chemical ionization mass spectrometer (ToF-CIMS) applying ionization with nitrate ions ( $^{15}\text{NO}_3^-$ ) detected some nitrated oxidized species in one limonene-OH oxidation experiment with high NO concentrations (12 August 2013) (Zhao et al., 2018). Although there was no calibration available to derive absolute concentrations, the time series of mass to  
180 charge ratios gave information about the relative abundance of these species.

Measurements of formaldehyde (HCHO) concentrations were available from either one of three instruments which included an instrument making use of the Hantzsch reaction (AL4021, Aero Laser GmbH), the DOAS instrument that is also used for the detection of OH, and a cavity ring-down spectroscopy (CRDS) analyzer (Picarro G2307) (Glowania et al., 2021). Measurements using the Hantzsch method were available in the experiments in 2012; measurements with DOAS were  
185 available in the experiments in 2015; measurements with CRDS were available in the experiments in 2019. Measurements were corrected for an unaccounted instrumental zero value ( $< 0.5$  ppbv) observed in the clean dark chamber in some experiments.

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**Table 1.** Instrumentation for radical and trace-gas measurements in the chamber experiments.

Species	Method	Time resolution	1 $\sigma$ precision	1 $\sigma$ accuracy
OH	DOAS <sup>a</sup>	205 s	$0.8 \times 10^6 \text{ cm}^{-3}$	6.5 %
	LIF <sup>b</sup>	47 s	$0.3 \times 10^6 \text{ cm}^{-3}$	13 %
HO <sub>2</sub> , RO <sub>2</sub>	LIF	47 s	$1.5 \times 10^7 \text{ cm}^{-3}$	16 %
OH reactivity	Laser flash photolysis + LIF	180 s	0.3 s <sup>-1</sup>	0.5 s <sup>-1</sup>
NO	Chemiluminescence	60 s	20 pptv	5 %
NO <sub>2</sub>	Chemiluminescence + photolytical converter	60 s	20 pptv	5 %
O <sub>3</sub>	Chemiluminescence	180 s	60 pptv	5 %
Limonene	PTR-TOF-MS <sup>c</sup>	40 s	15 pptv	14 %
	GC-FID <sup>d</sup>	45 min	4 – 8 %	5 %
	DOAS <sup>e</sup>	100 s	20 %	7 %
Formaldehyde	CRDS <sup>f</sup>	300 s	90 pptv	10 %
	Hantzsch <sup>g</sup>	60 s	25 pptv	8.6 %
Acetone	GC-FID	45 min	4 – 8 %	5 %
HONO	LOPAP <sup>h</sup>	300 s	3 pptv	10 %
Photolysis frequencies	Spectroradiometer	60 s	10 %	18 %

<sup>a</sup> Differential optical absorption spectroscopy. <sup>b</sup> Laser-induced fluorescence. <sup>c</sup> Proton transfer reaction time-of-flight mass spectrometry. <sup>d</sup> Gas chromatography coupled with flame ionization detector. <sup>e</sup> Differential optical absorption spectroscopy, available for the experiments in 2015. <sup>f</sup> Cavity ring-down spectroscopy, available for the experiments in 2019. <sup>g</sup> not available in the experiments on 12 August 2013 and 05 June 2020 <sup>h</sup>Long-path absorption photometer.

**2.3 Limonene oxidation experiments**

Before the start of an experiment, the chamber was cleaned by flushing dry, ultra-pure synthetic air through the chamber overnight to purge out trace gases that remained from previous experiments. To humidify the air at the start of the experiment, water vapor from boiling ultra-pure water (Milli-Q) was flushed into the chamber, until the relative humidity reached about 70%. The relative humidity gradually decreased to 30 – 50 % as a result of the increasing temperature in the chamber over the



course of the experiment and the dilution by the dry replenishing air. Before the injection of limonene, the chamber roof was opened to allow sunlight to irradiate the clean chamber air (zero air phase). In the illuminated chamber, small amounts of nitrous acid (HONO), formaldehyde, and acetone were formed with a rate of a few hundred pptv h<sup>-1</sup> (Rohrer et al., 2005) presumably from chamber wall reactions. Therefore, the primary source of OH and NO in most of the experiments was the photolysis of HONO leading also to a continuous increase of nitrogen oxide concentrations (NO<sub>x</sub>).

In total, seven experiments investigating limonene oxidation were performed. Chemical conditions can be divided by the NO concentration levels (Table 2), for which the contributions of different RO<sub>2</sub> loss reactions varied between radical propagation reactions (i.e., reaction with NO), radical termination channels (i.e., reactions with HO<sub>2</sub> and RO<sub>2</sub>) and isomerisation reactions.

In the experiments with low NO mixing ratios of 0.1 to 0.15 ppbv (01 September 2012 (Fuchs et al., 2021a), 04 July 2019 (Bohn et al., 2021b)), about 3 to 4 ppbv of limonene was injected three times. Between each injection, limonene was oxidized for about 90 to 120 minutes, so that most of the limonene reacted away before the next injection. To suppress NO concentrations during the experiments, approximately 50 to 60 ppbv of O<sub>3</sub> produced by a silent discharge ozonizer (O3Onia) was injected before opening the chamber roof.

In experiments with medium NO concentrations ranging from 0.25 to 0.4 ppbv (08 and 10 August 2012; Fuchs et al., 2021a, b)), about 4 ppbv limonene was injected two hours after opening the roof. No additional trace gases were added. Measured O<sub>3</sub> mixing ratios increased from about 1 ppbv to 10 ppbv as a result of the photolysis of NO<sub>2</sub>, which was produced from the reaction between peroxy radicals and NO.

In the experiment with the high NO concentrations (03 August 2015, (Bohn et al., 2021c)), about 15 ppbv of NO was injected into the chamber before opening the chamber roof and 10 ppbv of limonene at later times. When most of the limonene was consumed within two hours after the first injection, an additional injection of 10 ppbv of limonene was done. In this work, the HCHO yield is only analysed based on the measurement before the second limonene injection (Section 3.1.1), because of the potential secondary production of HCHO from the oxidation of secondary products. The radical concentrations and OH reactivities are only analysed after the second limonene injectionthe later part of the experiment (Section 3.2.3) was analyzed, because radical measurements failed during the first part of the experiment. A large fraction of NO was already titrated by ozone at this timeafter the second limonene injection. When most of the limonene was consumed within two hours after the first injection, an additional injection of 10 ppbv of limonene was done.

Lastly, a limonene ozonolysis experiment was conducted on 05 June 2020 (Bohn et al., 2021a), in which no NO<sub>x</sub> was present. This experiment intended to elucidate the ozonolysis chemistry. The chamber roof was closed at all times. In the first half of the experiment, about 4 ppbv of limonene was injected in addition to 45 ppbv O<sub>3</sub>. After three hours about 4.5 ppbv of limonene was re-injected together with O<sub>3</sub>, so that O<sub>3</sub> mixing ratios reached 70 ppbv. 100 ppmv of CO was added 30 minutes before the second injection to scavenge OH radicals that are produced from the limonene ozonolysis reaction.

**Table 2.** Experimental conditions during the time period when the radical budget of limonene oxidation experiments is analysed.  $k_{bi}$  is the sum of the total loss rate constant of RO<sub>2</sub> due to bi-molecular reactions with NO, HO<sub>2</sub>, and other RO<sub>2</sub> calculated from measured concentrations. Values are averages for the period of limonene oxidation analyzed in this work except for limonene concentrations, for which maximum concentrations after the injection are given. In experiments with multiple limonene injections, the range of the injections is noted.

Experiment	[NO] (ppbv)	[HO <sub>2</sub> ] (10 <sup>8</sup> cm <sup>-3</sup> )	$k_{bi}$ (s <sup>-1</sup> )	[OH] (10 <sup>6</sup> cm <sup>-3</sup> )	[O <sub>3</sub> ] (ppbv)	Limonene (ppbv)	Date
Ozonolysis	0	1.5 – 6.0	0.005 – 0.15	< 1	40 – 65	4	05 June 2020
Low NO	0.05 – 0.10	5 – 6	0.02 – 0.03	2 – 4	40 – 50	2 – 4	01 September 2012
	0.1	10	0.04	3	105	4	13 June 2015
	0.10 – 0.15	4 – 6	0.03 – 0.04	5 – 10	60	2 – 2.5	04 July 2019
Medium NO	0.2	3	0.05	2	5	4	08 August 2012
	0.3	4	0.07	4	5	4	10 August 2012
High NO	0.7	11	0.15	8	45	10	03 August 2015

**2.4 Model calculations**

The acquired measurements of trace gases and radicals are compared against a zero-dimensional box model applying the Master Chemical Mechanism (MCM) version 3.3.1 (Saunders et al., 2003; Jenkin et al., 2015). In addition to the chemistry from the MCM, chamber-specific processes including dilution and small productions of HONO, acetone and formaldehyde in the presence of sunlight are included in the model. Dilution in the chamber is implemented as a first-order loss process. The rate constant is calculated based on the monitored replenishment flow rate. The parameterization for the production of chamber sources for nitrous acid, formaldehyde and acetone follows the description in Rohrer et al. (2005) and Kaminski et al. (2017), in which production rates are parameterized as functions of temperature, relative humidity, and radiation. The source strength

for the production rates are scaled for each experiment from the observed increase in concentrations for the part of the experiment when the chamber roof was opened, but limonene was not present (zero-air phase).

270 In addition, a background OH reactivity in the range of  $1 \text{ s}^{-1}$  is present in the illuminated, clean chamber due to the presence of unmeasured OH reactants. In order to account for this background reactivity, an artificial OH reactant that behaves like CO is implemented in the model. Its concentration is adjusted in the model to match the observed OH reactivity during the zero-air phase and is assumed to be constant during the rest of the experiment.

275 The OH yield from limonene ozonolysis in the model calculations in this work is updated based on the IUPAC recommendations (Cox et al., 2020) decreasing the value from 87% to 66%. This is supported by multiple experimental studies (Aschmann et al., 2002; Herrmann et al., 2010; Forester and Wells, 2011) as well as theoretical studies (Wang and Wang, 2021). The decomposition product of the Criegee intermediate (MCM name: LIMOOb) is also updated, in which the terminal carbonyl group remains during the vinyl hydroperoxide mechanism (VHP). In addition, instead of forming a primary RO<sub>2</sub> (MCM name: C923O2) by eliminating a carbonyl group, decomposition of LIMOOb leads to the production of a secondary  $\beta$ -oxo substituted RO<sub>2</sub> (L5O2, Fig. 1). This is supported by the theoretical investigation of the ozonolysis of cyclohexene that the departure of the carbonyl group is not competitive without any inducing functional group (e.g.,  $\beta$ -hydroperoxyl) (Rissanen et al., 2014).

285 Three simulation model runs are performed for each experiment. In all model runs, physical parameters including temperature, pressure, photolysis frequencies, and the dilution rate of trace gases due to the replenishment flow are constrained to observations. If available, HONO concentrations are prescribed as measured to constrain the production from the chamber. In addition, ozone concentrations in the model are constrained to ensure that shortcomings of the model to predict ozone do not complicate the interpretation by an inappropriate fraction of limonene reacting with ozone. Time series of NO and NO<sub>2</sub> concentrations are constrained to observations in the model runs except for the third set of simulations to avoid potential impacts of shortcomings of the model to describe these species.

290 In the first set of simulations (denoted as “reference run”), model runs are performed without any further constraints or modifications. In the second set of simulations (denoted as “constrained run”), HO<sub>2</sub> concentrations are prescribed as measured to constrain the OH-production rate from the HO<sub>2</sub>+NO reaction. In this model run, OH reactivity is also adjusted to the measurements to yield an OH loss rate as observed (Section 3.3.1 to 3.3.4). In the third set of simulations (Section 3.5), NO and NO<sub>2</sub> concentrations are not constrained to investigate the fate of nitrogen oxides, radical concentrations and OH reactivity are also free parameters in the model.

295 OH reactivity from oxidation products tends to be overestimated by the model. Potential reasons include wall loss reactions of low volatility compounds such as organic nitrates and peroxides, uncertainties from the reactivity of products and intermediates that are mostly derived using structure-activity relationship (SAR) in the model (Jenkin et al., 1997; Saunders et al., 2003), and chemical loss due to reactions that are not included in the MCM (e.g., isomerisation reactions). To reduce the OH reactivity

in the model, it is assumed that organic nitrates and peroxides derived from limonene oxidation undergo a first order loss process.

300 The additional loss rate for organic nitrates is estimated from the decaying signal at the corresponding mass/charge ratio of the least oxidized C10 nitrate species ( $C_{10}H_{17}NO_6$ ) observed by the chemical ionization mass spectrometry (CIMS) instrument after the chamber roof was closed in the experiment with high NO concentrations. The lifetime of the least oxidized species C10 nitrate is used to estimate the loss rate, as the only C10 nitrate species from limonene oxidation that the MCM includes is  $C_{10}H_{17}NO_4$ . The loss rate constant is equivalent to a lifetime of about 2 hours (Supplementary materials Fig. S1, Zhao et al. (2018)), which is comparable to the chemical loss rate in the reaction with OH for conditions of these experiments (chemical lifetime of 0.5 to 4 hours). The specific reason for the additional loss of nitrates could not be identified, but might be due to wall loss or due to loss by hydrolysis reactions in the humidified air similar to findings in an isoprene-rich forest (Romer et al., 2016).

Organic peroxides, however, could not be detected by the CIMS instrument and hence the additional loss rate is adjusted such that the simulated OH reactivity agrees with measurements in the experiments with low and medium NO, when there should have been significant production of organic peroxides. This requires a lifetime of 10 minutes, much shorter than the lifetime of the order of hours under typical atmospheric conditions or those in the current experiments.

### 3. Results

#### 315 3.1 Product yields from the oxidation of limonene

##### 3.1.1 Formaldehyde and acetone yields from the oxidation of limonene by OH and O<sub>3</sub>

Formaldehyde (HCHO) is one of the oxidation products of the reaction of limonene with the OH radical as well as with ozone. It is mainly produced from the oxidation of the terminal double bond in limonene (Fig. 1). The product yield of HCHO from the oxidation of limonene by OH and O<sub>3</sub> can be determined from the chamber experiments by comparing the measured concentrations of HCHO to the amount of oxidized limonene calculated from the measured limonene, OH and O<sub>3</sub> concentrations. As HCHO has also a small chamber source (Section 2.3) and it is lost by its reaction with OH and by photolysis, its concentration needs to be corrected for these losses following the method presented in Kaminski et al. (2017) and Rolletter et al. (2019).

For the evaluation of the HCHO yields, only measurements from the first two hours of the experiment after the first limonene injection are used, because further oxidation of accumulating organic products could contribute to the production of HCHO at later times of the experiment. This is demonstrated by a rapid increase of HCHO when 80% of limonene had reacted away

after a roughly linear relationship between HCHO and limonene concentrations (Fig. 1 and Supplementary Material Fig. S2). To derive the HCHO yield, a linear regression is performed for data until 40% of limonene is consumed and the slope of the linear regression gives the HCHO yield. This results in values of  $(12\pm3)\%$ ,  $(13\pm3)\%$ , and  $(32\pm5)\%$  for the OH oxidation experiments with low, medium and high NO mixing ratios, respectively (Fig. 2).

Formaldehyde is only produced from one of the three major RO<sub>2</sub> species formed in the initial reaction of limonene with OH. The structure-activity relationship (SAR) (Peeters et al. 2007) gives a yield of the formation of this RO<sub>2</sub> radical (Fig. 1) that results from the OH addition to the terminal C=C double bond (MCM name: LIMCO2) of 37% with an error of 15%. When the LIMCO2 radical reacts with NO or RO<sub>2</sub> radicals, an alkoxy radical is formed that subsequently forms HCHO from its decomposition together with a carbonyl compound (MCM name: LIMKET, Fig. 1). Therefore, the expected HCHO yield would be 37% at maximum from which the fraction of RO<sub>2</sub> reacting with other reaction partners such as HO<sub>2</sub> and the formation of organic nitrates in the reaction with NO (value determined in this work:  $(34\pm5)\%$ , Section 3.1.2) needed to be subtracted. The uncertainty in the yield of organic nitrates could be higher because the values are determined for all RO<sub>2</sub> species from limonene oxidation by OH, but the nitrate yield for individual RO<sub>2</sub> could vary. The fraction of RO<sub>2</sub> reacting with NO is more than 85% in the experiments with high and medium NO, and 65% in the experiment with low NO. The relative error of the fraction of RO<sub>2</sub> reacting with NO could be up to 35% due to the uncertainties of the reaction rate constants. Therefore, the HCHO yields expected from SAR in the experiments with high and medium NO is  $(22\pm9)\%$  and in the experiment with low NO is  $(16\pm6)\%$ .

All observed HCHO yields agree with SAR-derived HCHO yields which carry high relative uncertainties (40%). This could explain the discrepancies between the observed yield for the experiment with high NO mixing ratios and the SAR-derived yield. The largest discrepancy could be observed for medium NO levels. A higher yield of LIMCO2 or lower yield of organic nitrates for the reaction of LIMCO2 with NO could explain the discrepancies observed for the experiments with low NO. Another possible reason is that there are other reaction channels of the LIMCO2 peroxy radical that are competitive with the bimolecular reactions with NO and HO<sub>2</sub> ( $k_{bi}$  up to  $0.07\text{ s}^{-1}$ ) for conditions of the experiments with low and medium NO, but would not be relevant in the experiment with high NO mixing ratios ( $k_{bi}$  up to  $2\text{ s}^{-1}$ ). These reaction channels would not produce formaldehyde such as isomerisation. Possible isomerisation reactions of LIMCO2 are further discussed in Section 4.3.1.

The formation of HCHO at a later time in the experiments includes the production from further oxidation of first generation products. Therefore, HCHO yields are increasing over the course of the experiment to values of 40 to 90% with lowest yields in the experiments with low NO (Fig. S2). Part of the differences between the experiments could be due to the differences in the contributions of various product species, so that numbers are not necessarily comparable. The HCHO yield remains below 100% in all experiments. This is consistent with HCHO being only produced from the oxidation of the terminal C=C bond of the limonene structure on a short time scale of several hours in typical atmospheric conditions, so that total HCHO yield is limited to one in the limonene oxidation scheme.

360 Previous studies reported formaldehyde yields for the OH-oxidation of limonene between 36 and 43% (Larsen et al., 2001; Lee et al., 2006) (Table 3). The experiments by Larsen et al. (2001) and Lee et al. (2006) were performed at high NO concentrations, but the yield of HCHO yield is higher than the HCHO yield determined in the experiment with high NO in this work. However, experiments by Larsen et al. (2001) and Lee et al. (2006) were performed with much higher concentrations of limonene and NO (Table 3) and it is not clear, if only HCHO from the first oxidation step is considered (Fig. 1), so that  
365 numbers may not be entirely comparable. In the study by Librando and Tringali (2005), formaldehyde yields were determined to be 27 and 92% in experiments with high limonene mixing ratios of 13 and 2 ppmv, respectively, but in the absence of NO. Yields in their experiments may not comparable to yields in this work, because the fate of organic peroxy radicals was likely dominated by atmospherically not relevant  $\text{RO}_2 + \text{RO}_2$  recombination reactions.

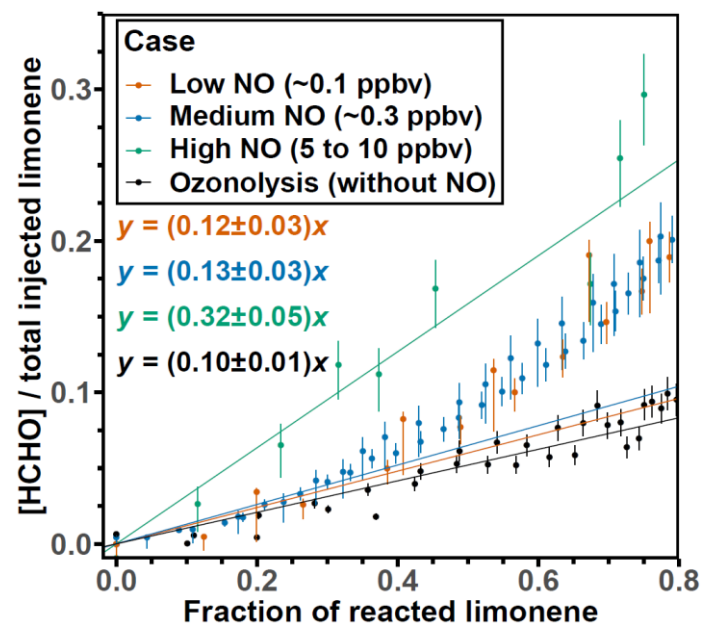
The HCHO yield derived from the pure ozonolysis experiment in this work is  $(10 \pm 1)\%$  in the presence of the OH scavenger.  
370 The same value is obtained, if the formaldehyde yield is determined from the part of the ozonolysis experiment without OH scavenger, when approximately 40% of limonene reacted with OH that is produced from the ozonolysis reaction. Similar to the OH reaction, formaldehyde production is expected from the subsequent chemistry after the ozone addition to the terminal C=C double bond. Because ozone preferably (87%) adds to the endocyclic C=C double bond (Wang and Wang, 2021), a low yield can be expected. As there was no NO present during the experiment, production of formaldehyde from the reaction  
375 between limonene and OH could only be possible from the reaction of LIMCO<sub>2</sub> with peroxy radicals or unimolecular reactions (e.g. isomerisation). As the HCHO yield is the same independent on the addition of the OH scavenger, the yield from the limonene-OH reaction at zero NO must be similar to the HCHO yield from the limonene ozonolysis. The HCHO yield derived from the ozonolysis without the  
the presence of the OH scavenger is similar to the HCHO yield in the experiments with low  
NO concentrations. This is as would be expected because of the very low NO concentrations and the similar fraction of  
380 limonene that reacted with OH or O<sub>3</sub> at about 40—60% in both experiments. only in the experiments with

The formaldehyde yield from the limonene ozonolysis derived in this work agrees well with the yield of 10% determined in the work by Grosjean et al. (1993) performed with an OH scavenger. Yields were also determined in the work by Gong et al. (2018) from several experiments at various chemical conditions. Values of 5 to 11% derived in their experiments with a limonene:O<sub>3</sub> concentration ratio of 1:2 are consistent with results in this work. However, the HCHO yield was 11 to 27% in  
385 the experiments with a limonene:O<sub>3</sub> concentration ratio of about 1:100. This higher yield might be explained by additional formaldehyde production from the ozonolysis of secondary products (Fig. 1). It is worth noting that no significant differences could be observed in experiments with and without OH scavenger in the experiments by Gong et al. (2018) similar to findings in this work.  
The effects of humidity and presence of an OH scavenger on the HCHO yield were also investigated in Gong et al. (2018). In their experiments, the HCHO yield increases strongly with increasing humidity and in the absence of an OH  
390 scavenger when the limonene:O<sub>3</sub> ratio is was very low (1:100). On the other hand, the positive dependence of the HCHO yield  
on humidity and the absence of OH scavenger is much less significant when the limonene:O<sub>3</sub> concentration ratio is was higher  
(1:2). There is no significant impact of OH scavenger on the HCHO yield found in this study, which is consistent to the with

findings from the experiments in Gong et al. (2018) with conducted in similar relative humidity (30–50%) with high limonene:O<sub>3</sub> ratio in Gong et al. (2018).

at the was the does the presence of an the limonene in the experiments in Gong et al. (2018).

In the experiments in this work, there was no significant acetone production from the oxidation of limonene, as the production rate of acetone from the chamber source ( $\sim 80 \text{ pptv h}^{-1}$ ) could already explain the observed increase of the acetone concentration during the experiments. This suggests that unlike other monoterpenes, acetone is not a significant product from limonene oxidation. This is consistent with findings by Lee et al. (2006) and Larsen et al. (2001). Also, the MCM does not predict acetone as a product in the limonene oxidation scheme.



**Figure 2.** HCHO concentrations divided by the injected limonene concentration plotted versus the fraction of reacted limonene for the first injection in the experiments with different NO levels. The regression includes data points up to 40% of the fraction of reacted limonene.

**Table 3.** HCHO yields from the OH- and O<sub>3</sub>-oxidation of limonene determined in the experiments in this work and reported in literature. Maximum values for limonene, O<sub>3</sub>, and NO concentrations in the experiments are listed.

Limonene + OH	HCHO yield (%)	Limonene (ppbv)	NO (ppbv)		
Larsen et al., 2001	36 ± 5	1000	1000		
Librando and Tringali, 2005	27 – 92	2100 – 13200	0		
Lee et al., 2006	43 ± 5	120	132 <sup>a</sup>		
This work	12 ± 3	3.5	0.05 – 0.15		
	13 ± 3	3.5	0.3		
	32 ± 5	10	3 – 10		
Limonene + O <sub>3</sub>	HCHO yield (%)	Limonene (ppbv)	O <sub>3</sub> (ppbv)	OH scavenger	
Grosjean et al., 1993	10	1200	70 – 100	Yes <sup>b</sup>	
Gong et al., 2018	7 – 11	280	500	No	
	5 – 8	280	500	Yes <sup>c</sup>	
	13 – 27	183	19000	No	
	11 – 23	183	19000	Yes <sup>c</sup>	
This work	10 ± 1	4	50	No	
	11 ± 1	4	80	Yes <sup>d</sup>	

<sup>a</sup>Given as NO<sub>x</sub> concentration <sup>b</sup>200 ppmv cyclohexane <sup>c</sup>400 ppmv of 2-butanol or cyclohexane <sup>d</sup>60 ppmv CO



### 420 3.1.2 Organic nitrate yield from the oxidation of limonene by OH

The organic nitrate yield of the RO<sub>2</sub>+NO reaction for peroxy radicals produced from the limonene+OH reaction is determined for experiments in this work following the method described for the analysis of previous experiments in the SAPHIR chamber (Hantschke et al., 2021; Tan et al., 2021). The amount of organic nitrates (RONO<sub>2</sub>) in the chamber is estimated by the difference between the accumulated production of nitrogen oxides from the chamber source of HONO ( $Q_{\text{HONO}}$ ), which is the only relevant  
 425 source for nitrogen oxides in the experiments, and the total NO<sub>y</sub> (=NO<sub>x</sub> + HONO + HNO<sub>3</sub>) concentrations. This method assumes that the differences can be solely attributed to the production of peroxy acyl nitrate (PAN)-like species, which can act as a reservoir for nitrogen oxides and can be significant in the oxidation of specific organic compounds.

The source Strength of HONO can be calculated from the photo-stationary state between HONO, NO and OH using measured concentrations and measured photolysis frequencies:

$$430 \quad \frac{d[\text{HONO}]}{dt} = Q_{\text{HONO}} - j_{\text{HONO}}[\text{HONO}] + k_{\text{OH}+\text{NO}}[\text{OH}][\text{NO}] \approx 0 \quad (1)$$

$$Q_{\text{HONO}} = j_{\text{HONO}}[\text{HONO}] - k_{\text{OH}+\text{NO}}[\text{OH}][\text{NO}] \quad (2)$$

The total amount of organic nitrates can be calculated from the difference between the accumulated HONO production and the sum of other nitrogen oxide species considering also their loss due to dilution in the chamber with rate constant  $k_{\text{dil}}$  and the loss of NO<sub>2</sub> in the reaction with OH (Hantschke et al., 2021):

$$435 \quad [\text{RONO}_2] = \int (Q_{\text{HONO}} - k_{\text{OH}+\text{NO}_2}[\text{NO}_2][\text{OH}] - k_{\text{dil}}([\text{NO}] + [\text{NO}_2] + [\text{HONO}]))dt - ([\text{NO}] + [\text{NO}_2] + [\text{HONO}]) \quad (3)$$

Assuming that at least right after the injection of limonene, the production of organic nitrates is dominated by the reaction of NO with RO<sub>2</sub> derived from limonene-OH, the organic nitrate yield  $\Phi_{\text{limonene}+\text{OH}}$  can be calculated:

$$[\text{RONO}_2] = \Phi_{\text{limonene}+\text{OH}} \int ([\text{RO}_2]_{\text{limonene}} \times [\text{NO}] \times k_{\text{RO}_2+\text{NO}}) dt \quad (4)$$

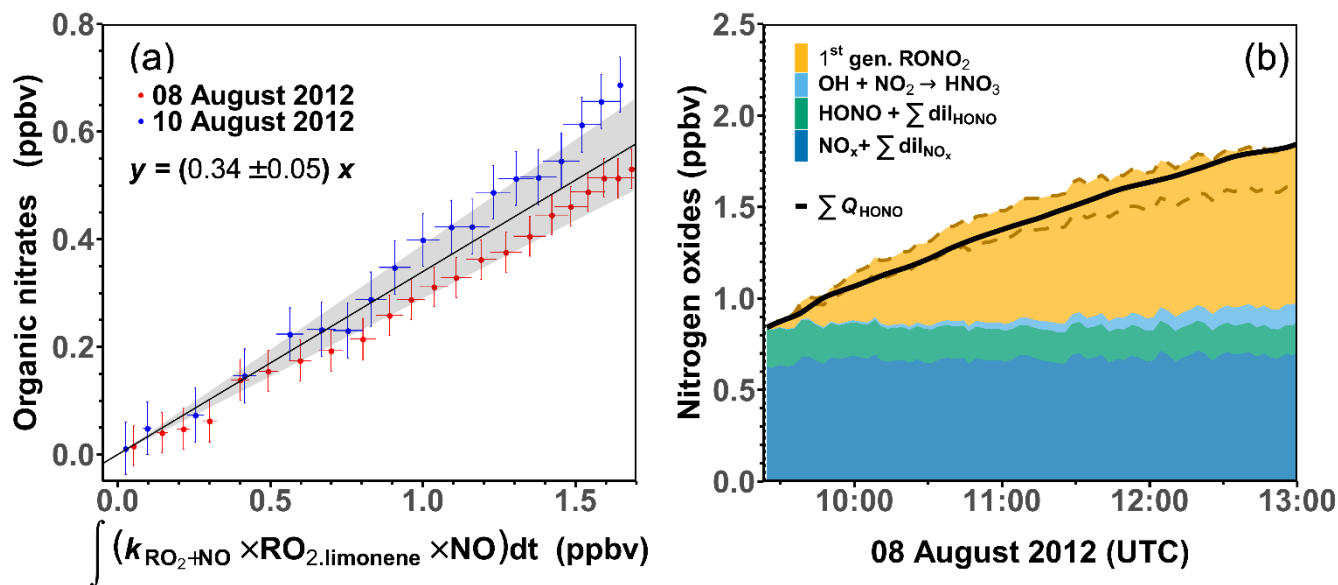
The fraction of RO<sub>2</sub> from limonene-OH oxidation to the measured total RO<sub>2</sub> concentration is estimated based on the ratio of  
 440 the OH reactivity from limonene to the OH reactivity from all OH reactants that are expected to produce RO<sub>2</sub> in the reaction with OH (Tan et al., 2021). The latter can be calculated by subtracting the background OH reactivity ( $k_{\text{OH}_{\text{bg}}}$ ) that includes the reactivities attributed to inorganic species and formaldehyde from the total measured OH reactivity ( $k_{\text{OH}}$ ):

$$[\text{RO}_{2\text{limonene}}] = \frac{k_{\text{OHlimonene}}}{k_{\text{OH}} - k_{\text{OH}_{\text{bg}}}} [\text{RO}_2] \quad (5)$$

Using Equation 3 and 4, the nitrate yield  $\Phi_{\text{limonene}+\text{OH}}$  is obtained as the slope of the linear regression between the calculated  
 445 organic nitrate concentrations and the integrated turnover rate of the reaction between RO<sub>2<sub>limonene</sub></sub> and NO. Only experiments with medium NO mixing ratios are used for this analysis here, as HONO measurements were performed and more than 90% of the limonene was oxidized by OH in these experiments. This results in a  $\Phi_{\text{limonene}+\text{OH}}$  of (34±5)% (Fig. 3). The

precision uncertainty (~15%) of  $\Phi_{\text{limonene}+\text{OH}}$  is determined by the precision of the measurements with linear error propagation. The error of  $\Phi_{\text{limonene}+\text{OH}}$  is estimated to be about 30%, which is mainly attributed to the accuracies of the reaction rate constants  $k_{\text{RO}_2+\text{NO}}$  (~30%) and the measurements of HONO (10%) and  $i_{\text{HONO}}$  (18%). ~~this calculation is mainly due to the accuracy of concentration measurements of  $\text{NO}_x$  species and radicals.~~ The organic nitrate yield of the  $\text{RO}_2$  from limonene ozonolysis is not determined in this study as a considerable amount of PANs could be formed according to the MCM model. Therefore the organic nitrate yield analysis is not conducted for the experiments at low  $\text{NO}$  mixing ratio.

The organic nitrate yield in this study is higher than values estimated using different SAR approaches of 19% (Jenkin et al., 2019) to 28% (Arey et al., 2001; Leungsakul et al., 2005). However, the value agrees well with nitrate yield derived in experiments, in which the yield was derived from the analysis of the aerosol chemical composition produced from the oxidation of limonene ((36±6)%; Rollins et al. (2010)).



**Figure 3.** (a) Regression between calculated organic nitrate mixing ratio and integrated turnover rate of the reaction of limonene-derived  $\text{RO}_2$  and  $\text{NO}$ . The regression only includes data when less than 60% of the limonene from the first injection reacted away. (b) Concentrations of nitrogen oxide species after the first limonene injection in the experiment with medium  $\text{NO}$  on 08 August 2012 compared to the total production of HONO from the chamber source. The organic nitrate contribution is calculated using a nitrate yield of (34±5)% for the reaction of limonene  $\text{RO}_2$  with  $\text{NO}$ , the uncertainty range is enclosed by the two dashed lines.

## 3.2 Comparison of modelled and measured concentration time series

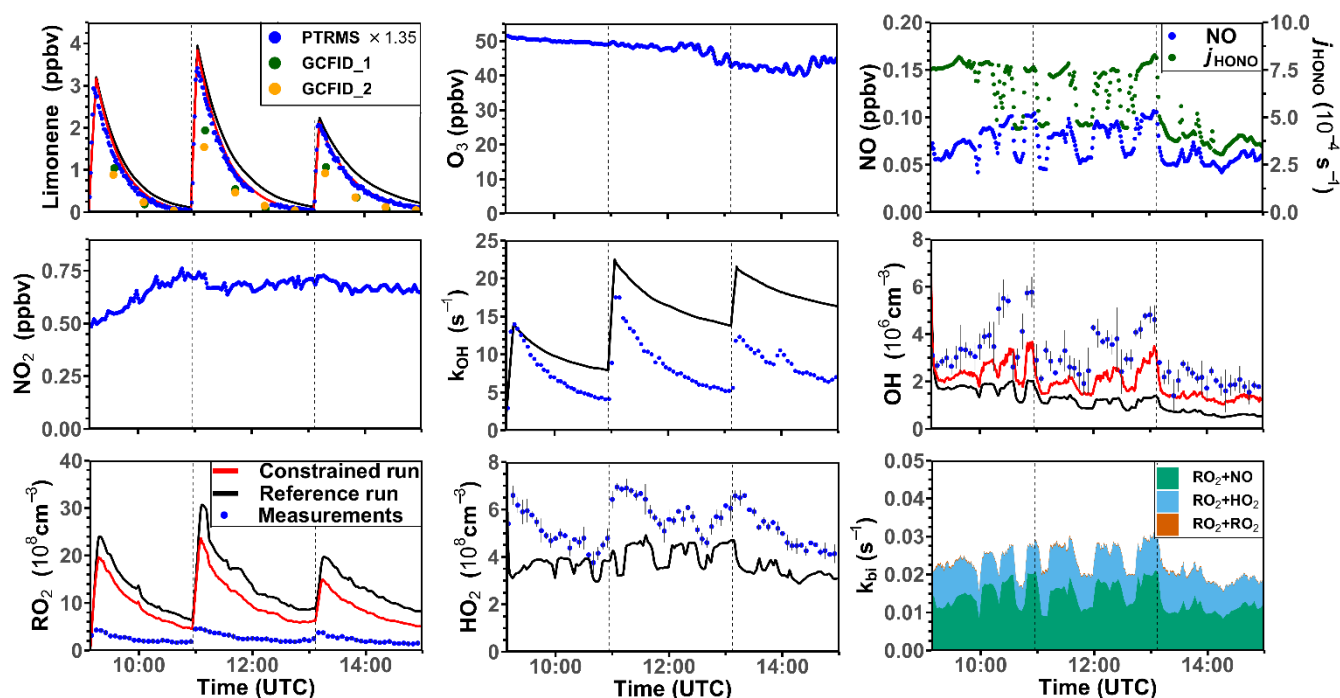
### 3.2.1 Model-measurement comparison for limonene photo-oxidation experiments at low NO mixing ratio

Three experiments were performed at low NO concentrations on 01 September 2012 (Fig. 4), 13 August 2015 and 04 July 2019 (Supplementary Material, Fig. S3 and S4). Measured OH concentrations during the limonene oxidation were about  $(2-7) \times 10^6 \text{ cm}^{-3}$  in the experiments in 2012 and about  $(5-11) \times 10^6 \text{ cm}^{-3}$  in the experiments in 2019. OH concentrations were highest, when most of the limonene was consumed. The overall higher OH concentrations in the experiments in 2019 were due to the higher NO mixing ratios ( $\sim 0.15$  ppbv) compared to the experiment in 2012 ( $\sim 0.05$  ppbv), which led to a faster OH production from the radical regeneration reaction of  $\text{HO}_2$  and NO. In these experiments, around 30 to 40% of limonene reacted with  $\text{O}_3$  and 60 to 70% of limonene reacted with OH. Measured  $\text{HO}_2$  concentrations were around  $(5-8) \times 10^8 \text{ cm}^{-3}$ . Measured  $\text{RO}_2$  concentrations were around  $(2-5) \times 10^8 \text{ cm}^{-3}$  in the experiment in 2012 and  $(5-10) \times 10^8 \text{ cm}^{-3}$  in the experiments in 2019, respectively. The average chemical lifetime of  $\text{RO}_2$  to bimolecular reactions with NO,  $\text{HO}_2$  and  $\text{RO}_2$  can be calculated using measured NO,  $\text{HO}_2$  and  $\text{RO}_2$  concentrations, respectively, resulting in a chemical lifetime of 25 to 50s. 60 to 70% of the  $\text{RO}_2$  radicals reacted with NO and 30 to 40% reacted with  $\text{HO}_2$ . Loss due to  $\text{RO}_2 + \text{RO}_2$  recombination reactions are predicted not to play a major role, if reaction rate constants are taken from the MCM that are much lower compared to the rate constants of the reactions with  $\text{HO}_2$ .

In the reference model run, which essentially uses the MCM chemistry without constraining radical production or destruction processes (Section 2.4), the OH reactivity is overestimated in the model by 3 to 5  $\text{s}^{-1}$  after nearly all limonene has reacted away. Right after the limonene injections,  $\text{HO}_2$  concentrations are underestimated by 20 to 50% and the  $\text{RO}_2$  concentrations are overestimated by 500 to 700%. OH is underestimated by at least 50%, which could partly result from the overestimation of the OH reactivity and underestimated  $\text{HO}_2$  concentration (and thereby the reaction rate of  $\text{HO}_2 + \text{NO}$ ). The underestimated OH concentration also leads to a slightly slower decay of the modelled limonene, so that modelled limonene concentrations are about 0.1 – 0.2 ppbv higher than measured values at the end of the experiment.

In the model run with adjusted OH reactivity and constrained  $\text{HO}_2$  concentration (constrained model run), the discrepancy between modelled and measured OH concentrations is reduced. They are still underestimated by 33% on average throughout the whole experiment and by about 50% one hour after the limonene injection, which could indicate a missing OH production process in the model. However, the temporal behaviour of the modelled limonene concentration agrees with the behaviour of the measurements, suggesting that measured OH concentrations are too high.

Maximum modelled  $\text{RO}_2$  concentrations are reduced by about 30% compared to the reference run as a result of the increased  $\text{HO}_2$  concentration in the constrained run leading to a higher  $\text{RO}_2$  loss by  $\text{RO}_2 + \text{HO}_2$  recombination reactions. However, this improvement is insufficient to explain measured  $\text{RO}_2$  concentrations, which are still at least a factor 4 lower than modelled values.



**Figure 4** Time series of radicals, inorganic and organic species in the limonene oxidation experiment with low NO mixing ratios on 01 September 2012. Limonene concentrations measured by the PTRMS are scaled by a factor of 1.35 to match the increase of OH reactivity during the injections of limonene. The vertical dashed lines represent times, when limonene was injected into the chamber. RO<sub>2</sub> bi-molecular reaction loss rates constants ( $k_{bi}$ ) are calculated based on the measured NO, HO<sub>2</sub>, and RO<sub>2</sub> concentrations using the reaction rate constants as included in the MCM. In the constrained model run HO<sub>2</sub> concentrations are constrained to measurements and the OH reactivity is adjusted by additional loss reactions to match measurements.

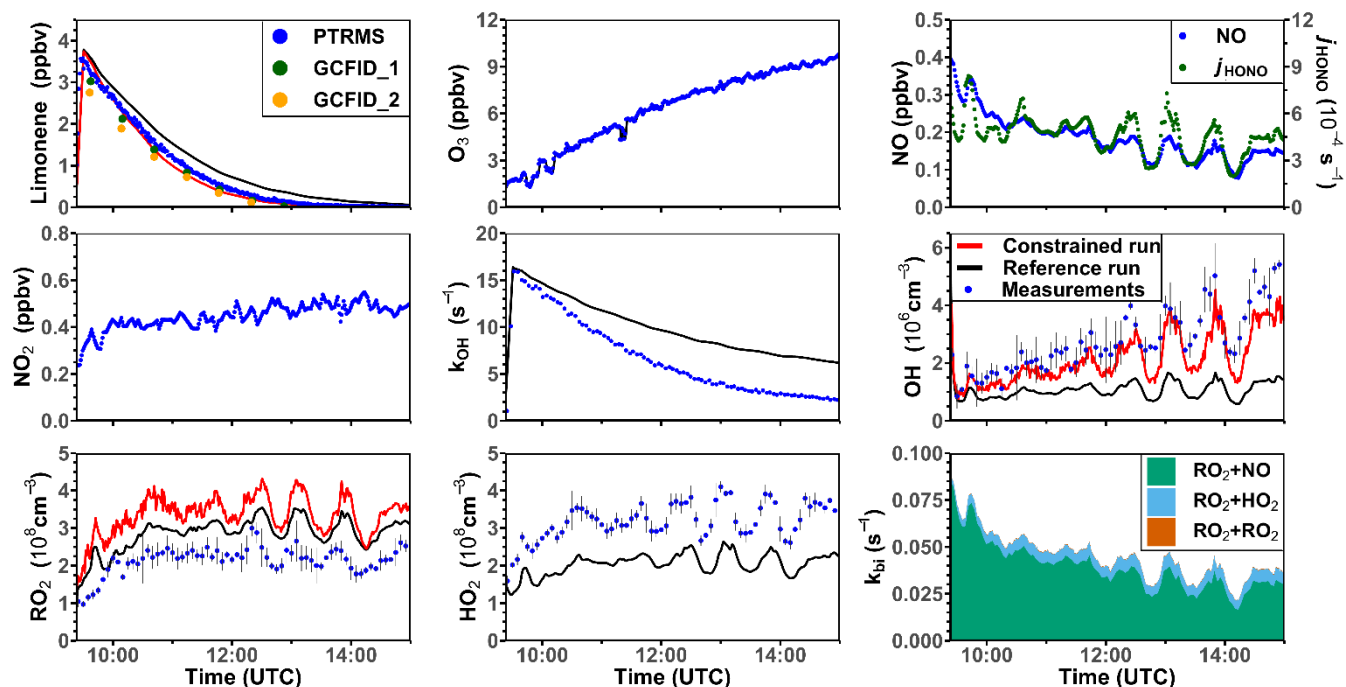
### 3.2.2 Model-measurement comparison for limonene photo-oxidation experiments at medium NO mixing ratios

Two oxidation experiments were performed at medium NO levels on 08 and 10 August 2012 (Fig. 5 and Supplementary Material Fig. S5). Throughout both experiments, measured NO mixing ratios ranged from 0.25 to 0.4 ppbv. More than 90% of the RO<sub>2</sub> derived from the limonene-OH reaction reacted with NO. O<sub>3</sub> mixing ratios increased gradually from about 1 ppbv to 10 ppbv as a result of the photolysis of NO<sub>2</sub>, which was produced from the reaction between organic peroxy radicals and HO<sub>2</sub> with NO. At such low O<sub>3</sub> concentrations, the reaction with OH was the dominant loss pathway for limonene (90%). The measured OH concentration ranged from  $(2-5) \times 10^6 \text{ cm}^{-3}$  and the measured HO<sub>2</sub> and RO<sub>2</sub> concentrations were about  $(2-5) \times 10^8 \text{ cm}^{-3}$ .

515 In the reference model run, the simulated OH reactivity increasingly deviates from measurements over the course of the experiment. The differences are about 2 to 4 s<sup>-1</sup> after two to three hours of oxidation when all limonene has been consumed. Contributors to the OH reactivity in the model in addition to limonene are mostly oxidation products such as aldehydes and ketones (~ 70%), organic peroxides (~ 15%) and organic nitrates (~ 15%) (Supplementary Material, Fig. S6). Simulated HO<sub>2</sub> concentrations are underestimated in the reference model run by around 10 to 30%. Hence, the simulated OH concentration is  
520 underestimated by 30 to 80% due to the slow regeneration rate from the reaction between HO<sub>2</sub> and NO as well as the faster removal rate of OH. As a result, limonene concentrations are overestimated by the model up to 0.3 ppbv throughout the experiment.

In the constrained model run, the simulated OH concentration is on average 20% lower than measured values. This difference is within the uncertainties of OH measurements. The higher modelled OH concentrations compared to the reference model run  
525 leads to a faster consumption of limonene compared to the reference model. This temporal behaviour better agrees with the temporal behaviour observed by PTRMS measurement, but the limonene consumption is slightly faster in the model than measurements suggests. Modelled RO<sub>2</sub> concentrations are 50 to 100% higher than measurements. Values are 10 to 20% higher compared to the reference model run right after the injection of limonene presumably due to the enhanced RO<sub>2</sub> production in the constrained model run, in which OH concentrations are higher.

530



**Figure 5.** Time series of radicals, inorganic and organic species in the limonene oxidation experiment at medium NO level on 08 August 2012. RO<sub>2</sub> bi-molecular reaction loss rate constants ( $k_{bi}$ ) are calculated based on the measured NO, HO<sub>2</sub>, and RO<sub>2</sub> concentrations using the reaction rate constants from the MCM. In the constrained model run HO<sub>2</sub> concentrations are constrained to measurements and the OH reactivity is adjusted by additional loss reactions to match measurements.

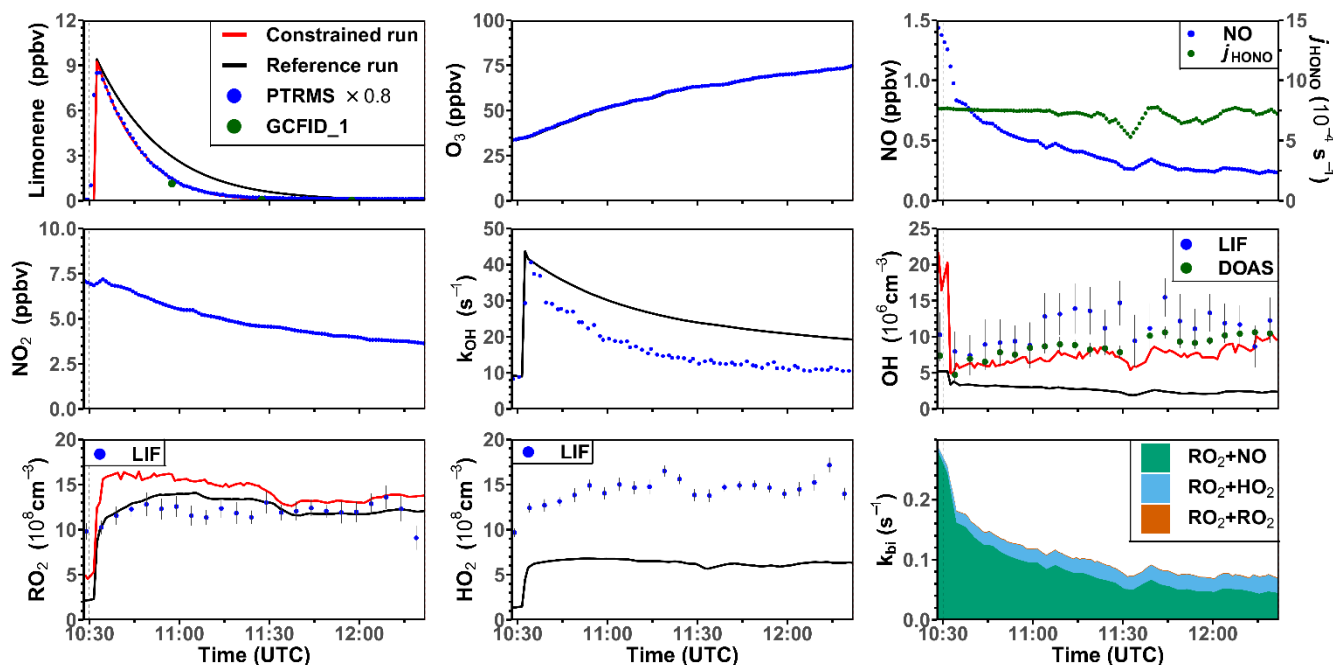
### 3.2.3 Model-measurement comparison for limonene photo-oxidation experiment at high NO mixing ratios

One experiment was performed with high NO mixing ratios on 03 August 2015. In this experiment, limonene was injected twice. Unfortunately, measurements of radicals failed during the first part of the experiment, so that only the part of the experiment after the second limonene injection can be analysed (Fig. 6). The ozone mixing ratio at the beginning of this part of the experiment was about 35 ppbv as a result of ozone production during the first part of the experiment. The OH concentration measured by DOAS was around  $(5-10) \times 10^6 \text{ cm}^{-3}$ , so that around 70% and 30% of limonene reacted with OH and O<sub>3</sub>, respectively. The OH concentration measured by LIF was around  $(5-15) \times 10^6 \text{ cm}^{-3}$ . The HO<sub>2</sub> concentration was about  $1 \times 10^9 \text{ cm}^{-3}$  throughout the experiment. The high NO and HO<sub>2</sub> concentrations led to a short RO<sub>2</sub> lifetime of 5 to 10 s, much shorter than in the other experiments with lower NO concentrations. The removal of RO<sub>2</sub> by bimolecular reactions was mostly due to the reaction with NO (85 %) and HO<sub>2</sub> (15 %).

In the reference model run, the model-measurement discrepancy of the OH reactivity is around  $3 \text{ s}^{-1}$  before the second limonene injection, and it further increases to  $10 \text{ s}^{-1}$  at the end of the experiment. The absolute discrepancy in OH reactivity is higher compared to other experiments because the total amount of limonene and therefore the production of oxygenated products was higher. Modelled OH and  $\text{HO}_2$  concentrations are both lower by 50 to 70% than the measured values. The low OH concentration in the model again leads to a slower decay of modelled limonene concentrations compared to observed values.  $\text{RO}_2$  concentrations show a good agreement with the measurement, with a discrepancy of less than 20%.

In the constrained model run, the simulated OH concentration is in good agreement with the measurement by DOAS in the first hour and only slightly underestimates the measurements by about 20% at the end of the experiment. As a result, the agreement between modelled and measured time series of limonene concentrations improves compared to the reference model run. Differences between  $\text{RO}_2$  concentrations in the constrained and reference model are rather small except for the point in time when limonene is injected and  $\text{RO}_2$  concentrations in the constrained model run increase more rapidly than observations.

This results in 30% difference between modelled and measured values during the first hour of the experiment. This can be explained by the increased  $\text{RO}_2$  production from the limonene oxidation by the OH radical which ~~concentration~~ is underestimated in the reference model run. Possible reasons for the overestimated  $\text{RO}_2$  concentration could include an underestimated loss rate of  $\text{RO}_2$  at NO mixing ratio of about 1 ppbv (Section 3.4), or an overestimated production of  $\text{RO}_2$  from the further oxidation of products from the previous limonene injection.



**Figure 6.** Time series of radicals, inorganic and organic species during the limonene oxidation experiment at high NO mixing ratios on 03 August 2015. Limonene concentrations measured by the PTRMS are scaled by a factor of 0.8 to match the increase of OH reactivity during the injection of limonene. RO<sub>2</sub> bi-molecular reaction loss rate constants ( $k_{bi}$ ) are calculated based on the measured NO, HO<sub>2</sub>, and RO<sub>2</sub> concentrations using the reaction rate constants from the MCM. In the constrained model run HO<sub>2</sub> concentrations are constrained to measurements and the OH reactivity is adjusted by additional loss reactions to match measurements.

### 3.2.4 Model-measurement comparison for limonene ozonolysis experiment in the dark with and without OH scavenger

The ozonolysis of limonene in the dark was investigated in a separate experiment on 05 June 2020 (Fig. 7). A significant OH concentration was observed with values up to  $1.2 \times 10^6 \text{ cm}^{-3}$  after the first injection of limonene as a result of the OH production from the ozonolysis reaction. OH concentrations were below the limit of detection of both DOAS and LIF after 100 ppmv CO had been injected as OH scavenger right before the second limonene injection. The measured HO<sub>2</sub> concentration was around  $3 \times 10^8 \text{ cm}^{-3}$  after the first limonene injection and increased to maximum concentrations of  $1 \times 10^9 \text{ cm}^{-3}$  after the second limonene injection due to the conversion of OH radicals formed from the ozonolysis in the reaction with excess CO. Because there was no limonene oxidation by OH, there was also less production of RO<sub>2</sub> radicals than the first limonene injection. However, the observed maximum RO<sub>2</sub> concentration after each limonene injection was about  $1 \times 10^9 \text{ cm}^{-3}$ .

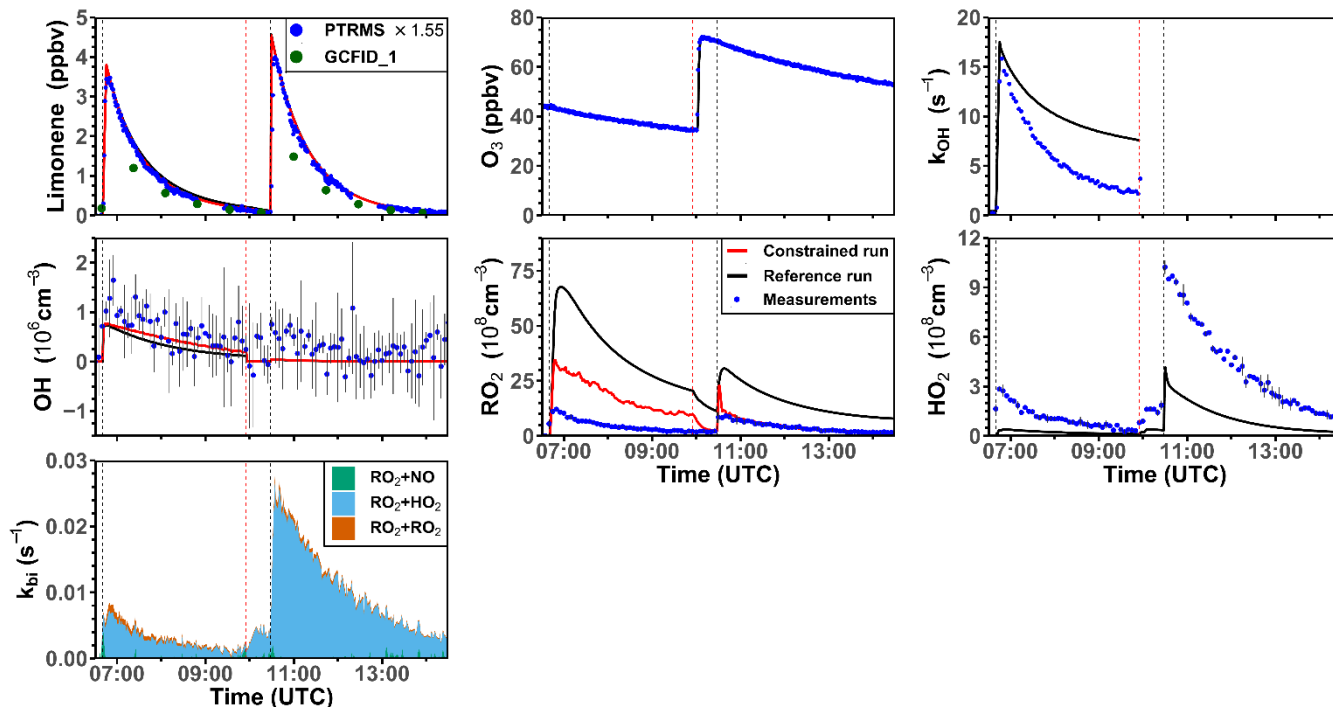
Similar as observed in the other experiments, modelled OH reactivity is higher than measured values by  $5 \text{ s}^{-1}$ . The maximum discrepancies appear right before the injection of CO, after which OH reactivity could not be measured due to the high contribution of CO. In the reference model run, HO<sub>2</sub> is underestimated by the model by around 90% during the first part of the experiment and modelled HO<sub>2</sub> is also a factor of three lower than measurements during the pure ozonolysis part in the presence of CO as OH scavenger. In contrast, measured RO<sub>2</sub> concentrations are drastically overestimated by the model by a factor of 7 right after each limonene injection.

In the constrained model run, simulated OH concentrations are 25% higher compared to the reference model as a result of the reduced OH reactivity in the model. The main difference between the results of the reference model run and the constrained model run is that RO<sub>2</sub> concentrations are reduced by half in the constrained model. This is caused by an increased RO<sub>2</sub> removal rate by the high HO<sub>2</sub> concentration.

Using measured RO<sub>2</sub> and HO<sub>2</sub> concentrations, the maximum reaction rate constants of the reaction of RO<sub>2</sub> with HO<sub>2</sub> ~~is-are~~ about  $0.005 \text{ s}^{-1}$  and  $0.02 \text{ s}^{-1}$  for the first and second limonene injection, respectively. In contrast, the RO<sub>2</sub> loss rate constant due to the recombination of organic peroxy radicals is calculated to be only  $0.001 \text{ s}^{-1}$ , so that it is expected that RO<sub>2</sub> reacted mainly with HO<sub>2</sub> to form peroxides, if only bimolecular reactions are considered. However, the loss due to RO<sub>2</sub>-RO<sub>2</sub> reactions could be of similar importance as the loss due to RO<sub>2</sub>-HO<sub>2</sub> reactions, if low HO<sub>2</sub> and high RO<sub>2</sub> concentrations as predicted by the



reference model run are used for the calculation. The large discrepancies between measured and modelled  $\text{RO}_2$  and  $\text{HO}_2$  radical  
 600 concentrations and possible explanations are further discussed in Sections 4.1 and 4.2.



**Figure 7.** Time series of radicals, inorganic and organic species during the limonene ozonolysis experiment in the dark on 05  
 June 2020. Limonene concentrations measured by the PTRMS are scaled by a factor of 1.55 to match the increase of OH  
 605 reactivity during the injection of limonene. The black vertical dashed lines represent when limonene was injected into the  
 chamber; the red vertical dashed line represents the injection of 100 ppmv of CO.  $\text{RO}_2$  bi-molecular reaction loss rate constants  
 ( $k_{bi}$ ) are calculated based on the measured NO,  $\text{HO}_2$ , and  $\text{RO}_2$  concentrations using the reaction rate constants in the MCM. In  
 the constrained model run  $\text{HO}_2$  concentrations are constrained to measurements and the OH reactivity is adjusted by additional  
 loss reactions to match measurements.

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### 3.3 Chemical OH radical budget using measured quantities

To evaluate whether unaccounted chemical processes are required to explain the total OH destruction rate in the experiments,  
 the rates of OH-producing reactions are calculated using measured trace gas and radical concentrations. Turnover rates of

single reactions are summed up and compared to the total OH destruction rate. Due to the short chemical lifetime of OH radicals ( $< 1$  s) steady-state conditions are expected that the production and destruction rates must be balanced.

The total OH destruction rate is obtained by computing the product of the measured OH reactivity and OH concentration. In experiments in year 2015, when OH was measured by both DOAS and LIF instruments, DOAS measurements are used for the calculation of total OH destruction rate. The uncertainty of the OH destruction rate is 16% calculated by error propagation of the measurement uncertainties. The main OH production processes included in the chemical budget analysis are listed in Table 4. OH production by photolysis of HONO and  $O_3$ , the reaction between  $HO_2+NO$ , and between  $HO_2+O_3$ , and the limonene ozonolysis reaction are considered. The uncertainties of these OH-producing processes range from 15% (photolysis processes) to 20% ( $HO_2+NO$  reaction and limonene ozonolysis reaction), which are derived from error propagation of the uncertainties of measurements (Table 1) and reaction rate constants (Atkinson et al., 2004; Cox et al., 2020).

Figure 8 and Figure S7 show the chemical budgets of OH radicals in the limonene oxidation experiments with different NO mixing ratios. The destruction and production rates of OH for experiments with medium (08 August 2012) and high NO (03 August 2015) are balanced within the uncertainties of measurements during all experiments. This is consistent with the overall good agreement between modelled and measured OH radical concentrations obtained for the constrained model run (Fig. 5 and 6). In the experiment with high NO, the total OH turnover rate is higher ( $> 20$  ppbv  $h^{-1}$ ) compared to the other experiments due to the high limonene concentration (10 ppbv) and the high NO concentration, both of which accelerate the turnover of radicals.

In experiments with medium and high NO concentrations, the main OH source after the limonene injection is the reaction between  $HO_2$  and NO ( $>85\%$ ), followed by the photolysis of HONO in the experiment with medium NO, and ozone photolysis and limonene ozonolysis in the experiment with high NO, when 60ppbv  $O_3$  was present. In total, about 85 to 100% of the OH radical production rate can be explained by the calculated processes that are listed in Table 4.

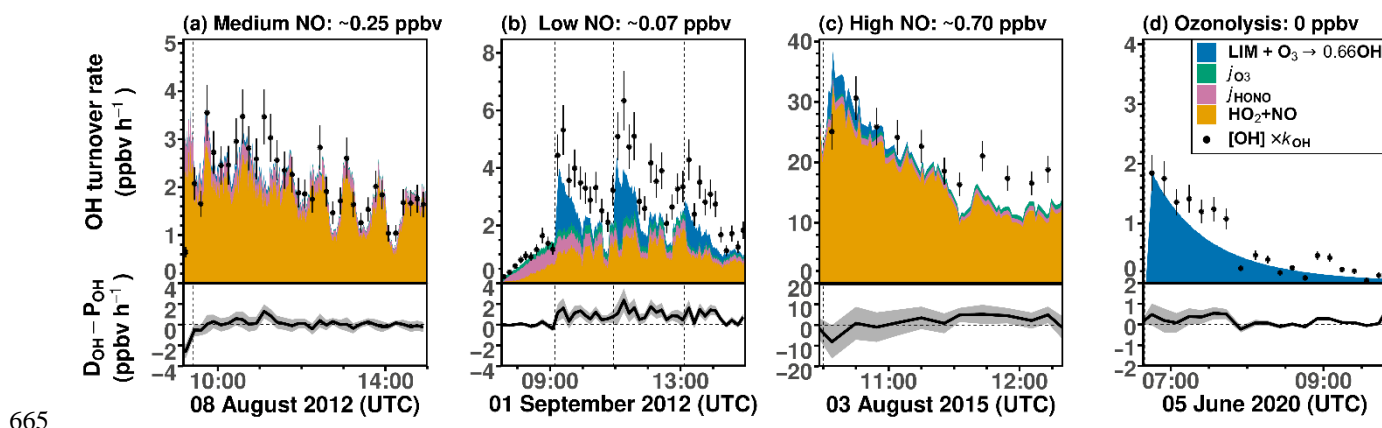
In the experiment with low NO on 01 September 2012 (Fig. 8b), the OH production rate is 6 ppbv  $h^{-1}$  after the injection of limonene, of which about 33% can be attributed to OH production from limonene ozonolysis. The NO concentration varies over the course of the experiment making OH regeneration from the  $HO_2+NO$  reaction an important OH source with a contribution of 15 – 50% to the total OH production in addition to OH production from the photolysis of HONO and  $O_3$ . About 1.0 ppbv  $h^{-1}$  (20 – 33%) of the OH destruction rate is not explained by these OH production processes, which is consistent with the underestimation of OH concentrations in the constrained model run compared to measured values (Fig. 4). However, the gap between the OH destruction rate and destruction rate is about 1 ppbv  $h^{-1}$  throughout the whole experiment and does not vary with the amount of limonene presence in the chamber. This suggests that either the missing OH source is not related to the oxidation of limonene or is due to measurement artefacts for example in the OH measurements, which would lead to an overestimation of the OH destruction rate. An artefact in the OH measurement would also be consistent with what is observed

645 in the constrained model run (Fig. 4), where the rapid decrease of the modelled limonene concentration suggests that the measured OH is too high in this experiment.

In the ozonolysis experiment without OH scavenger (Fig. 8d), OH is only produced by ozonolysis reaction of limonene. In the ozonolysis experiment, prior to the addition of CO as an OH scavenger (Fig. 8d), OH is only produced by the ozonolysis of limonene. The total OH production rate is about 2 to 3 ppbv h<sup>-1</sup> at the beginning of the oxidation and gradually declines while  
650 limonene is being consumed. The total OH destruction rate is well explained by the production from limonene ozonolysis suggesting that OH production from further ozonolysis reactions of product species is not significant for conditions of this experiment.

In conclusion, the OH production rate from the four major OH sources that are included in the calculations (Table 4) is balanced by the OH destruction rate within the 25% uncertainty of the calculation at the beginning of the experiment, when limonene-  
655 oxidation is most important in the experiments with medium and high NO and in the ozonolysis experiment. In the experiments with low NO concentrations, imbalances of 20 to 33% are observed indicating that an additional OH production process with a rate of 1.0 ppbv h<sup>-1</sup> would be required to explain the observed destruction rate, but there are indications that this could be due to a measurement artefact in the OH measurements.

In all experiments, the OH production rates are lower than OH destruction rates at later times of the experiments, when  
660 secondary chemistry becomes important. However, differences are similar to the uncertainty of the calculations. These discrepancies may indicate that additional OH could be produced from unaccounted reactions of oxidation products for example from the photolysis of organic peroxides in the photo-oxidation experiments (Badali et al., 2015).



665

**Figure 8.** 10-minutes-average values of total OH destruction rates compared to the sum of OH production rates from the major OH sources that can be calculated from measurements in the (a) medium NO, (b) low NO, (c) high NO, and (d) ozonolysis

experiments. Shaded areas in the difference plots give the uncertainties of the calculations. Production of OH from the reaction of O<sub>3</sub> and HO<sub>2</sub> is not included, because the contribution to the total OH production was negligible (< 0.01 ppbv h<sup>-1</sup>) for conditions of the experiments.

**Table 4.** Reactions that are included in the analysis of the OH production rate. Reaction rate constants are given for 298K and 1 atm. The reaction rate constants that are used in the analysis are calculated for the measured temperature.

Reaction:	<i>k</i> (298 K, 1 atm)	1σ uncertainty of <i>k</i> (%)	Reference:
HO <sub>2</sub> + NO → OH + NO <sub>2</sub>	$8.8 \times 10^{-12} \text{ cm}^3 \text{ s}^{-1}$	11	Atkinson et al. (2004)
HO <sub>2</sub> + O <sub>3</sub> → OH + 2O <sub>2</sub>	$2.0 \times 10^{-15} \text{ cm}^3 \text{ s}^{-1}$	22	Atkinson et al. (2004)
HONO + <i>hν</i> → OH + NO	<i>j</i> <sub>HONO</sub>	10	Measured
O <sub>3</sub> + <i>hν</i> → O( <sup>1</sup> D) + O <sub>2</sub>	<i>j</i> <sub>O<sub>3</sub></sub>	10	Measured
O( <sup>1</sup> D) + H <sub>2</sub> O → 2OH	$2.1 \times 10^{-10} \text{ cm}^3 \text{ s}^{-1}$	11	Atkinson et al. (2004)
O( <sup>1</sup> D) + M → O( <sup>3</sup> P) + M	$2.6 \times 10^{-11} \text{ cm}^3 \text{ s}^{-1}$	11	Atkinson et al. (2004)
Limonene + O <sub>3</sub> → 0.66RO <sub>2</sub> + 0.66OH	$2.1 \times 10^{-16} \text{ cm}^3 \text{ s}^{-1}$	11	Cox et al. (2020)

### 3.4 Chemical budget of first-generation peroxy radicals using measured quantities

The discrepancies between measured and simulated organic peroxy radical concentrations are much higher (up to a factor of 2) in the experiments with low NO concentrations and in the ozonolysis experiment compared to the experiments with medium or high NO concentrations. The analysis of the composition of the RO<sub>2</sub> concentrations using model results from the constrained model run (Section 2.4) shows that the concentrations of RO<sub>2</sub> produced in the initial reaction of limonene with OH and O<sub>3</sub> already exceed the measured total RO<sub>2</sub> concentrations (Fig. 9 and Supplementary Material Fig. S8). Model-measurement percentage differences are at least a factor of 2 higher than the accuracy of the measured RO<sub>2</sub> concentration (~25%). Therefore, the discrepancy suggests that additional loss pathways for RO<sub>2</sub> have to be included in the model.

To examine the magnitude of the additional RO<sub>2</sub> loss rate, a chemical budget analysis for RO<sub>2</sub> radicals is performed similarly to the analysis for OH radicals (Section 3.3). As the chemical loss rate constants of peroxy radicals are within the range of 0.01 to 0.20 s<sup>-1</sup>, steady-state concentrations can be assumed. The production rate of the peroxy radicals produced right after the limonene injection is well-defined by the loss rate of limonene due to the reactions with OH<sup>-</sup> and O<sub>3</sub>. Therefore, only measurements during the first 30 minutes after the first limonene injection are used for the analysis, so that calculations are not impacted much by additional RO<sub>2</sub> production from the subsequent oxidation of organic products. The removal rate constant of peroxy radicals includes bimolecular reactions ( $k_{bi}$ ):

$$k_{bi} = k_{RO_2+RO_2}[RO_2] + k_{RO_2+HO_2}[HO_2] + k_{RO_2+NO}[NO] \quad (6)$$

Values of the bimolecular reaction rate constants in the MCM for limonene-derived RO<sub>2</sub> radicals are:  $k_{RO_2+RO_2}$  ranging from 10<sup>-13</sup> to 10<sup>-12</sup> cm<sup>3</sup> s<sup>-1</sup>,  $k_{RO_2+HO_2} = 2.3 \times 10^{-11}$  cm<sup>3</sup> s<sup>-1</sup> at 298K,  $k_{RO_2+NO} = 9.0 \times 10^{-12}$  cm<sup>3</sup> s<sup>-1</sup> at 298K. The additional loss rate constant ( $k_{add}$ ) required to balance production ( $P_{RO_2}$ ) and destruction ( $L_{RO_2}$ ) rates can be calculated as:

$$L_{RO_2} = [RO_2](k_{bi} + k_{add}) = (0.66 \times k_{lim+O_3}[O_3] + k_{lim+OH}[OH])[lim] = P_{RO_2} \quad (7)$$

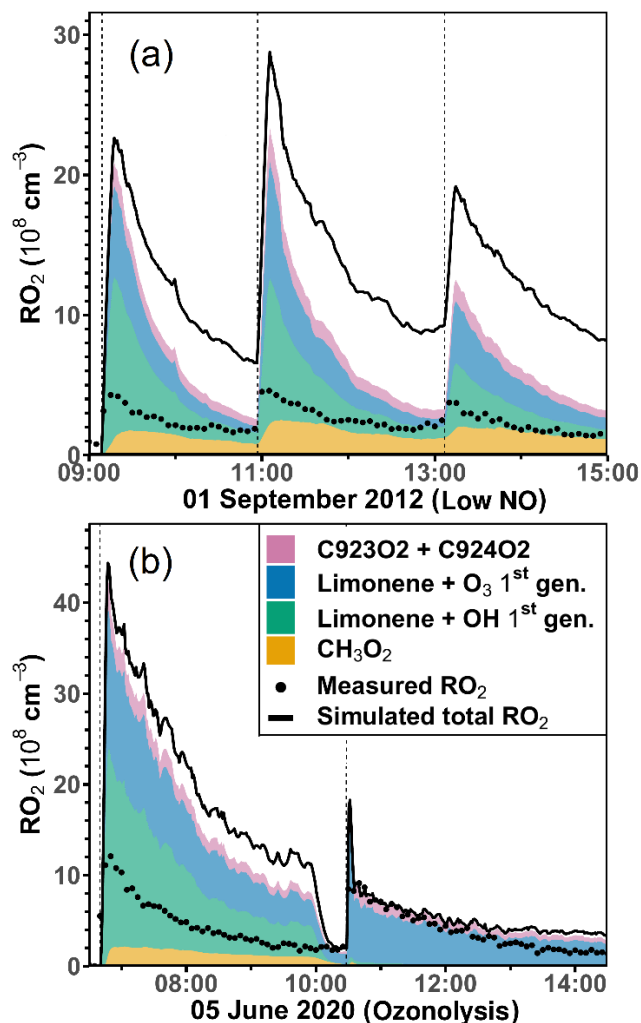
$$k_{add} = P_{RO_2}[RO_2]^{-1} - k_{bi} \quad (8)$$

In this calculation, measured concentrations of radicals and trace gases are used. The RO<sub>2</sub> yield of 0.66 from the limonene ozonolysis reaction assumes RO<sub>2</sub> radicals are produced from the vinyl hydroperoxide (VHP) mechanism together with an OH radical (Wang and Wang, 2021).

Results from the five experiments are summarized in Table 5. The values of the additional loss rate constant,  $k_{add}$ , range from 0.01 to 0.06 s<sup>-1</sup> in different experiments, but are similar with the high relative uncertainty of at least 50%. The large relative uncertainty is caused by the small differences between production and destruction rates, which also increase with increasing RO<sub>2</sub> and NO concentrations (and thereby  $k_{bi}$ ). The relative uncertainties of the additional loss are less than 100% in only three experiments, which include the ozonolysis experiment (05 June 2020), the experiments with low (01 September 2012), and medium NO concentrations (08 August 2012). In the ozonolysis experiment, the additional RO<sub>2</sub> loss is lower by a factor of 4 than in the other 2 experiments. The large difference in  $k_{add}$  could be attributed to the different RO<sub>2</sub> species that are formed from the photooxidation reaction and the ozonolysis reaction. RO<sub>2</sub> formed from the photo-oxidation reaction have retain their 6-member ring moiety, whereas the majority of RO<sub>2</sub> formed from the ozonolysis reaction are acyclic. In addition, This might be explained by the low temperature during this the ozonolysis experiment, which may could slow down the additional loss pathway. Another explanation could be the high fraction of RO<sub>2</sub> from limonene ozonolysis, which may behave differently from the RO<sub>2</sub> from the OH reaction with limonene.

Potential additional loss pathways of RO<sub>2</sub> radicals that are needed to balance the RO<sub>2</sub> production rate in the experiments would be radical conversion reactions that can also lead to the production of OH radicals, so that these pathways are potentially connected to imbalances found in the chemical budget of OH radicals (Section 3.3). It is worth noting that discrepancies in the

chemical budgets of RO<sub>2</sub> and OH radicals are both smaller in the ozonolysis experiment compared to the photochemistry experiments at low and medium NO mixing ratios.



**Figure 9.** Total RO<sub>2</sub> radical concentrations and their speciation from model calculations (constrained model run) compared to the measured values (black dots) for the experiments with low NO (a) and the ozonolysis (b) experiment. Methylperoxy radicals (CH<sub>3</sub>O<sub>2</sub>) are mainly produced from the oxidation of HCHO. Radicals produced in the initial reactions of limonene with either OH or O<sub>3</sub> are summed. C923O<sub>2</sub> + C924O<sub>2</sub> are RO<sub>2</sub> radicals produced from the further oxidation of the first-generation oxidation products. Names are taken from the MCM model.

**Table 5.** Additional removal rate constants ( $k_{\text{add}}$ ) that are required to balance the RO<sub>2</sub> production and destruction rates in the different experiments together with conditions of the experiments such as the percentage of limonene that reacted with OH (LIM+OH) or O<sub>3</sub> (LIM+O<sub>3</sub>). Only data from 30 minutes after the first limonene injection is analysed.

NO	Date	T (K)	LIM+OH (%)	LIM+O <sub>3</sub> (%)	$P_{\text{RO}_2}$ (10 <sup>7</sup> cm <sup>-3</sup> s <sup>-1</sup> )	[RO <sub>2</sub> ] (10 <sup>8</sup> cm <sup>-3</sup> )	$k_{\text{bi}}$ (10 <sup>-2</sup> s <sup>-1</sup> )	$k_{\text{add}}$ (10 <sup>-2</sup> s <sup>-1</sup> )
Zero	05 June 2020	286	49	51	2.3 ± 0.6	10.0 ± 1.4	0.9 ± 0.3	1.4 ± 0.7
Low	01 September 2012	313	59	41	2.8 ± 0.8	3.5 ± 0.5	2.5 ± 0.7	5.6 ± 2.7
Low	04 July 2019	302	72	28	3.1 ± 0.9	6.4 ± 1.0	3.1 ± 0.9	1.7 ± 1.7
Medium	08 August 2012	303	97	3	1.7 ± 0.5	1.4 ± 0.2	6.9 ± 2.1	5.2 ± 3.5
Medium	10 August 2012	302	95	5	1.8 ± 0.5	1.6 ± 0.2	8.2 ± 2.7	3.3 ± 4.2

### 3.5 Impacts of RO<sub>2</sub> model results on the modelled NO<sub>x</sub> concentrations

In the model runs described so far, NO and NO<sub>2</sub> concentrations are constrained to measured values. If these are not constrained, NO<sub>x</sub> is underestimated at the beginning of the experiments, but values are overestimated at the end (Fig. 10 and Supplementary Material Fig. S9). The discrepancy at the beginning can be mainly attributed to the overestimation of modelled RO<sub>2</sub> concentration, which leads to an overestimation of the formation of organic nitrates that act as sinks for NO<sub>x</sub> on the timescale of the experiments. To illustrate the impact of RO<sub>2</sub> concentrations on the modelled NO<sub>x</sub> concentrations, two model runs are compared: one with modelled RO<sub>2</sub> concentrations (reference run) and the second with modelled RO<sub>2</sub> concentrations adjusted to match the measurements.

RO<sub>2</sub> concentrations are adjusted by applying an additional loss with a constant-fixed rate constant ~~to-for~~ all six first-generation RO<sub>2</sub> derived from -OH and -O<sub>3</sub> oxidation (Fig. 1). The additional loss rate constant for RO<sub>2</sub> is around 0.01 to 0.06 s<sup>-1</sup>, similar to the loss rate constant derived in the analysis of the chemical budget for RO<sub>2</sub> ( $k_{\text{add}}$ , Section 3.4). In both model runs, the organic nitrate yield of the RO<sub>2</sub>+NO reaction for the first-generation RO<sub>2</sub> radicals from limonene+OH is adjusted to the yield (34%) that is found in the analysis of the experiments at medium NO mixing ratio (Section 3.1.2). Measured  $j_{\text{NO}_2}$ , O<sub>3</sub> and HO<sub>2</sub> concentrations are used in both model runs to constrain the loss rate of NO<sub>2</sub> and NO. It should be noted that only data within one hour after the first limonene injection is evaluated as RO<sub>2</sub> produced from the further oxidation of organic products are not considered.

Figure 10 shows the modelled NO and NO<sub>x</sub> concentrations for the two model runs. In the experiment with medium NO concentrations on 08 August 2012, RO<sub>2</sub> radical concentrations are overestimated by about 50 – 100% by the reference model

750 and modelled NO as well as NO<sub>x</sub> concentrations; are 25% lower than measurements. With an additional RO<sub>2</sub> loss rate constant of 0.05 s<sup>-1</sup> (Table 5), the fraction of RO<sub>2</sub> that reacts with NO reduces from 80 – 90% to 45 – 60%. Therefore, the loss of NO<sub>x</sub> by the formation of organic nitrates is also reduced, so that the model-measurement agreement for NO and NO<sub>x</sub> improves for the first two hours of the experiments.

755 Both model runs overestimate the NO<sub>x</sub> and NO concentrations; when all limonene reacted away after 13:00 UTC (Fig. 5). The measured NO<sub>x</sub> concentration remains stable at around 0.6 ppbv throughout the whole experiment after the injection of limonene. However, NO<sub>x</sub> concentrations increase at a rate of about 0.15 ppbv h<sup>-1</sup> in the reference model. The increase is reduced to less than 0.05 ppbv h<sup>-1</sup> in the model run with the additional RO<sub>2</sub> loss during the last two hours of the experiment. The production of NO<sub>x</sub> in the model at later times of the experiment can be explained by the production of NO<sub>2</sub> from the photolysis of the first-generation organic nitrates and their oxidation by OH. These effects are more important in the reference model run, when  
760 the modelled first-generation organic nitrates are high. To reconcile the difference in NO<sub>x</sub> concentrations between the model and measurements, a stronger nitrogen sink is required in the model. This may also suggest that the model underestimates the organic nitrate formation from the reaction of NO with RO<sub>2</sub> from the oxidation of product species. Another explanation would be that the lifetime of limonene-derived organic nitrates from OH-oxidation is too short in the model.

In the experiment with low NO concentrations on 01 September 2012, the fraction of RO<sub>2</sub> that reacts with NO reduces from  
765 about 50% to 16%; if an additional RO<sub>2</sub> loss with a rate constant of 0.06 s<sup>-1</sup> (Table 5) is applied. In this experiment, a large fraction of NO<sub>x</sub> in the model is lost due to the formation of PAN or PAN-like species from acyl peroxy radicals (e.g., CH<sub>3</sub>CO<sub>3</sub> and C<sub>8</sub>H<sub>15</sub>CO<sub>3</sub>) that are formed in the radical chain reaction of the ozonolysis reaction of limonene (Fig. 1). The additional loss of the initially formed RO<sub>2</sub> species competes with the reaction with NO<sub>2</sub> and therefore the formation of PAN reduces, if the additional loss is applied. This effect of reduced NO<sub>x</sub> loss in the ozonolysis reaction adds to the effect for a reduced organic  
770 nitrate formation discussed for the experiment on 08 September 2012 at medium NO.

Although the reduced NO<sub>x</sub> loss significantly improves the model-measurement agreement for the first part of the experiments, if an additional RO<sub>2</sub> loss process is included in the model, NO<sub>x</sub> concentrations are overestimated by this model at later times, when the chemistry of product species gains in importance. This could be due to neglecting the impact of the subsequent chemistry of the additional RO<sub>2</sub> loss reactions on nitrogen oxide concentrations. The chemistry of nitrogen oxide species in  
775 the experiment with low NO concentrations is more complex compared to the experiment with medium NO as a significant fraction of RO<sub>2</sub> radicals is produced by the ozonolysis of limonene in addition to the reaction with OH. Further investigation will be required to specifically clarify the impact of the formation of PAN and PAN-like species from the ozonolysis of limonene (Fig. 1). To our best knowledge, there is no experimental study investigating PAN formation from the oxidation of limonene.

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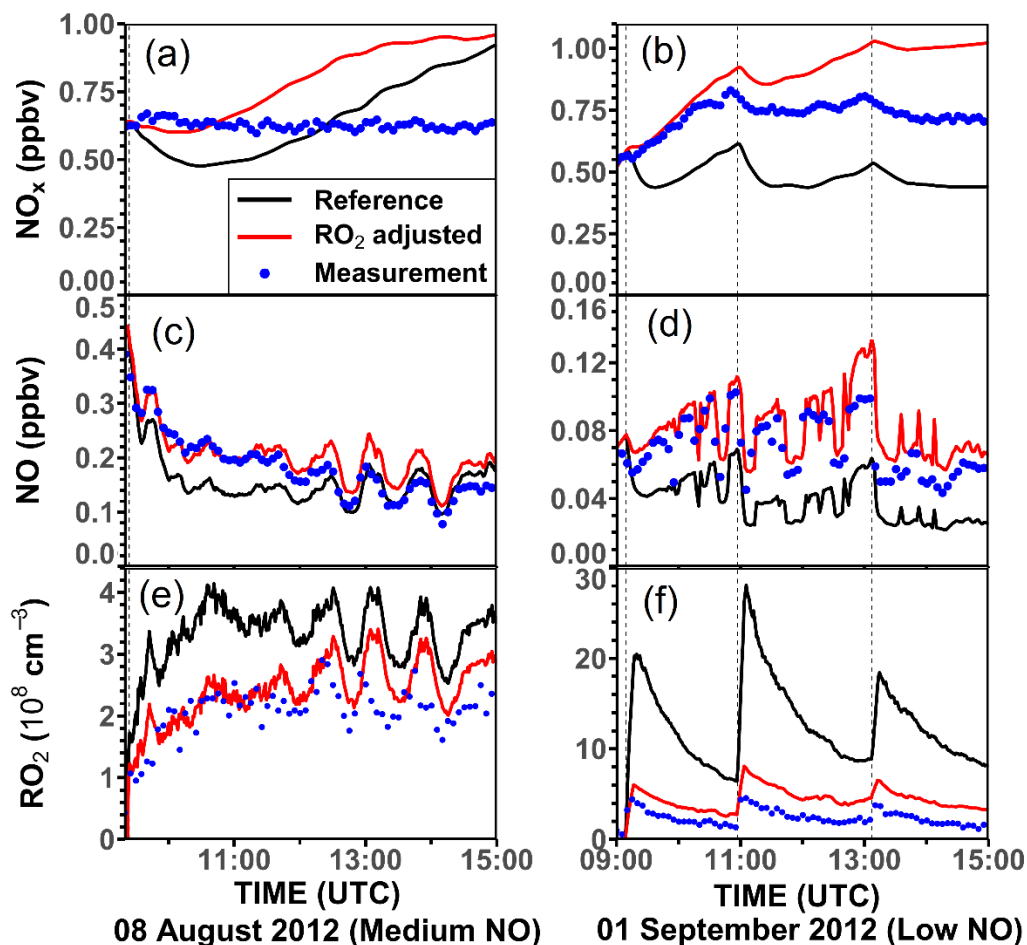


Figure 10. Example of the impact of too high modelled  $\text{RO}_2$  (e and f) on the modelled  $\text{NO}_x$  (a and b) and  $\text{NO}$  (c and d) concentrations in the experiments with medium  $\text{NO}$  (08 August 2012) and low  $\text{NO}$  (01 September 2012) concentrations. In both cases, the organic nitrate yield of 34% from the reaction of  $\text{NO}$  with first-generation  $\text{RO}_2$  from the limonene+OH reaction is taken from the analysis in this work.

## 4 Discussion

### 4.1 Sensitivity model runs including additional radical regeneration reactions for $\text{RO}_2$ radicals

Additional radical regeneration reactions are further explored by sensitivity model runs. These model runs aim to reduce the discrepancies between measured and modelled OH,  $\text{HO}_2$  and  $\text{RO}_2$  concentrations in the reference model. This is achieved by implementing additional reaction pathways:



where  $\text{RO}_2$  are the peroxy radicals distinguished from their production in the reaction of limonene with either OH (limOH- $\text{RO}_2$ ; i.e., LMAO<sub>2</sub>, LIMBO<sub>2</sub>, and LIMCO<sub>2</sub>, Fig. 1) or O<sub>3</sub> (limO<sub>3</sub>- $\text{RO}_2$ ; i.e. LIMALAO<sub>2</sub>, LIMALBO<sub>2</sub>, and L5O<sub>2</sub>, Fig. 1), because these peroxy radicals are structurally similar with peroxy radicals from the OH reaction having a  $\beta$ -OH moiety of a 6-carbon ring and limO<sub>3</sub>- $\text{RO}_2$  being acyclic peroxy radicals with a  $\beta$ -oxo, an aldehyde and an isopropenyl group. Therefore, it is assumed that they have similar reaction pathways. ~~These reactions could involve a unknown reaction partner X, as used in (Hofzumahaus et al., (2009), or could be unimolecular reactions. Reactions could involve an unknown reaction partner X like for example used in Hofzumahaus et al. (2009) or could be unimolecular reactions.~~

Reaction rate constants for Reaction R1a and R1b ( $k_{\text{R1a}}$  and  $k_{\text{R1b}}$ ) are implemented as pseudo-first order reaction rate constants.  $\text{RO}_2$  within the same group (limOH- $\text{RO}_2$  or limO<sub>3</sub>- $\text{RO}_2$ ) are assumed to have the same rate constants. Reaction R1a would lead to  $\text{HO}_2$  production and Reaction R1b would lead to OH production. In the sensitivity model runs, the reaction rate constants are optimized to minimize the model-measurement discrepancies for OH,  $\text{HO}_2$ ,  $\text{RO}_2$  concentrations and OH reactivity. The sum of  $k_{\text{R1a}}$  and  $k_{\text{R1b}}$  must be within the range of the additional  $\text{RO}_2$  loss rate constant  $k_{\text{add}}$  (Section 4.1, Table 5). A missing  $\text{HO}_2$  source is found in the reference model for all experiments (Fig. 4 – 7). Assuming that the loss rate of the  $\text{HO}_2$  radical, which mainly reacts with NO, is correctly accounted for, an additional  $\text{RO}_2$  to  $\text{HO}_2$  conversion (Reaction R1a) is needed to bring measurement and model results in agreement. In contrast, missing OH is only found in the experiments with low NO as evident from the analysis of the chemical budget of OH radicals (Section 3.3, Fig. 8). These observations indicate that additional  $\text{RO}_2$  to OH conversion (Reaction R1b) can only be competitive with other bimolecular reactions for NO mixing ratios of less than 0.05 ppbv which is equivalent to a loss rate constant of  $k < 10^{-2} \text{ s}^{-1}$ .

The model-measurement agreement of radical concentrations is first optimized based on the second half of the ozonolysis experiment, when CO was added as OH scavenger. In this case, only limO<sub>3</sub>- $\text{RO}_2$  are present, but the conversion to either  $\text{HO}_2$  (Reaction R1a) or OH (Reaction R1b) cannot be distinguished, because OH rapidly converts to  $\text{HO}_2$ . To achieve agreement between modelled and measured  $\text{HO}_2$  concentrations during this part of the ozonolysis experiment, the sum of the additional loss rate constants ( $k_{\text{R1a}} + k_{\text{R1b}}$ ) would need to be  $(0.017 \pm 0.008) \text{ s}^{-1}$ . The uncertainty is mainly due to the uncertainty in the measurement of  $\text{HO}_2$  concentrations (~20%). The upper limit for the rate constant  $k_{\text{R1b}}$  for the loss of limO<sub>3</sub>- $\text{RO}_2$  can be estimated from the first part of the ozonolysis experiment, when no OH scavenger was present. Since 80 to 100% of the observed OH production can already be explained by OH production from the limonene ozonolysis reaction (Fig. 8d), the rate constant of  $k_{\text{R1b}}$  for limO<sub>3</sub>- $\text{RO}_2$  would need to be less than  $0.004 \text{ s}^{-1}$ . This implies that the rate constant  $k_{\text{R1b}}$  for limOH- $\text{RO}_2$  is also less than  $\sim 0.004 \text{ s}^{-1}$  as about 40% of limonene is oxidized by OH in the ozonolysis experiment without OH scavenger.

The implementation of the Reaction 1a for limO<sub>3</sub>- $\text{RO}_2$  cannot significantly improve the model-measurement discrepancies of  $\text{HO}_2$  concentrations in the experiments, when limonene is predominantly oxidized by OH. Also in the ozonolysis experiment,

HO<sub>2</sub> concentrations are still underestimated by about 40% during the part of the experiment without OH scavenger. Hence, the reaction rate constant  $k_{R1a}$  for an additional loss of limOH-RO<sub>2</sub> is also optimized to match the measured HO<sub>2</sub> concentrations.

Optimization of the reaction rate constant  $k_{R1a}$  for the additional loss of limOH-RO<sub>2</sub> for individual experiments results in values that differ by one order of magnitude. For instance, the optimum rate constant is  $(0.006 \pm 0.003) \text{ s}^{-1}$  in the ozonolysis experiment without OH scavenger, but it is  $(0.05 \pm 0.03) \text{ s}^{-1}$  in the experiment with medium NO concentrations on 08 August 2012. These ~~optimiszed~~ rate constants are consistent with the values of the loss rate constant  $k_{add}$  (Table 5), with the rate required in the ozonolysis experiment having a slower rate while the rate required in the experiment with medium NO having a faster rate. The exact reason for such large differences is not clear, but could be related to the higher temperature ( $16 - 27^\circ\text{C}$ ) in the photo-oxidation experiments, when the chamber air was exposed to sunlight. The average value of the rate constant for the conversion from RO<sub>2</sub> to HO<sub>2</sub> for the experiments in this work is  $0.03 \text{ s}^{-1}$ . This value is applied to all sensitivity model runs in the following to illustrate its impacts on modelled RO<sub>2</sub>, HO<sub>2</sub> concentrations and OH reactivity (Table 6).

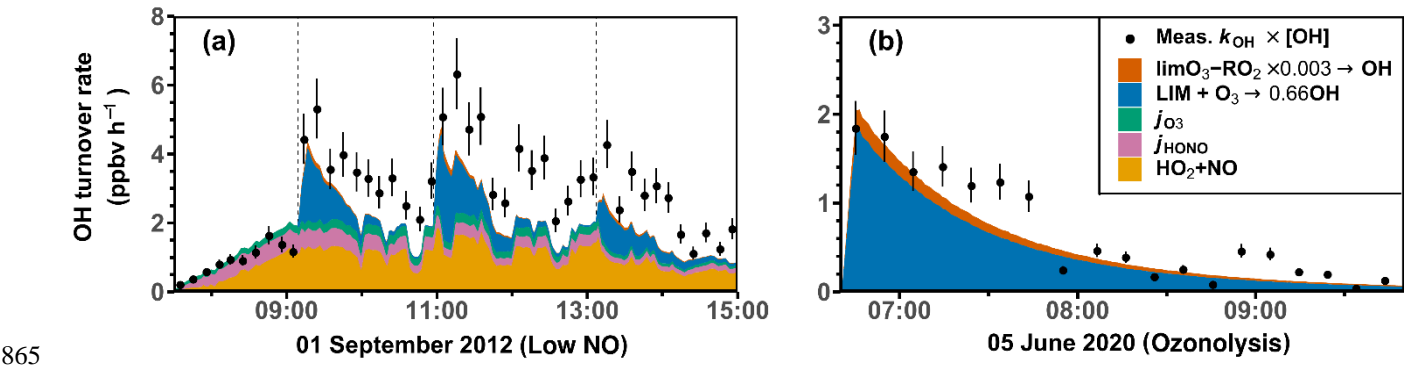
A summary of all reactions included for the sensitivity run is available in Table 6. Figure 11 shows the increase in the OH production rate in the sensitivity model runs that include the conversion of limO<sub>3</sub>-RO<sub>2</sub> to OH at a rate constant of  $0.004 \text{ s}^{-1}$ . The total OH production rate increases by about  $0.2 \text{ ppbv h}^{-1}$  in both experiments corresponding to a 5% and 10% increase, respectively. This reduces the imbalance between OH production and destruction rates in the experiment with low NO by about 20% without significantly impacting the balance in the ozonolysis experiment. This demonstrates that the additional OH production from the conversion of first-generation RO<sub>2</sub> from OH- or O<sub>3</sub>- oxidation of limonene to OH is not sufficient to fully close the gap between OH production and destruction rates in the experiment with low NO, for which the discrepancy is largest among all experiments in this work.

Figure 12 to 14 and Figure S10 to S12 show radical concentrations and OH reactivity obtained in the reference and sensitivity model runs. In the sensitivity model run, the model-measurement agreement for RO<sub>2</sub> and HO<sub>2</sub> concentrations improves compared to the reference model run as can be expected from the adjustment of the reaction rate constant. In the experiment with low NO concentrations, however, an optimal agreement of both, RO<sub>2</sub> and HO<sub>2</sub> concentrations, cannot be simultaneously achieved. This suggests that some fraction of the additional RO<sub>2</sub> loss pathway may not regenerate HO<sub>2</sub> or OH radicals.

In the sensitivity model run the overestimation of the OH reactivity is reduced even without introducing additional loss pathways of oxidised products as implemented in the constrained model run (Section 2.4), because the production of organic peroxides is reduced due to the competition with the additional RO<sub>2</sub> loss reaction. For example, the percentage of RO<sub>2</sub> reacting with HO<sub>2</sub> reduces from about 50% to 25% and from 90% to 30% in the experiment with low NO and in the ozonolysis experiment, respectively. In the sensitivity model, no closed-shell products are produced from the additional RO<sub>2</sub> loss reaction. The good model-measurement agreement of the OH reactivity suggests that organic products from these reactions are not reactive or they are rapidly lost for example to the chamber wall. Therefore, no further conclusions, about the type of products formed from Reaction R1 can be drawn from these experiments.

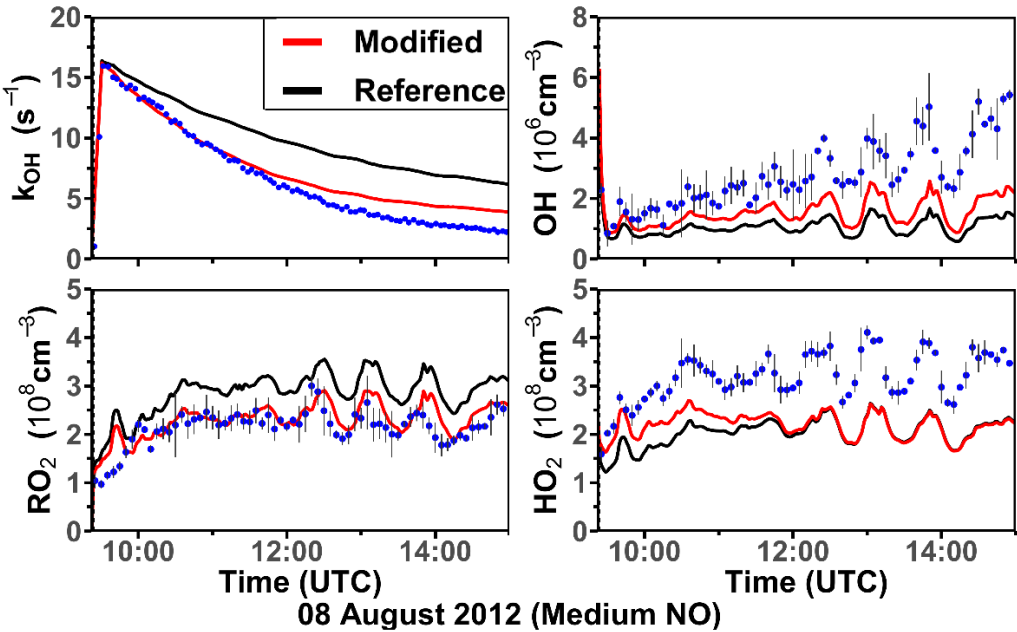
**Table 6.** Modification of chemical reactions implemented in the sensitivity simulations runs.

Reaction	Reaction rate constant	Comment
LIMALAO2 → OH	0.003 s <sup>-1</sup>	Illustrate the impact of the additional OH source on the OH budget in the ozonolysis experiment, when there is no OH scavenger.
LIMALBO2 → OH	0.003 s <sup>-1</sup>	
L5O2 → OH	0.003 s <sup>-1</sup>	
LIMALAO2 → HO2	0.014 s <sup>-1</sup>	Derived from the optimisation of HO <sub>2</sub> model-measurement agreement in the ozonolysis experiment when there is OH scavenger. Assuming $k_{R1b}$ for limO <sub>3</sub> -RO <sub>2</sub> is 0.003 s <sup>-1</sup>
LIMALBO2 → HO2	0.014 s <sup>-1</sup>	
L5O2 → HO2	0.014 s <sup>-1</sup>	
LIMAO2 → HO2	0.030 s <sup>-1</sup>	Mean value of the rate derived from the optimisation of HO <sub>2</sub> model-measurement agreement in the experiments with low NO, medium NO and the ozonolysis experiment.
LIMBO2 → HO2	0.030 s <sup>-1</sup>	
LIMCO2 → HO2	0.030 s <sup>-1</sup>	

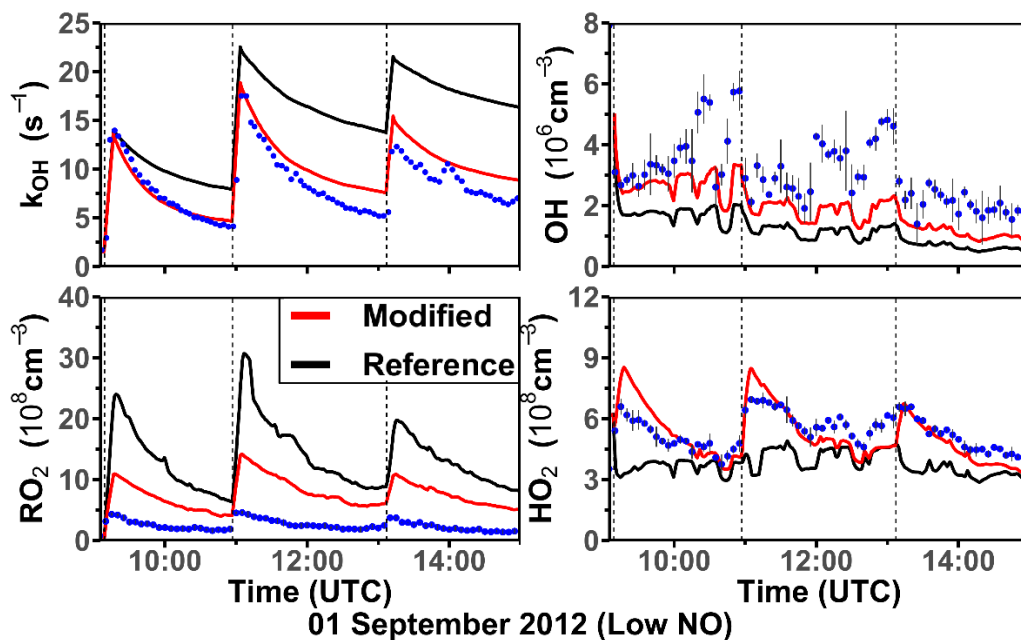


**Figure 11.** Measured 10-minutes-mean total OH production rate compared with the OH production rate from the main measured OH sources for (a) the experiment with low NO concentration on 01 September 2012 and (b) the ozonolysis

experiment on 05 June 2020 for the sensitivity model run that includes additional OH production from the reaction of RO<sub>2</sub> from limonene ozonolysis and HO<sub>2</sub> (Reaction R2c).

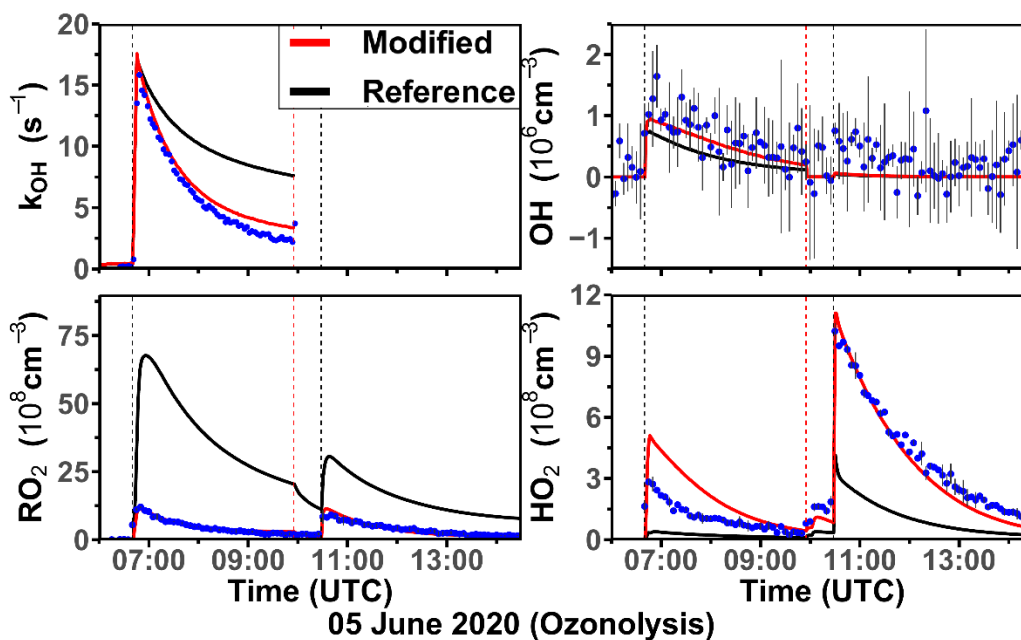


**Figure 12.** Modelled and measured OH reactivity, HO<sub>2</sub>, RO<sub>2</sub>, and OH concentrations for the experiment with medium NO on 08 August 2012. Results from the reference model (reference) and the sensitivity model run (modified) that includes additional RO<sub>2</sub> loss processes producing OH and HO<sub>2</sub> (Table 6) are compared.



01 September 2012 (Low NO)

875 **Figure 13.** Modelled and measured OH reactivity, HO<sub>2</sub>, RO<sub>2</sub>, and OH concentrations for the experiments with low NO concentrations on 01 September 2012. Results from the reference model (reference) and the sensitivity model run (modified) that includes additional RO<sub>2</sub> loss processes producing OH and HO<sub>2</sub> (Table 6) are compared.



05 June 2020 (Ozonolysis)

880 **Figure 1214.** Modelled and measured OH reactivity, HO<sub>2</sub>, RO<sub>2</sub>, and OH concentrations for ~~the experiments with medium NO~~  
~~(top) and low NO (middle) concentrations, and for the ozonolysis experiment (bottom)~~the ozonolysis experiment on 05 June  
2020. Results from the reference model (reference) and the sensitivity model run (modified) that includes additional RO<sub>2</sub> loss  
processes producing OH and HO<sub>2</sub> (Table 6) are compared.

## 885 4.2 Possible additional OH sources from RO<sub>2</sub> reactions

Possible underlying mechanisms of the additional RO<sub>2</sub> loss and the production of OH are discussed in the following section.  
It should be noted that the additional OH source discussed here is referring to the slow additional OH source ( $k_{R1b} < 0.003 \text{ s}^{-1}$ )  
that could only slightly reduce the discrepancy between the OH production and destruction rates (Fig. 11). The larger  
discrepancy in the chemical OH budget that is observed in the experiment with low NO concentrations (Fig. 11a) compared  
890 to the other experiments cannot be explained by the additional conversion of RO<sub>2</sub> to OH and, hence, it is not further discussed  
here. The rate constant of the additional RO<sub>2</sub> to OH conversion,  $k_{R1b}$ , is much slower than the total loss rate constant of RO<sub>2</sub>  
due to bi-molecular reactions ( $k_{bi} > 0.01 \text{ s}^{-1}$ ) or the additional RO<sub>2</sub> to HO<sub>2</sub> conversion ( $k_{R1a} \sim 0.017 \text{ s}^{-1}$ ). Its contribution to the  
production rate of OH would also be small in all experiments ( $< 10\%$  of the total OH production rate). Therefore, there is no  
strong evidence for an additional conversion of RO<sub>2</sub> to OH for experimental conditions in this study.

### 895 4.2.1 RO<sub>2</sub> isomerisation reactions

Isomerisation of RO<sub>2</sub> could lead to the production of OH, which is shown in the OH-oxidation of methacrolein (e.g., Crounse  
et al., 2012) and isoprene (e.g., Novelli et al., 2020). Isomerisation reactions for RO<sub>2</sub> from the limonene oxidation by OH and  
O<sub>3</sub> are investigated by Møller et al. (2020) and Chen et al. (2021), respectively. Of the peroxy radical LMAO<sub>2</sub>, LIMBO<sub>2</sub> and  
LIMCO<sub>2</sub> that are produced from the limonene oxidation by OH, it was calculated that LMAO<sub>2</sub> and LIMBO<sub>2</sub> could undergo  
900 -OH H-shift with a rate constant of  $10^{-3}$  to  $10^{-4} \text{ s}^{-1}$ . LIMCO<sub>2</sub> could undergo isomerisation reactions that are competitive with  
bimolecular reactions for atmospheric conditions, which include a cyclization reaction with a rate constant of 0.2 to  $0.8 \text{ s}^{-1}$  and  
an allylic-H shift reaction with a rate constant of 0.1 to  $1.7 \text{ s}^{-1}$  (Fig. 153). On the other hand, peroxy radicals LIMALAO<sub>2</sub>,  
LIMALBO<sub>2</sub>, and L5O<sub>2</sub> that are produced from the ozonolysis of limonene could all undergo much faster isomerisation  
reactions ( $k > 0.5 \text{ s}^{-1}$ ) such as aldehydic H-shift and cyclisation reactions (Fig. 164) due to the loss of steric hinderance after  
905 the ring-opening ozonolysis reaction.

Subsequent reaction steps after the first isomerisation reaction were not investigated in the work by Møller et al. (2020) and  
by Chen et al. (2021). Therefore, potential OH production from subsequent reactions are estimated with available SAR (e.g.,  
Vereecken and Peeters, 2009; Vereecken and Nozière, 2020; Vereecken et al., 2021).

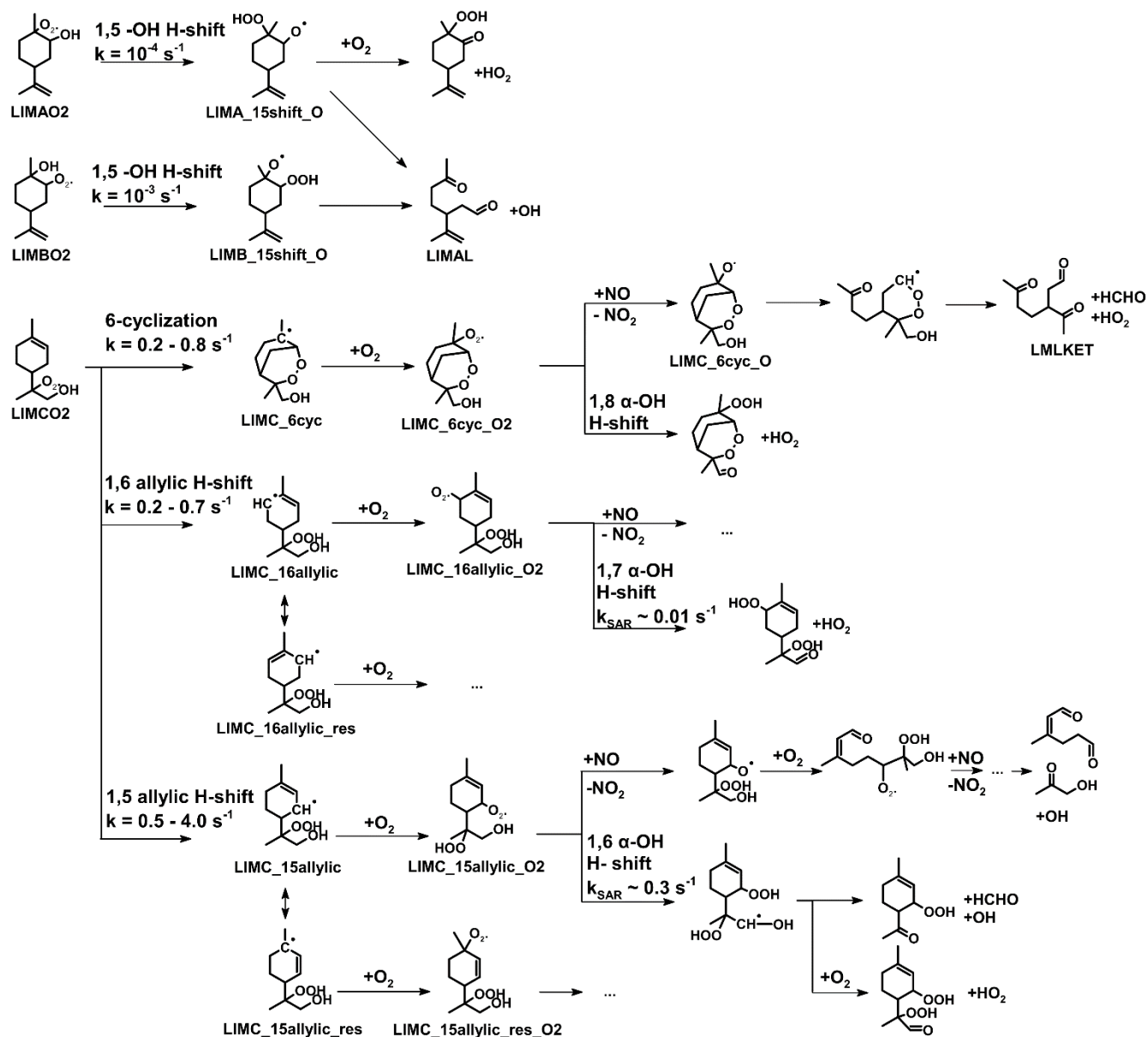
The subsequent reaction of  $\beta$ -OOH substituted alkoxy radicals, LIMA\_15shift\_O and LIMB\_15shift\_O, which are products  
910 of the 1,5 -OH H-shift reactions of LMAO<sub>2</sub> and LIMBO<sub>2</sub> respectively, is a ring-breaking decomposition reaction that

produces an OH radical. For the cyclization product from the isomerisation of LIMCO<sub>2</sub>, LIMC\_6cyc\_O<sub>2</sub>, it may either undergo bimolecular reactions or isomerisation by abstracting the  $\alpha$ -H atom of the hydroxyl group (Fig. 153). Isomerisation of LIMC\_6cyc\_O<sub>2</sub> could result in an aldehyde together with an HO<sub>2</sub> radical. However, it is uncertain, if the isomerisation reaction of LIMC\_6cyc\_O<sub>2</sub> can compete with other reaction channels, as the SAR does not apply to bicyclic compounds. The reaction between LIMC\_6cyc\_O<sub>2</sub> and NO results in a bicyclic alkoxy radical (LIMC\_6cyc\_O), which then dissociates to a cyclic intermediate, analogous to the bicyclic alkoxy radical produced from the OH-oxidation of  $\beta$ -pinene (Vereecken and Peeters, 2004). The dissociation of LIMC\_6cyc\_O may eventually produce an HO<sub>2</sub> radical, which could not explain the production of OH at zero NO condition.

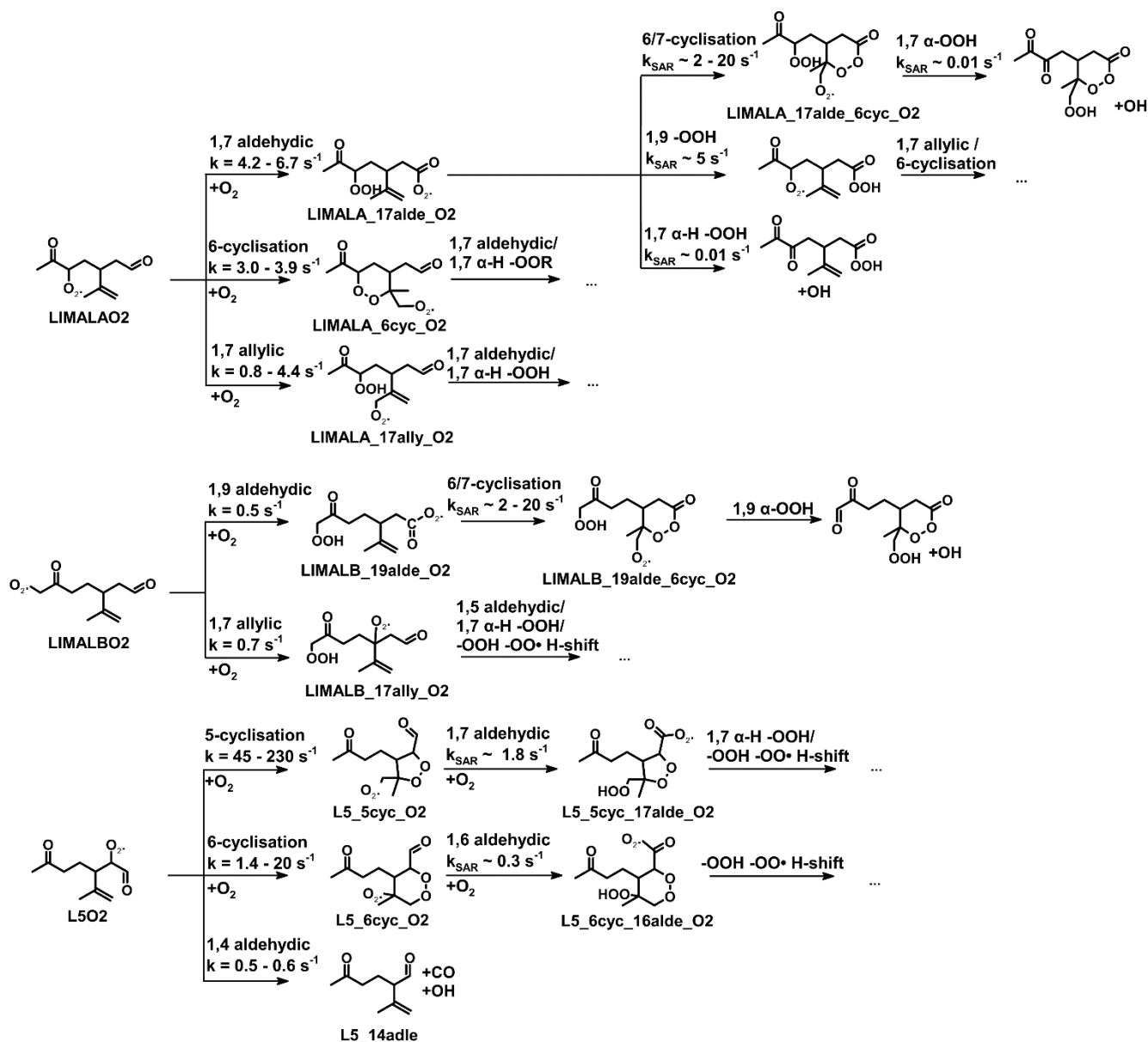
For limO<sub>3</sub>-RO<sub>2</sub>, their subsequent reactions after the first isomerisation reaction are also expected to be very fast ( $k > 0.1 \text{ s}^{-1}$ ) because of the presence of either an aldehyde group or a C=C double bond. However, allylic H-shift, cyclisation, and aldehydic H-shift reactions do not affect the RO<sub>2</sub> and OH concentrations as the resulting alkyl radicals do not decompose into a closed-shell product and an OH radical. Instead, an oxygen molecule rapidly adds to the alkyl radical site to form a highly oxidised RO<sub>2</sub>.

One of the possible additional OH sources from RO<sub>2</sub> isomerisation reactions could be from the H-abstraction of the  $\alpha$ -OOH group (Bianchi et al., 2019). In this case, the  $\alpha$ -OOH substituted alkyl radical could quickly decompose into a carbonyl product and an OH radical. Because of the fast first and second step of the isomerisation reaction, it is expected that limO<sub>3</sub>-RO<sub>2</sub> could form RO<sub>2</sub> with a hydroperoxide group that allows them to undergo  $\alpha$ -OOH H-shift reaction (e.g., LIMALA\_17alde\_O<sub>2</sub>, LIMALB\_19alde\_O<sub>2</sub>, L5\_5cyc\_17alde\_O<sub>2</sub> (Fig. 164)). The SAR-estimated  $\alpha$ -OOH H-abstraction rate constant is about  $10^{-3}$  to  $10^{-2} \text{ s}^{-1}$  (Vereecken and Nozière, 2020), which is slightly faster than the additional RO<sub>2</sub> loss rate constant  $k_{\text{R1b}}$  ( $< 0.003 \text{ s}^{-1}$ ) applied in the sensitivity run. It should be noted that the SAR does not consider the impacts of neighbouring functional groups on the  $\alpha$ -OOH H-shift rate. All limO<sub>3</sub>-RO<sub>2</sub> have a  $\beta$ -oxo group near the radical site, which could increase the H-abstraction rate near the  $\beta$ -oxo group by about one order of magnitude (e.g., Crounse et al., 2013), including the  $\alpha$ -OOH H-abstraction. However, RO<sub>2</sub> derived from the isomerisation of limO<sub>3</sub>-RO<sub>2</sub> still have other possible isomerisation reaction pathways that are even more competitive ( $k > 1 \text{ s}^{-1}$ ) than the  $\alpha$ -OOH H-shift. One example is the H-shift reaction from the hydroperoxyl group to another peroxy group (Vereecken and Nozière 2020). This complicates the chemistry of these highly oxidized peroxy radicals and it is unclear, whether they eventually undergo an  $\alpha$ -OOH H-abstraction.





**Figure 153.** Unimolecular reaction pathways of RO<sub>2</sub> radicals from the reaction of limonene with OH reported in Møller et al. (2020) and subsequent anticipated reaction pathways. Reaction rate constants denoted with  $k_{\text{SAR}}$  are directly taken from SAR for peroxy radicals (Vereecken and Nozière, 2020). The unimolecular reaction rate constant for 1,8 α-OH H-shift is not available.



**Figure 164.** Unimolecular reaction pathways for the major limonene-ozonolysis-derived RO<sub>2</sub> radicals. Rate constants taken from calculations in Chen et al. (2021), in which stereoisomers are considered and therefore a range of values are given. Other rate constants ( $k_{SAR}$ ) are based on SAR in Vereecken and Nozière (2020) and Vereecken et al. (2021). It should be noted that their SAR does not address the effect of steric hindrance (in the case of a cyclic compound) or multiple functional groups near the abstracted H-atom on the H-shift rate constant.

#### 4.2.2 Reactions between RO<sub>2</sub> and HO<sub>2</sub>

Another possible RO<sub>2</sub> loss reaction that leads to OH production and is not considered in the reference model is the reaction of β-oxo-substituted RO<sub>2</sub> with HO<sub>2</sub>. Based on the work by Jenkin et al. (2019), RO<sub>2</sub>+HO<sub>2</sub> reactions can lead to different products depending on the functional groups nearby the peroxy group of the RO<sub>2</sub> radical:



960 It has been shown in experimental studies investigating simple β-oxo substituted RO<sub>2</sub> that they can form an alkoxy radical together with an OH radical (Reaction R2c) instead of a hydroperoxide compound (Reaction 2a) (Jenkin et al., 2007; Hasson et al., 2012; Praske et al., 2015). With the branching ratios that are taken from the SAR, which is derived using simple β-oxo substituted RO<sub>2</sub>, the OH yield of the RO<sub>2</sub>+HO<sub>2</sub> reaction for limO<sub>3</sub>-RO<sub>2</sub> is about 30% (Jenkin et al., 2019). This value is similar to the OH production rate in the sensitivity runs using an additional RO<sub>2</sub> loss rate constant of  $k_{\text{R1b}} = 0.003 \text{ s}^{-1}$ . However, 965 theoretical investigation by Iyer et al. (2018) suggests that the OH yield of the RO<sub>2</sub>+HO<sub>2</sub> reaction may not be high enough (< 1%) based on the energy barriers that were calculated in that study for limO<sub>3</sub>-RO<sub>2</sub>. Currently, there is no laboratory study on the OH yield from the RO<sub>2</sub>+HO<sub>2</sub> reaction for large RO<sub>2</sub> and therefore the OH yield of the RO<sub>2</sub>+HO<sub>2</sub> for large RO<sub>2</sub> is highly uncertain.

### 970 4.3 Possible additional HO<sub>2</sub> sources from RO<sub>2</sub> reactions

#### 4.3.1 RO<sub>2</sub> isomerisation reactions

Similar to the additional OH source, HO<sub>2</sub> can also be produced from the isomerisation reaction of RO<sub>2</sub> radicals (e.g., Crounse et al., 2012; Peeters et al., 2014). Again, the possibility of additional conversion from RO<sub>2</sub> to HO<sub>2</sub> by isomerisation is investigated using the isomerisation pathways calculated for RO<sub>2</sub> derived from limonene oxidation and SARs (Vereecken and 975 Peeters, 2009; Møller et al., 2020; Vereecken and Nozière, 2020; Chen et al., 2021; Vereecken et al., 2021).

Peroxy radicals LMAO2 and LIMBO2 that are produced from the OH-oxidation of limonene can undergo a slow ( $k < 10^{-3} \text{ s}^{-1}$ ) -OH H-shift reaction that is one order of magnitude slower than the rate of the RO<sub>2</sub> to HO<sub>2</sub> conversion applied in the sensitivity run (Fig. 153). In addition, the production of HO<sub>2</sub> through the H-abstraction by O<sub>2</sub> of the alkoxy radical

LIMA\_15shift\_O is not as favourable as the ring-cleavage alkoxy dissociation that eventually produces an OH radical (Vereecken and Peeters, 2009). Therefore, even with the potential production of HO<sub>2</sub> through the isomerisation of RO<sub>2</sub> derived from the isomerisation of LIMCO<sub>2</sub> (e.g., 1,8 α-OH H-shift of LIMC\_6cyc\_O<sub>2</sub>), the production of HO<sub>2</sub> is limited by the 37% yield of LIMCO<sub>2</sub> from the oxidation of limonene by OH. In addition, the rate constant of the H-shift reaction for the intermediate radicals derived from LIMCO<sub>2</sub> (e.g., LIMC\_6cyc\_O<sub>2</sub>, LIMC\_16allylic\_O<sub>2</sub>, LIMC\_15allylic\_O<sub>2</sub>) have a high uncertainty as it is assumed that the SAR for acyclic compounds can be applied for cyclic RO<sub>2</sub>. For these reasons, isomerisation reactions for limOH-RO<sub>2</sub> are unlikely the reason for the additional HO<sub>2</sub> production and RO<sub>2</sub> loss required to match observed radical concentration measurements.

For limO<sub>3</sub>-RO<sub>2</sub>, reaction rate constants of the first two of the isomerisation reaction are about one to two orders of magnitude faster than the RO<sub>2</sub> to HO<sub>2</sub> conversion rate used in the sensitivity run (Fig. 164). As discussed in Section 4.2.1, one of the possible RO<sub>2</sub> loss mechanisms through isomerisation reaction is a α-OOH H-abstraction reaction. Although the value of the rate constant of the α-OOH H-abstraction reaction derived from SAR is on the same magnitude (~ 10<sup>-2</sup> s<sup>-1</sup>) as the RO<sub>2</sub> to HO<sub>2</sub> conversion rate constant applied in the sensitivity run, abstraction of the hydrogen with an α-OOH group would lead to the production of an OH radical rather than a HO<sub>2</sub> radical. Therefore, isomerisation reactions of limO<sub>3</sub>-RO<sub>2</sub> can also not explain the missing RO<sub>2</sub> to HO<sub>2</sub> conversion resulting from observations in the experiments in this work.

#### 995 4.3.2 Reaction rate constant of the RO<sub>2</sub> recombination reaction

Apart from isomerisation, HO<sub>2</sub> could also be produced from the dissociation of alkoxy radicals derived from RO<sub>2</sub> from the reaction of limonene with OH. Alkoxy radicals could be produced from the recombination reaction of RO<sub>2</sub> radicals in addition to the reaction of RO<sub>2</sub> with NO:



The current knowledge about the branching ratio between Reaction R3a to R3d, as well as the RO<sub>2</sub> self- or cross-reaction rate constants is limited especially for complex RO<sub>2</sub> derived from monoterpenes. There are no specific investigations for RO<sub>2</sub> from limonene. Reaction rate constants implemented in the MCM model are based on estimated cross-reaction rates between RO<sub>2</sub> and methyl peroxy radicals (CH<sub>3</sub>O<sub>2</sub>), (Jenkin et al., 1997, 2019). The reaction rate constants of the RO<sub>2</sub> recombination reactions,  $k_{\text{RO}_2+\text{RO}_2}$ , for limonene-derived radicals are between 10<sup>-12</sup> to 10<sup>-13</sup> cm<sup>3</sup> s<sup>-1</sup> in the MCM consistent with results for RO<sub>2</sub> from methyl cyclohexene, which contain a tri-substituted endocyclic double bond like limonene (Boyd et al., 2003).

However, the reaction rate constant  $k_{\text{RO}_2+\text{RO}_2}$  could be higher, if the cross-reaction partners are other large limonene-derived radicals rather than  $\text{CH}_3\text{O}_2$ . For example, Berndt et al., (2018) investigated the self-reaction rate constants for  $\text{RO}_2$  derived from the reaction of  $\alpha$ -pinene with OH after they undergo two steps of unimolecular reactions (i.e.,  $\text{C}_{10}\text{H}_{16}\text{OH}(\text{O}_2)_2\text{-O}_2$ ). They found that values range between 1 and  $4 \times 10^{-11} \text{ cm}^3 \text{ s}^{-1}$  in this case. However, it should be noted that these high rate constants are derived from the production rate of peroxide products ( $\text{ROOR}$ , Reaction R3d), rather than the loss rate of  $\text{RO}_2$ .

Using the values of the reaction rate constants  $k_{\text{RO}_2+\text{RO}_2}$  for  $\text{RO}_2$  from limonene oxidation from the MCM, the upper limit of the  $\text{RO}_2$  loss rate constant due to  $\text{RO}_2$ - $\text{RO}_2$  reactions is about  $10^{-3} \text{ s}^{-1}$  in the ozonolysis experiment and experiments with low NO, and  $2 \times 10^{-4} \text{ s}^{-1}$  in the experiments with medium NO. From the additional loss rate constant ( $\sim 10^{-2} \text{ s}^{-1}$ ; Table 5) determined from the chemical budget analysis for  $\text{RO}_2$ , the value of the reaction rate constant for  $\text{RO}_2$ - $\text{RO}_2$  reaction that would be required to explain the observations ( $k'_{\text{RO}_2+\text{RO}_2}$ ) can be calculated. This results in values of  $k'_{\text{RO}_2+\text{RO}_2}$  that are about  $3 \times 10^{-10}$ ,  $1 \times 10^{-11}$ ,  $3 \times 10^{-11} \text{ cm}^3 \text{ s}^{-1}$  in the medium NO, low NO and ozonolysis experiments, respectively. The uncertainties of the rate constants are about 50 – 60%, which are derived from the error propagation of  $\text{RO}_2$  concentrations and optimal rate constants in the sensitivity model run (Table 6). It should be noted that these values are collective loss rate constants of all first-generation  $\text{RO}_2$  species from limonene oxidation before the formation of closed-shell products, including highly-oxidized  $\text{RO}_2$  produced from potential auto-oxidation reactions.

The values of the reaction rate constant  $k'_{\text{RO}_2+\text{RO}_2}$  found in the low NO experiment and ozonolysis experiment are in the same order of magnitude ( $10^{-11}$  to  $10^{-10} \text{ cm}^3 \text{ s}^{-1}$ ) as values reported by Berndt et al., (2018) for  $\text{RO}_2$  from  $\alpha$ -pinene oxidation. Berndt et al., (2018) also showed that the reaction rate constant for the  $\text{RO}_2$ - $\text{RO}_2$  self-reaction increases, when the  $\text{RO}_2$  becomes more oxidised. This hints at the importance of  $\text{RO}_2$  recombination reactions for  $\text{RO}_2$  derived from limonene oxidation could be higher than previously thought, because of the rapid isomerisation reaction of these radicals (Møller et al. (2020) and Chen et al. (2021); Section 4.2.1).

In the experiment with low NO concentrations, the additional loss rate constant for  $\text{RO}_2$  radicals that is required to explain measured  $\text{RO}_2$  concentrations ( $k \sim 0.06 \text{ s}^{-1}$ , Table 5) is higher than the rate constant of the additional  $\text{RO}_2$  to  $\text{HO}_2$  conversion required to explain measured  $\text{HO}_2$  concentration ( $k \sim 0.006 - 0.02 \text{ s}^{-1}$ ). This would be consistent with a faster reaction rate constant for the  $\text{RO}_2$ - $\text{RO}_2$  reaction, because only a fraction of the  $\text{RO}_2$ - $\text{RO}_2$  reaction would lead to the formation of alkoxy and therefore  $\text{HO}_2$  radicals (Reaction 3).

However, it would be unclear, why the reaction constant  $k'_{\text{RO}_2+\text{RO}_2}$  required in the experiment with medium NO mixing ratio would be higher compared to other experiments. It is also worth noting that the decomposition of alkoxy radicals produced from  $\text{RO}_2$  from the ozonolysis of limonene leads to the production of peroxy radicals which do not lead to the production of  $\text{HO}_2$  in most of the  $\text{RO}_2$ - $\text{RO}_2$  reaction chain (Fig. 1). Therefore the missing production of  $\text{HO}_2$  in the ozonolysis experiment cannot be explained by a higher than previously thought reaction rate constant of the  $\text{RO}_2$ - $\text{RO}_2$  reaction.

## 5 Conclusions

The photooxidation of limonene by OH and O<sub>3</sub> was investigated in experiments for zero, low (~0.1 ppbv), medium (~0.4 ppbv) and high (~ 1 ppbv) NO levels in the atmospheric simulation chamber SAPHIR. The experiments were conducted with limonene mixing ratios of 4 – 10 ppbv and O<sub>3</sub> mixing ratios ranging from 0 – 50 ppbv.

1045 The analysis of measured radical concentrations in the experiments revealed that current knowledge about the limonene oxidation as implemented in the Master Chemical Mechanism cannot explain observed values specifically concerning radical regeneration. Observed OH and HO<sub>2</sub> concentrations were a factor of 2 to 3 higher than predicted by model calculations, whereas measured RO<sub>2</sub> concentrations were at least 50% lower than modelled values. The following processes in the limonene mechanism impacting radical concentrations could be identified that are not appropriately described:

- 1050 • The loss rate of OH radicals is too high in the model as seen in higher-than-observed OH reactivity values ~~in the model~~. Although it cannot be excluded that chamber wall losses reduced the concentration of organic oxidation products, this hints that the reactivity of products species with respect to their reaction with OH is low or other products other than currently thought are produced for example by the competition of unaccounted radical reaction pathways.
- 1055 • The yield of organic nitrates from the reaction of RO<sub>2</sub> radicals formed in the initial reaction of OH with limonene is found to be (34±5)%, which agrees with the measurements by Rollins et al. (2010), but which is about 10% higher than calculated from structure-activity relationships. The higher yield of organic nitrates reduces the efficiency of the radical regeneration in the limonene mechanism.
- 1060 • Formaldehyde is expected to be formed from the reaction chain after the addition of OH to the terminal C=C double bond, if RO<sub>2</sub> radicals react with NO, so that the formaldehyde yield would be similar to the yield of that RO<sub>2</sub> species (37%). The low formaldehyde yield of (13±3)% in the experiments with medium NO concentrations suggests that there is an unaccounted RO<sub>2</sub> loss reaction not producing formaldehyde that is competitive at 200 pptv NO.
- 1065 • OH production and destruction rates are balanced in most of the experiments, if measured OH reactivity and measured HO<sub>2</sub> concentrations are used for calculating reaction rates. This demonstrates that measured values are consistent and confirm the shortcomings of the limonene mechanism with regards to describing the HO<sub>2</sub> production and OH reactivity.
- An unaccounted RO<sub>2</sub> loss process with a rate constant of 0.02 to 0.06 s<sup>-1</sup> is required to balance the RO<sub>2</sub> production rate from the reaction of OH with organic compounds. Formation of HO<sub>2</sub> with a rate constant of 0.03 s<sup>-1</sup> and 0.017 s<sup>-1</sup> from an additional reaction of the RO<sub>2</sub> from the reaction of limonene with OH and O<sub>3</sub>, respectively, can explain part of the model-measurement discrepancies for HO<sub>2</sub>.
- 1070 • An unaccounted RO<sub>2</sub> loss process for RO<sub>2</sub> from the ozonolysis of limonene that is competitive against the reaction with NO prevents the formation of NO<sub>x</sub> reservoir species PAN and PAN-like species as suggested in the MCM model.

The observed NO<sub>x</sub> concentrations do not exhibit a distinct temporal behaviour that would be expected neither from the rapid loss of NO<sub>x</sub> species at the beginning of limonene oxidation when RO<sub>2</sub> derived from limonene oxidation reacts with NO<sub>x</sub>, and NO<sub>x</sub> reformation from the thermal decomposition of PAN species at the later times of the experiments when limonene has reacted away.

Overall, the results of the experiments clearly demonstrate that loss reactions of RO<sub>2</sub> from the oxidation of limonene are not well understood. Unaccounted RO<sub>2</sub> reactions lead to an enhanced radical regeneration. Organic products likely are less reactive than products that are currently thought to be formed. Time series of measured radical concentrations indicate that their further oxidation reactions need to be investigated to explain observed values at later times of the experiments, when limonene had reacted away. The formation of NO<sub>x</sub> reservoir species (PAN / PAN-like species) is lower than expected. However, this is partly counter-acted by a high yield of (34±5)% of organic nitrates. Oxidation products are also likely to have a high organic nitrates yield as indicated by the low measured NO<sub>x</sub> concentrations that would otherwise be expected to continuously increase over the course of the experiment due to the continuous emission of HONO by the chamber film.

Rate constants of RO<sub>2</sub> isomerisation reactions proposed by Møller et al. (2020) and Chen et al. (2021) are too low or too fast ( $k \sim 10^{-4}$  to  $10^{-3}$  and  $1$  to  $10^2$  s<sup>-1</sup>) to explain observed radical concentrations and expected products are not consistent. A possible explanation could be that the reaction rate constant  $k_{\text{RO}_2+\text{RO}_2}$  of RO<sub>2</sub> recombination reactions for RO<sub>2</sub> from limonene oxidation is higher than the reaction rate constants that are calculated by SAR implemented in the MCM. For example, experiments for RO<sub>2</sub> from α-pinene oxidation by Berndt et al. (2018) show that the rate constant can be one to two orders of magnitude faster than implemented in the MCM model for α-pinene ( $10^{-13}$  to  $10^{-12}$  cm<sup>3</sup> s<sup>-1</sup>). These values are consistent with the additional loss rate required to explain radical concentrations in the experiments with limonene in this work. However, the importance of the alkoxy pathway of the RO<sub>2</sub>+RO<sub>2</sub> reaction for large monoterpene-derived RO<sub>2</sub> is still unclear and needs further investigation.

*Data availability:* Data from the experiments in the SAPHIR chamber used in this work are available on the EUROCHAMP data home page. 08 August 2012: <https://doi.org/10.25326/JNMN-YC22> (Fuchs et al., 2021b); 10 August 2012: <https://doi.org/10.25326/2PGS-FP66> (Fuchs et al., 2021c); 01 September 2012: <https://doi.org/10.25326/77N2-ZK22> (Fuchs et al., 2021a); 03 August 2015: <https://doi.org/10.25326/BP56-WP95> (Bohn et al., 2021c), 04 July 2019: <https://doi.org/10.25326/C4SW-TP73> (Bohn et al., 2021b); 05 June 2020: <https://doi.org/10.25326/7ZKX-347> (Bohn et al., 2021a).

*Supplement.* The supplement related to this article is available online at:

1105 *Author contributions.* JYSP, AN and HF wrote the manuscript. MK, AN and HF designed and led the experiments in the chamber. BB (radiation), RT, AL, IHA and RW (organic compounds), XL (HONO), FR (ozone, nitrogen oxides), HPD and PC (radicals), SN (OH reactivity), CC and AN (radicals and OH reactivity) were responsible for measurements used in this work. All co-authors commented and discussed the manuscript and contributed to the writing of the manuscript.

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# Investigation of the limonene photooxidation by OH at different NO<sub>x</sub> levels-concentrations in the atmospheric simulation chamber SAPHIR

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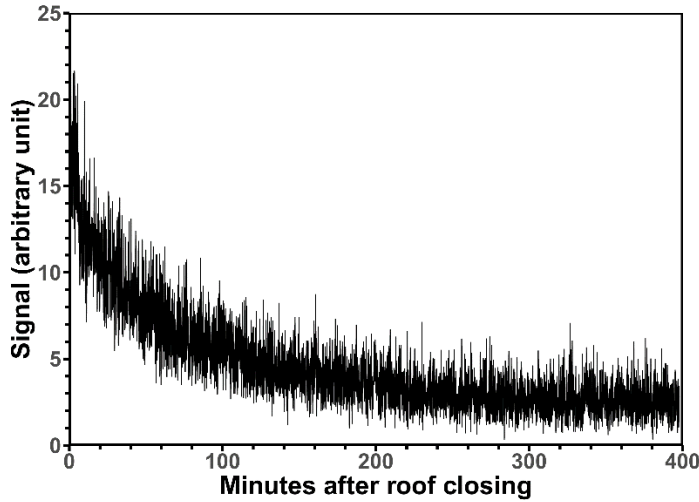
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## 1. Nitrate wall loss rate



30 **Figure S1.** Nitrate ion CIMS signal for the compounds  $C_{10}H_{17}NO_6$  ( $m/z$  310) during a high NO (10 ppbv) limonene oxidation experiment (Zhao et al., 2018). The rate constant of this loss process is  $8.46 \times 10^{-3} \text{ min}^{-1}$ .

## 2. Calculation of product yield

To calculate the time series of the product yield, chamber source and chemical loss processes have to be considered to correct the measured formaldehyde (HCHO) and limonene concentration (Rolletter et al., 2019). Both species are subject to dilution loss as a result of replenishing flow, this can be expressed as:

$$\Delta[x] = -k_{\text{dil}}[x]\Delta t \quad (\text{S1})$$

where  $[x]$  is the concentration of the chemical species;  $k_{\text{dil}}$  is the dilution constant measured during the experiment. HCHO has additional losses from photolysis and the reaction with OH. The calculation of these chemical loss processes ( $\Delta[\text{HCHO}]_{\text{chem}}$ ) follows the description in the Master Chemical Mechanism version 3.3.1 (MCM v.3.3.1):

$$\Delta[\text{HCHO}]_{\text{chem}} = -(j_{\text{HCHO}} + 5.4 \times 10^{-12} \exp\left(\frac{135}{T}\right) [\text{OH}]) [\text{HCHO}] \Delta t \quad (\text{S2})$$

where  $j_{\text{HCHO}}$  is the photolysis rate of HCHO. The corrected concentration is then iteratively calculated by using Eq. S1 and Eq. S2:

$$[\text{LIM}]_{\text{corr}_{t+1}} = [\text{LIM}]_t + k_{\text{dil}_t} [\text{LIM}]_t \Delta t \quad (\text{S3})$$

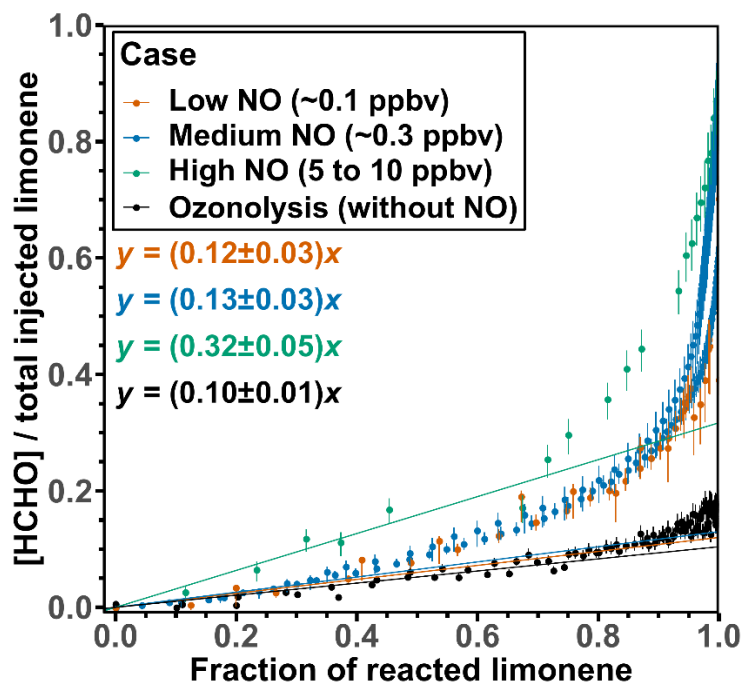
$$45 \quad [\text{HCHO}]_{\text{corr}_{t+1}} = [\text{HCHO}]_t + (k_{\text{dil}_t} + j_{\text{HCHO}_t} + 5.4 \times 10^{-12} \exp\left(\frac{135}{T}\right) [\text{OH}]_t) [\text{HCHO}]_t \Delta t \quad (\text{S4})$$

$$[\text{HCHO}]_{\text{LIM}_{\text{Oxd}}} = [\text{HCHO}]_{\text{corr}_{t+1}} - Q_{\text{HCHO}} \quad (\text{S5})$$

where  $[\text{LIM}]_{\text{corr}}$  and  $[\text{HCHO}]_{\text{corr}}$  are the corrected limonene and HCHO concentration respectively. To determine the amount of HCHO emitted from the chamber wall during the experiment, the chamber roof is opened to allow the chamber to be irradiated before limonene is injected into the chamber (zero-air phase). The production rate of chamber HCHO is then determined using the HCHO measurement during the zero-air phase. With this production rate, a control simulation in which no limonene is injected into the chamber is conducted, the resulting HCHO concentration is corrected using equation S4 to yield the HCHO concentration attributed from chamber source ( $Q_{\text{HCHO}}$ ). The amount of HCHO produced from the oxidation of limonene ( $[\text{HCHO}]_{\text{LIMoxd}}$ ) could be calculated by subtracting the corrected chamber-emitted HCHO concentration from  $Q_{\text{HCHO}}$ . To calculate the amount of reacted limonene, the following equation is followed:

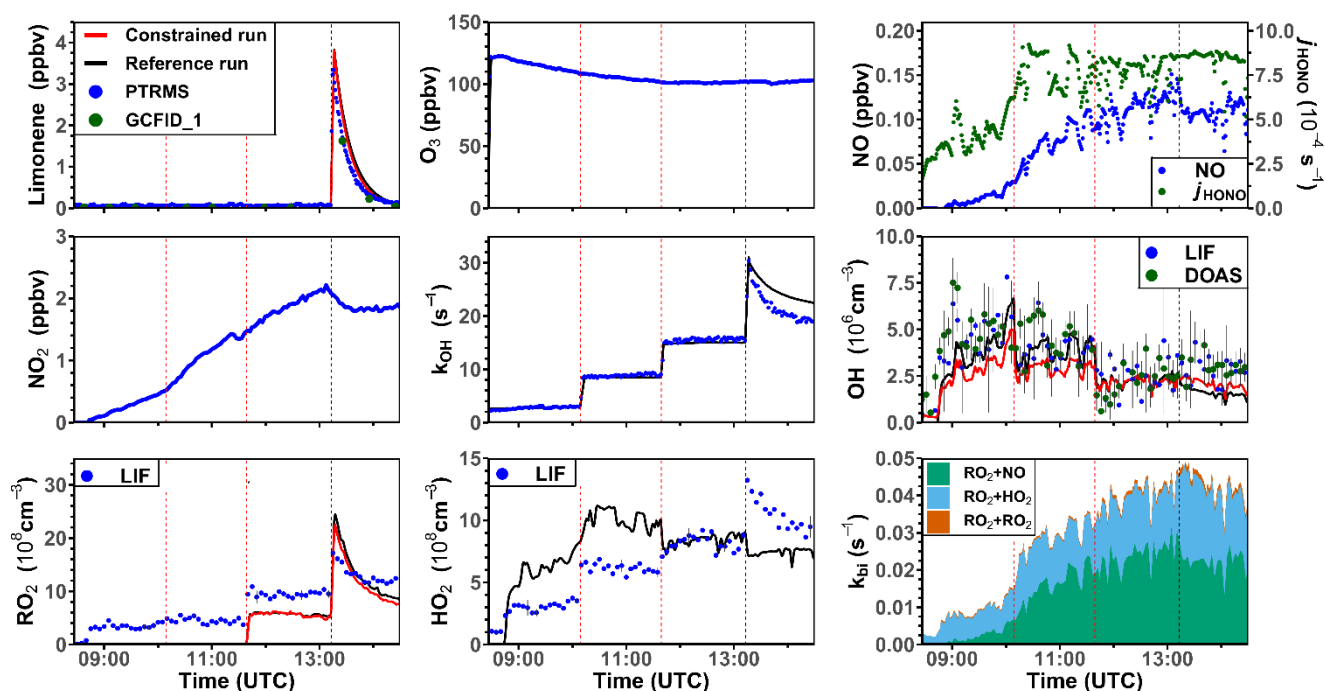
$$\text{LIM}_{\text{reacted}_t} = \sum_{t=0}^{t=t'} ([\text{LIM}] \times (k_{\text{LIM}+\text{O}_3} \times [\text{O}_3] + k_{\text{LIM}+\text{OH}} \times [\text{OH}])) \quad (\text{S6})$$

where  $\text{LIM}_{\text{reacted}_t}$  is the total amount of reacted limonene at time  $t'$ ,  $[\text{O}_3]$  and  $[\text{OH}]$  are the measured  $\text{O}_3$  and OH concentrations respectively.

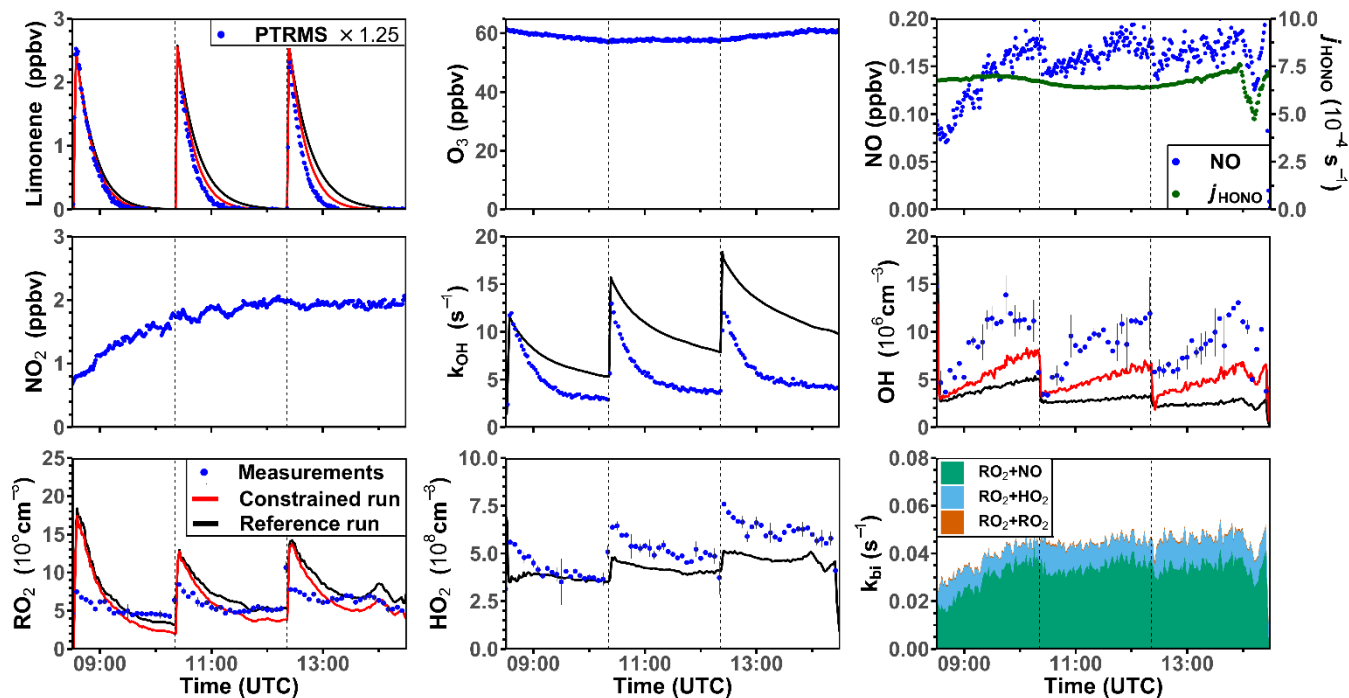


**Figure S2.** HCHO concentrations divided by the injected limonene concentration plotted versus the fraction of reacted limonene for the first injection in the experiments with different NO levels.

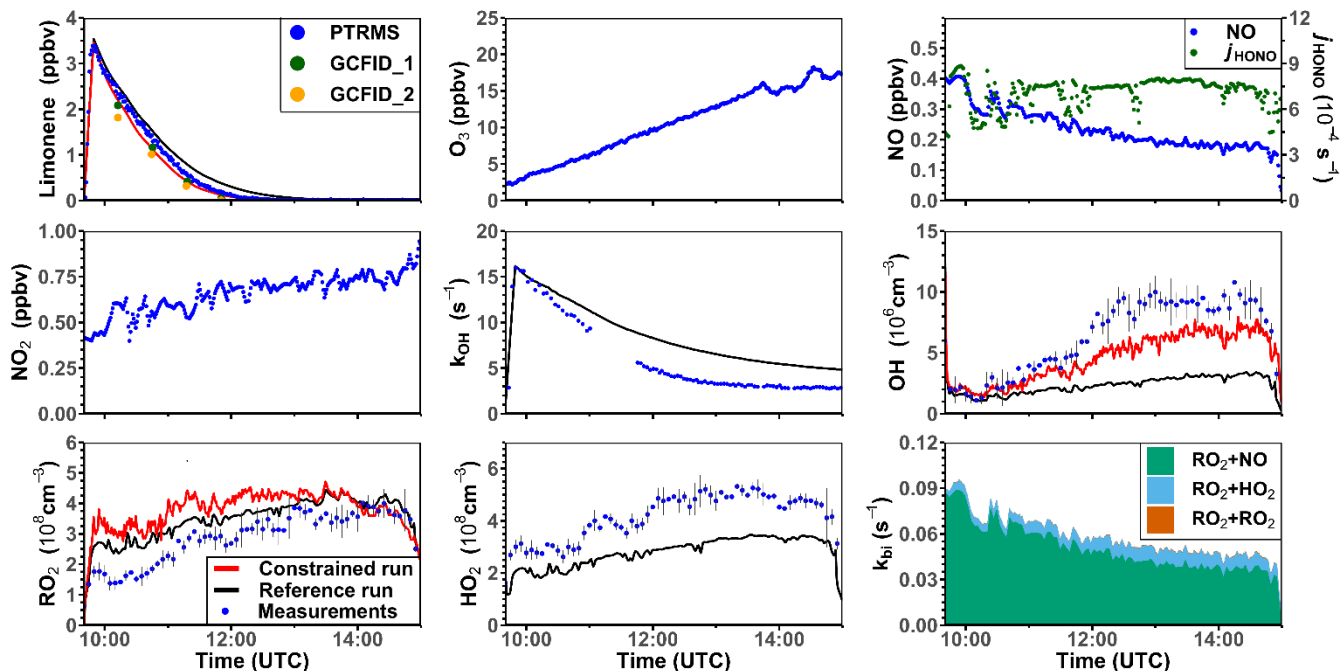
### 3. Model-measurement comparison for the other limonene oxidation experiments (Section 3.2 in the main text)



**Figure S3.** Time series of radicals, inorganic and organic species during the limonene oxidation experiment at low NO mixing ratio on 13 June 2015. The black line denoted the modelled results from the reference model with  $O_3$ ,  $NO_x$  and HONO are constrained; the red line denoted the modelled results from the constrained model with  $HO_2$  constrained and  $k_{OH}$  adjusted to the measurement, and the dots are the measurements.  $RO_2$  bi-molecular reaction loss rate constants ( $k_{bi}$ ) are calculated based on the measured  $NO$ ,  $HO_2$ , and  $RO_2$  concentrations using reaction rate constants from the MCM model. The first red dashed line indicates the injection of 750 ppb of  $CO$ ; the second red dashed line indicates the injection of 60 ppm of  $CH_4$ .



80 **Figure S4.** Time series of radicals, inorganic and organic species during the limonene oxidation experiment at low NO mixing  
 85 ratio on 04 July 2019. Limonene concentrations measured by PTRMS are scaled by a factor of 1.25 to match the increase of  
 OH reactivity during limonene injections. The black line denoted the modelled results from the reference model with  $O_3$ ,  $NO_x$   
 and HONO being constrained; the red line denoted the modelled result from the constrained model with  $HO_2$  constrained  
 and  $k_{OH}$  adjusted to the measurement.  $RO_2$  bi-molecular reaction loss rate constants ( $k_{bi}$ ) are calculated based on the measured  
 NO,  $HO_2$ , and  $RO_2$  concentrations using reaction rate constants from the MCM model.



**Figure S5.** Time series of radicals, inorganic and organic species during the limonene oxidation experiment at medium NO mixing ratio on 10 August 2012. The black line denoted the modelled results from the reference model with  $O_3$ ,  $NO_x$  and HONO being constrained; the red line denoted the modelled results from the constrained model with  $HO_2$  constrained and  $k_{OH}$  adjusted to the measurement.  $RO_2$  bi-molecular reaction loss rate constants ( $k_{RO_2}$ ,  $k_{bi}$ ) are calculated based on the measured NO,  $HO_2$ , and  $RO_2$  concentrations using reaction rate constants from the MCM model.

#### 4. Contribution of $k_{OH}$ from limonene oxidation products and intermediates

OH reactivity is overestimated at all limonene oxidation experiments after limonene injections. To identify the contribution to the total  $k_{OH}$  from limonene oxidation products and intermediates, the total  $k_{OH}$  is subtracted by the  $k_{OH}$  attributed to limonene and the background with the following formula:

$$k_{OH_{intermediates}} = k_{OH_{total}} - 4.28 \times 10^{-11} \times \exp\left(\frac{401}{T}\right) \times [LIM] - k_{OH_{background}}$$

where  $k_{OH_{total}}$  is the total measured or simulated OH reactivity;  $[LIM]$  is the limonene concentration;  $k_{OH_{background}}$  is the OH reactivity contributed by unknown contaminants ( $k_{OH} \sim 1 \text{ s}^{-1}$ ) and inorganic compounds (e.g., NO,  $O_3$ ). Contribution to  $k_{OH_{intermediates}}$  from different groups of species is also calculated, which includes acyl peroxy nitrates (PANs), organic nitrates ( $RONO_2$ ), organic peroxide ( $ROOH$ ), first-generation product of limonene ozonolysis ( $O_3$  1<sup>st</sup> gen.), first-, second-, and third-

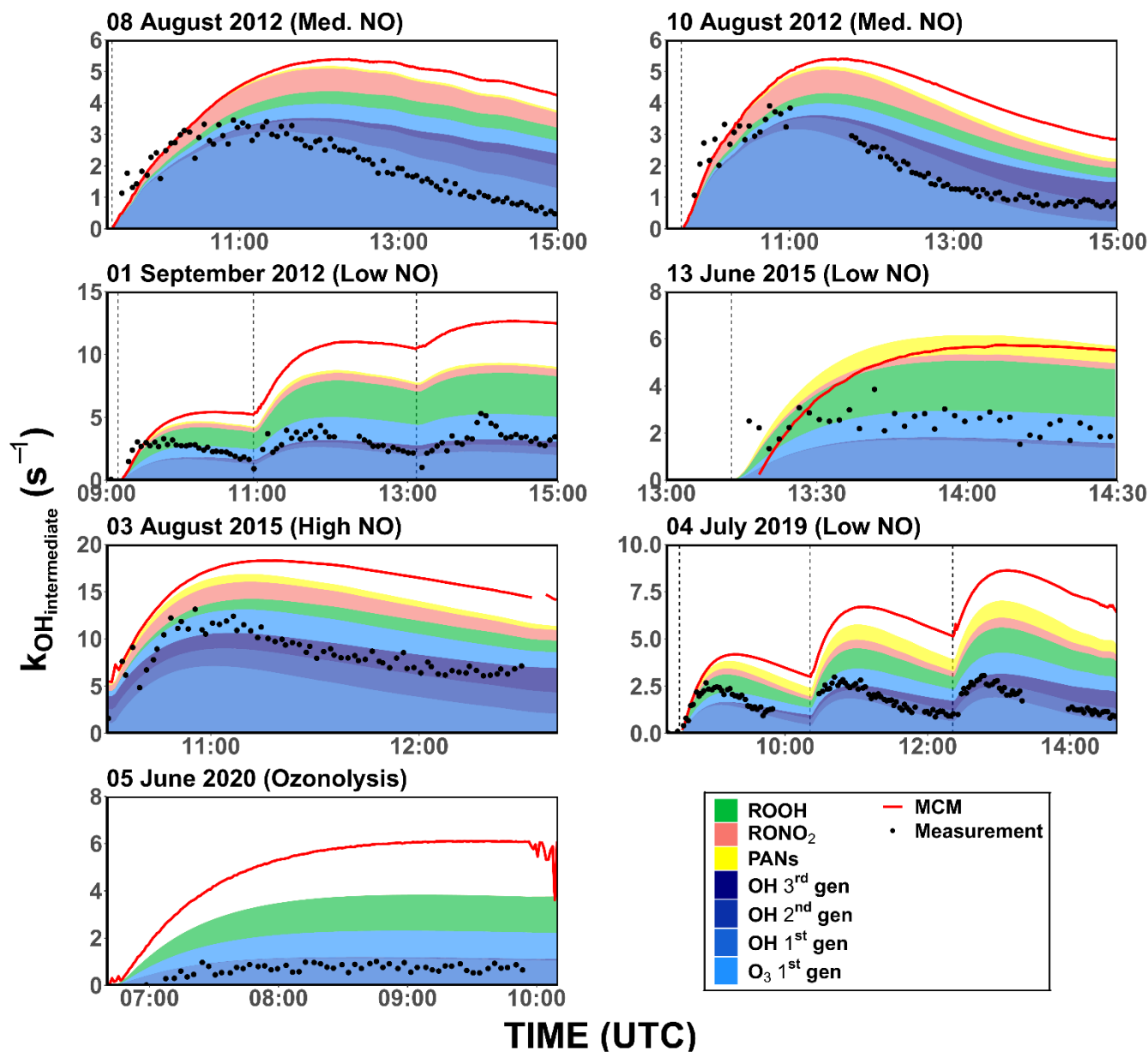


generation products from limonene-OH oxidation (OH 1<sup>st</sup> gen., OH 2<sup>nd</sup> gen., and OH 3<sup>rd</sup> gen.) (Table S1). Reaction rate constants of limonene and its intermediates with OH and O<sub>3</sub> are all taken from the MCM.

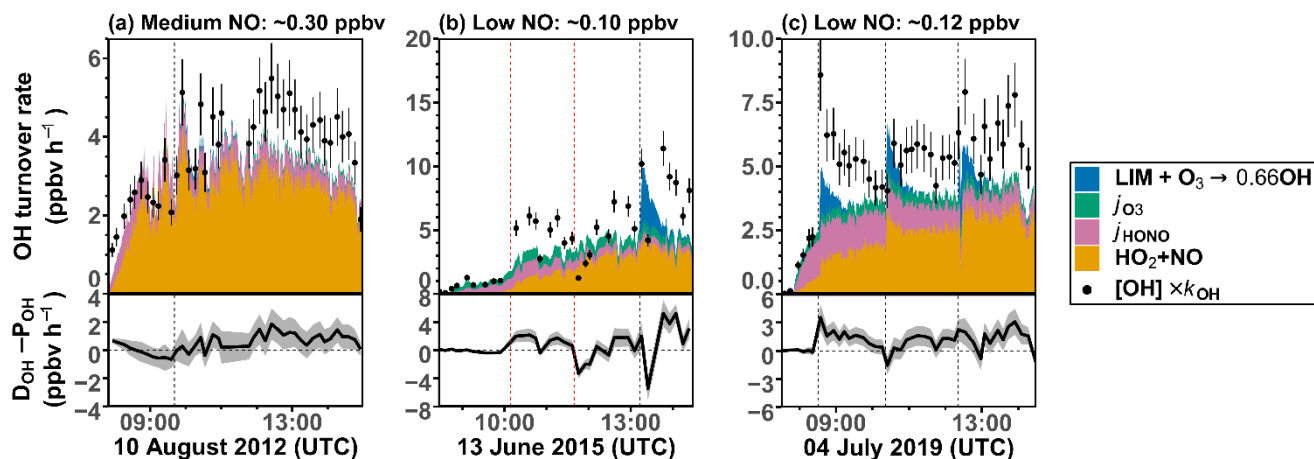
Group	MCM species
OH 1 <sup>st</sup> gen.	LIMAL, LIMKET
OH 2 <sup>nd</sup> gen.	LMLKET
OH 3 <sup>rd</sup> gen.	CO25C6CHO, C517CHO, HMVKBCHO
O <sub>3</sub> 1 <sup>st</sup> gen.	C622CHO, C624CHO, C729CHO
ROOH	LIMAOOH, LIMBOOH, LIMCOOH, LMKAOOH, LMKBOOH, LIMALOOH, C817OOH, C926OOH, LIMALAOOH, LIMALBOOH, C923OOH, C924OOH, C728OOH, C622OOH, C826OOH, C729OOH, C627OOH, C818OOH, C517OOH
RONO2	LIMANO3, LIMBNO3, LIMCNO3, LMKANO3, LMKBNO3, LIMALNO3, C923NO3, C817NO3, C728NO3, C826NO3, C517NO3
PANs	C923PAN, C822PAN, C729PAN, C622PAN, C817PAN, C626PAN, C823PAN, C727PAN, C627PAN, C517PAN, C5PAN2, HMVKBPAN, PHAN, PAN

**Table S1.** MCM species that are included for the calculation of the contribution to  $k_{\text{OH\_intermediate}}$ .

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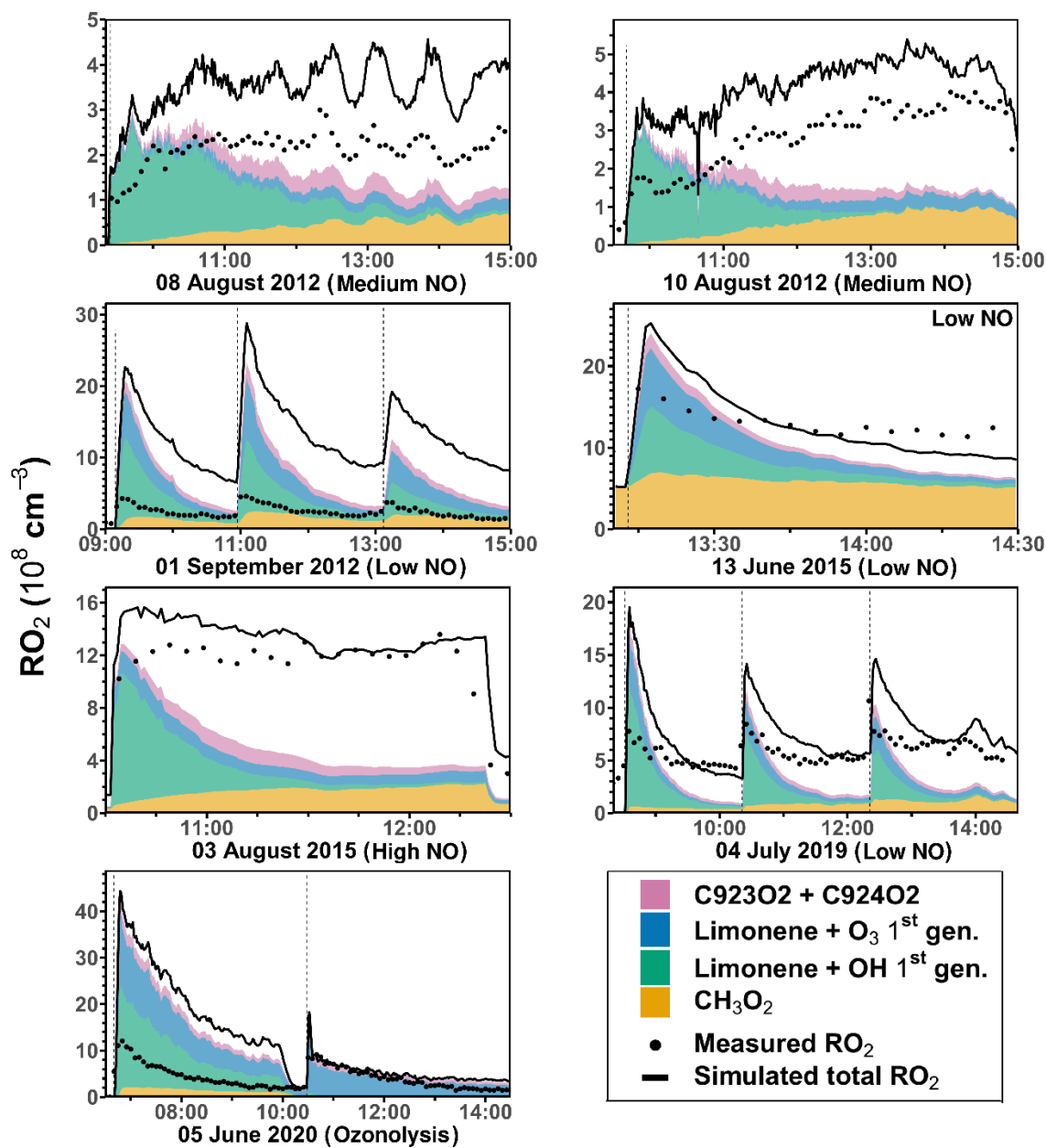
110 **Figure. S6** OH reactivity ( $k_{\text{OH}}$ ) contributions from the oxidation of limonene-derived products and intermediates from the measurements and modelled values. The model results are based on the constrained model run (O<sub>3</sub>, NO<sub>x</sub>, HONO, and HO<sub>2</sub> are constrained). The modelled total OH reactivity,  $k_{\text{OH,intermediate}}$ , is less than sum of single contributions on 13 June 2015, because the slowly increasing chamber background reactivity is not captured throughout the experiment.



**Figure S7.** Similiar to Fig. 8 in the main text. 10-minutes-average values of total OH destruction rates compared to the sum of OH production rates from the main OH sources that can be calculated from measurements. Shaded areas in the difference plots give the uncertainties of the calculations. Production of OH from the reaction of  $O_3$  and  $HO_2$  was negligible ( $< 0.01 \text{ ppbv h}^{-1}$ ) for conditions of the experiments.

## 6. Composition of $RO_2$ in the simulation (Section 3.4 in the main text)

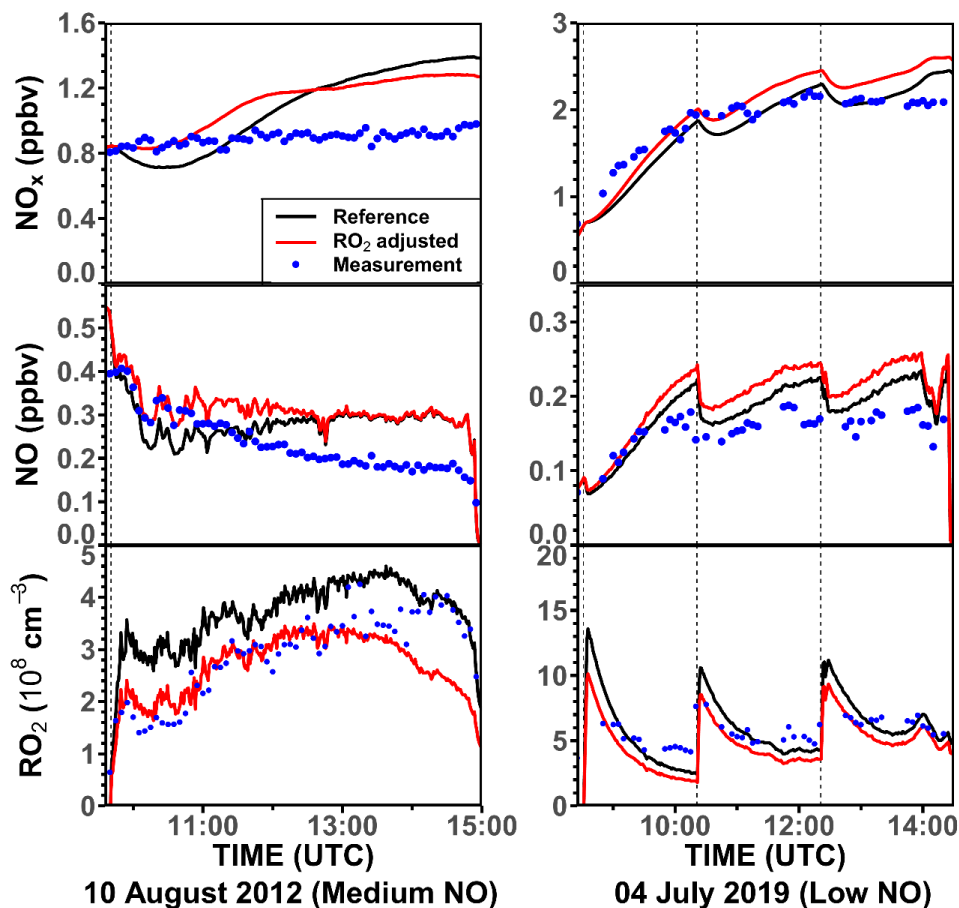
To identify the cause of the overestimation of peroxy radicals in the low  $NO_x$  and the ozonolysis experiments, concentrations of the peroxy radicals from the oxidation reaction are calculated and divided into four groups. The first group consists of the three peroxy radicals from the oxidation of limonene by OH, which includes LIMAO<sub>2</sub>, LIMBO<sub>2</sub> and LIMCO<sub>2</sub> (naming follows the MCM); the second group consists of the main peroxy radicals that are produced from limonene ozonolysis, which includes LIMALAO<sub>2</sub>, LIMALBO<sub>2</sub>, and CH<sub>3</sub>CO<sub>3</sub>; the third group consists of C<sub>9</sub>23O<sub>2</sub> and C<sub>9</sub>24O<sub>2</sub>, which is the minor peroxy radical products from the ozonolysis reaction and one of the peroxy radicals produced from the OH-oxidation of the first-generation OH-oxidation product; and the fourth group is the methyl peroxy radical (CH<sub>3</sub>O<sub>2</sub>), which is produced from reactions of CH<sub>3</sub>CO<sub>3</sub> as well as the oxidation of methane during the experiment on 13 June 2015.



**Figure S8.** Similar to Fig. 9 in the main text. The total  $RO_2$  radical concentrations and their speciation from model calculations (constrained model run) compared to the measured values for all the experiments. Methylperoxy radicals ( $CH_3O_2$ ) are mainly produced from the oxidation of ~~limonene~~HCHO in most of the experiments or from the oxidation of  $CH_4$  during the experiment on 13 June 2015. Radicals directly produced from the reaction of limonene with either OH or  $O_3$  are summed. C923O2 +

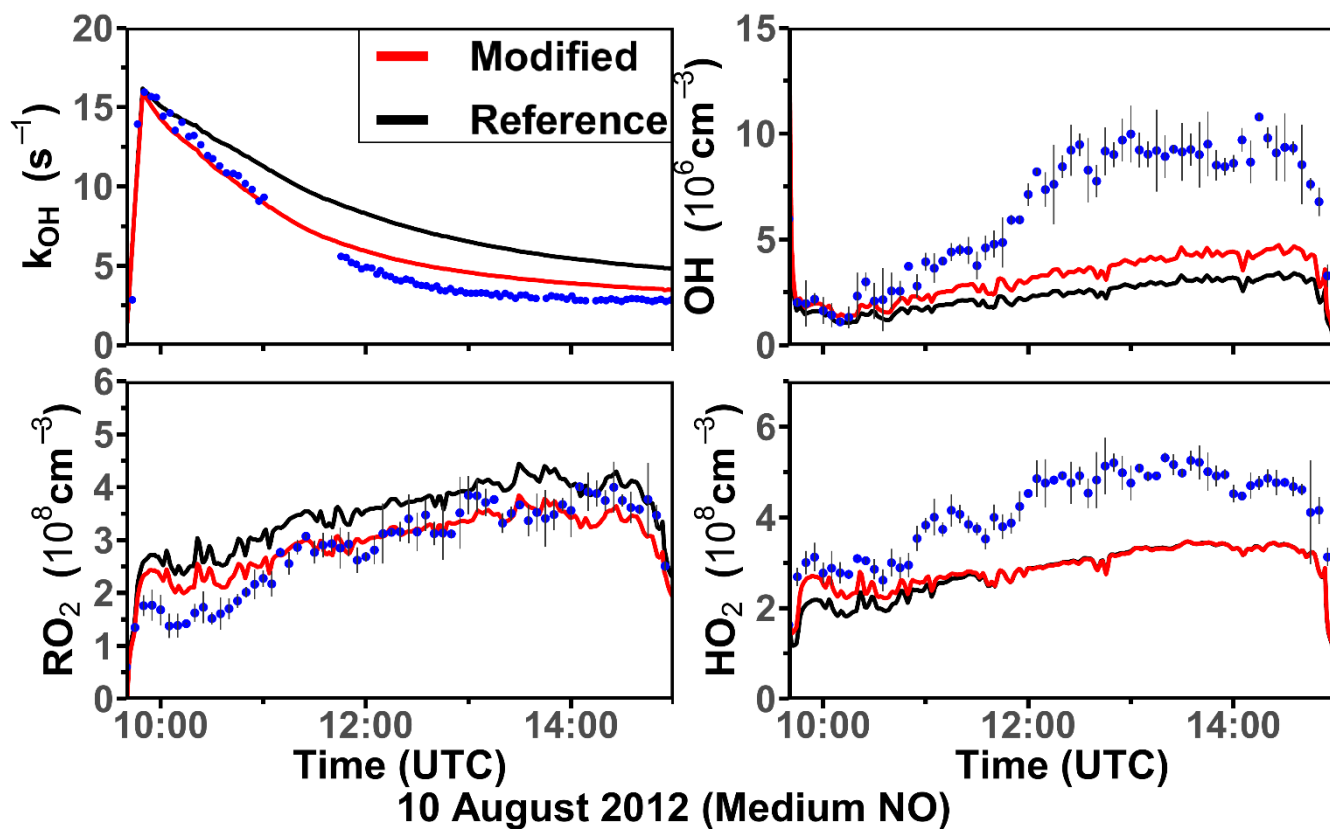
C924O2 are RO<sub>2</sub> radicals produced from the further oxidation of the first-generation oxidation products. Names are taken from the MCM.

## 140 7. Impacts of RO<sub>2</sub> model results on the modelled NO<sub>x</sub> concentrations (Section 3.5 in the main text)

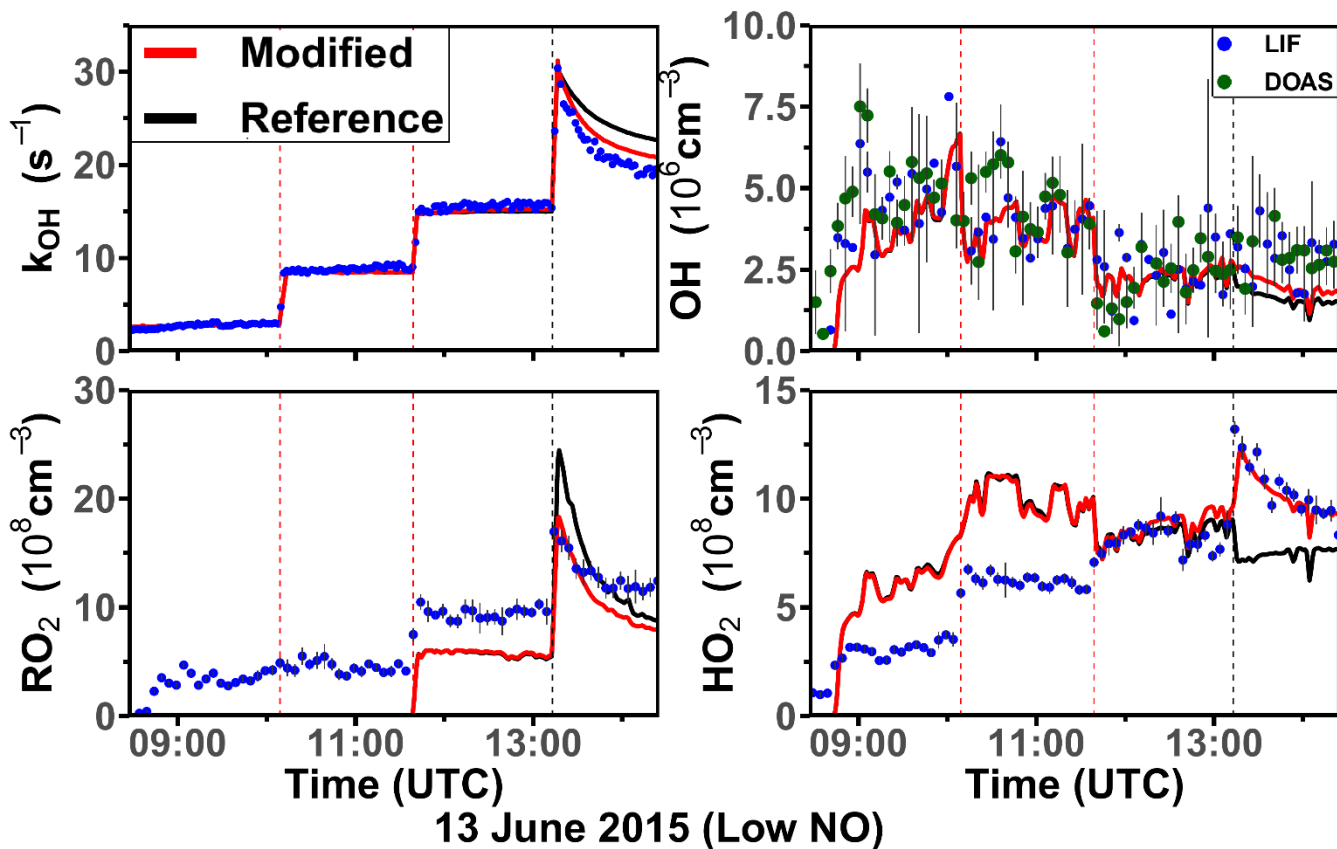


**Figure S9.** Similar to Fig. 10 in the main text. Example of the impact of modelled RO<sub>2</sub> on the modelled NO<sub>x</sub> and NO concentrations in the experiments with medium NO (10 August 2012) and low NO (04 July 2019) concentrations. In both cases, the organic nitrate yield for the first-generation RO<sub>2</sub> from the limonene+OH reaction is taken from the analysis in this work (34%).

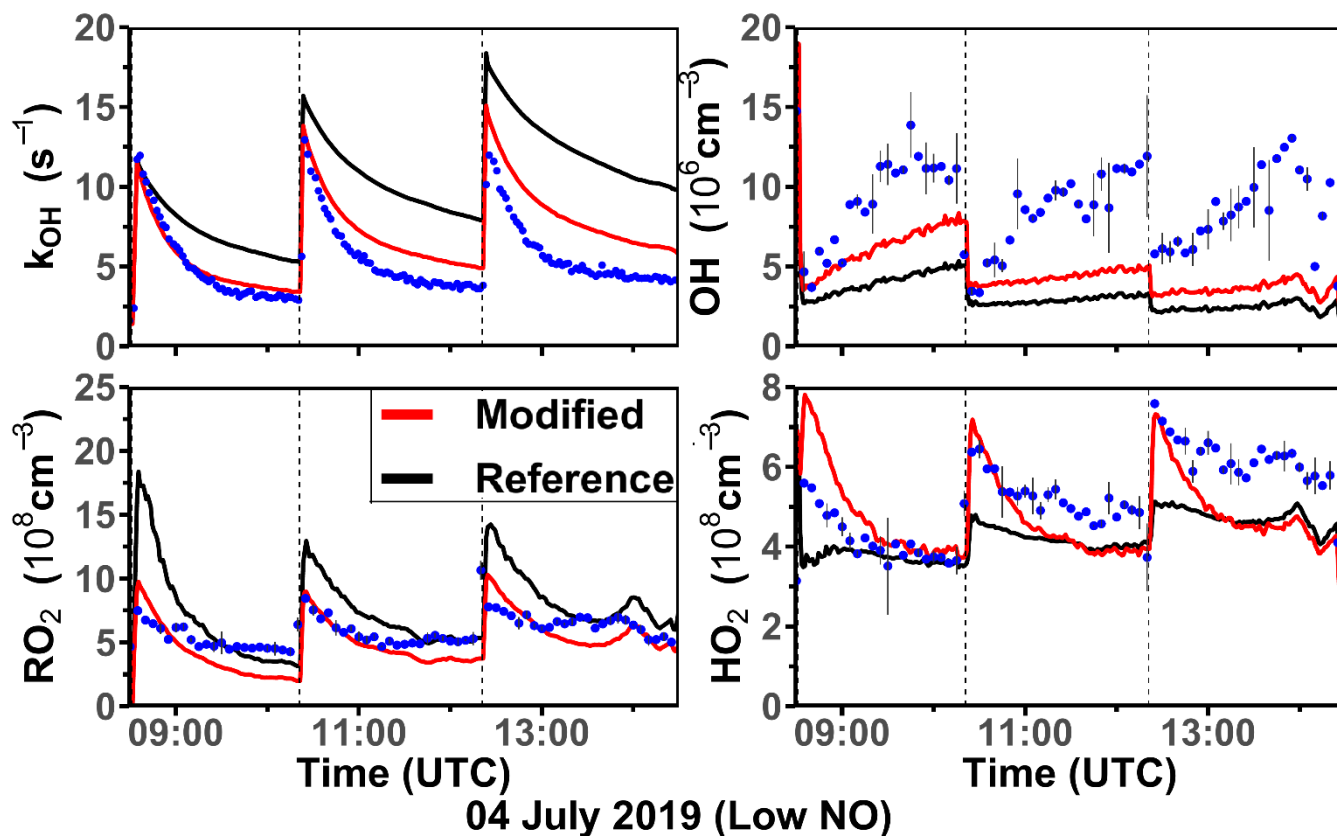
## 8. Sensitivity run (Section 4.1 in the main text)



**Figure S10.** Similar to Fig. 12 to Fig. 14 in the main text. Modelled and measured OH reactivity,  $HO_2$ ,  $RO_2$ , and OH concentrations for the experiments with medium NO concentrations on 10<sup>th</sup> August 2012. Results from the reference model (reference) and the sensitivity model run (modified) that includes additional  $RO_2$  loss processes that produce  $HO_2$ .



**Figure S11.** Similar to Fig. 12 to Fig. 14 in the main text. Modelled and measured OH reactivity, HO<sub>2</sub>, RO<sub>2</sub>, and OH concentrations for the experiments with low NO concentrations on 13<sup>th</sup> June 2015. Results from the reference model (reference) and the sensitivity model run (modified) that includes additional RO<sub>2</sub> loss processes that produce HO<sub>2</sub>.



**Figure S12.** Similar to Fig. 12 to Fig. 14 in the main text. Modelled and measured OH reactivity, HO<sub>2</sub>, RO<sub>2</sub>, and OH concentrations for the experiments with low NO concentrations on 04<sup>th</sup> July 2019. Results from the reference model (reference) and the sensitivity model run (modified) that includes additional RO<sub>2</sub> loss processes that produce HO<sub>2</sub>.

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