

# Iron from coal combustion particles dissolves much faster than mineral dust under simulated atmospheric acid conditions

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**Abstract.** Mineral dust is the largest source of aerosol iron (Fe) to the offshore global ocean, but acidic processing of coal fly ash (CFA) in the atmosphere ~~could be an important source of soluble aerosol Fe~~ may result in a disproportionately higher contribution of bioavailable Fe. Here, we determined the Fe speciation and dissolution kinetics of CFA from Aberthaw (United Kingdom), Krakow (Poland), and Shandong (China) in solutions which simulate atmospheric acidic processing. In CFA-PM<sub>10</sub> fractions, 8%-21.5% of the total Fe was as hematite and goethite (dithionite extracted Fe), 2%-6.5% as amorphous Fe (ascorbate extracted Fe), while magnetite (oxalate extracted Fe) varied from 3%-22%. The remaining 50%-87% of Fe was associated with ~~other Fe-bearing phases, possibly~~ aluminosilicates. High concentrations of ammonium ~~sulphate-sulfate~~ ((NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>), often found in wet aerosols, increased Fe solubility of CFA up to 7 times at low pH (2-3). ~~The oxalate effect on the Fe dissolution rates at pH 2 varied considerably depending on the samples, from no impact for Shandong ash to doubled dissolution for Krakow ash~~ Our results showed a large variability in the effects of oxalate on the Fe dissolution rates at pH 2, ~~from no impact in Shandong ash to doubled dissolution in Krakow ash~~. However, this enhancement was suppressed in the presence of high concentrations of (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>. Dissolution of highly reactive (~~amorphous~~) Fe was insufficient to explain the high Fe solubility at low pH in CFA, and the modelled dissolution kinetics suggests that other ~~Fe-bearing~~ phases such as magnetite may also dissolve ~~relatively~~ rapidly under acidic conditions. Overall, Fe in CFA dissolved up to 7 times faster ~~than in a Saharan dust precursor sample~~ than in Saharan dust samples at pH 2. Based on these laboratory data, we developed a new scheme for the proton- and oxalate- promoted Fe dissolution of CFA, which was implemented into the global atmospheric chemical transport model IMPACT. The revised model showed a better agreement with observations ~~of surface concentration of dissolved Fe~~ Fe solubility in aerosol particles over the Bay of Bengal, ~~due to the initial rapid release of Fe and the suppression of the oxalate-promoted dissolution at low pH~~ due to the rapid Fe release at the initial stage at highly acidic conditions. The improved model ~~also~~ enabled us to predict sensitivity to a more dynamic range of pH changes, particularly between anthropogenic combustion and biomass burning aerosols.

## 36 **1 Introduction**

37 The availability of iron (Fe) limits primary productivity in high-nutrient low-chlorophyll (HNLC) regions of the global ocean  
38 including the subarctic North Pacific, the East Equatorial Pacific and the Southern Ocean (Boyd et al., 2007; Martin, 1990). In  
39 other regions of the global ocean such as the subtropical North Atlantic, the Fe input may affect primary productivity by  
40 stimulating nitrogen fixation (Mills et al., 2004; Moore et al., 2006). These areas are particularly sensitive to changes in the  
41 supply of bioavailable Fe. Atmospheric aerosols are an important source of soluble (and, thus potentially ~~bio-~~  
42 ~~accessible~~bioavailable) Fe to the offshore global ocean. The deposition of ~~bio-accessible~~ bioavailable-Fe to the ocean can alter  
43 biogeochemical cycles and increase the carbon uptake, consequently affecting the climate (e.g., Jickells and Moore, 2015;  
44 Jickells et al., 2005; Kanakidou et al., 2018; Mahowald et al., 2010; Shi et al., 2012). In general, ~~bioavailable~~-~~bio-accessible~~  
45 Fe consists of aerosol dissolved Fe, and Fe-nanoparticles which can be present in the original particulate matter and/or formed  
46 during atmospheric transport as a result of cycling into and out of clouds (Shi et al., 2009). It is in addition possible that other  
47 more refractory forms of Fe could be solubilised in the surface waters by zooplankton (Schlosser et al., 2018) or the microbial  
48 community (Rubin et al., 2011).

49 ~~The Fe transported in the atmosphere~~ Atmospheric-Fe is largely derived from lithogenic sources, which contribute around 95%  
50 of the total Fe in suspended particles (e.g., Shelley et al., 2018) and ~~hence~~ most studies ~~so far have~~ concentrated on atmospheric  
51 processing of mineral dust (e.g., Cwiertny et al., 2008; Fu et al., 2010; Ito and Shi, 2016; Shi et al., 2011a; Shi et al., 2015).  
52 Mineral dust has low Fe solubility (dissolved Fe/ total Fe) near the source regions, generally below ~~0.51~~% (e.g., Shi et al.,  
53 2011c; Sholkovitz et al., 2009; Sholkovitz et al., 2012), increasing somewhat as a result of ~~processes occurring during~~  
54 ~~atmospheric transport~~atmospheric processing (e.g., Baker et al., 2021; Baker et al., 2020). Other sources of ~~bio-accessible~~  
55 ~~bioavailable~~ Fe to the ocean are from combustion sources such as biomass burning, coal combustion, ~~and~~ oil combustion, ~~and~~  
56 ~~metal smelting~~ (e.g., shipping emissions) (e.g., Ito et al., 2018; Rathod et al., 2020). Although these sources are only a small  
57 fraction of the total Fe in atmospheric particulates, the Fe solubility of pyrogenic sources can be 1–2 orders of magnitude  
58 higher than in mineral dust (~~Ito et al., 2021b and references therein~~), and thus can be important in promoting carbon uptake.  
59 However the Fe solubility of ~~these~~ pyrogenic sources ~~vary~~-~~varies~~ considerably depending on the particular sources with higher  
60 values observed for oil combustion and biomass burning ~~than coal combustion sources~~ (Ito et al., 2021b and references therein).

61 Wang et al. (2015) estimated that coal combustion ~~produces~~-emitted around  $\sim 0.9 \text{ Tg yr}^{-1}$  of ~~atmospheric~~-Fe ~~into the atmosphere~~  
62 (on average for 1960–2007), contributing up to  $\sim 86\%$  of the total anthropogenic Fe emissions. A more recent study, which has  
63 included metal smelting as ~~an~~ atmospheric Fe source, estimated that coal combustion emitted  $\sim 0.7 \text{ Tg yr}^{-1}$  of Fe for the year  
64 2010, contributing around 34% of the total anthropogenic Fe ~~atmospheric loading~~ (Rathod et al., 2020). Although the use of  
65 coal as a ~~principle~~-~~principal~~ energy source has been recently reduced as a result of concern about air quality and global warming,  
66 coal is still an important energy source in a number of countries in particular in the Asia-Pacific region (BP, 2020). In China,  
67 most of the total energy is supplied by coal, contributing over 50% of the global coal consumption in 2019, followed by India  
68 (12%), and the US (8%). Germany and Poland are the largest coal consumers in Europe, accounting together for around 40%  
69 of the European usage (BP, 2020). South Africa is also among the principal countries for coal consumption (BP, 2020) and is  
70 a source of ~~Fe-bearing~~ particles to the ~~Fe-limited~~anaemic Southern Ocean (e.g., Ito et al., 2019).

71 Coal fly ash (CFA) is a by-product of coal combustion. This generally consists of glassy spherical particles (e.g., Brown et al.,  
72 2011), which are formed through different transformations (decomposition, fusion, agglomeration, volatilization) of mineral  
73 matter in coal during combustion (e.g., Jones, 1995), and are transported with the flue gases undergoing rapid solidification.  
74 CFA are co-emitted with acidic gases such as sulf~~ph~~ur dioxide ( $\text{SO}_2$ ), nitrogen oxides ( $\text{NO}_x$ ) and carbon dioxide ( $\text{CO}_2$ ) (e.g.,  
75 Munawar, 2018).

76 During long-range transport, CFA particles undergo atmospheric processing with the CFA surface coated by acidic species  
77 such as ~~sulphuric-sulfuric~~ acid ( $\text{H}_2\text{SO}_4$ ) and oxalic acid ( $\text{H}_2\text{C}_2\text{O}_4$ ) in atmospheric aerosols. Aged CFA particles are hygroscopic  
78 and absorb water at typical relative humidity in the marine atmosphere. ~~As a result, -This forms-~~ a thin layer of water with high  
79 acidity, low pH and high ionic strength is formed around the particles (Meskhidze et al., 2003; Spokes and Jickells, 1995; Zhu  
80 et al., 1992). In addition, ammonia ( $\text{NH}_3$ ) which is a highly hydrophilic gas, can also partition into the aerosol phase, react  
81 with  $\text{H}_2\text{SO}_4$  and form ammonium ~~sulphate-sulfate~~ ( $(\text{NH}_4)_2\text{SO}_4$ ) an important inorganic salt contributing to the high ionic  
82 strength in ~~such aged~~ atmospheric aerosols (Seinfeld and Pandis, 2016).

83 ~~-At~~ low pH conditions, Fe solubility in aerosols increases, as the high concentration of protons ( $\text{H}^+$ ) weakens the Fe-O bonds  
84 facilitating the detachment of Fe from the surface lattice (Furrer and Stumm, 1986). Li et al. (2017) provided the first  
85 observational evidence ~~to confirm that the~~ acidification leads to the release of Fe from anthropogenic particles.

86 In addition to these inorganic processes, organic ligands can also enhance atmospheric Fe dissolution by forming soluble  
87 complexes with Fe (e.g., Cornell and Schwertmann, 2003). For example,  $\text{H}_2\text{C}_2\text{O}_4$  is an important organic species in  
88 ~~atmospheric~~ aerosols (e.g., Kawamura and Bikkina, 2016). Laboratory studies have demonstrated that  $\text{H}_2\text{C}_2\text{O}_4$  increases Fe  
89 solubility of ~~atmospheric~~ aerosol sources (Chen and Grassian, 2013; Johnson and Meskhidze, 2013; Paris and Desboeufs, 2013;  
90 Paris et al., 2011; Xu and Gao, 2008). Recently, observations over the Bay of Bengal indicate that  $\text{H}_2\text{C}_2\text{O}_4$  contributes to the  
91 increase of dissolved Fe in atmospheric water ~~dissolved-Fe~~ (Bikkina et al., 2020).

92 To simulate the Fe dissolution in CFA, it is necessary to determine the dissolution kinetics under realistic conditions. Previous  
93 studies have investigated the Fe dissolution kinetics of CFA under acidic conditions. Chen et al. (2012) simulated acidic and  
94 cloud processing of certified CFA. Fu et al. (2012) determined the dissolution kinetics of CFA samples at pH 2, while Chen  
95 and Grassian (2013) investigated the effect of organic species (e.g., oxalate and acetate) at pH 2-3. These studies showed that  
96 high acidity and the presence of oxalate enhanced Fe dissolution at the surface of CFA particles, similar to those reported in  
97 mineral dust (Chen et al., 2012; Chen and Grassian, 2013; Fu et al., 2012; Ito and Shi, 2016; Shi et al., 2011a). They also  
98 demonstrated that there are large differences in dissolution rates in different types of CFA, likely related to Fe speciation.

99 Furthermore, high ionic strength, commonly seen in aerosol water, affects the activity of molecular species present in solution,  
100 consequently it can significantly impact the Fe dissolution behaviour. Recent studies have considered the effect of the high  
101 ionic strength on the Fe dissolution kinetics of CFA under acidic conditions. For example, the Fe solubility of CFA samples  
102 was measured at pH 1-2 with high sodium chloride (NaCl) concentrations (Borgatta et al., 2016), and with high sodium nitrate  
103 ( $\text{NaNO}_3$ ) concentrations Kim et al. (2020). In real atmospheric conditions, NaCl or  $\text{NaNO}_3$  are unlikely to be the main driver  
104 of high ionic strength in aged CFA. Although NaCl can coagulate with dust particles in the marine boundary layer (Zhang et  
105 al., 2003), the aging of ~~coal-fly-ash~~CFA is primarily by the uptake of secondary species, particularly ~~sulphate-sulfate~~ and  
106 ammonia (Li et al., 2003). Ito and Shi (2016) found that at low pH and high concentration of  $(\text{NH}_4)_2\text{SO}_4$  the Fe solubility of  
107 mineral dust is likely to be enhanced by the adsorption of ~~sulphate-sulfate~~ ions on the particle surface. However, to date the  
108 effect of high  $(\text{NH}_4)_2\text{SO}_4$  concentrations on the Fe dissolution behaviour in combustion sources in the presence or absence of  
109 oxalate remains unknown.

110 The dissolution kinetics measured by Chen and Grassian (2013) ~~has-have~~ been used to develop a modelled dissolution scheme  
111 for CFA, assuming a single ~~Fe-bearing~~Fe phase in CFA (Ito, 2015). However, there are multiple ~~Fe-bearing~~ Fe phases in CFA,  
112 primarily hematite, magnetite and Fe in aluminium silicate glass (Brown et al., 2011; Chen et al., 2012; Fu et al., 2012; Kukier  
113 et al., 2003; Kutchko and Kim, 2006; Lawson et al., 2020; Sutto, 2018; Valeev et al., 2019; Waanders et al., 2003; Wang, 2014;  
114 Zhao et al., 2006), but also accessory Fe-bearing minerals for example silicates, carbonate, ~~sulphides-sulfides~~ and ~~sulphates~~  
115 ~~sulfates~~ (Zhao et al., 2006). These phases have a range of reactivities. Previous studies showed that CFA dissolves much faster

116 during the first 1-2 hours than subsequently (Borgatta et al., 2016; Chen et al., 2012; Chen and Grassian, 2013; Fu et al., 2012;  
117 Kim et al., 2020), confirming the existence of multiple Fe-bearing phases within a single CFA sample with large different  
118 difference in Fe dissolution from different phases dissolution behaviour.

119 In this study, laboratory experiments were conducted to determine the dissolution kinetics of coal combustion sources emission  
120 products (e.g., i.e., coal fly ash CFA) during simulated atmospheric acidic processing in the presence of  $(\text{NH}_4)_2\text{SO}_4$  and oxalate  
121 which are commonly found in atmospheric aerosols. In particular, we investigated the effect of high  $(\text{NH}_4)_2\text{SO}_4$  concentrations  
122 on the proton-promoted and oxalate-promoted Fe dissolution at low pH conditions. Our study also determined the Fe-bearing  
123 Fe-phases present in the CFA and compared them to those present in mineral dust. The experimental results enabled us to  
124 develop a new Fe release scheme for CFA sources which was then implemented into the global atmospheric chemical transport  
125 model IMPACT. The model results were compared with observations of Fe solubility surface concentration of dissolved Fe in  
126 aerosol particles over the Bay of Bengal from Bikkina et al. (2020).

## 127 2 Materials and Methods

### 128 2.1 Sample collection and subsequent size fractionation

129 CFA samples were collected from the electrostatic precipitators at three coal-fired power stations at different locations: United  
130 Kingdom (Aberthaw ash), Poland (Krakow ash), and China (Shandong ash). The bulk samples were resuspended to obtain  
131 dust aerosol fractions representative of particles emitted into the atmosphere. A custom-made resuspension system was used  
132 to collect the  $\text{PM}_{10}$  fraction (particles with an aerodynamic diameter smaller than  $10\ \mu\text{m}$ ), which is shown in Fig. S1. Around  
133 20 g of sample was placed into a glass bottle and injected at regular intervals (2-5 sec) into a glass reactor ( $\sim 70\ \text{L}$ ) by flushing  
134 the bottle with pure nitrogen. The air in the reactor was pumped at a flow rate of  $30\ \text{L}\ \text{min}^{-1}$  into a  $\text{PM}_{10}$  sampling head.  
135 Particles were collected on  $0.6\ \mu\text{m}$  polycarbonate filters and transferred into centrifuge tubes. The system was cleaned  
136 manually and flushed for 10 min with pure nitrogen before loading a new sample. A soil sample from Libya (Soil 5,  
137 32.29237N/22.30437E) was dry sieved to  $63\ \mu\text{m}$  (which is referred to as Libya dust) and used as an analogue for a Saharan  
138 mineral dust precursor to make a comparison between CFA and mineral dust and used for the comparison of CFA with mineral  
139 dust.

### 140 2.2 Fe dissolution kinetics

141 The Fe dissolution kinetics of the CFA samples was/were determined by time-dependent leaching experiments. We followed  
142 a similar methodology as in Ito and Shi (2016).  $\text{PM}_{10}$  fractions were exposed to  $\text{H}_2\text{SO}_4$  solutions at pH 1, 2 or 3, in the presence  
143 of  $\text{H}_2\text{C}_2\text{O}_4$  and/or  $(\text{NH}_4)_2\text{SO}_4$  to simulate acidic processing in aerosol conditions. The concentration of  $\text{H}_2\text{C}_2\text{O}_4$  in the  
144 experiment solutions was chosen based on the molar ratio of oxalate and sulphate-sulfate in  $\text{PM}_{2.5}$  (particles with an  
145 aerodynamic diameter smaller than  $2.5\ \mu\text{m}$ ) from observations over the East Asia region (Yu et al., 2005). Around 50 mg of  
146 CFA was leached in 50 ml of acidic solution to obtain a dust particles/liquid ratio of  $1\ \text{g}\ \text{L}^{-1}$ . The sample solution was mixed  
147 continuously on a rotary mixer, in the dark at room temperature. A volume of 0.5 mL was sampled at fixed time intervals (2.5,  
148 15, 60 min and 2, 6, 24, 48, 72, and 168 hours after the CFA sample was added to the experiment solution) and filtered through  
149  $0.2\ \mu\text{m}$  pore size syringe filters. The dissolved Fe concentration in the filtrate was determined using the ferrozine method  
150 (Viollier et al., 2000). Leaching experiments were also conducted on the Libyan dust precursor sample. The relative standard  
151 deviation (RSD) at each sampling time varied from 4 % to 15 % ( $n=7$ ).

152 The pH of all the experiment solutions was calculated using the E-AIM model III for aqueous solutions (Wexler and Clegg,  
153 2002). In part this was because the high ionic strength generated by the elevated concentration of  $(\text{NH}_4)_2\text{SO}_4$  prevents  
154 electrochemical sensors from making accurate pH measurements. For the experiment solutions with no  $(\text{NH}_4)_2\text{SO}_4$ , the pH

155 was measured by a pH meter before adding the ash and at the end of the experiments. The solution pH increased after adding  
156 the ash, and the change in pH was used to estimate the buffer capacity of alkaline minerals in the samples, including for  
157 example calcium carbonates ( $\text{CaCO}_3$ ), lime ( $\text{CaO}$ ), and portlandite ( $\text{Ca(OH)}_2$ ). The estimated concentration of  $\text{H}^+$  buffered was  
158 used to input the concentration of  $\text{H}^+$  into the E-AIM model. For each experiment, the pH was calculated before adding the  
159 CFA samples and at the end of the experiments. The pH of the original solution before adding the samples was estimated from  
160 the molar concentrations ( $\text{mol L}^{-1}$ ) of  $\text{H}_2\text{SO}_4$ ,  $\text{H}_2\text{C}_2\text{O}_4$  and  $(\text{NH}_4)_2\text{SO}_4$  used to prepare the solution. The model inputs included  
161 the total concentrations of  $\text{H}^+$  (without  $\text{H}_2\text{C}_2\text{O}_4$  contribution),  $\text{NH}_4^+$ ,  $\text{SO}_4^{2-}$  and  $\text{H}_2\text{C}_2\text{O}_4$ . For the experiment solutions with no  
162  $(\text{NH}_4)_2\text{SO}_4$ , we calculated the final pH by reducing the total  $\text{H}^+$  concentration input into the model to match the pH measured  
163 at the end of the experiments. The buffered  $\text{H}^+$  was then estimated from the difference between the original and final  $\text{H}^+$   
164 concentration input into the model. To determine the final pH of the solutions with high ionic strength, the  $\text{H}^+$  concentration  
165 input in the model was calculated as the difference between the  $\text{H}^+$  concentration in the original solution and the buffered  $\text{H}^+$   
166 estimated at low ionic strength.

167 For the solution with no  $(\text{NH}_4)_2\text{SO}_4$ , the difference between calculated and measured pH is  $<7\%$ . Table S1 reports the  
168 concentrations of  $\text{H}_2\text{SO}_4$ ,  $\text{H}_2\text{C}_2\text{O}_4$  and  $(\text{NH}_4)_2\text{SO}_4$  in the experiment solutions, the original and final pH from model estimates  
169 (including  $\text{H}^+$  concentrations and activities), and the pH measurements for the solution with low ionic strength.

### 170 2.3 Sequential extractions

171 The content of Fe oxide species in the samples was determined by Fe sequential extraction (Baldo et al., 2020; Poulton and  
172 Canfield, 2005; Raiswell et al., 2008; Shi et al., 2011b). The Fe oxide species included highly reactive amorphous Fe oxide-  
173 hydroxide (FeA), crystalline Fe oxide-hydroxide, mainly goethite and hematite (FeD), and Fe associated with magnetite (FeM).

174 To extract FeA, samples were leached in an ascorbate solution buffered at pH 7.5 (Raiswell et al., 2008; Shi et al., 2011b). The  
175 ascorbate solution contained a deoxygenated solution of  $50 \text{ g L}^{-1}$  sodium citrate,  $50 \text{ g L}^{-1}$  sodium bicarbonate, and  $10 \text{ g L}^{-1}$  of  
176 ascorbic acid. Around 30 mg of CFA was leached for 24 hours in 10 mL of ascorbate extractant, mixed continuously on a  
177 rotary mixer. The extraction solution was then filtered through a  $0.2 \mu\text{m}$  membrane filter. In order to extract FeD, the residue  
178 was leached for 2 more hours in a dithionite solution buffered at pH 4.8 ( $50 \text{ g L}^{-1}$  sodium dithionite in 0.35 M acetic acid and  
179  $0.2 \text{ M}$  sodium citrate) (Raiswell et al., 2008; Shi et al., 2011b).

180 For the extraction of FeM, the CFA samples were first leached for 2 hours using a citrate-buffered dithionite solution to remove  
181 FeD. The residue collected after filtration was then leached for 6 hours in a solution of  $0.2 \text{ M}$  ammonium oxalate ( $(\text{NH}_4)_2\text{C}_2\text{O}_4$ )  
182 and  $0.17 \text{ M}$   $\text{H}_2\text{C}_2\text{O}_4$  at pH 3.2 (Poulton and Canfield, 2005). The Fe extractions were all carried out in the dark at room  
183 temperature. The Fe concentration in the filtered extraction solutions was measured using the ferrozine method (Viollier et al.,  
184 2000) or by inductively coupled plasma optical emission spectrometry (ICP-OES) analysis for the solutions containing high  
185 concentration of oxalate.

186 The total Fe content in the samples was determined by microwave digestion in concentrated nitric acid ( $\text{HNO}_3$ ) followed by  
187 inductively coupled plasma mass spectrometry (ICP-MS) analysis. [The recovery of Fe assessed using a standard reference](#)  
188 [material for urban particulate matter \(NIST SRM 1648A\) was around 89%. Therefore, the total Fe in the Libyan dust precursor](#)  
189 [sample could be underestimated somewhat as crystalline aluminium silicate minerals may not be fully digested.](#)

190 [The sequential extraction techniques were tested using the Arizona Test Dust \(ATD, Power Technology, Inc.\).](#) The RSD%  
191 obtained for each extract using the [Arizona-test dust ATD](#) was 3% for FeA, 11% for FeD, 12% for FeM ( $n=7$ ) and 2% for the  
192 total Fe ( $n=73$ ). [A summary of the results for the ATD is reported in Table S2.](#)

## 2.4 X-ray absorption near edge structure (XANES) analysis

We collected XANES spectra to qualitatively examine the Fe speciation in the CFA samples. The XANES spectra at the Fe K-edge were collected at the Diamond Light Source beamline I18. A Si(111) double-crystal monochromator was used in the experiments. The beam size was 400  $\mu\text{m}$   $\times$  400  $\mu\text{m}$ . The XANES spectra were collected from 7000 to 7300 eV at a resolution varying from 0.2 eV for 3 s in proximity to the Fe K-edge (7100–7125 eV) to 5 eV for 1 s from 7100 to 7300 eV. Powder samples were suspended in methanol and deposited on Kapton<sup>®</sup> tape. The analysis was repeated three times. We measured the XANES spectra of the CFA-PM<sub>10</sub> fractions and mineral standards including hematite, magnetite, and illite. Data were processed using the Athena program, part of the software package Demeter (version 0.9.26) (Ravel and Newville, 2005).

## 2.5 Model description

This study used the Integrated Massively Parallel Atmospheric Chemical Transport (IMPACT) model (Ito et al., 2021a and references therein). The model simulates the emission, chemistry, transport, and deposition of Fe-containing aerosols and the precursor gases of inorganic and organic acids. The coating of acidic species on the surface of Fe-containing aerosols promotes the release of soluble Fe in the aerosol deliquescent layer and enhances the aerosol Fe solubility (Li et al., 2017). On the other hand, the external mixing of oxalate-rich aerosols with Fe-rich aerosols can suppress the oxalate-promoted Fe dissolution at low concentration of oxalate near the source regions (Ito, 2015). However, the internal mixing of alkaline minerals such as calcium carbonate with Fe-containing dust aerosols can suppress the Fe dissolution (Ito and Feng, 2010). Since CFA particles are co-emitted with acidic species, the transformation of relatively insoluble Fe in coal combustion aerosols into dissolved Fe is generally much faster than that for mineral dust aerosols during their atmospheric lifetime (Ito, 2015; Ito and Shi, 2016). Additionally, the size of CFA particles is substantially smaller than that of mineral dust. Thus, we adopted an observationally constrained parameter for the dry deposition scheme (Emerson et al., 2020) to improve the simulation of dry deposition velocity of fine particles.

To improve the accuracy of our simulations of Fe-containing aerosols, we revised the on-line Fe dissolution schemes in the original model (Ito et al., 2021a) in conjunction with ~~the mineralogy-based emission rates and~~ a more dynamic range of pH estimates. ~~To implement 3-step dissolution schemes, we used the mineral-specific emission inventory for anthropogenic Fe emissions (Rathod et al., 2020).~~ To apply the Fe dissolution schemes for high ionic strength in aerosols, we used the mean activity coefficient for pH estimate (Pye et al., 2020). Moreover, the dissolution rate was assumed to be dependent of pH for highly acidic solutions (pH < 2) unlike in the former dissolution scheme (Ito, 2015), which allowed us to predict the sensitivity of Fe dissolution to pH lower than 2.

To validate the new dissolution scheme, we compared our model results with observations of ~~Fe solubility surface concentration of dissolved Fe~~ in PM<sub>2.5</sub> aerosol particles over the Bay of Bengal (Bikkina et al., 2020).

## 3 Experimental results

### 3.1 Fe dissolution kinetics

We determined that Krakow ash had the largest buffer capacity, around 0.008 moles of buffered H<sup>+</sup> per litre, which was related to the content of alkaline minerals in the sample. The buffer capacity of Aberthaw and Shandong ash was ~10 times smaller than that of Krakow ash, around 0.0007 moles of buffered H<sup>+</sup> per litre. Leaching Krakow ash in 0.005 M H<sub>2</sub>SO<sub>4</sub>, the initial concentration of H<sup>+</sup> was similar to the concentration of the H<sup>+</sup> buffered. As a result, the solution pH raised from approximately 2.1 to 2.7 corresponding to a pH change of around 20% (Table S1). For all the other experimental conditions, the pH change was below 12% (Table S1). At the pH conditions used in this study (pH 1-3), acid buffering was fast and likely

231 occurred within the first 1-2 hours. We assumed that the calculated final pH was representative of the solution pH over the  
232 duration of the experiments. The leaching experiments were conducted up to 168 h to better capture the dissolution curve in  
233 the kinetic model but also considering the tropospheric lifetime of aerosol particles.

234 Dissolved Fe at different time intervals is reported as Fe%, which is the fraction of Fe dissolved to the total Fe content (FeT)  
235 in the CFA samples. For all samples, a fast dissolution rate was observed at the beginning of the experiment. In the case of  
236 Krakow ash, ~~a~~the dissolution plateau was reached after 2-hour leaching in 0.005 M H<sub>2</sub>SO<sub>4</sub> as sufficient Fe may be dissolved  
237 from the highly reactive Fe species to suppress the dissolution of less reactive Fe which was likely due to the pH change. For  
238 that sample/initial condition the pH increased to 2.7, and no more Fe was dissolved, leading to a total Fe solubility of ~9%  
239 over the duration of the experiment (7 days) (Fig. 1a). Dissolving Krakow ash in 0.01 M H<sub>2</sub>SO<sub>4</sub> (Fig. 1a), the experiment  
240 solution had a final calculated pH of 2.1. The total Fe solubility was 34% at pH 2.1, almost 4 times higher than that at pH 2.7  
241 (in 0.005 M H<sub>2</sub>SO<sub>4</sub>). Dissolution of Aberthaw and Shandong ash was slower compared to Krakow ash (Figs. 1b and 2c,  
242 respectively). Leaching Aberthaw and Shandong ash in 0.005 M H<sub>2</sub>SO<sub>4</sub> resulted in solutions with a pH of around 2.2. At this  
243 pH, the total Fe solubility was 18% for Aberthaw ash and 21% for Shandong ash, which is 9-10 times higher than the total Fe  
244 solubility at pH 2.9 (in 0.001 M H<sub>2</sub>SO<sub>4</sub>), around 2% for both samples.

245 The experimental treatment of dissolved Fe from Krakow ash in 0.05 H<sub>2</sub>SO<sub>4</sub> solution with 1 M (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> (Fig. 1a) resulted  
246 in a final predicted pH of 2.1. At that pH, the total Fe solubility of Krakow ash increased from 34% with no (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> to 48%  
247 with high (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> concentration. The total Fe solubility of Krakow ash was around 28% at pH 3.0 with 1 M (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>  
248 (Fig. 1a), 3 times higher than that at pH 2.7 with no (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>. At around pH 2, the total Fe solubility of Aberthaw (Fig. 1b)  
249 and Shandong ash (Fig. 1c) increased by around 20% and 30% in the presence of (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>. By contrast, the total Fe solubility  
250 at pH 3.1 with 1 M (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> was 7.5% for Aberthaw ash (Fig. 1b) and 14% for Shandong ash (Fig. 1c), respectively, which  
251 was around 4 and 7 times higher than in the experiments carried out at pH 2.9 without (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>.

252 The Fe dissolution of the CFA samples in H<sub>2</sub>SO<sub>4</sub> solutions with 0.01 M H<sub>2</sub>C<sub>2</sub>O<sub>4</sub> (at around pH 2) is shown in Fig. 2. The total  
253 Fe solubility of Krakow ash at pH 1.9 with 0.01 M H<sub>2</sub>C<sub>2</sub>O<sub>4</sub> was 61% (Fig. 2a), which was almost 2 times higher than that at  
254 pH 2.1 but without H<sub>2</sub>C<sub>2</sub>O<sub>4</sub> (Fig. 2a). For Aberthaw ash, oxalate contribution to the dissolution process led to a total Fe  
255 solubility of 30% at pH 2.0 (Fig. 2b), which was 70% higher than in the experiment carried out in 0.005 M H<sub>2</sub>SO<sub>4</sub> (~pH 2.2)  
256 (Fig. 2b). Shandong ash dissolution behaviour was not affected by the presence of oxalate (Fig. 2c).

257 We also investigated the effect of high (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> concentration on oxalate-promoted dissolution. In Fig. 2a, the total Fe  
258 solubility of Krakow ash decreased from 61% at pH 1.9 in the presence of oxalate to 54% at pH 2.0 with oxalate and (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>.  
259 For Aberthaw ash, the total Fe solubility at pH 2.0 decreased from 30% in the presence of oxalate to 19% after the addition of  
260 (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> (Fig. 2b).

261 Figure 3 shows the Fe dissolution behaviour of Krakow ash at different pH conditions in the presence of 1 M (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> and  
262 H<sub>2</sub>C<sub>2</sub>O<sub>4</sub> (0.01-0.03 M depending on the solution pH). The total concentration of oxalate ions was calculated using the E-AIM  
263 model and was similar at different pH conditions, 0.015 at pH 1.0 (Experiment 7 Table S2S3), 0.009 at pH 2.0, and 0.01 at pH  
264 2.9 (Experiments 3 Table S2S3). The highest total Fe solubility was observed at pH 1.0 (~67%). At pH 2.0, the total Fe  
265 solubility decreased to 54%, and no substantial variations were observed between pH 2.0 and pH 2.9 (54% -51%). At pH 1.0,  
266 the concentration of H<sup>+</sup> was considerably higher compared to pH 2.0-2.9, leading to a faster dissolution rate. The total  
267 concentration of oxalate ions was 1.5-1.6 times higher in the solution at pH 1.0 than at pH 2.0-2.9, which may also contribute  
268 to the faster dissolution rate. C<sub>2</sub>O<sub>4</sub><sup>2-</sup> concentration increased with rising pH. Although the concentration of H<sup>+</sup> was lower at pH  
269 2.9 than at pH 2.0, the E-AIM model estimated that C<sub>2</sub>O<sub>4</sub><sup>2-</sup> contributed around 35% of the total oxalate concentration at pH  
270 2.9, which was 4.5 times higher than at pH 2.0 (Experiments 3 Table S2S3). The similar dissolution behaviour at pH 2.0 and

271 pH 2.9 conditions may reflect the combination of these two opposite factors, higher concentration of  $C_2O_4^{2-}$  but lower  
272 concentration of  $H^+$  at pH 2.9 compared to 2.0.

273 We determined the Fe dissolution behaviour of Krakow ash at pH 1.0 in the presence of oxalate and increasing concentrations  
274 of  $(NH_4)_2SO_4$ . The ash was leached in  $H_2SO_4$  solutions with 0.03 M  $H_2C_2O_4$  at pH 1.0, while the concentration of  $(NH_4)_2SO_4$   
275 varied from 0 to 1.5 M. In Fig. 4, the total Fe solubility of Krakow ash in the presence of oxalate was 75% at pH 1.0 and  
276 decreased to 68% after the addition of 0.5 M  $(NH_4)_2SO_4$ . Higher  $(NH_4)_2SO_4$  concentrations did not affect the Fe dissolution  
277 behaviour in the presence of oxalate at pH 1.0.

### 278 3.2 Fe speciation

279 The Fe-bearing Fe-phases in the CFA samples determined through sequential extractions are shown in Fig. 5c. The Fe  
280 speciation in the Saharan-Libyan dust precursor-sample is added for comparison. Krakow ash had a total Fe (FeT) content of  
281 5.2%, while FeT in Aberthaw and Shandong ash was 3.1% and 1.6% respectively. Amorphous Fe (FeA/FeT) was 6.5% in  
282 Krakow ash, 2% in Aberthaw ash, and 4.6% in Shandong ash. The CFA samples showed very different dithionite Fe (FeD/FeT)  
283 content, 21.5% in Krakow ash, 8% in Aberthaw ash and 14.8% in Shandong ash. The content of magnetite (FeM/FeT) was  
284 considerably higher in Krakow ash (22.4%) compared to Aberthaw (2.9%) and Shandong (4.5%) ash. About 50%–87% of Fe  
285 was contained in other phases most likely in aluminosilicates. Overall, CFA had more magnetite and highly reactive amorphous  
286 Fe and less dithionite Fe than the Libyan dust precursor sample.

287 In Figs. S25a-b, the Fe K-edge XANES spectra of Krakow and Aberthaw ash showed a single peak in the pre-edge region at  
288 around 7114.3 eV and 7114.6 eV, respectively. In the edge region, Aberthaw ash showed a broad peak at around 7132.2 eV,  
289 while the peak of Krakow ash was slightly shifted to 7132.9 eV and narrower. The pre-edge peak at around 7115.4 suggests  
290 that Fe was mainly as Fe(III). The spectral features of Aberthaw and Krakow ash are different from those of the hematite,  
291 magnetite and illite standards suggesting that the glass fraction was dominant and controlled their spectral characteristics,  
292 which is consistent with the results of the Fe sequential extractions. The XANES Fe K-edge spectra of the CFA samples have  
293 some common features with those of Icelandic dust but tend to differ from mineral dust sourced in the Saharan dust source  
294 region. In the pre-edge region of the spectrum, Icelandic dust (sample D3 in Figs. 5a-b) showed a main peak at around  
295 7114.4 eV and a second less intense peak at around 7112.7 eV, while a broad peak was observed at around 7131.9 eV in the  
296 edge region (Baldo et al., 2020). A mineral dust sample from western Sahara (WS dust in Figs. 5a-b) showed a distinct double  
297 peak in the pre-edge region at around 7113.9 and 7115.2 eV, and a main peak in the edge region at around 7133.3 eV (Baldo  
298 et al., 2020). The XANES Fe K-edge spectra of the CFA samples have some common features with those of Icelandic dust, but  
299 differs from northern African dust (Fig. S2). Aluminium silicate glass is also dominant in Icelandic dust (Baldo et al., 2020).  
300 In the pre-edge region, Icelandic dust (sample MIR 45 in Fig. S2) showed a main peak at around 7114.4 eV and a second less  
301 intense peak at around 7112.7 eV, while a broad peak was observed at around 7131.9 eV in the edge region (Baldo et al., 2020).  
302 Northern African dust (western Sahara in Fig. S2) showed a distinct double peak in the pre-edge region at around 7113.9 and  
303 7115.2 eV, and a main peak in the edge region at around 7133.3 eV (Baldo et al., 2020). The similarities between Icelandic  
304 ash and CFA could be because aluminium silicate glass is dominant in these samples (e.g., Baldo et al., 2020; Brown et al.,  
305 2011), while Fe-bearing phases in mineral dust from the Saharan region are primarily iron oxides minerals such as hematite  
306 and goethite, clay minerals and feldspars (e.g., Shi et al., 2011b).

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## 307 4 Fe simulation from the IMPACT model

### 308 4.1 Fe dissolution scheme

309 Based on the laboratory experiments carried out on the CFA samples, we implemented a 3-step dissolution scheme for proton-  
310 promoted and oxalate-promoted Fe dissolution (Table 1). The Fe dissolution kinetics ~~was~~ ~~were~~ described as follows (Ito, 2015):

$$311 \sum_i RFe_i = k_i(pH, T) \times a(H^+)^{m_i} \times f_i \quad (1)$$

312 where  $RFe_i$  is the dissolution rate of individual mineral  $i$ ,  $k_i$  is the rate constant (moles Fe  $g^{-1} s^{-1}$ ),  $a(H^+)$  is the  $H^+$  activity in  
313 solution,  $m_i$  represents the empirical reaction order for protons. The function  $f_i$  ( $0 \leq f_i \leq 1$ ) accounts for the suppression of  
314 mineral dissolution by competition for oxalate between surface Fe and dissolved Fe (Ito, 2015):

$$315 f_i = 0.17 \times \ln([\text{lig}] \times [Fe]^{-1})_i + 0.63 \quad (2)$$

316 in which,  $[Fe]$  is the molar concentration (mol  $L^{-1}$ ) of  $Fe^{3+}$  dissolved in solution, and  $[\text{lig}]$  is the molar concentration of ligand  
317 (e.g., oxalate).  $f_i$  was set to 1 for the proton-promoted dissolution.

318 The scheme assumes 3 rate constants “fast”, “intermediate” and “slow” for the proton-promoted, and the proton + oxalate-  
319 promoted dissolution (Table 1). These were obtained by fitting the parameters to our measurements for Krakow ash in  $H_2SO_4$   
320 and  $(NH_4)_2SO_4$  at pH 2-3, with and without oxalate (Experiments 2 and 3 in Table S1), which are shown in Fig. 6. The fast  
321 rate constant represents highly reactive Fe species such as amorphous Fe oxyhydroxides, Fe carbonates and Fe  
322 ~~sulphates~~ ~~sulfates~~. The intermediate rate constant can be applied to nano-particulate Fe oxides, while more stable phases  
323 including for example Fe-aluminosilicate and crystalline Fe oxides have generally slower rates (Ito and Shi, 2016; Shi et al.,  
324 2011a; Shi et al., 2011b; Shi et al., 2015). Similarly, we predicted the dissolution kinetics of Aberthaw ash and Shandong ash  
325 (Figs. 7S3-S5). The dissolution kinetics of Krakow ash ~~were~~ ~~as~~ calculated based also on the experimental results at pH 1.0,  
326 which is shown in Fig. S6-S2 in comparison with kinetics predicted at pH 2.0 and pH 2.9 conditions.

327 The contribution of the oxalate-promoted dissolution to dissolved Fe was derived as the difference between the estimated  
328 dissolution rates for the proton + oxalate-promoted dissolution and the proton-promoted dissolution:

$$329 RFe_{i(\text{oxalate})} = RFe_{i(\text{proton} + \text{oxalate})} - RFe_{i(\text{proton})} \quad (3)$$

330 The Fe dissolution rates were predicted at a wider range of pH using Eq. (1) and Eq. (3) and the parameters in Table 1:

$$331 RFe_i = RFe_{i(\text{proton} + \text{oxalate})} \text{ when } RFe_{i(\text{oxalate})} < 0 \quad (4)$$

332 Since  $RFe_{i(\text{oxalate})}$  is less than 0 at low pH ( $< 2$ ), this equation applies to highly acidic conditions. As a result, the predicted  
333 amount of dissolved Fe was smaller when using the dissolution rate for the proton + oxalate-promoted dissolution,  $RFe_{i(\text{proton} +$   
334  $\text{oxalate})}$ , rather than the rate for the proton-promoted dissolution,  $RFe_{i(\text{proton})}$ , at pH  $< 2$ . Accordingly, the dissolution rate,  $RFe_i$ ,  
335 was less dependent on the pH compared to  $RFe_{i(\text{proton})}$  at highly acidic conditions, possibly due to the competition for the  
336 formation of surface complexes.

337 At pH  $> 2$  when oxalate does promote Fe dissolution, the following equation applies:

$$338 RFe_i = RFe_{i(\text{proton})} + RFe_{i(\text{oxalate})} \text{ when } RFe_{i(\text{oxalate})} > 0 \quad (5)$$

#### 339 4.2 Aerosol Surface concentration of dissolved Fe solubility over the Bay of Bengal

340 The new dissolution scheme was applied in the IMPACT atmospheric chemistry transport model to predict the Fe solubility  
341 surface concentration of dissolved Fe in atmospheric particles collected over the Bay of Bengal, which is an area for which  
342 there are detailed field measurements available (Bikkina et al., 2020; Kumar et al., 2010; Srinivas and Sarin, 2013; Srinivas et  
343 al., 2012) and multi-modelling analyses have been done (Ito et al., 2019). It thus represents a test for our experimental results  
344 in actual field conditions. Three sensitivity simulations were performed to explore the effects of the uncertainties associated  
345 with the dissolution schemes and mineralogical component of Fe. In addition, the former setting (Ito et al., 2021a) was used  
346 in the IMPACT model for comparison.

347 For all simulations, In sensitivity Test 0, the total Fe emissions from anthropogenic combustion sources and biomass burning  
348 emission in anthropogenic aerosols were estimated using Fe emission the Fe emission inventory of Ito et al. (2018)  
349 including also emissions from the iron and steel industry, whereas Fe emissions from mineral dust sources were dynamically  
350 simulated (Ito et al., 2021a) factors by each sector such as energy, heavy industry, and iron and steel industry for the simulation  
351 years (Ito et al., 2018), whereas in sensitivity Test 1, Test 2, and Test 3, the mineral-specific emission inventory for the year  
352 2010 by Rathod et al. (2020) was used. In Test 0, we ran the model without the upgrades of the dissolution scheme discussed  
353 in section 2.4, and apply in addition the photoinduced dissolution scheme for both combustion and dust aerosols (Ito, 2015;  
354 Ito and Shi, 2016), which was turned off in Test 1, Test 2, and Test 3 due to the lack of laboratory measurements under high  
355 ionic strength. To estimate the aerosol pH, we applied a H<sup>+</sup> activity coefficient of 1 for Test 0, while the mean activity  
356 coefficient from Pye et al. (2020) was used for the other tests. The dissolution rate was assumed as pH-independent for highly  
357 acidic solutions (pH < 2) (Ito, 2015) in Test 0, based on the laboratory measurements in Chen et al. (2012), while no pH  
358 threshold was considered in Test 1, Test 2, and Test 3 as the total dissolution (proton + oxalate) was suppressed at pH < 2 from  
359 the predicted dissolution rate.

360 In Test 1, we used the new dissolution scheme accounting for the proton- and oxalate- promoted dissolution of Krakow ash  
361 for all combustion aerosols in the model (Table 1). The dissolution kinetics was were calculated using the mineral-specific  
362 inventory base mineralogy for anthropogenic Fe emissions reported in Table S11 of Rathod et al. (2020). The Fe composition  
363 of wood was used for open biomass burning (Matsuo et al., 1992). In this simulation, 3-three Fe pools were considered.  
364 Sulphate-Sulfate Fe in Rathod et al. (2020) was assumed as fast pool, magnetite Fe as intermediate pool, hematite, goethite  
365 and clay Fe-aluminosilicate as slow pool. In Test 2, we calculated the dissolution kinetics only considering the proton-promoted  
366 dissolution. In Test 3, the Fe pools were as determined here for Krakow ash: ascorbate Fe (FeA) as fast pool, magnetite Fe  
367 (FeM) as intermediate pool, hematite plus goethite Fe (FeD) and other Fe as slow pool (Fig. 5). FeA contains highly reactive  
368 Fe species with fast dissolution rates (Raiswell et al., 2008; Shi et al., 2011b). FeM appeared to work well for the different fly  
369 ash samples in the dissolution scheme as intermediate Fe pool. FeD is associated with crystalline Fe oxides and a predominant  
370 proportion of this is which are mostly highly insoluble (Raiswell et al., 2008; Shi et al., 2011b), thus it was considered as slow  
371 pool in the dissolution scheme. We assumed other Fe to be mostly as-Fe-bearing aluminosilicates and considered this as slow  
372 Fe pool.

373 The temporally and regionally averaged, model-calculated surface concentration of aerosol Fe (Fig. 7), dissolved Fe (Fig. 8)  
374 and Fe solubility (Figs. 9 and S7) for the fine mode (PM<sub>2.5</sub>) along the cruise tracks were compared with the measurements over  
375 the Bay of Bengal for the period extending from 27 December 2008 to 26 January 2009 (Bikkina et al., 2020). Observations  
376 of total Fe concentration and Fe solubility in PM<sub>2.5</sub> along the cruise tracks over the Bay of Bengal for the period extending  
377 from 27 December 2008 to 26 January 2009 (Bikkina et al., 2020) were compared with temporally and regionally averaged  
378 data from model estimates. The daily averages of model results were calculated from hourly mass concentrations in the air  
379 over the surface ocean along the cruise tracks. The average aerosol Fe concentration of total Fe observed over the Bay of

380 Bengal ~~varies-varies~~ from  $145 \pm 144 \text{ ng m}^{-3}$  over the North Bay of Bengal (27 December 2008 - 10 January 2009) to  $55 \pm 23$   
381  $\text{ng m}^{-3}$  over the South Bay of Bengal (11-26 January 2009) (Bikkina et al., 2020). In Fig. 78, the modelled ~~-aerosol-Fe~~  
382 concentrations of total Fe exhibit a similar variability to that of measurements with relatively higher values over the North Bay  
383 of Bengal ( $101-59 \pm 57-29 \text{ ng m}^{-3}$  in Test 0, and  $81 \pm 37 \text{ ng m}^{-3}$  in Test 1-3 (different sensitivity simulations) compared to the  
384 South Bay of Bengal ( $21-20 \pm 123 \text{ ng m}^{-3}$  in different sensitivity simulations in Test 0, and  $34 \pm 25 \text{ ng m}^{-3}$  in Test 1-3).  
385 However, the modelled concentrations of total Fe were underestimated by a factor of  $2.9 \pm 1.5$ . The model reproduced the  
386 source apportionment of Fe (Fig. 78 - Table S4) which is qualitatively derived from previous observational studies indicating that  
387 the ~~aerosol-Fe~~ concentrations of total Fe in aerosols over the North Bay of Bengal are influenced by emissions of dust and  
388 combustion sources from the Indo-Gangetic Plain (Kumar et al., 2010), whereas combustion sources (e.g., biomass burning  
389 and fossil-fuel) from South-East Asia are dominant over the South Bay of Bengal (Kumar et al., 2010; Srinivas and Sarin,  
390 2013). On the other hand, the model could not reproduce the peak in total Fe concentration (1.8% of Fe content in  $\text{PM}_{2.5}$  sample)  
391 reported around 29 December 2008. The total Fe observed in  $\text{PM}_{10}$  ( $430 \text{ ng m}^{-3}$ ) on 29 December 2008 is lower than that  
392 measured on the day before ( $667 \text{ ng m}^{-3}$ ) and the day after ( $773 \text{ ng m}^{-3}$ ), whereas that in  $\text{PM}_{2.5}$  peaked on 29 December 2008  
393 (Srinivas et al., 2012). Thus, the extreme value recorded only for  $\text{PM}_{2.5}$  on this date may be an outlier. The total Fe observed in  
394  $\text{PM}_{2.5}$  ( $613 \text{ ng m}^{-3}$ ) is higher than that in  $\text{PM}_{10}$  ( $430 \text{ ng m}^{-3}$ ) (Srinivas et al., 2012). This may be due to the measurement  
395 uncertainty including sample collection with two different high-volume samplers (Kumar et al., 2010).

396 The comparison of Fe solubility using the same total Fe emissions directly represents the effect of the new dissolution scheme  
397 on  $\text{PM}_{2.5}$ .

398 The average aerosol dissolved Fe concentration measured over the North Bay of Bengal ( $16 \pm 9 \text{ ng m}^{-3}$ ) is slightly lower than  
399 that over the South Bay of Bengal ( $18 \pm 10 \text{ ng m}^{-3}$ ) (Bikkina et al., 2020). The model prediction of dissolved Fe over the North  
400 Bay of Bengal was  $6 \pm 2 \text{ ng m}^{-3}$  Fe in Test 0,  $21 \pm 10 \text{ ng m}^{-3}$  in Test 1, and  $31 \pm 28 \text{ ng m}^{-3}$  in Test 2, and  $13 \pm 10 \text{ ng m}^{-3}$  in  
401 Test 3. The aerosol dissolved Fe estimated over the South Bay of Bengal was  $6 \pm 1 \text{ ng m}^{-3}$  in Test 0,  $15 \pm 10 \text{ ng m}^{-3}$  in Test 1,  
402  $32 \pm 22 \text{ ng m}^{-3}$  in Test 2, and  $12 \pm 7 \text{ ng m}^{-3}$  in Test 3. In Fig. 8, our model results show that the contribution of mineral dust  
403 to aerosol dissolved Fe was higher over the North Bay of Bengal ( $14\% \pm 6\%$  in Test 1,  $28\% \pm 34\%$  in Test 2, and  $33\% \pm 26\%$   
404 in Test 3) compared to the South Bay of Bengal ( $3\% \pm 1\%$  in Test 1,  $1\% \pm 1\%$  in Test 2, and  $3\% \pm 1\%$  in Test 3). Overall,  
405 anthropogenic combustion sources were dominant over the Bay of Bengal accounting for  $84\% \pm 12\%$  in Test 1,  $72\% \pm 29\%$   
406 in Test 2, and  $69\% \pm 24\%$  in Test 3 of the aerosol dissolved Fe. Moreover, after 22 January 2009, the contribution of open  
407 biomass burning sources increased up to 47% in Test 1, 64% in Test 2, and 60% in Test 3 (Fig. 8).

408 The aerosol Fe solubility measured over the South Bay of Bengal is higher than that over the North Bay of Bengal, respectively  
409  $32\% \pm 11\%$  and  $15\% \pm 7\%$  (Bikkina et al., 2020), and model estimates showed a similar trend (Fig. S79). In Fig. S79 and  
410 Table S5, the calculated average Fe solubilities over the North Bay of Bengal in Test 1 ( $11\% \pm 4\%$ ), Test 2 ( $17\% \pm 5\%$ ), and  
411 Test 3 ( $17\% \pm 6\%$ ) in Test 3 ( $18\% \pm 10\%$ ) were in good agreement with observations, while lower Fe solubility was  
412 estimated in Test 0 ( $8\% \pm 5\%$ ) and higher values were obtained for Test 1 ( $28\% \pm 8\%$ ). The aerosol Fe solubility over the  
413 South Bay of Bengal was better captured in Test 1 ( $3043\% \pm 54\%$ ) and Test 3 ( $379\% \pm 7\%$ ), whereas Test 0 showed higher  
414 variability ( $378\% \pm 22\%$ ). The proton-promoted dissolution scheme in Test 2 significantly overestimated the Fe solubility over  
415 the Bay of Bengal (Fig. 9 and Table S5 Figs. 9 and S7). The aerosol Fe solubility was largely overestimated in all scenarios  
416 after 22 January 2009, as open biomass burning sources become dominant (Fig. 8 and Table S4).

417 The comparison between observations and model predictions of aerosol Fe solubility over the Bay of Bengal is shown in Fig.  
418 S93. The agreement between measurements and model predictions was the best in Test 1 and Test 3. These exhibited good  
419 correlation with observations ( $R = 0.60-49$  in Test 1 and  $R = 0.51-54$  in Test 3), and the lowest centred-root-mean-squared

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420 ~~(RMS)~~ difference between the simulated and observed ~~aerosol~~ Fe solubilities (RMSE = 116 in Test 1 and RMSE = 124 in Test  
421 3). In Test 0, the model estimates showed ~~higher-a-greater~~ difference from observations (RMSE = 221) and poor correlation  
422 (R = 0.2630).

## 423 5 Discussion

### 424 5.1 Dissolution behaviour of Fe in CFA

425 In this study, the Fe dissolution kinetics of CFA samples from UK, Poland and China ~~was-were~~ investigated under simulated  
426 atmospheric acidic conditions. A key parameter in both the atmosphere and the simulation experiments is the pH of the water  
427 interacting with the CFA particles. The lower the pH of the experimental solution the faster the dissolution and eventually the  
428 higher the amount of Fe dissolved. Our results showed a strong pH dependence in low ionic strength conditions, with higher  
429 dissolution rates at lower pH. For example, reducing the solution pH from 2.7 to 2.1, the Fe solubility of Krakow ash ~~in H<sub>2</sub>SO<sub>4</sub>~~  
430 ~~only~~ increased by a factor of 4 (Fig. 1a) over the duration of the experiments, while the Fe solubility of Aberthaw and Shandong  
431 ash increased by 9-10 times from pH 2.9 to pH 2.2 (Figs. 1b-c). This enhancement is higher than that observed in studies  
432 conducted on mineral dust samples, which showed that one pH unit can lead to 3-4 times difference in dissolution rates (Ito  
433 and Shi, 2016; Shi et al., 2011a). Furthermore, Chen et al. (2012) reported that the Fe solubility of the certified CFA 2689 only  
434 increased by 10% from pH 2 to pH 1, after 50 hours of dissolution in acidic media. The Fe solubility of CFA (PM<sub>10</sub> fractions)  
435 after 6 hours at pH 2 was 6%-10% for Aberthaw and Shandong ash respectively, and 28% for Krakow ash (Fig. 1). ~~The Fe in~~  
436 ~~our CFA samples initially dissolved faster than those used by Fu et al. (2012). These values are higher than the Fe solubilities~~  
437 ~~measured by Fu et al. (2012), who reported 2.9%-4.2% Fe solubility in bulk CFA from three coal-fired power plants in China~~  
438 ~~after 12-hour leaching at pH 2. This suggest that Fe in our CFA samples initially dissolved faster than those used in Fu et al.~~  
439 ~~(2012). The Fe solubility after 72-hour leaching in H<sub>2</sub>SO<sub>4</sub> at around pH 2 varied from around 12% and 17% (Aberthaw and~~  
440 ~~Shandong ash) to 34% (Krakow ash). These values are at the lower end of the range or below those reported in Chen et al.~~  
441 ~~(2012), who measured a Fe solubility of ~20%-70% in certified CFA samples after accumulated acid dissolution of 72 hours~~  
442 ~~at pH 2. These results suggest that there are considerable variabilities in the pH dependent dissolution of Fe in CFA. This -could~~  
443 ~~be due to differences in the Fe speciation between CFA samples and/or the different leaching media used.~~

444 Our results showed that high ionic strength has a major impact on dissolution rates of CFA at low pH (i.e., pH 2-3). The Fe  
445 solubility of CFA increased by approximately 20%-40% in the presence of 1 M (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> at around pH 2 over the duration  
446 of the experiments, and by a factor from 3 to 7 at around pH 3 conditions (Fig. 1). At high ionic strength, the activity of ions  
447 in solution is reduced, thus, in order to maintain similar pH conditions, the H<sup>+</sup> concentration has to be increased (Table S1).  
448 Although Fe dissolution was primarily controlled by the concentration of H<sup>+</sup>, the high concentration of ~~sulphate-sulfate~~ ions  
449 could ~~also~~ be ~~also~~ an important factor contributing to Fe dissolution, in particular when the concentration of H<sup>+</sup> in the system  
450 was low (e.g., pH 3). Previous research found that the high ability of anions to form soluble complexes with metals can enhance  
451 Fe dissolution (Cornell et al., 1976; Cornell and Schwertmann, 2003; Furrer and Stumm, 1986; Hamer et al., 2003;  
452 Rubasinghege et al., 2010; Sidhu et al., 1981; Surana and Warren, 1969). ~~Sulphate-Sulfate~~ ions adsorbed on the particles  
453 surface form complexes with Fe (e.g., Rubasinghege et al., 2010). This may increase the surface negative charge favouring the  
454 absorption of H<sup>+</sup> and thereby increase ~~the-dissolution-rate~~ ~~Fe dissolution at the particle surface~~. In addition, the formation of  
455 surface complexes may weaken the bonds between Fe and the neighbouring ions (Cornell et al., 1976; Furrer and Stumm,  
456 1986; Sidhu et al., 1981). Cwiertny et al. (2008) reported that at pH 1-2 the high ionic strength generated by NaCl up to 1 M  
457 did not influence Fe dissolution of mineral dust particles. However, Ito and Shi (2016) showed that the high ionic strength  
458 resulting from the addition of 1 M (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> in leaching solutions at pH 2-3 enhanced the Fe dissolution of dust particles,  
459 which was also observed here for the CFA samples. Borgatta et al. (2016) compared the Fe solubility of CFA from USA

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460 Midwest, North-East India, and Europe in acidic solution (pH 1-2) containing 1 M NaCl. The Fe solubility measured after 24  
461 hours varied from 15% to 70% in different CFA (bulk samples) at pH 2 with 1 M NaCl, which was considerably higher than  
462 that observed at pH 2 with 1 M NaNO<sub>3</sub> (<20%) (Kim et al., 2020). Both studies did not investigate the impact of ionic strength  
463 on the dissolution behaviour, i.e., by comparing the dissolution at low and high ionic strength. Note that both studies did not  
464 specify how the pH conditions were maintained at pH 2. Here, we considered the most important sources of high ionic strength  
465 in aerosol water and simulated Fe dissolution in the presence of (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> and H<sub>2</sub>C<sub>2</sub>O<sub>4</sub> under acidic conditions. We emphasize  
466 that the pH under high ionic strength here is estimated from a thermodynamic model, similar to those implemented in the  
467 IMPACT model.

468 The presence of oxalate enhanced Fe dissolution in Krakow and Aberthaw ash but not in Shandong ash at around pH 2 (Fig.  
469 2). The effect of oxalate on the Fe dissolution kinetics has also been studied by Chen and Grassian (2013) at pH 2 (11.6 mM  
470 H<sub>2</sub>C<sub>2</sub>O<sub>4</sub>). After 45-hour leaching, the Fe solubility of the certified CFA 2689 increased from 16% in H<sub>2</sub>SO<sub>4</sub> at pH 2 to 44% in  
471 H<sub>2</sub>C<sub>2</sub>O<sub>4</sub> at the same pH (Chen and Grassian, 2013). Therefore, the enhancement in Fe solubility of CFA in the presence of  
472 oxalate observed in this study (from no impact in Shandong ash to doubled dissolution in Krakow ash) is lower than ~~the 2.8~~  
473 ~~time increase in Fe solubility reported that reported~~ for the certified CFA 2689 ~~which was around by 2.8 times~~ (Chen and  
474 Grassian, 2013). Since no data are available in Chen and Grassian (2013), we are unable to make a comparison with the other  
475 two certified CFA samples. The Fe solubility of Krakow ash after 48-hour leaching at pH 1.9 with 0.01 M H<sub>2</sub>C<sub>2</sub>O<sub>4</sub> (Fig. 2a)  
476 was 53%, which is within the range of Fe solubilities observed in Chen and Grassian (2013) for the certified CFA samples at  
477 similar pH and H<sub>2</sub>C<sub>2</sub>O<sub>4</sub> concentrations (from 44% to 78%), whereas the Fe solubility of Aberthaw and Shandong ash (Figs.  
478 2b-c, 18%-17% after 48-hour leaching at pH 2.0 with 0.01 M H<sub>2</sub>C<sub>2</sub>O<sub>4</sub>) was considerably lower than that of certified CFA  
479 (Chen and Grassian, 2013). These results suggest a large variability in the effects of oxalate on the Fe dissolution rates in  
480 different types of CFA.

481 Our results also indicated that high (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> concentrations suppress oxalate-promoted Fe dissolution of CFA (Fig. 2), which  
482 was not considered in previous research. At pH 1.9 in the presence of oxalate, the Fe solubility of Krakow ash decreased by  
483 around 10% after the addition of (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>, while the Fe solubility of Aberthaw ash decreased by 35% (Fig. 2). We used the  
484 E-AIM model to estimate the concentration of oxalate ions and their activity (Table S2S3). The pH influences the speciation  
485 of H<sub>2</sub>C<sub>2</sub>O<sub>4</sub> in solution (e.g., Lee et al., 2007). H<sub>2</sub>C<sub>2</sub>O<sub>4</sub> is the main species below pH 2, whereas HC<sub>2</sub>O<sub>4</sub><sup>-</sup> is dominant between  
486 pH 2-4. Above pH 4, C<sub>2</sub>O<sub>4</sub><sup>2-</sup> is the principal species. In our experiments, H<sub>2</sub>C<sub>2</sub>O<sub>4</sub> is mainly as HC<sub>2</sub>O<sub>4</sub><sup>-</sup> at around pH 2  
487 (Experiments 3-4 in Table S2S3). In the presence of (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>, the activity coefficient of HC<sub>2</sub>O<sub>4</sub><sup>-</sup> was reduced by  
488 approximately 35-38% (Experiments 3 in Table S2S3). Increasing the ionic strength lowers the activity of the oxalate ions,  
489 but at the same time favours the dissociation of the acid. At around pH 2 conditions, the E-AIM model estimated that the  
490 activity of C<sub>2</sub>O<sub>4</sub><sup>2-</sup> was reduced by around one order of magnitude in the presence of (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>, while its concentration  
491 increased 12-15 times (Experiments 3 in Table S2S3). The adsorption of anions can reduce oxalate adsorption on the particle  
492 surface due to electrostatic repulsion which results in slower ~~dissolution rates~~release of Fe (Eick et al., 1999). Precipitation of  
493 ammonium hydrogen oxalate (NH<sub>4</sub>HC<sub>2</sub>O<sub>4</sub>) can also occur in the system, but this is very soluble and easily re-dissolves forming  
494 soluble oxalate species (Lee et al., 2007). We speculate that the high concentration of ~~sulphate-sulfate~~ ions is likely to be  
495 responsible for inhibiting the oxalate-promoted dissolution by reducing oxalate adsorption on the particle surface. At pH 1 in  
496 the presence of oxalate, increasing the concentration of (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> from 0.5 M to 1.5 M did not affect the Fe dissolution  
497 behaviour of the CFA samples (Fig. 4). As previously discussed, the adsorption of ~~sulphate-sulfate~~ ions on the particle surface  
498 may inhibit oxalate-promoted dissolution. However, once the saturation coverage is reached, increasing the concentration of  
499 anions has no further effect on the dissolution rate (Cornell et al., 1976).

500 Fe speciation is an important factor affecting the Fe dissolution behaviour. CFA particles have very different chemical and  
501 physical properties depending for example on the nature of coal burned, combustion conditions, cooling process and particle  
502 control devices implemented at the power stations (e.g., Blissett and Rowson, 2012; Yao et al., 2015). This is likely the reason  
503 why the Fe speciation observed in the CFA samples analysed in this study from different locations varied considerably (Fig.  
504 5). In the CFA samples, the Fe dissolution curves for different pH and ionic strengths generally showed the greatest rate of Fe  
505 release within the first 2 hours, followed by a slower dissolution, reaching almost a plateau at the end of the experimental run.  
506 This indicates the presence of multiple **Fe-bearing Fe**-phases in CFA particles with a wide range of reactivity. Initially, highly  
507 reactive phases were the main contribution to dissolved Fe. As the dissolution continued, ~~more stable~~**more refractory** phases  
508 became the dominant source of dissolved Fe (Shi et al., 2011a). SEM analysis conducted on CFA samples showed that CFA  
509 particles are mostly spherical (e.g., Chen et al., 2012; Dudas and Warren, 1987; Valeev et al., 2018; Warren and Dudas, 1989)  
510 with Fe oxide aggregates on the surface (Chen et al., 2012; Valeev et al., 2018). The analysis of the CFA samples processed  
511 in aqueous solution at low pH suggests that initially Fe dissolved from the reactive external glass coating (Dudas and Warren,  
512 1987; Warren and Dudas, 1989) and from the Fe oxide aggregates on the particle surface (Chen et al., 2012; Valeev et al.,  
513 2018). Subsequently, Fe is likely realised from the structure of the aluminium silicate glass (Chen et al., 2012; Dudas and  
514 Warren, 1987; Valeev et al., 2018; Warren and Dudas, 1989), and crystalline Fe oxide phases (Warren and Dudas, 1989).  
515 Overall, Krakow ash showed the fastest dissolution rates, but the dissolution of highly reactive Fe species as FeA is insufficient  
516 to account for the high Fe solubility observed at low pH. Our results showed that once the FeA dissolved, additional Fe was  
517 dissolved from more refractory **Fe-bearing Fe**-phases. The modelled dissolution kinetics obtained using FeM as intermediate  
518 pool were in good agreements with measurements (Figs. ~~S37-S26~~). FeM is likely to be primary magnetite but may contain a  
519 fraction of the more reactive aluminosilicate glass. Our model results suggest that magnetite in CFA particles may be more  
520 soluble than has been shown in Marcotte et al. (2020). It is possible that in real CFA samples the ~~mineral~~ physicochemical  
521 properties ~~of minerals~~ including for example crystal size, degree of crystallinity, cationic and anionic substitution in the lattice  
522 which influence the Fe dissolution behaviour (e.g., Schwertmann, 1991) are likely to be different from those of the reference  
523 minerals analysed in Marcotte et al. (2020). ~~In order to investigate the links between Fe solubility and Fe~~  
524 ~~speciation/mineralogy~~~~In order to estimate in detail the relative contribution of different mineral phases to dissolved Fe, more~~  
525 ~~work is needed to determine the Fe mineralogy in CFA samples at emission and after atmospheric processing, in combination~~  
526 ~~with solubility experiments~~~~most detailed work would be needed to determine Fe mineral phases in pristine and processed CFA~~  
527 ~~particles.~~

528 Finally, the modelled dissolution kinetics obtained using the new dissolution scheme for CFA (Table 1) showed better  
529 agreement with laboratory measurements than when using the original scheme (Ito, 2015) (Figs. ~~S8 and S9~~~~10~~). In Figs. ~~S8~~~~10a-~~  
530 ~~b~~, we compared the Fe dissolution kinetics of Krakow ash at around pH 2 and 3 with 1 M (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> calculated using the  
531 proton-promoted dissolution scheme in Table 1 with the dissolution kinetics calculated at similar pH but using the proton-  
532 promoted dissolution scheme for combustion aerosols in Ito (2015) (Table ~~S3~~~~56~~). The dissolution scheme in Ito (2015) was  
533 based on laboratory measurements conducted at low ionic strength (Chen et al., 2012) and assumed a single **Fe-bearing Fe**  
534 phase in combustion aerosol particles, while the new dissolution scheme considered the high ionic strength of aerosol water  
535 and assumed three rate constants, for fast, intermediate and slow kinetics of the different **Fe-bearing Fe**-phases present in CFA  
536 particles. The Fe dissolution kinetics obtained using the new dissolution scheme showed a better agreement with measurements  
537 and was enhanced compared to the model estimates obtained using the original dissolution scheme (Ito, 2015) for low ionic  
538 strength conditions (Figs. ~~S8~~~~10a-b~~). Figures ~~S9~~~~10c-d~~ shows the Fe dissolution kinetics of Krakow ash at pH 2.0 and 2.9 with  
539 0.01 M H<sub>2</sub>C<sub>2</sub>O<sub>4</sub> and 1 M (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> calculated using the proton- and oxalate-promoted dissolution scheme in Table 1 and the  
540 dissolution kinetics calculated at similar pH and H<sub>2</sub>C<sub>2</sub>O<sub>4</sub> concentration but using the scheme in Ito (2015) (i.e., single phase  
541 dissolution, see Table ~~S3~~~~56~~). The Fe dissolution kinetics predicted using the new dissolution scheme had a much better

542 agreement with measurements. Figure [S9e-10e](#) shows the suppression of the oxalate-promoted dissolution at pH 2.0 and high  
543  $(\text{NH}_4)_2\text{SO}_4$  concentrations. At pH 2, the proton-promoted dissolution was comparable to the proton + oxalate-promoted  
544 dissolution (Fig. [S9e10e](#)), with  $R_{\text{Fe(oxalate)}}$  close to zero (see Eq. 3). At pH 2.9, the proton + oxalate-promoted dissolution was  
545 higher than the proton + oxalate-promoted dissolution (Fig. [S9d10f](#)), with  $R_{\text{Fe(oxalate)}} > 0$  (Eq. 5).

546 Moreover, the new 3-step dissolution scheme better captured the initial fast dissolution of CFA (Figs. [2-310](#)) which was also  
547 observed in previous research (Borgatta et al., 2016; Chen et al., 2012; Chen and Grassian, 2013; Fu et al., 2012; Kim et al.,  
548 2020) (except for the certified CFA 2689 in Chen et al. (2012) which showed increasing dissolution rates over the duration of  
549 the experiment). Furthermore, the new scheme enabled us to account for the different Fe speciation determined in the CFA  
550 samples, which could be a key factor contributing to the different Fe dissolution behaviour observed in the present study and  
551 in literature (Borgatta et al., 2016; Chen et al., 2012; Chen and Grassian, 2013; Fu et al., 2012; Kim et al., 2020). In Figs. [S3-](#)  
552 [S57](#), the dissolution kinetics of Aberthaw and Shandong ash calculated using the dissolution rates in Table 1 and the **Fe-bearing**  
553 **Fe**-phases determined in the samples showed a good agreement with measurements.

## 554 5.2 Comparison with mineral dust

555 High ionic strength also impacted the dissolution rates of the **Saharan-Libyan dust precursor**-sample at low pH (Fig. [S40S4](#)).  
556 At around pH 2 conditions, the proton-promoted Fe dissolution of **Libyan dust Libya dust** was enhanced by ~40% after the  
557 addition of  $(\text{NH}_4)_2\text{SO}_4$ . At around pH 2 and with 0.01 M  $\text{H}_2\text{C}_2\text{O}_4$ , the Fe solubility of **Libyan dust Libya dust** decreased by  
558 ~30% in the presence of  $(\text{NH}_4)_2\text{SO}_4$ . Overall, the Fe solubility of **Libyan dust Libya dust** was lower compared to that observed  
559 in the CFA samples. After 168 hour-leaching at pH 2.1 with 1 M  $(\text{NH}_4)_2\text{SO}_4$ , the Fe solubility of **Libyan dust Libya dust** was  
560 7.2% (Fig. [S40S4](#)), which was from around 3 to 7 times lower compared to that of the CFA samples (Fig. 1). At around pH 2  
561 conditions in the presence of oxalate and high  $(\text{NH}_4)_2\text{SO}_4$  concentration, the Fe solubility of **Libyan dust Libya dust** rose to  
562 ~13.6% (Fig. [S40S4](#)), which is still 4 times lower than that of Krakow ash and around 1.5 lower than Aberthaw and Shandong  
563 ash (Fig. 2). The Fe solubilities of **the Libyan dust** observed in this study are comparable with those of the Tibesti dust ([Tibesti](#)  
564 [Mountains, Libya, 25.583333N/16.516667E](#)) in Ito and Shi (2016) at similar experimental conditions.

565 The enhanced Fe solubility in CFA compared to mineral dust could be primarily related to the different Fe speciation (Figs. 5  
566 [and S2](#)). CFA contained more highly reactive Fe and magnetite but less hematite and goethite than mineral dust.

567 Although mineral dust is the largest contribution to aerosol Fe while CFA accounts for only a few percent, atmospheric  
568 processing of CFA may result in a larger than expected contribution of **bio-accessible bioavailable**-Fe deposited to the surface  
569 ocean. It is thus important to quantify the amount and nature of CFA in atmospheric particles.

## 570 5.3 Comparison of modelled Fe solubility with field measurements

571 The model results obtained using **the emission inventory from Rathod et al. (2020) and** the new dissolution scheme for the  
572 proton + oxalate-promoted dissolution (Table 1) in Test 1 and Test 3 provided a better estimate of **dissolved Fe aerosol Fe**  
573 **solubility** over the Bay of Bengal than the other tests (Figs. [8-9](#); and [S7S3](#)). At the same time, the new model improved the  
574 agreement of aerosol Fe solubility from Test 0 ([7068% ± 45%](#)) to Test 1 ([4435% ± 32%](#)) and Test 3 ([4847% ± 1%](#)) with the  
575 field data ( $25\% \pm 3\%$ ) but still overestimated it after 22 January 2009, when open biomass burning sources become dominant  
576 ([Fig. 8](#)) ([Bikkina et al., 2020](#)) **as also shown in Fig. 8 and Table S4**. This could be due to the unrepresentative Fe speciation  
577 used in Test 1 and Test 3 for biomass burning over the Bay of Bengal. To reduce the uncertainty in model predictions, emission  
578 inventories could be improved through a comprehensive characterization of Fe species in combustion aerosol particles.

579 The revised model also enabled us to predict sensitivity to a more dynamic range of pH changes, particularly between  
580 anthropogenic combustion and biomass burning by the suppression of the oxalate-promoted dissolution at pH lower than 2. In  
581 Test 0, the dissolution rate was assumed to be independent from the pH for extremely acidic solutions (pH < 2). The results  
582 show that the proton-promoted dissolution scheme in Test 2 significantly overestimated aerosol dissolved FeFe solubility (Figs.  
583 8, 9 and S37), which indicates the suppression of the proton + oxalate-promoted dissolution at pH < 2. In Fig. 40S5, the model  
584 estimates of surface concentration of dissolved Fe aerosol Fe solubility over the Bay of Bengal considerably improved in Test  
585 1 (RMSE 11) compared to Test 0 (RMSE 21), but more work is needed to improve size-resolved Fe emission, transport, and  
586 deposition. The model results in Test 1 also indicate a larger contribution of pyrogenic dissolved Fe over regions with strong  
587 anthropogenic combustion sources to the atmospheric Fe loading, such over as East Asia (Fig. 11), but a smaller contribution  
588 of biomass burning sources downwind from tropical biomass burning regions (Fig. 412). We demonstrated that the  
589 implementation of the new Fe dissolution scheme, including a rapid Fe release at the initial stage and highly acidic conditions,  
590 enhanced the model estimates. However, in Test 1, we turned off the photo-reductive dissolution scheme (Ito, 2015), which  
591 was based on the laboratory measurements in Chen and Grassian (2013). To determine the photoinduced dissolution kinetics  
592 of CFA particles it is necessary to account for the effect of high concentration of (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> on photo-reductive dissolution  
593 rate which should be considered in future research.

#### 594 **Data availability statement**

595 The new dissolution schemes for the proton-promoted and oxalate-promoted dissolution are reported in Table 1. Table S1  
596 reports the concentrations of H<sub>2</sub>SO<sub>4</sub>, H<sub>2</sub>C<sub>2</sub>O<sub>4</sub> and (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> in the experiment solutions, the original and final pH from model  
597 estimates (including H<sup>+</sup> concentrations and activities), and the pH measurements for the solution with low ionic strength. Table  
598 S2-S3 contains the summary of the concentration and activity of total oxalate ions, C<sub>2</sub>O<sub>4</sub><sup>2-</sup>, and HC<sub>2</sub>O<sub>4</sub><sup>-</sup> in the experiment  
599 solutions calculated using the E-AIM model III. The observations of the surface-mass concentration of aerosol-total Fe,  
600 dissolved Fe and Fe solubility for the fine mode (PM<sub>2.5</sub>) over the Bay of Bengal are from Bikkina et al. (2020) and are available  
601 at <https://pubs.acs.org/doi/10.1021/acsearthspacechem.0c00063>. The -modelled mass concentrations of total Fe in aerosol  
602 particles and the aerosol Fe solubilities over the Bay of Bengal are reported in Table S4 and Table S5, respectively. The Fe  
603 speciation, the measurements of the Fe dissolution kinetics, and the results of the IMPACT model for each sensitivity  
604 simulation (Test 0-3) can be downloaded at: <https://doi.org/10.25500/edata.bham.00000702>.

#### 605 **Author contributions**

606 CB, ZS, and AI designed the experiments and discussed the results. ZS supervised the experimental and data analyses. CB  
607 conducted the experiments and the data analysis with contributions from ZS, AI, MDK and ND. ND, ZS and KI performed  
608 the XANES measurements. AI developed the model of the dissolution kinetics and performed the model simulations. Krakow  
609 and Aberthaw ash were provided by TJ, while Shandong ash was provided by WL. Soil 5 from Libya was collected by ND.  
610 CB prepared the article with contributions from MDK and all the other co-authors.

#### 611 **Competing interests**

612 The authors declare that they have no conflict of interest.



613 **Acknowledgments**

614 CB is funded by the Natural Environment Research Council (NERC) CENTA studentship (grant no. NE/L002493/1). Support  
615 for this research was provided to AI by JSPS KAKENHI (grant no. 20H04329), Integrated Research Program for Advancing  
616 Climate Models (TOUGOU) (grant no. JPMXD0717935715) from the Ministry of Education, Culture, Sports, Science and  
617 Technology (MEXT), Japan. We acknowledge Diamond Light Source for time on Beamline/Lab I18 under the Proposals:  
618 SP22244-1; SP12760-1; SP10327-1.

619 **Financial support**

620 This research has been supported by the Natural Environment Research Council [CENTA-DTP](#) (grant no. NE/L002493/1),  
621 JSPS KAKENHI (grant no. 20H04329), the Integrated Research Program for Advancing Climate Models (TOUGOU) (grant  
622 no. JPMXD0717935715).

623 **Table 1. Constants used to calculate Fe dissolution rates for fossil fuel combustion aerosols, based on laboratory experiments**  
 624 **conducted at high ionic strength.**

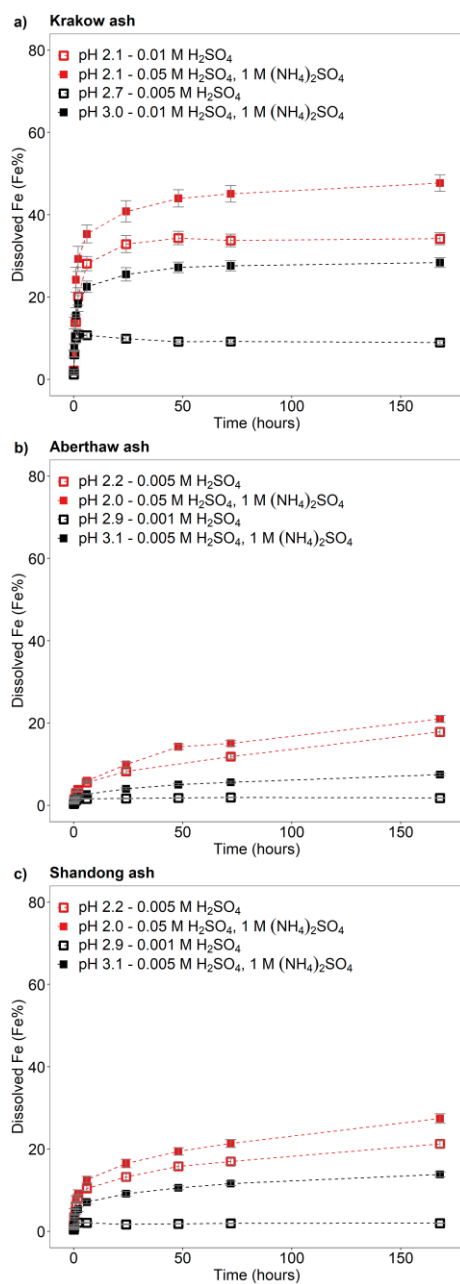
Stage	Kinetic	Scheme	Rate constant - $k(\text{pH}, T)^a$	$m^c$
I	Fast	Proton	$7.61 \times 10^{-6} \exp[E(\text{pH})^b \times (1/298 - 1/T)]$	0.241
II	Intermediate	Proton	$1.91 \times 10^{-7} \exp[E(\text{pH})^b \times (1/298 - 1/T)]$	0.195
III	Slow	Proton	$2.48 \times 10^{-7} \exp[E(\text{pH})^b \times (1/298 - 1/T)]$	0.843
I	Fast	Proton + Oxalate	$5.54 \times 10^{-6} \exp[E(\text{pH})^b \times (1/298 - 1/T)]$	0.209
II	Intermediate	Proton + Oxalate	$1.50 \times 10^{-7} \exp[E(\text{pH})^b \times (1/298 - 1/T)]$	0.091
III	Slow	Proton + Oxalate	$1.77 \times 10^{-8} \exp[E(\text{pH})^b \times (1/298 - 1/T)]$	0.204

625 <sup>a</sup>  $k(\text{pH}, T)$  is the pH and temperature dependent 'far-from-equilibrium' rate constant (moles Fe  $\text{g}^{-1} \text{s}^{-1}$ ). The Fe dissolution  
 626 scheme assumes 3 rate constants "fast", "intermediate" and "slow" for the proton- and oxalate-promoted dissolution. The  
 627 parameters were fitted to our measurements for Krakow ash.

628 <sup>b</sup>  $E(\text{pH}) = -1.56 \times 10^3 \times \text{pH} + 1.08 \times 10^4$ . The parameters were fitted to the measurements for soils (Bibi et al., 2014).

629 <sup>c</sup>  $m$  is the reaction order with respect to aqueous phase protons, which was determined by linear regression from our  
 630 experimental data in the pH range between 2 and 3 for proton- and oxalate-promoted dissolution schemes.

631

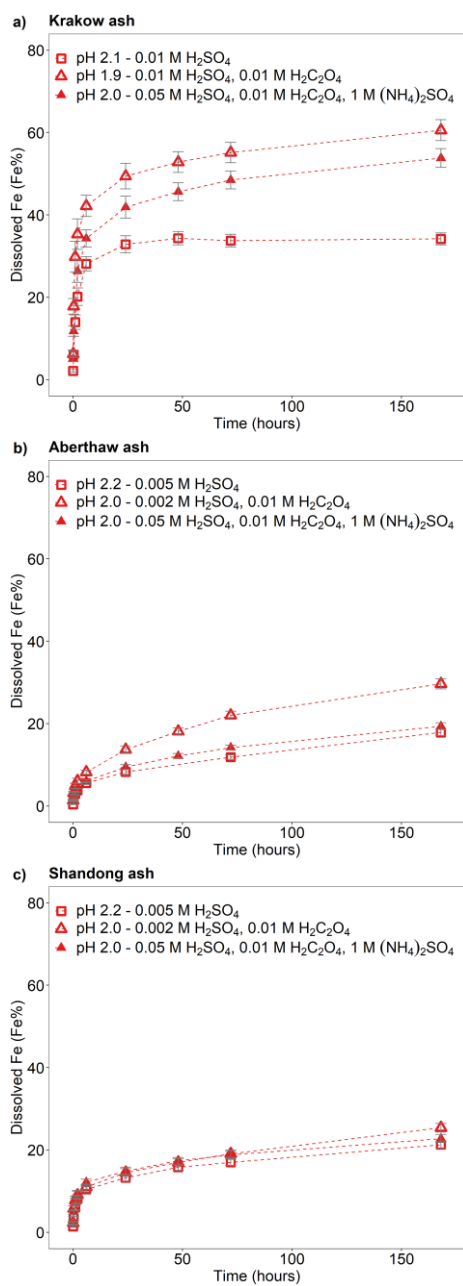


632

633 Figure 1: Fe dissolution kinetics of a) Krakow ash, b) Aberthaw ash and c) Shandong ash in H<sub>2</sub>SO<sub>4</sub> solutions (open rectangles) and  
 634 with 1 M (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> (filled rectangles). The molar concentrations of H<sub>2</sub>SO<sub>4</sub> and (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> in the experiment solutions are shown.  
 635 The final pH of the experiment solutions is also reported, which was calculated using the E-AIM model III for aqueous solution  
 636 (Wexler and Clegg, 2002) accounting for the buffer capacity of the CFA samples (Experiments 1-2 in Table S1). The experiments  
 637 conducted at around pH 2 are in red, while the experiments at around pH 3 are in black. The data uncertainty was estimated using  
 638 the error propagation formula.

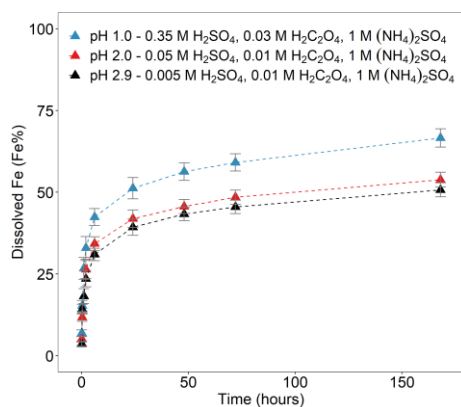
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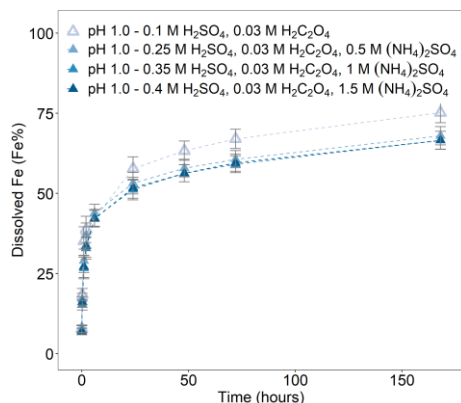
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640 **Figure 2:** Fe dissolution kinetics of a) Krakow ash, b) Aberthaw ash, and c) Shandong ash in H<sub>2</sub>SO<sub>4</sub> solutions at around pH 2 (red  
 641 open rectangles), with 0.01 M H<sub>2</sub>C<sub>2</sub>O<sub>4</sub> (red open triangles), and 1 M (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> (red filled triangles). The molar concentrations of  
 642 H<sub>2</sub>SO<sub>4</sub>, H<sub>2</sub>C<sub>2</sub>O<sub>4</sub> and (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> in the experiment solutions are shown. The final pH of the experiment solutions is also reported,  
 643 which was calculated using the E-AIM model III for aqueous solution (Wexler and Clegg, 2002) accounting for the buffer capacity  
 644 of the CFA samples (Experiments 1, 3-4 at around pH 2). The data uncertainty was estimated using the error propagation formula.



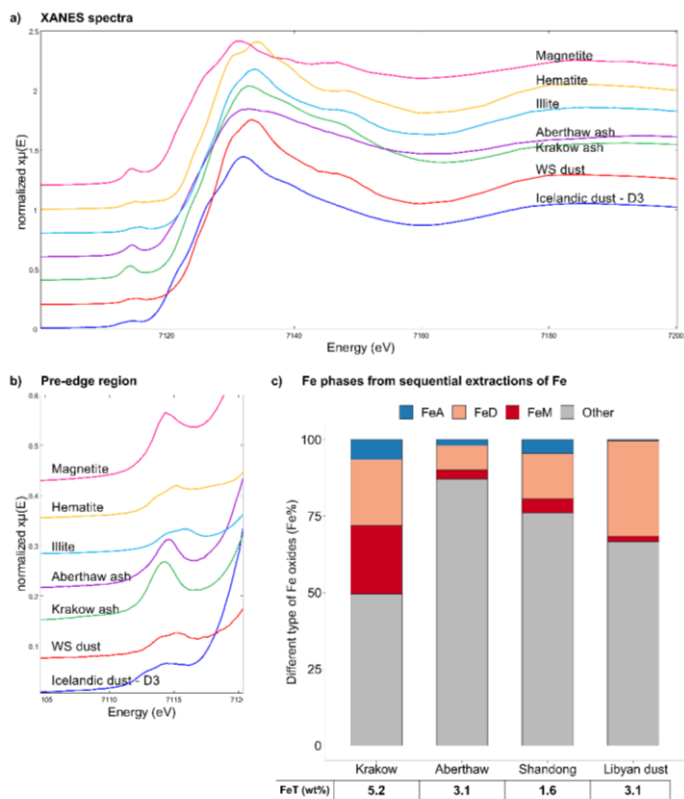
645

646 **Figure 3:** Fe dissolution kinetics of Krakow ash in  $\text{H}_2\text{SO}_4$  solutions at pH 1.0 with 0.03 M  $\text{H}_2\text{C}_2\text{O}_4$  and 1 M  $(\text{NH}_4)_2\text{SO}_4$  (blue filled  
 647 triangles), at pH 2.0 with 0.01 M  $\text{H}_2\text{C}_2\text{O}_4$  and 1 M  $(\text{NH}_4)_2\text{SO}_4$  (red filled triangles), and at pH 2.9 with 0.01 M  $\text{H}_2\text{C}_2\text{O}_4$  and 1 M  
 648  $(\text{NH}_4)_2\text{SO}_4$  (black filled triangles). The molar concentrations of  $\text{H}_2\text{SO}_4$ ,  $\text{H}_2\text{C}_2\text{O}_4$  and  $(\text{NH}_4)_2\text{SO}_4$  in the experiment solutions are shown.  
 649 The final pH of the experiment solutions is also reported, which was calculated using the E-AIM model III for aqueous solution  
 650 (Wexler and Clegg, 2002) accounting for the buffer capacity of the CFA samples (Experiment 7 at pH 1.0, Experiment 3 at pH 2.0,  
 651 and Experiment 3 at pH 2.9 in Table S1). The data uncertainty was estimated using the error propagation formula.



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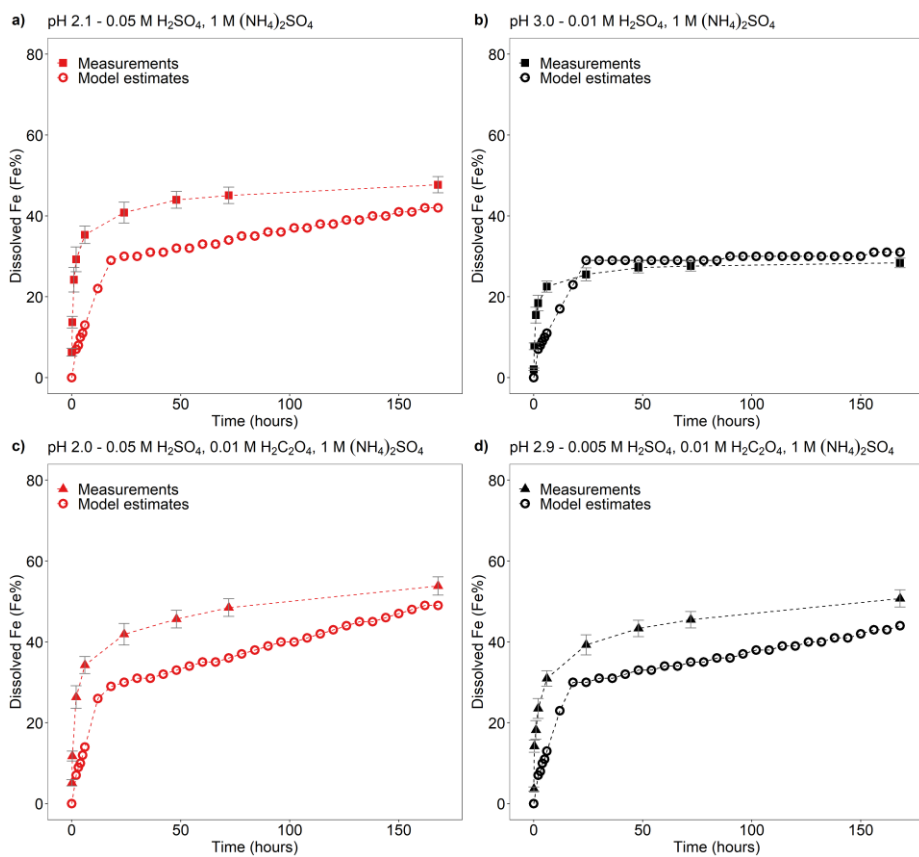
653 **Figure 4:** Fe dissolution kinetics of Krakow ash in  $\text{H}_2\text{SO}_4$  solutions at pH 1.0 with 0.03 M  $\text{H}_2\text{C}_2\text{O}_4$  and concentration of  $(\text{NH}_4)_2\text{SO}_4$   
 654 from 0 to 1.5 M. The molar concentrations of  $\text{H}_2\text{SO}_4$ ,  $\text{H}_2\text{C}_2\text{O}_4$  and  $(\text{NH}_4)_2\text{SO}_4$  in the experiment solutions are shown. The final pH of  
 655 the experiment solutions is also reported, which was calculated using the E-AIM model III for aqueous solution (Wexler and Clegg,  
 656 2002) accounting for the buffer capacity of the CFA samples (Experiments 5-8 in Table S1). The data uncertainty was estimated  
 657 using the error propagation formula.



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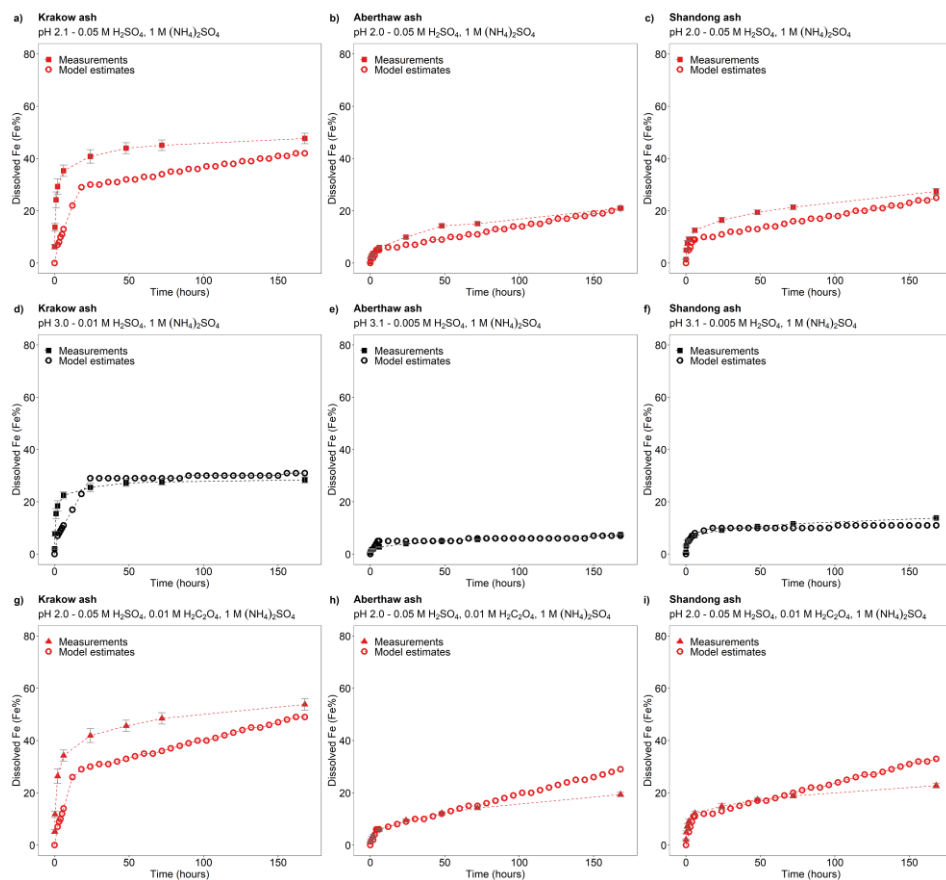
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659 **Figure 5: Fe speciation in CFA and mineral dust samples. a-b) Fe K-edge XANES spectra of Krakow ash, Aberthaw ash, magnetite,**  
 660 **hematite, and illite standards, mineral dust from the Dyngjúsundur dust hotspot in Iceland - D3 (Baldo et al., 2020), and mineral**  
 661 **dust from western Sahara - WS dust (Shi et al., 2011b). c) Percentages of ascorbate Fe (amorphous Fe, FeA), dithionite Fe**  
 662 **(FeDgoethite/hematite, FeD), magnetite Fe (FeM), and other Fe (including Fe in aluminosilicates) to the total Fe (FeT) in the coal-fly**  
 663 **ashCFA samples and mineral dust from Africa (Libya dust)Libyan dust precursor. The FeT (as %wt.) was is given below each**  
 664 **sample column. The data uncertainty was estimated using the error propagation formula: 4% for FeA/FeT, 11% for FeD/FeT, 12%**  
 665 **for FeM/FeT, and 2% for FeT.**



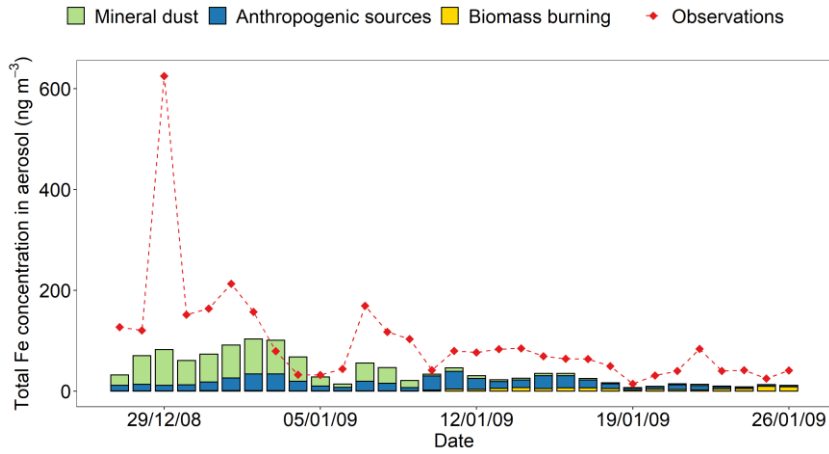
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667 **Figure 6: Comparison between the Fe dissolution kinetics of Krakow ash predicted using Eq. (1) and measured in H<sub>2</sub>SO<sub>4</sub> solutions**  
 668 **a-b) with 1 M (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>, c-d) with 0.01 M H<sub>2</sub>C<sub>2</sub>O<sub>4</sub> and 1 M (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>. The molar concentrations of H<sub>2</sub>SO<sub>4</sub>, H<sub>2</sub>C<sub>2</sub>O<sub>4</sub> and (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>**  
 669 **in the experiment solutions are shown. The final pH of the experiment solutions is also reported, which was calculated using the E-**  
 670 **AIM model III for aqueous solution (Wexler and Clegg, 2002) accounting for the buffer capacity of the CFA samples (Experiments**  
 671 **2-3 in Table S1). The experiments conducted at around pH 2 are in red, while the experiments at around pH 3 are in black. The data**  
 672 **uncertainty was estimated using the error propagation formula.**



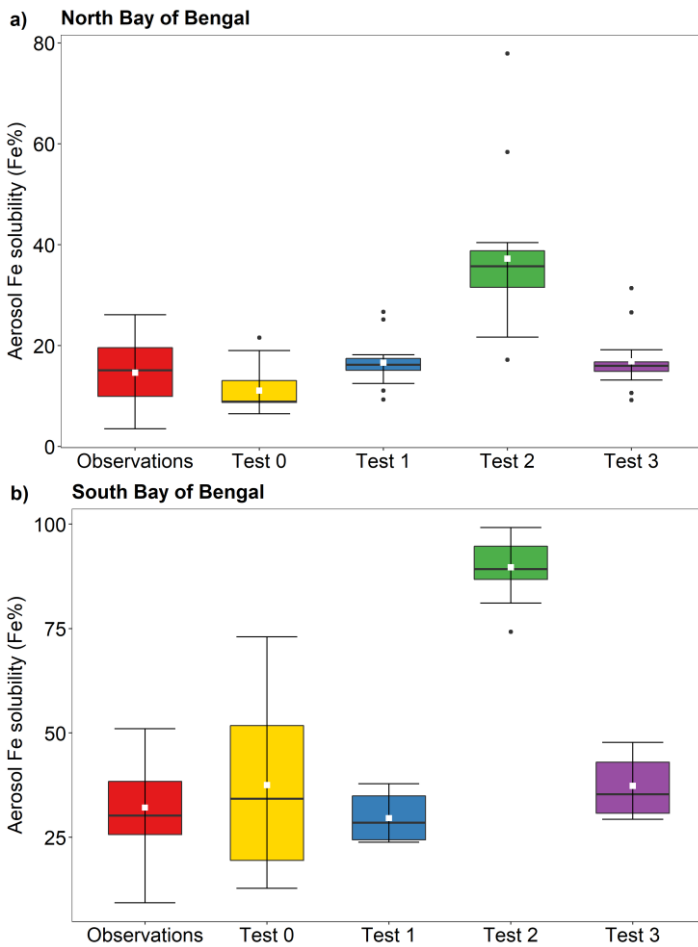
**Figure 7: Comparison between the Fe dissolution kinetics of Krakow, Aberthaw, and Shandong ashes predicted using Eq. (1) and measured in a-c) H<sub>2</sub>SO<sub>4</sub> solutions at around pH 2 with 1 M (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> (Experiments 2 at around pH 2 in Table S1), d-f) H<sub>2</sub>SO<sub>4</sub> solutions at around pH 3 with 1 M (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> (Experiments 2 at around pH 3 in Table S1), g-i) H<sub>2</sub>SO<sub>4</sub> solutions at pH 2.0 with 0.01 M H<sub>2</sub>C<sub>2</sub>O<sub>4</sub> and 1 M (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> (Experiments 3 at pH 2.0 in Table S1). The molar concentrations of H<sub>2</sub>SO<sub>4</sub>, H<sub>2</sub>C<sub>2</sub>O<sub>4</sub> and (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> in the experiment solutions are shown. The final pH of the experiment solutions is also reported, which was calculated using the E-AIM model III for aqueous solution (Wexler and Clegg, 2002) accounting for the buffer capacity of the CFA samples.**





683 **Figure 8: Surface-Mass concentration of total Fe in PM<sub>2.5</sub> aerosol particles over the Bay of Bengal from 27 December 2008 to 26**  
 684 **January 2009. Observations are from Bikkina et al. (2020) (red filled diamonds). Aerosol-Fe was calculated along the cruise tracks**  
 685 **using the IMPACT model. The concentrations of total Fe were calculated along the cruise tracks in the North Bay of Bengal (27**  
 686 **December 2008 - 10 January 2009) and the South Bay of Bengal (11-26 January 2009) using the IMPACT model. The total Fe**  
 687 **emissions from anthropogenic combustion sources (ANTHRO) and biomass burning (BB) were estimated using the emission**  
 688 **inventory of (Ito et al., 2018), whereas Fe emissions from mineral dust sources (DUST) were dynamically simulated (Ito et al., 2021a).**

689 The total Fe emission in anthropogenic aerosols was estimated using Fe emission factors by each sector such as energy, industry,  
 690 and iron and steel industry for the simulation years (Ito et al., 2018) in sensitivity Test 0 (yellow-filled circles), while the mineral  
 691 specific emission inventory for the year 2010 by Rathod et al. (2020) was used in the other tests. The contribution of mineral dust  
 692 sources, anthropogenic sources and biomass burning to total Fe is shown for Test 1-3.

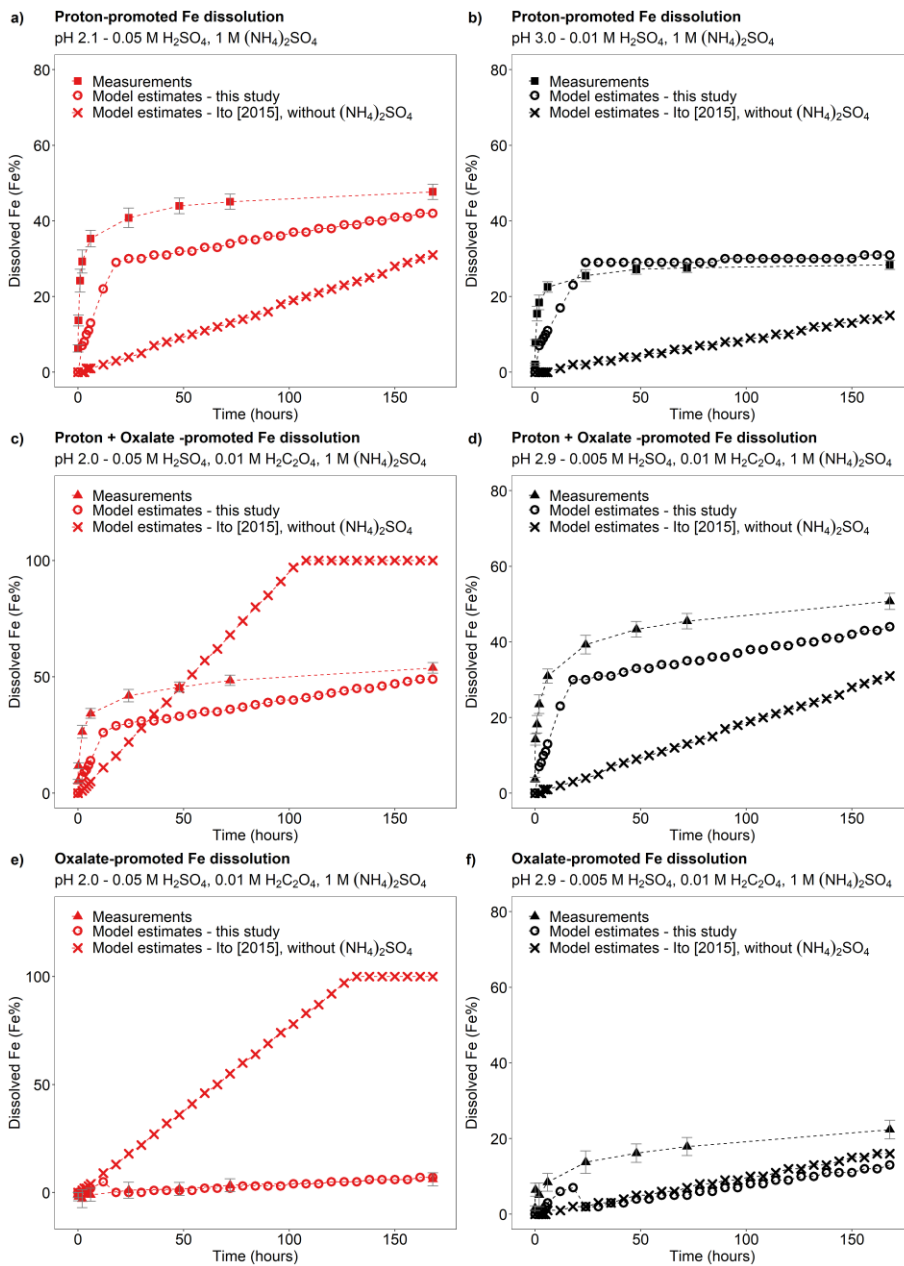


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693  
694 **Figure 9:** Fe solubility in PM<sub>2.5</sub> aerosol particles over a) the North Bay of Bengal, and b) the South Bay of Bengal from 27 December  
695 2008 to 26 January 2009. Observations are from Bikkina et al. (2020). Model estimates of Test 0, Test 1, Test 2, and Test 3 were  
696 calculated along the cruise tracks using the IMPACT model. In Test 0, we run the model without upgrades (Ito et al., 2021a) and  
697 applying the proton-promoted, oxalate-promoted, and photoinduced dissolution schemes for combustion aerosols in Table S6 (Ito,  
698 2015). The proton + oxalate dissolution scheme (Table 1) was applied in Test 1 and 3, while proton-promoted dissolution is used for  
699 Test 2. We adopted the base mineralogy for anthropogenic Fe emissions (Rathod et al., 2020) in Test 1 and 2. In Test 3, the Fe  
700 speciation of Krakow ash was used for all combustion sources. The small white square within the box shows the mean. The solid line  
701 within the box indicates the median. The lower and upper hinges correspond to the 25<sup>th</sup> and 75<sup>th</sup> percentiles. The whiskers above  
702 and below the box indicate the 1.5 × interquartile range, and the data outside this range are plotted individually. Surface  
703 concentration of dissolved Fe in PM<sub>2.5</sub> aerosol particles over the Bay of Bengal from 27 December 2008 to 26 January 2009.  
704 Observations are from Bikkina et al. (2020) (red filled diamonds). Aerosol dissolved Fe was calculated along the cruise tracks using  
705 the IMPACT model. In Test 0 (yellow filled circles), we ran the model without upgrades in the Fe dissolution scheme (Ito et al.,  
706 2021a), and applying the proton-promoted, oxalate-promoted and photoinduced dissolution schemes for combustion aerosols. The  
707 contribution of mineral dust sources, anthropogenic sources and biomass burning is shown for Test 1-3. The proton + oxalate  
708 dissolution scheme (Table 1) was applied in Test 1 and 3, while proton-promoted dissolution is used for Test 2. We adopted the  
709 mineral-specific inventory for anthropogenic Fe emissions (Rathod et al., 2020) in Test 1 and 2. In Test 3, the Fe speciation of Krakow  
710 ash was used for all combustion sources.

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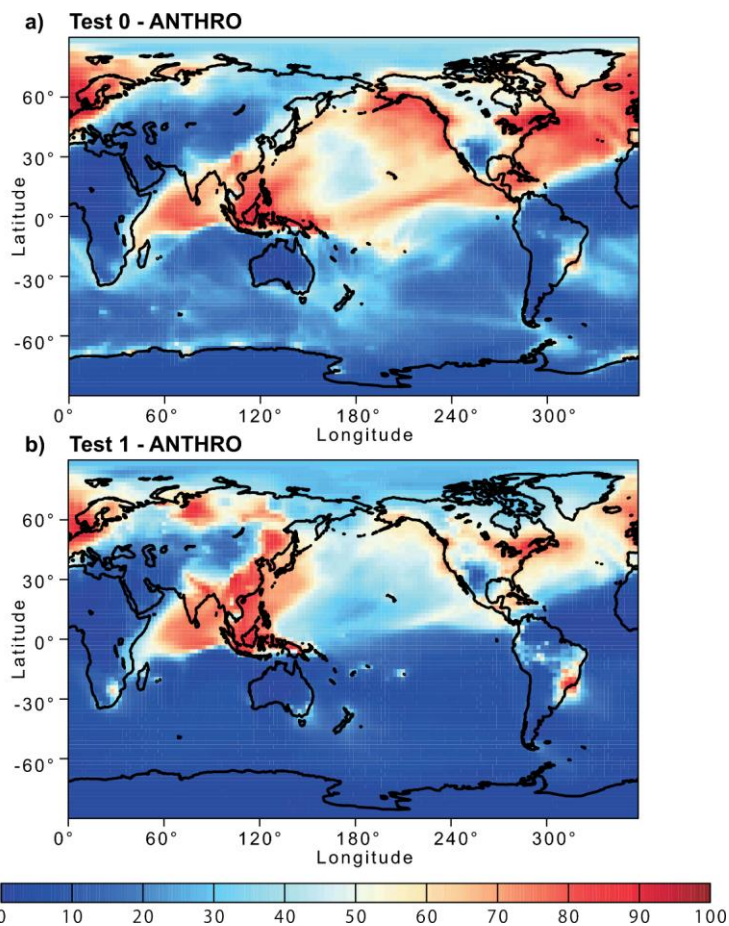


711

712 **Figure 10: Comparison-Comparison between the Fe dissolution kinetics of Krakow ash calculated using the original (Ito, 2015) and**  
 713 **the new dissolution scheme (Tables 1 and S6). a-b) Proton-promoted Fe dissolution in H<sub>2</sub>SO<sub>4</sub> solutions with 1 M (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> at pH**  
 714 **2.1 (a), and at pH 3.0 (b) (Experiment 2 at pH 2.1, and Experiment 2 at pH 3.0 in Table S1). c-d) Proton + oxalate promoted Fe**  
 715 **dissolution in H<sub>2</sub>SO<sub>4</sub> solutions with 0.01 M H<sub>2</sub>C<sub>2</sub>O<sub>4</sub> and 1 M (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> at pH 2.0 (c), and at pH 2.9 (d) (Experiment 3 at pH 2.0, and**  
 716 **Experiment 3 at pH 2.9 in Table S1). The Fe dissolution kinetics were predicted using the rate constants in Table 1 calculated in this**  
 717 **study (open circles) and the dissolution scheme for combustion aerosols in Ito (2015) (cross marks). Note that the dissolution scheme**  
 718 **in Ito (2015) was calculated based on laboratory measurements conducted at low ionic strength. e-f) Contribution of the oxalate-**

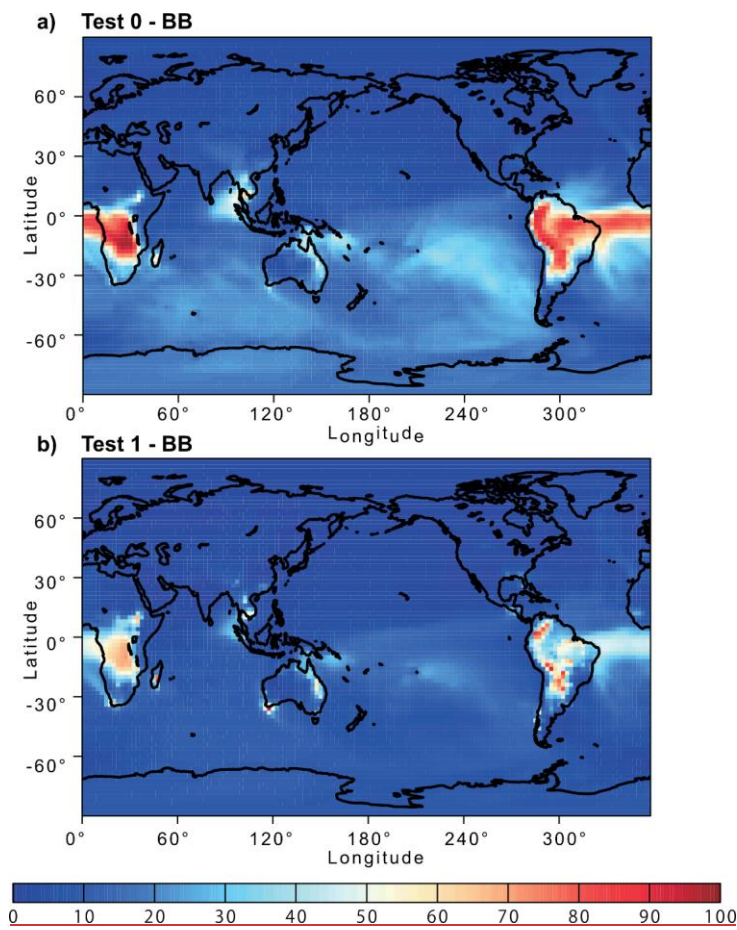
719 promoted dissolution to dissolved Fe estimated using Eq. (3). The molar concentrations of  $H_2SO_4$ ,  $H_2C_2O_4$  and  $(NH_4)_2SO_4$  in the  
720 experiment solutions are shown. The final pH of the experiment solutions is also reported, which was calculated using the E-AIM  
721 model III for aqueous solution (Wexler and Clegg, 2002) accounting for the buffer capacity of the CFA samples

722 between observations and model estimates of Fe solubility in  $PM_{2.5}$  aerosol particles over the Bay of Bengal from 27 December 2008  
723 to 26 January 2009. Observations are from Bikkina et al. (2020). Aerosol-Fe solubility was calculated along the cruise tracks using  
724 the IMPACT model. The Taylor diagram summarizes the statistics for the comparison between observations of aerosol Fe solubility  
725 and the different simulations (Test 0-3). The dashed curves in blue indicate the standard deviation values. The curves in red denote  
726 the root-mean-squared difference between the observational data and the model predictions. The dashed lines in black represent  
727 the correlation coefficients.



729 **Figure 1142:** Percentage contribution of anthropogenic combustion (ANTHRO) aerosol to the atmospheric dissolved Fe  
730 concentration Proportion (%) of pyrogenic dissolved Fe in aerosol dissolved Fe concentration near the ground surface from a) Test  
731 0 and b) Test 1 for December 2008 and January 2009. In Test 0, we ran the model without upgrades in the Fe dissolution scheme  
732 (Ito et al., 2021a) and applying the proton-promoted, oxalate-promoted and photoinduced dissolution schemes for combustion  
733 aerosols in Table S3-S6 (Ito, 2015). The proton + oxalate dissolution scheme (Table 1) was applied in Test 1 and we adopted the base  
734 mineralogy mineral-specific-inventory for anthropogenic Fe emissions (Rathod et al., 2020).

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738 **Figure 12: Percentage contribution of biomass burning (BB) aerosol to the atmospheric dissolved Fe concentration near the ground**  
739 **surface from a) Test 0 and b) Test 1 for December 2008 and January 2009. In Test 0, we ran the model without upgrades in the Fe**  
740 **dissolution scheme (Ito et al., 2021a) and applying the proton-promoted, oxalate-promoted and photoinduced dissolution schemes**  
741 **for combustion aerosols in Table S6 (Ito, 2015). The proton + oxalate dissolution scheme (Table 1) was applied in Test 1 and we**  
742 **adopted the base mineralogy for anthropogenic Fe emissions (Rathod et al., 2020).**

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