

# H<sub>2</sub>SO<sub>4</sub> and particle production in a Photolytic Flow Reactor. Chemical modeling, cluster thermodynamics and contamination issues

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10 **Abstract.** Size distributions of particles formed from sulfuric acid (H<sub>2</sub>SO<sub>4</sub>) and water vapor in a Photolytic Flow Reactor (PhoFR) were measured with a nano-particle mobility sizing system. Experiments with added ammonia and dimethylamine were also performed. H<sub>2</sub>SO<sub>4(g)</sub> was synthesized from HONO, sulfur dioxide, and water vapor, initiating OH oxidation by HONO photolysis. Experiments were performed at 296 K over a range of sulfuric acid production levels and for 16 to 82 % relative humidity. Measured distributions generally had a large particle mode that was roughly log-normal; mean diameters  
15 ranged from 3 to 12 nm and widths (lnσ) were ~0.3. Particle formation conditions were stable over many months. Addition of single-digit pmol/mol mixing ratios of dimethylamine led to very large increases in particle number density. Particles produced with ammonia, even at 2000 pmol/mol, showed that NH<sub>3</sub> is a much less effective nucleator than dimethylamine. A two-dimensional simulation of particle formation in PhoFR is also presented that starts with gas-phase photolytic production of H<sub>2</sub>SO<sub>4</sub> followed by kinetic formation of molecular clusters and their decomposition determined by their thermodynamics.  
20 Comparisons with model predictions of the experimental results dependency on HONO and water vapor concentrations yield phenomenological cluster thermodynamics and help delineate the effects of potential contaminants. The added-base simulations and experimental results provide support for previously published dimethylamine-H<sub>2</sub>SO<sub>4</sub> cluster thermodynamics and provide a phenomenological set of ammonia-sulfuric acid thermodynamics.

## 1 Introduction

25 Particle formation in the atmosphere has long been studied (McMurry et al. 2005; Kulmala et al. 2004) to ascertain potential impacts on health (Nel 2005) and on climate processes (IPCC 2013). For example, nano-particles (characterized as < 10 nm in diameter) can have special health effects as their small size allows for efficient transport into lung tissue (Kreyling et al. 2006). They also influence climate by growing to sizes large enough to affect radiative forcing and the properties of clouds. Despite numerous and wide-ranging studies devoted to understanding new particle formation,  
30 mechanisms and nucleation rates applicable to many regions of the atmosphere remain uncertain.

Sulfuric acid-driven nucleation is a prime source of nanoparticles in the atmosphere (Kuang et al. 2012; Sipilä et al. 2010) thus it is the starting point for many laboratory studies. Previous work on particle nucleation in the binary (water-sulfuric acid) system (Kirkby et al. 2011; Ball et al. 1999; Zollner et al. 2012; Ehrhart et al. 2016; Yu et al. 2017) have concluded that binary nucleation can be significant at low temperatures such as at high latitudes and in the upper  
5 troposphere. The sulfuric acid/water binary system also serves as an important baseline diagnostic for comparing experimental results. Finally, nanoparticle growth by sulfuric acid and water vapors is of interest as well as uptake of oxidized organic compounds by acidic nanoparticles. Good knowledge of the formation and stability of binary nanoparticles is needed to understand their subsequent growth via other compounds.

Previous laboratory studies of nucleation in the binary system diverge widely, especially for results taken at or near  
10 room-temperature, suggesting experimental details may significantly affect results. For example, does it matter if H<sub>2</sub>SO<sub>4</sub> is provided by a bulk or a photolytic source? Does the type of photolytic precursor- O<sub>3</sub>, H<sub>2</sub>O<sub>2</sub>, H<sub>2</sub>O, etc.-matter? (Sipilä et al. 2010; Berndt et al. 2008; Laaksonen et al. 2008) The CLOUD experimental results at 278 K and below (Kürten et al. 2016; Ehrhart et al. 2015) has alleviated some of these concerns yet room temperature results can provide more stringent tests due to a greater sensitivity to thermodynamics. Other issues include (i) limitations imposed by particle detector characteristics as  
15 well as cluster/particle wall losses (McMurry 1983; Kürten et al. 2015; 2018) and (ii) determining the concentration of H<sub>2</sub>SO<sub>4</sub> (Sipilä et al. 2010; Kürten et al. 2012; Young et al. 2008) which is typically uncertain to a factor of two (Eisele and Tanner, 1993), although higher accuracies ( $\pm 33\%$ , Kürten et al. 2012) can be achieved. These experimental challenges can significantly influence results and their interpretation yet these largely known issues can be addressed to some degree.

Contaminants are the biggest unknown factor in these types of experiments and it is important to ascertain whether they  
20 are present at levels that can influence particle formation rates. If the contaminant is an amine, even a very low abundance can be a point of concern. For example, Zollner et al. (2012) argued that a  $10^{-14}$  mixing ratio of methylamine could have affected their binary system measurements. Glasoe et al. (2015) presented data from the same apparatus as Zollner et al. and they carried this argument further and estimated that contaminant dimethylamine mixing ratios during their binary system measurements were less than or equal to  $10^{-15}$ . If the contaminant is NH<sub>3</sub>, however, it likely needs to reach the single-digit  
25 pmol/mol (pptv) level or higher to significantly interfere with measurements in the binary system at room temperature. Kirkby et al. (2011) and more recently Kürten et al. (2016) estimate ammonia contaminant levels of 4-to-10 pptv NH<sub>3</sub> for their experiments performed at 292 - 298 K; it is not clear if this level of ammonia had a significant effect on their results. Recently, Yu et al. (2017) reported upper limits for NH<sub>3</sub> and dimethylamine of 23 and 0.5 pptv, respectively, for their putative base-free nucleation experiments. Yet their nucleation rates are not extreme outliers, suggesting that their  
30 dimethylamine level was probably much lower than 0.5 pptv. Nonetheless, uncertainty introduced by undetectable (at the current state-of-the-art) levels of contaminants underscores the need for multiple approaches for studying sulfuric acid nucleation.

Here we describe an apparatus and results from experiments on the formation of sulfuric acid nanoparticles from photolytically-generated sulfuric acid vapor via OH+SO<sub>2</sub> photochemistry initiated with HONO photolysis at ~350-to-370

nm. Although nitrous acid is considered an important contributor to OH radical formation in many situations (Sörgel et al. 2011), little has been done to understand its photolysis that leads to sulfuric acid formation and new particle formation. We also studied the effects of adding ammonia or dimethylamine; both are known to greatly enhance particle production rates (Almeida et al. 2013; Glasoe et al. 2015; Yu et al. 2012; Ortega et al. 2012; Nadykto and Yu 2011). We present  
5 experimental results where temporary contamination of the apparatus was evident yet long-term results indicate a relatively constant level of cleanliness in the experiment. The experimental results are compared to simulations of the flow reactor that couple the flow with photo-chemical kinetics and an acid-base particle formation scheme. In addition to providing H<sub>2</sub>SO<sub>4</sub> concentrations, the model results and their comparison to experimental particle characteristics has led to phenomenological cluster free energies for the ammonia-sulfuric acid system at 52 % relative humidity. Finally, we present a compendium of  
10 results from photolytic particle formation experiments near room temperature.

## 2 Methods

The Photolytic Flow Reactor (PhoFR) is a vertically-aligned cylindrical glass tube with an inner diameter of 5.0 cm, a length of ~130 cm, a volume of approximately 2.5 L and topped with a 23 cm long conical glass piece with several flow inlets (Fig. 1a). In the course of this work, a Teflon screen was positioned between the cone and the flow reactor to calm the  
15 jetting from the inlets. A ~ 105 cm length of PhoFR is jacketed and kept at a constant temperature, typically 296 K, by circulation of thermostated water. The main flow of gas was nitrogen from a liquid nitrogen gas-pack and the total flow rate was 2.9 sLpm (standard L / min, 273 K and 1 atm). The flow contained small amounts of SO<sub>2</sub> and HONO, typically 16 and 0.02 μmol/mol (ppmv), respectively, and up to several % water vapor; relative humidity was set by sending a portion of the flow over a heated water reservoir and then through a thermostated, vertically-aligned tube that removed excess water vapor.  
20 Total pressure was slightly above ambient, ~ 0.98 atm: gauge pressure was monitored continuously and it was typically 0.001 atm. The oxygen level from the liquid nitrogen, stated to be 10 ppmv or less, was apparently sufficient for the subsequent oxidation chemistry - noting little differences in particle size distributions upon adding several % O<sub>2</sub> to the flow. For all liquid nitrogen cylinder change-overs, the high pressure side of the regulator is flushed several times before exposing the lines to the new supply of gas - a standard procedure used by Ball et al., Zollner et al. and Glasoe et al. Also keeping in  
25 line with that past work, filters have not been used on any gas-supply lines.

Entering gas flows were monitored and set by mass flow meters under computer control. Typical flows for baseline conditions in sLpm or sccm (standard cm<sup>3</sup> / min, 273 K, 1 atm) were dry gas at 1.4 sLpm, fully humidified air at 1.5 sLpm, HONO-laden (~15 ppmv) N<sub>2</sub> flow at 4.2 sccm, and SO<sub>2</sub>-laden flow at 32 sccm (1500 ppmv SO<sub>2</sub>-in-N<sub>2</sub>). These baseline conditions help diagnose the long term stability of the system. The baseline number densities of SO<sub>2</sub> and HONO in the flow  
30 reactor (accounting for dynamic dilution) are 4x10<sup>14</sup> and 5.2x10<sup>11</sup> cm<sup>-3</sup>, respectively. Three sections were not insulated or thermo-regulated: (i) the conical top section, (ii) the top 10 cm of the flow reactor where the base-addition port resides, and

(iii) the bottom 20 cm where aerosol was sampled. The fully humidified line and the port where it enters the cone were gently heated (298-300 K) to eliminate condensation when room temperature was less than 296 K.

The SO<sub>2</sub>-in N<sub>2</sub> mixture (Minneapolis Oxygen) was reported (Liquid Technologies Corporation, EPA Protocol) to contain 1500 ppmv SO<sub>2</sub> +/- 10%. Water vapor was taken from a gently heated ~500 mL volume of deionized water (Millipore) that also contained a few grams of concentrated sulfuric acid to suppress potential base contamination from the bulk water. This humidified flow then passed through 80 cm of vertically-aligned Teflon tubing (~6.2 mm ID) held at the temperature of the flow reactor.

Photolyte HONO was continuously produced (Febo et al. 1995) by flowing nitrogen laden with ~15 ppmv HCl vapor into a small (25 mL) round-bottom flask containing 1-2 grams of powdered NaONO(s), held at 40-50°C (Fig. 1b). HONO vapor and co-product NaCl(s) are produced in a classic double-displacement reaction. The powder could be very slowly mixed with a small (1 cm long) stir bar and results generally did not depend on whether the powder was stirred. Periodic gentle shaking of the flask usually led to only temporary changes in particle number densities.

The HONO level exiting the generator is likely to be equal to the HCl level entering it. The HCl-generator and a water vapor pre-saturator were temperature-controlled at typically 20 °C. A saturated (~6 m, molal) NaCl aqueous solution in the pre-saturator yields a relative humidity of 76 % in the flow: a stable amount of water vapor stabilizes the solution in the HCl-generator, which contains a solution with a 2-to-1 mole ratio for NaCl to H<sub>2</sub>SO<sub>4</sub>. The HCl-generator solution was prepared initially with concentrations of 3.5 m NaCl and 1.75 m H<sub>2</sub>SO<sub>4</sub> and calculations (Wexler and Clegg, 2002; Friese and Ebel, 2010) result in an HCl vapor pressure of 9.3x10<sup>-6</sup> atm. UV absorption measurements to determine the HONO level in this flow are described in the Supplement (S5.1) and results indicate that the source has a HONO level of about 1.5x10<sup>-5</sup> atm. This suggests that the HCl-generator's HCl vapor pressure is slightly larger than the calculated value. While the water vapor pre-saturator minimized loss of water from the HCl-generator, small temperature differences between these two vessels can introduce variability and possibly a bias.

Four black lights that have a UVA spectral irradiance centered at 360 nm illuminated about a 115 cm length of the jacketed flow reactor from a distance of about 15 cm from the reactor center. An estimate of the fluence (5x10<sup>15</sup> photon cm<sup>-2</sup> s<sup>-1</sup>) indicates a photolysis rate coefficient of approximately 10<sup>-3</sup> s<sup>-1</sup> for HONO. Described in the Supplement (S5.2) are experiments where production of methylvinylketone and methacrolein from the oxidation of isoprene were monitored, yielding (together with the 15 ppmv HONO level in the source flow) a HONO photolysis rate coefficient of 8x10<sup>-4</sup> s<sup>-1</sup>.

H<sub>2</sub>SO<sub>4</sub> is formed via (i) OH produced via HONO photolysis, (ii) OH addition to SO<sub>2</sub>, (iii) H-atom abstraction by O<sub>2</sub> and (iv) reaction of SO<sub>3</sub> with H<sub>2</sub>O molecules (Lovejoy et al., 1996). The HO<sub>2</sub> and NO radicals generated in this process can react together and generate an additional OH radical. When SO<sub>2</sub> is present at a few ppmv, the dominant loss for OH is OH + SO<sub>2</sub>: a pseudo-first-order loss rate coefficient is given by [SO<sub>2</sub>]\*k<sub>OH+SO<sub>2</sub></sub> = 4x10<sup>14</sup> cm<sup>-3</sup> \* 8.9x10<sup>-13</sup> cm<sup>3</sup>s<sup>-1</sup> = 360 s<sup>-1</sup>. With this SO<sub>2</sub> baseline level, OH reacts with HONO for typical conditions only about 1 % of the time: the OH first-order loss rate coefficient is ~3 s<sup>-1</sup>, from [HONO]\*k<sub>OH+HONO</sub> = 5x10<sup>11</sup> cm<sup>-3</sup> \* 6x10<sup>-12</sup> cm<sup>3</sup>s<sup>-1</sup>. Yet at low SO<sub>2</sub> levels, loss of OH due to reaction with HONO can be significant.

H<sub>2</sub>SO<sub>4</sub> levels build as the flow moves down the reactor, forming H<sub>2</sub>SO<sub>4</sub> molecular clusters and these clusters grow into stable particles. These particles accumulate enough material, primarily H<sub>2</sub>SO<sub>4</sub> and H<sub>2</sub>O, to grow to several nm in diameter. Growth due to OH or HO<sub>2</sub> uptake followed by reaction with absorbed SO<sub>2</sub> may also contribute to growth.

Particles were sampled on axis at the exit of the flow reactor, about 120 cm from the conical inlet, with a custom-built mobility-sizing and counter system designed for nanometer-sized particles. Briefly, size-classified particles (Am-241 charger and a TSI 3085 nanoDMA) were detected with a diethyleneglycol (DEG), sheathed condensation particle counter (CPC) in tandem with a butanol-based CPC (Jiang et al. 2011). This system is denoted ‘DEG system’ in this study. The DEG CPC was operated with a saturator temperature of 57°C, a condenser temperature of 20°C, 0.36 L/min condenser flow and 0.07 L/min capillary flow. The nanoDMA was operated with 2 L/min aerosol-in and monodispersed-out flows and a 13 L/min sheath flow, as in Glasoe et al. (2015).

For a few experiments, ammonia or dimethylamine as trace gases were added through a port at the top of the flow reactor. A discussion of their mixing into the main flow is presented in the Supplement (S7.1). Their sources were permeation tubes, and 100s or single-digit pptv levels could be set by either a single- or a double-stage, respectively, dynamic dilution system (Freshour et al. 2014; Glasoe et al. 2015). Ammonia was used in the single-dilution system and dimethylamine was dedicated for use in the double-dilution system. Permeation rates were determined periodically by re-directing the base-laden flow through an acidic solution and monitoring the change in pH over time (Freshour et al., 2014).

## 2.1 Model

The 2-dimensional model of the flow reactor incorporating the photochemical kinetics of H<sub>2</sub>SO<sub>4</sub> formation was built on a previous model of acid-base molecular cluster formation which was fully corroborated against a commercial computational fluid dynamics simulation (Hanson et al. 2017). The flow profile can be set to either plug or fully-developed laminar, the formation of clusters with up to ten H<sub>2</sub>SO<sub>4</sub> and ten base molecules can be simulated. If so desired, clusters larger than ten H<sub>2</sub>SO<sub>4</sub> molecules can be simulated using a growth-only mechanism. Note that clusters without a base molecule represent a weighted average of the binary H<sub>2</sub>SO<sub>4</sub>-H<sub>2</sub>O thermodynamics for a given relative humidity. The detailed photochemistry in our experiment includes the production of OH, its reactions with SO<sub>2</sub> as well as with HO<sub>2</sub>, NO, NO<sub>2</sub>, HONO, HNO<sub>3</sub>, H<sub>2</sub>O<sub>2</sub> etc. The rate coefficients and mechanisms are presented in the Supplement (S7, Table S1). The acid and base species and all molecular clusters as well as OH are lost to the walls limited only by diffusion.

The model reacts, convects and diffuses all reactants and products and yields the abundance of H<sub>2</sub>SO<sub>4</sub> and its molecular clusters, the largest clusters are then correlated to the abundance of experimentally determined particles (Panta et al. 2012; Hanson et al. 2017). Coagulation was not implemented, because cluster-cluster interactions are not significant for most of the conditions of the present work. Water molecules are not explicitly tracked but hydration is taken into when calculating the collisional rate coefficient and the size of the clusters, assuming bulk properties. Increases in computational times can be significant when large clusters are simulated using the growth-only mode, e.g. a factor of eight for adding clusters up to 250 H<sub>2</sub>SO<sub>4</sub> molecules compared to stopping growth at the 10 acid, 3 base cluster. Yet it is desirable to simulate very large

clusters via uptake of  $\text{H}_2\text{SO}_4$  assuming no loss to compare results to measured size distributions. Further analysis of cluster growth and loss processes, including growth-only for clusters larger than 10  $\text{H}_2\text{SO}_4$  molecules, is presented in the Supplement (S1.3).

Ammonia or dimethyl amine could be included at a trace level with the flow entering the simulated reactor whereupon acid-base clustering and particle formation commence (note that base is lost to the wall, limited by diffusion). The model assumes rapid mixing of base into the main flow. Justification for this is presented in the Supplement (S7.1). The photochemistry is described in detail in the Supplement (S7) and the acid-base clustering reactions are described in detail in Hanson et al. (2017) along with thermodynamic schemes for clusters of the bases with sulfuric acid. Scheme DMA\_I from that work was used here while a new cluster thermodynamics scheme for the ammonia-added experiments was developed for  $\text{NH}_3\text{-H}_2\text{SO}_4$  clusters at 52 % relative humidity (see S8).

### 3 Results and Discussion

#### 3.1 Particle formation evaluation.

The stability of particle formation conditions over several months is demonstrated by presenting the number and the average size of particles for baseline conditions. In the next section, the modeled photochemistry for baseline conditions is presented to provide baseline sulfuric acid concentrations within PhoFR and we discuss how the size distributions were analyzed. In subsequent sections, these analytical devices will be applied to the results of experiments where reactant levels were varied. In the Supplement (S1.0) is a typical time series of the raw data (the count rates for each channel) and a table with the overall correction factors.

Shown in Figure 2 are (a) the total particle number density,  $N_p$ , and (b) so-called “leading-edge” (see S1.1 in the Supplement) mode diameters over a 6 month period for baseline conditions: 52 % relative humidity (RH), 296 K, total flow of 2.9 sLpm, and a flow of  $\text{N}_2$  through the HONO source,  $Q_4$ , of 4.2 sccm. The data were binned according to the flow of the  $\text{SO}_2$  mixture,  $Q_1$ , either 4 sccm or > 16 sccm. The abundance of HONO is 20 ppbv and  $\text{SO}_2$  is either 2 ppmv or > 8 ppmv. Shown in the Supplement (S1.2) are representative particle size distributions - corrected for size-dependent diffusion losses in CPC transport and inlet lines.  $N_p$  was determined by summing the particle concentrations with  $D_p$  of ~2.4 nm and larger because the two smallest diameter concentrations are the local minimum for most of the size distributions. Furthermore, these small diameter data can have large random uncertainties due to large corrections applied to low count rates. Discussed in the Supplement (S4) are possible sources of the scatter in the data.

Note the data presented as gold diamonds: these are  $N_p$  (low  $\text{SO}_2$ ) on the day of, and the day after, a gas supply cylinder change-over. This event could be due to entrainment of dust particles into the supply lines. Nothing like this happened on the five other cylinder change-overs that occurred during this time interval. What is different about this cylinder exchange is not known. The effects are temporary as a 90 % decrease in  $N_p$  occurred in a few hours, an additional 70 % drop occurred overnight and a day later  $N_p$  is within the upper range of the scatter for baseline conditions.

The measured size distributions are governed by the interplay between the spatial distribution of  $[H_2SO_4]$ , whether base is added, and the nature of potential contaminant species. For example, small- and mid-sized particles probably form somewhat downstream of the top of the reactor whereas the largest particles at the leading edge of the distributions are formed near the top of the reactor. The largest particles must originate at the top of the reactor, having the highest overall exposure to  $H_2SO_4$ . These so-called leading-edge particles are the focus of our analysis.

The leading-edge particles are greatly enhanced when base was added, whether ammonia or dimethylamine. In these cases, the leading-edge particles are prominent in the distributions and are described by log-normals (see the distributions presented below). The leading-edge volume-mean diameters for the added-base experiments are similar to those of the no-added base distributions. So we propose that the leading-edge particles are indicative of the nucleation conditions at the top of PhoFR. In the Supplement (S1.1) is more discussion of the leading-edge mode of the particle size distributions and supporting results from the simulation (S1.2: plots of modeled distributions with and without added  $NH_3$ .)

The high  $SO_2$  data (Fig. 2a) exhibits an  $N_p$  that averages about  $2 \times 10^4 \text{ cm}^{-3}$  since late February; also the leading edge of the size distributions (Fig. 2b), fit to log-normal functions, indicate mode diameters of about 6 nm with  $\ln\sigma$  values of  $\sim -0.35$ . The large drop in  $N_p$  on the 23rd of February is due to a Teflon mesh (ultrasonically cleaned and soaked overnight in a dilute sulfuric acid solution) placed between the cone and the flow reactor. The edges of the Teflon mesh fit in the gap of the glass joint without disturbing the Teflon-encapsulated o-ring. The mesh was installed because flow visualization experiments, similar to those described in Ball et al. (1999), revealed extensive back-streaming into the cone. Back-streaming can carry  $H_2SO_4$  from the illuminated section into the cone to initiate nucleation there. With the Teflon mesh in place, a trend in  $N_p$  with time cannot be discerned in Fig. 2a. Similarly, leading-edge mode diameters indicate that  $D_{le}$  is roughly constant over the time period Feb 24 to Jun 20 (Fig. 2b).

While the effects on  $N_p$  (Fig. 2a) due to the addition of the mesh are large, the effects on mode diameter are less pronounced. On the other hand, there is a five week period beginning the middle of April 2018 that has mode diameters about 1 nm larger than those during the preceding and following time periods. What was different about this time period is not known however potential changes in flow patterns and variations in room temperature are potential explanations.

Since changes in  $D_{le}$  are small or negligible, the growth conditions in PhoFR must be stable during this 5-month time period. The cumulative exposure of particles to  $H_2SO_4$  as they travel down PhoFR is constant, indicating that the UV flux and reactant concentrations are also. The overall stability in  $N_p$  during this time also indicates that the purity of the system is stable. Variations in  $N_p$  might have been influenced by changes in potential contaminants, yet the HCl source for the HONO generator is temperature-sensitive and flow patterns can be influenced by temperature variations of the non-thermoregulated sections of the flow reactor. An expected increase in cleanliness over time, due to acid building up on surfaces and binding potential base-emitting contaminants, is not exhibited in the data.

### 3.1.1 Simulated reactant distributions

Shown in Fig. 3 are simulated centerline concentrations of the gas-phase species and two molecular clusters. In order of abundance at the end of the reactor on the left axis:  $\text{H}_2\text{SO}_4$ ,  $\text{NO}_2$ ,  $\text{NO}$ ,  $\text{HO}_2$ ,  $\text{H}_2\text{O}_2$ ,  $\text{HO}_2\text{NO}_2$  and  $\text{NH}_3$ ; and on the right axis,  $\text{OH}$ ,  $(\text{H}_2\text{SO}_4)_2$  and  $10^3$  times the  $(\text{H}_2\text{SO}_4)_{10}$  cluster abundance. This simulation was performed with  $[\text{HONO}] = 5.2 \times 10^{11} \text{ cm}^{-3}$ , simulating an experiment with  $Q_4 = 4.2 \text{ sccm}$ . These conditions are close to those for the data depicted in Fig. 2 with the simulation being strictly binary nucleation.

Sulfuric acid rises steadily and reaches  $1.2 \times 10^{10} \text{ cm}^{-3}$  by the end of the lighted section that extends from 0 to 110 cm. The downstream section of the reactor with the highest sulfuric acid level is where particles achieve most of their growth: over the bottom 2/3 of PhoFR, an axial distance of 40 to 125 cm,  $[\text{H}_2\text{SO}_4]$  averages about  $8 \times 10^9 \text{ cm}^{-3}$ . We partition the reactor into a top third and a bottom two thirds. Although somewhat arbitrary, it provides a point of view for discussing the experimental results. Furthermore, this point of view is congruent with the experimental finding that a large particle mode at the leading edge of the size distributions is discernible, especially so when base was added. So although clusters are formed and particles are nucleated along the length of the reactor, we seek to explain only the largest of them.

With this perspective, we can calculate from bulk properties the growth of the leading-edge particles due to their accumulating  $\text{H}_2\text{SO}_4$  and  $\text{H}_2\text{O}$  (assuming no evaporation) as they traverse the bottom 2/3 of the flow reactor. Using centerline values, an increase in particle diameter of 4.8 nm is estimated as they travel from 40 to 125 cm, using the bulk approximation to calculate the increase in diameter (Verheggen and Mozurkewich, 2002; Wexler and Clegg, 2002). This is in accord with the leading-edge mode diameters in Fig. 2b of about 6 nm, considering that nascent particles are roughly 1.3 nm in diameter; using bulk properties for the 4 acid cluster assuming it is large enough for evaporation to be negligible. There is also a 0.3 nm difference between mobility and volume/mass diameters (Larriba et al. 2010). Thus modeled  $\text{H}_2\text{SO}_4$  on-axis concentrations and residence time along with the assumption of bulk properties for the small particles is an adequate starting point for discussing growth in this experiment.

Growth was also explored with the model and simulated particle size distributions (Supplement, S1.3. Fig. S7.1) are consistent with the growth calculation in the preceding paragraph. The simulated clusters were grown to hundreds of  $\text{H}_2\text{SO}_4$  molecules using growth-only for clusters larger than 10  $\text{H}_2\text{SO}_4$  molecules. The ammonia-added simulations show a  $D_{1e}$  of about 4 nm (Fig. S1.3.1b) and 6 nm (Fig. S7.1) for  $Q_4 = 2.1$  and 4.2 sccm, respectively. These mode diameters are consistent with the bulk-properties growth analysis.

The added-base simulations also provide information on nucleation near the top of the reactor. The axial distribution of critical clusters, assumed to contain 4  $\text{H}_2\text{SO}_4$  molecules, and those just larger reach a steady state by about 40 cm (Fig. S1.3.2) while very few of the 20 and larger  $\text{H}_2\text{SO}_4$  clusters have yet formed. Nucleation in the top third of the flow reactor is important and heavily influences the large particle mode when base is present. Downstream regions contribute mid-sized particles that influence the shape of the simulated particle size distributions; this can be seen in binary, added-dimethylamine and added-ammonia simulations that are compared in Figs. S1.3.1c. Nonetheless, these simulations support a partitioning of



the reactor as a rhetorical tool for discussing the results and for drawing broad conclusions about the presence of contaminants in this region.

### 3.2 Variation of $N_p$ with [reactant]

#### 3.2.1 Dependence on HONO

5 Shown in Fig. 4a are  $N_p$  vs.  $Q_4$ , the flow through the HONO source while the other reactants were held constant: 296 K, 52 % RH,  $SO_2$  at 8 ppmv or higher. The data are primarily measurements without added base (black squares) but the results from two runs where base was added are also shown. Fig. 4b are typical size distributions for measurements at  $Q_4 = 4.2$  sccm for experiments with and without added base. Several more representative size distributions as a function of  $Q_4$  are shown in the Supplement (S1.2).

10 The  $N_2$  flow through the HONO source,  $Q_4$ , is a proxy for HONO abundance and thus sulfuric acid. The variation of the volume-mean diameter of the leading-edge mode with  $Q_4$  is presented in the Supplement (Fig. S1.2.2) and particle size scales approximately linearly with  $Q_4$ . This suggests that particles are exposed to linearly increasing amounts of  $H_2SO_4$  over this range of  $Q_4$ . This data supports the  $Q_4$ -as-proxy notion that  $H_2SO_4$  levels are proportional to the HONO concentration in PhoFR which is set by the nitrogen flow ( $Q_4$ ) through the HONO source.

15 The nominally binary  $N_p$  has a power-dependence on  $Q_4$  of about 4 (dashed line) which is also the case for the  $NH_3$  added (230 pptv) data. For ammonia added at this level there is only a modest effect on  $N_p$ , a qualitative finding that is not congruent with recent experimental work (Kürten et al. 2016; Glasoe et al. 2015). For added dimethylamine at  $\sim 2$  pptv, however, there is a large effect on  $N_p$  and on its dependence on  $Q_4$ , consistent with other experimental work (e.g. Glasoe et al.; Almeida et al. 2013). More results and discussion of the added-base experiments are presented below.

20 A power dependence of 5 for  $N_p$  on  $H_2SO_4$  was exhibited for the  $H_2SO_4$ - $H_2O$  binary system (Zollner et al. 2012) which is somewhat larger than that exhibited in Fig. 4b; other bulk experiments have power dependencies on  $H_2SO_4$  that range up to  $\sim 20$  (Wyslouzil et al. 1991; Viisanen et al. 1997). Yet the CLOUD experiment (Kürten et al. 2016), also with photolytic generation of  $H_2SO_4$ , shows a power dependency of 3.7 at 292 K for  $[H_2SO_4]$  concentrations from  $3 \times 10^8$  to  $1.5 \times 10^9$   $cm^{-3}$ . An ammonia-contaminant abundance of 4 pptv was stated to apply to those results. Experimental results (Glasoe et al. 2015; Almeida et al. 2013) indicate power dependencies on  $H_2SO_4$  are significantly affected when a base is present, corroborating the assertion that our nominally pure results were affected by the presence of an impurity base compound.

#### 3.2.2 Effects of added ammonia and dimethylamine.

When base was added to PhoFR, its mixing ratio was calculated assuming it has fully mixed and there is no loss to the wall. There is wall loss in the experiment and mixing of the base into the main flow takes an amount of time. Nonetheless, 30 these mixing ratios are convenient for discussion and they are directly linked to the flow of added base. Care needs to be

taken using these mixing ratios when comparing the results with simulations and other experiments. See the Supplement (S3.1 and S7.1) for more on base mixing into the flow.

With data for nominally clean conditions for comparison, the effect of 230 pptv  $\text{NH}_3$  on the large particle abundance is significant in Fig. 4a, about a factor of 5, a factor that does not significantly depend on the level of HONO and thus  $\text{H}_2\text{SO}_4$  present in the flow reactor. The experimental size distributions (e.g. red triangles in Fig. 4b) reveal a more distinct and larger leading edge mode than the nominally pure data. Plots of  $D_{le}$  as HONO was varied are presented in the Supplement (S3.1) and the effect of added  $\text{NH}_3$  is a ~20% increase in  $D_{le}$ . The shift in the distributions to slightly larger sizes is due to enhanced particle formation in the top third of the flow reactor, shifting upstream the peak nucleation rates compared to that in the absence of added  $\text{NH}_3$ . This is supported by the simulated size distributions shown in the Supplement (S1.3) where the leading-edge of the size distributions becomes more distinct when ammonia is added to the simulations (Figs. S1.3.1).

Previous work has shown large increases in  $N_p$  when ammonia was added to a (nominally clean) binary sulfuric acid-water nucleating system. At  $\text{H}_2\text{SO}_4$  concentrations of a few times  $10^9 \text{ cm}^{-3}$ , Ball et al. (1999), Zollner et al. (2012), and Glasoe et al. (2015) observed factors of 10-to-1000, ~1000, and  $10^6$  for ammonia levels of a few pptv, 25 pptv, and 55 pptv, respectively. Also, Kürten et al. (2016) showed that particle production in the CLOUD experiment increased by about a factor of 100 upon addition of several hundred pptv  $\text{NH}_3$  at 292 K and  $[\text{H}_2\text{SO}_4]$  of  $1.5\text{-}2.2 \times 10^8 \text{ cm}^{-3}$ : this factor may have been even larger if the nominally binary system was not affected by a purported 4 pptv ammonia contaminant. We think that the presence of a contaminant in our nominally pure measurements is responsible for the low enhancement factors in particle numbers when 100s of pptv  $\text{NH}_3$  are added. There will be more discussion on this below.

Dimethylamine addition at 2 pptv (+100/-50%) had a large effect on the number of particles (blue circles, Fig. 4a) and even the smallest particles (mobility diameter of 1.7 nm) increased by about 2 orders of magnitude (Fig. 4b). Nonetheless, the leading edge of the distributions is clearly the dominant mode for these conditions. It is interesting that the shape of the distributions is similar to the nominally binary cases (black diamonds, Fig. 4b). The Supplement (S3.2) presents additional measured size distributions for the dimethylamine-added experiments.

It is notable that  $N_p$  is not particularly sensitive to  $\text{H}_2\text{SO}_4$  above  $Q_4 = 2.7 \text{ sccm}$ . Model results also indicate a leveling off in the calculated  $N_p$  as  $Q_4$  increases (see section 3.3 below) which appears to be due to scavenging of the amine by particles. Nonetheless, it appears that the potential contaminant for the nominally binary experiments is a much less effective nucleator than dimethylamine is at a level of 2 pptv.

Since effects due to adding dimethylamine at the single-digit pptv level are large, it would be desirable to experimentally investigate amine additions at lower levels. With the current dynamic dilution system, base addition at levels lower than a few pptv are swamped by the precision uncertainty in the flow meter readings. More results from these types of experiments await further improvement in the dimethylamine delivery system. Another alternative is exploring conditions where nucleation is expected to slow such as at low  $Q_4$  and/or at temperatures warmer than 296 K.

### 3.2.2.1 Variation of $N_p$ with added base.

Shown in Fig. 5 are the total number of particles plotted as a function of added ammonia level for a fixed amount of HONO either  $Q_4 = 2.1$  (yellow) or 4.2 (red) sccm. The open squares represent the range of data obtained for nominally binary conditions (without added base). There are significant effects on  $N_p$  due to the addition of  $\text{NH}_3$  at the top of the reactor, over a factor of ten for both sets of data.

At large  $\text{NH}_3$  exposures (high levels and/or prolonged addition) particle counts increased dramatically with exposure time, indicating a conditioning of the flow reactor wall. This is demonstrated in the Supplement (S6) that presents measurements on days when 2000 pptv  $\text{NH}_3$  was added. The 2000 pptv  $\text{NH}_3$  data in Fig. 5 were taken soon after ammonia introduction, minimizing the effects of high ammonia exposure.

The large variability of the  $\text{NH}_3$  data in Fig. 5 mirrors the underlying variability in  $N_p$  without added  $\text{NH}_3$  (Fig. 4a). Yet, within the scatter of the measurements the dependence of  $N_p$  upon  $\text{NH}_3$  is smaller than the 1.6 power dependence found in the bulk-source experiments of Glasoe et al. (2015). A close to linear dependence on ammonia can be ascertained from the results of other photolytic  $\text{H}_2\text{SO}_4$  production experiments: the flow reactor experiments of Benson et al. (2009, 2011) and Berndt et al. (2010), and the 292 K CLOUD chamber experimental results (Kürten et al. 2016; Kirkby et al. 2011). On the other hand, the 292 K ACDC theoretical ammonia-sulfuric acid nucleation rates predict a power dependence on ammonia of between 2 and 3, depending on conditions (Kürten et al. 2016).

Simulated  $N_p$  as a function of added ammonia is shown in Fig. 5 and they are roughly in accord with the experimental data. The major discrepancy is at low added  $\text{NH}_3$  where simulated  $N_p$  is significantly lower than experimental  $N_p$ . The presence of a contaminant that influences the experimental  $N_p$ , particularly at low ammonia levels, can contribute to this discrepancy. At high  $\text{NH}_3$  levels, the effect of the contaminant was assumed to be diminished and the cluster thermodynamics were adjusted so that simulations matched experiment. Thus the experimental data at  $Q_4 = 4.2$  sccm with ammonia  $\geq 500$  pptv guided the development of the  $\text{H}_2\text{SO}_4$ - $\text{NH}_3$  cluster thermodynamics used in these simulations (see the Supplement S8). We do not seek to establish the accuracy of the cluster thermodynamics but instead a phenomenological description of the results: the  $\text{NH}_3$ - $\text{H}_2\text{SO}_4$  thermodynamics developed and used here are phenomenological.

Incomplete agreement across the full range of the present experimental results can also be due in part to an inadequate representation of the actual flow and the mixing of base into the flow in the simulations, however, this would not be expected to depend on the amount of added-ammonia or on  $Q_4$  (see Supplement S7.1 for more on base mixing into the flow.) Small changes to a few cluster free energies, 1 or 2 kcal/mol, can significantly alter predicted  $N_p$ .

For ammonia levels greater than a few hundred pptv, this set of thermodynamics (labeled NH3\_52) yields simulated  $N_p$  that varies with  $\text{NH}_3$  to the 1.6 power for  $Q_4 = 4.2$  sccm conditions and  $\text{NH}_3$  to the 1.9 power for the  $Q_4 = 2.1$  sccm conditions. Since the dependencies on  $\text{NH}_3$  for these simulations and those of the theoretical ACDC rates (Kürten et al. 2016) are greater than is exhibited in the present and previous work (Benson et al. 2011; Berndt et al., 2010; Kürten et al. 2016; Kirkby et al. 2011), there may be a commonality across this set of experimental work: that contaminants affected the nominally binary

measurements. The low dependence of particle formation rate on ammonia (or low ‘enhancement factors’ e.g. Benson et al., 2011) exhibited in previous work (Benson et al. 2011; Berndt et al. 2010; Kirkby et al. 2011; Kürten et al. 2016) may have been due in part to the influence of contaminants. A ‘saturation effect’ at high ammonia levels may also act to limit (Kirkby et al. 2011) the ammonia dependence of the nucleation rate. Yet there is congruence of results from a few of the experiments  
5 at high ammonia conditions (see 3.4.1 below.)

The added-dimethylamine data in Fig. 5 show that dimethylamine has a very large effect on  $N_p$ , 2 to 3 orders of magnitude ( $Q_4 = 2.1$  sccm for this data). There is a low dependency on dimethylamine abundance where  $N_p$  scales approximately linearly with amine mixing ratio. Simulations using DMA\_I thermodynamics (Hanson et al. 2017) are also shown in Fig. 5 and simulated  $N_p$  mimic fairly well the experimental  $N_p$  and its variation with dimethylamine, except  
10 perhaps at 30 pptv dimethylamine where simulated  $N_p$  is  $3 \times 10^7 \text{ cm}^{-3}$ . Coagulation would reduce simulated  $N_p$  considerably: with a coagulation rate coefficient of  $2 \times 10^{-9} \text{ cm}^3/\text{s}$ , an  $N_p$  of  $3 \times 10^7 \text{ cm}^{-3}$  results in a coagulation rate of  $2 \times 10^{-9} (3 \times 10^7)^2 = 2 \times 10^6 \text{ cm}^{-3} \text{ s}^{-1}$ . In just five seconds, a third of the simulated particles can coagulate. This rough estimate suggests coagulation is important for those conditions and the effect should be properly evaluated in the simulations.

The dimethylamine results presented in Figs. 4 and 5 are small sets of data and for Fig. 4 dimethylamine was added at a  
15 level that challenges the lower range of the dynamic dilution system. Nonetheless, the thermodynamic scheme DMA\_I yields cluster concentrations that are consistent with the measured  $N_p$  and its trends with dimethylamine level. Since the thermodynamics scheme DMA\_I (Hanson et al. 2017) was developed by comparing to the dimethylamine- $\text{H}_2\text{SO}_4$  data of Glasoe et al. (2015), the present data and the Glasoe et al. dimethylamine results are tied together in a semi-quantitative sense.

### 20 **3.2.3 Water variation and addition of dimethyl amine..**

Shown in Fig. 6 as filled squares are measured  $N_p$  vs. humidity, calculated from the flow rate of the humidified nitrogen. Total flow rate, HONO, and  $\text{SO}_2$  levels were kept constant; the humidified flow rate was varied from 0.5 to 2.4 sLpm. Although the overall data is phenomenologically exponential (the solid line in the figure), over limited ranges the data exhibits power dependencies on RH of between 4 and 6. A strong dependence of the number of particles on RH is expected  
25 for the binary sulfuric acid water nucleating system, and the power dependence here lies at the low end of range (5-to-9) reported by Zollner et al. (2012). A plot of the size of the leading edge mode vs. humidity is presented in the Supplement (Fig. S1.2.2b).

A set of data with 2-to-5 pptv dimethylamine added is shown as the diamonds (filled and open are  $Q_4=4.2$  and 2.1 sccm, respectively). There is much less water dependence (approximately linear) when dimethylamine is present which is  
30 consistent with theoretical notions (Almeida et al. 2013; Henschel et al. 2016) that dimethylamine- $\text{H}_2\text{SO}_4$  clusters are not particularly sensitive to  $\text{H}_2\text{O}$ . This postulate has also been elucidated in several other publications (e.g. Kurten et al. 2008; Coffman and Hegg, 1995). The data indicates there may be a slightly higher sensitivity to water vapor at the low  $Q_4$  conditions. A complicating factor in fully interpreting this data is that the steady-state  $\text{H}_2\text{SO}_4$  abundance (the monomer and

all its hydrates) changes with RH because its overall diffusivity changes about 10 % as RH varies from 15 to 80 % (Hanson and Eisele, 2000.) More experimental work is needed in this interesting system.

Supposing there are dimethylamine-type base contaminants in the putatively base-free experiments (solid squares), it clearly does not reach the single digit pptv level for baseline 52 % RH conditions. Indeed, simulated particle number densities with a level of 0.005 pptv dimethylamine entering the flow reactor were consistent with the 52% RH,  $Q_4=4.2$  sccm results (see section 3.3 below). A set of simulations were run from 0.005 up to 2 pptv dimethylamine and predicted  $N_p$  scaled linearly with base level. At the 2 pptv level, an  $N_p$  of about  $10^7$   $\text{cm}^{-3}$  was predicted while experimental  $N_p$  is  $3 \times 10^6$   $\text{cm}^{-3}$ . Note that an  $N_p$  at the  $10^7$   $\text{cm}^{-3}$  level will be significantly affected by coagulation which is not captured in the simulations.

### 10 3.2.4 SO<sub>2</sub>.

Particle size and number density were found to depend on SO<sub>2</sub> abundance. Shown in Fig. 7 is  $N_p$  vs. the flow rate of the SO<sub>2</sub> mixture,  $Q_1$ . HONO source flow rate  $Q_4$  was 4.2 sccm for this data. Despite its scatter, the data show the SO<sub>2</sub> level affects both the number of large particles and their size,  $D_{v,le}$  (shown in Fig. S1.2.2c): both increase with [SO<sub>2</sub>] and begin to level-off at high [SO<sub>2</sub>]. This qualitative behavior is expected as at low SO<sub>2</sub> abundance not all of the OH will react with SO<sub>2</sub> and above a certain level there should not be much more of an effect with increases in SO<sub>2</sub>. Young et al. (2008) also report a stronger-than-expected dependence of their results on SO<sub>2</sub> abundance.

A set of simulations that includes a reaction between HO<sub>2</sub> and SO<sub>2</sub> is shown as the solid line in Fig. 7. Note that a level of 200 pptv of NH<sub>3</sub> entering the flow reactor was included. The experimental results show increases with SO<sub>2</sub> that are roughly in line with the model simulations. Without this reaction the model shows (the dashed line) much smaller increases in  $N_p$  (40 % vs. 250 % with the reaction) and in size (Fig. S1.2.2c, 10% vs. 20% with the reaction) as SO<sub>2</sub> increases from 2 to 16 ppmv.

The simulation assumed a value of  $3 \times 10^{-17}$   $\text{cm}^3/\text{s}$  for  $k_{\text{HO}_2+\text{SO}_2}$ . There is disagreement whether HO<sub>2</sub> reacts with SO<sub>2</sub> as well as potential end products (Chen et al. 2014; Kurten et al. 2011); we assumed H<sub>2</sub>SO<sub>4</sub> and OH. Experimental values for this rate coefficient range from upper limits of  $1 \times 10^{-18}$   $\text{cm}^3/\text{s}$  (Graham et al. 1979) and  $2 \times 10^{-17}$   $\text{cm}^3/\text{s}$  (Burrows et al. 1979), to a value of  $8 \times 10^{-16}$   $\text{cm}^3/\text{s}$  (Payne et al. 1973). A heterogeneous reaction occurring in the particles involving SO<sub>2</sub> would help explain the dependence of  $D_{v,le}$  on SO<sub>2</sub> abundance (Fig. S1.2.2c) while leaving  $N_p$  undisturbed.

### 3.3 Characteristics of a potential contaminant

Shown in Fig. 8 are the experimental  $N_p$  as a function of HONO from Fig. 4a along with model simulated  $N_p$ . The simulations were run for NH<sub>3</sub> at 0 and 200 pptv using NH3\_52 thermodynamics and for dimethylamine at 0.005 pptv using DMA\_I thermodynamics (Hanson et al. 2017); SO<sub>2</sub> was set to 16 ppmv and  $k_{\text{HO}_2+\text{SO}_2}$  was  $3 \times 10^{-17}$   $\text{cm}^3/\text{s}$ . The experimental data is for nominally-clean conditions.

The simulations with  $\text{NH}_3$  at 200 pptv yield  $N_p$  similar to the experimental and furthermore dependencies upon HONO align with experimental dependencies. The powerful nucleator dimethylamine entering the flow reactor at 5 ppqv ( $1.2 \times 10^5 \text{ cm}^{-3}$ ) also yields a simulated  $N_p$  at  $Q_4 = 4.2 \text{ sccm}$  close to the experimental  $N_p$  of about  $2.5 \times 10^4 \text{ cm}^{-3}$ . The variation of predicted  $N_p$  with HONO, however, is disparate from the experimental variation, where the simulated  $N_p$  levels off at high values of  $Q_4$ . This leveling off is due, at least in part, to a simple number limitation: the largest simulated  $N_p$  is  $4 \times 10^4 \text{ cm}^{-3}$  which is about one third of the number density of dimethylamine molecules introduced. A strict limit would be reached depending on how many dimethylamine molecules are in each particle. Nonetheless, the simulations suggest the contaminant acts more like ammonia than dimethylamine.

While the presence of 200 pptv ammonia is consistent with the experimental  $N_p$ , methylamine has comparable power dependencies on acid. These are plotted as the purple circles in Fig. 8 where the methylamine nucleation rates were taken from the expression in Table S2 of Glasoe et al. (2015) and a 4 s nucleation time was applied. Since it is significantly less powerful than dimethylamine, a larger abundance of 0.5 pptv is needed to give  $N_p$  comparable to the experiment and the full range of  $Q_4$  is covered, assuming scavenging of methylamine by clusters would be minimal. An impurity with an abundance of a fraction of a pptv may last a long time due to a low evaporation rate. These considerations would make methylamine (or perhaps another primary amine) a suitable candidate for a potential gas-phase base contaminant in PhoFR. Of course, whether the contaminant is ammonia or methylamine (or perhaps a combination) cannot be determined at this time. However, it appears that studying the primary amines would be interesting in this context as well as for understanding their effects on sulfuric acid nucleation rates. The Supplement (S9) presents some more discussion on the effects of  $\text{SO}_2$ .

### 3.4 Comparison to previous results.

A number of previous results are compiled along with the present measurements in Fig. 9 for nominally base-free conditions. The present results are assigned the simulated  $\text{H}_2\text{SO}_4$  value in the center of the reactor and at 30 cm into the illuminated region. The nucleation rate  $J$  was taken to be  $N_p$  divided by the time the center of the flow travels from 20 to 40 cm, 4 s. This time is presumed to apply for the nominally clean conditions here. On the other hand, with base added intentionally, significant nucleation may also occur in the 0 to 20 cm region where base abundance is high. Uncertainties in  $J$  are probably on the order of a factor of 2. Uncertainty in  $\text{H}_2\text{SO}_4$  is about a factor of two, based on the calculated values at 15 and 60 cm, which are -49 and +106 %, resp., from the 30 cm value. The radial profile of  $\text{H}_2\text{SO}_4$  at 30 cm axial distance is flat from the center out to a radius of 1.7 cm. See the Supplement for radial profiles of  $\text{H}_2\text{SO}_4$  (Fig. S1.3.3).

The experimental data in Fig. 9 were taken over a range of temperatures, 288 to 300 K, and relative humidities, 2.3 to 75 % RH; conditions indicated in the legend. The present results extrapolate to rates that are in fair agreement with Benson et al. 2009 and much of the CLOUD data set (Kirkby et al. 2011; Kürten et al. 2016) except for the 40 % RH at 298 K data. The bulk-source  $\text{H}_2\text{SO}_4$  data reported by Zollner et al. is included for reference; it was corrected from 38% RH to 52 % RH, increasing by about a factor of 5 using a  $\text{RH}^5$  dependency. The difference between the bulk-source and present photolytic

H<sub>2</sub>SO<sub>4</sub> is about 4 orders of magnitude; the Kürten et al. (2016) 40 % RH data is closest to this set of bulk data, within about two orders of magnitude.

There is apparent agreement of several data sets for H<sub>2</sub>SO<sub>4</sub> concentrations of 10<sup>8</sup> to 10<sup>9</sup> cm<sup>-3</sup>: our lowest J (and the extrapolation of our data, dotted line), Yu et al. (2017), Benson et al. (2009), Kürten et al. (2016) and Kirkby et al. (2012) but it is complicated by the wide range of relative humidities: 2.3 % RH up to 75 % RH. The data of Young et al. (2008) suggests a very low contamination level however there are unresolved issues in measured [H<sub>2</sub>SO<sub>4</sub>] ( see the factor of ten disparity in their Fig. 5). Lack of experimental water dependencies and assessment of base-levels makes drawing conclusions from these comparisons fraught with difficulty. Nonetheless, it is interesting that the dependencies of J on sulfuric acid level are similar in many of these studies. This suggests there is an underlying similarity in particle formation conditions such as contaminant identity and level (which seems unlikely) or the critical cluster's H<sub>2</sub>SO<sub>4</sub>-content is not particularly sensitive to the type or abundance of the contaminant.

### 3.4.1 Comparison of nucleation rates for added ammonia

Plotted in Fig. 10 are nucleation rates vs. ammonia abundance for measurements at low [H<sub>2</sub>SO<sub>4</sub>], 5x10<sup>7</sup> and 1.5x10<sup>8</sup> cm<sup>-3</sup>, and temperatures between 288 and 293 K. Also plotted are predictions according to the present data using the box-model and methodology presented in Hanson et al. (2017). The experimental data from the CLOUD project for 292.5 K were taken from Dunne et al. (2017) and were also presented by Kürten et al. (2016). The Benson et al. (2009, 2011) work was performed at 288 K and significant extrapolation of nucleation rates were applied to get comparable sulfuric acid concentrations (see the caption). The Berndt et al. (2011) work was performed at 293 K and extrapolation was needed to get comparison rates for the 1.5x10<sup>8</sup> cm<sup>-3</sup> [H<sub>2</sub>SO<sub>4</sub>] conditions.

The model predictions using the NH<sub>3</sub>\_52 thermodynamics developed here gives rates that are congruent with the CLOUD data and with Berndt et al. (2011) while NH<sub>3</sub>\_I thermodynamics (calculated only for [H<sub>2</sub>SO<sub>4</sub>] = 1.5x10<sup>8</sup> cm<sup>-3</sup>) gives rates too high by two-to-three orders of magnitude. NH<sub>3</sub>\_I is a set of ammonia-sulfuric acid thermodynamics derived in Hanson et al. (2017) that skirted the lower limit of the Glasoe et al. (2015) ammonia data set. Benson et al. (2009, 2011) is quite disparate and a temperate correction would lessen the discrepancy for the set of data at the low H<sub>2</sub>SO<sub>4</sub> but it would worsen it at the higher H<sub>2</sub>SO<sub>4</sub>.

With the box-model predictions using NH<sub>3</sub>\_52 thermodynamics serving as a bridge, the present ammonia-added data agrees with both the CLOUD data (Kürten et al., 2016; Dunne et al. 2017) and the Berndt et al. (2011) data. Since the box-model rates using NH<sub>3</sub>\_I thermodynamics (Hanson et al. 2017) are much too high, we can conclude that the Glasoe et al. (2015) ammonia data set it was based on does not agree with the present measurements. Recently, Kürten (2019) concluded that the NH<sub>3</sub>\_II (stronger binding than NH<sub>3</sub>\_I) thermodynamics of Hanson et al. (2017) yields nucleation rates much higher than the CLOUD measurements.

## 4 Summary

We presented a new experimental apparatus for studying particle formation involving photolytically-formed H<sub>2</sub>SO<sub>4</sub> vapor and results show the system is reproducible and responds to changes in water, HONO and SO<sub>2</sub> concentrations largely as expected. Modeled particle formation rates could be made congruous with experimental observations by including either dimethylamine at a level of  $5 \times 10^{-15}$  mole fraction or NH<sub>3</sub> at a level of  $\sim 2 \times 10^{-10}$  mole fraction. Also, the dependence of N<sub>p</sub> on SO<sub>2</sub> level was best explained by a reaction between HO<sub>2</sub> and SO<sub>2</sub> that yields (ultimately) H<sub>2</sub>SO<sub>4</sub> and OH with a rate coefficient of  $3 \times 10^{-17}$  cm<sup>3</sup>/s.

Comparison of the present results to other photolytic H<sub>2</sub>SO<sub>4</sub> experiments yields several suppositions. Their divergence from the bulk-source data of Zollner et al. (2012) suggests these experiments are not clean enough and/or they are subject to an unknown reaction or photochemistry. The similarity of the present results to those of Benson et al. (2009), Kirkby et al. (2011), Kürten et al. (2016) and Yu et al. (2017) suggests a common element that affects nucleation beyond what bulk-source H<sub>2</sub>SO<sub>4</sub> experiments reveal. The outlier results of Berndt et al. (2010, 2014) and Benson et al. (2011) may suffer from relatively high level of contaminants: Berndt et al. (2014) suggested that a pptv-level of amine could have been present in their experiment. As can be seen in Fig. 9, there is a remarkable agreement of the H<sub>2</sub>SO<sub>4</sub> power dependencies for Kirkby et al. (2011), Yu et al. (2017), and the present results. This may be due to a similarly-sized critical cluster across these studies.

Side products from photolytic generation of H<sub>2</sub>SO<sub>4</sub> that enhance nucleation were suggested by Berndt et al. (2008), however, Sipilä et al. (2010) found no difference between nucleation rates whether H<sub>2</sub>SO<sub>4</sub> was produced photolytically or taken from a bulk source. Yet much of the Sipilä et al. (2010) photolytic nucleation rates are many orders of magnitude too high for the putative binary system (see Fig. 9 comparing the present results, the Zollner et al. (2012) bulk-liquid data, Yu et al. (2017) and results from the CLOUD experiment: Kirkby et al. (2011), Kürten et al. (2016).) With the exception of their bulk 298 K 30% RH results, the Sipilä et al. (2010) data largely overlap the Benson et al. (2011) and Berndt et al. (2014) data and probably also suffer from amine contaminants at the pptv-level.

The total particle number strongly depended on relative humidity with RH<sup>4</sup> and RH<sup>6</sup> power relationships over RH ranges of 15 to 35 % and 40 to 77%, respectively. The CLOUD 298 K results (Kürten et al., 2016) show a power dependency of 4 on RH from 40 to 75 % at 298 K in rough agreement with the present results. Yu et al. (2017) reported a nucleation rate that depended linearly on RH that seems to be out of line with these other data sets.

The weak dependence of N<sub>p</sub> on added NH<sub>3</sub> near room temperature, also reflected in a few other studies (Kirkby et al. 2011; Kürten et al. 2016, Benson et al., 2011), is probably due to a contaminant that overwhelms ammonia-induced nucleation, especially at low levels of added ammonia. We surmised that a contaminant in our system is not consistent with dimethylamine but is consistent with a few hundred pptv of ammonia; alternatively, we postulated that 0.5 pptv of methylamine could also be responsible.

The model simulations with NH<sub>3</sub>-H<sub>2</sub>SO<sub>4</sub> thermodynamic schemes NH3\_I and, because it is stronger, NH3\_II (Hanson et al. 2017), result in N<sub>p</sub> that greatly exceed the present experimental results. With the simulations serving as a bridge between



these two experiments, we conclude that the present experimental data and the Glasoe et al. (2015)  $\text{NH}_3\text{-H}_2\text{SO}_4$  results do not agree. Glasoe et al. (2015) noted that their  $\text{NH}_3\text{-H}_2\text{SO}_4$  nucleation rates were much higher than those of Ball et al. (1999) and Zollner et al. (2012), but with the present results as a backdrop the Glasoe et al. criticisms of those two studies are blunted. In hindsight we postulate an avenue for an amine contamination in the Glasoe et al. (2015) ammonia experiments:  
5 several amino-compounds were studied in succession using the same dynamic dilution system. Since ammonia was used between amines, holdover of the amine is possible and even small levels would significantly boost particle numbers, compromising the ammonia-sulfuric acid system measurements. Note that in the present experimental setup, there were two dynamic dilution systems, one dedicated for ammonia and one for dimethylamine.

Additions of dimethylamine resulted in large abundances of particles which limited the range of conditions we were able  
10 to study. The number densities are such that a model with proper treatments of coagulation and cluster-cluster collisions is needed to fully interpret the results. Nonetheless, the experimental results are in decent agreement with model simulations using the thermodynamic scheme (DMA\_I, Hanson et al., 2017) that best captured the Glasoe et al. (2015) dimethylamine- $\text{H}_2\text{SO}_4$  experimental results. We found low RH dependencies when dimethylamine was added, in line with expectations. Note the details of this preliminary finding need further work: (i) RH affects the steady-state sulfuric acid and (ii)  
15 coagulation effects need to be properly evaluated.

Atmospheric implications of the present work are of a qualitative nature. The current work suggests that nucleation rates in the  $\text{NH}_3\text{-H}_2\text{SO}_4$  system for a few studies can be seen to converge but more measurements near room temperature are needed to aid the development of ammonia-sulfuric acid thermodynamics (e.g. this work, Hanson et al. 2017; Kürten, 2019). We concluded that the experimental nucleation rates in this system from Glasoe et al. (2015) are discordant. On the other  
20 hand, as alluded to in the previous paragraph, the current work is consistent with the Glasoe et al. (2015) dimethylamine- $\text{H}_2\text{SO}_4$  results. Also, the much-predicted low RH dependency for dimethylamine- $\text{H}_2\text{SO}_4$  nucleation finds experimental corroboration here. Finally, even if the reaction of  $\text{HO}_2$  with  $\text{SO}_2$  occurs with a rate coefficient of  $1 \times 10^{-16} \text{ cm}^3 \text{ s}^{-1}$ , it is probably an insignificant source of atmospheric hydroxyl radicals and oxidized sulfur compounds.

In the future, a series of measurements in the dimethylamine- $\text{H}_2\text{SO}_4$  system with added dimethylamine at fractional pptv  
25 levels and low relative humidities are planned. We also plan to study the relative humidity dependence of ammonia-induced  $\text{H}_2\text{SO}_4$  nucleation as well as variations of temperature on both amine- and ammonia-addition nucleation. In the long term, the system developed here will be used in particle growth studies where nm-diameter particles prepared in the Glasoe et al. (2015) apparatus are directed through PhoFR along with target organic compounds.

30 **Data availability.** All data presented in this manuscript are available by contacting the corresponding author.

#### **Author contribution.**

HA and JV built the particle detector and performed preliminary experiments, MA helped design and carry out experiments, SM carried out added- $\text{NH}_3$  experiments and helped with the manuscript, JK helped develop the photochemical

module, and DH developed and ran the simulations, developed and carried out experiments and prepared the manuscript with contributions from all co-authors. The authors declare that they have no conflict of interest.

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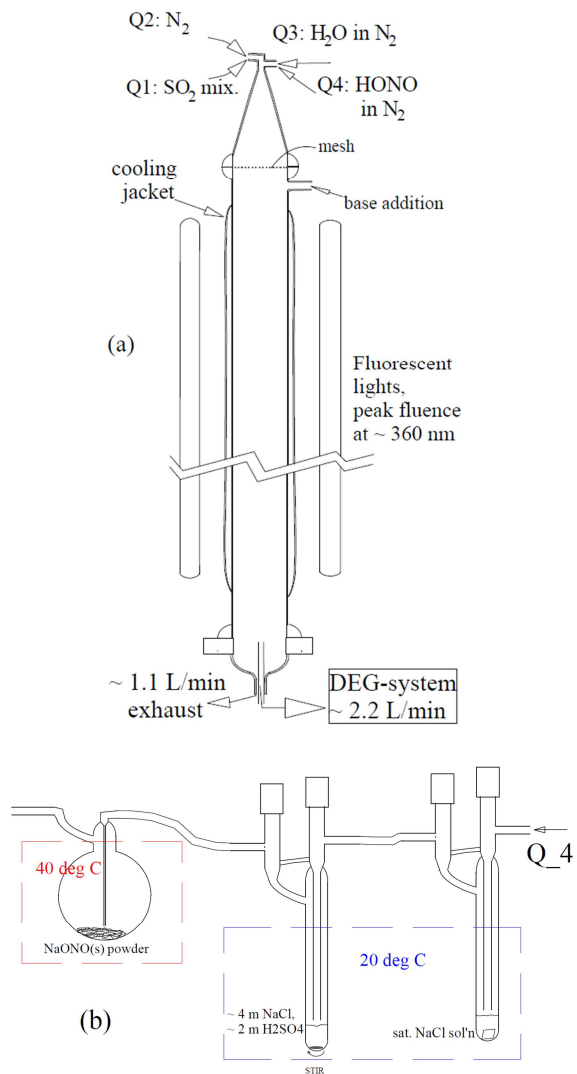
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Figures and captions.



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**Fig. 1 (a) PhoFR schematic and (b) HONO source. The average flow velocity of 2.8 cm/s yields an average residence time in PhoFR of approximately 45 s. The concentrations listed in (b) are in molal (mole per kg H<sub>2</sub>O).**

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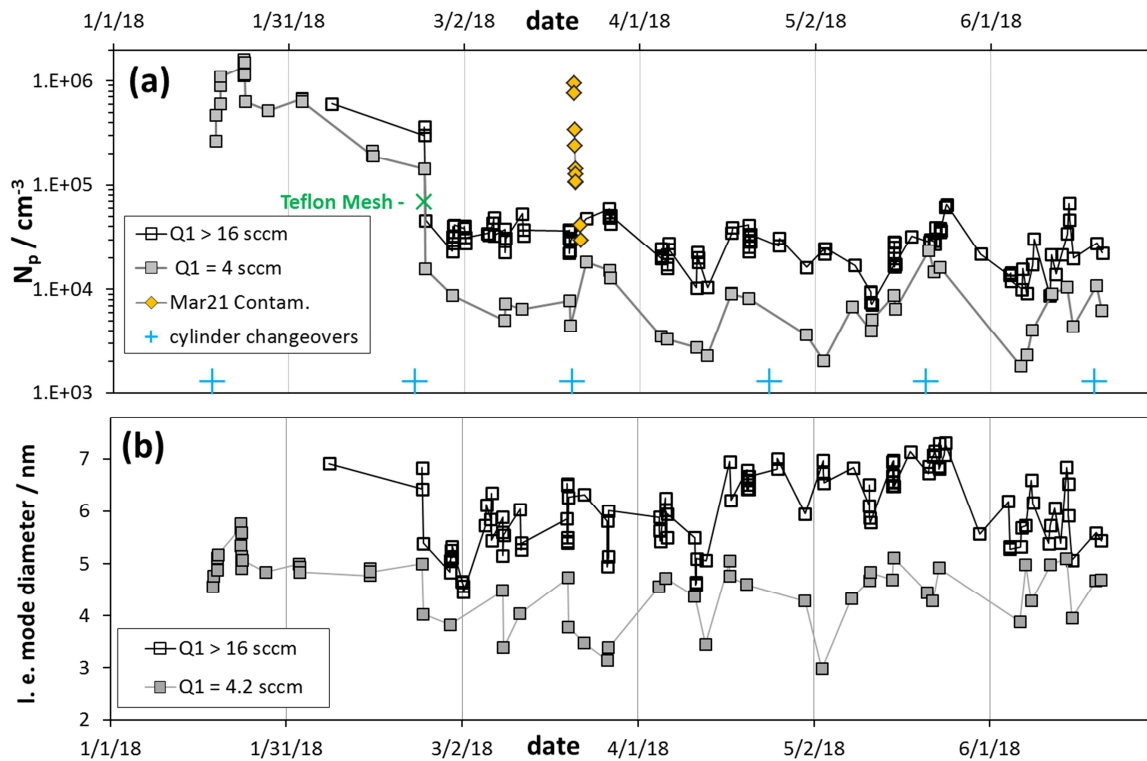


Fig. 2. (a) Number of large particles for baseline HONO ( $Q_4=4.2 \text{ sccm}$ :  $[\text{HONO}] = 5 \times 10^{11} \text{ cm}^{-3}$ ) plotted vs. time for two different  $\text{SO}_2$  levels, equivalent to 2 and  $> 8 \text{ ppmv}$ . Data on 21 and 22 Mar are shown as the yellow diamonds and are for low  $\text{SO}_2$  conditions:  $N_p$  is severely elevated due to a suspected dust contaminant. (b) Leading edge mode diameters plotted versus time also binned by  $\text{SO}_2$  level.

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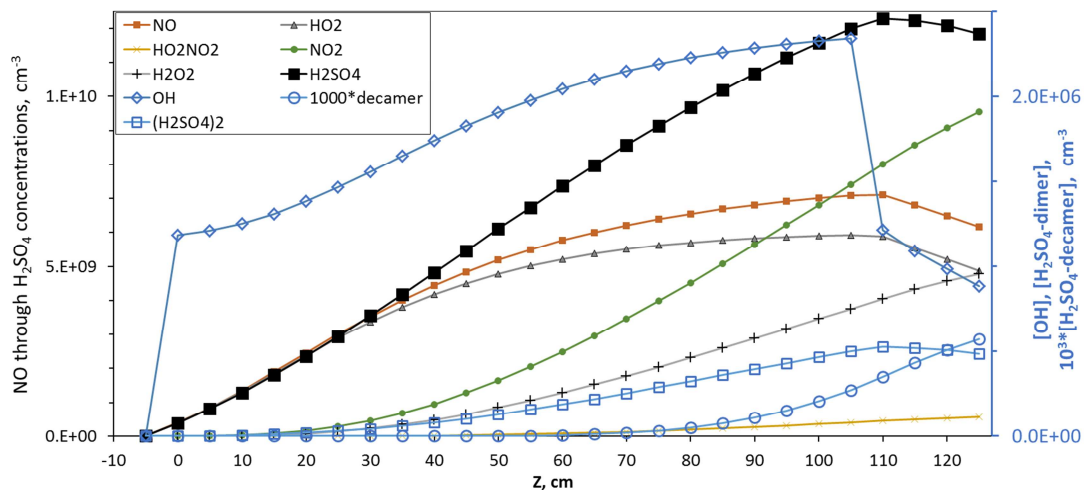


Fig. 3. Model simulation for  $[\text{HONO}] = 5.2 \times 10^{11} \text{ cm}^{-3}$ ,  $[\text{SO}_2] = 4 \times 10^{14} \text{ cm}^{-3}$  and no base. Concentrations of NO through  $\text{H}_2\text{SO}_4$  are plotted on the left axis; concentrations of OH and the  $(\text{H}_2\text{SO}_4)_2$  and  $(\text{H}_2\text{SO}_4)_{10}$  clusters on the right axis. These simulations are equivalent to experimental conditions of  $Q_4 = 4.2 \text{ sccm}$ ,  $Q_1 = 32 \text{ sccm}$ . The lighted section is from 0 to 110 cm. At 110 cm HONO photolysis ceases and  $[\text{OH}]$  (right axis) drops to a level supplied primarily by  $\text{HO}_2 + \text{NO}$  (a reaction between  $\text{HO}_2$  and  $\text{SO}_2$  was included, see section 3.2.4).

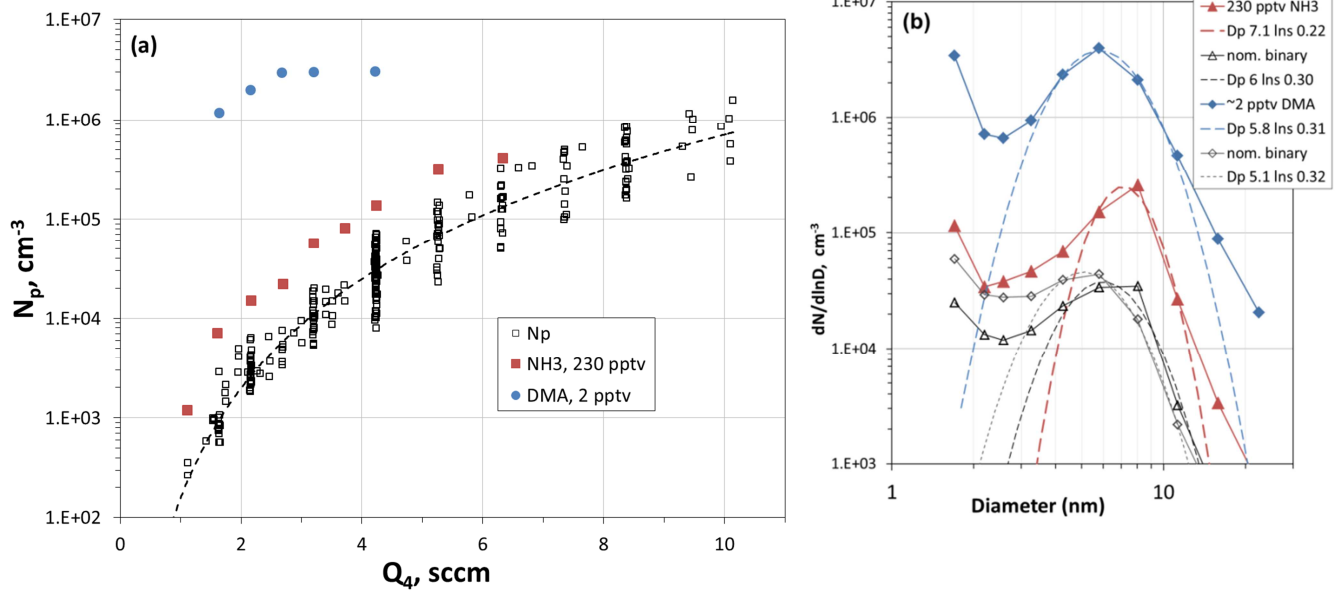
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5 Fig. 4. (a) Number of large particles as a function of  $Q_4$ , the HONO-laden flow rate. RH was 52 %,  $T = 296$  K, and  $[SO_2] > 2.5 \times 10^{14} \text{ cm}^{-3}$  (10 ppmv). For reference,  $Q_4 = 4.2$  sccm results in a modeled value of  $\sim 4 \times 10^9 \text{ cm}^{-3}$  for  $H_2SO_4$  at  $Z = 35$  cm and  $R = 0$ . Base-added experimental results are shown as the circles (dimethylamine) and red squares (ammonia). (b) Size distributions showing the effect of added  $NH_3$  (red triangles) and added dimethylamine (blue diamonds). Nominal binary distributions for those runs are also shown. The log-normal distributions are also shown (dashed lines) and the legend indicates the mode diameter and  $\ln \sigma$  in that order.

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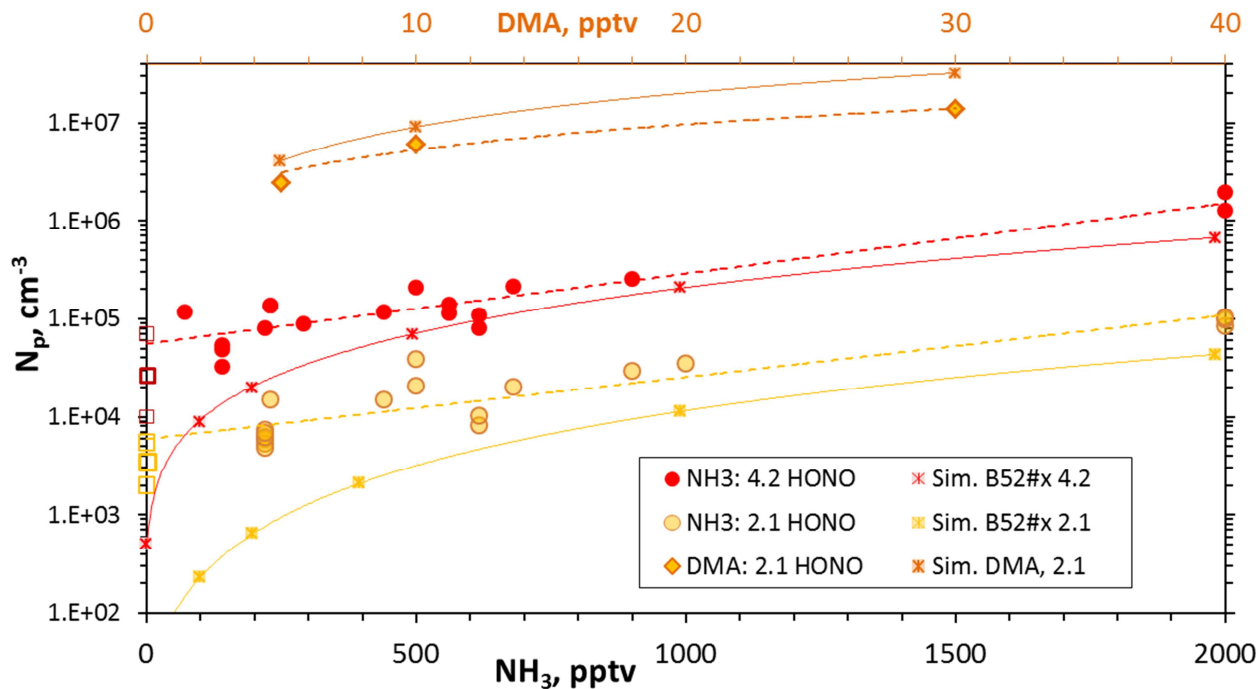
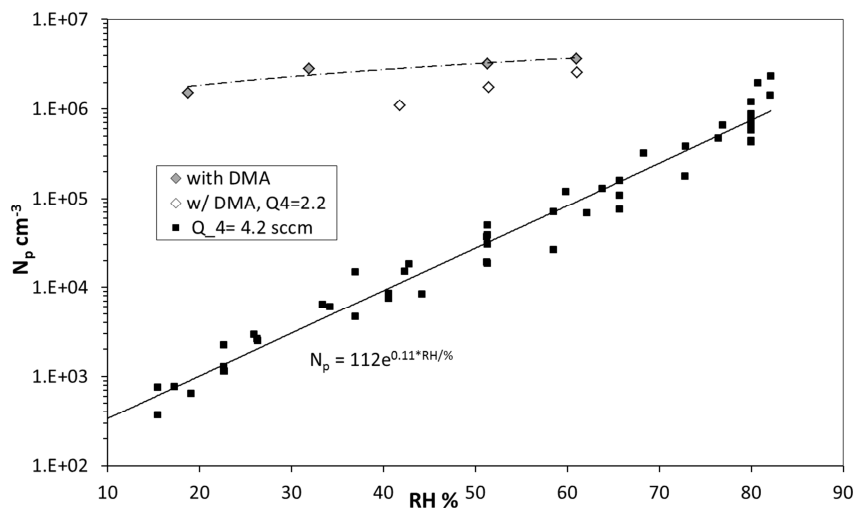
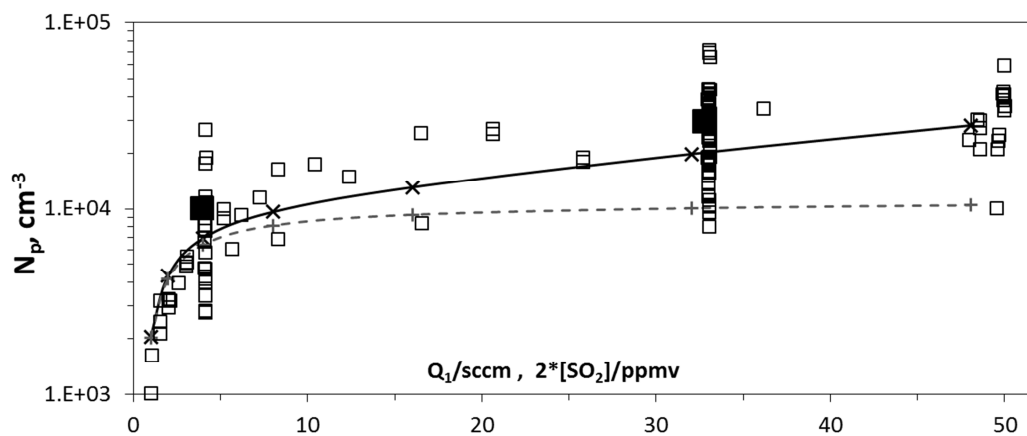


Fig. 5. Variation of measured  $N_p$  with added  $\text{NH}_3$  for  $Q_4$  of 4.2 sccm and 2.1 sccm and for added dimethylamine at  $Q_4 = 2.1$  sccm (top axis for dimethylamine level). Simulated  $N_p$  are shown for  $\text{NH}_3_{52}$  (ammonia) and  $\text{DMA}_I$  (dimethylamine) thermodynamics. The average and the range of measured  $N_p$  without added base are shown as the squares for the two  $Q_4$  levels. Lines connect data for simulations (solid) and guide the eye for experimental (dashed).  $\text{SO}_2$  level was  $> 12$  ppmv.

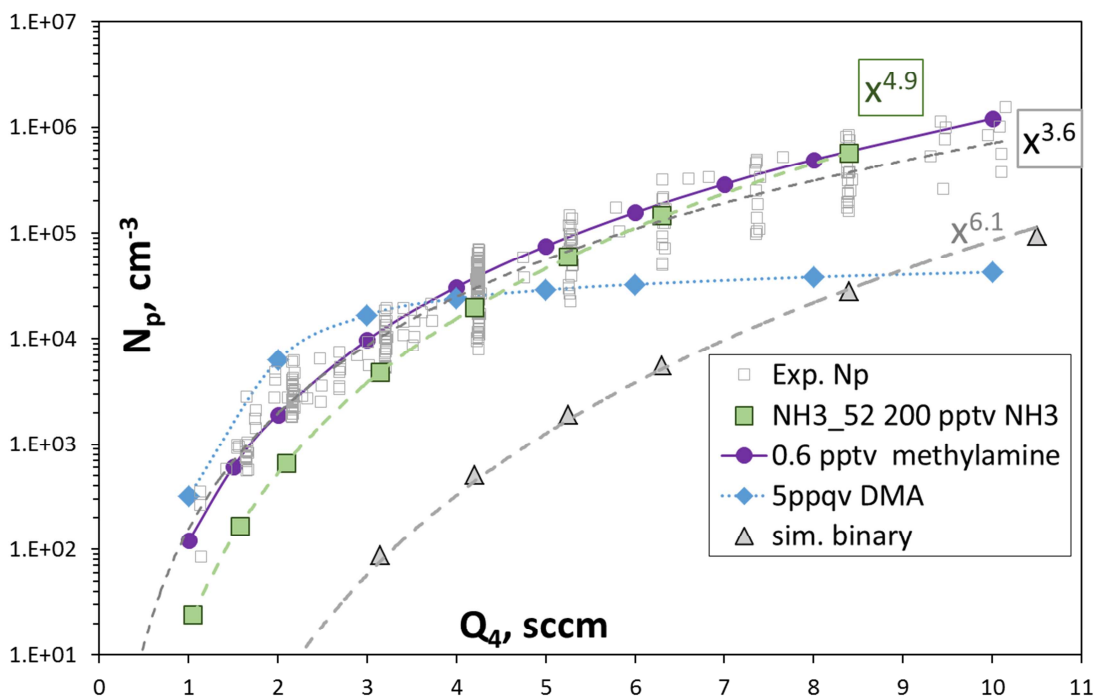
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5 Fig. 6. Variation of  $N_p$  with RH in % (RH determined by the fraction of flow through the water saturator,  $Q_3$ )  $Q_4$  was 4.2 sccm and  $Q_1 > 20$  sccm ( $[SO_2] > 10$  ppmv). Also shown are data with dimethyl amine added: at 2 pptv (filled diamonds) and data at a lower  $Q_4 = 2.1$  sccm and dimethyl amine at 5 pptv.



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15 Fig. 7. Number of large particles vs. flow rate of  $SO_2$  mixture. The HONO-source flow rate,  $Q_4$ , was 4.2 sccm which results in roughly  $5 \times 10^{11} \text{ cm}^{-3}$  [HONO] in PhoFR. For reference, an  $SO_2$  mixture flow rate of 32 sccm results in an  $[SO_2]$  of  $4 \times 10^{14} \text{ cm}^{-3}$  in PhoFR (about 16 pptv). The solid and dashed lines are model values for  $N_p$  and size with 200 pptv  $NH_3$  entering the flow reactor and a  $k_{3x5}$  ( $HO_2 + SO_2$ ) rate coefficient of  $3 \times 10^{-17} \text{ cm}^3/\text{s}$  (x's, solid lines) and in the absence of this reaction (+s and dashed lines). The solid squares indicate the average at  $Q_1 = 4$  and 32 sccm.



10 Figure 8.  $N_p$  vs.  $Q_4$ , the HONO-containing flow. Experimental from Fig. 4(a), simulated is on-axis  $N_p$  at axial position = 120 cm into PhoFR. Green symbols are ammonia at 200 pptv and the gray triangles are the binary, simulated with scheme NH3\_52 thermodynamics; the blue diamonds are simulations with 0.005 pptv dimethylamine added using DMA\_I thermodynamics. The purple circles are 0.6 pptv methylamine from Glasoe et al. (2015). Power dependencies indicated in the plot.

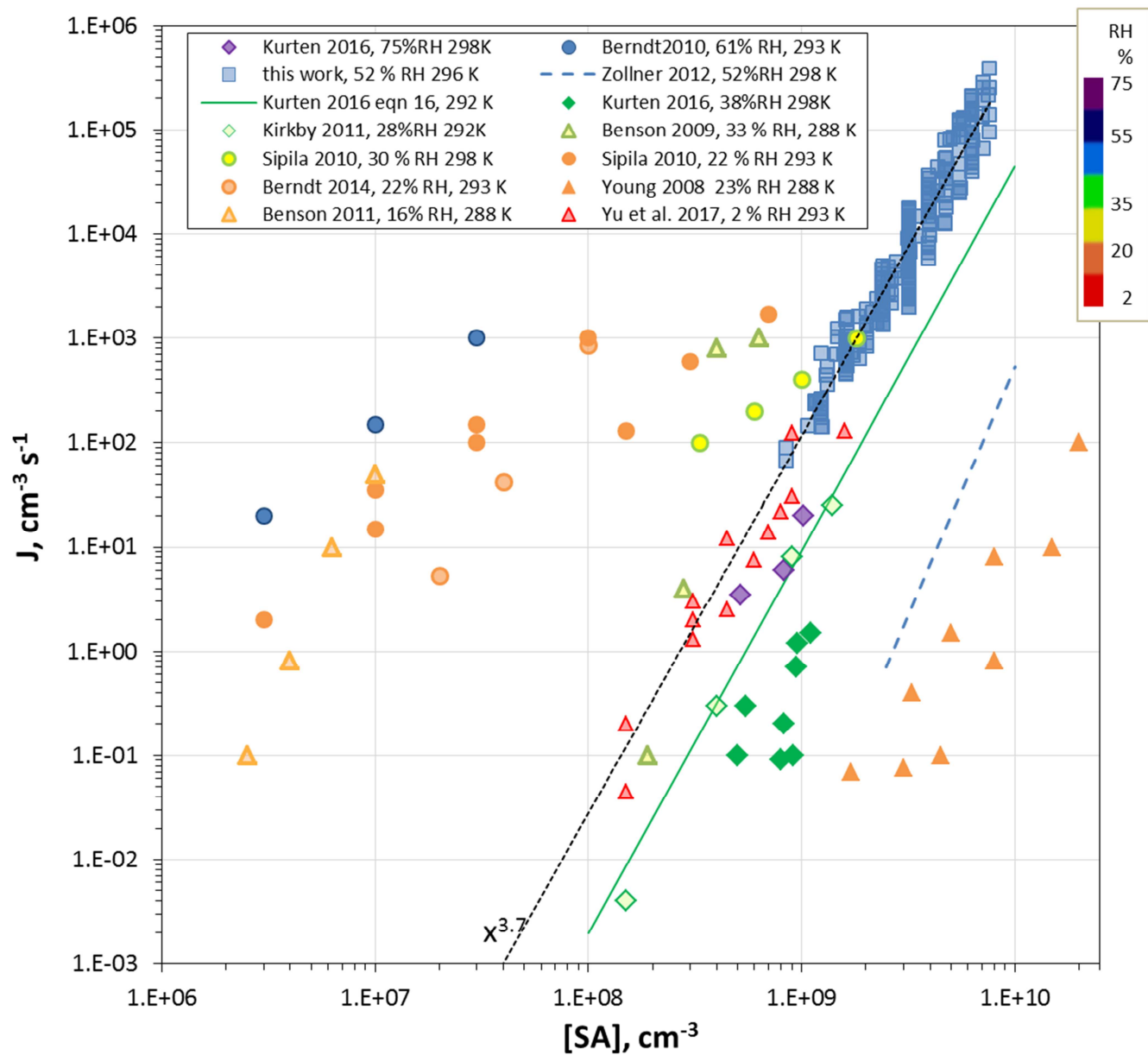


Fig. 9: Comparison of results from previous work (all photolytic  $\text{H}_2\text{SO}_4$  production except Zollner et al., 2012) for nominally clean conditions. RH color-coding was applied to the points and temperatures are indicated in the legend.

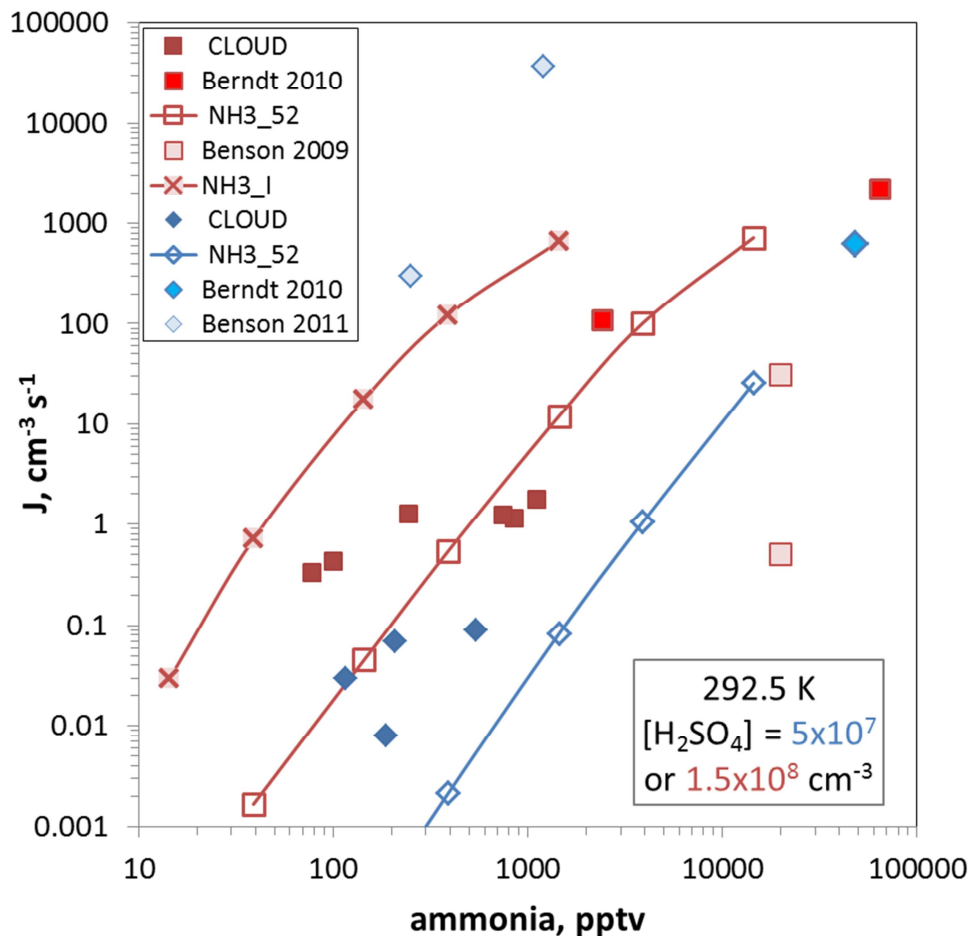


Fig. 10. Ammonia-sulfuric acid nucleation rate vs. ammonia abundance. Sulfuric acid level is  $5 \times 10^7 \text{ cm}^{-3}$  for the blue diamonds and  $1.5 \times 10^8 \text{ cm}^{-3}$  for the red squares. CLOUD data is from Dunne et al., 292.5 K, neutral conditions. Berndt et al. (2010), 293 K, has their squared dependence on  $[\text{H}_2\text{SO}_4]$  applied which results in a division by  $\sim 30$  to extrapolate to the  $1.5 \times 10^8 \text{ cm}^{-3}$  conditions; no corrections needed for the  $5 \times 10^7 \text{ cm}^{-3}$  data point. Benson et al. (2009) report a 4 power dependence on sulfuric acid and correction factors are 5 and divide by 16. Benson et al. (2011) requires multiplicative factors of  $\sim 40$  to extrapolate to  $5 \times 10^7 \text{ cm}^{-3}$   $[\text{H}_2\text{SO}_4]$ . Box model nucleation rates for the two different  $[\text{H}_2\text{SO}_4]$  are shown for the NH3\_52 thermodynamics and J for the  $1.5 \times 10^8 \text{ cm}^{-3}$  conditions was also predicted using NH3\_I from Hanson et al. (2017).

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