



# **Heterogeneous photochemistry of imidazole-2-carboxaldehyde: HO<sub>2</sub> radical formation and aerosol growth**

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## **Abstract**

The multiphase chemistry of glyoxal is a source of secondary organic aerosol (SOA), including its light-absorbing product imidazole-2-carboxaldehyde (IC). IC is a photosensitizer that can contribute to additional aerosol ageing and growth when its excited triplet state oxidizes hydrocarbons (reactive uptake) via H-transfer chemistry. We have conducted a series of photochemical coated-wall flow tube (CWFT) experiments using films of IC and citric acid (CA), an organic proxy and H-donor in the condensed-phase. The formation rate of gas-phase HO<sub>2</sub>



radicals ( $P_{HO_2}$ ) was measured indirectly by converting gas-phase NO into  $NO_2$ . We report on experiments that relied on measurements of  $NO_2$  formation, NO loss; and HONO formation.  $P_{HO_2}$  was found to be a linear function of (1) the  $[IC] \times [CA]$  concentration product, and (2) the photon actinic flux. Additionally, (3) a more complex function of relative humidity ( $25\% < RH < 63\%$ ), and of (4) the  $O_2/N_2$  ratio ( $15\% < O_2/N_2 < 56\%$ ) was observed, most likely indicating competing effects of dilution,  $HO_2$  mobility and losses in the film. The maximum  $P_{HO_2}$  was observed at 25–55% RH and at ambient  $O_2/N_2$ . The  $HO_2$  radicals form in the condensed-phase when excited IC triplet states are reduced by H-transfer from a donor, CA in our system, and subsequently react with  $O_2$  to re-generate IC, leading to a catalytic cycle. OH does not appear to be formed as a primary product but is produced from the reaction of NO with  $HO_2$  in the gas phase. Further, seed aerosols containing IC and ammonium sulfate were exposed to gas-phase limonene and  $NO_x$  in aerosol flow tube experiments, confirming significant  $P_{HO_2}$  from aerosol surfaces. Atmospheric implications consist in a potentially relevant contribution of triplet state photochemistry for gas-phase  $HO_2$  production, aerosol growth and ageing.

## 1. Introduction

The sources and sinks of radicals play an important role in the oxidative capacity of the atmosphere. Radicals and other oxidants initiate the chemical degradation of various trace gases, which is key in the troposphere (Jacob, 1999). The hydroxyl (OH) and peroxy ( $HO_2$ ) radicals belong to the  $HO_x$  chemical family and are primarily generated by ultraviolet radiation photochemical reactions (Calvert and Pitts, 1966), like the reaction of  $O(^1D)$  (from  $O_3$ ) with  $H_2O$ , or photolysis of HONO, HCHO,  $H_2O_2$ , or acetone. Some secondary gas-phase sources are the ozonolysis of alkenes or  $O(^1D) + CH_4$  (Monks, 2005). The oxidation of VOCs by OH and other oxidants in the presence of NO leads to perturbations in the  $HO_x$ ,  $NO_x$ , and  $RO_x$  radical cycles that affect  $O_3$  and aerosol formation (Monks, 2005; Sheehy et al., 2010). The kinetics and photochemical parameters of these reactions are relatively well-known in the gas-phase (Atkinson et al., 2004; Sander et al., 2011). However, this does not apply to the sources and sinks for  $HO_x$  in atmospheric droplets and on aerosol surfaces (Ervens et al., 2011). Uptake of OH from the gas-phase, and  $H_2O_2$  photolysis in the condensed phase are the primary known sources for  $HO_x$  in the condensed-phase.  $HO_2$  is highly soluble and the concentrations of OH, the most effective oxidant



58 in the condensed phase, depend on HO<sub>2</sub>. Another source of HO<sub>x</sub> radicals is from the chemical  
59 reactions of reduced metal ions and H<sub>2</sub>O<sub>2</sub>, known as Fenton reactions (Fenton, 1894; Deguillaume  
60 et al., 2005). Direct photolysis of H<sub>2</sub>O<sub>2</sub>, nitrite, nitrate (Zellner et al., 1990), hydroperoxides (Zhao  
61 et al., 2013), and light absorbing secondary organic aerosol (SOA) (Badali et al., 2015) are also  
62 sources of HO<sub>x</sub> in the condensed-phase. Other studies have shown that the photochemistry of iron  
63 (III) oxalate and carboxylate complexes, present in aqueous environments (e.g. wastewater,  
64 clouds, fogs, particles), can initiate a radical chain reaction serving as an aqueous source of HO<sub>2</sub>  
65 and Fe<sup>2+</sup>. Fe<sup>2+</sup> can then regenerate OH starting a new cycle of Fenton reactions (Weller et al.,  
66 2013a, 2013b). The temperature dependent rate constants of OH in the aqueous phase have been  
67 studied for a limited subset of organics (Ervens et al., 2003). However, there is still a wide gap  
68 with respect to understanding the sources, sinks, kinetics and photochemical reaction pathways of  
69 HO<sub>x</sub> radicals in the condensed phase (George et al., 2015).

70 Our study investigates photosensitizers as an additional HO<sub>x</sub> source that may be relevant to further  
71 modify RO<sub>x</sub> and NO<sub>x</sub> reaction cycles in both the condensed- and gas-phases. It is motivated by  
72 the formation of superoxide in terrestrial aqueous photochemistry (Draper and Crosby, 1983;  
73 Faust, 1999; Schwarzenbach et al., 2002), by more recent observations that irradiated surfaces  
74 containing titanium dioxide generate HO<sub>x</sub> radicals in the gas-phase (Yi et al., 2012) and by the  
75 generation of OH from metal oxides acting as photocatalysts in mineral dust (Dupart et al., 2012).  
76 Past studies have demonstrated the reactivity of glyoxal towards ammonium ions and amines as a  
77 source for light-absorbing brown carbon (Nozière et al., 2009; Galloway et al., 2009; Shapiro et  
78 al., 2009; Kampf et al., 2012). One of these products is imidazole-2-carboxaldehyde (IC)  
79 (Galloway et al., 2009), which absorbs light at UV wavelengths ( $\lambda < 330$  nm) (Maxut et al., 2015).  
80 Other imidazole-type compounds and light-absorbing products are formed in minor amounts but  
81 can nonetheless impact optical and radiative properties of SOAs (Sareen et al., 2010; Trainic et  
82 al., 2011). Photochemical reactions by these species are not typically accounted for in models yet,  
83 but have a possible role for SOA formation and aerosol aging mechanisms (Sumner et al., 2014).  
84 Photosensitizers are light absorbing compounds that absorb and convert the energy of photons into  
85 chemical energy that can facilitate reactions, e.g., at surfaces or within aerosols (George et al.,  
86 2015). For example, aerosol seeds containing humic acid or 4-(benzoyl)benzoic acid (4-BBA),  
87 two other known photosensitizers, can induce the reactive uptake of VOCs when exposed to light,  
88 leading to secondary organic aerosol (SOA) formation (Monge et al., 2012). Aregahegn et al.



(2013) and Rossignol et al. (2014) suggested a mechanism for autophotocatalytic aerosol growth, where radicals are produced from the reaction of an H-donor hydrocarbon species, in this case limonene, and the triplet state of IC. Field measurements on fog water samples confirmed that triplet excited states of organic compounds upon irradiation can oxidize model samples such as syringol (a biomass burning phenol) and methyl jasmonate (a green leaf volatile), accounting for 30 – 90% of their loss (Kaur et al., 2014).

The existence of such photocatalytic cycles could be of atmospheric significance. Canonica et al. (1995) suggested indeed that the initial carbonyl, triggering the photochemical properties, is regenerated via a reaction with oxygen producing HO<sub>2</sub>. To our knowledge, the production of such radical side products was not investigated under atmospheric conditions previously. We therefore report here on the HO<sub>2</sub> radical production from IC in the condensed-phase.

100

## 101 2. Experimental Section

A series of flow tube experiments were conducted to investigate the formation of gas-phase HO<sub>2</sub> radicals from IC photochemistry using two different CWFT reactors (Sect. 2.1). Section 2.2 describes aerosol flow tube experiments that in absence of other known radical sources confirm that HO<sub>2</sub> production from aerosols can start photochemistry. All experiments were performed at atmospheric pressure.

### 107 2.1. Coated-wall flow tube experiments

The CWFT experiments were designed to investigate the gas-phase production of HO<sub>2</sub> radicals from a film containing IC and citric acid (CA) matrix as a function of UV light intensity, IC concentration in the film, relative humidity (RH), and O<sub>2</sub> mixing ratio. Two similar experimental setups were used as shown in Fig. 1. Some of the differences, not major, consist in the flow reactor volume, surface area, flow rates, IC mass loading, NO mixing ratio, temperature inside the reactor and the connected instrumentation.

**Setup 1.** Experiments were conducted in a photochemical flow-system equipped with a Duran glass CWFT (0.40 cm inner radius, 45.2 and 40.0 cm length, inner surface = 113.6 and 100.4 cm<sup>2</sup>, S/V = 5.00 cm<sup>-1</sup>), which was housed in a double jacketed cell coupled to a re-circulating water bath to control the temperature at 298 K; The setup is shown in Fig. 1A. A thin film of IC+CA was



deposited inside the tubular glass flow tube. The experimental procedure for the preparation of the films is described in Sect. 2.1.2. The system consisted of seven ultraviolet lamps (UV-A range, Philips Cleo Effect 22 W: 300-420 nm, 41 cm, 2.6 cm o.d.) surrounding the flow tube in a circular arrangement of 10 cm in diameter.

**Setup 2.** The second CWFT (CWFT 0.60 cm inner radius, 50 cm length, inner surface  $188.5 \text{ cm}^2$ ,  $S/V = 3.33 \text{ cm}^{-1}$ ) reactor had a glass jacket to allow water to circulate and maintain temperature control inside the tube at 292 K. The coated-wall tubes were snugly fit into the CWFT as inserts. The CWFT was surrounded by the same seven fluorescent lamps as in Setup 1. The light passed through different circulating water cooling jackets for both setups, thus providing a different light path for each setup.

**Setup 1 and 2.** The actinic flux in the flow tube reactor,  $F_{FT}(\lambda)$ , was measured by actinometry of  $\text{NO}_2$  (see Supplement for description of  $J_{\text{NO}_2}$  measurements), independently for both setups. The flows of  $\text{N}_2$ ,  $\text{O}_2$ , air and NO were set by mass flow controllers. The RH was set by a humidifier placed after the admission of  $\text{N}_2$  and  $\text{O}_2$  gases but before the admission of NO or  $\text{NO}_2$  (see Fig. 1), in which the carrier gas bubbles through liquid water at a given temperature. The humidifier could also be by-passed to set a RH of near zero. A typical measurement sequence is described in Sect. 2.1.2.

The  $J_{\text{NO}_2}$  was measured for both Setup 1 and 2 using  $\text{NO}_2$  actinometry. The  $J_{\text{NO}_2}$  with seven lamps was found to be  $2 \times 10^{-2} \text{ s}^{-1}$  for Setup 1 and  $1 \times 10^{-2} \text{ s}^{-1}$  for Setup 2 (see Fig. S2 for Setup 1, and Supplemental Information text for both Setups). These values were compared to direct irradiance measurements in the flow tube and thus normalized (see Sect. 3.1.1).

### 2.1.1. Flow tube instrumentation

The following gas-phase products exiting the flow tube were measured by three different instruments:  $\text{NO}_2$  by the University of Colorado Light Emitting Diode Cavity-Enhanced Differential Optical Absorption Spectroscopy (LED-CE-DOAS) instrument (Thalman and Volkamer, 2010), HONO by a Long Path Absorption Photometer (LOPAP, QuMA GmbH, Heland, J., 2001; Kleffmann et al., 2002), and NO by a chemiluminescence analyzer (Ecophysics CLD 77 AM, also used for  $\text{NO}_2$  in Setup 2).  $\text{HO}_2$  radicals were indirectly measured by detecting



147 NO<sub>2</sub> with the LED-CE-DOAS (Setup 1) and by the loss of NO with the chemiluminescence  
148 detector (Setup 2). The latter was preceded by a molybdenum converter to transform HONO and  
149 NO<sub>2</sub> to NO, and by an alkaline trap for HONO. Both, trap and converter, had a bypass to allow  
150 sequential measurements and thereby obtaining the concentration of NO<sub>2</sub> and HONO separately.  
151 HONO was measured by the LOPAP during some selected experiments (Kleffmann et al., 2002,  
152 2006).

### 153 **LED-CE-DOAS**

154 The LED-CE-DOAS instrument (Thalman and Volkamer, 2010) detects NO<sub>2</sub> absorption at blue  
155 wavelengths. A high power blue LED light source (420–490 nm) is coupled to a confocal high  
156 finesse optical cavity consisting of two highly reflective mirrors ( $R = 0.999956$ ) peaking at 460  
157 nm that are placed about 87.5 cm apart (sample path length of 74 cm). The absorption path length  
158 depends on wavelength, and was about ~11 km near peak reflectivity here. A purge flow of dry  
159 nitrogen gas is added to keep the mirrors clean. The light exiting the cavity is projected onto a  
160 quartz optical fiber coupled to a Princeton Instruments Acton SP2156 Czerny-Turner imaging  
161 spectrometer with a PIXIS 400B CCD detector. The mirror reflectivity was calculated by flowing  
162 helium and nitrogen gas, exploiting the difference in the Rayleigh scattering cross sections of both  
163 gases as described in Thalman et al. (2014). The gas exiting the flow tube was directly injected  
164 into the CE-DOAS cavity, and spectra were recorded every 60 seconds, and stored on a computer.  
165 For analysis we use BBCEAS fitting at NO<sub>2</sub> concentrations exceeding few ppbv (Washenfelder et  
166 al., 2008) and DOAS least squares fitting methods at lower concentrations (Thalman et al., 2015).  
167 The mirror alignment was monitored online as part of every spectrum by observing the slant  
168 column density of oxygen collision complexes, O<sub>2</sub>-O<sub>2</sub> (O<sub>4</sub>) (Thalman and Volkamer, 2010, 2013).  
169 The following reference spectra were taken from the literature: NO<sub>2</sub> (Vandaele et al., 2002) and  
170 O<sub>2</sub>-O<sub>2</sub> collision complexes (Thalman and Volkamer, 2013b). The detection limit for NO<sub>2</sub> was 50-  
171 100 pptv.

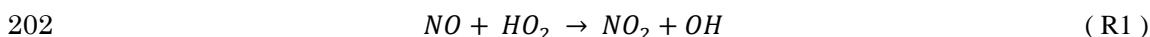
### 172 **2.1.2. Experimental conditions**

173 The IC+CA solutions were prepared by adding IC into a 1 M CA solution in 18 MΩ ultra-pure  
174 water to achieve IC to CA molecular ratios between 0.026 to 0.127 in the film. The bulk solutions  
175 for both Setup were prepared by weighing out 384-400 mg of CA in 2 mL of water and adding 4-  
176 20 mg of IC to the solution. The solutions for both setups were freshly prepared for each



177 experiment and the masses in the film were calculated at 50% RH from the CA hygroscopic growth  
 178 factors reported by Zardini et al., 2008 for both setups (for Setup 1: 5-18 mg of IC and 44 mg of  
 179 CA, for Setup 2: 1-5 mg of IC and 77 mg of CA). The range of concentrations in the films was  
 180 between 0.148 – 0.671 M.

181 The IC+CA solution coatings were produced by depositing 220-250  $\mu\text{L}$  (Setup 1) and 400  $\mu\text{L}$   
 182 (Setup 2) of the desired solution in a Duran glass tube, which was then dispersed into a thin and  
 183 viscous film. The film was dried with a gentle  $\text{N}_2$  stream humidified to a RH similar to the  
 184 experimental RH and room temperature. The film was rolled and turned upside down to deposit a  
 185 homogenous film throughout the entire inner surface of the flow tube. The homogeneity of the  
 186 film was confirmed by visual inspection. If a bright clear homogenous amorphous film from the  
 187 super-cooled solution was not observed, the film was discarded (e.g. observation of a turbid and  
 188 cracked crystallized appearance). The carrier gas flows consisted of premixed dry  $\text{N}_2$  and  $\text{O}_2$  (a  
 189 ratio of 4.5/1 in Setup 1 and a ratio of 2 in Setup 2), and NO controlled by mass flow controllers.  
 190 The total flow rates were: 500 mL/min for Setup 1 and 1500 mL/min for Setup 2. In Setup 1, a  
 191 dilution flow of 1000 mL/min was added at the end of the flow tube for a total of 1500 mL/min  
 192 during experiments when HONO was measured along with  $\text{NO}_2$ . All experiments were conducted  
 193 at ambient pressure, leading to gas residence times of 2.1 – 2.4 s (depending on flow tube volume,  
 194 for both setups) under laminar flow conditions. The  $\text{O}_2$  flow rate was varied between 0-110  
 195 mL/min to observe the dependence of  $\text{O}_2$  while keeping the total flow rate constant. A ratio of  
 196 4.5:1 of  $\text{N}_2$ : $\text{O}_2$  was maintained if any of the other gas flows were changed (e.g. NO, and/or  $\text{NO}_2$ )  
 197 for Setup 1. For Setup 2, a ratio of 2:1 of  $\text{N}_2$ : $\text{O}_2$  was also maintained, except for the  $\text{O}_2$   
 198 concentration dependence studies. The RH was kept constant at 50% RH during most experiments,  
 199 and varied between 10-60% RH to study humidity effects of the  $\text{HO}_2$  radical production. The  
 200 concentration of NO was  $\sim 1$  ppmv (Setup 1) and varied between 100 and 500 ppbv (Setup 2).  
 201 Scavenging of  $\text{HO}_2$  was achieved by the following reaction:



203 The lifetime of  $\text{HO}_2$  is about 5 ms when  $2.5 \times 10^{13}$  molecules  $\text{cm}^{-3}$  of NO are present (Setup 1),  
 204 which assures efficient conversion of  $\text{HO}_2$  molecules into  $\text{NO}_2$  ( $k = 8.0 \times 10^{-12}$   $\text{cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$   
 205 at 298 K, Sander et al., 2011). As shown in Fig. S1, 500 ppbv NO, the concentration used in Setup  
 206 2, was sufficient to efficiently convert  $\text{HO}_2$  into  $\text{NO}_2$ , see Sect. 3.1.1. The lifetime of gas phase





HO<sub>2</sub> with respect to loss to the organic film is about 0.1 s, based on a similar formula shown in Equation S3, where  $\gamma = 10^{-3}$  (upper limit by Lakey et al., 2015). Note that in view of the essentially diffusion controlled loss of HO<sub>2</sub> to the CWFT and tubing walls, the chosen scheme for determining the production of HO<sub>2</sub> radicals from the films by fast scavenging with NO is superior to a more selective detection method, e.g. LIF, which would require passing the HO<sub>2</sub> radicals into a separate setup with substantial losses. For selective experiments, the films were exposed to UV irradiation for over six hours which showed a minor change in the decrease of NO<sub>2</sub> concluding the stability of the reactivity of the films.

### 2.1.3. $J_{IC}$ calculations

The absorption cross section of IC and the calculated photolysis rate are shown in Fig. S3. The photolysis frequencies of IC were calculated using a similar procedure as described in Schwarzenbach et al. (2002). The spectral irradiance in the flow tube system was interpolated to the surface area of the flow tube to calculate the spectral photon flux density and the absorbed photon flux:

$$F_a^{IC} = \int_{300}^{420} F \times [1 - 10^{-\sigma_{IC}(\lambda) \times b \times C_{IC}}] d\lambda, \quad \text{where } F = \frac{F_{FT}(\lambda) \times SA}{N_a \times V_{film}}, \quad (1)$$

Where  $F_a^{IC}$  is the mean absorbed photon flux in Ein L<sup>-1</sup> s<sup>-1</sup> nm<sup>-1</sup> (1 Ein = 3.0 × 10<sup>5</sup> J per mole of photons at 400 nm),  $F$  is the spectral flux density that reaches the film in the flow tube in moles L<sup>-1</sup> s<sup>-1</sup> nm<sup>-1</sup>,  $b$  is the optical path length taken as the thickness of the film and  $C_{IC}$  is the concentration of IC in the film, and  $\sigma_{IC}$  is the IC absorption cross section. The absorption spectrum of IC in water was based on the measurements by Kampf et al. (2012), and re-normalized to the peak value of 10205 ± 2400 M<sup>-1</sup> cm<sup>-1</sup> at 284 nm (Maxut et al., 2015).  $V_{film}$  is the volume of the film calculated from the deposited mass of CA and the hygroscopic growth factors of CA (Zardini et al., 2008),  $SA$  is the surface area of the flow tube of the film, taken as the geometric area of the inner surface area of the flow tube in cm<sup>2</sup>,  $N_a$  is Avogadro's number in molecules mole<sup>-1</sup>. The IC photoexcitation rate  $J_{IC}$  was about 1.0 × 10<sup>-3</sup> s<sup>-1</sup> (upper limit).

We have also attempted to calculate an effective quantum yield for the formation of gas-phase HO<sub>2</sub> radicals ( $\phi_{HO2}$ ):

$$P_{HO2} = \frac{[NO_2] \times flow}{N_a \times V_{film}} \quad \phi_{HO2} = \frac{P_{HO2}}{F_a^{IC}} \quad (2)$$





Where  $P_{HO_2}$  is the  $HO_2$  production rate in  $\text{mol L}^{-1} \text{s}^{-1}$ ,  $F_a^{IC}$  is the calculated mean absorbed photon flux by IC (Eq. 1),  $[NO_2]$  is the gas-phase concentration of  $NO_2$  in molecules  $\text{cm}^{-3}$  assuming a 1:1 ratio to  $HO_2$  conversion,  $flow$  is the volumetric gas flow at the temperature in the CWTF and atmospheric pressure in  $\text{cm}^3 \text{s}^{-1}$ , and  $V_{film}$  is in L.

## 2.2. Aerosol flow-reactor experiments

A detailed description of the aerosol flow tube (AFT) is reported elsewhere (Monge et al., 2012; Aregahegn et al., 2013), therefore, only some principles are recalled below. The SOA experiments were conducted in a horizontal, cylindrical, Pyrex, aerosol flow reactor (13 cm i. d., 152 cm length) surrounded by seven UV lamps (Philips CLEO, 80W) with a continuous emission spectrum ranging from 300-420 nm (total irradiance of  $3.31 \times 10^{16}$  photons  $\text{cm}^{-2} \text{s}^{-1}$ ). The flow reactor consisted of Teflon stoppers and different flow controllers that maintained the gas/aerosol/UV irradiation contact time between 20-50 minutes. This flow reactor also consisted of an outer jacket that controlled the temperature at  $293 \pm 2$  K by water circulation using a thermostat (Model Huber CC 405).

Seed aerosols (50 nm) were produced by nebulizing a solution (at pH 6) containing ammonium sulfate (AS, 0.95 mM) and IC (1.3 mM), size selected by a DMA, and exposed to gas-phase limonene (500 ppbv) in the aerosol flow reactor. The typical aerosol mass loading in the reactor was  $2\text{-}3 \mu\text{g cm}^{-3}$ , corresponding to  $\sim 15000$  particles  $\text{cm}^{-3}$  with a starting diameter of 50 nm. As shown by Aregahegn et al. (in 2013), limonene is an efficient H-donor VOC that forms SOA via reactive uptake to IC containing seed aerosol. Due to the excess of limonene, and low seed aerosol surface are the consumption of limonene was below the detection limit. The aerosol growth was measured by means of an Ultrafine Condensation Particle Counter (UCPC) and a Scanning Mobility Particle Sizer Spectrometer (SMPS; both TSI), and similarly to the CWFT experiment, a flow of gaseous NO (from a 1 ppmv cylinder, Linde) was added to the carrier gas, and its conversion to  $NO_2$  monitored by chemiluminescence detector with a detection limit of 0.05 ppbv (ECO PHYSICS CLD 88). Due to the long residence time, the  $NO_2$  concentration is affected by its photolysis in the AFT. As discussed below,  $P_{HO_2}$  was calculated, in this case, from the growth of the particle diameter measured at the exit of the flow tube; the assumption is that growth was due to reactive uptake of limonene only, and that each limonene forms one  $HO_2$  radical. At 30 ppbv NO, the  $HO_2$  radical lifetime is around 2 sec.



### 265 **2.2.1. Experimental conditions**

266 The total flow rate in the aerosol flow reactor was between 400 – 1000 ml/min, ensuring laminar  
267 flow conditions. The RH was varied between 0 – 50%. The RH of particles in the flow reactor  
268 was controlled by saturating the carrier gas via a bubbler containing ultra-pure water (Milli Q, 18  
269 Mohm). The RH in the flow reactor system was varied by changing the gas flow rates to the  
270 bubbler and the temperature of the circulating water jacket of the bubbler. The RH was measured  
271 with a humidity sensor (Meltec UFT 75-AT, Germany) at the exit of the flow reactor. The  
272 concentrations for the flow tube experiments were the following: 30 ppbv of NO and 500 ppbv of  
273 limonene.

### 274 **2.3. Chemicals**

275 The following chemicals were used without further purification for CWFT studies: IC (97%,  
276 Sigma Aldrich), and CA (Sigma Aldrich). For Setup 1, the Duran glass tubes were soaked in a  
277 deconex® cleaning solution overnight, the next day they were rinsed with 18 MΩ water (Milli Q  
278 Element system). These flow tubes were etched with a 5% hydrofluoric acid solution after the  
279 washing procedure and again rinsed with water before any experimental use. The Duran flow  
280 tubes for Setup 2 were not initially etched with any acid but stored in a NaOH solution after  
281 washing and lastly rinsed with water; Setup 2 later confirmed that the treatment of flow tube with  
282 acids affects  $P_{HO_2}$  by rinsing with HCl and etching with HF solutions.

283 For the aerosol flow-reactor experiments gas-phase limonene was generated from commercially  
284 available limonene (Aldrich, 97%) by means of a permeation tube. The following chemicals were  
285 used without further purification: IC (97%, Sigma Aldrich) and succinic acid (Sigma Aldrich,  
286  $\geq 99.5\%$ ); 4-benzoylbenzoic acid (4-BBA, Aldrich 99%) and adipic acid (AA, Aldrich,  $\geq 99.5\%$ )  
287 were used to expand the CWFT studies to other photosensitizers.

288

## 289 **3. Results and Discussion**

### 290 **3.1. Coated-wall flow tube**

291 The following results represent the light dependent formation of  $HO_2$  indirectly from  
292 measurements of  $NO_2$  production and NO loss, measured with setup 1 and 2, respectively. Figure



293 2 shows a time series of NO<sub>2</sub> measured with setup 1 as a function of UV-A light, which confirms  
294 the light dependent radical production. This particular film had an IC/CA ratio of 0.026 (0.148M  
295 IC and 5.77M CA in the film). An evident increase of NO<sub>2</sub> is observed upon UV irradiation,  
296 directly reflecting the light mediated release of HO<sub>2</sub>, as shown in reaction (R1). The NO<sub>2</sub> signal  
297 decrease over time with all seven lamps was a common feature observed in all films; this could be  
298 due to HO<sub>2</sub> sinks in the film increasing with time, thus, the system only slowly evolves into a  
299 steady state. A small amount of NO<sub>2</sub> (0.5-1.5 ppbv) was observed during experiments that used  
300 only CA in absence of IC; therefore, the data in Fig. 2 and all data reported below have been  
301 corrected for this NO<sub>2</sub> background, measured routinely in between experiments. Figure 2 also  
302 indicates a strong correlation with irradiance, which is further discussed in the context of Fig. 4.  
303 Each data point was measured from a freshly prepared coated film in the flow tube. The  
304 uncertainty for experiments was based on the standard deviation of  $n$ , the number of experiments.  
305 The total uncertainty was  $\pm 6$ -27% (propagated error for normalization was  $\pm 7$ -29%) for the IC  
306 mass loading experiments in Setup 1 and up to a factor of two for the light dependence  
307 experiments. The uncertainty in Setup 2 was 10-50%. As discussed earlier, the lifetime of HO<sub>2</sub> in  
308 the system was about three orders of magnitude less than the residence time in the flow tube,  
309 therefore suggesting that most, if not all, reacted with NO to produce the observed NO<sub>2</sub> (R1).  
310 Theoretically, the system was clean of other oxidants such as O<sub>3</sub> (and thus NO<sub>3</sub>). The uptake of  
311 NO<sub>2</sub> in the film was very small to further produce any nitrate radicals, and the photolysis of NO<sub>2</sub>  
312 in the experiments to produce O<sub>3</sub> was insignificant ( $< 1\%$ ). The recombination of NO and O<sub>3</sub>  
313 contributes a negligible ( $< 0.1\%$ ) NO<sub>2</sub> source under our experimental conditions. RO<sub>2</sub> generation  
314 from the reaction between CA and OH from HONO photolysis was also ruled out since it is  
315 approximated to account for only 1% of the NO<sub>2</sub> production if we assume every OH from the  
316 photolysis reacts with CA. To our knowledge, the direct photolysis of CA to produce any RO<sub>2</sub>  
317 radicals has not been observed. Therefore, we believe that HO<sub>2</sub> is the essential oxidant for NO  
318 and refer to the measured NO<sub>2</sub> as HO<sub>2</sub> formation.

319 Figure 3 shows that the HO<sub>2</sub> production fluxes, in molecules cm<sup>-2</sup> min<sup>-1</sup>, increased with IC mass  
320 loading. The CA concentration was kept constant, and results are shown as the product between  
321 [IC]  $\times$  [CA], since we expect that the production rate of HO<sub>2</sub> is proportional to the concentration  
322 of IC, at constant illumination, and that of the potential H-donor, CA. For Setup 1, the HO<sub>2</sub> fluxes  
323 were measured as NO<sub>2</sub> mixing ratios, and calculated using the following equation:



$$Fluxes_{HO_2} = \frac{[NO_2] \times flow}{SA} \quad (3)$$

the description of these parameters have been previously explained (see Sect. 2.1.3). For Setup 2, the  $HO_2$  flux was calculated similarly, but only about half of the observed NO was considered to account for the loss of NO via the reaction with OH (see reaction in Supplement R1), meaning that for each  $HO_2$  scavenged two NO molecules were lost. In Figure 3, the data from Setup 1 are represented by the black squares and the data from Setup 2 are represented by the gray circles. Setup 1 measurements were taken at about ~50% RH and at room temperature. Setup 2 measurements were taken at 45% RH and at 292 K. Temperature has an effect on the observed gas-phase  $HO_2$  release from the film and thus needs to be accounted for, which is not accounted for in Fig. 3 but it is described in detail in Sect. 3.1.1.

Figure 4 shows that the  $HO_2$  production exhibited a linear dependence on the actinic flux for various  $[IC] \times [CA]$  molar products. From Sect. 2.1.3, we estimated an experimental  $\phi_{HO_2}$  of about  $6 \times 10^{-5}$ , reflecting other probable, unknown quenching processes in our system. Figure 4 also shows the formation of HONO from three different IC mass loadings. In all three cases the HONO:NO<sub>2</sub> ratio is < 1, confirming  $HO_2$  as a primary product and OH as a secondary product. Figure 5 shows the dependence of  $HO_2$  production observed via the loss of NO (Setup 2) on relative humidity (0 – 65%). Water partial pressure is an important parameter in the atmosphere and it seems to also have an important effect on the photochemical reactions studied here. At RH below ~10%, and at high RH above ~55%, the yield of  $HO_2$  radicals decreases. The maximum  $HO_2$  radical production is observed at moderate RH (20 – 55%). This is probably due to a combination of factors. In particular, at low RH the film may become more viscous reducing mobility, and thus the energy transfer within the film. This may decrease the  $HO_2$  yield as shown in Fig. 5. The reduced diffusivity of  $HO_2$  may also increase the residence time in the film and facilitate the self-reaction in the bulk phase: The diffusivity of  $H_2O$  in citric acid is in the range of  $10^{-7} - 10^{-8} \text{ cm}^2 \text{ s}^{-1}$  at 50% RH. If the  $HO_2$  diffusivity is between a factor of 10 and 100 lower than that of  $H_2O$  due to its larger size,  $10^{-9} \text{ cm}^2 \text{ s}^{-1}$ , the first order loss rate coefficient for diffusion out of the film,  $D/\delta^2$ ,  $\delta$  denoting the film thickness ( $4 \times 10^{-4} \text{ cm}$ ), becomes about  $k_D = 10^{-2} \text{ s}^{-1}$ . From the observed  $F_{HO_2}$ , the steady state concentration is then about  $F_{HO_2}/k_D/\delta = 4 \times 10^{16} \text{ cm}^{-3} = 10^{-7} \text{ M}$ . The loss rate coefficient due to  $HO_2$  self-reaction in the condensed phase ( $7.8 \times 10^5 \text{ M}^{-1} \text{ s}^{-1}$ ) at this concentration would become nearly  $0.1 \text{ s}^{-1}$ , somewhat higher than that for diffusional loss. Of



course these estimates carry a high uncertainty, but indicate that at lower humidity diffusivity gets low enough to effectively reduce the diffusional loss of HO<sub>2</sub> to the gas phase and favor its loss by self-reaction in the condensed phase. The potential presence of condensed phase sinks, such as RO<sub>2</sub>, formed from secondary chemistry of oxidized citric acid may add to this uncertainty. At high RH (> 55%), the amount of water associated with CA dilutes the reactants, and quenching of the excited IC triplet states gains in relative importance, consistent with findings in other studies (Stemmler et al., 2006, 2007; Jammoul et al., 2008). The RH effect can decrease the HO<sub>2</sub> production by a factor of 3, compared to the plateau of maximum HO<sub>2</sub> production between 20 – 55% RH.

Figure 6 shows the dependence of the HO<sub>2</sub> production based on the observed NO loss on the O<sub>2</sub> mixing ratio (Setup 2). The HO<sub>2</sub> production varied by about 20% over the range of conditions investigated. A marginal decrease below 15% O<sub>2</sub> appears to be significant compared to the maximum HO<sub>2</sub> production at ~40% O<sub>2</sub>, indicating that O<sub>2</sub> is needed for HO<sub>2</sub> formation. Sufficient O<sub>2</sub> dissolves in the aqueous phase to produce HO<sub>2</sub> radicals efficiently at atmospheric O<sub>2</sub> mixing ratios. Above 55% O<sub>2</sub> the HO<sub>2</sub> production decreased, which is probably due to quenching of excited IC triplet states by O<sub>2</sub>. Our results are qualitatively consistent with the observations of decreasing aerosol growth at high O<sub>2</sub> in the autophotocatalytic aerosol growth described in Aregahegn et al. (2013).

In order to test the possibility for excited IC triplet states to react with NO<sub>2</sub> at the surface of the film, experiments were conducted with NO<sub>2</sub>. While we did observe that the uptake of NO<sub>2</sub> on irradiated surfaces scaled with light intensity (see Fig. S4) the reactive uptake coefficient of NO<sub>2</sub> to produce HONO at the surface is rather small ( $< 2.5 \times 10^{-7}$ ), corresponding to a  $k_w$  of  $10^{-3} \text{ s}^{-1}$  and thus neither a significant loss of NO<sub>2</sub> nor a significant source of HONO. The primary fate of the nitrogen-containing aromatic alkoxy IC radical under atmospheric conditions is reaction with O<sub>2</sub>. However, we have not tested alternative quenching reactions of the triplet state, or other pathways of the reduced ketyl radical that do not result into formation of HONO.

### 3.1.1 Comparison of data sets

The experimental conditions probed differ in the actinic flux, NO concentration, temperature, and acidity. Here, we use the dependencies established in Sect. 3.1 to compare results from both setups. The data from Setup 2 were normalized to conditions of Setup 1. The difference in  $J_{\text{NO}_2}$



corresponds to multiplying results from Setup 2 with a factor of  $2.0 \pm 0.1$ .  $\text{HO}_2$  was measured indirectly by reacting it with NO, and Fig. S1 indicates the minimum NO concentration needed to efficiently scavenge all gas-phase  $\text{HO}_2$  is  $\sim 460$  ppbv of NO, indicating efficient conversion for Setup 1, and a conversion efficiency of  $\sim 0.6$  for Setup 2. The data from Setup 2 were multiplied by  $1.66 \pm 0.10$  to normalize for the NO conversion efficiency (Fig. S1), and by an additional factor  $1.25 \pm 0.10$  to match temperatures. We observed some limited variability depending on whether HF or HCl were used to clean the flow tube prior to experiments. A higher  $P_{\text{HO}_2}$  was observed when cleaning with HF (Setup 1) compared to storing in NaOH and either rinsing with water or HCl (Setup 2); this is accounted by multiplying data from Setup 2 with a factor of  $1.25 \pm 0.30$ . Notably, the error of the correction for the cleaning procedure that is propagated here is larger than the correction factor. The effect of the pretreatment of the flow tubes was not systematically studied, and thus remains a primary uncertainty in the comparison. No further correction was applied for slight differences in RH. The overall correction factor amounts to  $5.2 \pm 1.4$ , with the error reflecting the propagated uncertainty. This explains most the difference in  $P_{\text{HO}_2}$  between both setups. The normalized results agree within a factor of 2, which is a reasonably good agreement.

### 3.1.2 Extension to other photosensitizers

A limited number of experiments were performed using the CWFT approach, using 4-BBA as a photosensitizer, in presence of 790 ppbv of gaseous limonene (a possible H-donor) and NO. The organic thin film contained an organic acid matrix made of 4-BBA with/without adipic acid. Also in this system a substantial conversion of NO into  $\text{NO}_2$  was observed. That 4-BBA behaves similar to the IC system demonstrates that the chemistry discussed above can occur on different excited carbonyls. It is interesting to note that this photo-induced conversion, and  $\text{HO}_2$  production, was observed to be sustained over long times i.e., more than 15 h probably due to the catalytic nature of the underlying chemical cycles. However, a fraction of the IC did get consumed by photolysis reactions that do not form the excited triplet state (observed during overnight experiments). The  $\text{HO}_2$  flux for the 4-BBA system was estimated to be  $2.77 \times 10^{10}$  molecules  $\text{cm}^{-2} \text{min}^{-1}$  making the same assumption that each  $\text{HO}_2$  molecule reacts with NO to generate an  $\text{NO}_2$  molecule. The calculation is based on Eq. 3, where it depends on the concentration of  $\text{NO}_2$  as well as the surface area and residence time.

### 3.2. Aerosol Flow Tube



414 The aerosol flow tube experiments were conducted similarly to the study by Aregahegn et al.  
415 (2013), i.e., who demonstrated that in the absence of NO and known gas phase oxidants, seed  
416 particles containing IC can initiate SOA growth in presence of a gaseous H-donor (limonene).  
417 Figure 7 shows the results from similar experiments when NO was added to the system. No  
418 conversion of NO to NO<sub>2</sub> was observed prior to the injection of limonene into the flow tube. The  
419 presence of a gaseous H-donor and light clearly initiated a series of photochemical processes,  
420 leading to SOA growth and gaseous NO<sub>2</sub> production. However, the quantitative interpretation  
421 of these experiments is not straightforward due to efficient radical cycling in the  
422 VOC/NO<sub>x</sub>/light photochemical system, and the lack of a blank experiment that did not contain  
423 IC as part of the seed particles. Limitations arise from the much longer residence time, which  
424 allows NO<sub>2</sub> to be significantly photolyzed. The  $J_{NO_2}$  was estimated as  $\sim 6.75 \times 10^{-3} \text{ s}^{-1}$ , and  
425 corresponds to a photolysis lifetime of 2.5 minutes, which is smaller than the actual residence  
426 time in the flow tube ( $\sim 40$  mins). Secondary chemistry can lead, among others, to ozone  
427 production (O<sub>3</sub> lifetime at 500 ppbv limonene is  $\sim 7$  min), and secondary OH radical formation  
428 from the ozonolysis of limonene. Notably, NO<sub>x</sub> is not consumed in Fig. 7. The overall effect  
429 of this secondary chemistry is an increased SOA growth compared to an experiment without  
430 added NO (Aregahegn et al., 2013). As a consequence, the NO<sub>2</sub> yield cannot be used directly  
431 to assess P<sub>HO<sub>2</sub></sub> in presence of NO.

432 However, in the absence of NO these secondary processes can largely be avoided, and are  
433 reduced at a level where they cannot be identified (Aregahegn et al., 2013). Under such  
434 conditions, the particle growth rates presumably carry information about the photosensitizer  
435 cycling and subsequent HO<sub>2</sub> production. If we assume one molecule of limonene reacts to  
436 produce one HO<sub>2</sub>, the volume change of aerosols is proportional to the overall number of HO<sub>2</sub>  
437 produced. For example, a growth of 15,000 particles cm<sup>-3</sup> from diameter 51.4 nm to 68.5 nm in 40  
438 mins (residence time) is equal to P<sub>HO<sub>2</sub></sub> of  $1.67 \times 10^{14} \text{ molecules cm}^{-2} \text{ min}^{-1}$ . This should be  
439 interpreted as an upper limit for the actual P<sub>HO<sub>2</sub></sub>, because water uptake may also be  
440 contributing to the volume growth. However, compared to the CWFT experiments the much  
441 higher surface to volume ratio of nanoparticles is expected to enhance the chemical coupling  
442 of a gas-phase H-donor and the excited IC triplet state at the aerosol surface. This is at least  
443 in part deemed responsible for the two orders of magnitude higher P<sub>HO<sub>2</sub></sub> in the aerosol flow





444 tube compared to the CWFT experiments. Notably, even if  $\phi_{HO_2}$  in the aerosol flow tube was  
 445 two order of magnitude higher than in the CWFT, it is still significantly smaller than unity.

### 446 **Primary HO<sub>2</sub> formation from IC**

447 One of the main advantages of the CWFT is that it operates at much shorter residence time. From  
 448 Setup 1, we derive a  $P_{HO_2}$  of  $1.76 \times 10^{12}$  molecules  $\text{cm}^{-2} \text{min}^{-1}$  for  $\text{IC}/\text{CA} = 0.1$  and  $J_{NO_2} = 8 \times 10^{-3}$   
 449  $\text{s}^{-1}$ . This corresponds to  $2.9 \times 10^4$  molecules  $\text{cm}^{-3} \text{s}^{-1}$  once normalized by aerosol surface area  
 450 ( $1.18 \times 10^{-6} \text{cm}^2 \text{cm}^{-3}$ ), and  $J_{NO_2}$  in the aerosol flow tube. Such a primary radical flux is equivalent  
 451 to the OH radical production rate resulting from photolysis of  $\sim 1$  pptv of HONO in the aerosol  
 452 flow tube. Conversely, a  $P_{HO_2}$  of  $1.67 \times 10^{14}$  molecules  $\text{cm}^{-2} \text{min}^{-1}$  is equivalent to the OH radical  
 453 production rate from  $\sim 100$  pptv HONO in the aerosol flow tube. We conclude that seed particles  
 454 containing IC contribute significantly (equivalent to 1-100 pptv HONO) to the primary HO<sub>x</sub> radical  
 455 production rate in the aerosol flow tube experiments in the presence of NO (Fig. 7). Primary HO<sub>2</sub>  
 456 radicals formed from IC containing seed particles react rapidly with NO to form OH radicals under  
 457 the conditions shown in Figure 7. The H-donor species is further expected to form primary RO<sub>2</sub>  
 458 radicals. These primary HO<sub>2</sub> and RO<sub>2</sub> radicals add directly to the conversion of NO into NO<sub>2</sub>, and  
 459 indirectly by driving secondary NO-to-NO<sub>2</sub> conversion from the RO<sub>2</sub>/HO<sub>2</sub> radical chain. The  
 460 aerosol flow tube experiments thus qualitatively confirm the results obtained from macroscopic  
 461 surfaces, and highlight the potentially important role of surface-to-volume ratio and gaseous H-  
 462 donors to enhance the relevance of H-donor photochemistry as sources for HO<sub>x</sub>/RO<sub>x</sub> radicals and  
 463 SOA.

### 464 **3.3. Proposed mechanism**

465 A mechanism that can describe the results from the CWFT experiments is shown in Fig. 8. It  
 466 follows the mechanism first proposed by Canonica et al., in 1995. The primary product in our  
 467 system is the HO<sub>2</sub> radical, which forms from the reaction between a nitrogen-containing aromatic  
 468 alkoxy IC radical and a ground state oxygen molecule, recycling the IC molecule. The aromatic  
 469 alkoxy radicals form from the excited triplet state of IC via transfer of an H atom from an H-donor  
 470 (in our case likely to be CA, or the CA/H<sub>2</sub>O matrix). While a fraction of the IC will get consumed  
 471 by photolysis reactions that do not form the excited triplet state (see Sect 3.1.2.), IC is also  
 472 continuously produced from multiphase reactions, e.g., of glyoxal (Yu et al., 2011; Kampf et al.,  
 473 2012; Maxut et al., 2015). Another conclusion is that OH is a secondary product. If OH was a first



474 generation product we would have expected HONO:NO<sub>2</sub> ratios larger than 1:1. A smaller ratio  
475 was observed, as shown in Fig. 4, indicating that there was no direct evidence for primary  
476 formation of OH radicals. Interestingly, the H-donor species becomes activated as a result of H-  
477 abstraction, and can react further to produce organic peroxy radicals, as evidenced by the aerosol  
478 flow tube results.

479

#### 480 **4. Atmospheric relevance**

481 The atmospheric relevance of our findings consists of the possible effect of heterogeneous radical  
482 sources to modify atmospheric HO<sub>2</sub> radical concentrations, and facilitate aerosol growth and  
483 ageing by adding a radical source within aerosol particles. The production of gas-phase HO<sub>2</sub> from  
484 IC photosensitized heterogeneous chemistry is a possible source of gas-phase HO<sub>2</sub> radicals in  
485 ambient air. In order to estimate the possible relevance for HO<sub>2</sub> radical concentrations in urban air,  
486 we assume P<sub>HO<sub>2</sub></sub> of  $2 \times 10^{12}$  molecules cm<sup>-2</sup> min<sup>-1</sup> (IC/CA = 0.1, Setup 1) as a lower limit, and  $2$   
487  $\times 10^{14}$  molecules cm<sup>-2</sup> min<sup>-1</sup> (IC/AS = 0.1, aerosol flow tube) as an upper limit, and typical  
488 conditions in Mexico City (i.e.,  $J_{NO_2} = 8 \times 10^{-3}$  s<sup>-1</sup> at noontime in Mexico City, aerosol surface  
489 area = 15 cm<sup>2</sup> m<sup>-3</sup>; Volkamer et al., 2007). The normalized P<sub>HO<sub>2</sub></sub> during noon time in Mexico City  
490 ranges from  $2 \times 10^5$  to  $2 \times 10^7$  molecules cm<sup>-3</sup> s<sup>-1</sup>. This corresponds to a rate of new HO<sub>2</sub> radical  
491 production of 4 to 400 pptv HONO around solar noon in Mexico City (Li et al., 2010), where other  
492 radical sources produce about  $5.9 \times 10^7$  molecules cm<sup>-3</sup> s<sup>-1</sup> at solar noon (Volkamer et al., 2010).  
493 The upper range value suggests that aerosol surfaces can be a significant source of gas-phase HO<sub>x</sub>  
494 in places like Mexico City. However, the IC molar ratios used here are likely an upper limit  
495 compared to ambient aerosols, yet, in principle other brown carbon molecules (i.e. HULIS and/or  
496 other imidazole derivatives) may form additional gas-phase HO<sub>2</sub>. The heterogeneous HO<sub>2</sub> radical  
497 source could further be relatively more important in unpolluted regions under biogenic influences,  
498 where gas-phase radical production rates are lower. A more comprehensive characterization of the  
499 heterogeneous HO<sub>2</sub> source effect on gas-phase HO<sub>2</sub> radical concentrations hence deserves further  
500 investigation.

501 OH radical uptake from the gas-phase is a primary OH source in aerosols (Ervens and Volkamer,  
502 2010). Assuming a gas-phase OH concentration of 10<sup>6</sup> molecules cm<sup>-3</sup>, 15 cm<sup>2</sup> m<sup>-3</sup> aerosol surface



area, and  $\gamma_{\text{OH}}$  of unity, the rate of OH uptake is approximately  $2.3 \times 10^5$  molecules  $\text{cm}^{-3} \text{s}^{-1}$ . The above estimated  $P_{\text{HO}_2}$  is a result from H-transfer to form organic peroxy radicals which is comparable to the rate of OH uptake. The two similar estimates of  $\text{HO}_x$  suggest that IC is a significant source of radicals in the condensed phase of particles. This is a lower limit due to the unknown radical losses of  $\text{HO}_x$  to the condensed phase, which hold potential to leverage the  $\text{HO}_x$  source by up to a factor 10,000 if limited by the IC excitation rate. The unknown amount of  $\text{HO}_2$  that remains in the condensed-phase is a further source of OH in the condensed-phase that can start Fenton reactions (if iron is present) or other oxidizing pathways that can further age the aerosol. These results show that IC, and other aromatic carbonyl photosensitizers, are likely a relevant radical source in aerosol particles. Photo-induced radical generation in condensed phases is currently not represented in atmospheric models that describe aerosol ageing, and warrant further study.

515

## 516 5. Conclusion

Three different experimental setups consistently show that  $\text{HO}_2$  radicals are produced from the photochemistry of IC in a  $\text{CA}+\text{H}_2\text{O}$  matrix and in seed aerosols containing ammonium sulfate (in presence of a gas-phase H-donor, limonene). The linear correlations of  $P_{\text{HO}_2}$  (with  $[\text{IC}]/[\text{CA}]$  and irradiation) yielded maximum  $P_{\text{HO}_2}$  under atmospherically relevant irradiation,  $\text{O}_2$  and RH, but also revealed a complex role of film viscosity, and possibly acid effects. If the H-donor species is in the condensed phase, significant amounts of  $\text{HO}_2$  reach the gas-phase only for moderately high RH (~25 – 55% RH) that facilitates H-transfer, and allows molecules (IC,  $\text{HO}_2$ ) to move freely towards the surface of the film. When the film was too dry this mobility is inhibited due to enhance viscosity and significantly decreases the  $P_{\text{HO}_2}$ . At RH and  $\text{O}_2$  higher than 55%, we observe a decrease in  $P_{\text{HO}_2}$  probably due to dilution by water and competing quenching reactions in the film. If the H-donor species is in the gas-phase, significant  $\text{HO}_2$  production is also observed under dry conditions. The primary fate of the  $\text{IC}\cdot\text{-OH}$  radical at the surface is reaction with  $\text{O}_2$  to form  $\text{HO}_2$ .  $\text{NO}_2$  reactions do not appear to form HONO at the surface. Our results suggest that the radical source from photosensitizers such as IC can help jump-start photochemistry of VOCs. The effect on the gas-phase  $\text{HO}_2$  radical concentration increases for higher surface to volume ratio of aerosols, and in the presence of gas-phase H-donors. The autophotocatalytic growth of aerosols containing



533 photosensitizers via H-donor chemistry is a SOA source also in the presence of NO, and adds  
534 oxidative capacity inside aerosol particles. Further research on other types of H-donors and  
535 photosensitizers is necessary to compare different  $P_{\text{HO}_2}$  and rates of aerosol growth from reactive  
536 uptake of VOC that could potentially have a significant atmospheric relevance for SOA formation  
537 and heterogeneous aerosol ageing.

#### 538 **Author contributions**

539 M.A. and R.V. designed the experiments at PSI; C.G. and B.N. those at IRCELYON. L.G.P.,  
540 P.C.A., and K.Z.A. conducted the measurements, analyzed data, and contributed equally to this  
541 work. S.S.S., T.B.R. helped during the experiments, and all co-authors contributed to the data  
542 interpretation. L.G.P. and R.V. prepared the manuscript with contributions from all co-authors.

543

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## Figures

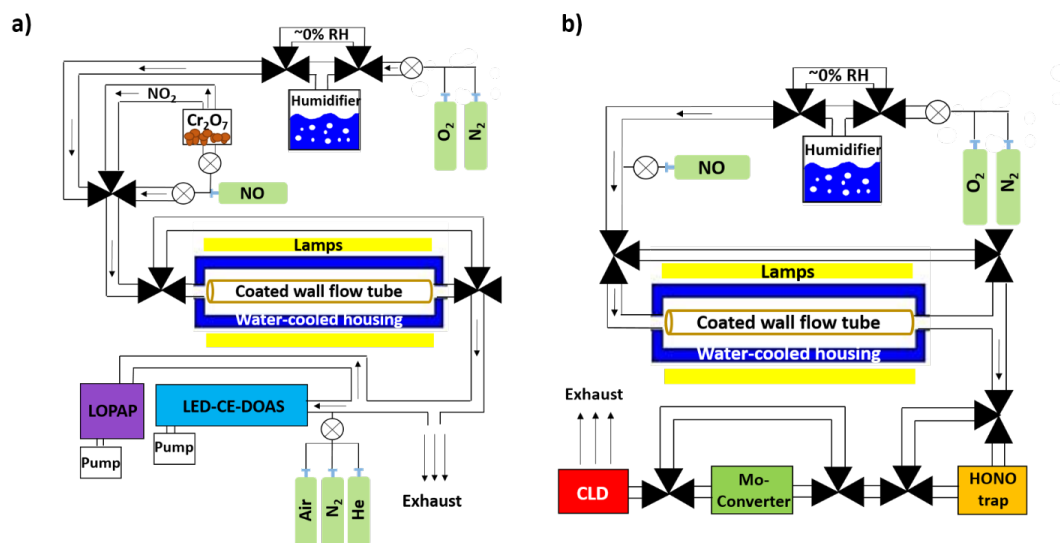
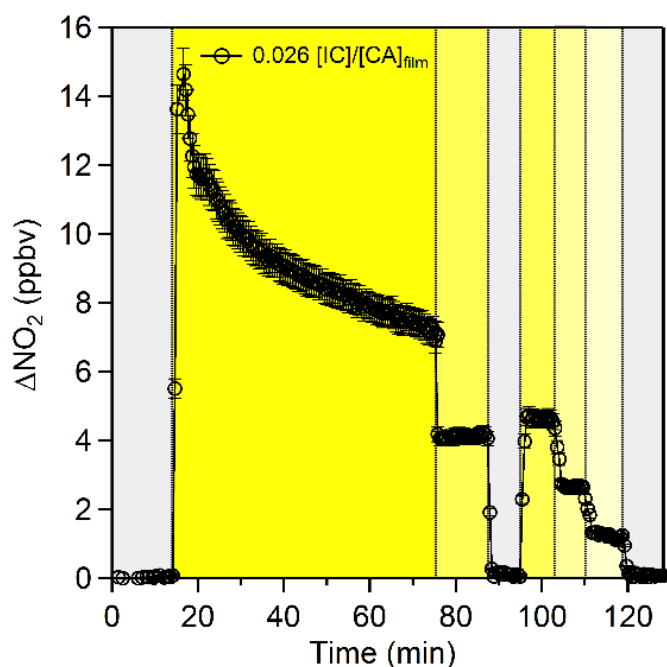


Figure 1. Sketch of the photochemical flow tube reactor setups at PSI for a) Setup 1 in 2013 measuring NO<sub>2</sub> generation and b) for Setup 2 in 2014 measuring NO loss.



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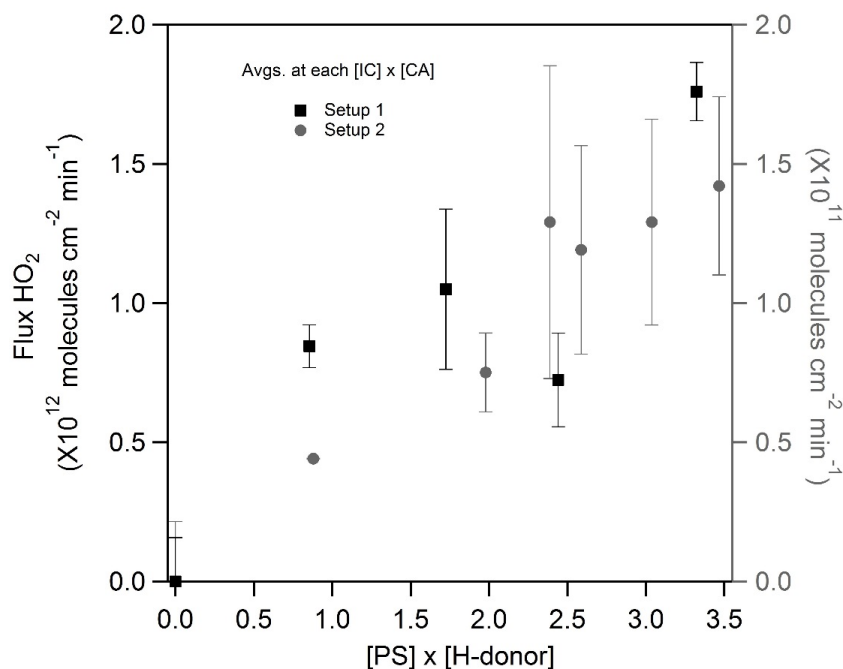
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722 Figure 2. NO<sub>2</sub> profile for a 0.025M IC bulk solution, whose concentration increases to ~0.2 M of  
 723 IC in the film due to the citric acid hygroscopic properties. The gray shaded areas indicate  
 724 periods where NO was exposed in the dark. The yellow shaded areas indicates the period of  
 725 irradiation; the decrease in the intensity of yellow represents the decrease in irradiance ( $2.26 \times$   
 726  $10^{16}$ ,  $1.47 \times 10^{16}$ ,  $1.14 \times 10^{16}$ , and  $3.94 \times 10^{15}$  photons  $\text{cm}^{-2} \text{s}^{-1}$ , for seven, five, three and one  
 727 lamp, respectively). This timeseries clearly indicates the light dependence production of HO<sub>2</sub>  
 728 radicals from the photosensitization of IC in a CA film.

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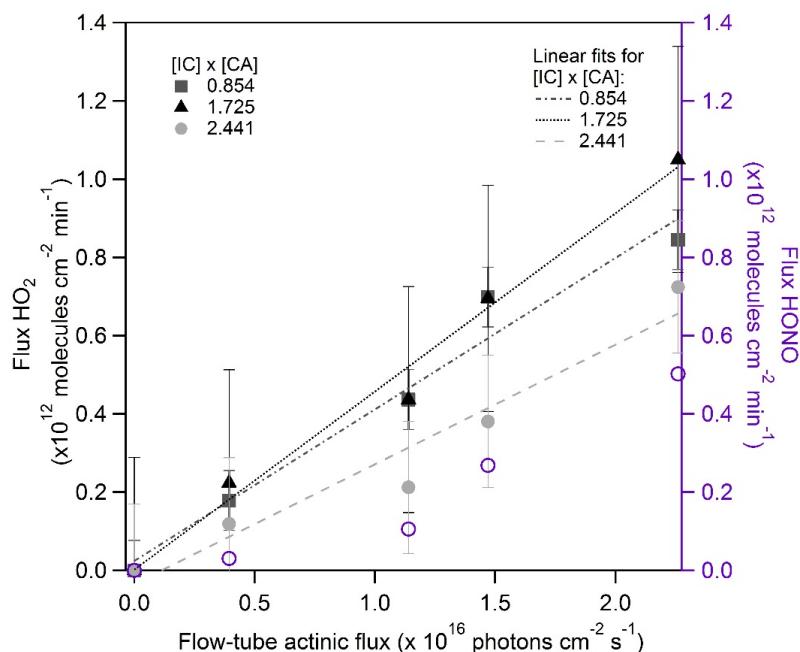
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732 Figure 3. A linear correlation of HO<sub>2</sub> as a function of IC concentration. The left y-axis  
 733 represents the values for Setup 1, while the right y-axis represents the values for Setup 2, (an  
 734 order of magnitude difference for both scales). The Setup 2 data falls between a factor of 2 and 3  
 735 from Setup 1 after accounting for differences between Setup 1 and 2, see Sect. 3.1.1.

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739 Figure 4.  $\text{HO}_2$  fluxes (molecules  $\text{cm}^{-2} \text{min}^{-1}$ ) as a function of actinic flux for a 300-420 nm range.

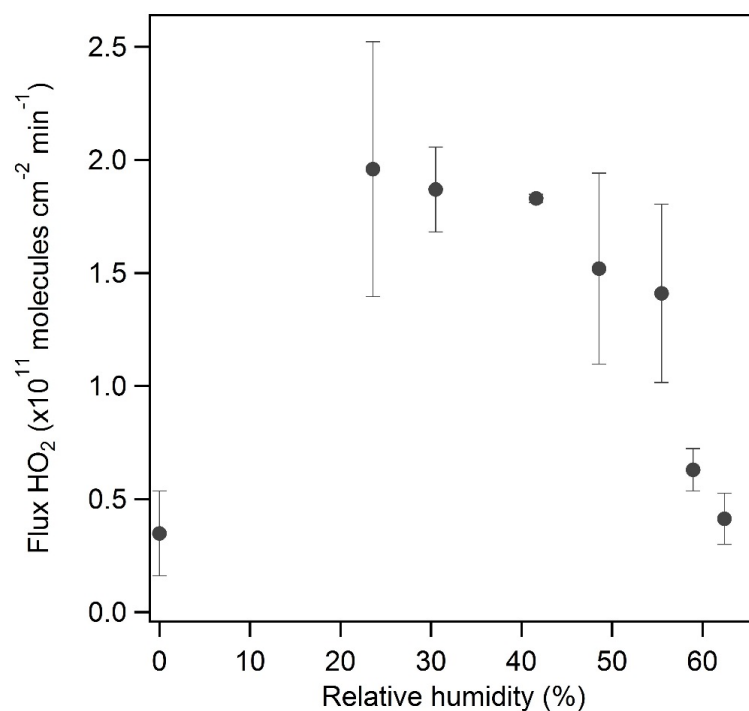
740 The data is plotted as a concentration product of  $[\text{IC}] \times [\text{CA}]$  (shown in the legend) which shows

741 the photochemical reaction between IC and CA in  $\text{H}_2\text{O}$  matrix and gaseous NO. HONO for

742 2.441 ( $[\text{IC}] \times [\text{CA}]$ ) is plotted on the right axis, showing a ratio of  $\text{HONO}:\text{NO}_2 < 1$ , which

743 suggests OH as a secondary product.

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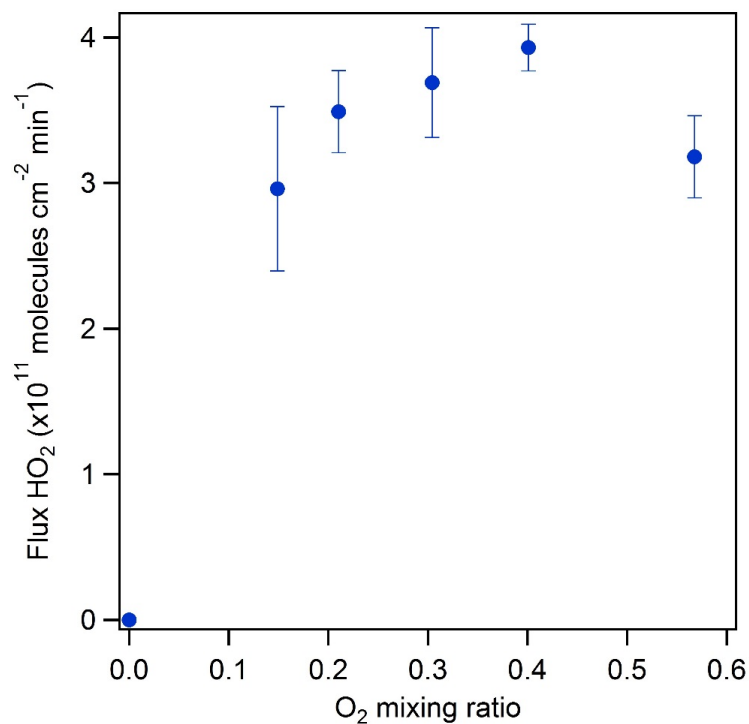
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747 Figure 5. The NO loss normalized to the film surface area as a function of relative humidity.

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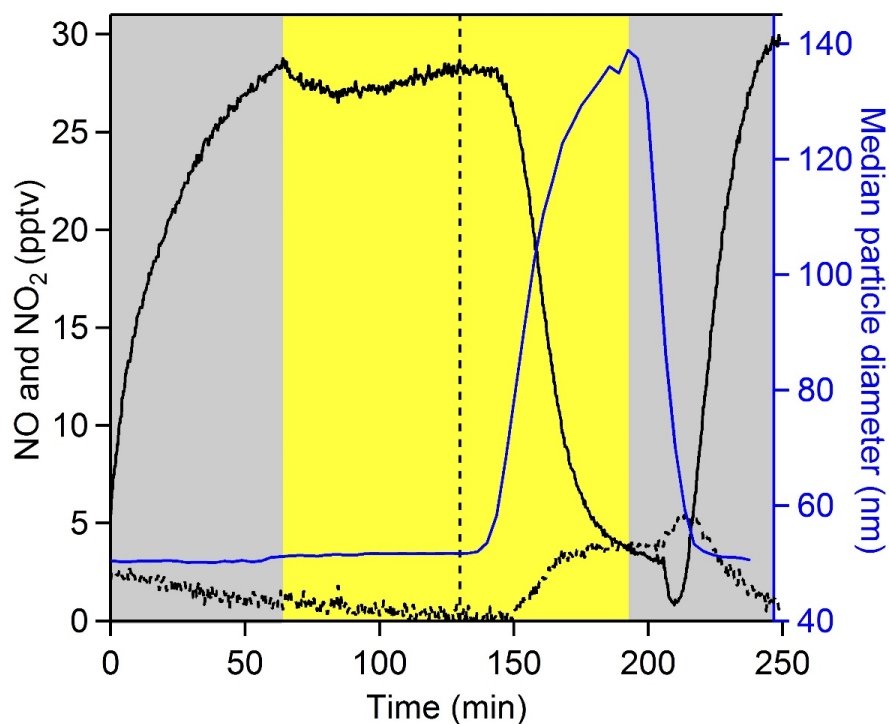
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751 Figure 6. Measured loss of NO above a film composed of IC and CA normalized of the film  
 752 surface area as a function of the O<sub>2</sub> mixing ratio.

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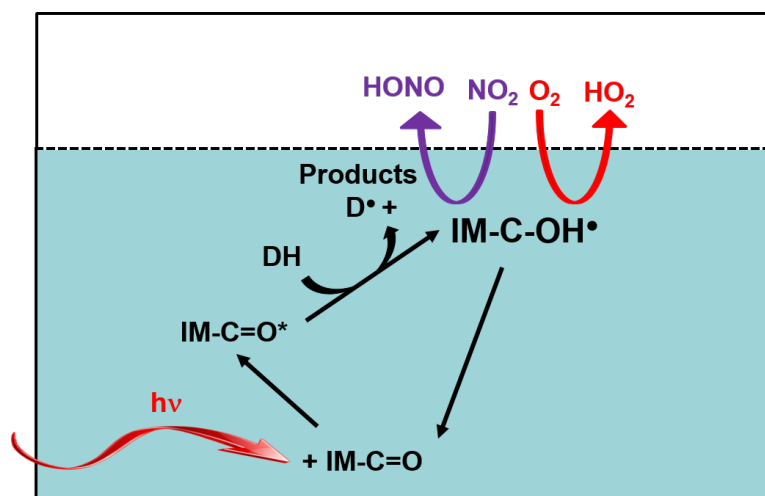
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756 Figure 7. Aerosol flow tube experiments show rapid conversion of NO (solid black line) into  
 757 NO<sub>2</sub> (dashed black line) only after the time when limonene (gaseous H-donor) is added into the  
 758 flowtube (vertical dashed line). The gray shaded areas represent experiment in the dark, and the  
 759 yellow shaded area represents the experiment under light exposure. The blue line represents the  
 760 growth of aerosols, right axis.

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763

764 Figure 8. Proposed mechanism, modified and expanded to photosensitization of IC based on  
 765 Canonica et al. (1995), George et al. (2005) and Aregahegn et al. (2013). The reaction in the  
 766 white square represents the gas-phase, and the blue square represents the aqueous phase. DH is  
 767 an H-donor (e.g. CA, another IC, H<sub>2</sub>O+CA matrix to be determined from flash photolysis).

768