

## Response to the comments of Anonymous Reviewer #1

Reviewer 1:

After carefully reviewing the revised version of the manuscript, it is apparent that the author spent a decent amount of effort to improve the clarity and readability of the manuscript, as well as discussing the assumptions and limitations of the method in greater detail. Even though this manuscript is a continuation of the previously published work of the author, there are several parts of the manuscript that are innovative and contain enough scientific significance to be published on ACP, including (1) using a new (and improved) formula to estimate the viscosity; (2) a comparison of the estimated viscosity with measurements from laboratory generated SOAs; (3) an estimation of the viscosity with different mass loadings; and (4) an estimation of the viscosity of the organic component of the biomass burning aerosols based on molecular composition. Just like any other models, this model has to make certain assumptions and is not perfect (also as reviewer 1 mentioned), but it is still important because it is one of the few so far that can estimate the viscosity of small organic mixtures (such as SOA), which will benefit the atmospheric community. Readers will be able to use the model from this manuscript to estimate viscosity of SOA-like mixtures, and some readers may even be able to further improve the model in the future. This paper certainly meets the publication standard for ACP. After reviewing the manuscript, there are a few parts that should be modified to be clearer to readers.

Responses:

We thank Anonymous Reviewer #1 for the thorough review and positive evaluation of our revised manuscript. Based on your constructive suggestions for improvement, we have made revisions as below.

Reviewer Comment 1:

Line 87-88. The author mentioned a piece of negative experimental evidence: “Gorkowski et al. (2017) did not observe significant diffusion limitations for glycerol and squalene in  $\alpha$ -pinene SOA. Quasi-equilibrium versus kinetically-limited or non-equilibrium SOA growth remains an open issue and warrants further investigations.” However, in a few other papers that the author mentioned (such as Abramson et al. PCCP, 2013, Zhang et al. ES&T Letters, 2018), there is positive experimental evidence showing that there are kinetic limitations regarding SOA evaporation, diffusion, and formation from multiphase reactions. It is better to mention these positive findings together with the Gorkowski et al. results to provide a more balanced viewpoint.

We agree and have added the following text in introduction:

“Several studies have observed kinetic limitations of bulk diffusion of organic molecules including polycyclic aromatic hydrocarbons (Abramson et al., 2013; Zhou et al., 2013) and isoprene-derived epoxydiols (Zhang et al., 2018) in SOA, while Gorkowski et al. (2017) did not observe significant diffusion limitations for glycerol and squalene in  $\alpha$ -pinene SOA.”

Reviewer Comment 2:

Line 318, 523. As previously discussed, the author agrees that the isoprene SOA generated from the PAM might be different from the ambient isoprene-derived SOA due to

different reaction mechanisms. So I would recommend to change “isoprene SOA” to “PAMgenerated isoprene SOA” in line 318, 523, and other parts of the manuscript, so as to avoid generalization of the isoprene SOA.

We agree and we clarify this point in the revised manuscript.

Reviewer Comment 3:

The Bateman et al. results in Figure 4 and Figure 6 are not consistent with the same result in Figure 7. As review #1 mentioned, bounce results are not accurate in measuring viscosity, but the transition from bounce to non-bounce can provide a small viscosity range where a particle changes its phase state from semi-solid to liquid. If a particle does not bounce, it should be liquid. But if a particle does bounce, it may still have a relative low viscosity that will not cause diffusion limitation. According to Bateman et al. (JPC A, 2015) and Reid et al. (Nature Communication, 2018), the bounce results shown in Bateman et al. (Nature Geoscience, 2015) should be in the range of 100-102 Pa s, corresponding to RH 60-80%. In Figure 4 and 6, the author assigned the RH to be 40-60%, which is different from Figure 7, where the RH range was 60-80%. Please make the RH in all Figures to 60-80%. The text that contains 40-60% needs to be changed to 60-80%, too.

It is actually consistent: Bateman et al. 2015 found that the semi-solid to liquid transition occurs at different thresholds for different types of SOA. Figures 4 (b) and 6 show the viscosity range Bateman et al. observed for isoprene SOA. Figure 7 includes the data for toluene SOA reported by Bateman et al. To clarify this detail, we have revised the manuscript as follows:

Sect. 3.2: “Indirect viscosity measurements are also included in shaded boxes for toluene-derived SOA (Bateman et al., 2015; Li et al., 2015).”

Fig. 4 caption: “The gray box in panel (b) represents estimated viscosity for isoprene SOA based on bounce measurements of Bateman et al. (2015).”

Reviewer Comment 4:

Line 444-446: the author says the O:C ratios based on nano-DESI-HERM was lower than the O:C reported by Song et al. (2016). So why a lower O:C ratio results in higher viscosity estimation then? In line 493-494, the author states that higher O:C ratio will result in a higher viscosity estimation, which is contrary to how the author explained the data in line 444-446. The part may need to be revised to proper explain the difference between the model and the measurement.

SOA were formed in different conditions by Song et al. and Hinks et al., so not only O:C ratio, but also distribution of oxidation products could be different in these studies, leading to uncertainties in viscosity estimation. This is certainly a limitation in current study and simultaneous measurements of chemical composition and viscosity are encouraged in future studies (as emphasized in the last sentence of abstract). Higher O:C would lead to higher glass transition temperature, but not necessarily to higher viscosity, as higher O:C may lead to an increase of hygroscopicity. This was confusing, so we revised the sentence as below.

Sect. 3.3: "..., which typically have higher O:C ratios and therefore would result in higher predicted values of glass transition temperature (Koop et al., 2011; Saukko et al., 2012)."

Reviewer Comment 5:

Line 500-501: the author should add "providing the upper limit of the viscosity of the organic component, while APPI MS gives the lower limit", to make it more clear that the predictions are only applicable to organic component rather than the whole biomass burning aerosols.

Following your comment, we clarified this point in the revised manuscript.

Reviewer Comment 6:

Line 908, the table and the text overlap with each other. Please fix that.

We have increased the space between the table and the text.

Reviewer Comment 7:

One general suggestion I have is about the figures. Figure 1 looks very much like the author's other paper on Nature Communications. It could give people the wrong impression that this was a similar paper compared with the old one, but actually this paper contains a decent amount of new information. In this future it is probably better to modify the figures not to be so similar to previous published ones when the author writes a follow up paper, so as to avoid confusion for the readers. But I understand why the author uses this style this time and no changes are needed from me for this draft.

Thank you for this comment. We would like to leave the figure as is, but will keep this observation in mind in the future.

Reviewer Comment 8:

One last comment I have is the using of the fragility parameter D. I think the current model is fine using different D values to predict the viscosity. But more recent physical chemistry theory about liquid/glass relaxation has been improved so that all D values could collapse into one single uniformed equation Elmatad et al. (JPC B, 2009). All the experimental data agree nicely with the new theory without introducing the D value. Maybe the author can consider that applying this theory to the viscosity estimation in the future.

We appreciate this suggestion and we will consider this treatment in our future studies.

Overall, this article provides an improved model of estimating glass transition temperature and viscosity of organic components that can extend to molar mass of up to 1100 g mol<sup>-1</sup>. The study cross compares with literature data and molecular measurement of the biomass burning aerosols to show the validity of the model. The manuscript reads well especially after the second revision, and is suitable to be published on ACP.

Thanks again for positive evaluation of our manuscript.

## References

Bateman, A. P., et al. (2015). "Sub-Micrometre Particulate Matter Is Primarily in Liquid Form over Amazon Rainforest." *Nature Geoscience* 9: 34.

Elmatad, Y. S., et al. (2009). "Corresponding States of Structural Glass Formers." *J. Phys. Chem. B.* 113(16): 5563-5567.

Abramson, E., et al. (2013). "Experimental Determination of Chemical Diffusion within Secondary Organic Aerosol Particles." *Phys. Chem. Chem. Phys.* 15(8): 2983-2991.  
Reid, J. P., et al. (2018). "The Viscosity of Atmospherically Relevant Organic Particles." *Nat. Commun.* 9(1): 956.

Song, M., et al. (2015). "Relative Humidity-Dependent Viscosities of Isoprene-Derived Secondary Organic Material and Atmospheric Implications for Isoprene-Dominant Forests." *Atmos. Chem. Phys.* 15(9): 5145-5159.

Zhang, Y., et al. (2018). "Effect of Aerosol-Phase State on Secondary Organic Aerosol Formation from the Reactive Uptake of Isoprene-Derived Epoxydiols (Iepox)." *Environ. Sci. Technol. Lett.* 5(3): 167-174.

## **Response to the comments of Anonymous Reviewer #2**

Reviewer

2:

The authors have done a reasonably satisfactory job of addressing most of the questions and concerns raised during peer-review. With its focus on estimating only the glass transition temperature and viscosity, and not the actual diffusivity and equilibration timescales, I still do not find much scientific value to this approach. All that has really been accomplished is to extend their previous model to include larger MW organics. However, the manuscript has improved during review and is now of an acceptable quality to recommend publication, after they address the major criticism in my original review that they have tried to side-step in their rebuttal (please see below). Although I rate the significance and originality of this manuscript to be rather low for ACP standards, we can let the community decide over time if this is a useful advance in our understanding of organic aerosol particles. Their rebuttal that the (superior, in my opinion) functional group-based method for estimating viscosity by Rothuff and Petters cannot account for mixed organic aerosol systems is well taken. The ability of these author's approach (extended here to higher molecular weights) to model mixtures is a positive attribute. The critical issue which the authors tried to avoid directly addressing in their rebuttal and revisions concerns the real need for a better understanding of diffusivity and equilibration timescales in atmospheric particles. Viscosity and T<sub>g</sub>, which is all this paper focuses on, is indirectly related to diffusivity, but does not provide the information required to understand equilibration timescales, or any of the other important processes the authors lay out in the paper's introduction to motivate their work. Throughout their rebuttal in response to my questions regarding the importance of diffusivity they just state "estimations of bulk diffusivity and mixing timescales are beyond the scope of this study". And this is why I do not find much merit to what is being reported in this manuscript. It is fine if the authors wish to restrict this paper to only consider T<sub>g</sub> and viscosity,

but then the authors MUST significantly modify their introduction and conclusions to make it clear to readers what exactly can and can NOT be learned from viscosity in relation to all the critical processes they outline in the introduction. Without making these necessary revisions, the authors are frankly being somewhat deceptive by presenting their viscosity-limited work as though it can directly advance our understanding of critical atmospheric physics and chemistry. To borrow from their introduction (from their revised manuscript), here are some of the processes they outline in such a way that the reader is led to believe their viscosity estimates will advance our understanding of these same processes (my emphasis):  
Line 64: “The particle phase state has been shown to affect gas uptake and chemical transformation of organic compounds due to kinetic limitations of bulk diffusion”

Line 70: “Water diffusion can be still fast even in an amorphous solid matrix under room temperature, but it can be hindered significantly under low temperatures (Mikhailov et al., 2009; Zobrist et al., 2011; Bones et al., 2012; Berkemeier et al., 2014; Price et al., 2014), affecting homogeneous vs. heterogeneous ice nucleation pathways”

Line 79: “Partitioning of semi-volatile compounds into viscous particles may result in kinetically-limited growth in contrast to quasi-equilibrium growth (Perraud et al., 2012; Shiraiwa and 81 Seinfeld, 2012; Booth et al., 2014; Zaveri et al., 2014; Mai et al., 2015; Liu et al., 2016), which also affects the evolution of particle size distribution upon SOA growth (Shiraiwa et al., 2013; Zaveri et al., 2018). Chamber experiments probing mixing timescales of SOA particles derived by oxidation of various precursors such as isoprene, terpene, and toluene have observed strong kinetic limitations at low RH, but not at moderate and high RH (Loza et al., 2013; Ye et al., 2016; Ye et al., 2018). Gorkowski et al. (2017) did not observe significant diffusion limitations for glycerol and squalene in  $\alpha$ -pinene SOA. Quasi-equilibrium versus kinetically-limited or non-equilibrium SOA growth remains an open issue and warrants further investigations.”

This is certainly a nice introduction that discusses many of these important and uncertain processes, with good references to recent findings. Unfortunately, estimating only the glass transition temperature (and thus phase state and viscosity) tells us very little about diffusivity, equilibrium timescales, heterogeneous ice nucleation, kinetic-limitations to particle growth, etc. Yet the introduction gives the reader the strong impression that the new results presented in this paper will in fact advance our understanding of these critical processes. To summarize, the authors need to be much more upfront regarding what can and what cannot be learned just from their estimates of the glass transition temperature, and the phase state and viscosity they estimate from  $T_g$ .

We thank the reviewer to the thorough reading of the manuscript and offering his/her perspective on the material presented in this paper. We agree that diffusivity and equilibration timescales are key in effects of phase state on gas-particle interactions. We respectfully disagree, however, that that “viscosity tells very little about diffusivity”. Although no attempt was made in this study to estimate diffusivity, a well-established Stokes-Einstein equation provides a direct path to diffusivity based on viscosity values presented in our study. We would like to point out that viscosity and diffusivity are directly connected by the Stokes-Einstein relation, which was first proposed by Einstein (1905) and validated with numerous experiments in the field of physical chemistry chemical physics and material science over the last century. In fact, it has been established as textbook knowledge; for example, please see the textbooks of physical chemistry (Atkins, 1998), glass science (Schmelzer and Gutzow, 2011), which has been applied in

atmospheric chemistry (Seinfeld and Pandis, 2006). We do acknowledge that this relation has some limitations that it is not applicable for bulk diffusivity of small molecules and it may also deviate for diffusion of organic molecules in highly viscous matrix by a few orders of magnitudes, as recently demonstrated by some experiments. The SE relation has been shown to work well for organic molecules with viscosity up to  $\sim 10^3$  Pa s, and above this viscosity SE can give lower limits, which is still often very useful (Price et al., 2016; Chenyakin et al., 2017). There are substantial numbers of studies, which demonstrated effects of viscosity and bulk diffusivity on gas-particle interactions, as cited in the manuscript. Equilibration timescale of SOA partitioning is not only determined by bulk diffusivity or viscosity, but also affected by other factors such as volatility, accommodation coefficient, particle size and mass loadings. We plan to conduct research on this topic in the follow-up studies. In response to the comments of reviewer 2, we elected to keep the overall flow of logic in the introduction unchanged. However, we have added the following text in introduction to clarify the relationship between viscosity, diffusivity and equilibrium timescales:

“Viscosity can be directly converted to bulk diffusivity of organic molecules using the Stokes-Einstein equation (Einstein, 1905; Atkins, 1998; Seinfeld and Pandis, 2006; Schmelzer and Gutzow, 2011). This has been shown to work well for organic molecules diffusing through materials with  $\eta$  below  $\sim 10^3$  Pa s (Price et al., 2016; Chenyakin et al., 2017). Note that this relation is not accurate for predicting the bulk diffusivity of water and small molecules and it may also underestimate diffusivity of organic molecules in highly viscous matrix by a few orders of magnitudes (Champion et al., 2000; Shiraiwa et al., 2011; Power et al., 2013; Marshall et al., 2016; Bastelberger et al., 2017; Reid et al., 2018).”

“Note that the equilibration timescale of SOA partitioning is not only determined by bulk diffusivity or viscosity, but also affected by other factors such as volatility, accommodation coefficient, particle size and mass loadings (Shiraiwa and Seinfeld, 2012; Mai et al., 2015; Liu et al., 2016).”

1 **Predicting the glass transition temperature and viscosity of secondary**  
2 **organic material using molecular composition**

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4

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15 *Submitted to Atmospheric Chemistry and Physics (ACP)*

16

17 **Abstract:**

18 Secondary organic aerosols (SOA) account for a large fraction of submicron particles in the  
19 atmosphere. SOA can occur in amorphous solid or semi-solid phase states depending on  
20 chemical composition, relative humidity (RH), and temperature. The phase transition between  
21 amorphous solid and semi-solid states occurs at the glass transition temperature ( $T_g$ ). We have  
22 recently developed a method to estimate  $T_g$  of pure compounds containing carbon, hydrogen, and  
23 oxygen atoms (CHO compounds) with molar mass less than 450 g mol<sup>-1</sup> based on their molar  
24 mass and atomic O:C ratio. In this study, we refine and extend this method for CH and CHO  
25 compounds with molar mass up to ~1100 g mol<sup>-1</sup> using the number of carbon, hydrogen, and  
26 oxygen atoms. We predict viscosity from the  $T_g$ -scaled Arrhenius plot of fragility (viscosity vs.  
27  $T_g/T$ ) as a function of the fragility parameter  $D$ . We compiled  $D$  values of organic compounds  
28 from literature, and found that  $D$  approaches a lower limit of ~10 (+/- 1.7) as the molar mass  
29 increases. We estimated viscosity of  $\alpha$ -pinene and isoprene SOA as a function of RH by  
30 accounting for hygroscopic growth of SOA and applying the Gordon-Taylor mixing rule,  
31 reproducing previously published experimental measurements very well. Sensitivity studies were  
32 conducted to evaluate impacts of  $T_g$ ,  $D$ , hygroscopicity parameter ( $\kappa$ ), and the Gordon-Taylor  
33 constant on viscosity predictions. Viscosity of toluene SOA was predicted using the elemental  
34 composition obtained by high-resolution mass spectrometry (HRMS), resulting in a good  
35 agreement with the measured viscosity. We also estimated viscosity of biomass burning particles  
36 using the chemical composition measured by HRMS with two different ionization techniques:  
37 electrospray ionization (ESI) and atmospheric pressure photoionization (APPI). Due to  
38 differences in detected organic compounds and signal intensity, predicted viscosities at low RH  
39 based on ESI and APPI measurements differ by 2-5 orders of magnitude. Complementary



40 measurements of viscosity and chemical composition are desired to further constrain RH-  
41 dependent viscosity in future studies.

42

## 43 **1. Introduction**

44 Secondary organic aerosols (SOA) account for a large fraction of submicron particles in the  
45 atmosphere and they play an important role in climate, air quality and public health (Goldstein  
46 and Galbally, 2007; Jimenez et al., 2009). Traditionally, SOA particles were assumed to be  
47 liquid with dynamic viscosity  $\eta$  below  $10^2$  Pa s, but a number of recent studies have shown that  
48 they can also adopt amorphous semi-solid ( $10^2 \leq \eta \leq 10^{12}$  Pa s), or glassy solid ( $\eta > 10^{12}$  Pa s)  
49 states, depending on chemical composition and temperature (Zobrist et al., 2008; Koop et al.,  
50 2011; Huang et al., 2018; Reid et al., 2018). The phase state is also strongly affected by relative  
51 humidity, as water can act as a plasticizer to lower viscosity (Mikhailov et al., 2009). Ambient  
52 and laboratory-generated SOA particles have been observed to bounce off the smooth hard  
53 surface of an inertial impactor at low RH, implying a non-liquid state (Virtanen et al., 2010;  
54 Saukko et al., 2012; Bateman et al., 2015; Jain and Petrucci, 2015), whereas predominantly  
55 biogenic SOA particles in the Amazon basin did not bounce off the impactor surface at high RH,  
56 implying they are primarily liquid (Bateman et al., 2016). Upon dilution or heating, SOA  
57 particles were observed to evaporate unexpectedly slowly (Cappa and Wilson, 2011; Vaden et  
58 al., 2011), and recent modeling studies have evaluated the contributions of low diffusivity and  
59 volatility to slow evaporation rates (Roldin et al., 2014; Yli-Juuti et al., 2017). Measurements of  
60 viscosity of SOA bulk material derived from oxidation of  $\alpha$ -pinene (Renbaum-Wolff et al., 2013;  
61 Zhang et al., 2015; Hosny et al., 2016), limonene (Hinks et al., 2016), isoprene (Song et al.,

62 2015), and toluene (Song et al., 2016a) have confirmed that SOA particles adopt a wide range of  
63 viscosities.

64 Viscosity can be directly converted to bulk diffusivity of organic molecules using the  
65 Stokes-Einstein equation (Einstein, 1905; Atkins, 1998; Seinfeld and Pandis, 2006; Schmelzer  
66 and Gutzow, 2011). This equation has been shown to work well for organic molecules diffusing  
67 through materials with  $\eta$  below  $\sim 10^3$  Pa s (Price et al., 2016; Chenyakin et al., 2017). Note that  
68 this relation is not accurate for predicting the bulk diffusivity of water and small molecules and it  
69 may also underestimate diffusivity of organic molecules in highly viscous matrix by a few orders  
70 of magnitudes (Champion et al., 2000; Shiraiwa et al., 2011; Power et al., 2013; Marshall et al.,  
71 2016; Bastelberger et al., 2017; Reid et al., 2018). The particle phase state, viscosity and bulk  
72 diffusivity have been shown to affect gas uptake and chemical transformation of organic  
73 compounds due to kinetic limitations of bulk diffusion (Shiraiwa et al., 2011; Abbatt et al., 2012;  
74 Kuwata and Martin, 2012; Zhou et al., 2013; Slade and Knopf, 2014; Arangio et al., 2015;  
75 Davies and Wilson, 2015; Wang et al., 2015; Berkemeier et al., 2016; Marshall et al., 2016; Liu  
76 et al., 2018; Pratap et al., 2018; Zhang et al., 2018), which may facilitate long-range transport of  
77 organic compounds embedded in viscous or glassy particles (Shrivastava et al., 2017b; Mu et al.,  
78 2018). Molecular motion can be hindered in a highly viscous matrix, slowing down  
79 photochemical reactions in particles (Lignell et al., 2014; Hinks et al., 2016). Water diffusion can  
80 be still fast even in an amorphous solid matrix under room temperature, but it can be hindered  
81 significantly under low temperatures (Mikhailov et al., 2009; Zobrist et al., 2011; Bones et al.,  
82 2012; Berkemeier et al., 2014; Price et al., 2014), affecting homogeneous vs. heterogeneous ice  
83 nucleation pathways (Murray et al., 2010; Wagner et al., 2012; Wang et al., 2012a; Wang et al.,  
84 2012b; Wilson et al., 2012; Baustian et al., 2013; Schill and Tolbert, 2013; Berkemeier et al.,

85 2014; Schill et al., 2014; Lienhard et al., 2015; Ignatius et al., 2016; Knopf et al., 2018). Despite  
86 the substantial implications of the SOA particle phase state, its effects on gas-particle  
87 interactions have not yet been considered explicitly in current climate and air quality models  
88 (Shrivastava et al., 2017a).

89         Partitioning of semi-volatile compounds into viscous particles may result in kinetically-  
90 limited growth in contrast to quasi-equilibrium growth (Perraud et al., 2012; Booth et al., 2014;  
91 Zaveri et al., 2014), which also affects the evolution of particle size distribution upon SOA  
92 growth (Shiraiwa et al., 2013; Zaveri et al., 2018). [Note that the equilibration timescale of SOA](#)  
93 [partitioning is determined by bulk diffusivity or viscosity, but also affected by other factors such](#)  
94 [as volatility, accommodation coefficient, particle size and mass loadings \(Shiraiwa and Seinfeld,](#)  
95 [2012; Mai et al., 2015; Liu et al., 2016\)](#). Chamber experiments probing mixing timescales of  
96 SOA particles derived by oxidation of various precursors such as isoprene, terpene, and toluene  
97 have observed strong kinetic limitations at low RH, but not at moderate and high RH (Loza et al.,  
98 2013; Ye et al., 2016; Ye et al., 2018). [Several studies have observed kinetic limitations of bulk](#)  
99 [diffusion of organic molecules including polycyclic aromatic hydrocarbons \(Abramson et al.,](#)  
100 [2013; Zhou et al., 2013\)](#) and isoprene derived epoxydiols (Zhang et al., 2018) in SOA, while  
101 Gorkowski et al. (2017) did not observe significant diffusion limitations for glycerol and  
102 squalene in  $\alpha$ -pinene SOA. Quasi-equilibrium versus kinetically-limited or non-equilibrium  
103 SOA growth remains an open issue and warrants further investigations.

104         Group contribution methods have been used to predict the viscosities of pure compounds  
105 when the functionality and molecular structure are known (Sastri and Rao, 1992; Rothfuss and  
106 Petters, 2017a). Song et al. (2016b) showed that estimations from group contribution approaches  
107 combined with either non-ideal or ideal mixing reproduced the RH-dependent trends particularly

108 well for the alcohol, di-, and tricarboxylic acid systems with viscosity of up to  $10^4$  Pa s. In  
109 contrast, model calculations overestimated the viscosity of more viscous compounds including  
110 mono-, di-, and trisaccharides by many orders of magnitude (Song et al., 2016b). A recent study  
111 compiled viscosity of organic compounds with atmospherically relevant functional groups,  
112 investigating the influence of the number and location of functional groups on viscosity  
113 (Rothfuss and Petters, 2017a). These studies provide important insights in estimating the  
114 viscosity of individual organic compounds.

115 Particle phase state can be characterized by a glass transition temperature ( $T_g$ ), which is a  
116 characteristic temperature representing a non-equilibrium phase transition from a glassy solid  
117 state to a semi-solid state as the temperature increases (Koop et al., 2011). Recently, we have  
118 developed a parameterization to estimate  $T_g$  of pure organic compounds comprised of carbon,  
119 hydrogen, and oxygen (CHO compounds) with molar mass less than  $450 \text{ g mol}^{-1}$  based on their  
120 molar mass and atomic O:C ratio (Shiraiwa et al., 2017). It has been applied successfully in a  
121 global chemistry climate model to predict  $T_g$  and the phase state of atmospheric SOA, which  
122 indicated that SOA particles are mostly liquid or semi-solid in the planetary boundary layer,  
123 while they should be glassy in the middle and upper troposphere (Shiraiwa et al., 2017). A recent  
124 study provided a consistent result, suggesting that mixing timescales of organic molecules within  
125 SOA are often  $< 1 \text{ h}$  in a global planetary boundary layer (Maclean et al., 2017).

126 It has been shown that SOA particles contain oligomeric compounds with molar masses  
127 higher than  $450 \text{ g mol}^{-1}$  (Gao et al., 2004; Tolocka et al., 2004; Nizkorodov et al., 2011; Nozière  
128 et al., 2015), which makes the previously developed parameterization incomplete. In this study,  
129 we extend the parameterization of  $T_g$  to higher molar mass compounds, and apply it to high-  
130 resolution mass spectrometry data for toluene SOA and biomass burning particles. The

131 Arrhenius approach and the Gordon-Taylor mixing rules were applied to estimate viscosity of  
132 SOA bulk materials to compare with the literature reported viscosity measurements. This method  
133 will be useful for estimations of viscosity of organic particles, for which high-resolution mass  
134 spectra are available. It can also be applied in global or regional models to evaluate impacts of  
135 the particle phase state on the role of SOA in climate and air quality.

136

## 137 **2. Parameterization development**

### 138 **2.1 Glass transition temperature**

139 Figure 1a shows the dependence of  $T_g$  on the molar mass ( $M$ ) of organic compounds. Solid  
140 markers represent measured  $T_g$  of 258 CHO compounds (Koop et al., 2011; Dette et al., 2014;  
141 Rothfuss and Petters, 2017a), while open markers represent 654 CHO compounds in SOA  
142 (Shiraiwa et al., 2014). Markers are color-coded by atomic O:C ratio. Their melting points ( $T_m$ )  
143 were estimated by the Estimation Programs Interface (EPI) Suite software version 4.1 (US-EPA,  
144 2012) and their  $T_g$  were estimated using the Boyer-Kauzmann rule:  $T_g = g \cdot T_m$  with  $g = 0.7$  (Koop  
145 et al., 2011; Shiraiwa et al., 2017). This rule can provide good estimates of  $T_g$ , as has been  
146 validated in previous work (Koop et al., 2011) and also shown in Fig. A2(a). A subset of data  
147 shown in Figure 1 was originally published in Shiraiwa et al. (2017) for compounds with  $M <$   
148  $450 \text{ g mol}^{-1}$ . This version of the figure has been updated to include a number of experimentally  
149 measured  $T_g$  values of larger compounds with  $M$  up to  $1153 \text{ g mol}^{-1}$ , including aliphatic  
150 compounds containing OH and/or COOH groups. Specifically, data for 76 aliphatic alcohols, 39  
151 carbohydrates and their derivatives, 4 carboxylic acids, and 4 hydroxy acids, as compiled by  
152 Rothfuss and Petters (2017b), have been added to Figure 1. Eight of these compounds are  
153 carbohydrates with  $M > 450 \text{ g mol}^{-1}$ . These updates are critical for reliable parameterization of  $T_g$

154 based on  $M$ . When  $M$  increases above  $\sim 500 \text{ g mol}^{-1}$ , the slope of  $T_g$  decreases, making it  
155 challenging to extrapolate the low- $M$  data from the original Shiraiwa et al. (2017) study to higher  
156  $M$  values. When  $M$  increases to  $\sim 1000 \text{ g mol}^{-1}$ , the corresponding  $T_g$  appears to level at around  
157 420 K.

158 Such dependence on  $M$  has been described for polymers with the Fox-Flory equation:

159  $T_g(M) = T_{g,\infty} - \frac{K_m}{M}$  (Fox Jr and Flory, 1950), where  $K_m$  is a constant and  $T_{g,\infty}$  is the asymptotic  
160 value of  $T_g$  specific to the polymer. We conducted a literature search and found that most of the  
161 reported  $T_{g,\infty}$  values fell below  $\sim 500 \text{ K}$  (Fox Jr and Flory, 1950; Onder et al., 1972; Montserrat  
162 and Colomer, 1984; Polymer handbook, 1999; Papadopoulos et al., 2004; Matsushima et al.,  
163 2017). The Fox-Flory equation works very well for high molar mass compounds and is also  
164 generally applicable to smaller compounds (Koop et al., 2011), as supported by an approximately  
165 linear dependence of  $T_g$  on the inverse molar mass in Fig. A1(a). Figure 1b plots the values of  $T_g$   
166 as a function of the atomic O:C ratio of organic molecules. Figures 1a and 1b clearly  
167 demonstrate that  $T_g$  depends primarily on the molar mass with a weak dependence on the atomic  
168 O:C ratio.

169 A parameterization for  $T_g$  calculation based on the molar mass and atomic O:C ratio was  
170 developed in our recent work, which is applicable to CH and CHO compounds with  $M < 450 \text{ g}$   
171  $\text{mol}^{-1}$  (Shiraiwa et al., 2017):

$$172 \quad T_g = A + BM + CM^2 + D (\text{O:C}) + E M (\text{O:C}) \quad (1)$$

173 where  $A = -21.57 (\pm 13.47) [\text{K}]$ ,  $B = 1.51 (\pm 0.14) [\text{K mol g}^{-1}]$ ,  $C = -1.7 \times 10^{-3} (\pm 3.0 \times 10^{-4}) [\text{K}$   
174  $\text{mol}^2 \text{g}^{-2}]$ ,  $D = 131.4 (\pm 16.01) [\text{K}]$  and  $E = -0.25 (\pm 0.085) [\text{K mol g}^{-1}]$ , respectively. These values  
175 were obtained by fitting the measured  $T_g$  of 179 CH and CHO compounds with  $M < 450 \text{ g mol}^{-1}$   
176 with multi-linear least squares analysis. Note that application of Eq. (1) may provide

177 unreasonable  $T_g$  values for compounds with  $M > 500 \text{ g mol}^{-1}$  because it does not account for the  
178 strong curvature in the  $T_g$  vs.  $M$  dependence shown in Figure 1a.

179 In this study we have developed an improved parameterization to predict  $T_g$  of CH and  
180 CHO compounds using the number of carbon ( $n_C$ ), hydrogen ( $n_H$ ), and oxygen ( $n_O$ ) that can also  
181 be applied to higher molar mass compounds. Motivated by a good correlation between  $T_g$  and  
182 volatility (Fig. 1a in Shiraiwa et al. (2017)), we use an equation with a similar formulation to the  
183 equation used to predict the saturation mass concentration or volatility (Donahue et al., 2011; Li  
184 et al., 2016):

$$185 \quad T_g = (n_C^0 + \ln(n_C)) b_C + \ln(n_H) b_H + \ln(n_C) \ln(n_H) b_{CH} + \ln(n_O) b_O + \ln(n_C) \ln(n_O) b_{CO} \quad (2)$$

186 where  $n_C^0$  is the reference carbon number,  $b_C$ ,  $b_H$  and  $b_O$  denote the contribution of each atom to  
187  $T_g$ , and  $b_{CH}$  and  $b_{CO}$  are coefficients that reflect contributions from carbon-hydrogen and carbon-  
188 oxygen bonds, respectively. These values were obtained by fitting the measured  $T_g$  of 42 CH  
189 compounds and 258 CHO compounds with multi-linear least squares analysis with 68%  
190 prediction and confidence intervals. The best-fit parameters are summarized in Table 1.

191 Note that the evaluation dataset used to derive Eq. (2) contains CH compounds with  $M <$   
192  $260 \text{ g mol}^{-1}$  (see Fig. A2b for comparison of measured and predicted  $T_g$ ). Thus, the application of  
193 Eq. (2) to higher molar mass compounds may require further refinement of the method when  
194 measured  $T_g$  for higher molar mass CH compounds becomes available. Figure 1c shows that the  
195  $T_g$  values predicted using Eq. (2) are in good agreement with the  $T_g$  values measured in  
196 experiments (see also Fig. A1(b)) or estimated by the Boyer-Kauzmann rule as indicated by the  
197 high correlation coefficient of 0.95.  $T_g$  of individual compounds can be predicted within  $\pm 21 \text{ K}$   
198 as indicated by the prediction band (dotted lines in Fig. 1c); however, this uncertainty may be

199 much smaller for multicomponent SOA mixtures under ideal mixing conditions as indicated in  
200 the confidence band (dashed lines, almost overlapping with the 1:1 line).

201         These results are noteworthy given that the parameterization (Eq. 2) does not consider  
202 either explicit molecular structures or functional groups. Previous studies have shown that  $T_g$  can  
203 be especially sensitive to the number of OH groups, which interact strongly through hydrogen  
204 bonding. For example, Nakanishi et al. (2011) found a direct relationship between  $T_g$  and the  
205 number of hydroxyl groups in a molecule for sugar alcohols;  $T_g$  increases as the number of OH  
206 groups increases. They reported that the correlation between  $T_g$  and the number of OH groups  
207 was much stronger than the correlation between  $T_g$  and the number of carbons in a molecule.  
208 Such a trend is implicitly included in Eq. (1) and (2), which contain the O:C ratio and number of  
209 oxygen atoms as parameters, respectively. Recently, Rothfuss and Petters (2017b) showed an  
210 approximately linear relationship between the number of OH groups and  $T_g$  for compounds with  
211 up to eight OH groups. Grayson et al. (2017) showed that addition of hydroxyl functional groups  
212 increases viscosity, a conclusion supported by both the experimental data and quantitative  
213 structure-property relationship model. The correlation between  $T_g$  and the number of carbon  
214 atoms is consistent with the free volume theory, in which molecular motion is restricted by the  
215 difference between the space required for a molecule to vibrate versus the space in which the  
216 molecule resides (i.e., the free volume) (White and Lipson, 2016). The correlation between  $T_g$   
217 and the number of OH groups is more consistent with the topological constraint theory, where  
218 the primary influence is the three dimensional structure of the molecule as determined by  
219 molecular bonds and hydrogen-bonding networks (Nakanishi and Nozaki, 2011; van der Sman,  
220 2013). Future experiments targeting more comprehensive  $T_g$  data, especially for higher molar  
221 mass compounds, would lead to further refinements of our  $T_g$  parameterizations.



222 Comparing Eq. (1) and (2), the two parameterizations give similar performance for  
223 compounds with  $M < 450 \text{ g mol}^{-1}$  as shown in Fig. A2c. The statistical measures of correlation  
224 coefficient (R), mean bias (MB), and root mean square error (RMSE) are 0.93,  $-6.45 \text{ K}$ , and  
225  $25.64 \text{ K}$ , respectively, for the performance of Eq. (1), while for Eq. (2), they are 0.95,  $3.15 \text{ K}$ ,  
226 and  $21.11 \text{ K}$ , respectively. It should be noted again that Eq. (1) cannot be used to predict  $T_g$  for  
227 compounds with  $M > 450 \text{ g mol}^{-1}$ . For example,  $T_g$  of stachyose ( $M = 667 \text{ g mol}^{-1}$ ) predicted by  
228 Eq. (1) is  $198 \text{ K}$ , while that by Eq. (2) is  $394 \text{ K}$ , which agrees much better with the measured  
229 mean  $T_g$  of  $396 \text{ K}$  (Rothfuss and Petters, 2017a). Eq. (2) is more flexible than Eq. (1) and can be  
230 potentially expanded to include compounds containing hetero-atoms (e.g., nitrogen or sulfur),  
231 once substantial sets of experimental values of  $T_g$  for such compounds become available.  
232 Regarding the applications to air quality and climate models, Eq. (1) can be applied in the  
233 volatility basis set (VBS) (Donahue et al., 2006; Donahue et al., 2011) and the molecular  
234 corridor approach (Shiraiwa et al., 2014; Li et al., 2016) to predict the  $T_g$  of SOA particles  
235 (Shiraiwa et al., 2017), while the new parameterization may be suitable for coupling with the  
236 statistical oxidation model which characterizes the SOA evolution as a function of  $n_C$  and  $n_O$   
237 (Cappa and Wilson, 2012; Jathar et al., 2015).

238 These parameterizations (Eqs. 1, 2) calculate  $T_g$  based on the elemental composition of  
239 organic compounds. SOA particles contain a number of organic compounds as well as a variable  
240 amount of liquid water, which has low  $T_g$  ( $136 \text{ K}$ ) and can act as a plasticizer (Mikhailov et al.,  
241 2009; Koop et al., 2011). Under humid conditions, SOA particles take up water by hygroscopic  
242 growth in response to RH, lowering  $T_g$  and viscosity of SOA particles. Estimations of  $T_g$  for  
243 SOA-water mixtures were discussed by Shiraiwa et al. (2017), who applied the Gordon-Taylor  
244 equation validated for a wide range of mixtures of organics, polymers, and water (Roos, 1993;

245 Hancock and Zograf, 1994; Zobrist et al., 2008; Dette et al., 2014; Dette and Koop, 2015).  
 246 Briefly,  $T_g$  of mixtures of SOA compounds under dry conditions ( $T_{g,org}$ ) were calculated  
 247 assuming the Gordon-Taylor constant ( $k_{GT}$ ) of 1 (Dette et al., 2014):  $T_{g,org} = \sum_i w_i T_{g,i}$ , where  $w_i$  is  
 248 the mass fraction of organic compound  $i$ , which can be derived using mass concentrations of  
 249 SOA products. The Gordon-Taylor equation can also be applied to calculate  $T_g$  of organic-water  
 250 mixtures considering the mass fraction of organics ( $w_{org}$ ) in SOA particles (Koop et al., 2011):

$$251 \quad T_g(w_{org}) = \frac{(1-w_{org})T_{g,w} + \frac{1}{k_{GT}}w_{org}T_{g,org}}{(1-w_{org}) + \frac{1}{k_{GT}}w_{org}} \quad (3)$$

252  $w_{org}$  can be calculated using the mass concentrations of water ( $m_{H_2O}$ ) and SOA ( $m_{SOA}$ ) as  $w_{org} =$   
 253  $m_{SOA} / (m_{SOA} + m_{H_2O})$ .  $m_{H_2O}$  can be estimated using the effective hygroscopicity parameter ( $\kappa$ )  
 254 (Petters and Kreidenweis, 2007):

$$255 \quad m_{H_2O} = \frac{\kappa \rho_w m_{SOA}}{\rho_{SOA} \left( \frac{1}{a_w} - 1 \right)} \quad (4)$$

256 The density of water ( $\rho_w$ ) is  $1 \text{ g cm}^{-3}$ , the density of SOA particles ( $\rho_{SOA}$ ) is assumed to be  $1.2 \text{ g}$   
 257  $\text{cm}^{-3}$  (Kuwata et al., 2012),  $m_{SOA}$  is the total mass concentrations of SOA, and  $a_w$  is the water  
 258 activity calculated as  $a_w = RH/100$ . Pajunoja et al. (2015) found that water uptake in subsaturated  
 259 conditions is inhibited until RH is high enough for dissolution of water in SOA particles with  
 260 relatively low O:C ratios. As oxidation of SOA increases, solubility of water increases and  
 261 dissolution occurs at lower RH values. In both cases, the use of subsaturated hygroscopicity  
 262 measurements was supported.

263

## 264 **2.2 Viscosity**

265 Temperature dependence of viscosity ( $\eta$ ) can be predicted using the modified Vogel-  
 266 Tammann-Fulcher (VTF) equation (Angell, 1991):

267 
$$\eta = \eta_{\infty} e^{\frac{T_0 D}{T - T_0}} \quad (5)$$

268 where  $\eta_{\infty}$  is viscosity at infinite temperature;  $T_0$  is the Vogel temperature;  $T$  is the ambient  
269 temperature. The fragility parameter,  $D$ , characterizes how rapidly the dynamics of a material  
270 slow down as  $T$  approaches  $T_g$ , reflecting to what degree the temperature dependence of the  
271 viscosity deviates from Arrhenius behavior. When  $T$  is close to  $T_g$  ( $T_g/T \approx 1$ ), smaller  $D$  values  
272 indicate that viscosity is sensitive to temperature change (fragile behavior); while larger  $D$  values  
273 indicate that viscosity is less sensitive to temperature change (strong or Arrhenius behavior).

274 Assuming  $\eta_{\infty} = 10^{-5}$  Pa s (Angell, 1991):

275 
$$\log \eta = -5 + 0.434 \frac{T_0 D}{T - T_0} \quad (6)$$

276 When  $T = T_g$ ,  $\eta = 10^{12}$  Pa s, which leads to (Angell, 1991; Angell, 2002):

277 
$$T_0 = \frac{39.17 T_g}{D + 39.17} \quad (7)$$

278 As can be seen in Eq. (7), both  $T_g$  and  $D$  are required to calculate  $\eta$  from Eq. (6) at a given  
279 temperature.

280 Figure 2 shows the  $T_g$ -scaled Arrhenius plot of fragility (viscosity versus  $T_g/T$ ) referred to  
281 as an Angell plot (Angell, 1995).  $D$  values of organic compounds are typically in the range of  
282  $\sim 5$ – $30$  (Angell, 1997). To estimate  $D$  values that could be applied to SOA compounds, we  
283 compiled measured fragility values. Fragility was often measured in the form of the fragility  
284 steepness index ( $m$ ), which represents the slope of the Arrhenius plot at the point where  $T = T_g$   
285 (Boehmer et al., 1993). Compounds with lower  $m$  exhibit higher  $D$  values, indicating stronger  
286 glass formers. The measured  $m$  of 95 organic compounds are included in the Supplement.  $m$  can  
287 be converted to  $D$  using the following equation (see the full derivation of this equation in  
288 Appendix A):

289 
$$D = \frac{665.89}{m-17} \quad (8)$$

290 Figure 3 shows the measured  $D$  as a function of (a) molar mass and (b) atomic O:C ratio  
291 of organic molecules. The molar mass exerts a stronger effect on fragility, while there is little  
292 dependence of  $D$  on the O:C ratio. As molar mass increases,  $D$  approaches a lower limit of 10.3  
293 ( $\pm 1.7$ ), consistent with the value of 10 used in our recent study (Shiraiwa et al., 2017). To  
294 evaluate the impact of the variations of  $D$  on viscosity prediction, sensitivity calculations were  
295 conducted as described in Sect. 3.

296 Besides the VTF equation, another commonly used equation for describing the  
297 temperature dependence of viscosity is the Williams-Landel-Ferry (WLF) equation:  $\log \frac{\eta(T)}{\eta(T_g)} =$   
298  $\frac{-C_1(T-T_g)}{C_2+(T-T_g)}$ , where empirical parameters  $C_1$  and  $C_2$  are adopted as 17.44 and 51.6 K, respectively  
299 (Williams et al., 1955; Schill and Tolbert, 2013; Wang et al., 2015). The two equations are  
300 mathematically equivalent, both defined with respect to a reference temperature, and their  
301 parameters are related through  $C_1 = \frac{DT_0}{2.303(T_g-T_0)}$  and  $C_2 = T_g - T_0$ . For the WLF equation,  $T_g$  is  
302 the reference temperature and there is a linear dependence assumed between temperature and  
303 free volume (O'Connell and McKenna, 1999; Huang and McKenna, 2001; Metatla and Soldera,  
304 2007). For the VTF equation, the reference is the Vogel temperature ( $T_0$ )—a hypothetical  
305 temperature at which all non-vibrational motion ceases and viscosity becomes infinite and the  
306 theoretical foundation of the VTF equation includes both thermodynamic and kinetic  
307 considerations (O'Connell and McKenna, 1999; Huang and McKenna, 2001; Metatla and  
308 Soldera, 2007). Recently, Rothfuss and Petters (2017b) applied a similar approach to model  
309 viscosity for sucrose particles by applying the VTF and Gordon-Taylor approaches. The  
310 calculations of viscosity of multi-component SOA mixtures in this study are based mainly on the

311 VTF equation and the difference between calculated results from the two equations will be  
312 briefly discussed in the following section.

313

### 314 **3. Comparison of predicted viscosity with measurements**

#### 315 **3.1. SOA formed from $\alpha$ -pinene and isoprene**

316 The purpose of this section is to demonstrate that viscosity of SOA material can be  
317 predicted over a broad range of RH values from four parameters:  $T_g$  of dry SOA ( $T_{g,org}$ ), fragility  
318 ( $D$ ), hygroscopicity ( $\kappa$ ), and the Gordon-Taylor constant for mixing SOA and water ( $k_{GT}$ ).  
319 Viscosity of  $\alpha$ -pinene SOA has been measured or estimated as a function of RH by several  
320 groups using multiple experimental techniques as shown in Fig. 4(a) (Abramson et al., 2013;  
321 Renbaum-Wolff et al., 2013; Kidd et al., 2014; Pajunoja et al., 2014; Bateman et al., 2015;  
322 Zhang et al., 2015; Grayson et al., 2016). The wide range of experimentally measured viscosities  
323 reported for  $\alpha$ -pinene SOA, particularly from 30-60% RH is most likely a consequence of the  
324 different experimental approaches, mass loadings and O:C ratios for each experiment. For  
325 instance, Grayson et al. (2016) used mass loadings of 121 to 14000  $\mu\text{g m}^{-3}$  and observed that  
326 viscosity decreased as mass loading increased. Higher mass loadings would lead to greater  
327 partitioning of semi-volatile and lower molar mass compounds into the particle phase, which  
328 would lead to the decrease of  $T_g$  and viscosity of the resulting SOA mixture, as very recently  
329 demonstrated experimentally by Jain et al. (2018). Grayson et al. (2016) concluded that their  
330 results should be considered a lower limit for viscosity of  $\alpha$ -pinene SOA in the atmosphere. It  
331 should also be noted that the viscosity measurements from Renbaum-Wolff et al. (2013) were for  
332 the water-soluble portion of the SOA. These datasets suggest that viscosity of  $\alpha$ -pinene SOA  
333 approaches very high values ( $\sim 10^8$  Pa s) below 20-30% RH and decreases with an increase in

334 RH reaching a value of  $\sim 10$  Pa s at 80% RH. As can be seen in Fig. 4(b), PAM-generated  
335 isoprene SOA is less viscous with  $\eta < 10^6$  Pa s even under dry conditions, undergoing a phase  
336 transition from a semi-solid phase to a liquid phase at  $\sim 55\%$  RH (Bateman et al., 2015; Song et  
337 al., 2015).

338 The solid lines with the shaded areas in Figure 4 are viscosity values predicted using  
339  $T_{g,org}$ ,  $D$ ,  $\kappa$ ,  $k_{GT}$ .  $T_{g,org}$  values were adopted by Berkemeier et al. (2014) who estimated  $T_{g,org}$  with  
340 the Boyer-Kauzmann rule using the melting point of representative SOA oxidation products.  
341 Note that Eq. (1) or (2) were not used to estimate  $T_{g,org}$ , which should be done in future studies  
342 by obtaining their elemental composition using high resolution mass spectrometry. For  $\alpha$ -pinene,  
343  $T_{g,org}$  was assumed to be 278 K corresponding to an O:C ratio of 0.5 (Berkemeier et al., 2014),  
344 which is a typical O:C ratio of  $\alpha$ -pinene SOA (Aiken et al., 2008; Chen et al., 2011; Putman et  
345 al., 2012).

346 The  $T_{g,org}$  selected for isoprene SOA was 255 K, corresponding to the O:C ratio of 0.6.  
347 Although no measurements of the O:C ratio for the experimental isoprene SOA data were  
348 reported, Song et al. (2015) estimated O:C of 0.64 – 1.1 based on literature values. As O:C ratios  
349 are useful in estimating  $T_{g,org}$ , we encourage the measurement of the O:C ratio of SOA when  
350 conducting viscosity measurements. In contrast to  $\alpha$ -pinene SOA, there are limited viscosity  
351 measurements for isoprene SOA. While the predicted viscosity is consistent with the  
352 experimental data, comparison of our model predictions to additional measurements is strongly  
353 recommended. Song et al. (2015) prepared isoprene SOA in a potential aerosol mass (PAM)  
354 reactor while the data by Bateman et al. (2015) were for isoprene SOA generated in a smog  
355 chamber. It has been suggested that under ambient conditions, the majority of isoprene-derived  
356 SOA can be derived through heterogeneous interactions with acidic sulfate particles forming

357 oligomers (Surratt et al., 2010; Lin et al., 2013; Gaston et al., 2014), which may increase  
358 viscosity compared to the model SOA generated in PAM or a chamber. Further studies are  
359 warranted to compare laboratory-generated and ambient isoprene SOA, and to investigate the  
360 effect of the acidic seed on the viscosity.

361 For both  $\alpha$ -pinene and isoprene SOA,  $D$  was set to 10 based on the analysis presented in  
362 Fig. 3(a).  $\kappa$  was set to 0.1 based on field and laboratory measurements (Gunthe et al., 2009;  
363 Lambe et al., 2011b; Pajunoja et al., 2014; Petters et al., 2017) and  $k_{GT}$  was assumed to be 2.5  
364 (Zobrist et al., 2008; Koop et al., 2011). Using these parameters, the predicted viscosities match  
365 well the magnitude and the RH-dependence of the measured viscosity of  $\alpha$ -pinene and isoprene  
366 SOA. Figure 4 also shows predicted viscosities (dotted lines) using the WLF equation, which  
367 shows similar values as the VTF equation, but slightly underestimates the viscosity of  $\alpha$ -pinene  
368 SOA at low RH and overestimates the viscosity of isoprene SOA at high RH.

369 Sensitivity studies were conducted to examine the effects of  $T_{g,org}$ ,  $D$ ,  $\kappa$  and  $k_{GT}$ , on the  
370 calculated viscosity. In these studies,  $T_{g,org}$  of  $\alpha$ -pinene and isoprene SOA were varied within 229  
371 – 328 K and 255 – 316 K, respectively, representing  $T_{g,org}$  of different oxidation states  
372 (Berkemeier et al., 2014).  $D$  was varied between 5 and 30, which is the range characteristic for  
373 organic compounds (see Fig. 3a).  $\kappa$  of 0.05 – 0.15 were used for  $\alpha$ -pinene and isoprene SOA  
374 (Lambe et al., 2011b; Pajunoja et al., 2015). For the Gordon-Taylor constant, values of  $2.5 \pm 1.5$   
375 were considered (Zobrist et al., 2008; Koop et al., 2011; Dette et al., 2014; Dette and Koop,  
376 2015).

377 The effect of varying each parameter on the calculated viscosity of  $\alpha$ -pinene SOA is  
378 illustrated in Fig. 5. Variations of  $\pm 50$  K in  $T_{g,org}$  result in 3-6 orders of magnitude difference in  
379 calculated values at dry conditions, indicating that  $T_{g,org}$  is a critical parameter for viscosity

380 estimations. Decreasing  $D$  from 10 to 5 led to a decrease of calculated values by more than one  
381 order of magnitude. The calculated results were within the upper limit of measurements when  
382 increasing  $D$  from 10 to 20, and the predicted values were only slightly enhanced when further  
383 increasing  $D$  from 20 to 30. Calculated values with variations in  $\kappa$  from 0.05 to 0.15 and  $k_{GT}$   
384 from 1.0 to 4.0 were all within the measured ranges.

385 For isoprene SOA, an increase of  $T_{g,org}$  to 287 K, which represents a higher oxidation  
386 state (Berkemeier et al., 2014), led to calculated values to be several orders of magnitude higher  
387 than the upper limit of measurements (Fig. 6a). When  $T_{g,org}$  reaches 316 K, isoprene SOA can  
388 occur as a solid for RH lower than  $\sim 40\%$ . Compared to  $\alpha$ -pinene SOA, a variation in  $D$  has a  
389 larger effect on the calculated viscosity (Fig. 6b). For a range of 5 – 30 for  $D$ , calculations with  
390 the  $D$  value of 10 agreed well with the measurements, while other  $D$  values resulted in calculated  
391 viscosity outside of the measured ranges. Figures 6c and 6d show that decreasing  $\kappa$  and  $k_{GT}$   
392 below the reference values, the predictions overestimate the measured  $\eta$  by one or two orders of  
393 magnitude. The latter is most evident at RH > 60%, where the calculated values were higher than  
394 the upper limit of measurements. Modeling results with  $\kappa$  and  $k_{GT}$  increasing to 0.15 and 4.0,  
395 respectively, were within the lower limit of measurements.

396 The above comparison between the measured and predicted viscosity demonstrates that  
397 the method described in this study can reproduce reasonably well the measured RH-dependent  
398 viscosity of SOA formed from  $\alpha$ -pinene and isoprene. The sensitivity calculations showed that  
399  $T_{g,org}$  contributed the most to the uncertainty in the viscosity estimates. Previous studies have  
400 shown that the experimental conditions such as particle mass concentrations (Grayson et al.,  
401 2016; Jain et al., 2018) and RH upon SOA formation (Kidd et al., 2014; Hinks et al., 2018) can



402 impact chemical composition of SOA and hence the phase state and viscosity. Further efforts to  
403 constrain the uncertainties are needed both in experiments and parameterizations.

404

### 405 **3.2. SOA formed from toluene**

406 In this and the following sections, we examine the feasibility of calculating the value of  
407  $T_{g,org}$  from mass spectrometry data on SOA. Hinks et al. (2017) measured the elemental  
408 composition of toluene SOA using nanospray desorption electrospray ionization high-resolution  
409 mass spectrometry (nano-DESI-HRMS) (Roach et al., 2010b, a). Toluene SOA were formed by  
410 OH photooxidation in an aerosol smog chamber at <2% RH (mass loading =  $23 \mu\text{g m}^{-3}$ ) and 75%  
411 RH (mass loading =  $8 \mu\text{g m}^{-3}$ ) to investigate the effect of RH on the chemical composition of  
412 toluene SOA formed under low- $\text{NO}_x$  conditions. Measurements revealed a significant reduction  
413 in the fraction of oligomers present in toluene SOA generated under high RH conditions  
414 compared to SOA generated under low RH conditions (Hinks et al., 2017). The detected molar  
415 mass of individual oxidation products spanned a range of 102 -  $570 \text{ g mol}^{-1}$  at high RH, which  
416 increased up to  $726 \text{ g mol}^{-1}$  at low RH.

417 Figure 7(a) shows the interdependence of glass transition temperature, volatility, and  
418 molar mass of the detected toluene SOA compounds. Glass transition temperatures were  
419 calculated using Eq. (2). Saturation mass concentrations or volatilities of detected compounds  
420 were estimated from the elemental composition by using the parameterization of Li et al. (2016).  
421 The analysis is based on the molecular corridor approach—a two-dimensional framework of  
422 volatility and molar mass of SOA components constrained by boundary lines of low and high  
423 atomic O:C ratio, corresponding to  $n$ -alkanes ( $\text{C}_n\text{H}_{2n+2}$ , O:C = 0) and sugar alcohols ( $\text{C}_n\text{H}_{2n+2}\text{O}_n$ ,  
424 O:C = 1), respectively (Shiraiwa et al., 2014; Li et al., 2016). The toluene SOA constituents are

425 well constrained by the molecular corridor and  $T_g$  are higher for compounds with higher molar  
426 mass and lower volatility.

427 Eq. (1) was used to calculate  $T_g$  for individual compounds with  $M < 450 \text{ g mol}^{-1}$ , while  
428 excluding compounds with molar mass higher than  $450 \text{ g mol}^{-1}$ . This approach was deemed  
429 reasonable as such high molar mass compounds account for  $< 10\%$  of all toluene SOA products  
430 formed at low RH, and for  $< 2\%$  formed at high RH. Eq. (2) was used to calculate  $T_g$  for all the  
431 detected compounds.  $T_g$  of dry toluene SOA ( $T_{g,\text{org}}$ ) was then computed using the Gordon-Taylor  
432 approach with  $k_{\text{GT}} = 1$  (Sect. 2.1). The relative mass concentrations of individual components  
433 were assumed to be proportional to their relative abundance in the nano-DESI-HRMS spectrum.  
434 This assumption has a number of caveats (Bateman et al., 2012; Nguyen et al., 2013), and as we  
435 will see below, it results in deviations between the predicted and measured viscosity. Table 2  
436 summarizes the results of such calculations, showing that the  $T_{g,\text{org}}$  by Eq. (1) – excluding high  
437 molar mass compounds – is about 10 K lower as compared to  $T_{g,\text{org}}$  by Eq. (2).  $T_{g,\text{org}}$  at low RH is  
438 predicted to be higher than  $T_{g,\text{org}}$  at high RH, which results from a lower abundance of high molar  
439 mass compounds observed at high RH. This trend is consistent with Kidd et al. (2014), who  
440 showed that SOA material formed under dry conditions is more viscous than that formed under  
441 wet conditions.

442 Figure 7(b) shows the predicted viscosity of toluene SOA as a function of RH, as  
443 compared to the measured viscosity of toluene SOA formed in an oxidation flow reactor at 13%  
444 RH (Song et al., 2016a). Indirect viscosity measurements are also included in shaded boxes for  
445 [toluene-derived SOA](#) (Bateman et al., 2015; Li et al., 2015). Lines with shaded areas are  
446 calculated viscosities using  $T_{g,\text{org}}$  as described above.  $\kappa$  was assumed to be 0.25 based on  
447 laboratory measurements (Lambe et al., 2011a; Hildebrandt Ruiz et al., 2015). To achieve good

448 fit,  $D$  was set to 13 and  $k_{GT}$  was assumed to be 3.0 (Dette et al., 2014). Estimations with Eq. (1)  
449 match the measured viscosity values very well over the entire RH range. Predictions with Eq. (2)  
450 overestimated the measurements by one or two orders of magnitude at moderate RH between 30%  
451 and 50%, while they agreed with the measurements derived at  $RH \geq 60\%$  and at the dry  
452 conditions.

453         There are several possible reasons for the difference between the measurements and  
454 predictions. First, the relative abundance of high molar mass compounds observed in HRMS  
455 measurements may be overestimated, as high molar mass compounds tend to have higher (yet  
456 generally unknown) ionization efficiencies compared to lower molar mass compounds. Second,  
457 the nano-DESI-HRMS analysis of toluene SOA was limited to  $m/z$  range of 100 -1000 (Hinks et  
458 al., 2017). It is possible that some SOA products with lower molar mass were present in particles  
459 but not detected, which would lead to an overestimation of  $T_g$ . Third, the chemical composition  
460 of toluene SOA are likely different between Hinks et al. (2017) and Song et al. (2016a) because  
461 of the differences in the experimental conditions. Specifically, toluene SOA was formed in a  
462 Teflon chamber in Hinks et al., while Song et al. used an oxidation flow reactor to generate  
463 toluene SOA. The O:C ratios are 0.71 at low RH and 0.63 at high RH based on nano-DESI-  
464 HRMS measurements in Hinks et al. (2017), while [the O:C ratio was 1.06 in Song et al. \(2016a\)](#)  
465 based on the aerosol mass spectrometry (AMS) measurements.

466         In addition, different mass loadings may have affected viscosity. Song et al. (2016)  
467 measured viscosity at two different mass loadings (60-100 and 600-1000  $\mu\text{g m}^{-3}$ ) and compared  
468 their results to [toluene SOA data in](#) Bateman et al. (2015) (30-50  $\mu\text{g m}^{-3}$ ) and Li et al. (2015)  
469 (44-125  $\mu\text{g m}^{-3}$ ), observing little impact of mass loadings on viscosity. We carried out a  
470 sensitivity study of mass loadings on viscosity using a set of compounds detected by HRMS. The

471 saturation mass concentration was predicted for each component using the molecular corridor  
472 approach (Li et al., 2016). Assuming that the mass signal intensity is proportional to the total  
473 mass concentration of the compound in the mixture, and applying the absorptive partitioning  
474 theory (Pankow, 1994), particle-phase concentrations of each compound were predicted to  
475 estimate  $T_g$  at different organic aerosol mass loading values (1-1000  $\mu\text{g m}^{-3}$ ). The glass transition  
476 temperature of the SOA mixture decreases as mass loading increases. Viscosity decreases up to  
477 two orders of magnitude at low RH, while at high RH they have little difference as shown in Fig.  
478 A3. Simultaneous measurements of viscosity and chemical composition with different mass  
479 loadings should be performed in future studies.

480

### 481 **3.3 Biomass Burning Particles**

482 To further explore the applicability of our viscosity prediction method using elemental  
483 composition as measured by HRMS, we performed similar calculations for biomass burning  
484 organic particles emitted from test facility burns of subalpine fir and lodgepole pine trees,  
485 conducted as a part of the FIREX 2016 campaign (Selimovic et al., 2017). These samples were  
486 analyzed by HRMS using two different ionization sources: electrospray ionization (ESI) and  
487 atmospheric pressure photoionization (APPI). Mass spectra shown in Fig. 8(a) and (b) indicate  
488 that a substantial number of compounds were detected by both methods (109 and 170  
489 compounds for subalpine fir and lodgepole pine, respectively). However, pronounced  
490 differences are also observed between the ESI and APPI spectra both in terms of the identity and  
491 signal intensities of the detected compounds.

492 Glass transition temperatures for the assigned CH and CHO compounds were computed  
493 using Eq. (2). Nitrogen and sulfur containing compounds (CHON and CHOS) are not yet

494 covered by Eq. (2) and were therefore excluded from the analysis. CHON and CHOS compounds  
495 comprised less than 10% of the detected ion intensity and <15% of the assigned compounds.  
496 Note that we do not intend to provide accurate estimates of viscosity of ambient biomass burning  
497 particles (as inorganic components are also not included in this analysis), but we investigate how  
498 the use of different ionization methods would lead to variations in our viscosity predictions.  $T_g$  of  
499 organic mixtures ( $T_{g,org}$ ) were then calculated using the Gordon-Taylor approach with  $k_{GT} = 1$ ,  
500 assuming that the relative concentration of each compound is proportional to its MS signal  
501 intensity. The calculated  $T_{g,org}$  values for the mixtures are specified in the legend of Figure 9. For  
502 both types of mixtures, the calculated  $T_{g,org}$  for the APPI MS data is lower than the value  
503 calculated based on the ESI MS data with a difference of 32 K for subalpine fir and 11 K for the  
504 lodgepole pine. Figure 9 shows the predicted viscosity as a function of RH, assuming  $D = 10$ ,  $\kappa$   
505 = 0.10 and  $k_{GT} = 2.5$ . The difference in  $T_{g,org}$  derived from ESI and APPI results in a variation of  
506 predicted viscosity at low RH by up to five and two orders of magnitude for subalpine fir and  
507 lodgepole pine, respectively.

508         The difference in the calculated  $T_{g,org}$  values is attributed to the chemical profile of the  
509 species detected using different ionization techniques as shown in mass spectra in Fig. 8(a) and  
510 (b). Van Krevelen diagrams in Fig. 8(c) and (d) illustrate these compositional differences  
511 between chemical species detected by ESI and APPI. ESI is more efficient at detection of polar  
512 compounds (Kiontke et al., 2016), which typically have higher O:C ratios and therefore would  
513 result in higher predicted values of [glass transition temperature](#) (Koop et al., 2011; Saukko et al.,  
514 2012). APPI enables the detection of nonpolar compounds with lower O:C ratios, in particular  
515 polycyclic aromatic hydrocarbons (PAHs), that have low ionization efficiencies when analyzed  
516 by ESI MS (Raffaelli and Saba, 2003; Itoh et al., 2006). Due to the complementary nature of

517 these ionization methods, it is most likely that the actual glass transition temperature and  
518 viscosity of each type of [organic components in biomass burning aerosols](#) are somewhere in  
519 between the values inferred from ESI and APPI data sets: ESI MS may be viewed as providing  
520 the upper limit of viscosity, while APPI MS gives the lower limit. Our results indicate that the  
521 use of complementary ionization techniques may help evaluate the associated uncertainty for the  
522 prediction of viscosity values based on the elemental composition as measured by HRMS.

523

#### 524 **4 Conclusions**

525 We have developed a parameterization for calculation of the glass transition temperature  
526 of individual SOA compounds with molar mass up to  $\sim 1100 \text{ g mol}^{-1}$  using the number of carbon,  
527 oxygen, and hydrogen atoms. Viscosity of SOA was estimated using the  $T_g$ -scaled Arrhenius plot  
528 of viscosity versus  $T_g/T$  and the Gordon-Taylor approach to account for mixtures of SOA and  
529 water. The fragility parameter  $D$  was compiled for organic compounds and we found that  $D$   
530 approaches a lower limit of  $\sim 10$  ( $\pm 1.7$ ) as the molar mass increases. The resulting viscosity  
531 estimations agree well with measured viscosity of  $\alpha$ -pinene and isoprene SOA, validating our  
532 method. Using HRMS data, glass transition temperatures of individual components and viscosity  
533 of toluene SOA were predicted, also resulting in a good agreement with measurements.  
534 However, we note that the predicted viscosities were higher than the measured values suggesting  
535 that additional considerations may need to be taken into account. For example, the ionization  
536 efficiency of both low and high molar mass compounds may have a pronounced effect on the  
537 relative abundance of different classes of compounds in HRMS data. The viscosity prediction  
538 method was also applied to biomass burning particles, whose elemental composition was  
539 measured using HRMS with two different ionization techniques. Substantial differences in

540 viscosity estimations were obtained using ESI and APPI mass spectra because these two  
541 ionization methods probe different subsets of compounds.

542 Figure 10 summarizes the predicted range of viscosity of  $\alpha$ -pinene SOA, isoprene SOA  
543 (generated by PAM), toluene SOA, and biomass burning particles. Isoprene SOA has lower  
544 viscosity, reflecting lower glass transition temperature due to relatively low molar mass of  
545 isoprene oxidation products.  $\alpha$ -pinene and toluene SOA have much higher viscosity with a  
546 different shape of the RH dependence due to differences in glass transition temperatures and  
547 hygroscopicity. Biomass burning particles have moderate viscosity between the two extreme  
548 cases. Currently, both predictions and measurements are subject to large uncertainties and  
549 variations. Complementary measurements of viscosity and chemical composition employing  
550 different ionization techniques are desired to further constrain RH-dependent viscosity in future  
551 studies. Current  $T_g$  parameterizations do not consider functionality or molecular structure  
552 explicitly and further measurements of  $T_g$  and viscosity of SOA would allow us to refine the  
553 method presented in this study. Nevertheless, current results offer a promising starting point and  
554 such simple parameterizations are practical for predicting viscosity of particles as measured by  
555 HRMS. The developed viscosity prediction method should also be useful in recent efforts of  
556 simulating the distribution of SOA phase state and related properties in regional or global air  
557 quality models (e.g., Maclean et al., 2017; Shiraiwa et al., 2017).

558

## 559 **Appendix A: Conversion of fragility steepness index ( $m$ ) to fragility ( $D$ )**

560 Fragility steepness index ( $m$ ) is defined as:

561 
$$m = \lim_{T \rightarrow T_g} \frac{d \log \eta}{d(T_g/T)} \quad (\text{A1})$$

562 Combining Eq. (A1) with Eq. (6) gives:

563 
$$m = \lim_{T \rightarrow T_g} \frac{d}{d(T_g/T)} \left( -5 + 0.434 \frac{T_0 D}{T - T_0} \right) \quad (\text{A2})$$

564 Considering that  $\eta = 10^{12}$  Pa s at  $T = T_g$  (Angell, 1991), and by defining  $\Delta x = 1 - T_g/T$ , and a  
 565 combination with Eq. (7) leads to:

$$\begin{aligned}
 m &= \lim_{\Delta x \rightarrow 0} \frac{1}{\Delta x} \left( 12 - \left( -5 + 0.434 \frac{\frac{39.17 T_g}{D + 39.17} D}{\frac{T_g}{1 - \Delta x} - \frac{39.17 T_g}{D + 39.17}} \right) \right) \\
 &= \lim_{\Delta x \rightarrow 0} \frac{1}{\Delta x} \left( 17 - 0.434 \frac{39.17 T_g D (1 - \Delta x)}{D T_g + 39.17 T_g \Delta x} \right) \\
 &= \lim_{\Delta x \rightarrow 0} \frac{(665.89 + 17D)}{(D + 39.17 \Delta x)} \\
 &= \frac{665.89 + 17D}{D} \quad (\text{A3})
 \end{aligned}$$

566

567 Note that Eq. (A3) is derived assuming the high temperature limit of viscosity  $\eta_\infty$  is equal to  $10^{-5}$   
 568 Pa s (Angell, 1991) in the VTF equation (Eq. 5). Similar equations for the relation between  $m$   
 569 and  $D$  were given by previous studies using different  $\eta_\infty$  and units (Angell et al., 1994; Angell,  
 570 2002; Bones et al., 2012) and applying those gave very similar results in our study.

571

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578



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936



937 **Table 1.** Composition classes and the  $n_C^0$  and  $b$  values (K) for glass transition temperature  
 938 parameterizations obtained by least-squares optimization using the measurements compiled in  
 939 Koop et al., (2011), Dette et al., (2014) and Rothfuss and Petters (2017b).

| Classes | $n_C^0$          | $b_C$             | $b_H$               | $b_{CH}$          | $b_O$             | $b_{CO}$          |
|---------|------------------|-------------------|---------------------|-------------------|-------------------|-------------------|
| CH      | 1.96<br>(±1.81)  | 61.99<br>(±53.65) | -113.33<br>(±44.47) | 28.74<br>(±20.86) |                   |                   |
| CHO     | 12.13<br>(±2.66) | 10.95<br>(±13.60) | -41.82<br>(±14.78)  | 21.61<br>(±5.30)  | 118.96<br>(±9.72) | -24.38<br>(±4.21) |

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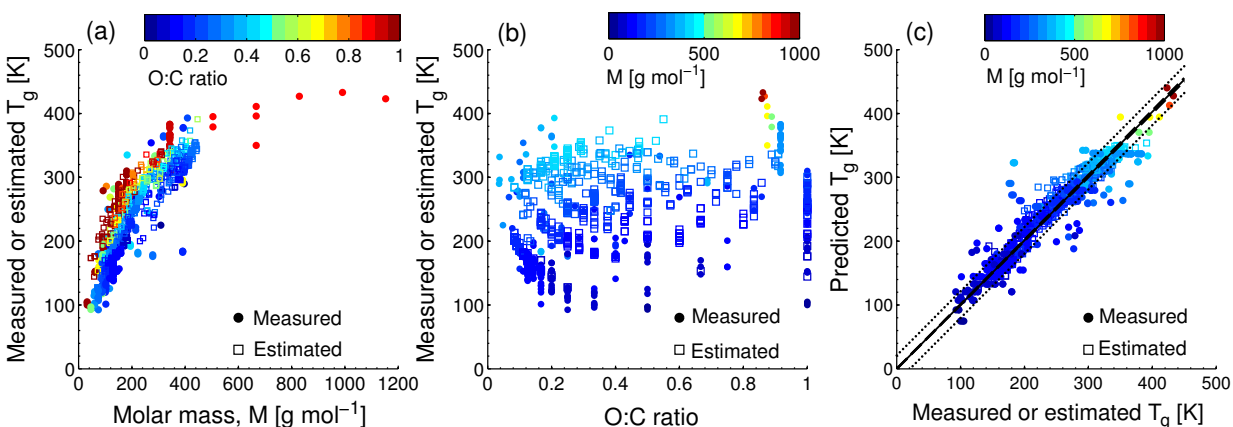
942

943 **Table 2.** Glass transition temperatures calculated using Eq. (1) and (2) for toluene SOA  
 944 produced at low relative humidity (< 2%) and high relative humidity (75%) conditions.

| $T_{g,org}$ (K) | low RH | high RH |
|-----------------|--------|---------|
| Equation (1)*   | 299    | 295     |
| Equation (2)    | 313    | 303     |

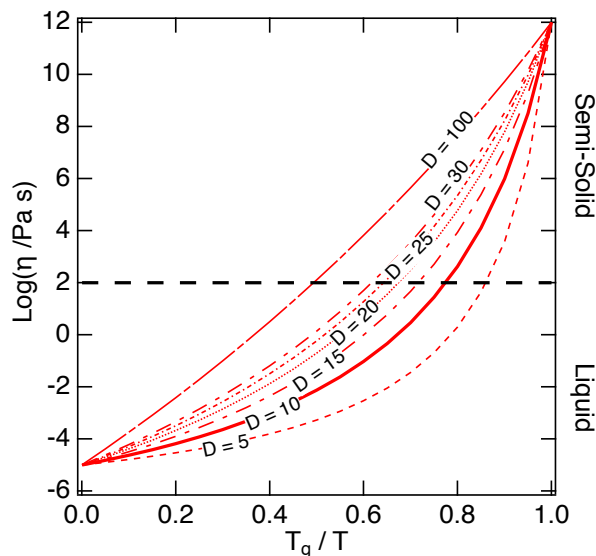
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946 \* Compounds with  $M > 450 \text{ g mol}^{-1}$  were excluded from the analysis.

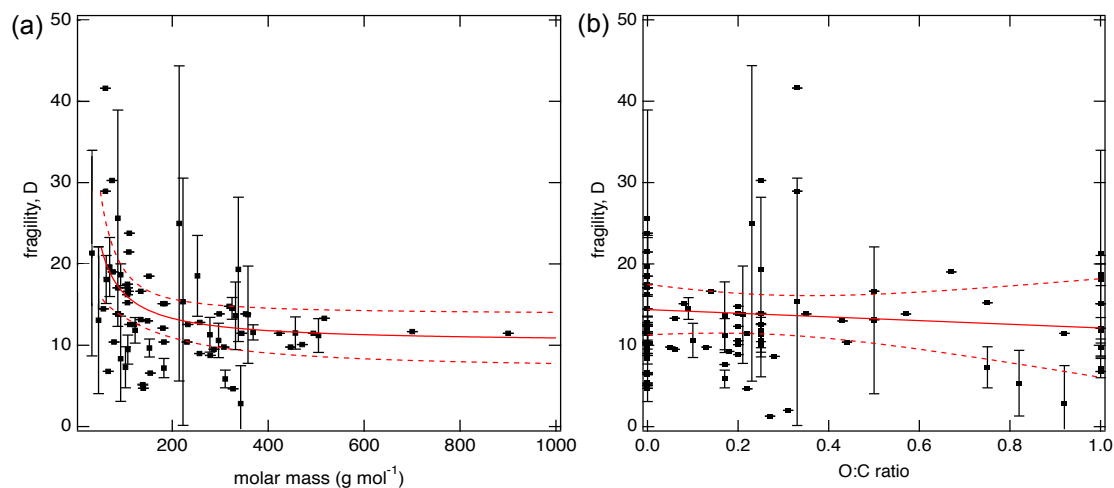


947  
 948 **Figure 1.** Characteristic relationships between molecular properties and the glass transition  
 949 temperature ( $T_g$ ) of organic compounds. (a)  $T_g$  of organic compounds as measured (circles) and  
 950 estimated with the Boyer-Kauzmann rule (squares) plotted against molar mass. The markers are  
 951 color-coded by atomic O:C ratio. (b) Measured (circles) and estimated (squares)  $T_g$  of organic  
 952 compounds plotted against O:C ratio. The markers are color-coded by molar mass. (c) Predicted  
 953  $T_g$  for CHO compounds using a parameterization (Eq. 2) developed in this study compared to  
 954 measured (circles) and estimated  $T_g$  by the Boyer-Kauzmann rule (squares). The solid line shows  
 955 1:1 line and the dashed and dotted lines show 68% confidence and prediction bands,  
 956 respectively.

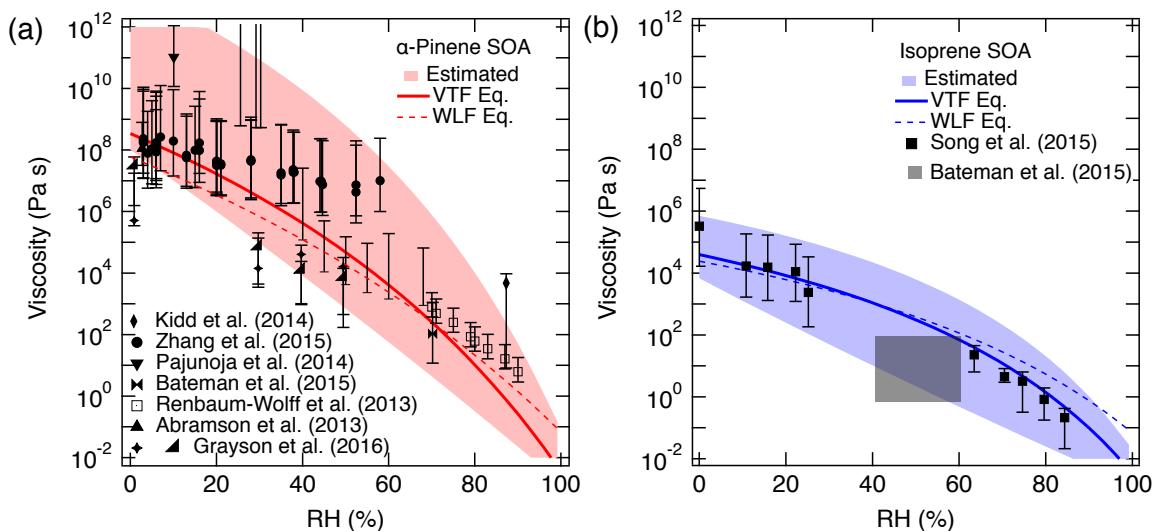
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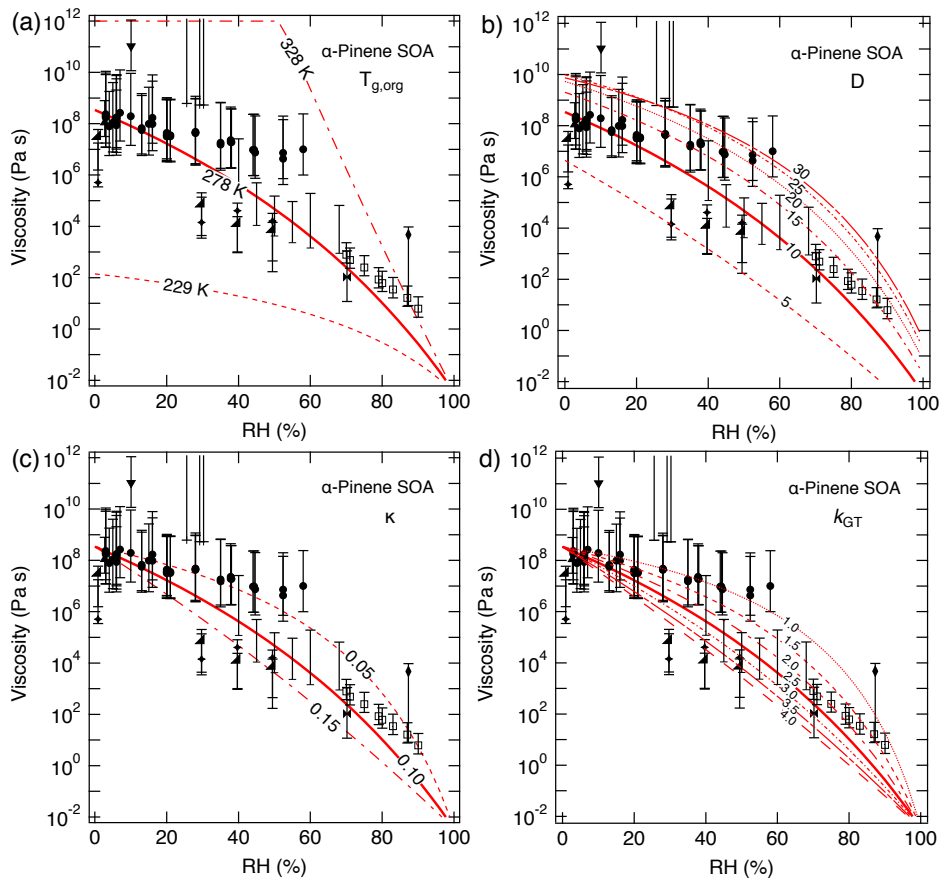
959  
 960 **Figure 2.** The Angell plot of viscosity ( $\eta$ ) vs.  $T_g/T$ . The lines represent different fragility  
 961 parameter ( $D$ ) values in the range of 5 - 100, with  $D = 10$  (the solid line) used as a base case for  
 962 this study. A large fragility parameter value is associated with a strong glass former, while  
 963 fragile materials are associated with lower values. The black dashed line at viscosity of  $10^2$  Pa s  
 964 indicates the approximate threshold between liquid and semi-solid states.



965  
 966 **Figure 3.** Fragility parameter of organic compounds ( $D$ ) plotted against (a) molar mass and (b)  
 967 atomic O:C ratio. Error bars are standard deviations. The solid red lines represent the fitted  
 968 curves with fitted equations for (a)  $D = 602.6/M + 10.3$  and (b)  $D = 14.4 - 2.3(\text{O:C})$  respectively.  
 969 Dashed red lines indicate the 95% confidence band.  
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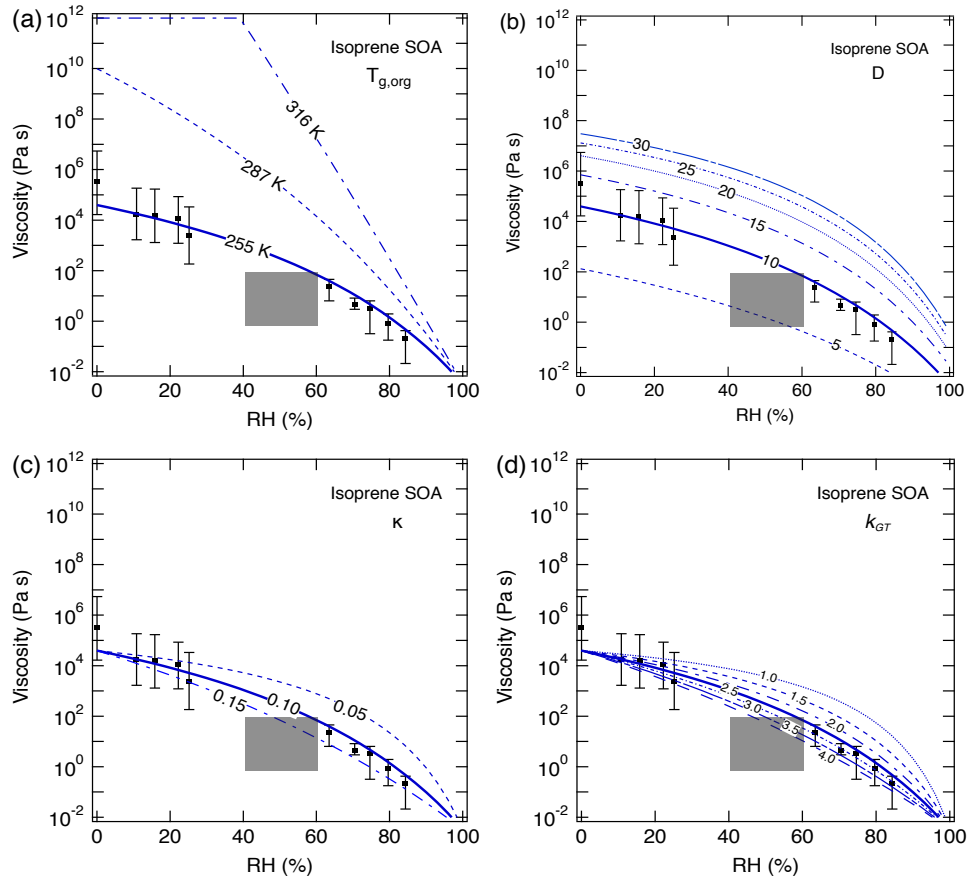


972  
 973 **Figure 4.** Comparison of measured and predicted viscosity of (a)  $\alpha$ -pinene SOA and (b) isoprene  
 974 SOA at 295 K as a function of RH. The solid lines represent base simulations with the VTF  
 975 equation, while the dotted line represents viscosity predicted using the WLF equation  
 976 [parameters: glass transition temperature of dry SOA ( $T_{g,org}$ ), fragility ( $D$ ), hygroscopicity ( $\kappa$ )  
 977 and Gordon-Taylor constant ( $k_{GT}$ ): (a) 278.5 K, 0.1, 10 and 2.5; (b) 255 K, 0.1, 10 and 2.5. The  
 978 shaded regions were determined by varying these parameters (a) upper (lower) limit:  $T_{g,org}$  = 300  
 979 K (278.5 K),  $\kappa$  = 0.1 (0.1),  $D$  = 20 (10),  $k_{GT}$  = 2.5 (2.0); (b) upper (lower limit):  $T_{g,org}$  = 255 K  
 980 (255 K),  $\kappa$  = 0.10 (0.15),  $D$  = 15 (8),  $k_{GT}$  = 2.5 (4.0). Panel (a): Renbaum-Wolff et al. (2013)  
 981 data represents viscosity for water-soluble portion of SOA; Grayson et al. (2016) data in the panel (a)  
 982 represents two different mass loadings ( $121 \mu\text{g m}^{-3}$ ;  $520 \mu\text{g m}^{-3}$ ). Panel (b): The gray box in  
 983 panel (b) represents estimated viscosity for isoprene SOA based on bounce measurements of  
 984 Bateman et al. (2015).  
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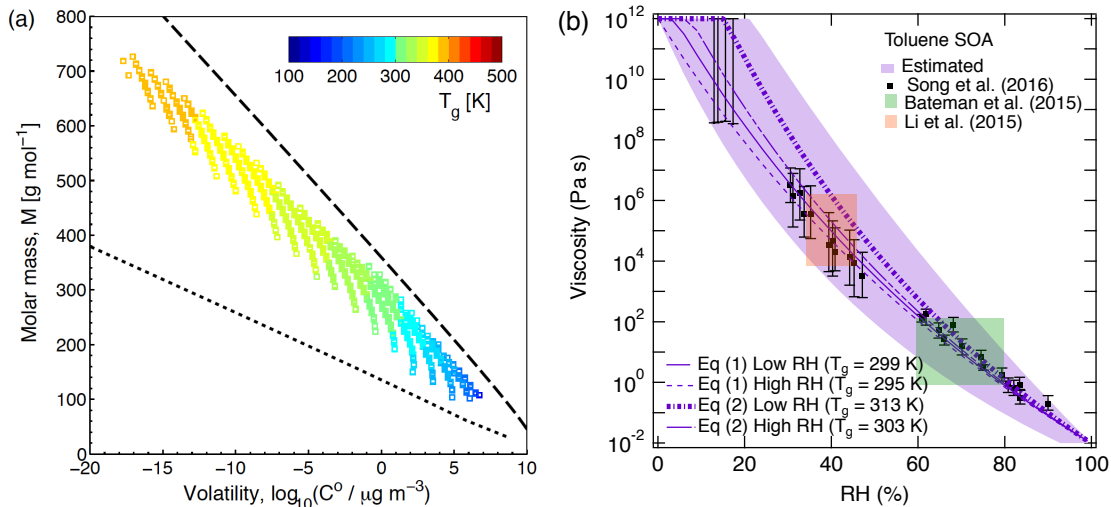
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988 **Figure 5.** Sensitivity calculations for viscosity of  $\alpha$ -pinene SOA at 295 K as a function of RH by  
 989 varying: (a) glass transition temperature of dry SOA ( $T_{g,org}$ ), (b) fragility ( $D$ ), (c) hygroscopicity  
 990 ( $\kappa$ ), and (d) Gordon-Taylor constant ( $k_{GT}$ ).



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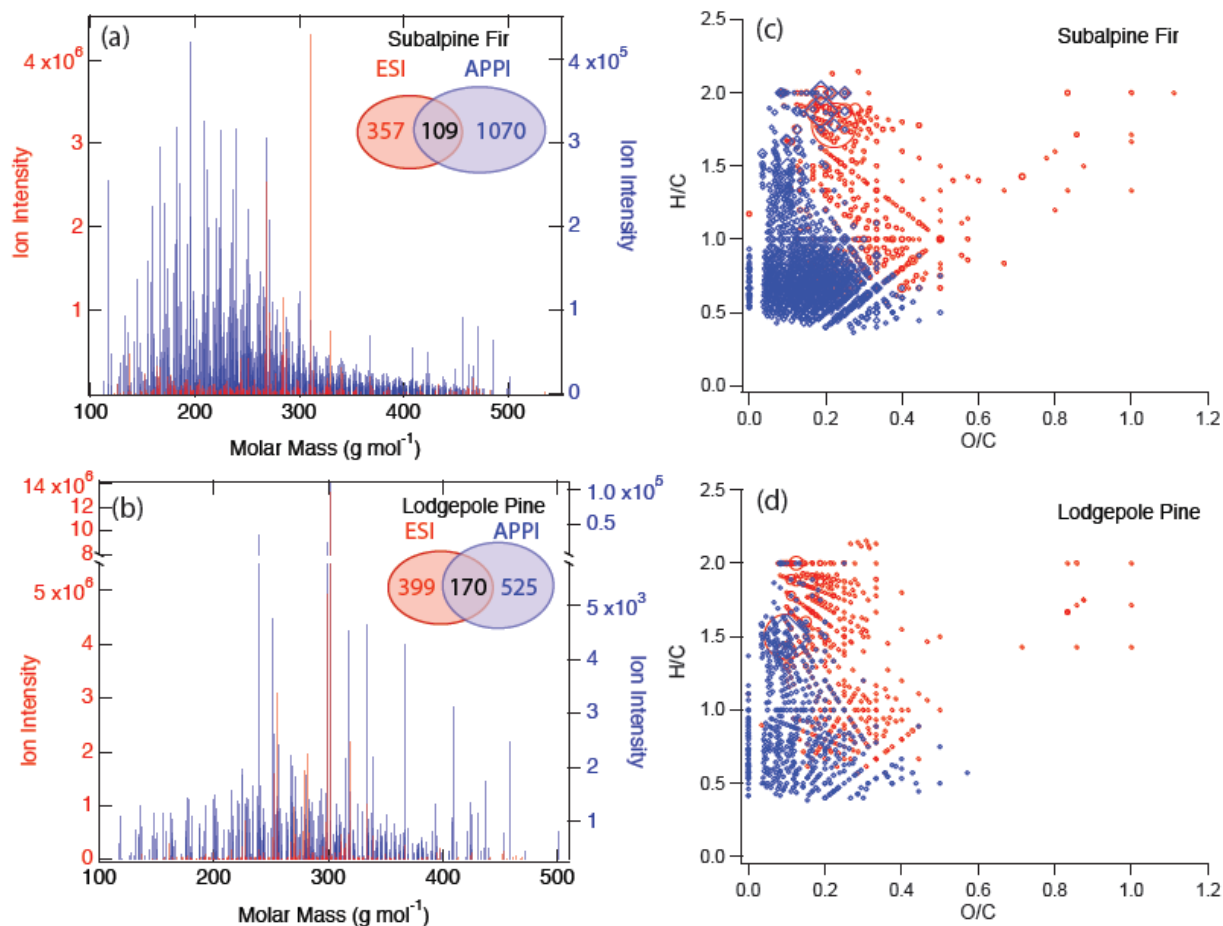
**Figure 6.** Sensitivity calculations for viscosity of isoprene SOA at 295 K as a function of RH by varying: (a) glass transition temperature of dry SOA ( $T_{g,org}$ ), (b) fragility ( $D$ ), (c) hygroscopicity ( $\kappa$ ), and (d) Gordon-Taylor constant ( $k_{GT}$ ). Data points are measured viscosity by Song et al. (2015) and the gray box represents estimated viscosity based on bounce measurements of Bateman et al. (2015).



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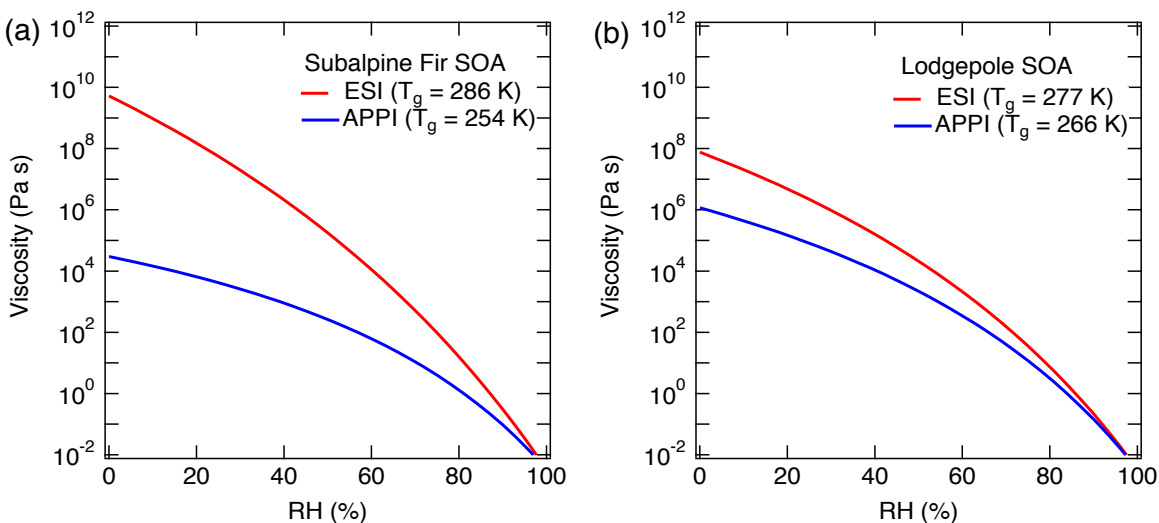
1000 **Figure 7.** (a) Molecular corridor of molar mass plotted against volatility of toluene SOA formed  
 1001 under dry conditions (Hinks et al., 2017) color-coded by glass transition temperature ( $T_g$ )  
 1002 estimated using Eq. (2). The upper dashed line indicates the low O:C bound of the molecular  
 1003 corridor (linear alkanes  $C_nH_{2n+2}$  with O:C = 0), and the lower dotted line indicates the high O:C  
 1004 bound (sugar alcohols  $C_nH_{2n+2}O_n$  with O:C = 1). (b) Comparison of measured (markers) and  
 1005 modeled (lines) viscosity of toluene SOA at 295 K as a function of RH. Viscosities were  
 1006 calculated using fragility ( $D$ ) of 13, the hygroscopicity ( $\kappa$ ) of 0.25 and the Gordon-Taylor  
 1007 constant ( $k_{GT}$ ) of 3.0 with different glass transition temperatures of dry SOA ( $T_{g,org}$ ) as estimated  
 1008 using Eq. (1) or (2) under low and high RH conditions. The shaded regions were calculated by  
 1009 varying those parameters:  $T_{g,org} = 313$  K (295 K),  $\kappa = 0.20$  (0.25),  $D = 13$  (10),  $k_{GT} = 2.5$  (3.5) for  
 1010 the upper (lower) limit. Mass loadings were  $23 \mu\text{g m}^{-3}$  for Low RH and  $8 \mu\text{g m}^{-3}$  for High RH  
 1011 (Hinks et al., 2017).

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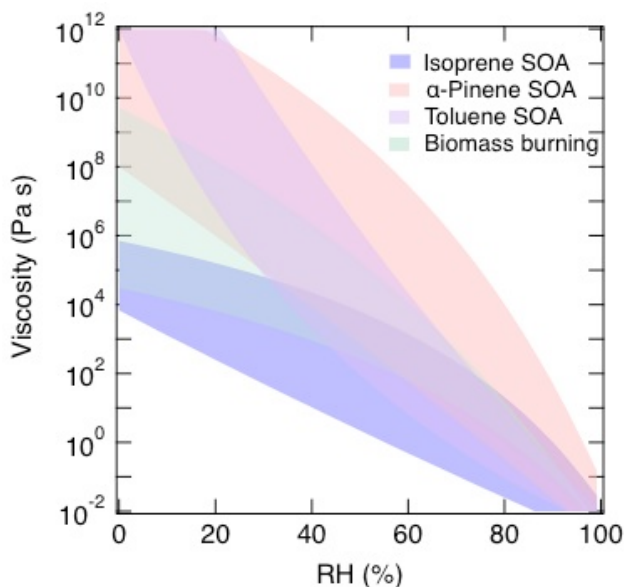
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 1014 **Figure 8.** Mass spectra of biomass burning organic particles collected from test burns of (a)  
 1015 subalpine fir and (b) lodgepole pine as measured by high resolution mass spectrometry with  
 1016 two ionization techniques: electron spray ionization (ESI, red) and atmospheric pressure  
 1017 photoionization (APPI; blue). Numbers of elemental formulas identified by ESI (red), APPI  
 1018 (blue) and both modes (black) are also specified. Van Krevelen plots of the compounds  
 1019 identified by ESI (red) and APPI (blue) mode in BBOA from burning of (c) subalpine fir and (d)  
 1020 lodgepole pine.  
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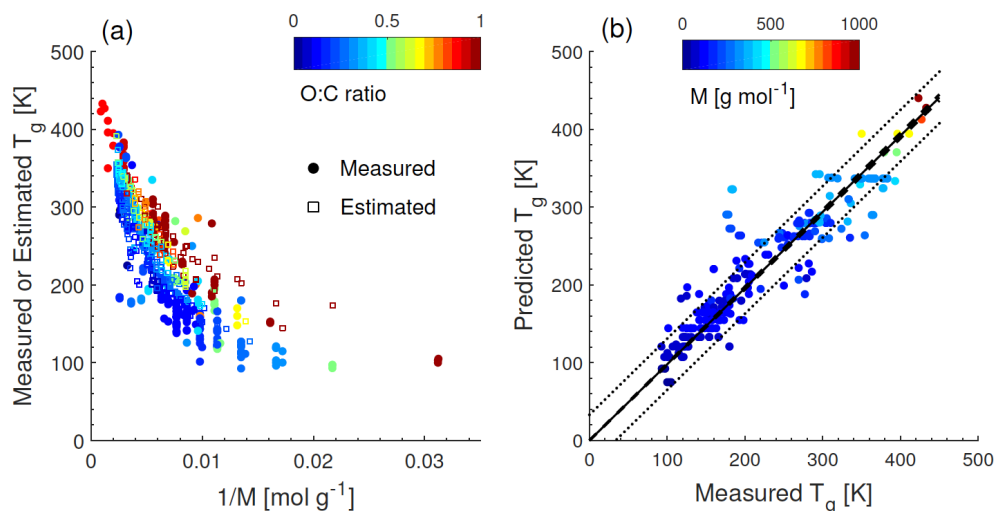
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 1023 **Figure 9.** Sensitivity of the predicted viscosity for biomass burning particles of (a) subalpine fir  
 1024 and (b) lodgepole pine trees as measured by high resolution mass spectrometry to the ionization  
 1025 technique: electrospray ionization (ESI, red) and atmospheric pressure photoionization (APPI;  
 1026 blue).  $T_{g,org}$  are specified in the figure legend and other used parameters are fixed to  $\kappa = 0.1$ ,  $D =$   
 1027  $10$ ,  $k_{GT} = 2.5$ . Different results are obtained for the same sample because ESI and APPI probe a  
 1028 different subset of compounds (Figure 8).

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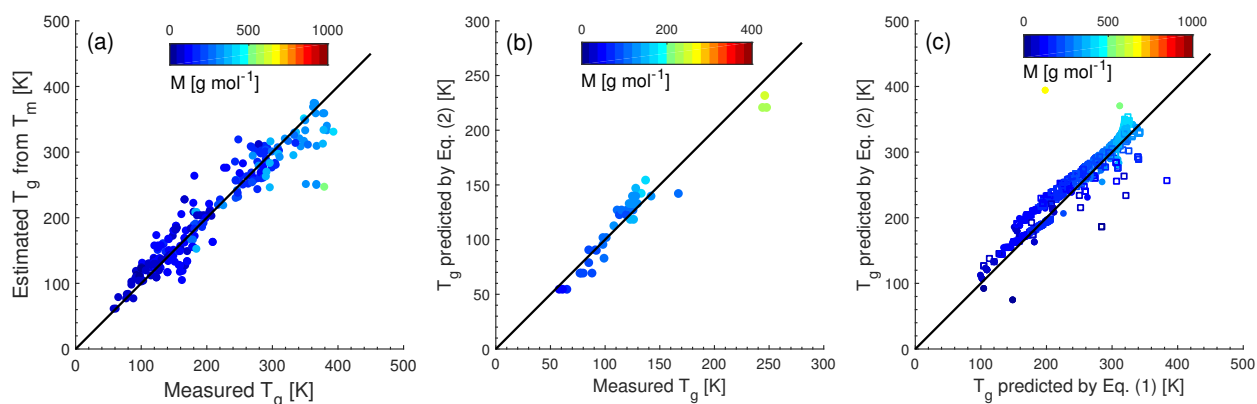


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 1034 **Figure 10.** Summary of predicted range of viscosity of  $\alpha$ -pinene SOA (red), isoprene SOA  
 1035 (blue), toluene SOA (purple), and biomass burning particles (green).

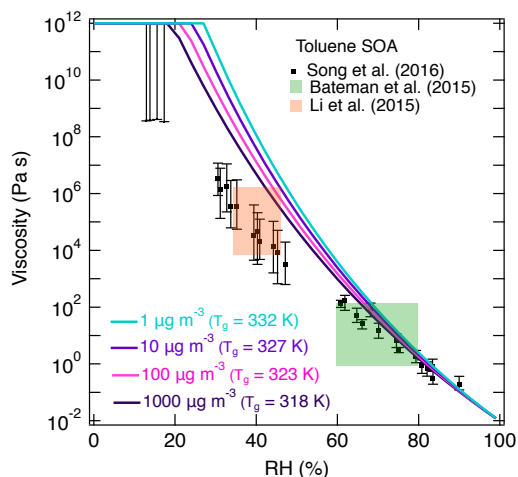
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 1038 **Figure A1.** (a)  $T_g$  of organic compounds as measured (circles) and estimated with the Boyer-  
 1039 Kauzmann rule (squares) plotted against the inverse molar mass. The markers are color-coded by  
 1040 atomic O:C ratio. (b) Predicted  $T_g$  for CHO compounds using a parameterization (Eq. 2)  
 1041 developed in this study compared to measured  $T_g$  (circles). The solid line shows 1:1 line and the  
 1042 dashed and dotted lines show 68% confidence and prediction bands, respectively.  
 1043



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 1045 **Figure A2.** (a) Comparison of measured and estimated  $T_g$  by the Boyer-Kauzmann rule for 251  
 1046 organic compounds (Koop et al., 2011; Dette et al., 2014; Rothfuss and Petters 2017b) with their  
 1047 measured  $T_m$  available. The markers are color-coded by molar mass. (b, c) Predicted  $T_g$  using Eq.  
 1048 (2) compared with (b) measured  $T_g$  for CH compounds and (c) predicted  $T_g$  using Eq. (1) for  
 1049 CHO compounds. The solid line shows 1:1 line. Solid circle markers represent organic  
 1050 compounds as compiled in Koop et al. (2011) and open square marker represent SOA oxidation  
 1051 products in Shiraiwa et al. (2014) in panel (c).  
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 1054 **Figure A3.** Effect of mass loading on predicted viscosity for toluene SOA. Solid lines represent  
 1055 the predicted viscosity with Eq. (2) using chemical composition of toluene SOA formed at low  
 1056 RH. Viscosity was predicted with different mass loadings ranging from 1-1000  $\mu\text{g m}^{-3}$ . Markers  
 1057 and shaded boxes represent experimentally measured viscosity values. Song et al. (2016a) mass  
 1058 loadings were 60-100 and 600-1000  $\mu\text{g m}^{-3}$ . Bateman et al., (2015) and Li et al., (2015) mass  
 1059 loadings were 30-50  $\mu\text{g m}^{-3}$  and 44-125  $\mu\text{g m}^{-3}$ , respectively.  
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