



# Evaluated kinetic and photochemical data for atmospheric chemistry: Volume VIII - gas phase reactions of organic species with four, or more, carbon atoms ( $\geq C_4$ )

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**Abstract.** This article, the eighth in the series, presents kinetic and photochemical datasheets evaluated by the IUPAC Task Group on Atmospheric Chemical Kinetic Data Evaluation. It covers the gas phase thermal and photochemical reactions of organic species with four, or more, carbon atoms ( $\geq$  C<sub>4</sub>) available on the IUPAC website in 2019, including thermal reactions of closed-shell organic species with HO and NO<sub>3</sub> radicals, and their photolysis. The article consists of a summary table, containing the recommended kinetic parameters for the evaluated reactions, and a supplement containing the datasheets, which provide information upon which the recommendations are made.

# 1 Introduction

In the mid-1970s it was appreciated that there was a need for the establishment of an international panel to produce a set of critically evaluated rate parameters for reactions of interest for atmospheric chemistry. To this end the CODATA Task Group on Chemical Kinetics, under the auspices of the International Council of Scientific Unions (ICSU), was constituted in 1977, and tasked to produce an evaluation of relevant, available kinetic and photochemical data. The first evaluation by this international committee was published in J. Phys. Chem. Ref. Data



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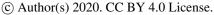
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in 1980 (Baulch et al., 1980), followed by Supplements in 1982 (Baulch et al., 1982) and 1984 (Baulch et al., 1984). In 1986 the IUPAC Subcommittee on Gas Kinetic Data Evaluation for Atmospheric Chemistry superseded the original CODATA Task Group for Atmospheric Chemistry. The Subcommittee continued its data evaluation program with Supplements published in 1989 (Atkinson et al., 1989), 1992 (Atkinson et al., 1992), 1997 (Atkinson et al., 1997a), 1997 (Atkinson et al., 1997b), 1999 (Atkinson et al., 1999), and 2000 (Atkinson et al., 2000).

The gas-phase evaluation work was expanded to include heterogeneous reactions of gases on solid and liquid substrates in 2005. Aqueous-phase reactions of atmospheric importance were added in 2015. The IUPAC group's work now includes over 1400 gas-phase, heterogeneous, and aqueous-phase reactions of importance in atmospheric chemistry. Reflecting the broader scope the group changed its name to the IUPAC Task Group on Atmospheric Chemical Kinetic Data Evaluation in 2013. Cox (2012) and Cox et al. (2018) discuss the history of IUPAC data evaluations and their role in addressing the critical societal challenges of stratospheric ozone loss, tropospheric ozone formation, acid rain, urban air pollution, aerosol formation, and climate change.

In 2000 the evaluation was made available on the worldwide web (since 2016, http://iupac.pole-ether.fr). The IUPAC website hosts an interactive data base with a search facility and hyperlinks between the summary table and the datasheets, both of which can be downloaded as individual Word and PDF files. Work is underway to convert the datasheets to machine readable xml files which will enable automatic transfer of IUPAC recommended data into atmospheric models. The IUPAC group continues to update and extend the set of evaluated reactions. To enhance the accessibility of this updated material to the scientific community, the evaluation is being published as a series of articles in Atmospheric Chemistry and Physics (Atkinson et al., 2004, 2006, 2007, 2008; Crowley et al., 2010; Ammann et al., 2013). We present here in Volume VIII new datasheets for gas-phase thermal and photochemical initiation reactions of organic species with four, or more, carbon atoms. The coverage of this volume includes evaluation of the thermal reactions of the organic species with HO and NO<sub>3</sub> radicals, and photolysis. The reactions with O<sub>3</sub> are included in a separate volume within this series (Cox et al., 2020), along with the chemistry of the Criegee intermediates produced.







# 2 Guide to the gas-phase datasheets

For each reaction covered in this volume, a datasheet with details about e.g. experimental methods and a justification of the choice of preferred value is available in the supplementary information. The datasheets covering gas-phase reactions are principally of two types: (i) those for individual thermal reactions and (ii) those for the individual photochemical reactions.

### 2.1 Thermal reactions

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The datasheets begin with a statement of the reactions including known / potential product channels when this information is available. The available kinetic data on the reactions are summarized under two headings: (i) Absolute Rate Coefficients, and (ii) Relative Rate Coefficients. Under both headings, we list the published experimental data as absolute rate coefficients. If the temperature coefficient has been measured, the results are given in a temperature dependent form over a stated temperature range. For bimolecular reactions, the temperature dependence is usually expressed in the normal Arrhenius form,  $k = A \exp(-B/T)$ , where B = E/R. For a few bimolecular reactions, we have listed temperature dependencies in alternative forms such as  $k = C(T/298 \text{ K})^n \exp(-D/T)$  or  $k = ET^2 \exp(-F/T)$  where the original authors have found that alternative expressions give a better fit to the data. In our recommendations we seek to provide simple Arrhenius expressions that describe the kinetics over the atmospherically relevant temperature range (200-300 K). More complex expressions which are often needed to describe the kinetic behaviour over larger ranges of temperature are given in the Comments on Preferred Values section in the datasheets. Rate coefficients are given here in units of cm<sup>3</sup> molecule<sup>-1</sup> s<sup>-1</sup>. Note that "molecule" is not a unit, but is included for clarity. For pressure dependent combination and dissociation reactions, the non-Arrhenius temperature dependence is used. This is discussed more fully in a subsequent section of this guide. Single temperature data are presented as such and wherever possible the rate coefficient at, or close to, 298 K is quoted directly as measured by the original authors. This means that the listed rate coefficient at 298 K may differ slightly from that calculated from the Arrhenius parameters determined by the same authors. Rate coefficients at 298 K marked with an asterisk indicate that the value was calculated by extrapolation of a measured temperature range which did not include 298 K. The tables of experimental data are supplemented by a series of comments summarizing the experimental details. The following abbreviations, relating to experimental techniques, are used in the Techniques and Comments sections:





A- absorption

AS – absorption spectroscopy

110 CCD – charge coupled detector

CIMS - chemical ionization mass spectroscopy/spectrometry

CL - chemiluminescence

CRDS – cavity ring-down spectroscopy

DF - discharge flow

115 EPR – electron paramagnetic resonance

F - flow system

FP - flash photolysis

FTIR - Fourier transform infrared

FTS – Fourier transform spectroscopy

120 GC – gas chromatography/gas chromatographic

HPLC – high-performance liquid chromatography

IR - infrared

LIF – laser induced fluorescence

LMR – laser magnetic resonance

125 LP – laser photolysis

MM – molecular modulation

 $MS-mass\ spectrometry/mass\ spectrometric$ 

P – steady state photolysis

PLP – pulsed laser photolysis

130 PR – pulse radiolysis

RA – resonance absorption

RF - resonance fluorescence

 $RR-relative\ rate$ 

S – static system

135 TDLS – tunable diode laser spectroscopy

UV – ultraviolet

UVA – ultraviolet absorption

VUVA - vacuum ultraviolet absorption

140 For measurements of relative rate coefficients, wherever possible the comments contain the





actual measured ratio of rate coefficients together with the rate coefficient of the reference reaction used to calculate the absolute rate coefficient listed in the data table. The absolute value of the rate coefficient given in the table may be different from that reported by the original author owing to a different choice of rate coefficient of the reference reaction. Whenever possible the reference rate coefficient data are those preferred in the present evaluation.

The preferred values in the datasheets are based on our consideration of the suitability of experimental method and coverage of applicable parameter space (temperature, total pressure of diluent gas, partial pressure of gas-phase species) within the atmospherically relevant range. The general approach and methods used have been reviewed recently by Cox (2012). It is recognized that preferred values may change with publication of new data, and such changes are updated at the website. The preferred rate coefficients are presented (i) at a temperature of 298 K and (ii) in temperature dependent form over a stated temperature range. This is followed by a statement of the uncertainty limits in  $\log k$  at 298 K and the uncertainty limits either in (E/R) or in n, for the mean temperature in the range. Some comments on the assignment of uncertainties are given later in this guide to the datasheets. The Comments on Preferred Values describe how the selection was made and give any other relevant information. The extent of the comments depends upon the present state of our knowledge of the particular reaction in question. The datasheets are concluded with a list of the relevant references.

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## 2.2 Conventions concerning rate coefficients

All of the reactions in the table are elementary processes. Thus the rate expression is derived from a statement of the reaction, e.g.

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$$A + A \rightarrow B + C$$

$$-\frac{1}{2}\frac{d[A]}{dt} = \frac{d[B]}{dt} = \frac{d[C]}{dt} = k[A]^2$$
 Eq. (1)

Note that the stoichiometric coefficient for A, i.e. 2, appears in the denominator before the rate of change of [A] (which is equal to  $2k[A]^2$ ) and as a power on the right-hand side. Representations of k as a function of temperature characterize simple "direct" bimolecular reactions. Sometimes it is found that k also depends on the pressure and the nature of the bath

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gas. This may be an indication of complex-formation during the course of the bimolecular reaction, which is always the case in combination reactions. In the following sections the representations of *k* which are adopted in these cases are explained.

### 2.3 Treatment of combination and dissociation reactions

180 Unlike simple bimolecular reactions such as those considered in Sect. 2.2, combination reactions

$$A + B + M \rightarrow AB + M$$

and the reverse dissociation reactions

$$AB + M \rightarrow A + B + M$$

are composed of sequences of different types of physical and chemical elementary processes.

Their rate coefficients reflect the more complicated sequential mechanism and depend on the temperature, *T*, and the nature and concentration of the third body, M. In this evaluation, the combination reactions are described by a formal second-order rate law:

$$\frac{d[AB]}{dt} = k[A][B]$$
 Eq. (2)

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while dissociation reactions are described by a formal first-order rate law:

$$\frac{-d[AB]}{dt} = k[AB]$$
 Eq. (3)

In both cases, *k* depends on the temperature and on the concentration of M, i.e., [M]. To rationalize the representations of the rate coefficients used in this evaluation, we first consider the Lindemann-Hinshelwood reaction scheme. The combination reactions follow an elementary mechanism of the form,

$$A + B \to AB^* \tag{1}$$

$$AB^* \to A + B \tag{-1}$$

$$AB^* + M \rightarrow AB + M \tag{2}$$





while the dissociation reactions are characterized by:

$$AB + M \rightarrow AB^* + M \tag{-2}$$

$$AB* + M \rightarrow AB + M \tag{2}$$

$$AB^* \to A + B \tag{-1}$$

Assuming quasi-stationary concentrations for the highly excited unstable species AB\* (i.e. that  $d[AB^*]/dt \approx 0$ ), it follows that the rate coefficient for the combination reaction is given by:

$$k = k_1 \left( \frac{k_2[M]}{k_{-1} + k_2[M]} \right)$$
 Eq. (4)

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while that for the dissociation reaction is given by:

$$k = k_{-2}[M] \left(\frac{k_{-1}}{k_{-1} + k_2[M]}\right)$$
 Eq. (5)

In these equations the expressions before the parentheses represent the rate coefficients of the process initiating the reaction, whereas the expressions within the parentheses denote the fraction of reaction events which, after initiation, complete the reaction to products. In the low pressure limit ([M] → 0) the rate coefficients are proportional to [M]; in the high pressure limit ([M] → ∞) they are independent of [M]. It is useful to express k in terms of the limiting low pressure and high pressure rate coefficients,

$$k_0 = \lim k([M])$$
 for  $[M] \to 0$  and  $k_\infty = \lim k([M])$  for  $[M] \to \infty$ 

230 From this convention, the Lindemann-Hinshelwood equation is obtained

$$k = \frac{k_0 k_\infty}{k_0 + k_\infty}$$
 Eq. (7)

It follows that, for combination reactions,  $k_0 = k_1 k_2 [M] / k_{-1}$  and  $k_{\infty} = k_1$ , while, for dissociation reactions,  $k_0 = k_{-2} [M]$  and  $k_{\infty} = k_{-1} k_{-2} / k_2$ . Since detailed balancing applies, the ratio of the rate coefficients for combination and dissociation at a fixed T and [M] is given by the equilibrium constant  $K_c = k_1 k_2 / k_{-1} k_{-2}$ .

Starting from the high-pressure limit, the rate coefficients fall off with decreasing third body

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concentration [M] and the corresponding representation of k as a function of [M] is termed the "falloff curve" of the reaction. In practice, the above Lindemann-Hinshelwood expressions do not suffice to characterize the falloff curves completely. Because of the multistep character of the collisional deactivation ( $k_2$ [M]) and activation ( $k_2$ [M]) processes, and energy- and angular momentum-dependences of the association ( $k_1$ ) and dissociation ( $k_1$ ) steps, as well as other phenomena, the falloff expressions have to be modified. This can be done by including a broadening factor F to the Lindemann-Hinshelwood expression (Troe, 1979):

$$k = \frac{k_0 k_\infty}{k_0 + k_\infty} F = k_0 \left(\frac{1}{1+x}\right) F = k_\infty \left(\frac{x}{1+x}\right) F$$
 Eq. (8)

The broadening factor F depends on the ratio  $x = k_0/k_\infty$ , which is proportional to [M], and can be used as a measure of "reduced pressure". The first factors on the right-hand side represent the Lindemann-Hinshelwood expression and the additional broadening factor F, at not too high temperatures, is approximately given by (Troe, 1979):

$$\log F \cong \frac{\log F_c}{1 + \lceil \log(k_0/k_{\infty})/N \rceil^2}$$
 Eq. (9)

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where  $\log = \log_{10}$  and  $N \approx [0.75-1.27 \log F_c]$ .

When  $F_c$  decreases, the falloff curve broadens and becomes asymmetric (i.e.  $F(k_0/k_\infty) \neq F(k_\infty/k_0)$ ). The given equation for F then becomes insufficient and should be replaced, e.g. by

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$$F(x) \approx (1+x)/(1+x^n)^{1/n}$$
 Eq. (10)

where  $x = k_0/k_\infty$ ,  $n = [\ln 2 / \ln(2/F_c)] [0.8+0.2 x^q]$ ,  $q = (F_c-1) / \ln(F_c/10)$  and  $\ln = \log_e$  (Troe and Ushakov, 2014). While the former equation for  $\log F$  appears acceptable as long as  $F_c \ge 0.6$ , the latter equation for F should be used for  $F_c \le 0.6$ . With these equations, falloff curves are represented in terms of the three parameters  $k_0$  (being proportional to [M]),  $k_\infty$ , and  $F_c$ .

The parameters  $k_0$ ,  $k_\infty$ , and  $F_c$  depend on details of the intra- and intermolecular dynamics and in principle can be calculated. If the required information is not available, one has to obtain them by fitting experimental falloff curves with the expressions given above. Nevertheless, one may estimate  $F_c$  to be typically of the order of 0.49, 0.44, 0.39, and 0.35, if the reactants A and



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B in total have r = 3, 4, 5, and 6 external rotational degrees of freedom, respectively (Cobos and Troe, 2003; for the reaction HO + NO<sub>2</sub> + M, e.g. one would have r = 5 and  $F_c \approx 0.39$ );  $F_c$ may be lower, if low frequency vibrations in A or B are relevant in addition to the rotations and if collisions are inefficient. Over the range 200 - 300 K often one can neglect a temperature dependence of  $F_c$  (for detailed calculations of  $F_c$ , including a dependence on the bath gas M, see e.g. Troe 1983; Troe and Ushakov, 2011, 2014). The accuracy of F(x) as given above is estimated to be about 10 percent. Larger differences between experimentally fitted  $F_c$  often are an indication for inadequate falloff extrapolations to  $k_0$  and/or  $k_{\infty}$ . In this case, the apparent values for  $k_0$ ,  $k_\infty$ , and  $F_c$  still can provide a satisfactory representation of the considered experimental data, in spite of the fact that  $k_0$  and/or  $k_\infty$  are not the real limiting values. If falloff curves are fitted in different ways, changes in  $F_c$  require changes in the limiting  $k_0$  and  $k_{\infty}$ . In the present evaluation, we generally follow the experimentally fitted values for  $k_0$ ,  $k_{\infty}$  and  $F_c$ , provided that F<sub>c</sub> does not differ too much from the standard values given above and theoretically modelled values. If large deviations are encountered, the experimental data are re-evaluated using  $F_c$  -values as given above. Values of  $k_\infty$  for combination reactions without a barrier often have only weak temperature dependences which in practice can be neglected.

Besides the energy-transfer mechanism, i.e., reactions (1), (-1), and (2), a second mechanism may become relevant for some reactions considered here. This is the radical-complex (or chaperon) mechanism

$$A + M \to AM \tag{3}$$

$$AM \to A + M \tag{-3}$$

$$B + AM \rightarrow AB + M \tag{4}$$

which, in the low pressure range, leads to  $k_0 = (k_3 / k_{-3})k_4$  [M]. For some tri- and tetra-atomic adducts AB, e.g., O + O<sub>2</sub>  $\rightarrow$  O<sub>3</sub> and HO + C<sub>6</sub>H<sub>6</sub>  $\rightarrow$  HOC<sub>6</sub>H<sub>6</sub>, the value of  $k_0$  may exceed that from the energy-transfer mechanism and show stronger temperature dependences (Luther et al., 2005; Teplukhin and Babikov, 2016). This mechanism may also influence high pressure experiments when  $k_0$  from the radical-complex mechanism exceeds  $k_\infty$  from the energy-transfer mechanism (Oum et al., 2003). In this case falloff over wide pressure ranges cannot be represented by contributions from the energy-transfer mechanism alone, in particular when measurements at pressures above about 10 bar are taken into consideration.

The dependence of  $k_0$  and  $k_\infty$  on the temperature T is represented in the form  $k \propto T^{-n}$  except for





cases with an established energy barrier in the potential. We have used this form of temperature dependence because it usually gives a better fit to the data over a wider range of temperature than does the Arrhenius expression. It should be emphasised that the chosen form of the temperature dependence is often only adequate over limited temperature ranges such as 200–300 K. Obviously, the relevant values of n are different for  $k_0$  and  $k_\infty$ . In this evaluation, values of  $k_0$  are given for selected examples of third bodies M, and if possible for  $M = N_2$ ,  $O_2$ , or air.

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# 2.4 Treatment of complex-forming bimolecular reactions

Bimolecular reactions may follow the "direct" pathway

$$A + B \rightarrow C + D$$

and/or involve complex-formation, in the simplest way characterized by the steps

$$A + B \to AB^* \tag{1}$$

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$$AB^* \rightarrow A + B$$
 (-1)

$$AB^* \to C + D \tag{5}$$

$$AB^* + M \rightarrow AB + M \tag{2}$$

(there may be additional pathways following from AB\*; direct and complex-forming pathways may or may not be coupled). Assuming quasi-stationary concentrations of AB\* (i.e. that  $d[AB^*]/dt \approx 0$  as in section 2.3), a Lindemann-Hinshelwood type analysis leads to

$$d[AB]/dt = k_{Ass}[A][B]$$
 Eq. (11)

$$d[C]/dt = d[D]/dt = k_{CA} [A] [B]$$
 Eq. (12)

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$$d[A]/dt = -(k_{Ass} + k_{CA})[A][B]$$
 Eq. (13)

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The rate constants for association ( $k_{Ass}$ ) and for chemical activation leading to product formation ( $k_{CA}$ ) then are given by

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$$k_{\text{Ass}} = k_1 k_2 [M] / (k_{-1} + k_2 [M] + k_5)$$
 Eq. (14)

$$k_{\text{CA}} = k_1 k_5 / (k_{-1} + k_2 [M] + k_5)$$
 Eq. (15)

Note that  $k_{\rm Ass}$  and  $k_{\rm CA}$  are dependent on the nature and concentration of the third body M, in addition to their temperature dependence. In reality, as for combination and dissociation reactions, the given expressions for  $k_{\rm Ass}$  and  $k_{\rm CA}$  have to be extended by suitable broadening factors F to account for the multistep character of processes (2) and the energy- and angular momentum-dependences of processes (1), (-1), and (5). These broadening factors, however, generally differ for  $k_{\rm Ass}$  and  $k_{\rm CA}$ ; also they generally differ from those of simple combination reactions described in section 2.3. One should note that association and chemical activation here are coupled such that their joint treatment is complicated. Some simplification is reached when the processes first are treated separately and the coupling is introduced at the end (Troe, 2015). The corresponding rate constants of the separated processes are denoted by  $k_{\rm Ass}$ \* and  $k_{\rm CA}$ \* and are given by

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$$k_{\text{Ass}}^* = k_1 k_2 [M] / (k_{-1} + k_2 [M])$$
 Eq. (16)

and

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$$k_{\text{CA}}* = k_1 k_5 / (k_2 [M] + k_5).$$
 Eq. (17)

 $k_{\rm Ass}$ \* then corresponds to the rate constant of a combination reaction described in section 2.3 and has a broadening factor  $F_{\rm Ass}$ \*(x\*).  $k_{\rm CA}$ \* has to be treated in a different way and is expressed in the form

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$$k_{\text{CA}}^* = k_{\text{Ass},\infty} \left[ \frac{1}{(1+x^*)} \right] F_{\text{CA}}^*(x^*)$$
 Eq. (18)

with  $x^* = k_{\text{Ass},\infty}$  [M] /  $k_{\text{CA},\infty}$ \* and a broadening factor  $F_{\text{CA}}$ \*(x) (Stewart et al., 1989). The latter factor is generally larger than  $F_{\text{Ass}}$ \*(x\*) (Troe, 2015). The rate parameters  $k_{\text{CA},0}$ \* and  $k_{\text{CA},\infty}$ \*





depend on the molecular parameters and can be calculated theoretically or fitted experimentally (after the coupling between association and chemical activation has been accounted for). In practice one may try to represent the rate constants in the form of rate constants of separated processes *k*<sub>Ass</sub>\* and *k*<sub>CA</sub>\*. Coupling these rate constants then leads to a full representation of the rate constants in terms of the six rate parameters *k*<sub>Ass,0</sub>, *k*<sub>Ass,∞</sub>, *F*<sub>Ass,c</sub>, *k*<sub>CA,0</sub>, *k*<sub>CA,∞</sub>, and *F*<sub>CA,c</sub>. If one neglects the coupling and fits these parameters directly from the experiments (Miller and Klippenstein, 2001), however, one has to be aware of the fact that the values obtained do not correspond to those of separated, single-channel, association and chemical activation processes (for more details, see Troe, 2015).

As a consequence of the multistep character of complex-forming bimolecular reactions, a variety of temperature - and pressure – dependences of  $k_{Ass}$  and  $k_{CA}$  are observed. The low pressure limit of the total rate constants  $k_{tot} = k_{Ass} + k_{CA}$ , i.e.,  $k_{tot,0} = k_{CA,0} = k_1k_5/(k_{-1} + k_5)$ , because of different energy – and angular momentum – dependences of the specific rate constants  $k_1$ ,  $k_{-1}$ , and  $k_5$ , may increase or decrease with temperature, the latter with the possibility to a change with an increase above a certain temperature.  $k_{tot}$ , as given above, may increase with pressure from  $k_{CA,0}$  to  $k_1$ , with  $M = H_2O$  often being a particularly efficient third body in the pressure – dependent range. The pressure dependence generally becomes less apparent with increasing temperature. Finally, the further fate of an addition product AB is of importance. It may be collisionally reactivated to energies where  $k_5 >> k_{-1}$ , such that formation of C + D is enhanced (in comparison to energies where  $k_5 << k_{-1}$ ). There is also the possibility that A-M (or B-M) complexes are formed which react in a chaperon mechanism with B (or A) and then form products.  $M = H_2O$  here again may be particularly efficient. Without detailed theoretical analysis, in general, it will be difficult to disentangle the intrinsic mechanism. Therefore, reference to theoretical work is given for selected reactions.

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### 2.5 Photochemical reactions

The datasheets begin with a list of feasible primary photochemical transitions for wavelengths usually down to 170 nm, along with the corresponding enthalpy changes at 0 K where possible or alternatively at 298 K. Calculated threshold wavelengths corresponding to these enthalpy changes are also listed, bearing in mind that the values calculated from the enthalpy changes at 298K are not true "threshold values". This is followed by tables which summarise the available experimental data for: (i) absorption cross sections and (ii) quantum yields. These data are



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supplemented by a series of comments. The next table lists the preferred absorption cross section data and the preferred quantum yields at appropriate wavelength intervals. For absorption cross sections the intervals are usually 1 nm, 5 nm or 10 nm. Any temperature dependence of the absorption cross sections is also given where possible. The aim in presenting these preferred data is to provide a basis for calculating atmospheric photolysis rates. For absorption continua the temperature dependence is often represented by Sulzer-Wieland type expressions (Astholz et al., 1981). Alternately a simple empirical expression of the form:  $\log_{10}(\sigma_{T1}/\sigma_{T2}) = B^*(T_1-T_2)$  is used. The comments again describe how the preferred data were selected and include other relevant points. The photochemical datasheets are concluded with a list of references.

### 2.6 Conventions concerning absorption cross sections

These are presented in the datasheets as "absorption cross sections per molecule, base e." They are defined according to the equation:

420 I / 
$$I_0 = \exp(-\sigma[N]l)$$
 Eq. (19)

where I<sub>0</sub> and I are the incident and transmitted light intensities, [N] is the number concentration of absorber (expressed in molecule cm<sup>-3</sup>), l is the path length (expressed in cm), and  $\sigma$  is the absorption cross section (units of cm<sup>2</sup> molecule<sup>-1</sup>). Note that "molecule" is not a unit but is included here for clarity. Other definitions and units are frequently quoted. The closely related quantities "absorption coefficient" and "extinction coefficient" are often used, but care must be taken to avoid confusion in their definition, see Calvert (1990) for definitions and discussion. It is always necessary to know the units of concentration and of path length and the type of logarithm (base e or base 10) corresponding to the definition. The decadic molar absorption coefficient,  $\varepsilon$ , is often quoted, particularly in the older literature, and is defined as:

$$\varepsilon = \{1/([A]I)\}\log_{10}(I_0/I),$$
 Eq. (20)

where [A] is the concentration of the absorber expressed in units of moles per liter. While  $\epsilon$  is often called an extinction coefficient, the term "extinction" should more properly be used for the sum of absorption and scattering. To convert from  $\epsilon$  (base 10, units of dm³ mol⁻¹ cm⁻¹) to  $\sigma$  (base  $\epsilon$ , units of cm² molecule⁻¹) multiply by  $3.82 \times 10^{-20}$ .



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# 2.7 Assignment of uncertainties

Under the heading "reliability," estimates have been made of the absolute accuracies of the preferred values of k at 298 K and of the preferred values of E/R over the quoted temperature range. The accuracy of the preferred rate coefficient at 298 K is quoted as the term  $\Delta \log k$ , where  $\Delta \log k = d$  and d is defined by the equation,  $\log k = c \pm d$ . This is equivalent to the statement that k is uncertain to a factor of f, where  $d = \log f$ . The accuracy of the preferred value of E/R is quoted as the term  $\Delta(E/R)$ , where  $\Delta(E/R) = g$  and g is defined by the equation E/R =  $h \pm g$ . d and g are uncertainties corresponding approximately to 95% confidence limits. For second-order rate coefficients listed in this evaluation, an estimate of the uncertainty at any given temperature within the recommended temperature range may be obtained from the equation:

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$$\Delta \log k(T) = \Delta \log k(298 \text{ K}) + 0.4343 \{\Delta E/R(1/T - 1/298 \text{ K})\}\$$
 Eq. (21)

The assignment of these absolute uncertainties in k and E/R is our subjective assessment. They are not determined by a rigorous, statistical analysis of the database, which is generally too limited to permit such an analysis. Rather, the uncertainties are based on our knowledge of the techniques, the difficulties of the experimental measurements, the potential for systematic errors, and the number of studies conducted and their agreement or lack thereof. Experience shows that for rate measurements of atomic and free radical reactions in the gas phase, the precision of the measurement, i.e. the reproducibility, is usually good. Thus, for single studies of a particular reaction involving one technique, standard deviations, or even 95% confidence limits, of  $\pm 10\%$  or less are frequently reported in the literature. Unfortunately, when we compare data for the same reaction studied by more than one group of investigators and involving different techniques, the rate coefficients sometimes differ by a factor of 2 or even more. This can only mean that one or more of the studies has involved large systematic uncertainty which is difficult to detect. This is hardly surprising since, unlike molecular reactions, it is not always possible to study atomic and free radical reactions in isolation, and consequently mechanistic and other difficulties frequently arise. On the whole, our assessment of uncertainty limits tends towards the cautious side. Thus, in the case where a rate coefficient has been measured by a single investigation using one particular technique and is unconfirmed by independent work, we typically suggest an uncertainty of a factor of 2.

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In contrast to the usual situation for the rate coefficients of thermal reactions, where intercomparison of results of a number of independent studies permits a realistic assessment of reliability, for many photochemical processes there is a scarcity of reliable data. Thus, we do

not feel justified at present in assigning uncertainty limits to the parameters reported for the

photochemical reactions.

**Author contribution**: All authors defined the scope of the work. AM, TJW, JNC, MEJ and RAC developed and drafted the data sheets and manuscript. All authors reviewed, refined, and revised the manuscript and data sheets.

480 **Competing interests:** The authors declare that they have no conflict of interest.

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Reaction	Reaction     Reaction       number     Molecule' s'	$k_{298}$ cm <sup>3</sup> molecule <sup>-1</sup> s <sup>-1</sup>	$\Delta \log k^{a}_{298}$	Temp. dependence of k/cm³molecule-1 s-1	Temp.	$\Delta(E/R)/K^a$
HO reactions bas	HO reactions based on datasheets in Supplement and on the IUPAC website updated in 2019	updated in 2019			,	
HOX_VOC/	HO + CH3CH2CH2 → H2O + CH2CH2CH2CH3 → H3O + CH3CHCH2CH3					
	overall	$2.35 \times 10^{-12}$	± 0.06	$9.8 \times 10^{-12} \exp(-425/T)$	180-300	± 100
HOx_VOC8	$HO + CH_2 = C(CH_3)CH = CH_2 \text{ (isoprene)} \rightarrow \text{products}$	$1.0 \times 10^{-10}$	$\pm 0.06$	$2.1 \times 10^{-11} \exp(465/T)$	240-630	± 150
HOx_VOC9	$HO + \alpha$ -pinene $\rightarrow$ products	$5.3 \times 10^{-11}$	± 0.08	$1.3 \times 10^{-11} \exp(410/T)$	240-360	± 100
HOx_VOC14	$HO + CH_3CH_2CH_2CHO \rightarrow products$	$2.3 \times 10^{-11}$	± 0.08	$5.8 \times 10^{12} \exp(410/T)$	250-430	$\pm 250$
HOx_VOC15	$HO + CH_2 = C(CH_3)CHO \rightarrow products$	$3.0 \times 10^{-11}$	± 0.08	$8.4 \times 10^{12} \exp(380/T)$	230-380	± 100
$HOx_VOC20$	$HO + CH_3C(O)CH_2CH_3 \rightarrow products$	$1.1 \times 10^{12}$	$\pm 0.10$	$1.5 \times 10^{-12} \exp(-90/T)$	210-300	± 200
HOx_VOC21	$HO + CH_3C(O)CH = CH_2 \rightarrow products$	$2.0 \times 10^{-11}$	$\pm 0.10$	$2.6 \times 10^{-12} \exp(610/T)$	230-380	± 200
$HOx_VOC22$	HO + pinonaldehyde → products	$3.9 \times 10^{-11}$	$\pm 0.15$	$5.2 \times 10^{-12} \exp(600/T)$	230-380	± 300
HOx_VOC27	$\text{HO} + \text{CH}_3\text{CH}_2\text{CH}_2\text{CH} \rightarrow \text{products}$	$8.5\times10^{-12}$	± 0.06	$5.3 \times 10^{-12} \exp(140/T)$	260-380	± 200
HOx_VOC28	$HO + CH_3CH(OH)CH_2CH_3 \rightarrow products$	$8.7 \times 10^{-12}$	± 0.08			
$HOx_VOC29$	$HO + (CH_3)_2C(OH)CH = CH_2 \rightarrow products$	$6.3 \times 10^{-11}$	$\pm 0.08$	$8.1 \times 10^{-12} \exp(610/T)$	230-300	± 200
$HOx_VOC31$	HO + 3-methylfuran → products	$9.3 \times 10^{-11}$	$\pm 0.15$			
$HOx_VOC33$	$HO + (CH_3)_2C(OH)CHO \rightarrow products$	$1.4 \times 10^{-11}$	$\pm 0.10$			
$HOx_VOC42$	$HO + 1-C_4H_9ONO_2 \rightarrow products$	$1.6 \times 10^{-12}$	$\pm 0.06$			
HOx_VOC43	$HO + 2 \cdot C_4H_9ONO_2 \rightarrow products$	$8.6 \times 10^{-13}$	$\pm 0.15$			
HOx_VOC46	$HO + CH_3CH_2C(O)CH_2ONO_2 \rightarrow products$	$8.2 \times 10^{-13}$	$\pm 0.30$			
HOx_VOC47	$HO + CH_3CH(ONO_2)C(O)CH_3 \rightarrow products$	$1.2 \times 10^{-12}$	$\pm 0.30$			
HOx_VOC48	$HO + CH_2 = C(CH_3)C(O)OONO_2 (MPAN) \rightarrow products$	$2.9 \times 10^{-11}$	+0.2			
$HOx_VOC60$	$\mathrm{HO} + (\mathrm{CH}_3)_3\mathrm{CH} \rightarrow \mathrm{H}_2\mathrm{O} + (\mathrm{CH}_3)_3\mathrm{C}$					
	$\rightarrow$ H <sub>2</sub> O + (CH <sub>3</sub> ) <sub>2</sub> CHCH <sub>2</sub>					
	Overall	$2.1 \times 10^{-12}$	$\pm 0.04$	$5.4 \times 10^{-12} \exp(-285/T)$	210-300	$\pm 150$
HOx_VOC61	$HO + 2$ -methylpropene $\rightarrow$ products	$5.1 \times 10^{-11}$	$\pm 0.04$	$9.4 \times 10^{-12} \exp(505/T)$	290-430	± 200
$HOx_VOC62$	$HO + 1$ -butene $\rightarrow$ products	$3.1 \times 10^{-11}$	± 0.06	$6.6 \times 10^{-12} \exp(465/T)$	290-430	± 150
HOx_VOC63	$HO + cis-2$ -butene $\rightarrow$ products	$5.6 \times 10^{-11}$	$\pm 0.10$	$1.1 \times 10^{-11} \exp(485/T)$	290-430	± 200
HOx_VOC64	$HO + trans-2$ -butene $\rightarrow$ products	$7.1 \times 10^{-11}$	± 0.06	$1.1 \times 10^{-11} \exp(553/T)$	290-430	± 200
HOx_VOC66	$HO + CH_3C(O)C(O)CH_3 \rightarrow products$	$2.3 \times 10^{-13}$	$\pm 0.06$	$5.25 \times 10^{-13} \exp(-243/T)$	240-350	± 50
HOx_VOC67	$HO + n \cdot C_3H_7C(O)OH \rightarrow products$	$1.8 \times 10^{-12}$	$\pm 0.15$			
HOx_VOC68	$HO + i - C_3H_7CHO \rightarrow products$	$2.6 \times 10^{-11}$	$\pm 0.04$	$6.8 \times 10^{-12} \exp(410/T)$	240-425	09 ∓
$HOx_VOC69$	$HO + (CH_3)_2 CHCH_2 OH \rightarrow products$	$8.9 \times 10^{-12}$	$\pm 0.08$	$2.73 \times 10^{-12} \exp(352/T)$	240-370	± 120
$HOx_VOC70$	$HO + (CH_3)_3COH \rightarrow products$	$1.1 \times 10^{-12}$	$\pm 0.06$	$1.6 \times 10^{-12} \exp(-121/T)$	240-314	± 75
HOx_VOC76	$\mathrm{HO} + \mathrm{C_2H_3CH}(\mathrm{OH})\mathrm{CHO} \rightarrow \mathrm{C_2H_3CH}(\mathrm{OH})\mathrm{CO} + \mathrm{H_2O}$					
	$\rightarrow$ C <sub>2</sub> H <sub>5</sub> C(OH)CHO + H <sub>2</sub> O	:				
	overall	$2.4 \times 10^{-11}$	$\pm 0.10$			
HOx_VOC77	$\text{HO} + \text{C}_2\text{H}_3\text{CH}(\text{OH})\text{CH}_2\text{ONO}_2 \rightarrow \text{products}$	$7.0 \times 10^{-12}$	± 0.20			
HOx_VOC78	+ $C_2H_5CH(ONO_2)CH_2OH \rightarrow products$	$7.4 \times 10^{-12}$	$\pm 0.20$			
HOx_VOC79	HO + CH <sub>3</sub> C(O)CH(OH)CH <sub>3</sub> $\rightarrow$ H <sub>2</sub> O + CH <sub>2</sub> C(O)CH(OH)CH <sub>3</sub>					
	Circ(O)C(Cir)Circ → products					
	Overall	$9.7 \times 10^{-12}$	± 0.10	$1.24 \times 10^{-12} \exp(612/T)$	280-350	± 350
HOx_VOC84	$HO + \alpha$ -terpinene $\rightarrow$ products	$3.5\times10^{-10}$	± 0.08			





	# 150 # 100 # 100 # 50 # 150		.0 ± 300 0 ± 200 50 ± 200	± 200 ± 600		009 =	
	240-420 220-360 280-320 230-360 310-430	298430	330-1410 230-350 310-1050	210-350	290-350	290-350	
	1.62 × 10 <sup>-1</sup> exp(460/T) 3.41 × 10 <sup>-1</sup> exp(470/T) 4.14 × 10 <sup>-1</sup> exp(754/T) 2.5 × 10 <sup>-1</sup> exp(377/T) 4.0 × 10 <sup>-1</sup> exp(579/T)	$2.2 \times 10^{-10}$ $2.3 \times 10^{-10}$	$3.8 \times 10^{-11} \text{exp(-2520/T)}$ $2.3 \times 10^{-12} \text{exp(-190/T)}$ $2.5 \times 10^{-11} \text{exp(-1270/T)}$	1.8 × 10 <sup>-12</sup> exp(340/T) 2.4 × 10 <sup>-12</sup> exp(965/T)	$1.6 \times 10^{-12} \exp(970/T)$	$1.9 \times 10^{-1} \exp(970/T)$ $4.7 \times 10^{-13} \exp(1220/T)$	
H H 0.10 H H 0.10 H H 0.10 H H 0.10	H 0.05 H 0.05 H 0.05 H 0.15 H 0.15 H 0.15	± 0.15 ± 0.30 ± 0.30 ± 0.30	± 0.50 ± 0.06 ± 0.20	± 0.06 ± 0.10	± 0.10	+ 0.10 + 0.08 + 0.15 + 0.15	
2.2 × 10 · 1 3.2 × 10 · 10 6.7 × 10 · 11 4.7 × 10 · 11 9.0 × 10 · 11 2.0 × 10 · 10 2 × 10 · 10 2 × 10 · 10	$2.5 \times 10^{-1}$ $7.6 \times 10^{-1}$ $1.65 \times 10^{-10}$ $5.2 \times 10^{-11}$ $8.0 \times 10^{-11}$ $8.3 \times 10^{-11}$ $2.1 \times 10^{-10}$ $2.8 \times 10^{-10}$	$\begin{array}{c} 1.2 \times 10^{10} \\ 2.2 \times 10^{10} \\ 2.3 \times 10^{10} \\ 1.9 \times 10^{10} \end{array}$	$8 \times 10^{-15}$ $1.2 \times 10^{-12}$ $3.5 \times 10^{-13}$	$5.6 \times 10^{-12}$ $6.2 \times 10^{-11}$	$4.2 \times 10^{-11}$	4.8 × 10 <sup>-11</sup> 2.8 × 10 <sup>-11</sup> 1.0 × 10 <sup>-10</sup> 2.0 × 10 <sup>-10</sup> 1.5 × 10 <sup>-10</sup>	
HO + α-phellandrene → products HO + β-phellandrene → products HO + α-cedrene → products HO + longifolene → products HO + c-copaene → products HO + β-caryophyllene → products HO + α-humilene → products	TO + α-numintence → products  HO + β-pinence → products  HO + limonence → products  HO + camphence → products  HO + 2-carence → products  HO + 2-carence → products  HO + β-varence → products  HO + β-varence → products		$\begin{aligned} & HO + C_6H_6 \text{ (benzene)} \rightarrow H_2O + C_6H_5 \\ & \rightarrow HOC_6H_6 \end{aligned}$ Overall $HO + C_6H_5CH_3 \text{ (toluene)} \rightarrow H_2O + C_6H_5CH_2 \\ & \rightarrow HOC_5H_5CH_3 \end{aligned}$	Overall  HO + $m$ -CH <sub>3</sub> C <sub>6</sub> H <sub>4</sub> OH ( $m$ -cresol) $\rightarrow$ H <sub>2</sub> O + CH <sub>3</sub> C <sub>6</sub> H <sub>4</sub> O $\rightarrow$ H <sub>2</sub> O + CH <sub>3</sub> C <sub>6</sub> H <sub>4</sub> OH  Overall  HO + $o$ -CH <sub>3</sub> C <sub>6</sub> H <sub>4</sub> OH ( $o$ -cresol) $\rightarrow$ H <sub>2</sub> O + CH <sub>3</sub> C <sub>6</sub> H <sub>4</sub> OH $\rightarrow$ H <sub>2</sub> O + CH <sub>3</sub> C <sub>6</sub> H <sub>4</sub> OH $\rightarrow$ H <sub>2</sub> O + CH <sub>3</sub> C <sub>6</sub> H <sub>4</sub> OH	Overall $Overall$ $Overa$	Overall HO + C <sub>6</sub> H <sub>5</sub> OH (phenol) → H <sub>2</sub> O + C <sub>6</sub> H <sub>5</sub> O → H <sub>2</sub> O + C <sub>6</sub> H <sub>2</sub> OH → HOC <sub>6</sub> H <sub>5</sub> OH → HOC <sub>6</sub> H <sub>5</sub> OH Overall HO + 1,2-dilydroxybenzene (1,2-C <sub>6</sub> H <sub>4</sub> (OH) <sub>2</sub> ) → products HO + 1,2-dilydroxy-3-methylbenzene → products HO + 1,2-dilydroxy-4-methylbenzene → products	
HOX_VOC88 HOX_VOC89 HOX_VOC90 HOX_VOC91 HOX_VOC91 HOX_VOC93	HOX_VOC99 HOX_VOC100 HOX_VOC101 HOX_VOC102 HOX_VOC103 HOX_VOC103 HOX_VOC104	HOX_VOC106 HOX_VOC107 HOX_VOC108 HOX_VOC109	HOx_AROM1 HOx_AROM2	HOx_AROM3 HOx_AROM4	HOx_AROM5	HOX_AROM6 HOX_AROM7 HOX_AROM8 HOX_AROM9	





± 0.30 ± 0.15 ± 0.20 ± 0.30 ± 0.15	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	$\pm 0.08$ 5.9 × $10^{-12}$ exp(225/ $T$ ) 290-350 $\pm 1.70$ $\pm 0.08$			± 0.10 3.0 × 10 <sup>-12</sup> exp(-3050/T) 290-430 ± 0.10 3.2 × 10 <sup>-13</sup> exp(-950/T) 230-480 ± 0.10	± 0.10 3.0 × 10 <sup>-12</sup> exp(-3050/T) 290.430 ± 0.10 3.2 × 10 <sup>-13</sup> exp(-950/T) 230.480 ± 0.10 1.78×10 <sup>-12</sup> exp(-530/T) 200-380 1.28×10 <sup>-13</sup> exp(570/T)}	± 0.10 3.0 × 10 <sup>-12</sup> exp(-3050/T) 290-430 ± 0.10 3.2 × 10 <sup>-13</sup> exp(-950/T) 230-480 ± 0.10 1.78×10 <sup>-12</sup> exp(-530/T) 20-380 ± 0.08 1.78×10 <sup>-14</sup> exp(570/T)} ± 0.12 ± 0.12	± 0.10 3.0 × 10 <sup>-12</sup> exp(-3050/T) 290-430 ± 0.10 3.2 × 10 <sup>-13</sup> exp(-950/T) 230-480 ± 0.10 1.78×10 <sup>-13</sup> exp(-550/T) 230-480 ± 0.08 {1.78×10 <sup>-12</sup> exp(-530/T) + 200-380 ± 0.12 ± 0.12 ± 0.12	± 0.10 3.0 × 10 <sup>-12</sup> cxp(-3050/T) 290-430 ± 0.10 3.2 × 10 <sup>-13</sup> cxp(-950/T) 230-480 ± 0.00 ± 0.08 {1.78×10 <sup>-12</sup> cxp(-530/T) + 200-380 ± 0.12 ± 0.12 ± 0.12 ± 0.12 ± 0.12 ± 0.12 ± 0.12 + 0.12	± 0.10 3.0 × 10 <sup>-12</sup> exp(-3050/T) 290-430 ± 0.10 3.2 × 10 <sup>-13</sup> exp(-950/T) 230-480 ± 0.00 1.78×10 <sup>-13</sup> exp(-530/T) + 200-380 ± 0.12 1.28×10 <sup>-14</sup> exp(570/T)} ± 0.12 ± 0.12 ± 0.12 ± 0.12 ± 0.12 ± 0.12	± 0.10 3.0 × 10 <sup>-12</sup> cxp(-3050/T) 290-430 ± 0.10 3.2 × 10 <sup>-13</sup> cxp(-950/T) 230-480 ± 0.10 3.2 × 10 <sup>-13</sup> cxp(-950/T) 230-480 ± 0.10 (1.78×10 <sup>-13</sup> cxp(-530/T) + 200-380 ± 0.12 ± 0.12 (1.28×10 <sup>-14</sup> cxp(570/T)) + 200-380 ± 0.13 (1.28×10 <sup>-14</sup> cxp(570/T) + 200-380 ± 0.13 (1.28×10 <sup>-14</sup> cxp(570/T) + 200-380 ± 0.13 (1.28×10 <sup>-14</sup> cxp(570/T) + 200-380 ± 0.1	± 0.10 3.0 × 10 <sup>-12</sup> exp(-3050/T) 290.430 ± 0.10 3.2 × 10 <sup>-13</sup> exp(-950/T) 230.480 ± 0.10 3.2 × 10 <sup>-13</sup> exp(-950/T) 230.480 ± 0.10 (1.78×10 <sup>-13</sup> exp(-530/T) + 200-380 ± 0.12 ± 0.12 ± 0.12 ± 0.12	± 0.10 3.0 × 10 <sup>-12</sup> cxp(-3050/T) 290.430 ± 0.10 3.2 × 10 <sup>-13</sup> cxp(-950/T) 230.480 ± 0.10 3.2 × 10 <sup>-13</sup> cxp(-950/T) 230.480 ± 0.03 {1.78×10 <sup>-13</sup> cxp(-530/T) + 200-380 ± 0.12 ± 0.12 ± 0.13 ± 0.12 ± 0.13 ± 0.13 ± 0.15 ± 0.15	± 0.10 3.0 × 10 <sup>-12</sup> exp(-3050/T) 290-430 ± 0.10 ± 0.10 3.2 × 10 <sup>-13</sup> exp(-950/T) 230-480 ± 0.10 ± 0.08 {1.78×10 <sup>-12</sup> exp(-530/T) + 200-380 ± 0.12 ± 0.12 ± 0.12 ± 0.12	± 0.10 3.0 × 10 <sup>-12</sup> exp(-3050/T) 290.430 ± 0.10 3.2 × 10 <sup>-13</sup> exp(-950/T) 230.480 ± 0.10 ± 0.08 {1.78×10 <sup>-12</sup> exp(-530/T) + 200-380 ± 0.12 ± 0.12 ± 0.12 ± 0.12 ± 0.12 ± 0.12 ± 0.12 ± 0.12 ± 0.13 ± 0.13 ± 0.15 ± 0.15 ± 0.15 ± 0.15 ± 0.15 ± 0.15 ± 0.15 ± 0.15 ± 0.15 ± 0.15	± 0.10 3.0 × 10 <sup>-12</sup> exp(-3050/T) 290.430 ± 0.10 3.2 × 10 <sup>-12</sup> exp(-950/T) 230.480 ± 0.10 ± 0.08 {1.78×10 <sup>-12</sup> exp(-530/T) + 200-380 ± 0.12 ± 0.12 ± 0.13 ± 0.12 ± 0.13 ± 0.15 ±	± 0.10 3.0 × 10 <sup>-12</sup> exp(-3050/T) 290.430 ± 0.10 3.2 × 10 <sup>-13</sup> exp(-950/T) 230.480 ± 0.10 ± 0.10 ± 0.12 {1.78 × 10 <sup>-13</sup> exp(570/T)} 230.480 ± 0.12 ± 0.12 ± 0.12 ± 0.12 ± 0.12 ± 0.12 ± 0.13 ± 0.15 ± 0.25 ± 0.10 ± 0.25 ± 0.25	± 0.10 3.0 × 10 <sup>-12</sup> exp(-3050/T) 290.430 ± 0.10 3.2 × 10 <sup>-13</sup> exp(-950/T) 230.480 ± 0.10 3.2 × 10 <sup>-13</sup> exp(-950/T) 230.480 ± 0.12 (1.78×10 <sup>-13</sup> exp(570/T)) 230.480 ± 0.12 ± 0.12 (1.78×10 <sup>-14</sup> exp(570/T)) 230.480 ± 0.12 ± 0.12 (1.8×10 <sup>-14</sup> exp(570/T)) 230.480 ± 0.13 ± 0.13 (1.8×10 <sup>-14</sup> exp(570/T)) 230.480 ± 0.25 ± 0.25 (1.8×10 <sup>-14</sup> exp(570/T)) 230.480 ± 0.25 ± 0.25 (1.8×10 <sup>-14</sup> exp(570/T)) 230.480 ± 0.25 ± 0.25 (1.8×10 <sup>-14</sup> exp(570/T)) 230.480	± 0.10 3.0 × 10 <sup>-12</sup> exp(-3050/T) 290.430 ± 0.10 3.2 × 10 <sup>-13</sup> exp(-950/T) 230.480 ± 0.10 ± 0.08 {1.78×10 <sup>-12</sup> exp(-530/T) + 200-380 ± 0.12 ± 0.12 ± 0.12 ± 0.12 ± 0.12 ± 0.12 ± 0.12 ± 0.12 ± 0.13 ± 0.13 ± 0.15 ± 0.15 ± 0.15 ± 0.25 ± 0.15 ± 0.25 ± 0.15 ± 0.25 ± 0.25 ± 0.25 ± 0.25 ± 0.25	± 0.10 3.0 × 10 <sup>-12</sup> exp(-3050/T) 290.430 ± 0.10 3.2 × 10 <sup>-12</sup> exp(-950/T) 230.480 ± 0.10 ± 0.08 {1.78×10 <sup>-12</sup> exp(-530/T)} 230.480 ± 0.12 ± 0.12 ± 0.25 ± 0	± 0.10 3.0 × 10 <sup>-12</sup> exp(-3050/T) 290.430 ± 0.10 3.2 × 10 <sup>-13</sup> exp(-950/T) 230.480 ± 0.10 3.2 × 10 <sup>-13</sup> exp(-950/T) 230.480 ± 0.12 (1.78×10 <sup>-13</sup> exp(570/T)) 230.480 ± 0.12 ± 0.12 (1.78×10 <sup>-14</sup> exp(570/T) 230.480 ± 0.12 ± 0.12 (1	± 0.10 3.0 × 10 <sup>-12</sup> exp(-3050/T) 290-430 ± 0.10 3.2 × 10 <sup>-13</sup> exp(-950/T) 230-480 ± 0.10 3.2 × 10 <sup>-13</sup> exp(-950/T) 230-480 ± 0.08 {1.78×10 <sup>-13</sup> exp(570/T)} 230-480 ± 0.12 ± 0.12 ± 0.13 ± 0.25 ±	± 0.10 3.0 × 10 <sup>-12</sup> exp(-3050/T) 290.430 ± 0.10 3.2 × 10 <sup>-12</sup> exp(-950/T) 230.480 ± 0.10 ± 0.08 {1.78×10 <sup>-12</sup> exp(-530/T) + 200-380 ± 0.12 ± 0.12 ± 0.25 ±
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HO + 3-methyl-2-nitrophenol → products HO + 4-methyl-2-nitrophenol → products HO + 5-methyl-2-nitrophenol → products HO + 6-methyl-2-nitrophenol → products HO + 1,4-benzoquinone → products	The control of the co	$\rightarrow$ products HO + C <sub>6</sub> H <sub>5</sub> CH <sub>2</sub> OH (benzaldehyde) $\rightarrow$ products HO + C <sub>6</sub> H <sub>5</sub> CH <sub>2</sub> OH (benzyl alcohol) $\rightarrow$ products	$NO_{ m s}$ reactions based on datasheets in Supplement and on the $IUPAC$ website updated in 2019	ed on datasheets in Supplement and on the IUPAC website NO <sub>3</sub> + 2-methylpropane, $(CH_3)CH \rightarrow products$ NO + 2-methylpropane $(CH_3)C=(CH_3)\rightarrow products$	ied on datasheets in Supplement and on the IUPAC website  NO <sub>3</sub> + 2-methylpropane, (CH <sub>3</sub> ) <sub>8</sub> CH → products  NO <sub>3</sub> + 2-methylpropene ((CH <sub>3</sub> ) <sub>2</sub> C=CH <sub>2</sub> )→ products  NO <sub>4</sub> + 1-buttene → products  NO <sub>4</sub> + cis-2-buttene → products	ied on datasheets in Supplement and on the IUPAC website  NO <sub>3</sub> + 2-methylpropane, (CH <sub>3</sub> ) <sub>8</sub> CH → products  NO <sub>3</sub> + 1-butten → products  NO <sub>4</sub> + 1-butten → products  NO <sub>5</sub> + riss-2-butten → products	ied on datasheets in Supplement and on the IUPAC website  NO <sub>3</sub> + 2-methylpropane, (CH <sub>3</sub> ),CH → products  NO <sub>5</sub> + 2-methylpropene ((CH <sub>3</sub> ),C=CH <sub>2</sub> ) → products  NO <sub>5</sub> + 1-butene → products  NO <sub>5</sub> + cis-2-butene → products  NO <sub>5</sub> + trans-2-butene → products  NO <sub>5</sub> + d-limonene → products  NO <sub>7</sub> + 2-carene → products  NO <sub>7</sub> + 2-carene → products	red on datasheets in Supplement and on the IUPAC website  NO <sub>3</sub> + 2-methylpropane, (CH <sub>3</sub> ) <sub>2</sub> CH → products  NO <sub>3</sub> + 2-methylpropene ((CH <sub>3</sub> ) <sub>2</sub> C=CH <sub>2</sub> ) → products  NO <sub>3</sub> + 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products  NO <sub>3</sub> + sabinene → products  NO <sub>3</sub> + sabinene → products  NO <sub>3</sub> + coinene, cis and trans → products	red on datasheets in Supplement and on the IUPAC website  NO <sub>3</sub> + 2-methylpropane, (CH <sub>3</sub> ),CH → products  NO <sub>3</sub> + 2-methylpropene ((CH <sub>3</sub> ),C=CH <sub>3</sub> ) → products  NO <sub>3</sub> + 1-butene → products  NO <sub>3</sub> + 1-butene → products  NO <sub>3</sub> + reans-2-butene → products  NO <sub>3</sub> + trans-2-butene → products  NO <sub>3</sub> + 3-carene → products  NO <sub>4</sub> + 3-carene → products  NO <sub>4</sub> + 3-pinene → products  NO <sub>4</sub> + 3-pinene → products  NO <sub>5</sub> + 4-pinene → products  NO <sub>5</sub> + 4-pinene → products  NO <sub>5</sub> + 2-carene → products	red on datasheets in Supplement and on the IUPAC website  NO <sub>3</sub> + 2-methylpropane, (CH <sub>3</sub> ),CH → products  NO <sub>3</sub> + 2-methylpropane, (CH <sub>3</sub> ),C=CH <sub>2</sub> ) → 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 NO <sub>3</sub> + 3-carene → products  NO <sub>3</sub> + 3-carene → products  NO <sub>3</sub> + 3-poinene → products  NO <sub>3</sub> + 3-poinene → products  NO <sub>3</sub> + y-poinene → products  NO <sub>3</sub> + v-terpinene → products  NO <sub>3</sub> + α-repinene → products	red on datasheeas in Supplement and on the IUPAC website  NO <sub>3</sub> + 2-methylpropane, (CH <sub>3</sub> ) <sub>2</sub> CH → products  NO <sub>3</sub> + 2-methylpropene ((CH <sub>3</sub> ) <sub>2</sub> C=CH <sub>2</sub> ) → products  NO <sub>3</sub> + 1-butene → products  NO <sub>3</sub> + trans-2-butene → products  NO <sub>3</sub> + trans-2-butene → products  NO <sub>3</sub> + d-limonene → products  NO <sub>3</sub> + d-limonene → products  NO <sub>3</sub> + 3-carene → products  NO <sub>3</sub> + 3-carene → products  NO <sub>3</sub> + 3-prinene → products  NO <sub>3</sub> + myrcene → products  NO <sub>3</sub> + myrcene → products  NO <sub>3</sub> + v-terpinene → products	red on datasheeas in Supplement and on the IUPAC website  NO <sub>3</sub> + 2-methylpropane, (CH <sub>3</sub> ),CH → products  NO <sub>3</sub> + 2-methylpropene ((CH <sub>3</sub> ),CC+(F <sub>2</sub> ) → products  NO <sub>3</sub> + 2-methylpropene ((CH <sub>3</sub> ),C=(CH <sub>2</sub> ) → products  NO <sub>3</sub> + cis-2-butene → products  NO <sub>3</sub> + cis-2-butene → products  NO <sub>3</sub> + d-limonene → products  NO <sub>3</sub> + 2-carene → products  NO <sub>3</sub> + 3-carene → products  NO <sub>3</sub> + 3-carene → products  NO <sub>3</sub> + 3-prinene → products  NO <sub>3</sub> + subinene → products  NO <sub>3</sub> + subinene → products  NO <sub>3</sub> + corimone, cis and trans → products  NO <sub>3</sub> + corimone → products  NO <sub>3</sub> + corimone → products  NO <sub>3</sub> + corpulanene → products  NO <sub>3</sub> + cophellanene → products  NO <sub>3</sub> + cophellanene → products  NO <sub>3</sub> + cophellanene → products  NO <sub>3</sub> + campleone → products	red on datasheets in Supplement and on the IUPAC website  NO <sub>3</sub> + 2-methylpropane, (CH <sub>3</sub> ) <sub>2</sub> CH → products  NO <sub>3</sub> + 2-methylpropene ((CH <sub>3</sub> ) <sub>2</sub> C=(CH <sub>2</sub> ) → products  NO <sub>3</sub> + 1-butene → products  NO <sub>3</sub> + 1-butene → products  NO <sub>3</sub> + trans-2-butene → products  NO <sub>3</sub> + trans-2-butene → products  NO <sub>3</sub> + 2-carene → products  NO <sub>3</sub> + 3-pinene → products  NO <sub>3</sub> + 4-pinene → products  NO <sub>3</sub> + criepinene → products	red on datasheets in Supplement and on the IUPAC website  NO <sub>3</sub> + 2-methylpropane, (CH <sub>3</sub> ),CH → products  NO <sub>3</sub> + 2-methylpropane, (CH <sub>3</sub> ),C=CH <sub>3</sub> ) → products  NO <sub>3</sub> + 1-butene → products  NO <sub>3</sub> + 1-butene → products  NO <sub>3</sub> + reans-2-butene → products  NO <sub>3</sub> + 4-limonene → products  NO <sub>3</sub> + 3-carene → products  NO <sub>3</sub> + 3-carene → products  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<sub>3</sub> + 3-prinene → products  NO <sub>3</sub> + 4-terpinene → products  NO <sub>3</sub> + α-terpinene → products  NO <sub>3</sub> + α-terpinene → products  NO <sub>3</sub> + α-terpinene → products  NO <sub>3</sub> + α-prellandrene → products  NO <sub>3</sub> + α-copleme → products  NO <sub>3</sub> + α-copleme → products  NO <sub>3</sub> + α-copaene → products  NO <sub>3</sub> + α-copaene → products	red on datasheets in Supplement and on the IUPAC website  NO <sub>3</sub> + 2-methylpropane, (CH <sub>3</sub> ) <sub>2</sub> CH → products  NO <sub>3</sub> + 2-methylpropene ((CH <sub>3</sub> ) <sub>2</sub> C=CH <sub>2</sub> ) → products  NO <sub>3</sub> + 1-butene → products  NO <sub>3</sub> + 1-butene → products  NO <sub>3</sub> + rans-2-butene → products  NO <sub>3</sub> + rans-2-butene → products  NO <sub>3</sub> + 3-carene → products  NO <sub>4</sub> + 3-carene → products  NO <sub>5</sub> + carene → products  NO <sub>5</sub> + carene → products  NO <sub>4</sub> + carepinene → 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 $^{+\ 0.15}_{\ \pm\ 0.15}$   $^{+\ 0.15}_{\ \pm\ 0.15}$ 

 $3.8 \times 10^{-12}$   $9.9 \times 10^{-11}$   $1.7 \times 10^{-10}$   $1.5 \times 10^{-10}$ 

 $\begin{aligned} NO_3 + 1.2\text{-}dihydroxybenzene\,(1,2\text{-}C_6H_4(OH)_2) &\rightarrow \text{products} \\ NO_3 + 1.2\text{-}dihydroxy\text{-}3\text{-}methylbenzene\, &\rightarrow \text{products} \\ NO_3 + 1.2\text{-}dihydroxy\text{-}4\text{-}methylbenzene\, &\rightarrow \text{products} \end{aligned}$ 

NO3\_AROM7 NO3\_AROM8 NO3\_AROM9

 $\pm \ 0.15$ 

 $1.0\times10^{11}$ 

 $< 3 \times 10^{-17}$ 7.8 × 10<sup>-17</sup>

$$\begin{split} NO_{3} + C_{6}H_{6} \left( benzene \right) \rightarrow products \\ NO_{3} + C_{6}H_{3}CH_{3} \left( toluene \right) \rightarrow products \\ NO_{3} + m.-CH_{3}C_{6}H_{4}OH \left( m.-cresol \right) \rightarrow CH_{3}C_{6}H_{4}O + HNO_{3} \end{split}$$

NO3\_AROMI NO3\_AROM2 NO3\_AROM3

 $7.9 \times 10^{-12}$  $1.7 \times 10^{-11}$ 

 $NO_3 + valencene \rightarrow products$  $NO_3 + \alpha$ -terpineol  $\rightarrow products$ 

NO3\_VOC55 NO3\_VOC56  $\pm \ 0.15$ 

 $1.4\times10^{11}$ 

Overall  $\mathrm{NO}_3 + p\text{-}\mathrm{CH}_3\mathrm{C}_6\mathrm{H}_4\mathrm{OH} \ (p\text{-}\mathrm{cresol}) \to \mathrm{CH}_3\mathrm{C}_6\mathrm{H}_4\mathrm{O} + \mathrm{HNO}_3$ 

→ other products

Overall  $NO_3 + C_6H_5OH \text{ (phenol)} \rightarrow C_6H_5O + HNO_3$ 

NO3\_AROM6

Overall  $NO_3 + o\text{-}CH_3C_6H_4OH \text{ ($o$-cresol$)} \rightarrow CH_3C_6H_4O + HNO_3$ 

NO3\_AROM4

NO3\_AROM5

 $\pm \ 0.15$ 

 $1.1\times10^{11}$ 

$CH_3C(O)C(O)CH_3 + h\nu \rightarrow products$	$i-C_3H_7CHO + h\nu \rightarrow products$	cis/trans-but-2-enedial + $h\nu \rightarrow products$	4-oxopent-2-enedial + h $\nu \rightarrow$ products	2-nitrophenol + h $\nu \rightarrow$ products	benzaldehyde + h $\nu \rightarrow \text{products}$	3-methyl-2-nitrophenol + h $\nu \rightarrow$ products	4-methyl-2-nitrophenol + h $\nu \rightarrow \text{products}$
P23	P24	P26	P27	P28	P30	P31	P32

<sup>a</sup> The cited uncertainty corresponds approximately to 95% confidence limits.