

1 **Supporting Information for**

2 Significant source of secondary aerosol: formation from gasoline  
3 evaporation emissions in the presence of SO<sub>2</sub> and NH<sub>3</sub>

4 **Tianzeng Chen<sup>1,3,a</sup>, Yongchun Liu<sup>2,a</sup>, Qingxin Ma<sup>1,3,4,\*</sup>, Biwu Chu<sup>1,3,4</sup>, Peng Zhang<sup>1</sup>,**

5 **Changgeng Liu<sup>1</sup>, Jun Liu<sup>1,3</sup>, Hong He<sup>1,3,4,\*</sup>**

6 <sup>1</sup> State Key Joint Laboratory of Environment Simulation and Pollution Control, Research Center for  
7 Eco-Environmental Sciences, Chinese Academy of Sciences, Beijing 100085, China

8 <sup>2</sup> Beijing Advanced Innovation center for Soft Matter Science and Engineering, Beijing University  
9 of Chemical Technology, Beijing 100029, China

10 <sup>3</sup> University of Chinese Academy of Sciences, Beijing 100049, China

11 <sup>4</sup> Center for Excellence in Regional Atmospheric Environment, Institute of Urban Environment,  
12 Chinese Academy of Sciences, Xiamen 361021, China

13 <sup>a</sup> These authors contributed equally to this work and should be considered as co-first authors

14 *Corresponding authors:* [qxma@rcees.ac.cn](mailto:qxma@rcees.ac.cn) (Qingxin Ma), and [honghe@rcees.ac.cn](mailto:honghe@rcees.ac.cn) (Hong He)

## 15 S1. Vapor wall loss and gas-particle partitioning timescales

16 The loss of vapor by condensation onto the wall is generally considered to be a first-order process,  
17 which can be characterized by the first-order wall-loss coefficient  $k_w$  ( $s^{-1}$ ). According to the following  
18 equation reported by McMurry and Grosjean (1985), the value of  $k_w$  is equal to:

$$19 \quad k_w = \frac{A}{V} \times \frac{\alpha_w \bar{c}}{1.0 + \frac{\pi}{2} \times \left[ \frac{\alpha_w \bar{c}}{4(k_e D_{\text{gas}})^{0.5}} \right]}$$

20 in which A and V are the surface and volume of the smog chamber, respectively. For our cuboid smog  
21 chamber ( $L \times W \times H = 3.0 \times 2.5 \times 4.0$  m),  $A=59$  m<sup>2</sup>,  $V=30$  m<sup>3</sup>.  $\alpha_w$  is the mass accommodation coefficient  
22 of vapors onto the chamber walls,  $\bar{c}$  is the mean thermal speed of the molecules,  $k_e$  is the coefficient of  
23 eddy diffusion, and  $D_{\text{gas}}$  is the gas-phase diffusivity.

24 For a given vapor molecule, the mean thermal speed  $\bar{c}$  could be calculated according to the  
25 following equation:

$$26 \quad \bar{c} = \sqrt{\frac{8RT}{\pi MW}}$$

27 in which R is the ideal gas constant (i.e., 8.314 J mol<sup>-1</sup> K<sup>-1</sup>), T is the experimental temperature ( T=299.15  
28 K in this study), and MW is the molecular weight (an upper bound and a lower bound of molecular mass  
29 of organic vapors was adopted, i.e., 100 g mol<sup>-1</sup> and 300 g mol<sup>-1</sup> in this study).

30  $D_{\text{gas}}$  is assumed to vary with molecular weight (MW) and is equal to  $D_{\text{CO}_2}(MW_{\text{CO}_2}/MW)$ , with  
31  $D_{\text{CO}_2} = 1.38 \times 10^{-5}$  m<sup>2</sup> s<sup>-1</sup>. Therefore, this leaves  $k_e$  and  $\alpha_w$  as the two key unknowns. For the value of  $k_e$ ,  
32 0.015 s<sup>-1</sup> was estimated according to the values reported by previous studies for a 28 m<sup>3</sup> Caltech chamber  
33 (Loza et al., 2012; McMurry and Rader, 1985; Zhang et al., 2014). For the value of  $\alpha_w$ , 10<sup>-5</sup> was adopted  
34 according to the experimental results of Matsunaga and Ziemann (2010).

35 Then the timescale associated with vapor-wall loss ( $\tau_{g-w}$ ) is calculated to be:

36 
$$\tau_{g-w} = k_w^{-1}$$

37 for the timescale associated with reaching gas-to-particle partitioning equilibrium ( $\bar{\tau}_{g-p}$ ), which  
38 varies with particle number concentration and diameter, and could be approximately calculated to be:

39 
$$\bar{\tau}_{g-p} = (2\pi N_p \bar{D}_p D_{gas} \bar{F}_{FS})^{-1}$$

40 in which  $N_p$  is the particle number concentration,  $\bar{D}_p$  is the particle mean diameter,  $D_{gas}$  is the gas-  
41 phase diffusivity and  $\bar{F}_{FS}$  is the correction to the mass transfer flux due to noncontinuum effects and  
42 imperfect accommodation given in the following equation:

43 
$$\bar{F}_{FS} = \frac{0.75\alpha(1 + k_n)}{k_n^2 + k_n + 0.283k_n\alpha + 0.75\alpha}$$

44 in which  $\alpha$  is the mass accommodation coefficient onto particles, for which the value of 0.002 was  
45 adopted in this study, and  $k_n$  is the Knudsen number, defined as:

46 
$$k_n = \lambda/R_p$$

47 in which  $\lambda$  is the gas mean free path, which could be calculated as following equation:

48 
$$\lambda = \frac{3D_{gas}}{\bar{c}}$$

49 In our study, the SA yields were underestimated by a factor of 1.97–2.82 fold when considering  
50 the ratio of these two timescales (i.e.,  $\bar{\tau}_{g-p}/\tau_{g-w}$ ), which showed a decreasing trend with increasing SO<sub>2</sub>  
51 and NH<sub>3</sub> initial concentrations, suggesting that an increasing proportion of vapors is partitioned onto  
52 the suspended particle surface rather than the chamber wall. Meanwhile, the wall loss of sulfuric acid  
53 gas was also considered using this ratio (i.e.,  $\bar{\tau}_{g-p}/\tau_{g-w}$ ) to correct the sink of sulfur species.

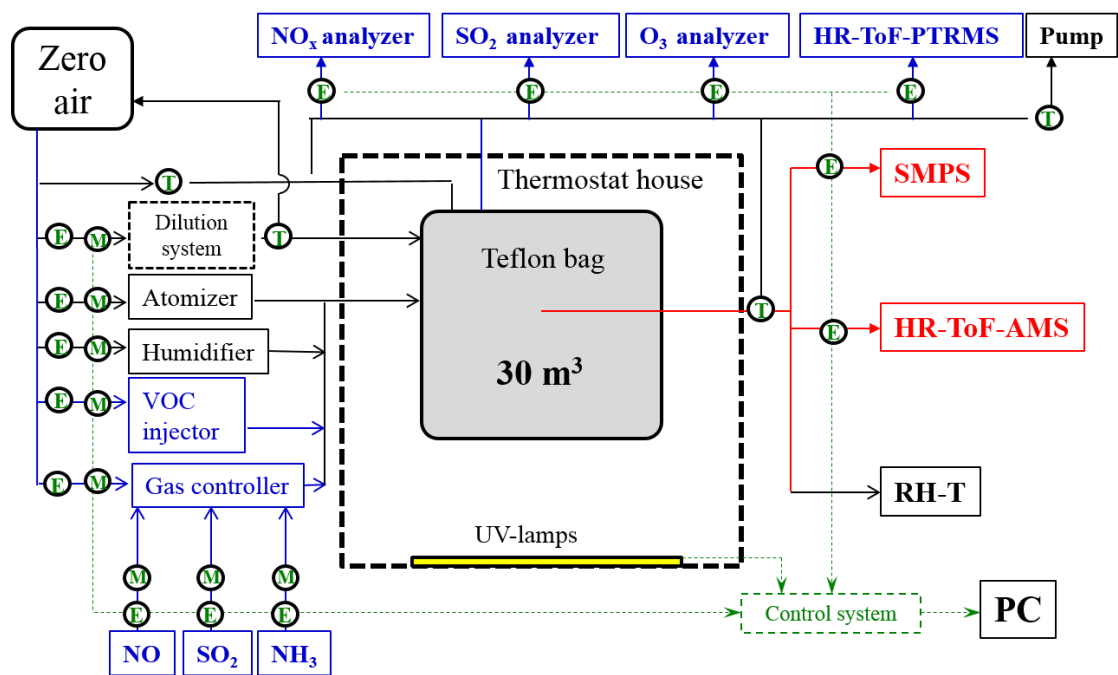
## 54 **S2. Positive matrix factorization (PMF)**

55 Positive Matrix Factorization (PMF) (Paatero, 1997; Paatero and Tapper, 1994) is a receptor model

56 and multivariate factor analysis tool that decomposes a matrix of speciated sample data into two matrices,  
57 namely factor contributions and factor profiles. In recent years, the PMF model was used for the analysis  
58 of high-resolution (HR) mass spectra data which can provide better separation of different organic  
59 components (Liu et al., 2014). This model was expressed as a bilinear factor model, namely,  $x_{ij} = \sum_p g_{ip} f_{pj}$   
60  $+ e_{ij}$ , where  $i$  and  $j$  refer to values of  $j$  species in  $i$  samples, respectively,  $p$  is the number of factors in the  
61 solution, and used a least-squares fitting process, minimizing a quality of fit parameter. In our study, we  
62 used the PMF software together with a modified version of the CU AMS PMF Execute Calcs Tool v  
63 2.06, which was developed by Ulbrich et al. (2009), to analyze the HR mass spectra ( $m/z$  12 – 170)  
64 (Zhang et al., 2011). The data and noise matrices input into the PMF analysis were generated from the  
65 PIKA version 1.15D. Ions were classified and down-weighted according to the signal-to-noise ratios  
66 (SNR).  $0.2 < \text{SNR} < 2$  was classified as the weak ions and down-weighted by a factor of 2,  $\text{SNR} < 0.2$  was  
67 bad ions and removed from the analysis and noise values of  $\text{CO}_2^+$ -related peaks at  $m/z$  16 (O), 17 (HO),  
68 18 ( $\text{H}_2\text{O}$ ), 28 (CO), and 44 ( $\text{CO}_2$ ) were down-weighted.

Table S1. The volume fraction of detected compounds for gasoline utilized in this study.

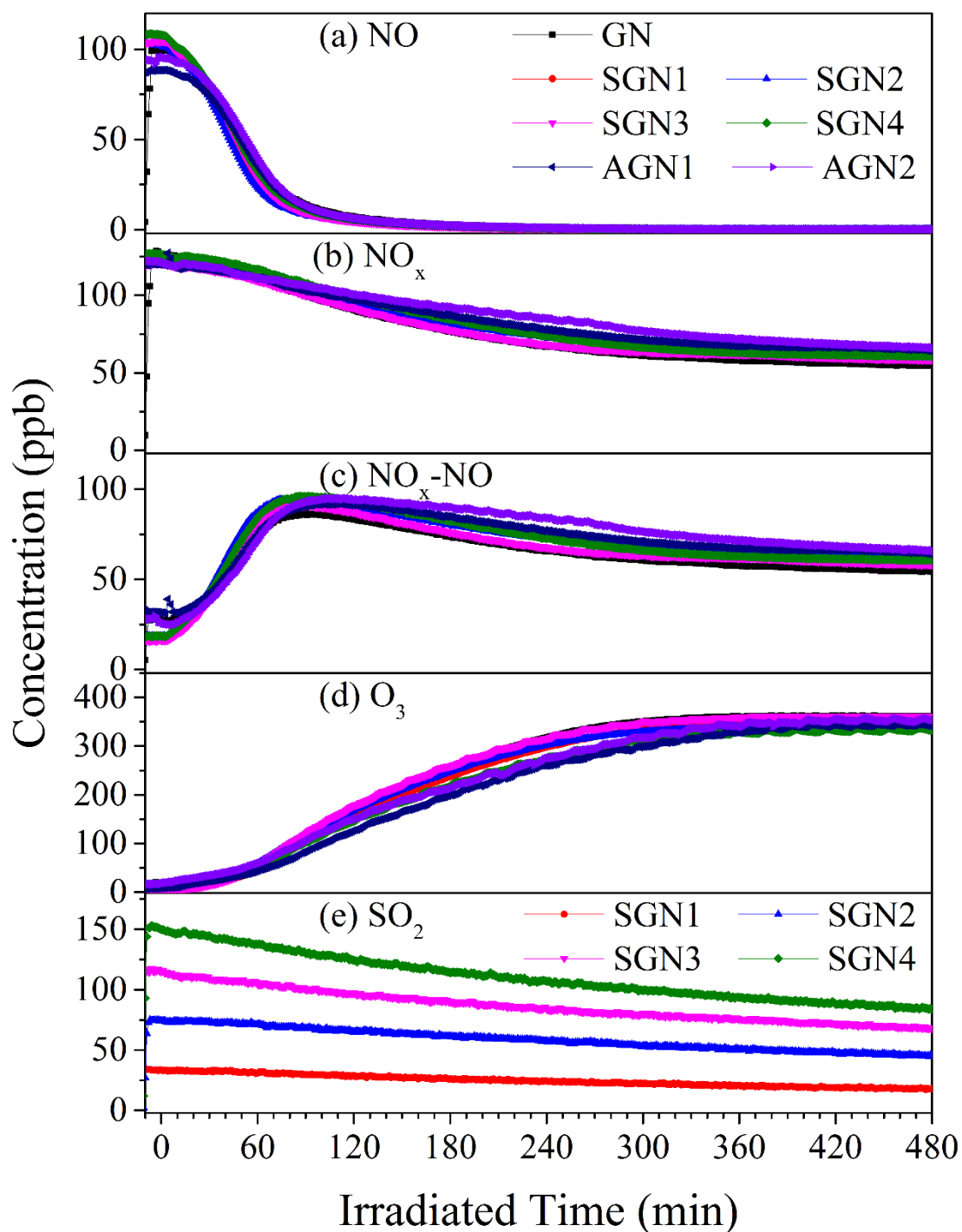
Compounds	Volume Fraction (v/v %)	Compounds	Volume Fraction (v/v %)
1,3-Butadiene	10.67	n-Octane	1.71
1-Pentene	0.00	p-Xylene and m-Xylene	2.28
trans-2-Pentene	0.06	Ethylbenzene	1.82
cis-2-Pentene	0.06	Nonane	0.75
Isoprene	1.33	o-Xylene	1.09
2,2-Dimethylbutane	1.11	Styrene	0.00
2,3-Dimethylbutane	7.74	Isopropylbenzene	0.30
2-Methylpentane	7.83	n-Propylbenzene	2.11
3-Methylpentane	5.63	1,3,5-Trimethylbenzene	0.93
1-Hexene	0.00	m-Ethyltoluene	0.93
n-Hexane	9.89	p-Ethyltoluene	0.93
2,4-Dimethylpentane	2.42	n-Decane	0.00
Methylcyclopentane	3.70	o-Ethyltoluene	0.60
Cyclohexane	1.91	1,2,4-Trimethylbenzene	5.12
2-Methylhexane	2.18	1,2,3-Trimethylbenzene	0.92
3-Methylhexane	2.62	m-Diethylbenzene	0.17
2,3-Dimethylpentane	2.53	p-Diethylbenzene	0.17
Benzene	0.58	n-Undecane	0.00
2,2,4-Trimethylpentane	3.87	n-Dodecane	0.83
n-Heptane	5.12		
Methylcyclohexane	2.43		
2,3,4-Trimethylpentane	1.20		
2-Methylheptane	0.62		
3-Methylheptane	0.59		
Toluene	4.90		



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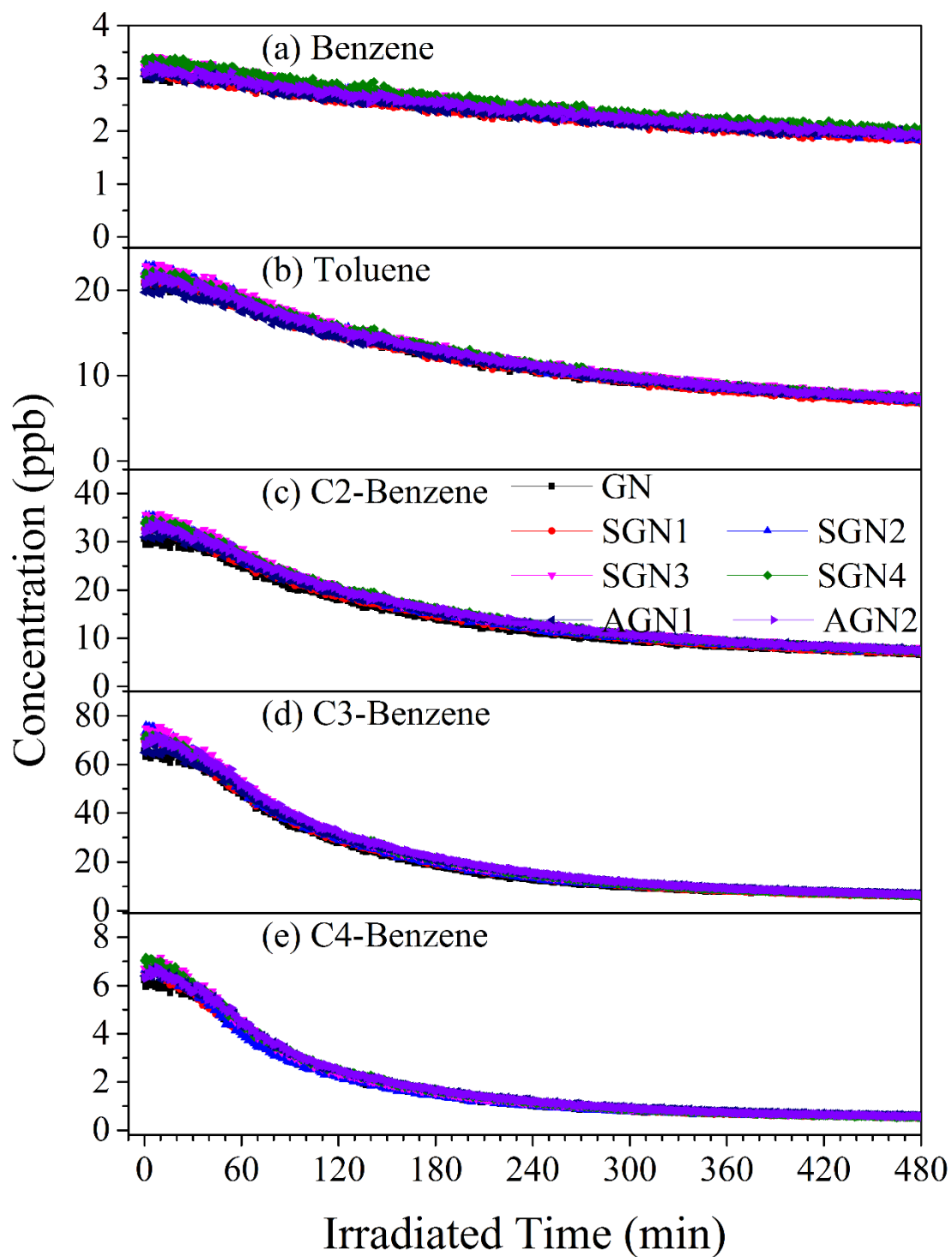
72 Fig. S1. Schematic of the RCEES-CAS smog chamber facility. E: Electromagnetic valve; T: Three-way valve. M:

73 Mass flow controller.



74

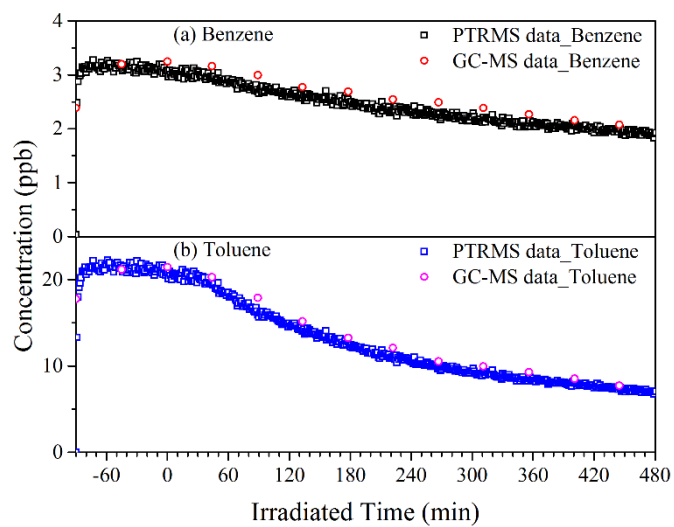
75 Fig. S2. Time variations of inorganic gas-phase species (a) NO, (b) NO<sub>x</sub>, (c) NO<sub>x</sub>-NO, (d) O<sub>3</sub>, and (e) SO<sub>2</sub> in photo-  
 76 oxidation of gasoline/NO<sub>x</sub> in the presence or absence of SO<sub>2</sub> and NH<sub>3</sub>. Letters in abbreviations represent the reactants  
 77 introduced into the chamber reactor, i.e., “G” represents gasoline, “N” represents nitrogen oxides, “S” represents  
 78 sulfur dioxide, “A” represents ammonia.



79

80 Fig. S3. Time variations of organic gas-phase species (a) Benzene, (b) Toluene, (c) C2-Benzene, (d) C3-Benzene,  
 81 and (e) C4-Benzene in photo-oxidation of gasoline/NO<sub>x</sub> in the presence or absence of SO<sub>2</sub> and NH<sub>3</sub>. Letters in  
 82 abbreviations represent the reactants introduced into the chamber reactor, i.e., “G” represents gasoline, “N”  
 83 represents nitrogen oxides, “S” represents sulfur dioxide, “A” represents ammonia.

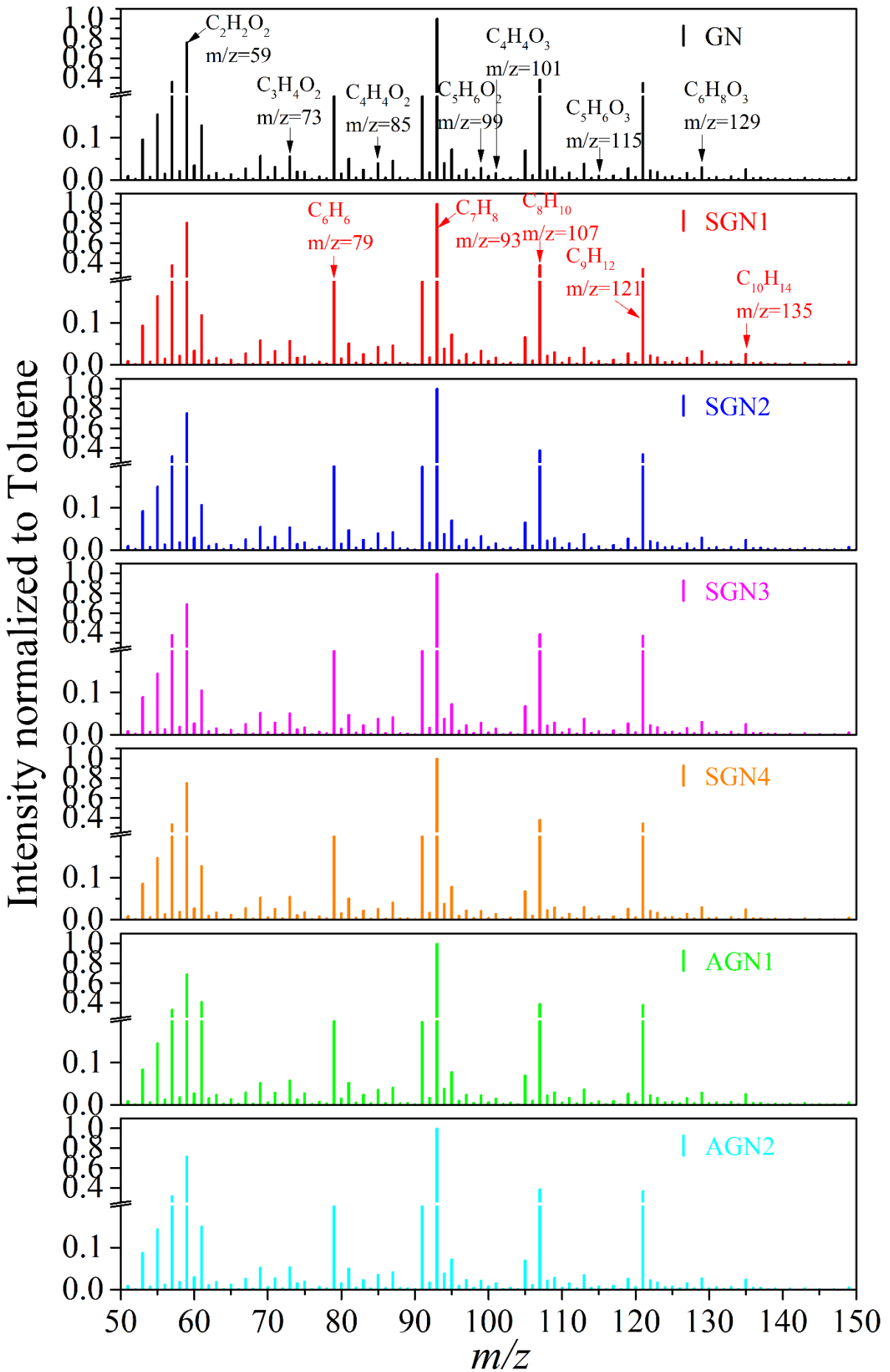




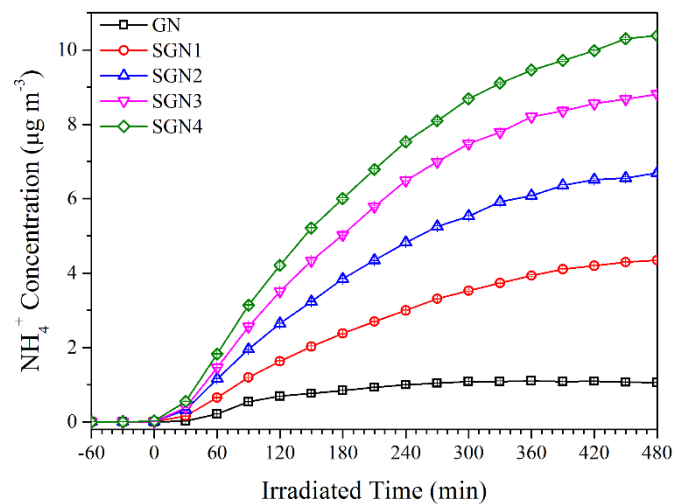
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85 Fig. S4. Time variations of (a) Benzene and (b) Toluene measured by HR-ToF-PTRMS and GC-MS during a typical chamber

86 experiment (experiment GN).



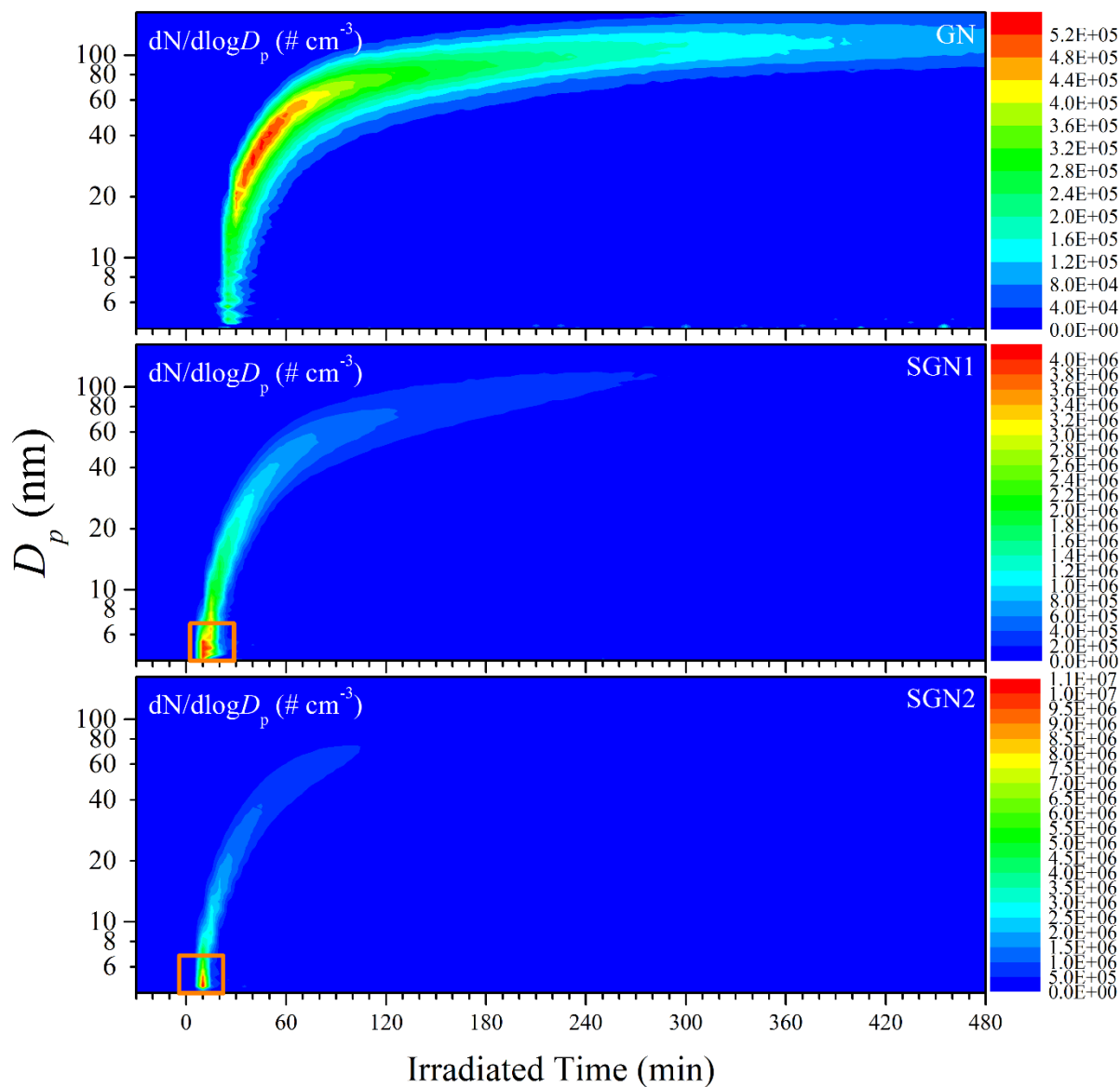
88 Fig. S5. Comparison of the mass spectrum of gas-phase species measured by HR-ToF-PTRMS after 480 min of the photo-  
89 oxidation reaction at different concentrations of SO<sub>2</sub> or NH<sub>3</sub>. Each bar is represented as an intensity normalized to  $m/z$  93 (i.e.,  
90 protonated toluene, C<sub>7</sub>H<sub>9</sub><sup>+</sup>), which had the most abundant intensity in the gasoline vapor. The mass peaks at  $m/z$  59, 73, 85, 99,  
91 101, 115, and 129 were tentatively assigned to the protonated ions of C<sub>2</sub>H<sub>2</sub>O<sub>2</sub> (glyoxal), C<sub>3</sub>H<sub>4</sub>O<sub>2</sub> (methylglyoxal), C<sub>4</sub>H<sub>4</sub>O<sub>2</sub>  
92 (butenedial), C<sub>5</sub>H<sub>6</sub>O<sub>2</sub> (4-oxo-2-pentenal), C<sub>4</sub>H<sub>4</sub>O<sub>3</sub> (2,3-epoxybutandial), C<sub>5</sub>H<sub>6</sub>O<sub>3</sub> (2-methyl-2,3-epoxybutandial), and C<sub>6</sub>H<sub>8</sub>O<sub>3</sub>  
93 (2,3-epoxy-1,4-dicarbonyl), respectively. And  $m/z$  79, 93, 107, 121, and 135 were assigned to the protonated ions of benzene,  
94 toluene, C2-benzene, C3-benzene, and C4-benzene, respectively.



95

96 Fig. S6. Time series of the ammonium aerosol formed during the photo-oxidation experiments with different  $\text{SO}_2$

97 concentrations without adding additional gaseous  $\text{NH}_3$  (i.e., GN, SGN1, SGN2, SGN3 and SGN4 listed in Table S2).

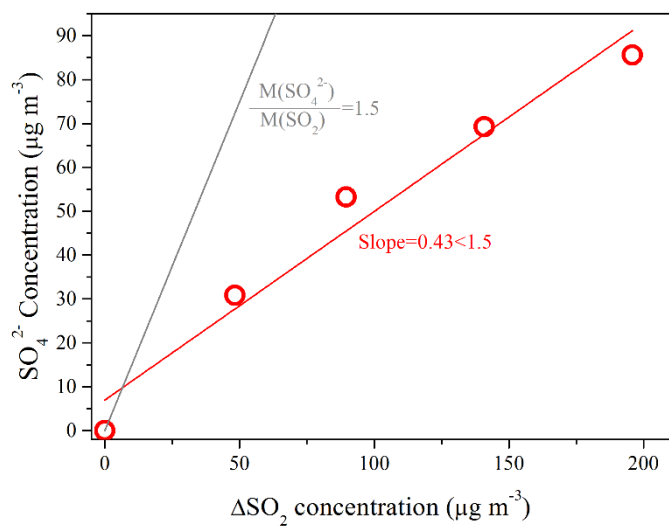


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99 Fig. S7. Time series of the smaller size distributions (4–160 nm) derived from SMPS equipped with a nanometer differential

100 mobility analyzer (Nano-DMA) for the generated secondary aerosol during the photo-oxidation experiments with different

101 SO<sub>2</sub> concentrations.

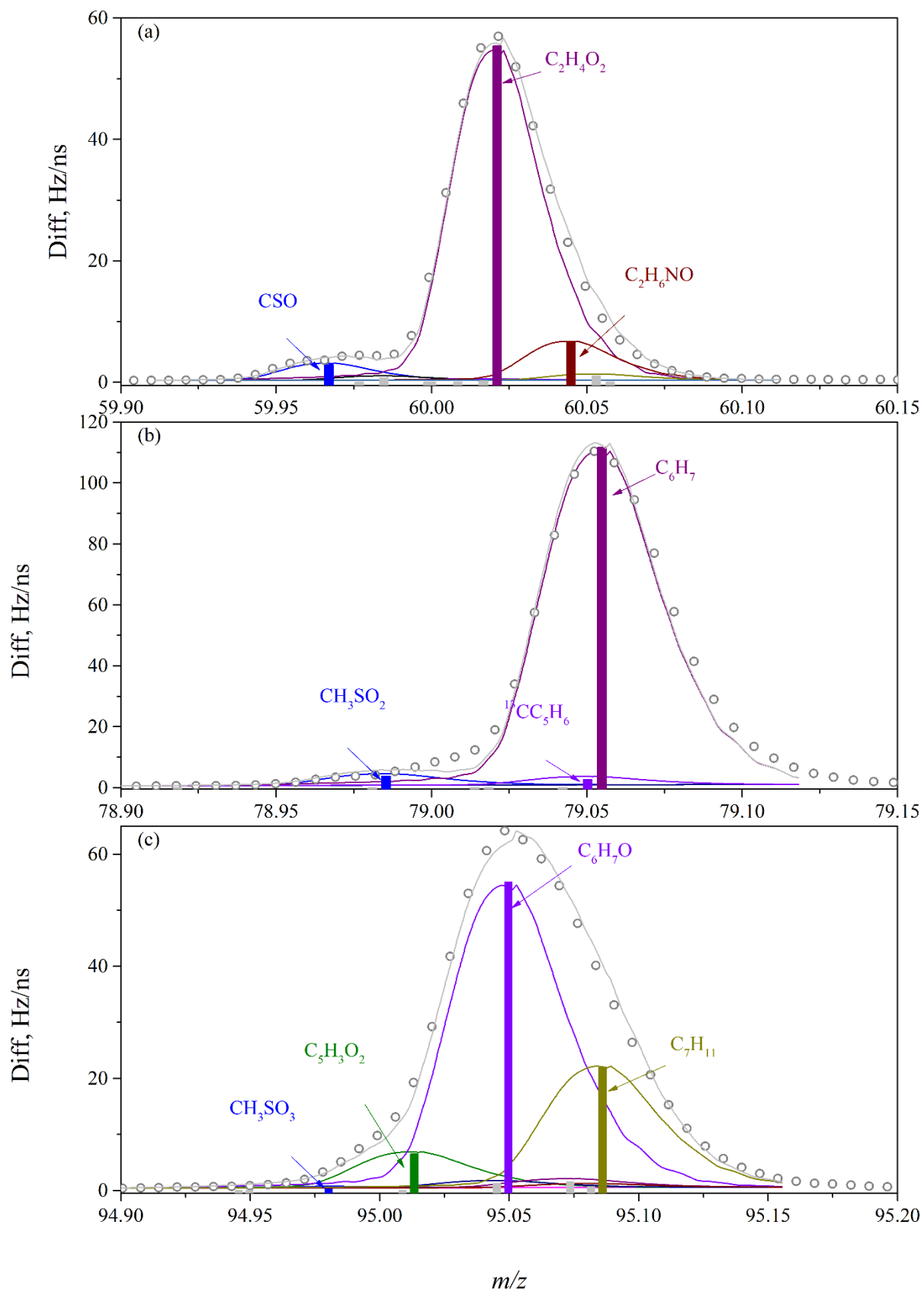


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103 Fig. S8. Amounts of consumed  $\text{SO}_2$  as a function of formed  $\text{SO}_4^{2-}$  under different  $\text{SO}_2$  initial concentrations conditions. The

104 red line is a linear fitting of all the corresponding data points.  $M(\text{SO}_4^{2-})$  and  $M(\text{SO}_2)$  represent the molecular weight of  $\text{SO}_4^{2-}$

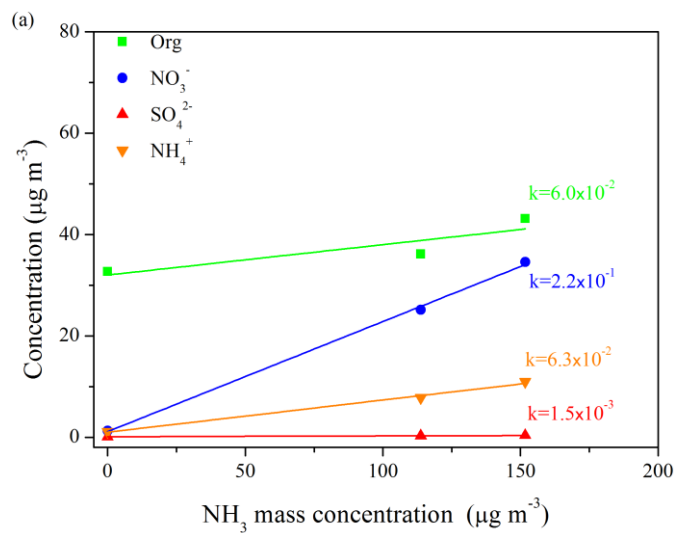
105 and  $\text{SO}_2$ , respectively, and the ratio of them is 1.5.



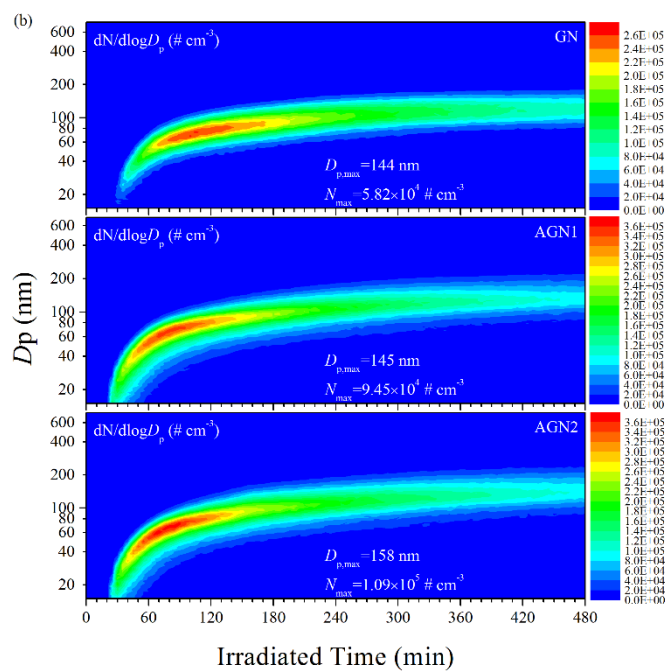
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107 Fig. S9. Fitted peaks of average W-mode mass spectrum of organosulfur compounds (OS), (a)  $\text{CSO}^+$ , (b)  $\text{CH}_3\text{SO}_2^+$ , (c)

108  $\text{CH}_3\text{SO}_3^+$ .

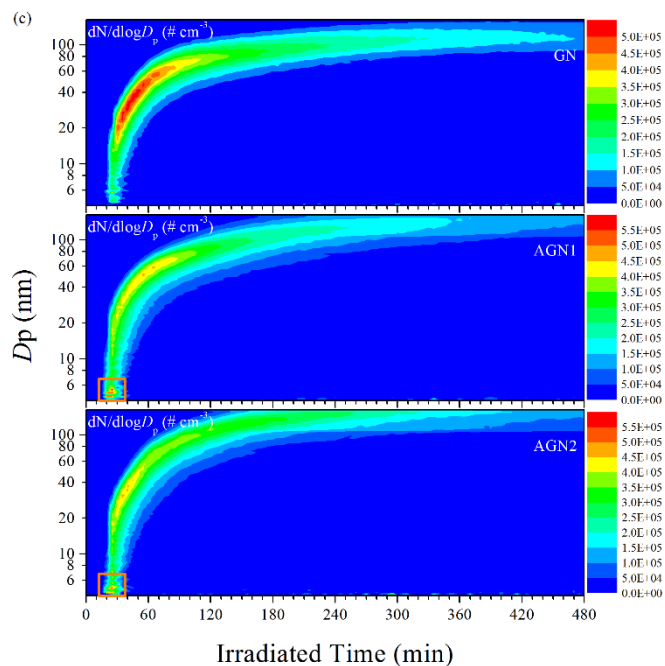


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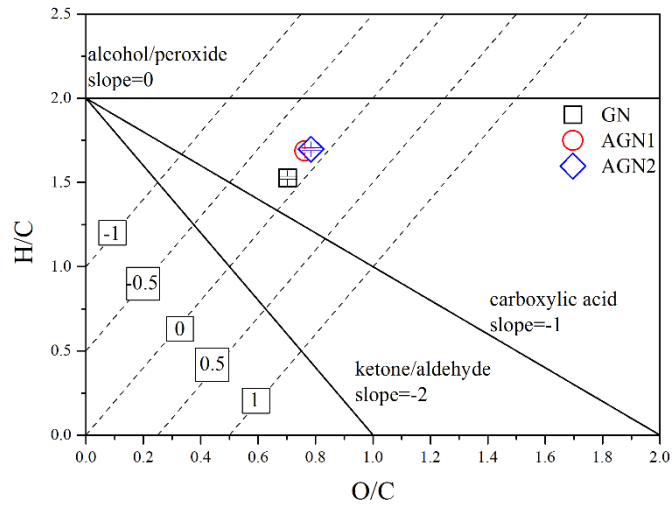


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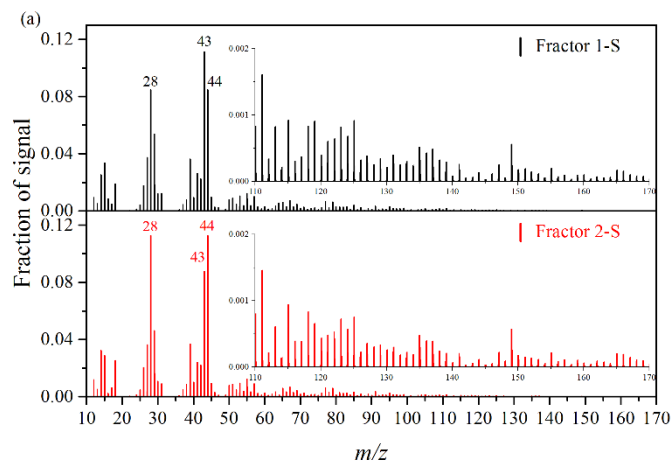
111  
 112 Fig. S10. (a) Linear relationship between the concentration of chemical species and  $\text{NH}_3$  under different  $\text{NH}_3$  initial  
 113 concentration conditions. Each line (green (organic), blue (nitrate), red (sulfate), and orange (ammonium)) represents a linear  
 114 fitting and the  $k$  values are the corresponding slopes for each chemical species. (b) Time series of the size distributions (20–700  
 115 nm) for the secondary aerosol generated during the photo-oxidation experiments with different  $\text{NH}_3$  concentrations.  $D_{p,\text{max}}$  and  
 116  $N_{\text{max}}$  represent the maximal diameter and number concentration of generated secondary aerosol, respectively, during each  
 117 photo-oxidation experiment. (c) Time series of the smaller size distributions (4–160 nm) derived from SMPS equipped with a  
 118 nanometer differential mobility analyzer (Nano-DMA) for the generated secondary aerosol during the photo-oxidation  
 119 experiments with different  $\text{NH}_3$  concentrations.



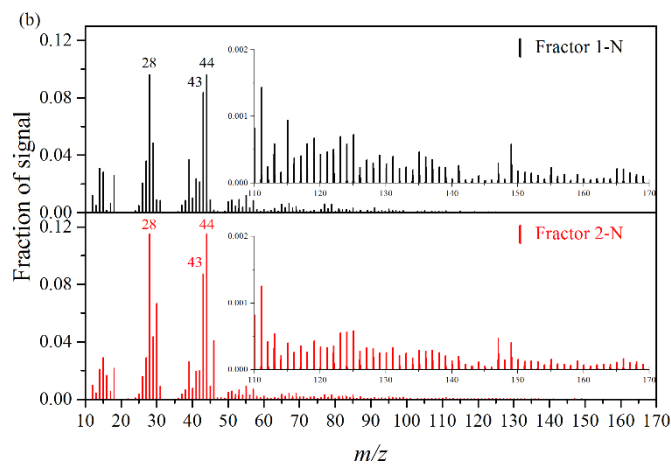
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121 Fig. S11. Average O/C and H/C in SOA formed from the photo-oxidation of gasoline vapor at different concentrations of NH<sub>3</sub>

122 (Exps. GN, AGN1 and AGN2).



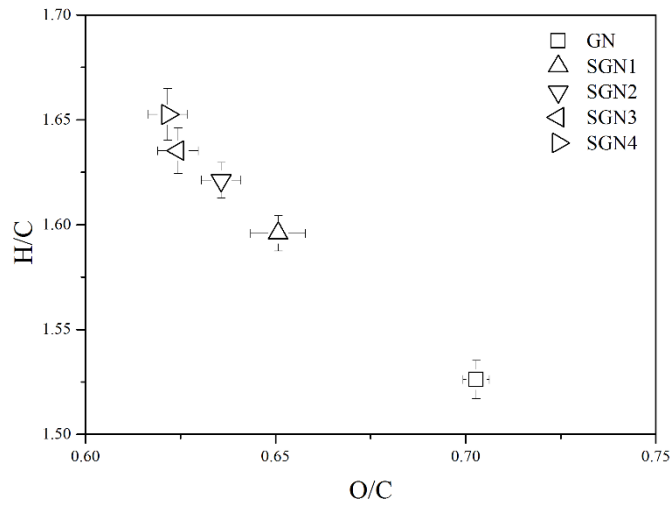
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125 Fig. S12. Mass spectra of the two factors identified from the PMF analysis to the AMS data derived from the experiments at

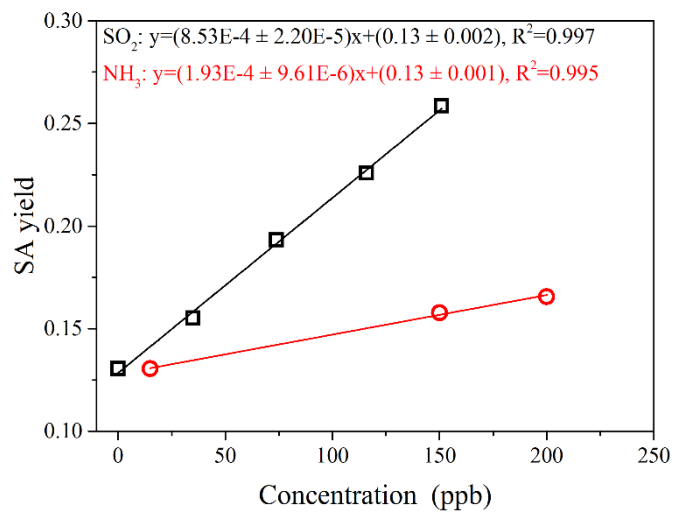
126 different concentrations of (a) SO<sub>2</sub> (Exp. GN, SGN1, SGN2, SGN3 and SGN4) and (b) NH<sub>3</sub> (Exp. GN, AGN1 and AGN2).



127

128 Fig. S13. Average O/C and H/C in SOA formed from the photo-oxidation of gasoline vapor at different concentrations of SO<sub>2</sub>

129 (Exp. GN, SGN1, SGN2, SGN3 and SGN4).



130

131 Fig. S14. Linear relationship between the concentration of SO<sub>2</sub> (or NH<sub>3</sub>) and the SA yield.

132 **References**

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