# Secondary Organic Aerosol Formation from Camphene Oxidation: Measurements and Modeling

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Abstract. While camphene is one of the dominant monoterpenes measured in biogenic and pyrogenic emissions samples, oxidation of camphene has not been well-studied in environmental chambers and very little is known about its potential to form secondary organic aerosol (SOA). The lack of chamber-derived SOA data for camphene may lead to significant uncertainties in predictions of SOA from oxidation of monoterpenes using existing parameterizations when camphene is a significant contributor to total monoterpenes. Therefore, to advance the understanding of camphene oxidation and SOA formation, and to improve representation of camphene in air quality models, a series of experiments were performed in the University of California Riverside environmental chamber to explore camphene SOA mass yields and properties across a range of chemical conditions at atmospherically relevant OH concentrations. The experimental results were compared with modeling simulations obtained using two chemically detailed box models, Statewide Air Pollution Research Center (SAPRC) and Generator for Explicit Chemistry and Kinetics of Organics in the Atmosphere (GECKO-A). SOA parameterizations were derived from the chamber data using both the two-product and volatility basis set (VBS) approaches. Experiments performed with added nitrogen oxides (NO<sub>x</sub>) resulted in higher SOA mass yields (up to 64%) than experiments performed without added NO<sub>x</sub> (up to 28%). In addition, camphene SOA mass yields increased with SOA mass  $(M_0)$  at lower mass loadings, but a threshold was reached at higher mass loadings in which the SOA mass yields no longer increased with  $M_0$  SAPRC modeling of the chamber studies suggested that the higher SOA mass yields at higher initial NO<sub>x</sub> levels were primarily due to higher production of peroxy radicals (RO<sub>2</sub>) and the generation of highly oxygenated organic molecules (HOMs) formed through unimolecular RO<sub>2</sub> reactions. SAPRC predicted that in the presence of NO<sub>x</sub>, camphene RO<sub>2</sub> reacts with NO and the resultant RO<sub>2</sub> undergo hydrogen (H)-shift isomerization reactions; as has been documented previously, such reactions rapidly add oxygen and lead to products with very low volatility (i.e., HOMs). The end products formed in the presence of NO<sub>x</sub> have significantly lower volatilities, and higher O:C ratios, than those formed by initial camphene  $RO_2$  reacting with hydroperoxyl radicals (HO<sub>2</sub>) or other  $RO_2$ . Further analysis reveals the existence of an extreme  $NO_x$ regime, where the SOA mass yield can be suppressed again due to high NO/HO<sub>2</sub> ratios. Moreover, particle densities were found to decrease from 1.47 to 1.30 g cm<sup>-3</sup> as [HC]<sub>0</sub>/[NO<sub>x</sub>]<sub>0</sub> increased and O:C decreased. The observed differences in SOA mass yields were largely explained by the gas-phase RO<sub>2</sub> chemistry and the competition between RO<sub>2</sub> + HO<sub>2</sub>, RO<sub>2</sub> + NO, RO<sub>2</sub> + RO<sub>2</sub>, and RO<sub>2</sub> autoxidation reactions.

# 1 Introduction

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On a global scale, biogenic monoterpene emissions are estimated to contribute 14% of the total reactive volatile organic compound (VOC) flux (Tg C) (Guenther, 1995). Camphene is an ubiquitous monoterpene emitted from biogenic sources (Geron et al., 2000; Hayward et al., 2001; Ludley et al., 2009; Maleknia et al., 2007; White et al., 2008) and pyrogenic sources (Akagi et al., 2013; Gilman et al., 2015; Hatch et al., 2015). Many studies have reported camphene as a top contributor by mass in measured biogenic and pyrogenic monoterpene emissions (Benelli et al., 2018; Hatch et al., 2019; Komenda, 2002; Mazza & Cottrell, 1999; Moukhtar et al., 2006). For example, in measurements of laboratory and prescribed fires reported by Hatch et al. (2019), camphene was among the top two monoterpenes emitted from subalpine and Douglas fir fires based on emission factors (mass of compound emitted/mass of fuel burned).

+ OH

$$k_{OH} = 5.3 \times 10^{-11}$$
 $H_{3}C$ 
 $CH_{3}$ 
 $CH_{2}$ 
 $+ NO_{3}$ 
 $k_{NO3} = 6.6 \times 10^{-13}$ 

Figure 1. Camphene chemical structure and reaction rate constants (unit: cm³ molecule-1 s-1) with major atmospheric oxidants.

When emitted to the atmosphere, monoterpenes form oxygenated compounds through reactions with oxidants such as hydroxyl radicals (OH), ozone (O<sub>3</sub>) and nitrate radicals (NO<sub>3</sub>); compounds with sufficiently low volatility can then condense to form secondary organic aerosol (SOA). Figure 1 shows the chemical structure of camphene and its reaction rate constants with major atmospheric oxidants. The SOA formation potential of individual monoterpenes can vary greatly based on their molecular structure, atmospheric lifetimes, and the volatility of their oxidation products (Atkinson and Arey, 2003; Griffin et al., 1999; Ng et al., 2007a; Zhang et al., 1992). Previous experimental studies of other monoterpenes (such as  $\alpha$ -pinene,  $\beta$ -pinene, d-limonene, etc.) have reported SOA mass yields from ~10% to 50% through OH oxidation and from ~ 0 to 65% through NO<sub>3</sub> oxidation; among the studied monoterpenes, d-limonene often has the highest reported yields (Mutzel et al., 2016; Griffin et al., 1999; Ng et al., 2007b; Fry et al., 2014). Few studies have been published regarding camphene SOA formation.

Past experimental studies of camphene largely have been focused on gas-phase reactivity with OH, NO<sub>3</sub>, and/or O<sub>3</sub> and gas-phase product identification (e.g., Atkinson et al., 1990; Gaona-Colmán et al., 2017; Hakola et al., 1994). Baruah et al. (2018) performed a kinetic and mechanism study of the camphene oxidation initiated by OH radicals using density functional theory (DFT), in which the rate constant and atmospheric lifetime were reported. It was also suggested that addition at the terminal double bond carbon atom could account for 98.4% of the initial OH-addition. A product study by Gaona-Colmán et al. (2017) showed obvious NO<sub>x</sub> dependence in OH + camphene experiments, in

which the molar yield of acetone was enhanced by a factor of 3, 33% relative to 10%, in the presence of  $NO_x$  (2–2.3 ppmv of NO).

Hatfield and Huff-Hartz studied SOA formation from ozonolysis of VOC mixtures, in which the added camphene was considered a non-reactive VOC and assumed to have little to no effect on SOA mass yields (Hatfield & Hartz, 2011). Mehra et al. (2020) recently published a compositional analysis study of camphene SOA. Although SOA mass yields were not provided, they demonstrated the potential contribution of highly oxygenated organic molecules (HOMs) and oligomers to camphene SOA formed in an oxidation flow reactor (OFR). Afreh et al. (2020) presented the first mechanistic modeling study of camphene SOA formation. While relatively high SOA mass yields were reported (with final SOA mass and yields twice that of  $\alpha$ -pinene), no chamber-based SOA data were available for measurement–model comparison at that time.

SOA formation has been shown to be highly dependent on gas-phase  $NO_x$  concentrations; and more precisely, the relative ratios of  $NO:HO_2$ , hydroperoxyl radicals: $RO_2$ , peroxy radicals (Henze et al., 2008;  $NO:HO_2$ , hydroperoxyl radicals: $NO:HO_2$ , peroxy radicals (Henze et al., 2008;  $NO:HO_2$ ,  $NO:HO_2$ ). During chamber experiments,  $NO:HO_2$  (Henze et al., 2005). During chamber experiments,  $NO:HO_2$  (Henze et al., 2001). During chamber experiments,  $NO:HO_2$  (Henze et al., 2001). During chamber experiments,  $NO:HO_2$  (Henze et al., 2001). No:Honz et al., 2006;  $NO:HO_2$  (Henze et al., 2001). No:Honz et al., 2006;  $NO:HO_2$  (Henze et al., 2006). No:Honz et al., 2006;  $NO:HO_2$  (Henze et al., 2006). No:Honz et al., 2008;  $NO:HO_2$  (Henze et al., 2006). The  $NO:HO_2$  (Henze et al., 2006). The  $NO:HO_2$  (Henze et al., 2006). The  $NO:HO_2$  (Henze et al., 2006). The NO:HO2 (Henze et al., 2006)

The atmospheric gas-phase autoxidation of RO<sub>2</sub> has been identified as another key pathway of SOA formation (Crounse et al., 2013; Jokinen 2014; Ehn et al., 2017; Bianchi et al., 2019). The RO<sub>2</sub> radical undergoes intramolecular H-atom abstraction reactions to form a hydroperoxide functionality and an alkyl radical (RO), to which a new RO<sub>2</sub> will be formed by adding O<sub>2</sub>. The autoxidation process can repeat several times until terminated by other pathways and will form low-volatility compounds known as highly oxygenated organic molecules (HOMs) (Bianchi et al., 2019). Recent theoretical and experimental studies have been conducted to understand HOM formation from monoterpenes such as α-pinene and β-pinene (Zhang et al., 2017; Quéléver et al., 2019; Xavier et al., 2019; Pullinen et al., 2020; Ye et al., 2020), but the potential importance and mechanisms of HOM formation from camphene have not been well investigated.

Here, we present the first systematic study of SOA formation from camphene using laboratory-based chamber experiments and chemically detailed box models. The experiments were conducted at varying NO<sub>x</sub> levels and the chamber data were used to provide SOA parameterizations based on the two-product (Odum et al., 1996) and volatility

basis set (VBS) modeling approaches (Donahue et al., 2006; Donahue et al., 2009). Two chemically detailed box models, Statewide Air Pollution Research Center (SAPRC) and Generator for Explicit Chemistry and Kinetics of Organics in the Atmosphere (GECKO-A), were used to provide mechanistic insights into the chamber observations and to elucidate the connections between the fate of RO<sub>2</sub>, HOM forming mechanisms, and camphene SOA formation.

## 2 Methods

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# 2.1 Chamber Facility and Instrumentation

The camphene photooxidation experiments were conducted in the University of California, Riverside (UCR) dual indoor environmental chamber. Chamber characterization and features have been previously described in detail (Carter et al., 2005). Briefly, the UCR environmental chamber consists of two 90 m³ collapsible Teflon reactors (2MIL (0.0508 mm) FEP film) kept at a positive pressure differential (3.73–4.98 Pa) to the enclosure where the reactors are located to minimize contamination during experiments. The enclosure is relative humidity controlled (<0.1%), temperature controlled ( $300 \pm 1$  K), and continuously flushed with dry purified air (dew point <-40 °C). Prior to and between experiments, reactors were collapsed to a volume <20 m³ for cleaning. The cycle of filling-purging the reactors was repeated until particle number concentrations were <5 cm $^{-3}$  and NO<sub>x</sub> mixing ratios were <1 ppb. The reactors were then flushed with dry purified air and filled up to 90 m³ overnight. The filling-purging of the reactors is controlled by an "elevator" program in LabView.

NO and NO<sub>2</sub> mixing ratios were monitored by a Thermo Environmental Instruments Model 42C chemiluminescence NO<sub>x</sub> analyzer. O<sub>3</sub> mixing ratios were monitored by a Dasibi Environmental Corp. Model 1003-AH O<sub>3</sub> analyzer. An Agilent 6890 gas chromatograph with flame ionization detector (GC-FID) was used to measure the camphene levels during the experiments.

Multiple instruments were used for particle-phase monitoring. Each reactor was equipped with a scanning mobility particle sizer (SMPS), including a TSI 3081 differential mobility analyzer (DMA), to measure the particle mass concentration. Particle effective density was directly measured by an Aerosol Particle Mass Analyzer (APM, Kanomax) with a SMPS built in house (Malloy et al., 2009). Chemical composition of SOA was measured using HR-ToF-AMS (DeCarlo et al., 2006) and analyzed to obtain O:C and H:C ratios by applying the method of Canagaratna et al. (2015). Data processing was performed using the ToF-AMS Analysis Toolkit 1.57 and PIKA 1.16 on Igor Pro 6.36. Based on aA prior characterization of this UCR chamber system (Li et al., 2016) reported an the experimental uncertainty in measured SOA yields of seconds.

Particle wall loss corrections were performed following the method described in Cocker et al. (2001). Vapor wall loss of organics has been reported in multiple chambers (e.g., Zhang et al., 2015, 2014; Schwantes et al., 2019); and has been modeled as a function of the mass and volatility of the condensing compounds, condensation sink, and characteristics of the chamber (e.g.,- La et al., 2016; Zhang et al., 2014; Ye et al., 2016). The extent to which these observations and modeling simulations are relevant in the UCR chamber is unclear, given the significant difference in chamber sizes. The UCR chamber is 4.5 times larger (90 m³) than the largest referenced chamber in these studies (20 m³) and most are ~10 m³. —In the UCR chamber, the role of vapor wall loss has been investigated in SOA

experiments using various precursor compounds (including α-pinene and m-xylene) under seed and no seed conditions (Clark et al., 2016; L. Li et al., 2015). There has been no evidence of non-negligible vapor wall loss in those experiments, including no measurable differences in SOA formation-in experiments with and without seed. have been observed in any of these experiments indicating negligible vapor wall losses. In this work, stability tests on camphene also resulted indemonstrated negligible vapor wall loss of the parent compound. Thus without evidence to suggest otherwise, the assumption of negligible vapor wall loss was maintained assumed for these experiments. It is noted that This assumption is further discussed where this assumption does not it may affect the major conclusions regarding the role of gas-phase chemistry on SOA formation. Particle effective density was directly measured by an Aerosel Particle Mass Analyzer (APM, Kanomax) with a SMPS built in house (Malloy et al., 2009). Chemical composition of SOA was measured using HR-ToF-AMS (DeCarlo et al., 2006) and analyzed to obtain O:C and H:C ratios by applying the method of Canagaratna et al. (2015). Data processing was performed using the ToF-AMS Analysis Toolkit 1.57 and PIKA 1.16 on Igor Pro 6.36. Based on a prior characterization of this UCR chamber system (Li et al., 2016), the experimental uncertainty in measured SOA yield is < 6.65%.

# 2.2 Experimental Conditions

A series of 13 camphene photooxidation experiments were carried out under varying levels of camphene and  $NO_x$  (Table 1). Due to the relatively high melting point of camphene (51 °C), camphene (Sigma-Aldrich, purity > 96 %, FG) was injected into a glass manifold (heated to 50 °C by heating tape) using a preheated (~50-55 °C) microliter syringe. As camphene evaporated it was carried to the reactors by dry purified compressed air flowing through a glass manifold at 8 LPM for 15 mins. Injection lines from the glass manifold to the reactors were also heated to reduce losses of camphene.  $H_2O_2$  (Sigma Aldrich, 50 wt.% in  $H_2O$ ) was injected by adding 200  $\mu$ l onto glass wool in glass tubing and then placing the tubing in a 56 °C oven with 10 LPM of dry purified compressed air flowing through the tubing for 15 mins and into the reactors. An inert tracer, perfluorohexane (Sigma-Aldrich, 99 %) or perfluorobutane (Sigma-Aldrich, 99 %), was injected to the reactors through the heated glass manifold by a carrier gas of 50 °C pure  $N_2$ . NO (Matheson, UHP) at known volume and pressure was transferred and injected through the same glass manifold as the inert tracer. When gaseous injection of camphene,  $H_2O_2$ , inert tracer, and NO (when used) was completed, the reactors were internally mixed using built-in blowers to ensure uniform distribution of chemicals, and then irradiated using UV black lights (115w Sylvania 350BL) to start photooxidation. No seed aerosol was used in this study. All experiments were conducted under dry conditions (relative humidity < 0.1 %) at 300 K. The initial conditions of the experiments are summarized in Table 1.

**Table 1**. Summary of initial conditions for chamber experiments and box model simulations.

	Expt.	Chamber E	Initial Conc xperiments a		Initial Conditions for GECKO-A Simulations				
		Camphene (ppb)	Added NO <sub>x</sub> (ppb)	*H <sub>2</sub> O <sub>2</sub> (ppb)	HC/NO <sub>x</sub> (ppb/ppb)	Camphene (ppb)	NO <sub>x</sub> (ppb)	H <sub>2</sub> O <sub>2</sub> (ppb)	HC/NO <sub>x</sub> (ppb/ppb)
without	WO1	7		854		10		1000	
$NO_x$	WO2	9		1148		10		1000	

	WO3	28		1212		25		1000	
	WO4	57		1182		50		1000	
	WO5	120		1212		100		1000	
	WO6	223		1576		150		1000	
	W1	7	89	854	0.08	10	80	1000	0.13
	W2	25	138	1040	0.18	25	80	1000	0.31
	W3	32	62	1136	0.51	25	80	1000	0.31
with NO <sub>x</sub>	W4	43	7	860	5.91	50	80	1000	0.63
INO <sub>X</sub>	W5	60	94	1227	0.64	50	80	1000	0.03
	W6	131	98	1167	1.33	100	80	1000	1.25
	W7	172	60	1121	2.88	150	80	1000	1.88

<sup>\*</sup> H<sub>2</sub>O<sub>2</sub> mixing ratio was targeted at 1ppm but corrected based on tracer (perfluorohexane or perfluorobutane) concentration to offset initial reactor volume bias. Corrected H<sub>2</sub>O<sub>2</sub> mixing ratios were used in SAPRC modeling.

# 2.3 Model Configurations and Conditions

The chamber experiments were modeled using two different box models, SAPRC and GECKO-A. The SAPRC model was chosen because it has been designed to evaluate gas-phase chemistry in the UCR chamber. The GECKO-A model was chosen because of the ability to predict both gas and particle phase composition, and the prior work of Afreh et al. (2020), in which GECKO-A was used to study SOA formation from camphene. The initial conditions of the simulations are summarized in Table 1.

# **2.3.1 SAPRC**

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A gas-phase oxidation mechanism was derived using the SAPRC mechanism generation system (MechGen) with modified initial rate constants (camphene with OH, NO<sub>3</sub> and O<sub>3</sub>) based on published literature data (Atkinson and Arey, 2003). MechGen, described elsewhere (Carter, 2021; Carter, 2020b; Jiang et al., 2020), is capable of generating fully explicit mechanisms for the atmospheric reactions of many types of organic compounds and the intermediate radicals they form. MechGen uses experimentally derived rate constants and branching ratios if data are available and otherwise uses estimated rate constants and branching ratios based on group additivity and other estimation methods. This system was used to derive reactions of explicit and lumped organic compounds and products in the development of the SAPRC-18 mechanism (Carter, 2020a) and a detailed SAPRC furans mechanism (Jiang et al., 2020).

The MechGen-derived camphene mechanism was implemented into the SAPRC box model to simulate chamber experiments under the same chemical conditions as the chamber experiments, where the initial hydrocarbon concentrations and NO<sub>x</sub> levels were as defined in Table 1. The SAPRC box model system has been used for chemical mechanism development, evaluation, and box modeling applications since the mid-1970s (Carter, 1990, 1994, 2000, 2010a, 2010b, 2020a). The initial conditions and relevant chemical parameters for environmental chamber experiments are required inputs; simulations can be performed using multiple versions of the SAPRC gas-phase chemical mechanism. In this work, the recently published version, SAPRC-18 (Carter, 2020a), was selected as the base mechanism because it represents the current state of the science and includes the most up-to-date model species and explicit representation of RO<sub>2</sub> chemistry.

# 2.3.2 **GECKO-A**

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GECKO-A is a nearly explicit mechanism generator and SOA box model. GECKO-A relies on experimental data and structure-activity relationships (SARs) to generate detailed oxidation reaction schemes for organic compounds. The generated reaction schemes are applied in the SOA box model to simulate SOA formation based on the absorptive gas/particle partitioning model of Pankow (1994), where thermodynamic equilibrium between the gas and an ideal particle phase is assumed. Detailed descriptions of GECKO-A, including mechanism generation and SOA formation, are provided by Aumont et al. (2005) and Camredon et al. (2007). GECKO-A has been used to predict SOA in a number of studies (e.g., Aumont et al., 2012; Lannuque et al., 2018; McVay et al., 2016), including camphene (Afreh et al., 2020). Details of the camphene mechanism and SOA box modeling were described in Afreh et al. (2020). Briefly, the camphene mechanism includes  $1.3 \times 10^6$  reactions and  $1.8 \times 10^5$  oxidation products; vapor pressures of products were calculated based on the Nannoolal method (Nannoolal et al., 2008).

The GECKO-A simulations were performed for a predefined set of conditions, prior to the chamber experiments, and thus in some cases differ from the experimental conditions. GECKO-A simulations were performed under two NO<sub>x</sub> conditions, with 80 ppb of NO<sub>x</sub> and without NO<sub>x</sub> (Table 1). For both NO<sub>x</sub> conditions, the initial hydrocarbon mixing ratios were set at 10, 25, 50, 100, and 150 ppb. All simulations were run under the following initial conditions: 1000 ppb of H<sub>2</sub>O<sub>2</sub>, 1 µg m<sup>-3</sup> of organic seed with molecular weight of 250 g mol<sup>-1</sup>, 298 K temperature, 1% relative humidity, and 50° solar zenith angle (required to compute the photolysis frequencies). Simulation results for camphene were compared with chamber data including SOA mass yields, precursor decay rates, and oxidant levels.

# 3. Experimental and Modeling Results

Table 2 summarizes the measured initial NO/NO<sub>2</sub> mixing ratios, initial camphene concentration ([HC]<sub>0</sub>), reacted camphene concentration ( $\Delta$ [HC]), SOA mass ( $M_o$ ) formed, particle density, final peak particle diameter ( $d_p$ ), photochemical aging time, irradiation time, and SOA mass yield (SOA mass formed,  $M_o$ /hydrocarbon reacted,  $\Delta$ HC) for all 13 experiments. Except for Fig. 4, in which SOA mass yields are shown as a function of photochemical age, all SOA mass yields refer to the mass at the end of the experiments ( $\sim$ 6 hours). Measured and predicted gas-phase species are presented in Sect. 3.1; SOA mass and yields are presented in Sect. 3.2. The predicted fate of RO<sub>2</sub> in the context of initial HC to initial NO<sub>x</sub> mixing ratio ([HC]<sub>0</sub>/[NO<sub>x</sub>]<sub>0</sub>) is presented in Sect. 3.3.

Table 2. Chamber SOA data, WO indicates experiments without added NO<sub>x</sub> and W with added NO<sub>x</sub>.

Expt.	Initial NO/NO <sub>2</sub>	[HC] <sub>0</sub>	Δ[ΗС]	$M_{ m o}$	PM den.	**Peak $d_{\rm p}$	Irradiation time	Photochemical aging time	SOA mass yield
	ppb	$\mu g m^{-3}$	$\mu g m^{-3}$	$\mu g m^{-3}$	g cm <sup>-3</sup>	nm	hour	hour	
WO1	0/0	41	41	6.1	1.42	126	4.9	16.1	0.15
WO2	0/0	49	49	3.7	1.42	125	5.0	16.7	0.08
WO3	0/0	155	153	42.0	*1.36	214	6.1	17.7	0.27
WO4	0/0	313	305	84.4	*1.34	270	6.7	15.8	0.28

WO5	0/0	663	597	158.6	1.30	286	6.7	9.5	0.27
WO6	0/0	1230	844	162.4	*1.31	492	6.1	5.0	0.19
W1	86/2	40	40	14.6	1.46	120	5.1	50.6	0.36
W2	114/24	140	140	46.1	1.47	188	5.2	40.6	0.33
W3	51/11	177	177	112.3	*1.44	185	6.0	42.0	0.64
W4	5/2	238	237	96.0	1.35	290	5.9	16.1	0.41
W5	45/49	334	334	199.5	*1.44	430	5.8	33.6	0.60
W6	42/56	724	724	428.8	*1.42	665	5.8	12.7	0.59
W7	45/15	956	950	494.3	*1.39	800	6.4	8.75	0.52

<sup>\*</sup> Estimated using best fit line shown in Fig. S6.

# 3.1 Gas-Phase Reactivity

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Figure 2 shows measured and predicted camphene consumption for the 13 photooxidation experiments, and the calculated time-dependent  $\beta$  values (ratio of RO<sub>2</sub> + NO to the sum of RO<sub>2</sub> + NO and RO<sub>2</sub> + HO<sub>2</sub>) (Henze et al., 2008; Pye et al., 2010) based on SAPRC predictions for each experimental condition. Additional comparisons of measured and predicted gas-phase species are shown in Fig. S1. Higher camphene decay rates and higher OH levels (0.15-0.88 ppt with added NO<sub>x</sub>; 0.05–0.29 ppt without added NO<sub>x</sub>) were observed and predicted for experiments with added NO<sub>x</sub> than without; likely due to the fast recycling of OH when NO<sub>x</sub> was present (Fig. 2). For all experiments, the  $\beta$  values changed as a function of time due to changing chemical conditions. Note that due to off-gassing of NO<sub>x</sub> from the Teflon reactor (Carter et al., 2005),  $\beta$  values simulated here were larger than 0 even for experiments without added  $NO_x$ . Experiments with added  $NO_x$  have  $\beta$  values from 0.12–1, while experiments without added  $NO_x$  have values < 0.12. For all parameters (camphene consumption, NO<sub>x</sub> decay, O<sub>3</sub> formation, and OH levels), the SAPRC simulation results were generally in good agreement with the experimental data. The exception to the generally good agreement was O<sub>3</sub> predictions in experiments without added NO<sub>x</sub>, which have a relatively strong dependence on the HONO offgassing rate. The quantity  $\Delta([O_3]-[NO])$  has been used to evaluate the rate of NO oxidation by  $RO_2$  for  $VOC-NO_x$ systems in SAPRC mechanism development (Carter and Lurmann, 1990; Carter, 1999; Carter, 2009; Carter, 2020). Figure S2 shows the comparison of the  $\Delta([O_3]-[NO])$  values between chamber measurements and SAPRC simulations for experiments with added NO<sub>x</sub>. The SAPRC box model captures the rates of RO<sub>2</sub>+NO well, and supports the use of the SAPRC model to interpret chamber observations especially in the presence of NO<sub>x</sub>. Unfortunately, it is hard to quantify how well constrained the other RO2 reaction rates and product yields are without corresponding measurements, which are not available. In this case, the SAPRC model was largely used to probe the mechanism (diagnostic) and not to predict yields (prognostic).

<sup>\*\*</sup> Peak  $d_p$  refers to the diameter of particles at the peak of the size distribution plot at the end of the experiment. The uncertainty of peak  $d_p$  values is less than 5%.

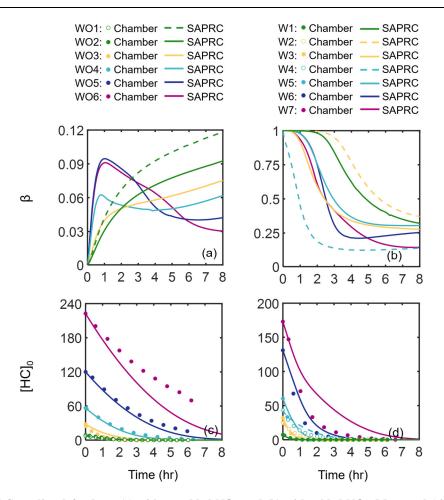


Figure 2. SAPRC predicted  $\beta$  values: (a) without added NO<sub>x</sub>, and (b) with added NO<sub>x</sub>. Measured (circles) and predicted (lines) camphene consumption as a function of irradiation time: (c) without added NO<sub>x</sub>, and (d) with added NO<sub>x</sub>. The hollow makers used in (c) and (d) are equivalent to dashed lines defined in the legends.

## 3.2 SOA Mass and Yield

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Measured SOA mass yields are shown in Fig. 3 as a function of SOA mass ( $M_0$ ) for experiments with (squares) and without (circles) added NO<sub>x</sub>. The SOA mass yields were much higher in experiments with added NO<sub>x</sub> (0.33–0.64) than experiments without added NO<sub>x</sub> (0.08–0.28). The SOA mass yields measured at the lowest [HC]<sub>0</sub>/Δ[HC] may be an underestimate due to the assumption of negligible vapor wall loss, which would have the largest effect at low  $\Delta$ [HC] (Krechmer et al., 2020). - The observed trends in SOA mass yields were unexpected based on prior chamber studies of SOA formation from monoterpenes, such as OH oxidation studies of α- and β-pinene, in which SOA mass yields were reported to be suppressed under high-NO<sub>x</sub> conditions (Eddingsaas et al., 2012; Pullinen et al., 2020; Sarrafzadeh et al., 2016).

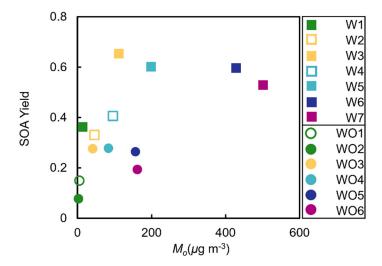


Figure 3. Measured camphene SOA mass yields as a function of SOA mass ( $M_0$ ). Squares indicate experiments with (W) and circles without (WO) added NO<sub>x</sub>. Initial HC mixing ratios are differentiated by color; open symbols are used to indicate replicate initial HC mixing ratios.

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Figure 3 shows another unexpected observation: the SOA mass yields decreased at high SOA mass under both NO<sub>x</sub> conditions, which was captured in the measurements and also in the GECKO-A model simulations (see Sect. 5). In the presence of NO<sub>x</sub>, the observed SOA mass yields increased with  $M_0$  for  $M_0 \le 112 \,\mu g \, m^{-3}$ , plateaued between 112  $\mu g \, m^{-3} < M_0 \le 429 \,\mu g \, m^{-3}$ , and then decreased for  $M_0 > 429 \,\mu g \, m^{-3}$ . Without NO<sub>x</sub>, the observed SOA mass yields increased for  $M_0 \le 42 \,\mu g \, m^{-3}$ , plateaued between 42  $\mu g \, m^{-3} < M_0 \le 159 \,\mu g \, m^{-3}$ , and then decreased for  $M_0 > 159 \,\mu g \, m^{-3}$ . The difference between the peak SOA mass yield and the SOA mass yield at the highest [HC]<sub>0</sub> was ~0.12 with added NO<sub>x</sub> and ~0.08 without added NO<sub>x</sub>. These unexpected trends in SOA mass yield While the SOA mass yields at the highest [HC]<sub>0</sub> may not be statistically different within the uncertainty of the measurements, sthis trend was also observed in the GECKO-A model simulations (see Sect. 5) and thus were further investigated, and largely reasonably explained, by the RO<sub>2</sub> fate based on box model simulations (see Sect. 4 & 5).

The varying [OH] levels in the chamber experiments led to a wide range of photochemical aging times, from hours to days. The irradiation time was converted to equivalent photochemical aging time in the ambient atmosphere using equation (1) (Aumont et al., 2012):

$$\tau = \frac{1}{[OH]_{atm}} \int_{0}^{t} [OH]_{sim} dt \tag{1}$$

where  $[OH]_{atm}$  was assumed to be  $2 \times 10^6$  molecule cm<sup>-3</sup>. Figure 4 shows the measured SOA mass yields as a function of photochemical aging time calculated using OH values predicted by SAPRC ( $[OH]_{sim}$ ). The SOA mass yields are dependent on OH levels and thus photochemical aging time. The yield curves for most experiments plateaued or nearly plateaued by the end of the experiment. Higher  $[HC]_0$  generally led to steeper increases in SOA mass yield as a function of aging time. Experiments with added  $NO_x$  generally had longer photochemical aging times than experiments without added  $NO_x$ ; without added  $NO_x$ , all experiments may not have fully plateaued and thus would have had higher SOA mass yields at longer irradiation times. even a However, even at the same aging time (Fig. S8),

the SOA yields were higher in the <u>experiments</u> with added NO<sub>x</sub> <u>experiments</u>. The higher SOA mass yields in experiments with added NO<sub>x</sub> may partially be attributed to the difference in [OH] levels and extents of aging. Similar NO<sub>x</sub> effects have been reported in many previous studies (e.g., Ng et al., 2007a; Sarrafzadeh et al., 2016). Sarrafzadeh et al. (2016) proposed that in a study of β-pinene the OH level was the main factor that accounted for differences in SOA mass yields under varying [NO<sub>x</sub>]<sub>0</sub>. In the camphene experiments presented herein, the aging effects were determined to be less important than RO<sub>2</sub> chemistry, since the SOA mass yield curves as a function of photochemical aging already plateau or nearly plateau by the end of experiments (Fig. 4) and the shapes of the growth curves (Fig. S9 and Fig. S10) indicate different kinetics and contributions from oxidation products that form slowly among and between experiments with and without added NO<sub>x</sub> -(Ng et al., 2006).

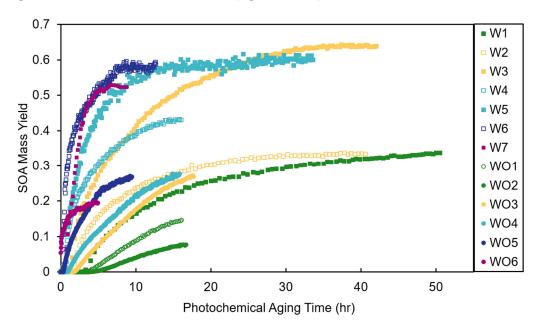
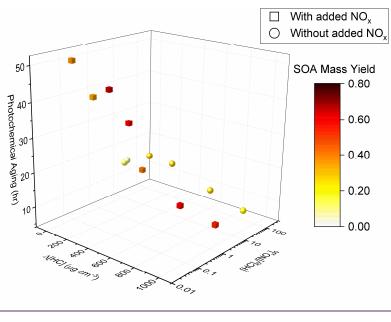


Figure 4. Measured SOA mass yields as a function of photochemical aging time in experiments with added  $NO_x$  (squares) and experiments without added  $NO_x$  (circles).

may double resulted in -a factor of two increase in the SOA mass yield). The chamber data presented here exhibit a general trend that indicate that the highest SOA mass yields from camphene,—were observed in a regime under the regular regime (distinguished from the extreme [NO<sub>x</sub>] regime), higher SOA mass yields are observed from camphene oxidation atof higher Δ[HC] and smaller moderate [HC]<sub>0</sub>/[NO<sub>x</sub>]<sub>0</sub>; this regime is distinguished from an extreme [NO<sub>x</sub>] regime, proposed in section 4.2, in which SOA mass yields are suppressed at the lowest [HC]<sub>0</sub>/[NO<sub>x</sub>]<sub>0</sub> (also shown in Fig. 5). These observations are different from those in This is different from studies of α-pinene, in which smaller lower [HC]<sub>0</sub>/[NO<sub>x</sub>]<sub>0</sub> generally led to lower SOA mass yield (Eddingsaas et al., 2012). The rends above observed trends are were further explored in the following sections, particularly the role of explained in the following sections with RO<sub>2</sub> fate based on SAPRC simulations.



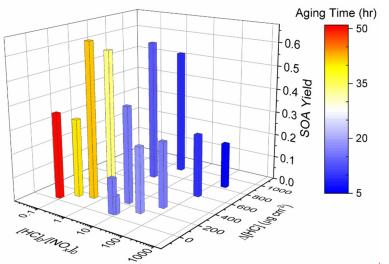


Figure 5. SOA mass yield (color bar) as a function of  $\Delta[HC]$ ,  $[HC]_0/[NO_x]_0$ , and photochemical aging time, with added  $NO_x$  experiments square markers and without added  $NO_x$  experiments round markers.

Figure 5. SOA mass yields dependence on [HC]<sub>0</sub>/[NO<sub>\*</sub>]<sub>0</sub>,  $\Delta$ [HC], and photochemical aging time.

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# 3.3 [HC]<sub>0</sub>/[NO<sub>x</sub>]<sub>0</sub> and the Fate of Peroxy Radicals

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Table S1 shows the experimental [HC]<sub>0</sub>/[NO<sub>x</sub>]<sub>0</sub> and the SAPRC predicted fate of total RO<sub>2</sub> (calculated as the summation of RO<sub>2</sub> radicals that undergo bimolecular reactions) for all the chamber runs. In Fig. 6, the fate of total RO<sub>2</sub> is shown as a function of [HC]<sub>0</sub>/[NO<sub>x</sub>]<sub>0</sub>. The majority of RO<sub>2</sub> was predicted to undergo bimolecular reactions with HO<sub>2</sub> or NO across the range of  $[HC]_0/[NO_x]_0$  values sampled. At  $[HC]_0/[NO_x]_0 < 6$ , > 50% of the RO<sub>2</sub> was predicted to react with NO; and at [HC]<sub>0</sub>/[NO<sub>x</sub>]<sub>0</sub> > 10, > 50% of the RO<sub>2</sub> was predicted to react with HO<sub>2</sub>. A roughly 50:50 branching of RO<sub>2</sub> between NO and HO<sub>2</sub> was reached when [HC]<sub>0</sub>/[NO<sub>x</sub>]<sub>0</sub> was 6:1, which is close to the ratio that was suggested in Presto et al. (2005). When [HC]<sub>0</sub>/[NO<sub>x</sub>]<sub>0</sub> increased over 50, the total fraction of bimolecular RO<sub>2</sub> + RO<sub>2</sub> increased from 0 to 30%. In addition, the normalized total RO<sub>2</sub> concentration (total [RO<sub>2</sub>]/[HC]<sub>0</sub>, ppbv/ppbv) increased as [HC]<sub>0</sub>/[NO<sub>x</sub>]<sub>0</sub> decreased (Fig. 7), suggesting more oxygenated RO<sub>2</sub>s were formed by NO pathway than others, which is consistent with the formation of HOMs with added NO<sub>x</sub>. There is a general trend of increasing SOA mass yield with decreasing [HC]<sub>0</sub>/[NO<sub>x</sub>]<sub>0</sub> (Fig. 5 and Fig. 7), with the exception of four outliers (W1, W2, WO1, and WO2) that have relatively low SOA mass yields. Experiments WO1, WO2, W1 had the lowest  $\Delta$ [HC] (49, 41, and 40  $\mu g/m^3$ , respectively, Table 2), indicating the SOA mass yields were influenced by  $\Delta[HC]$  as well as RO<sub>2</sub> chemistry. The connections between the fate of RO<sub>2</sub> and observed SOA mass yields are further discussed in Sect. 4. Though vapor wall loss has been found to be negligible in previous UCR chamber experiments, such experiments were typically conducted at higher [HC]<sub>0</sub>. Thus, it is acknowledged that vapor wall loss could affect the measured SOA yields, particularly for experiments W1-2 and WO1-2 with low  $[HC]_0$  (or  $M_0$ ). A vapor wall loss correction for those experiments would increase the measured SOA, but would not affect the following discussion or conclusions regarding the role of RO<sub>2</sub> chemistry.

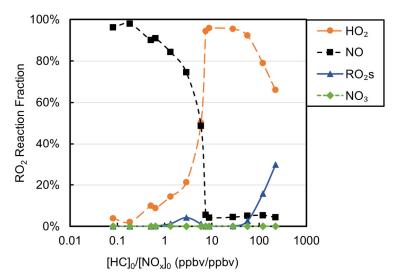


Figure 6. Fractions of total RO<sub>2</sub> reactions of each type as a function of [HC]<sub>0</sub>/[NO<sub>x</sub>]<sub>0</sub> based on Table S1.

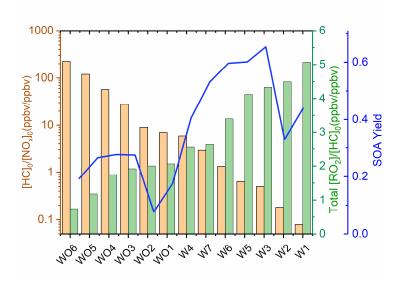


Figure 7. Relationship between total  $[RO_2]/[HC]_0$ ,  $[HC]_0/[NO_x]_0$ , and SOA mass yields.

By assuming the gas-phase chemistry and product distribution were similar when  $RO_2$  + NO accounted for more than 80% of the total  $RO_2$  consumption and when  $RO_2$  +  $HO_2$  accounted for more than 80% of the total  $RO_2$  consumption, experiments with (W1–3, 5–6) and without (WO1–4) added  $NO_x$  were grouped and used to derive SOA parameters using the two-product (Odum et al., 1996) and VBS approaches (Donahue et al., 2006; Donahue et al., 2009). The resultant parameters are shown in Table 3 (two-product) and Table 4 (VBS).

**Table 3.** Two-Product Model SOA parameters.

-	$\alpha_1$	$\log_{10} C^*_1$	$\alpha_2$	$\log_{10} C^*_2$
Without NO <sub>x</sub>	0.0017	1.08	0.3139	0.92
With NO <sub>x</sub>	0.4484	1.77	0.2398	-2.94

**Table 4.** VBS Model SOA parameters.

C*	$^{\dagger}lpha_{ m wo}$	$^{\dagger}lpha_{ m w}$
0.1	0.0001	0.2657
1	0.0152	0.0008
10	0.3069	0.0357
100	0.0001	0.4222
1000	0.0003	0.0000

<sup>†</sup> wo refers to without added NO<sub>x</sub>; w refers to with added NO<sub>x</sub>.

## 4 Discussion

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The reaction rate constant of camphene with  $O_3$  is relatively low compared to OH, and thus it is expected that OH is the dominant oxidant in the photooxidation of camphene under chamber conditions, especially with the high initial  $H_2O_2$  (~1 ppm) concentrations. This is supported by SAPRC simulation results (see Fig. S3 in SI), in which  $O_3$  accounts for 0–3% and  $NO_3$  for 0–16% of camphene oxidation, demonstrating the important role of OH oxidation in these studies.

# 4.1 Camphene + OH Gas-phase Mechanism

Figure 8 shows the MechGen predicted reactions and products of OH-initiated oxidation of camphene in the presence of  $NO_x$  through one major pathway, which had a yield of 0.83 (a more detailed reaction mechanism schematic is presented in Fig. S4). The reaction starts with OH addition to the  $CH_2$ =(C) position to form a ring-retaining alkyl radical, which further reacts with  $O_2$  to form the camphene peroxy radical,  $RO_2$ -a.  $RO_2$ -a can react with oxidants (NO,  $RO_3$ ,  $RO_2$ , and/or other  $RO_2$ ) to create an alkoxy radical, RO-a, with  $RO_3$  conversion; or form stable products such as organic nitrate (NO3CAMP1), hydroperoxide (HO2CAMP1), and alcohol (RO2CAMP1) compounds. The cyclic alkoxy radical RO-a can undergo prompt beta ( $\beta$ )-scission ring-opening reaction, and then  $RO_2$  addition to form another peroxy radical,  $RO_2$ -b. In the presence of  $RO_3$ , rapid  $RO_3$ -cission decomposition, or ring-opening reactions of the camphene alkoxy radicals ( $RO_3$ -b and  $RO_3$ -c) occur through the  $RO_3$ -through the  $RO_3$ -d with lower carbon number and higher O:C ratio (increases from 0.30 for  $RO_3$ -a to 0.71 for  $RO_3$ -d).

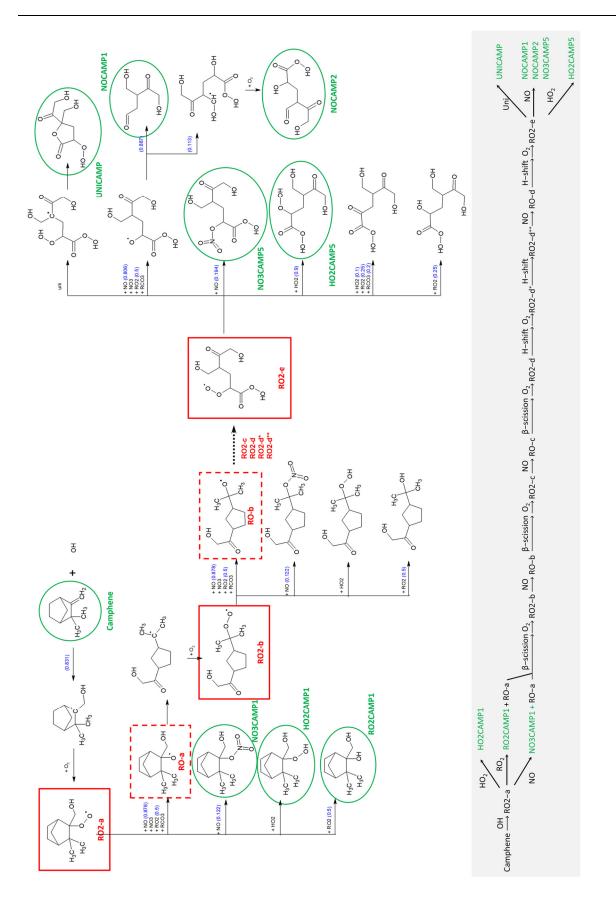


Figure 8. Schematic of the OH-initiated oxidation of camphene mechanism in SAPRC at 298 K and atmospheric pressure in the presence of NO<sub>x</sub>. Check Fig. S4 for more details.

MechGen predicted that RO<sub>2</sub>-d could undergo 1,5 H-shift isomerization nearly instantaneously, even in the presence of ~ 100 ppb NO<sub>x</sub>. Subsequent rapid addition of O<sub>2</sub> can form a new peroxy radical RO<sub>2</sub>-d\* which can undergo 1,7 H-shift isomerization and form the peroxy radical RO<sub>2</sub>-d\*\*. RO<sub>2</sub>-d\*\* can participate in termination reactions with NO and HO<sub>2</sub> to form organic nitrate (NO3CAMP4) and hydroperoxide (HO2CAMP4) products, which are known as highly oxygenated organic molecules (HOMs). In the presence of NO<sub>x</sub>, RO<sub>2</sub>-d\*\* can also react with NO to form the alkoxy radical RO-d that can undergo 1,4 H-shift isomerization and then O<sub>2</sub> addition to form the new peroxy radical RO<sub>2</sub>-e which will also lead to the formation of HOMs such as NO3CAMP5, HO2CAMP5, and UNICAMP. A recent SOA study by Mehra et al. (2020) demonstrated the formation of HOMs in camphene chamber experiments under both low NO<sub>x</sub> (30 ppb camphene, ~ 0 ppb NO<sub>x</sub>) and medium NO<sub>x</sub> (30 ppb camphene, 2.2 ppb NO, 58.4 ppb NO<sub>2</sub>) conditions. Based on their observations and analysis, the average molecular formula of the camphene SOA was C<sub>7.26</sub>H<sub>9.85</sub>O<sub>4.03</sub> for low NO<sub>x</sub> and C<sub>6.63</sub>H<sub>9.7</sub>N<sub>0.12</sub>O<sub>4.21</sub> for the medium NO<sub>x</sub> conditions, which also suggest the occurrence of ring-opening and decomposition reactions during camphene photooxidation, as predicted by MechGen.

#### 4.2 The Formation of HOMs and Influence on SOA Mass Yields

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**Table 5.** Log<sub>10</sub>  $C^*$  value for selected 1<sup>st</sup> generation of stable end products formed from camphene reactions with OH.

•		Atom		O:C $\log_{10} C^*$		Species	Atom				O:C	$\log_{10} C^*$	
	С	Н	О	N				С	Н	О	N		
HO2CAMP1	10	18	3	0	0.30	2.5	NO3CAMP1	10	17	4	1	0.40	3.5
HO2CAMP2	10	18	4	0	0.40	1.7	NO3CAMP2	10	17	5	1	0.50	2.6
HO2CAMP3	7	12	4	0	0.57	2.5	NO3CAMP3	7	11	5	1	0.71	3.5
HO2CAMP4	7	12	7	0	1.00	-1.3	NO3CAMP4	7	11	8	1	1.14	-0.1
HO2CAMP5	7	12	8	0	1.14	-4.3	NO3CAMP5	7	11	9	1	1.29	-2.8
RO2CAMP1	10	18	2	0	0.20	3.8	NOCAMP1	6	10	4	0	0.67	2.6
UNICAMP	7	10	7	0	1.00	-3.9	NOCAMP2	7	10	7	0	1.00	-1.1

**Table 6.** Fractions of peroxy radical RO<sub>2</sub>-a reactions of each type, calculated based on SAPRC simulations.

E4	[HC] <sub>0</sub>	*[HC] <sub>0</sub> /[NO <sub>x</sub> ] <sub>0</sub>	SOA Mass	Fraction of RO <sub>2</sub> -a Reaction						
Expt.	(ppb)	(ppbv/ppbv)	Yield	NO	HO <sub>2</sub>	RCO <sub>3</sub>	RO <sub>2</sub>	NO <sub>3</sub>		
WO1	7	7	0.15	0.03	0.97	0	0	0		
WO2	9	9	0.08	0.02	0.98	0	0	0		
WO3	28	28	0.27	0.02	0.97	0	0	0		
WO4	57	57	0.28	0.03	0.89	0	0.08	0		
WO5	120	120	0.27	0.03	0.64	0.02	0.30	0		
WO6	223	223	0.19	0.03	0.54	0.02	0.41	0		
W1	7	0.08	0.36	1.00	0	0	0	0		
W2	25	0.18	0.33	1.00	0	0	0	0		
W3	32	0.51	0.64	0.97	0.03	0	0	0		
W4	43	5.91	0.41	0.46	0.53	0.01	0	0		
W5	60	0.64	0.60	0.97	0.03	0	0	0		
W6	131	1.33	0.59	0.88	0.12	0.01	0.01	0		
W7	172	2.88	0.52	0.65	0.30	0.03	0.01	0		

<sup>\*</sup>The  $[HC]_0/[NO_x]_0$  for WO1–6 experiments were estimated assuming 1 ppb of NO<sub>x</sub>.

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Table 5 lists the log *C\** values and O:C ratios for the major camphene products predicted; vapor pressures of products were calculated based on the Nannoolal method (Nannoolal et al., 2008). HOMs have much lower volatilities than the earlier terminal products such as NO3CAMP1, HO2CAMP1, and RO2CAMP1. HOMs formed by autoxidation steps in camphene radical chain reactions are mediated by the H-shift isomerization of RO<sub>2</sub>-d and RO-d. Table 6 shows the SAPRC predicted fate of RO<sub>2</sub>-a for all chamber runs; the fate of summed RO<sub>2</sub> is shown in Table S1, which includes RO<sub>2</sub>-a~d and all the RO<sub>2</sub> radicals formed from other minor pathways. For the experiments without added NO<sub>x</sub> (WO1–6), once the initial peroxy radical RO<sub>2</sub>-a was formed, a large fraction of RO<sub>2</sub>-a (0.54-0.98) quickly reacted with HO<sub>2</sub> to form the terminal product HO2CAMP1, while only 2–3% of RO<sub>2</sub>-a reacted through the NO pathway and led to the generation of HOMs. For the experiments with added NO<sub>x</sub> (W1–7), much higher RO<sub>2</sub>-a + NO fractions (0.65–1.00) were predicted by SAPRC. The fates of summed RO<sub>2</sub> also suggested that not only RO<sub>2</sub>-a, but also the other RO<sub>2</sub> radical intermediates would tend to favor further reactions through the NO reaction chain to form lower volatility products.

Based on the predicted fate of RO<sub>2</sub> in SAPRC simulations, the higher SOA mass yields in experiments with NO<sub>x</sub> were due to the formation of HOMs through autoxidation in the presence of NO<sub>x</sub>. In general, faster RO<sub>2</sub> reaction with NO, HO<sub>2</sub> or other RO<sub>2</sub> limits HOM formation by autoxidation (Bianchi et al., 2019). In previous monoterpene SOA studies, HOM formation was often observed when NO<sub>x</sub> was absent or under lower NO<sub>x</sub> conditions (Pye et al., 2019; Schervish and Donahue, 2020; Zhao et al., 2018). For example, Zhao et al. (2018) demonstrated that autoxidation for some RO<sub>2</sub> is competitive with RO<sub>2</sub> + NO at ppb levels of NO for O<sub>3</sub>-initiated  $\alpha$ -pinene oxidation. They also reported that HOM formation decreased as the initial NO concentration increased from 0 ppb to 30 ppb. In the camphene experiments presented herein, the reverse trend was observed (see experiments WO4, W4 and W5 conducted with

 $\sim$ 50 ppb camphene at different NO<sub>x</sub> levels). This was due to the key RO<sub>2</sub> species, RO<sub>2</sub>-d, which was predicted to form only in the presence of NO<sub>x</sub> and had a fast enough autoxidation rate constant to effectively compete with bimolecular reactions.

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While the decreasing SOA mass yields at high [HC]<sub>0</sub> and M<sub>o</sub> in experiments with and without added NO<sub>x</sub> (shown in Fig. 3) may not be statistically different within the uncertainty of the measurements, RO<sub>2</sub> chemistry was explored as an explanation for the apparent trends. The decreasing SOA mass yields at high [HC]<sub>0</sub> and  $M_0$  in all experiments (shown in Fig. 3) can also be explained by RO<sub>2</sub> chemistry. For experiments with added NO<sub>x</sub>, a shift in the RO<sub>2</sub> reaction pathways from NO to HO<sub>2</sub> can explain the the decreasing SOA mass vield trend was most likely due to thyieldse shift of RO<sub>2</sub>-reaction pathways from NO to HO<sub>2</sub>. The fraction of RO<sub>2</sub>-a + NO decreased from 0.97 (W5) to 0.65 (W7) while the fraction of RO<sub>2</sub>-a + HO<sub>2</sub> increased from 0.03 (W5) to 0.3 (W7). For the experiments without NO<sub>x</sub>, the shift from  $RO_2 + HO_2$  to self- and cross-reactions of  $RO_2$  at high  $[HC]_0$  and  $M_0$  led to can explain the decreasing SOA mass yields. When [HC]<sub>0</sub> increased from 57 ppb to 223 ppb, the fractions of RO<sub>2</sub>-a + HO<sub>2</sub> decreased from 0.89 (WO4) to 0.54 (WO6) and the fraction of RO<sub>2</sub>-a + RO<sub>2</sub> increased by a factor of five, from 0.08 to 0.41. Moreover, this shift from bimolecular reactions with HO<sub>2</sub> to RO<sub>2</sub> as [HC]<sub>0</sub> increased also occurred in the context of the total RO<sub>2</sub> (Table S1). Generally, products that were predicted to form from one RO<sub>2</sub> reacting with another RO<sub>2</sub> in the absence of NO<sub>x</sub>, had relatively higher volatility than those formed from that RO<sub>2</sub> reacting with HO<sub>2</sub>; for example, RO2CAMP1 formed from RO<sub>2</sub>-a + RO<sub>2</sub> was more volatile than HO2CAMP1 formed from RO<sub>2</sub>-a + HO<sub>2</sub> (Table 5). The increasing fraction of self- and cross-reactions of RO<sub>2</sub> therefore is one likely explanation for the decreasing SOA mass yields at high  $\Delta$ HC and  $M_0$  in the experiments without NO<sub>x</sub>.

The relatively low SOA mass yields in experiments W1 and W2 (0.36 and 0.33) In experiments W1 and W2, also the relatively low SOA mass yields (0.36 and 0.33) can be partially attributed to explained due to differences in product distribution. An underestimation of the SOA mass yields in these experiments due to the assumption of negligible wall loss is not sufficient to explain these relatively low yields. , though an additional explanation that cannot be entirely ruled out for the low SOA yield observed in run W1 2 is the potential of vapor wall loss. A comparison of the product distributions between W1, W2, W3 and W5 suggested similar yields of NO3CAMP1-5 and NOCAMP1-2, but major differences in yields of UNICAMP and HO2CAMP1-5 (Fig. S5). Experiments W3 and W5 were selected for comparison because of their closest total RO<sub>2</sub> fractional reaction distribution (approximately 90% RO<sub>2</sub> + NO and 10% RO<sub>2</sub> + HO<sub>2</sub>) to W2 (98% RO<sub>2</sub> + NO and 2% RO<sub>2</sub> + HO<sub>2</sub>) and W1 (96% RO<sub>2</sub> + NO and 4% RO<sub>2</sub> + HO<sub>2</sub>) but higher SOA mass yield (0.64 and 0.6). W1 and W2 were predicted to have much smaller SOA mass yield than W3 and W5 in the low volatility products HO2CAMP1-5 (especially product HO2CAMP5, the lowest volatility among all listed products in Table 5,  $\log_{10}C^* = -4.3$ ) and UNICAMP (the second lowest volatility shown in Table 5,  $\log_{10}C^*$ = -3.9), which can contribute to the lower SOA mass yield. Further analysis of W1 and W2 revealed a likely cause for the different yields of HO2CAMP1-5 and UNICAMP. W1 and W2 were predicted to have delayed peaks of [OH] (after 3-4 hours of irradiation) which likely was due to the high NO<sub>x</sub> concentrations (Fig. S1b). Correspondingly, the [HO<sub>2</sub>] was highly suppressed during the first 2 hours of irradiation. Under high [NO<sub>x</sub>], the RO<sub>2</sub>-e + HO<sub>2</sub> pathway shown in Fig. 8 therefore could be suppressed, resulting in a lower yield of HO2CAMP5. This indicates a second "extreme NOx" regime may exist at high [NOx] and significantly lower [HC]0/[NOx]0.

# 5 GECKO-A simulations

## 5.1 SOA Mass and Yield

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The comparison of gas- and particle-phase species between chamber experiments and GECKO-A model simulations are shown in Fig. S1a and Fig. S1b. Without added NO<sub>x</sub>, GECKO-A predicts much smaller camphene consumption rates and no O<sub>3</sub> formation, while both the chamber data and SAPRC simulations suggest a final O<sub>3</sub> mixing ratio of ~10 ppb (Fig. S1a). This may be due to an underrepresentation of data and relevant pathways for low to no NO<sub>x</sub> conditions in the GECKO-A mechanism generation system, and the incomplete treatment of wall effects in the application of the GECKO-A box model. The without added NO<sub>x</sub> simulations therefore are not further discussed. With added NO<sub>x</sub>, GECKO-A shows good agreement with the experimental data and SAPRC simulations in the context of camphene consumption, O<sub>3</sub>, and OH levels.

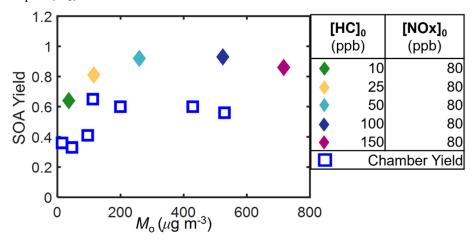


Figure 9. Predicted SOA mass yields based on GECKO-A model simulations.

Figure 9 shows the predicted SOA mass yields based on GECKO-A. For simulations with added NO<sub>x</sub>, while the model predicted higher SOA mass yields (0.64–0.93) than were observed (0.33–0.64), the trends in the SOA mass yields were consistent between chamber observation and simulations. The simulated SOA mass yield increased with SOA mass for SOA mass <  $260\mu g$  m<sup>-3</sup>, plateaued for SOA mass between 260 and 524  $\mu g$  m<sup>-3</sup>, and then decreased for SOA mass >  $524 \mu g$  m<sup>-3</sup>.

The predicted O:C ratio and average carbon number (Fig. 10), defined as the mole-weighted averaged carbon number for the main products (~95% by mass), were consistent with the plateauing/decreasing SOA yields at higher [HC]<sub>0</sub> (Fig. 9). The average carbon number was calculated using equation (2):

Average carbon number = 
$$\frac{\sum_{i} \frac{nC_{i} \times M_{0,i}}{MW_{i}}}{\sum_{i} \frac{M_{0,i}}{MW_{i}}}$$
(2)

where  $nC_i$ ,  $M_{o,i}$ , and MW<sub>i</sub> are the carbon number, mass, and molecular weight of species i, respectively. With added NO<sub>x</sub>, the average carbon number of both the gas and particle phases increased as [HC]<sub>0</sub> increased, while the O:C ratio decreased. These trends indicate there is a significant fraction of higher volatility compounds formed that contribute to SOA at higher [HC]<sub>0</sub> (or  $M_o$ ), resulting in lower SOA mass yields. In addition, only at the highest two [HC]<sub>0</sub> were

non-negligible fractions of precursor predicted to react with O<sub>3</sub> and NO<sub>3</sub> (Fig. S7), suggesting a larger fraction of higher-volatility nitrogen-containing products. More detailed comparisons of GECKO-A simulations with chamber experiments are presented by Afreh et al. (2020) for camphene and McVay et al. (2016) for α-pinene.

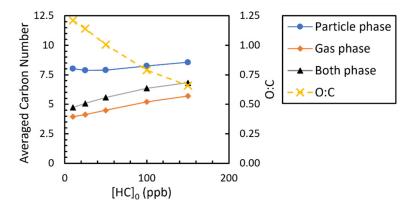


Figure 10. GECKO-A predicted particle O:C and mole-weighted averaged carbon number of products with added NO<sub>x</sub>.

# 5.2 Particle Density and O:C

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Figure 11a shows the GECKO-A predicted O:C ratio and measured O:C ratio as a function of  $[HC]_0/[NO_x]_0$  for all experiments. A good agreement in O:C ratios was observed between the model predictions and chamber data. The O:C ratio decreased from 1.21 to 0.39 as  $[HC]_0/[NO_x]_0$  increased from 0.13 to 223, supporting that more highly oxygenated products were formed at lower  $[HC]_0/[NO_x]_0$ .

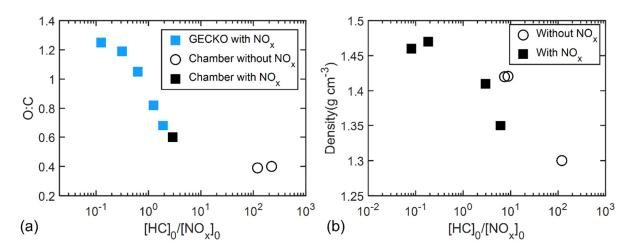


Figure 11. (a), O:C ratio as a function of  $[HC]_0/[NO_x]_0$  with AMS data and prediction by GECKO-A simulation. (b), Particle density (directly measured by APM–SMPS) shown as a function of  $[HC]_0/[NO_x]_0$ .

A negative correlation was also observed between measured particle density and  $[HC]_0/[NO_x]_0$ . The final density of particles decreased from 1.47 g cm<sup>-3</sup> to 1.30g cm<sup>-3</sup> as  $[HC]_0/[NO_x]_0$  increased from 0.08 to 120 (Fig.11b). The change in O:C ratio could account for the change in density. O:C and H:C have been used in semi-empirical SOA density parameterizations (Nakao et al., 2013; Kuwata et al., 2012), in which O:C plays a dominant role in determining organic particle density compared to H:C. Consistent with the semi-empirical formulations, the density of particles

formed from oxidation of camphene increased as O:C increased (from 0.39 to 1.21), while H:C varies over a smaller range (from 1.42 to 1.79). The change in density supports the proposed explanation that more oxygenated products were formed under lower [HC]<sub>0</sub>/[NO<sub>x</sub>]<sub>0</sub>. The wide range in final density and the correlation with [HC]<sub>0</sub>/[NO<sub>x</sub>]<sub>0</sub> shown here has not been previously reported. The SOA mass of each experiment in this study was calculated with its own density of SOA, instead of applying an averaged density. A list of particle densities used in this study can be found in Table 2.

# **6 Conclusions**

The first SOA mass yields from oxidation of camphene based on experiments performed in UCR environmental chamber with varying [NO<sub>x</sub>]<sub>0</sub> are presented herein. Higher SOA mass yields were measured with added NO<sub>x</sub> (0.33–0.64) than without added NO<sub>x</sub> (0.08–0.26) at atmospherically relevant OH concentrations. SOA formation from the oxidation of camphene showed different NO<sub>x</sub> dependence than what has previously been reported for other monoterpenes (e.g.,  $\alpha$ -pinene, d-limonene) and n-alkanes (carbon≤ 10), in which higher SOA mass yields were measured when [NO<sub>x</sub>] was lower (Nøjgaard et al., 2006; Ng et al., 2007b). For camphene oxidation, higher  $\Delta$ [HC] and lower [HC]<sub>0</sub>/[NO<sub>x</sub>]<sub>0</sub> (within 0.5–200) generally led to higher SOA mass yields. Similar NO<sub>x</sub> dependence has been observed for two sesquiterpenes (longifolene and aromadendrene) but was attributed to the production of nonvolatile organic nitrates with no detailed mechanistic analysis provided at that time (Ng et al., 2007b).

Although  $[HC]_0/[NO_x]_0$  shows clear correlation with SOA mass yield, this quantity cannot completely represent the underlying  $RO_2$  chemistry. The  $RO_2$  chemistry and the competition between varying bimolecular  $RO_2$  and unimolecular  $RO_2$  reaction pathways, explored using SAPRC MechGen, can be used to explain the dependence of SOA mass yields on HC and  $NO_x$ . The  $RO_2$  + NO pathway favored in experiments with added  $NO_x$  formed HOMs with much lower volatilities than products formed in other pathways. In addition to the regular  $NO_x$  regime introduced above  $([HC]_0/[NO_x]_0 > 0.5)$ , the results suggested an extreme  $NO_x$  regime where significantly high  $[NO_x]$  may suppress SOA mass yield. High  $NO_x$  levels concentration may suppress the  $NO_x$  regime where significantly products such as  $NO_x$  reactions the experiments, causing a subsequent reduction in the yields of low volatility products such as  $NO_x$  rich environments with extremely high ratios of  $NO_x$  to  $NO_x$  to  $NO_x$  has yield from oxidation of camphene might be significantly suppressed. As demonstrated here, simulations with chemically detailed box models such as SAPRC are useful for identifying SOA formation regimes.

Overall, SOA formation from oxidation of camphene may be larger in polluted environments (e.g., urban environments) than NO<sub>x</sub>-free environments. This reveals a possible underestimation of SOA formed from oxidation of camphene and potentially other VOCs that are assumed to have lower SOA mass yields at higher NO<sub>x</sub> levels. Further chamber and modeling studies of other understudied VOCs will be important for identifying other systems in which moderate NO<sub>x</sub> levels can promote HOM formation.

# **Data Availability**

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The experimental and modeling data is available upon request from the corresponding authors.

# **Supplement**

The supplement related to this article is available and can be download from ACP assigned link.

#### 530 Author Contributions

QL and JJ contributed equally to the study and share the first authorship. QL performed chamber experiments, data analysis and led the first draft of the manuscript. JJ derived and implemented the camphene mechanism in SAPRC, conducted SAPRC model simulations and led discussions on the chemistry of camphene SOA formation. IA carried out GECKO-A model simulations. QL and JJ interpreted the results and wrote the manuscript with IA. QL, JJ, KB and DC finalized the final manuscript. All the listed authors contributed to the revisions of the manuscript. The project was supervised by KB and DC.

## **Competing Interests**

The authors declare that they have no conflict of interest.

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