



# Multiphase Reaction of SO<sub>2</sub> with NO<sub>2</sub> on CaCO<sub>3</sub> Particles. 1. Oxidation of SO<sub>2</sub> by NO<sub>2</sub>

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7 Abstract. Heterogeneous/multiphase reaction of SO2 with NO2 on solid or aqueous particles is thought to be a 8 potentially important source of sulfate in the atmosphere, for example, during heavily polluted episodes (haze), 9 but the reaction mechanism and rate are uncertain. In this study, we investigated the heterogeneous/multiphase 10 reaction of SO<sub>2</sub> with NO<sub>2</sub> on individual CaCO<sub>3</sub> particles in N<sub>2</sub> using Micro-Raman spectroscopy in order to 11 assess the importance of the direct oxidation of SO<sub>2</sub> by NO<sub>2</sub>. In the SO<sub>2</sub>/NO<sub>2</sub>/H<sub>2</sub>O/N<sub>2</sub> gas mixture, the CaCO<sub>3</sub> 12 solid particle was first converted to the Ca(NO<sub>3</sub>)<sub>2</sub> droplet by the reaction with NO<sub>2</sub> and the deliquescence of 13 Ca(NO<sub>3</sub>)<sub>2</sub>, and then NO<sub>2</sub> oxidized SO<sub>2</sub> in the Ca(NO<sub>3</sub>)<sub>2</sub> droplet forming CaSO<sub>4</sub>, which appeared as needle-shaped 14 crystals. Sulfate was mainly formed after the complete conversion of CaCO3 to Ca(NO3)2, that is, during the 15 multiphase oxidation of SO<sub>2</sub> by NO<sub>2</sub>. The precipitation of CaSO<sub>4</sub> from the droplet solution promoted sulfate formation. The reactive uptake coefficient of SO<sub>2</sub> for sulfate formation is on the order of 10<sup>-8</sup>, and RH enhanced 16 the uptake coefficient. We estimate that the direct multiphase oxidation of SO<sub>2</sub> by NO<sub>2</sub> is not an important source 17 18 of sulfate in the ambient atmosphere compared with the  $SO_2$  oxidation by OH in the gas phase.





### 19 1 Introduction

20 Sulfate is a major component of atmospheric particulate matter. It contributes to a large fraction of 21 atmospheric aerosol particles in both urban and rural areas (Seinfeld and Pandis, 2006; Zhang et al., 2007). 22 Sulfate is either from primary source, such as sea spray, or from secondary source, i.e., by the oxidation of 23 reduced sulfur compounds such as dimethyl sulfide (DMS), carbonyl sulfur (COS), and SO<sub>2</sub> (Seinfeld and Pandis, 24 2006). In the continent, the main source of sulfate is the oxidation of  $SO_2$ , an important air pollutant from fossil 25 fuel combustion. SO<sub>2</sub> can be oxidized in the gas phase, mainly by OH, or in the particle phase such as by  $H_2O_2$ , 26 O<sub>3</sub>, or O<sub>2</sub> catalyzed by transition metal ions in cloud or fog water (Seinfeld and Pandis, 2006; Finlayson-Pitts and 27 Pitts Jr., 1999) or by O<sub>3</sub> or photochemical reactions on particle surface (Zhu et al., 2011; Li et al., 2006; Li et al., 28 2007; Shang et al., 2010; Li et al., 2011). 29 Although various pathways of SO<sub>2</sub> oxidation are identified, the source of sulfate and relative importance of 30 various pathways of SO<sub>2</sub> oxidation forming sulfate in the atmosphere still remain uncertain. For example, during 31 heavily polluted episodes (haze) in China in recent years, high concentrations of sulfate were observed, but the 32 source of sulfate is elusive (Wang et al., 2016; Wang et al., 2014a; Zheng et al., 2015b; Guo et al., 2014). The 33 relative contribution of regional transport versus local formation and physical and chemical mechanisms 34 responsible for sulfate formation are still not clear. Recent studies have highlighted heterogeneous reactions of 35  $SO_2$  on solid or liquid particles to be a possibly important source of sulfate based on model, field and laboratory 36 studies (Huang et al., 2014; Zhu et al., 2011; Cheng et al., 2016; Gao et al., 2016; Zheng et al., 2015a; Wang et al., 37 2014b; He et al., 2014; Fu et al., 2016; Xue et al., 2016; Xie et al., 2015). During haze episodes, relative humidity 38 (RH) is often high (Zhang et al., 2014; Wang et al., 2016; Zheng et al., 2015b) and particles or some components 39 of particles can deliquesce forming liquid water. In particular, several recent studies propose that the multiphase 40 oxidation of SO<sub>2</sub> by NO<sub>2</sub>, another important air pollutant, on liquid particles may be a major pathway of sulfate 41 formation (Cheng et al., 2016; Wang et al., 2016; Xue et al., 2016; Xie et al., 2015). Both SO<sub>2</sub> and NO<sub>2</sub> are from 42 fossil fuel combustion and both concentrations are often high during haze episodes, and their reaction may 43 significantly contribute to sulfate formation.

44 In order to assess and quantify the role of the heterogeneous reactions of SO<sub>2</sub> in sulfate formation, laboratory 45 studies are needed to understand the reaction process and obtain kinetic parameters for modeling such as uptake coefficients of SO<sub>2</sub>. Among many studies investigating the heterogeneous reactions of SO<sub>2</sub> on various particles 46 47 (Goodman et al., 2001; Li et al., 2011; Shang et al., 2010; Huang et al., 2015; Huang et al., 2016; Zhou et al., 2014; Li et al., 2004; Kong et al., 2014; Passananti et al., 2016; Cui et al., 2008; Chu et al., 2016; Zhao et al., 48 49 2015; Li et al., 2006; Wu et al., 2011; He et al., 2014; Liu et al., 2012; Ma et al., 2008; Park and Jang, 2016; 50 Ullerstam et al., 2002; Sorimachi et al., 2001; Ullerstam et al., 2003; Wu et al., 2013; Wu et al., 2015), only a few 51 have investigated the heterogeneous reaction of SO<sub>2</sub> in the presence of NO<sub>2</sub> (He et al., 2014; Liu et al., 2012; Ma et al., 2008; Park and Jang, 2016; Ullerstam et al., 2003; Ma et al., 2017). These studies found that NO<sub>2</sub> can 52 53 promote sulfate formation from SO<sub>2</sub> oxidation (He et al., 2014; Liu et al., 2012; Ma et al., 2008; Park and Jang, 54 2016; Ullerstam et al., 2003). However, the mechanism of this effect is still not clear and only few studies 55 reported kinetic parameters such as uptake coefficient of SO<sub>2</sub> in the presence of NO<sub>2</sub>. Importantly, most of these 56 studies focused on the gas-solid reactions on particles. Very few laboratory studies have investigated the 57 multiphase reaction of  $SO_2$  with  $NO_2$  on atmospheric aqueous particles or solid-aqueous mixed phase aerosol





particles, and the uptake coefficient of  $SO_2$  on atmospheric aqueous particles due to the reaction with  $NO_2$  is largely unknown. From several decades ago until now, a number of studies have investigated the aqueous reaction of soluble S(IV) species ( $H_2SO_3$ ,  $HSO_3^-$ ,  $SO_3^{2-}$ ) with  $NO_2$  in dilute bulk solution (Lee and Schwartz, 1983; Ellison and Eckert, 1984; Clifton et al., 1988; Littlejohn et al., 1993) relevant to the conditions in cloud water. However, in aqueous aerosol particles, the reaction rate and process may be substantially different from in bulk solution due to high ion strength resulted from high concentrations of solutes, potential interactions of sulfate with other ions, and low water activity in aerosol particles.

65 In this study, we investigated the heterogeneous reaction of SO<sub>2</sub> with NO<sub>2</sub> on CaCO<sub>3</sub> particles at the ambient RH. CaCO<sub>3</sub> is an important component of mineral aerosols, especially in East Asia (Cao et al., 2005; Song et al., 66 67 2005; Okada et al., 2005) and it is a very reactive component (Krueger et al., 2004; Li et al., 2010; Li et al., 2006; Prince et al., 2007a). It is also one of the few alkaline particles in the atmosphere, especially in northern China, 68 69 which can neutralize acids on particles and increase the pH of aerosol water, thus promoting the apparent 70 solubility and uptake of SO<sub>2</sub>. The reaction of SO<sub>2</sub> with NO<sub>2</sub> on CaCO<sub>3</sub> has been suggested by field observations, 71 which showed internal mixing of CaCO<sub>3</sub>, CaSO<sub>4</sub>, and Ca(NO<sub>3</sub>)<sub>2</sub> in particles (Hwang and Ro, 2006; Li and Shao, 72 2009; Zhang et al., 2000). More importantly, as shown below, during the reaction on CaCO<sub>3</sub>, aqueous phase can 73 be formed, which allows us to investigate the multiphase reaction of SO<sub>2</sub> with NO<sub>2</sub>. We studied the reaction of 74 SO<sub>2</sub> and NO<sub>2</sub> on individual CaCO<sub>3</sub> particles using Micro-Raman spectrometer with a flow reaction system. 75 Combining the chemical and optical information from Micro-Raman spectrometer, we systematically 76 investigated the reaction process and quantified the reactive uptake coefficient of SO<sub>2</sub> due to the oxidation by NO<sub>2</sub> based on sulfate production rate. We further assessed the importance of the multiphase reaction of SO<sub>2</sub> with 77 78  $NO_2$  in the atmosphere. In this study, we present the findings of this reaction in  $N_2$ . We used  $N_2$  instead of air as a 79 carrier gas to exclude the inference of  $O_2$  in SO<sub>2</sub> oxidation, which is key to elucidate the direct oxidation of SO<sub>2</sub> 80 by NO<sub>2</sub>. In a companion paper we shall report the findings of the multiphase reaction of SO<sub>2</sub> with NO<sub>2</sub> in air to 81 explore the role of  $O_2$  in this reaction.

#### 82 2 Experimental

## 83 2.1 Apparatus and procedures

84 The experimental setup used in this study is illustrated in Fig. 1. The details of the setup have been described previously (Liu et al., 2008; Zhao et al., 2011). NO<sub>2</sub> and SO<sub>2</sub> of certain concentrations were prepared by adjusting 85 86 the flow rates of standard gases of specified concentrations (NO<sub>2</sub>: 1000 ppm in N<sub>2</sub>, Messer, Germany; SO<sub>2</sub>: 2000 87 ppm in N2, National Institute of Metrology P.R.China) and high-purity nitrogen (99.999%, Beijing 88 Haikeyuanchang Corp.). RH was regulated by adjusting the flow rates of humidified N2 and of dry N2 and other 89 dry gases. Humidified N2 was prepared by bubbling N2 through fritted glass in water. Flow rates of the gases were controlled by mass flow controllers (FC-260, Tylan, Germany). Mixed gases reacted with CaCO<sub>3</sub> particles 90 91 in a stainless steel reaction cell. Individual CaCO3 particles were deposited on a Teflon FEP film substrate 92 annealed to a silicon wafer. The substrate was then placed in the reaction cell, which has a glass cover on top of 93 the center. Through this top window, a Micro-Raman spectrometer (LabRam HR800, HORIBA Jobin Yvon) was 94 used to acquire the Raman spectra of particles. A 514 nm excitation laser was focused onto selected particles and





back scattering Raman signals were detected. The details of the instrument are described in previous studies (Liu
et al., 2008; Zhao et al., 2011).

97 The RH and temperature of the outflow gas from the reaction cell were measured by a hygrometer (HMT100,
98 Vaisala). Experiments of individual CaCO<sub>3</sub> particles reacting with NO<sub>2</sub> (75-200 ppm) and SO<sub>2</sub> (75-200 ppm)
99 mixing gas diluted with N<sub>2</sub> were conducted under certain RH (17-72%). All the measurements were carried out at

100  $25\pm0.5$  °C. Each reaction was repeated for three times.

101 In this study, the size of CaCO<sub>3</sub> particles was around 7-10 µm. During a reaction, components of an individual particle may distribute unevenly within the particle due to the formation of new aqueous phase or solid 102 103 phase, and particles may grow. Because particles are larger than the laser spot (~1.5 µm), Raman spectrum from 104 one point does not represent the chemical composition of the whole particle. Therefore Raman mapping was used 105 to obtain the spectra on different points of a particle in order to get the chemical information of the whole particle. 106 The mapping area is a rectangular slightly larger than the particle and mapping steps are 1×1 µm. Raman spectra in the range 800-3900 cm<sup>-1</sup> were acquired with exposure time of 1 s for each mapping point. During each 107 108 mapping (7-10 min, depending on the mapping area), no noticeable change in composition was detected. The 109 mean time of a mapping period was used as reaction time. During the reaction, microscopic images of particles 110 were also recorded. Raman spectra were analyzed using Labspec 5 software (HORIBA Jobin Yvon). Raman 111 peaks were fit to Gaussian-Lorentzian functions to obtain peak positions and peak areas on different points of the 112 particle. The peak areas were then added up to get the peak area for the whole particle.

Besides the reaction of CaCO<sub>3</sub> with SO<sub>2</sub> and NO<sub>2</sub>, other reaction systems including the reaction on Ca(NO<sub>3</sub>)<sub>2</sub>, NaNO<sub>3</sub>, NH<sub>4</sub>NO<sub>3</sub> particles with SO<sub>2</sub> or SO<sub>2</sub> and NO<sub>2</sub> mixing gas (summarized in Table 1) were also studied in order to elucidate the reaction mechanism.

CaCO<sub>3</sub> (98%, Sigma) with diameters about 7-10 μm on average, Ca(NO<sub>3</sub>)<sub>2</sub>·4H<sub>2</sub>O (ACS, 99-103%; Riedel-de
 Haën), NH<sub>4</sub>NO<sub>3</sub> (AR, Beijing Chemical Works), and NaNO<sub>3</sub> (AR, Beijing Chemical Works) were used without
 further purification.

- 119 2.2 Quantification of reaction products on the particle phase

120 The Raman intensity of a sample is described as Equation (1):

121 
$$I(v)=I_0 \bullet A(v) \bullet J(v) \bullet v^4 \bullet D \bullet K$$

(1)

where  $I_0$  is the intensity of incident laser, A(v) is the collection efficiency function of Raman spectrometer, 122 123  $J(v) \cdot v^4$  is the Raman scattering section of the sample, D is the number density of the sample, and K is the 124 effective depth of the sample. Raman intensity is not only determined by the amount of the sample molecules, but 125 also by the configuration of the instrument, whose influence cannot be eliminated unless internal standards are used. For soluble compounds, water can be used an internal standard (Zhao et al., 2011; Liu et al., 2008). 126 127 However, in this study, one product (CaSO<sub>4</sub>, see below) appeared as solid state. For solid particles of micro-scale, it is hard to add internal standards into the system. Therefore it is difficult to establish the relationship between 128 Raman intensity and the amount of sample molecules, which makes the quantification very challenging. 129 130 In this study, we chose seven individual  $CaSO_4$  particles varying in size as the standard for solid products.

131 The profile of each particle can be obtained by scanning the particle using Raman mapping with steps of 1, 1, and

132 2 µm for x, y, and z dimension, respectively. The volume of each particle was calculated based on 3D profiles of





133 the particles using a CAD software (AutoDesk). In order to minimize the influence variations of incident laser on

134 Raman intensity. These seven particles were measured before each experiment, which produced a calibration

135 curve for each experiment (Fig. S1).

## 136 2.3 Determination of reactive uptake coefficient

137 In this study, sulfate was produced from the oxidation of SO<sub>2</sub>. The reactive uptake coefficient  $\gamma$  of SO<sub>2</sub> on 138 individual particles was estimated from sulfate formation.  $\gamma$  is derived as the rate of sulfate formation 139 (d{SO<sub>4</sub><sup>2-</sup>}/dt) divided by the rate of surface collisions with an individual particle (Z),

140 
$$\gamma = \frac{\frac{d(SO_4^{2-})}{dt}}{Z}$$
. (2)  
141  $Z = \frac{1}{2}cA_S[SO_2],$  (3)

$$Z = \frac{1}{4} CA_s [SO_2],$$

$$142 \qquad \mathbf{c} = \sqrt{\frac{8RT}{\pi M_{SO_2}}} \quad , \tag{4}$$

where R is the gas constant, T is temperature,  $Mso_2$  is the molecular weight of  $SO_2$ , and c is the mean molecular velocity of  $SO_2$ ,  $A_s$  is the surface area of an individual particle. Z is the collision rate between  $SO_2$  and a particle.  $\{SO_4^{2-}\}$  indicates the amount of sulfate on the particle phase in mole, and  $[SO_2]$  indicates the concentration of  $SO_2$  in the gas phase.

 ${SO_4^{2-}}$  was determined by a calibration curve as stated above. In this study, since sulfate was mainly formed after the formation of Ca(NO<sub>3</sub>)<sub>2</sub> droplet as shown below, A<sub>s</sub> was calculated by estimating the diameter of the droplet according to its microscopic image and using a shape of spherical segment defined by the contact angle water droplet on Teflon (Good and Koo, 1979). For each experiment, at least three particles with different diameters were measured to get an average reactive uptake coefficient.

## 152 **3** Results and discussion

# 153 **3.1 Reaction products and particle morphology changes**

154 Figure 2 shows typical Raman spectra of a CaCO<sub>3</sub> particle during the reaction with SO<sub>2</sub> and NO<sub>2</sub>. The peak 155 at 1087 cm<sup>-1</sup> is assigned to the symmetric stretching mode of carbonate  $(v_1)$  (Nakamoto, 1997), which could be 156 detected during the initial stage of the reaction. Shortly after the reaction started, a peak at 1050 cm<sup>-1</sup> was 157 observed, which is attributed to the symmetric stretching mode of nitrate  $(v_1)$ . This demonstrates that calcium 158 nitrate (Ca(NO<sub>3</sub>)<sub>2</sub>) was produced during the reaction. A broad band at 2800-3800 cm<sup>-1</sup> was also observed together 159 with the formation of Ca(NO<sub>3</sub>)<sub>2</sub>. It is assigned to –OH stretching of liquid water. The formation of liquid water is attributed to the deliquescence of Ca(NO<sub>3</sub>)<sub>2</sub>, which is very hygroscopic and can deliquesce at ~10% RH (Liu et al., 160 161 2008; Al-Abadleh et al., 2003; Tang and Fung, 1997). After about 82 min, a new peak at 1013 cm<sup>-1</sup> was observed, 162 which is attributed to the symmetric stretching mode of sulfate  $(v_1)$  in anhydrite (CaSO<sub>4</sub>) (Sarma et al., 1998). 163 This peak clearly demonstrates that sulfate was formed. CaSO<sub>4</sub> as a reaction product has also been found in the 164 reaction of CaCO<sub>3</sub> with SO<sub>2</sub> and NO<sub>2</sub> in a previous study (Ma et al., 2013b). Afterwards, no other Raman peaks 165 than those of CaCO<sub>3</sub>, Ca(NO<sub>3</sub>)<sub>2</sub>, and CaSO<sub>4</sub> were detected until 1050 min after the reaction.





166 Concomitant with the formation of Ca(NO<sub>3</sub>)<sub>2</sub> and CaSO<sub>4</sub>, the microscopic morphology of the particle 167 changed significantly. The initial CaCO<sub>3</sub> particle was a crystal close to a rhombohedron of about 9-10 µm (Fig. 3a). After reacting with NO<sub>2</sub>/SO<sub>2</sub>, the surface of the particle became smoother, and then a liquid layer formed 168 169 surrounding the solid particle core (Fig. 3c). Raman spectra of the particle reveal that the outer liquid layer 170 consisted of Ca(NO<sub>3</sub>)<sub>2</sub> and water. As the reaction proceeded, the solid CaCO<sub>3</sub> core diminished gradually and 171 finally CaCO<sub>3</sub> was completely consumed and a Ca(NO<sub>3</sub>)<sub>2</sub> spherical droplet was formed (Fig. 3d). The whole 172 particle became larger due to the growth of the outer liquid layer. The diameter of the Ca(NO<sub>3</sub>)<sub>2</sub> droplet reached 173  $\sim 16 \,\mu$ m, and the droplet did not change much in the subsequent period of the reaction. Despite the invariant 174 droplet diameter, a new solid phase of needle-shaped crystals was formed as the reaction proceeded, which distributed unevenly in the droplet. The Raman spectra of the new solid phase and Raman mapping (Fig. S2) 175 176 reveal that this solid matter was CaSO<sub>4</sub>. The amount of CaSO<sub>4</sub> increased gradually during the reaction, and its 177 Raman peak could be observed more clearly at 1050 min.

#### 178 **3.2 Reaction process**

In order to learn about the reaction process and mechanism, the amounts of  $Ca(NO_3)_2$ ,  $CaSO_4$ , and  $CaCO_3$ , represented by the peak area at 1050, 1013, and 1087 cm<sup>-1</sup> in Raman spectra, respectively, were investigated as a function of reaction time. As shown in Fig. 4,  $Ca(NO_3)_2$  was produced before  $CaSO_4$ . Nitrate was detected immediately after the reaction started, and reached a maximum at ~50 min whereas sulfate did not reach the detection limit until 82 min of the reaction. Sulfate increased slowly in the reaction and we did not observe it leveling off even after 1050 min.

According to the time series of carbonate, nitrate, and sulfate, this reaction consisted of two successive processes. The first process was the formation of  $Ca(NO_3)_2$ , which was accompanied with the consumption of CaCO<sub>3</sub> (Fig. 4), indicating that  $Ca(NO_3)_2$  was produced due to the reaction of CaCO<sub>3</sub> with NO<sub>2</sub>. The detailed mechanism of the formation of  $Ca(NO_3)_2$  in the reaction  $CaCO_3$  with NO<sub>2</sub> have been studied by Li et al. (2010). The second process was the formation of  $CaSO_4$  through the oxidation of SO<sub>2</sub>. CaSO<sub>4</sub> was mainly produced after CaCO<sub>3</sub> was completely consumed and increased steadily as the reaction proceeded.

## 191 3.3 Reaction mechanism

#### 192 3.3.1 Mechanism of sulfate formation

Based on the results above, we found that a series of reactions of  $SO_2$  and  $NO_2$  on a CaCO<sub>3</sub> particle led to sulfate formation. Almost the entire sulfate was produced after a CaCO<sub>3</sub> particle was converted to a Ca(NO<sub>3</sub>)<sub>2</sub> droplet (Fig. 4), although in some experiments a trace amount of sulfate could be observed when a small amount of CaCO<sub>3</sub> was still left in the Ca(NO<sub>3</sub>)<sub>2</sub> droplet. The absence or low amount of sulfate before CaCO<sub>3</sub> was completely consumed might be due to the competition between the reaction of aqueous NO<sub>2</sub> with CaCO<sub>3</sub> and the reaction with SO<sub>2</sub>. This result suggests that forming a Ca(NO<sub>3</sub>)<sub>2</sub> droplet was key to the formation of sulfate.

This finding is further supported by the results of the reaction of  $SO_2$  with  $NO_2$  on a  $Ca(NO_3)_2$  droplet (Fig. 5 and Table 1). Using a  $Ca(NO_3)_2$  droplet as the reactant, the reaction with  $SO_2/NO_2$  at the same condition still produced  $CaSO_4$ , confirming  $CaCO_3$  was not necessary for sulfate formation. The reaction with  $Ca(NO_3)_2$ 





produced similar amount of sulfate to the reaction with  $CaCO_3$  based on Raman spectra and microscopic images (Fig. 5), which indicates that  $Ca(NO_3)_2$  droplet was important for sulfate formation. Therefore, we conclude that SO<sub>2</sub> was mainly oxidized via the multiphase reaction on the  $Ca(NO_3)_2$  droplet while  $CaCO_3$  mainly worked as a precursor of the  $Ca(NO_3)_2$  droplet.

The oxidant of SO<sub>2</sub> can be NO<sub>3</sub><sup>-</sup> or NO<sub>2</sub> in the Ca(NO<sub>3</sub>)<sub>2</sub> droplet here. In a reaction between Ca(NO<sub>3</sub>)<sub>2</sub> droplets and SO<sub>2</sub> (150 ppm) under 72% RH, we did not observe any sulfate formation on the basis of the Raman spectra and microscopic image after 5 h of reaction. This indicates that NO<sub>3</sub><sup>-</sup> was not the oxidant for SO<sub>2</sub> in our study, which was also consistent with a previous study (Martin et al., 1981). Therefore, we conclude that SO<sub>2</sub> was oxidized by NO<sub>2</sub> in the Ca(NO<sub>3</sub>)<sub>2</sub> droplet.

According to previous studies, NO<sub>2</sub> can oxidize sulfite and bisulfite ions into sulfate ion in aqueous phase
(Ellison and Eckert, 1984; Shen and Rochelle, 1998; Littlejohn et al., 1993). The overall mechanism was
described to be (Clifton et al., 1988):

214 
$$2NO_2(aq) + SO_3^{2-}(aq) + H_2O \rightarrow 2H^+ + 2NO_2^{-}(aq) + SO_4^{2-}(aq)$$
 (R1)

215  $2NO_2(aq) + HSO_3^{-}(aq) + H_2O \rightarrow 3H^+ + 2NO_2^{-}(aq) + SO_4^{2-}(aq)$  (R2)

Under the experimental conditions of our study, water uptake of  $Ca(NO_3)_2$  led to condensation of liquid water, which provided a site for aqueous oxidation of S(IV) by  $NO_2$ . The relative fractions of the three S(IV)species depend on pH and the equilibrium between them is fast (Seinfeld and Pandis, 2006). The pH of the droplet was mainly determined by the gas-aqueous equilibrium of  $SO_2$  in this study and estimated to be ~3 and thus main S(IV) species was  $HSO_3^-$ . Then  $SO_4^{2-}$  from S(IV) oxidation can react with  $Ca^{2+}$  forming  $CaSO_4$ precipitation as observed in Raman spectra due to the low value of  $K_{sp}$  for  $CaSO_4$  (Lide, 2009):

222 
$$\operatorname{Ca}^{2+}(\operatorname{aq}) + \operatorname{SO}_4^{2-}(\operatorname{aq}) \rightleftharpoons \operatorname{Ca}^{2-}(\operatorname{aq}) \rightleftharpoons$$

(R3)

Some previous studies have shown that  $SO_2$  can react with  $CaCO_3$  to produce calcium sulfite ( $CaSO_3$ ) (Li et al., 2006; Prince et al., 2007b; Ma et al., 2013a), and  $CaSO_3$  can be oxidized to  $CaSO_4$  by  $NO_2$  (Rosenberg and Grotta, 1980; Ma et al., 2013a). In our study, we investigated the reaction between  $CaCO_3$  and  $SO_2$  (150 ppm) at 72% RH. We found that both sulfate and sulfite were lower than the detection limit of our Raman spectrometer even after 300 min of the reaction. This indicates that forming  $CaSO_3$  was not the main pathway in  $CaSO_4$ formation in our study and  $CaCO_3$  did not directly contribute to the formation of  $CaSO_4$ .

## 229 **3.3.2** Effects of cations in sulfate formation

230 Since sulfate was observed to precipitate as  $CaSO_4$ , we further analyzed the effect of precipitation reaction 231 and cations on the aqueous oxidation of  $SO_2$  by  $NO_2$ . The spontaneity of the  $SO_2$  oxidation by  $NO_2$  for Reaction 232 (R2) can be analyzed using the reaction Gibbs energy as follows:

233 
$$\Delta_r G = \Delta_r G^{\theta} + RT ln \frac{a_{H^+}^3 a_{SO_4^2}^2 - a_{NO_2^-}^2}{a_{NO_2(aq)}^2 a_{HSO_3^-}^2}$$
(5)

where  $\Delta_r G$  is the reaction Gibbs energy,  $\Delta_r G^{\theta}$  is the standard reaction Gibbs energy, R is the gas constant, T is temperature, and a is the activity of various species.

The precipitation of CaSO<sub>4</sub> can substantially decrease the activity of  $SO_4^{2-}$ , and thus decrease  $\Delta_r G$  and promote the oxidation of SO<sub>2</sub> and sulfate formation. In order to test effects of cations, we replaced Ca<sup>2+</sup> with Na<sup>+</sup> or NH<sub>4</sub><sup>+</sup>. Based on Raman spectra, we found that in the reaction of a NaNO<sub>3</sub> or a NH<sub>4</sub>NO<sub>3</sub> droplet with NO<sub>2</sub>/SO<sub>2</sub>





239 no sulfate was formed after 300 min in the same reaction conditions as  $Ca(NO_3)_2$  and  $CaCO_3$  (Fig. 6 and Table 1). 240 Accordingly, no  $CaSO_4$  solid particles were observed in these droplets. Therefore, we concluded that the 241 precipitation of less soluble  $CaSO_4$  promoted the forward reaction, i.e., sulfate formation.

242 **3.4 Reactive uptake coefficient of SO<sub>2</sub>** 

243 The reactive uptake coefficients of SO<sub>2</sub> ( $\gamma$ ) for sulfate formation under different conditions are shown in 244 Table 2. Each reaction was repeated for three times, during which, three particles with different size were selected. y was higher at higher relative humidity, suggesting again that liquid water plays an important role in 245 the formation of CaSO<sub>4</sub>. At 17% RH, the reaction between CaCO<sub>3</sub> and NO<sub>2</sub> (the first process of the whole 246 247 reaction) proceeded very slowly, and the amount of liquid water formed due to the water uptake of  $Ca(NO_3)_2$  was very low. As a result, we did not observe the formation of CaSO<sub>4</sub> (the second process of the whole reaction) after 248 1000 min of the reaction and even at higher SO<sub>2</sub> and NO<sub>2</sub> concentrations (200 ppm SO<sub>2</sub>, 200 ppm NO<sub>2</sub>). Under 249 250 higher relative humidity (46% and 72% RH), sulfate was observed soon after the reaction. It is interesting to note 251 that there were no significant difference for  $\gamma$  between 46% and 72% RH. In either case, the reaction between 252 CaCO3 and NO2 proceeded quickly and CaCO3 was completely converted to a Ca(NO3)2 droplet within 100 min 253 after the reaction. In the presence of enough liquid water, RH seemed to be no longer a limiting factor. In such 254 conditions, an increase of NO<sub>2</sub> concentration (from 75 ppm to 200 ppm at 72% RH) promoted the reactive uptake 255 of SO<sub>2</sub>.

The reactive uptake coefficient of SO<sub>2</sub> for sulfate formation was determined to be on the order of  $10^{-8}$  at 46% 256 and 72% RH. This value is higher than the uptake coefficient (10<sup>-10</sup>) on mineral particles sampled from Cape 257 Verde Islands (the main contents being potassium feldspars and quartz) obtained by Ullerstam et al. (2003) using 258 259 NO<sub>2</sub>/SO<sub>2</sub> mixing gas and DRIFTS technique. But the uptake coefficient in this study is lower than the uptake coefficient of SO<sub>2</sub> on ATD particles in the presence of NO<sub>2</sub> ((2.10±0.08)×10<sup>-6</sup>) determined by Park and Jang 260 261 (2016).  $\gamma$  here is also much lower than the  $\gamma$  of SO<sub>2</sub> on oxalic acid particles in the presence of NO<sub>2</sub> and NH<sub>3</sub>  $(10^{-6} \sim 10^{-4})$  determined at varying RH reported by Wang et al. (2016). The difference in these uptake coefficients 262 263 is attributed to the different chemical composition of particles, reaction mechanism, reaction conditions, and the 264 ways that the particle surface is determined. It is worth noting that in the studies of Ullerstam et al. (2003) and 265 Park and Jang (2016), particles exist as solid state and sulfate formation is via gas-solid heterogeneous reaction, and in the study of Wang et al. (2016) sulfate formation is stated to be via aqueous reaction. In this study sulfate 266 267 formation was via gas-liquid-solid multiphase reaction and liquid water played a key role.

268 In the ambient atmosphere, the reactive uptake coefficient of  $SO_2$  due to the multiphase oxidation by  $NO_2$  is influenced by various factors such as RH, NO<sub>2</sub> concentration, pH, sulfate concentration, and the presence of other 269 ions in aerosol particles. For example, NO<sub>2</sub> concentrations in the atmosphere are much lower than those used in 270 271 this study. At lower NO<sub>2</sub> concentrations, the uptake coefficient of SO<sub>2</sub> decreases, because the oxidation rate of 272 SO<sub>2</sub> in aqueous phase decreases with decreasing NO<sub>2</sub> concentration. In addition, aqueous sulfate concentrations 273 in aerosol particles in the atmosphere are often high, which may suppress the reaction of SO<sub>2</sub> with NO<sub>2</sub> according 274 to the discussion above and Equation (5), and thus reduce the uptake coefficient of SO<sub>2</sub>. Therefore, the reactive 275 uptake coefficient of SO<sub>2</sub> obtained in this study ( $10^{-8}$  at 46-72% RH and 75 ppm NO<sub>2</sub>) can be regarded as an





upper limit of the reactive uptake coefficient of  $SO_2$  due to the multiphase reaction with  $NO_2$  in the ambient atmosphere.

#### 278 4 Conclusion and implications

279 We investigated the heterogeneous reaction of SO<sub>2</sub> with NO<sub>2</sub> on individual CaCO<sub>3</sub> particles in N<sub>2</sub> using Micro-Raman spectrometry. The reaction first converted the  $CaCO_3$  particle to the  $Ca(NO_3)_2$  droplet via the 280 reaction with NO2 in the SO2/NO2/H2O/N2 gas mixture and the deliquescence of Ca(NO3)2, and then formed 281 282 needle-shaped  $CaSO_4$  crystals in the  $Ca(NO_3)_2$  droplet via the multiphase reaction of SO<sub>2</sub> with NO<sub>2</sub>. The sulfate 283 formation was observed only during the multiphase oxidation by NO<sub>2</sub>, that is, after the complete conversion of  $CaCO_3$  to  $Ca(NO_3)_2$  droplet. The precipitation of  $CaSO_4$  from solution promoted sulfate formation. The reactive 284 uptake coefficient of SO<sub>2</sub> for sulfate formation in the multiphase reaction with NO<sub>2</sub> is on the order of  $10^8$  under 285 the experimental conditions of this study (RH: 46-72%, NO<sub>2</sub>: 75 ppm). The reactive uptake coefficient of SO<sub>2</sub> 286 287 was found to be enhanced at higher RH.

288 In order to assess the importance of the multiphase reaction of  $SO_2$  directly oxidized by  $NO_2$  to sulfate in the 289 atmosphere, we compare the lifetime of SO<sub>2</sub> due to the multiphase oxidation of SO<sub>2</sub> by NO<sub>2</sub> with the lifetime due to the gas phase oxidation of SO<sub>2</sub> by OH. Using a daytime OH concentration of  $1 \times 10^6$  molecule cm<sup>-3</sup> (Lelieveld 290 et al., 2016; Prinn et al., 2005), the lifetime of SO<sub>2</sub> in the atmosphere due to gas phase OH oxidation is around 12 291 292 days. The life time of SO<sub>2</sub> due to the multiphase oxidation by NO<sub>2</sub> is around 7000 days using the uptake 293 coefficient of SO<sub>2</sub> from this study  $(3.22 \times 10^{-8})$  and a typical particle surface area concentration for mineral aerosols in winter in Beijing (6.3×10<sup>-6</sup> cm<sup>-2</sup>) (Huang et al., 2015). Using an annual average particle surface 294 area concentration of  $PM_{10}$  in Beijing (1.4×10<sup>-5</sup> cm<sup>-3</sup>)(Wehner et al., 2008) results in a SO<sub>2</sub> life time of 3300 295 296 days due to the multiphase oxidation by NO<sub>2</sub>. In the atmosphere, the lifetime of  $SO_2$  due to the multiphase oxidation by NO<sub>2</sub> should be even longer than these values because the uptake coefficient of SO<sub>2</sub> used here 297  $(3.22 \times 10^{-8})$  is an upper limit of the uptake coefficient of SO<sub>2</sub> in the ambient atmosphere as discussed above. This 298 comparison indicates that the direct multiphase oxidation of SO<sub>2</sub> by NO<sub>2</sub> is not an important sink of SO<sub>2</sub> and 299 source of sulfate compared with the oxidation of SO<sub>2</sub> by OH. 300

In this study, we used the inert  $N_2$  as a carrier gas for the reaction mixture. In the ambient atmosphere,  $O_2$  is abundantly present and previous studies have suggested that  $O_2$  can enhance the reaction of sulfite with  $NO_2$  in bulk aqueous solution (Littlejohn et al., 1993). Therefore, the potential role of  $O_2$  in the reaction of  $SO_2$  with  $NO_2$ in aqueous aerosol particles warrants further studies and will be addressed in a companion paper.

Despite the less important role in sulfate formation, the multiphase oxidation of  $SO_2$  by  $NO_2$  on  $CaCO_3$ particles helps interpreting the findings from field studies. For example, internally mixed  $CaCO_3$  with  $Ca(NO_3)_2$ and  $CaSO_4$  particles with varying reacted fractions of  $CaCO_3$  were observed in the field (Hwang and Ro, 2006; Li and Shao, 2009), but how the internally mixed particles are formed is not clear. In this study we showed that  $CaSO_4$  can be formed inside the  $Ca(NO_3)_2$  droplet after the deliquescence of initially produced  $Ca(NO_3)_2$  through the reaction of  $SO_2$  with  $NO_2$ . In this way, internally mixed  $CaCO_3$  with  $Ca(NO_3)_2$  and  $CaSO_4$  particles can be formed. Moreover, Hwang and Ro (2006) found that  $CaSO_4$ -containing particles were observed to be almost





- 312 always internally mixed with nitrate. The multiphase reaction process of SO<sub>2</sub> with NO<sub>2</sub> on CaCO<sub>3</sub> particles found
- 313 this study can also explain this finding.
- 314
- 315 Acknowledgements
- 316 This work was supported by Natural Science Foundation Committee of China (41421064, 21190051,
- 317 40490265) and Ministry of Science and Technology (Grant No. 2002CB410802).





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Atmos. Chem. Phys. Discuss., https://doi.org/10.5194/acp-2017-610 Manuscript under review for journal Atmos. Chem. Phys. Discussion started: 3 July 2017

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# 502 Table 1 Summary of the results obtained in different reaction systems

| Particle                                  | Gases   | RH (%) | Whether sulfate was<br>detected |
|---|---|--------|---------------------------------|
| CaCO <sub>3</sub>                         | SO <sub>2</sub> (75 ppm)+NO <sub>2</sub> (75 ppm) | 72     | Yes                             |
| Ca(NO <sub>3</sub> ) <sub>2</sub> droplet | SO <sub>2</sub> (75 ppm)+NO <sub>2</sub> (75 ppm) | 72     | Yes                             |
| CaCO <sub>3</sub>                         | SO <sub>2</sub> (150 ppm)                         | 72     | No                              |
| Ca(NO <sub>3</sub> ) <sub>2</sub> droplet | SO <sub>2</sub> (150 ppm))                        | 72     | No                              |
| NaNO <sub>3</sub> droplet                 | SO <sub>2</sub> (75 ppm)+NO <sub>2</sub> (75 ppm) | 72     | No                              |
| NH <sub>4</sub> NO <sub>3</sub> droplet   | SO <sub>2</sub> (75 ppm)+NO <sub>2</sub> (75 ppm) | 72     | No                              |





- 504 Table 2. Reactive uptake coefficient of SO<sub>2</sub> for sulfate formation ( $\gamma$ ) during the reaction of SO<sub>2</sub> with NO<sub>2</sub> on
- 505 individual CaCO<sub>3</sub> particles under different conditions at 298 K.

| [SO <sub>2</sub> ] | [NO <sub>2</sub> ] | RH  | γ (×10 <sup>-8</sup> ) |
|--------------------|--------------------|-----|------------------------|
| (ppm)              | (ppm)              | (%) |                        |
| 75                 | 75                 | 72  | 3.22±1.08              |
| 75                 | 200                | 72  | 16.0±3.12              |
| 75                 | 75                 | 46  | 3.22±0.90              |
| 75                 | 75                 | 17  | $0^{a}$                |
| 200                | 200                | 17  | $0^{a}$                |

506 <sup>a</sup>: Sulfate was below the detection limit.









508 Fig. 1. Schematic diagram of the experimental setup. MFC: mass flow controller.







509

510 Fig. 2. Raman spectra of an individual CaCO<sub>3</sub> particle during the reaction with NO<sub>2</sub> (75 ppm) and SO<sub>2</sub> (75 ppm)

511 at 72% RH at the reaction time of 0, 8, 30, 95, and 1050 min.







512

513 Fig. 3. Microscopic images of an individual CaCO<sub>3</sub> particle (same as in Fig. 2) reacting with NO<sub>2</sub> (75 ppm) and

514 SO<sub>2</sub> (75 ppm) at 72% RH. a-f corresponds to the reaction time of 0, 6, 29, 37, 94, and 1050 min, respectively.







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Fig. 4. Raman peak intensity of carbonate, nitrate (left axis), and sulfate (right axis) as a function of time during the reaction of an individual CaCO<sub>3</sub> particle with NO<sub>2</sub> (75ppm) and SO<sub>2</sub> (75ppm) at 72% RH (same as in Fig. 2 and 3). Note that the scales of the left axis and right axis are different. The intensity of NO<sub>3</sub><sup>-</sup>, SO<sub>4</sub><sup>2-</sup>, and CO<sub>3</sub><sup>2-</sup> show the peak area at 1050, 1013, and 1087 cm<sup>-1</sup>, respectively, in Raman spectra obtained by Raman mapping.





522





524 Fig. 5. Raman spectra (a) and microscopic image (b) of a  $Ca(NO_3)_2$  droplet reacting with  $NO_2$  (75 ppm) and  $SO_2$ 

525 (75 ppm) at 72% RH at a reaction time of 300 min. The peak at 1014 cm<sup>-1</sup> in Raman spectra and crystals from the

526 microscopic image indicate CaSO<sub>4</sub> was formed in this reaction.





527



529 Fig. 6. Raman spectra of a NH<sub>4</sub>NO<sub>3</sub> (a) and NaNO<sub>3</sub> (b) droplet reacting with NO<sub>2</sub> (75 ppm) and SO<sub>2</sub> (75 ppm) at

530 72% RH at the reaction time of 300 min.

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