

1 **Relative humidity-dependent viscosity of secondary organic**  
2 **material from toluene photo-oxidation and possible**  
3 **implications for organic particulate matter over megacities**

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5 M. Song<sup>1,2</sup>, P. F. Liu<sup>3</sup>, S. J. Hanna<sup>1</sup>, R. A. Zaveri<sup>4</sup>, K. Potter<sup>5</sup>, Y. You<sup>1</sup>, S. T. Martin<sup>3,6</sup>, A.  
6 K. Bertram<sup>1</sup>

7 [1] {Department of Chemistry, University of British Columbia, Vancouver, BC, V6T 1Z1, Canada}

8 [2] {Department of Earth and Environmental Sciences, Chonbuk National University, Jeollabuk-  
9 do, Republic of Korea}

10 [3]{John A. Paulson School of Engineering and Applied Sciences, Harvard University, Cambridge,  
11 Massachusetts 02138, USA}

12 [4]{Atmospheric Sciences and Global Change Division, Pacific Northwest National Laboratory,  
13 Richland, WA, USA}

14 [5]{School of Chemistry, University of Bristol, Bristol, UK BS8 1TS, UK}

15 [6]{Department of Earth and Planetary Sciences, Harvard University, Cambridge, Massachusetts  
16 02138, USA}

17 Correspondence to: A. K. Bertram (bertram@chem.ubc.ca)

18

19 **Abstract**

20 To improve predictions of air quality, visibility, and climate change, knowledge of the viscosities  
21 and diffusion rates within organic particulate matter consisting of secondary organic material  
22 (SOM) is required. Most qualitative and quantitative measurements of viscosity and diffusion rates  
23 within organic particulate matter have focused on SOM particles generated from biogenic VOCs  
24 such as  $\alpha$ -pinene and isoprene. In this study, we quantify the relative humidity (RH)-dependent  
25 viscosities at  $295 \pm 1$  K of SOM produced by photo-oxidation of toluene, an anthropogenic VOC.

1 The viscosities of toluene-derived SOM were  $2 \times 10^{-1}$  to  $\sim 6 \times 10^6$  Pa·s from 30 to 90% RH, and  
2 greater than  $\sim 2 \times 10^8$  Pa·s (similar to or greater than the viscosity of tar pitch) for  $\text{RH} \leq 17\%$ . These  
3 viscosities correspond to Stokes-Einstein-equivalent diffusion coefficients for large organic  
4 molecules of  $\sim 2 \times 10^{-15}$   $\text{cm}^2 \cdot \text{s}^{-1}$  for 30% RH, and lower than  $\sim 3 \times 10^{-17}$   $\text{cm}^2 \cdot \text{s}^{-1}$  for  $\text{RH} \leq 17\%$ .  
5 Based on these estimated diffusion coefficients, the mixing time of large organic molecules within  
6 200 nm toluene-derived SOM particles is 0.1 - 5 hr for 30% RH, and higher than  $\sim 100$  hr for  $\text{RH}$   
7  $\leq 17\%$ . As a starting point for understanding the mixing times of large organic molecules in organic  
8 particulate matter over cities, we applied the mixing times determined for toluene-derived SOM  
9 particles to the world's top 15 most populous megacities. If the organic particulate matter in these  
10 megacities is similar to the toluene-derived SOM in this study, in Istanbul, Tokyo, Shanghai, and  
11 Sao Paulo, mixing times in organic particulate matter during certain periods of the year may be  
12 very short, and the particles may be well-mixed. On the other hand, the mixing times of large  
13 organic molecules in organic particulate matter in Beijing, Mexico City, Cairo, and Karachi may  
14 be long and the particles may not be well-mixed in the afternoon (3:00 – 5:00 local time) during  
15 certain times of the year.

16

## 17 **1 Introduction**

18 Volatile organic compounds (VOCs) are released into the atmosphere from both biogenic and  
19 anthropogenic sources. In the atmosphere, VOCs can form secondary organic material (SOM)  
20 through oxidation reactions with OH radicals,  $\text{NO}_3$  radicals, and  $\text{O}_3$ . SOM accounts for 20 – 80%  
21 of the mass of organic atmospheric particulate matter at various locations (Zhang et al., 2007;  
22 Jimenez et al., 2009). SOM typically consists of thousands of different compounds, and only 10 –  
23 20% of the individual molecules that make up SOM particles have been identified (Decesari et al.,  
24 2006; Hallquist et al., 2009). The lack of information on the chemical composition of SOM has  
25 resulted in a poor understanding of their physical properties, including the viscosity and molecular  
26 diffusion rates within SOM particles.

27 Knowledge of the viscosity and molecular diffusion rates within SOM particles is needed to predict  
28 the properties of these particles and understand their role in the atmosphere. For example, the size  
29 distribution and mode diameter depend on the diffusion rates of organic molecules within the

1 particles (Shiraiwa et al., 2013; Zaveri et al., 2014). Simulations show that total SOM mass  
2 concentrations can be overestimated or underestimated depending on what diffusion rates are used  
3 (Shiraiwa and Seinfeld, 2012). Chemical aging of atmospheric particles by heterogeneous  
4 reactions can depend on diffusion rates within SOM (Shiraiwa et al., 2011; Kuwata and Martin,  
5 2012; Zhou et al., 2013; Steimer et al., 2014; Houle et al., 2015) and heterogeneous ice nucleation  
6 may be influenced by the viscosity of SOM particles (Murray et al., 2010; Wang et al., 2012;  
7 Ladino et al., 2014; Schill et al., 2014; Wilson et al., 2012). Moreover, long-range transport of  
8 polycyclic aromatic hydrocarbons can depend on diffusion rates in a particle (Zelenyuk et al., 2012;  
9 Zhou et al., 2013) and the efflorescence of crystalline salts can be hindered for highly viscous  
10 SOM (Murray, 2008; Murray and Bertram, 2008; Bodsworth et al., 2010; Song et al., 2013).

11 Most qualitative and quantitative measurements of viscosity and diffusion rates within organic  
12 particulate matter have focused on SOM generated from biogenic VOCs such as  $\alpha$ -pinene and  
13 isoprene (Virtanen et al., 2010; Cappa et al., 2011; Perraud et al., 2012; Saukko et al., 2012;  
14 Abramson et al., 2013; Robinson et al., 2013; Renbaum-Wolff et al., 2013a; Bateman et al., 2015;  
15 Kidd et al., 2014; Pajunoja et al., 2014; Wang et al., 2014; Grayson et al., 2015b, Song et al., 2015).  
16 Recently, the viscosity and diffusion rates within SOM particles generated from anthropogenic  
17 VOCs have also been investigated. Using mass spectrometry, Loza et al. (2013) and Robinson et  
18 al. (2013) investigated mixing of toluene-derived SOM particles and SOM particles from  $\alpha$ -pinene  
19 ozonolysis. Results from both studies were consistent with toluene-derived SOM being in a highly  
20 viscous state. From bounce experiments, Saukko et al. (2012) reported that SOM particles derived  
21 from naphthalene and n-heptadecane are highly viscous upon increasing oxidation. Also from  
22 bounce experiments, Bateman et al. (2015) showed SOM derived from photo-oxidation of toluene  
23 had a viscosity  $> 100$  Pa·s for relative humidity (RH) values  $< 80\%$ . Li et al. (2015) showed  
24 through bounce experiments that SOM derived from *m*-xylene and 1,3,5-trimethylbenzene had a  
25 viscosity of  $> 100$  Pa·s at RH values less than 70%. Li et al. (2015) also used results of reactive  
26 uptake studies to infer that for RH values of 35 - 45% the diffusion coefficient of carboxylic acids  
27 within SOM generated from several anthropogenic VOCs (toluene, *m*-xylene and 1,3,5-  
28 trimethylbenzene) was  $\sim 10^{-13.5 \pm 0.5} \text{ cm}^2 \text{ s}^{-1}$ . Although there has been recent progress in measuring  
29 the viscosity and diffusion rates within SOM generated from anthropogenic VOCs, additional  
30 studies are needed to quantify the viscosities and diffusion rates over the full range of RH found  
31 in the atmosphere.

1 In the following, we measure the viscosities of toluene-derived SOM over the range of RH values  
2 found in the atmosphere. As in previous studies, SOM from the photo-oxidation of toluene serves  
3 as a proxy for organic particulate matter from anthropogenic sources in megacities (e.g. Pandis et  
4 al., 1992; Robinson et al., 2013). After determining viscosities as a function of RH, the Stokes-  
5 Einstein equation is used to convert the viscosities into equivalent diffusion rates of large organic  
6 molecules within toluene-derive SOM. The Stokes-Einstein equation should give reasonable  
7 values of diffusion rates when the viscosity is not near the viscosity of a glass ( $\sim 10^{12}$  Pa s) and  
8 when the molecules are roughly the same size or larger than the molecules in the SOM matrix  
9 (Champion et al., 2000; Koop et al., 2011; Shiraiwa et al., 2011; Power et al., 2013). Finally, the  
10 results are used to estimate the viscosities and diffusion rates in organic particulate matter over  
11 megacities.

12

## 13 **2 Experimental**

14 The production and collection of SOM particles onto hydrophobic substrates (which are needed  
15 for the beam mobility and poke-and-flow experiments) is discussed in Sect. 2.1. The viscosity of  
16 toluene-derived SOM was determined using the bead-mobility technique and the poke-flow  
17 technique together with simulations of fluid flow. These two techniques are discussed in Sects. 2.2  
18 and 2.3.

### 19 **2.1 Production and collection of secondary organic material on hydrophobic** 20 **substrates**

21 SOM aerosol particles having diameters less than 1  $\mu\text{m}$  were generated by toluene photo-oxidation  
22 in an oxidation flow reactor (OFR) (Kang et al., 2007; Lambe et al., 2011). The procedure for  
23 generating SOM from toluene photo-oxidation in the flow reactor has been given by Liu et al.  
24 (2015). Only the details relevant to the current experiments are given here.

25 For this study, the volume of the OFR was 13.3 L and the reactor was operated at a flow rate of  
26  $\sim 7 \text{ L m}^{-1}$  with a residence time in the range of  $\sim 110$  s. The temperature used in the OFR  
27 experiments was  $293 \pm 2$  K and the concentrations of toluene and ozone used in the flow reactor  
28 are listed in Table 1. Ozone was produced external to the flow reactor by irradiating pure air with

1 the ultraviolet emission from an Hg lamp ( $\lambda = 185$  nm). The injected ozone concentration was  $\sim 30$   
2 ppm. Hydroxyl radicals were produced inside the OFR by the following photochemical reactions:



5 The RH inside the reactor was held constant at  $13 \pm 3$  %. A recent study has shown that the  
6 viscosity of  $\alpha$ -pinene-derived SOM is dependent on the RH at which the SOM is generated (Kidd  
7 et al., 2014). Additional studies are needed to explore this potential RH effect on the viscosity of  
8 toluene-derived SOM.

9 Mass concentrations of SOM particles in the OFR were  $60\text{-}100 \mu\text{g m}^{-3}$  and  $600\text{-}1000 \mu\text{g m}^{-3}$  for  
10 the two different experimental conditions (see Table 1). For the mass concentration of  $60\text{-}100 \mu\text{g}$   
11  $\text{m}^{-3}$ , the oxygen-to-carbon (O:C) ratio was 1.08, calculated from the AMS mass spectra following  
12 the approach of Chen et al. (2011). This value can be compared with the O:C values ranged from  
13 0.9 to 1.3 measured for toluene-derived SOM generated in a similar OFR (Lambe et al., 2015). At  
14 the outlet of the OFR, two different methods were used for the collection of SOM particles. In the  
15 first method, SOM particles were collected on a hydrophobic slide using an electrostatic  
16 precipitator (TSI 3089, USA). After collection, the SOM particles on the hydrophobic slides,  
17 formed from coalescence during sampling, were smaller than  $\sim 5 \mu\text{m}$  in diameter. For the bead-  
18 mobility and poke-flow techniques, however, particle sizes between  $20 - 60 \mu\text{m}$  in diameter are  
19 needed. To generate these large sizes, the hydrophobic slides containing the SOM particles were  
20 placed inside an RH- and temperature-controlled flow cell (Pant et al., 2006; Bertram et al., 2011;  
21 Song et al., 2012) and the RH was increased to  $> 100\%$ . This procedure caused particle growth by  
22 water uptake and eventual coagulation among particles. This growth and coagulation process  
23 resulted in larger but fewer SOM particles on the hydrophobic slides. Details of this procedure are  
24 given by Renbaum-Wolff et al. (2015) and Song et al. (2015). This procedure was used for samples  
25 1, 2, 5, and 6 shown in Table 1.

26 In the second method, SOM particles were collected on hydrophobic surfaces using a single stage  
27 impactor (Prenni et al., 2009; Poschl et al., 2010). During impaction, the collected submicron SOM  
28 particles coagulated, resulting in particles with sizes between  $10$  and  $100 \mu\text{m}$  in diameter. These  
29 supermicron particles were used directly in the bead-mobility and poke-flow experiments. This  
30 procedure was used to collect samples 3, 4, 7, and 8 shown in Table 1.

1 For all the bead-mobility experiments, a Teflon substrate was used. For all the poke-and-flow  
2 experiments, hydrophobic glass slides coated with trichloro(1*H*,1*H*,2*H*,2*H*-perfluorooctyl)silane  
3 (Sigma-Aldrich) were used. The coating procedure is described in Knopf (2003).

## 4 **2.2 Bead-mobility experiments**

5 The bead-mobility technique was previously described in Renbaum-Wolff et al. (2013a, b). Briefly,  
6 a water suspension of  $\sim 1 \mu\text{m}$  insoluble melamine beads (Sigma Aldrich Cat. #86296) was  
7 nebulized and incorporated into supermicron SOM particles deposited on a hydrophobic substrate  
8 (toluene samples 1-4, Table 1). The hydrophobic substrate with the SOM particles and beads was  
9 placed in a flow-cell with variable RH and a temperature of  $295 \pm 1 \text{ K}$ . A continuous flow of  
10  $\text{N}_2/\text{H}_2\text{O}$  gas (flow rate  $\approx 1200 \text{ sccm}$ ) was passed over the supermicron particles. The flow above  
11 the particles resulted in a shear stress on the particle surface and internal circulations within the  
12 particle, which could be visualized by observing the beads within the particles with a light-  
13 transmitting microscope coupled to a CCD camera (Zeiss Axio Observer, magnification  $40\times$ ).  
14 Figure 1 shows images from a typical bead-mobility experiment for a toluene-derived SOM  
15 particle at 80% RH. Typically, 1 to 7 beads were monitored within a particle over 50 - 100 frames.  
16 The time between frames ranged from 0.2 s – 10 min depending on the velocity of the beads. From  
17 the location of the beads as a function of time, the speed of individual beads was determined. These  
18 individual speeds were then used to determine average bead speeds for a given sample and RH.  
19 The measured speeds of 3 - 10 beads were used to determine a mean bead speed. Bead speeds were  
20 not reported at  $\text{RH} < 60\%$  since at these RH values the movements of the beads were too slow to  
21 measure for typical observation times.

22 The average bead speed for a given sample and RH was converted to viscosity using a calibration  
23 line. The calibration line was developed by Song et al. (2015) from measurements of bead speed  
24 in sucrose-water particles over a range of RH values. The RH within the flow-cell was measured  
25 using a hygrometer with a chilled mirror sensor (General Eastern, Canada), which was calibrated  
26 by measuring the deliquescence RH for pure ammonium sulfate particles (80.0% RH at 293 K,  
27 Martin (2000)). The uncertainty of the hygrometer was  $\pm 0.5\%$  RH after calibration.

## 28 **2.3 Poke-flow technique in conjunction with fluid simulations**

1 The poke-and-flow technique in conjunction with fluid simulations was used to measure the  
2 viscosities of SOM particles at RH values less than 50%. This technique was not used at RH values  
3 > 50% since the flow rates of the SOM after poking were too fast to observe at these RH values.  
4 The qualitative method of poking an inorganic particle to determine its phase (i.e., solid or liquid)  
5 was introduced by Murray et al. (2012). Renbaum-Wolff et al. (2013a) and Grayson et al. (2015a)  
6 expanded on this method by measuring the characteristic flow time of a material after poking and  
7 extracting viscosity information from simulations of fluid flow. Briefly, supermicron toluene-  
8 derived SOM particles deposited on a hydrophobic substrate (Toluene 5 to 8, Table 1) were placed  
9 inside a flow-cell with RH control. The particles were conditioned for 30 min at > 70% RH, 60  
10 min at 60 – 70% RH, 2 h at 30 – 60% RH, and 3 h at  $\leq$  30% RH. These times should be sufficient  
11 for the particles to equilibrate with the surrounding water vapor based on recent measurements of  
12 diffusion coefficients of water within the water-soluble component of  $\alpha$ -pinene-derived SOM  
13 (Price et al., 2015). For example, the time to equilibrate with the surrounding of water vapor was  
14 calculated to be 25.3 min at 10 % RH based on diffusion coefficients of water within the water-  
15 soluble component of  $\alpha$ -pinene-derived SOM (Price et al., 2015). These diffusion coefficients  
16 should be applicable to SOM derived from toluene studied here, since both SOMs have similar  
17 viscosities as a function of RH (compare Fig. 2 in Renbaum-Wolff et al. (2013a) with Fig. 5 below).  
18 After equilibration, particles were poked using a sharp needle (0.9 mm  $\times$  40 mm) (Becton-Dickson,  
19 USA) that was mounted to a micromanipulator (Narishige, model MO-202U, Japan) and inserted  
20 through a small hole in the top of the flow-cell. The geometrical changes before, during, and after  
21 poking a particle were recorded by a reflectance optical microscope (Zeiss Axio Observer, 40 $\times$   
22 objective) equipped with a CCD camera. At 30 - 50% RH the action of poking the particles with  
23 the needle resulted in the material forming a half torus geometry (see Fig. 2a). From the images  
24 recorded after poking the particles, the experimental flow time,  $\tau_{\text{exp, flow}}$ , was determined. The  
25 experimental flow time was defined as the time taken for the equivalent-area diameter of the inside  
26 of the half torus geometry to reduce to 50% of the initial diameter. Here the equivalent-area  
27 diameter,  $d$ , is calculated as  $d = (4A/\pi)^{1/2}$  where  $A$  represents the hole area (Reist, 1992). For RH  
28 < 20% the SOM particles shattered after poking, and no restorative flow was observed over ~5 hr  
29 (See Fig. 2b). In this case  $\tau_{\text{exp, flow}}$  was set to > 5 hr.  
30 To determine viscosities from  $\tau_{\text{exp, flow}}$ , simulations of fluid flow were carried out with the finite-  
31 element analysis software package, *COMSOL Multiphysics* (Renbaum-Wolff et al., 2013a;

1 Grayson et al., 2015a). The mesh size used in the simulations was 4.04 – 90.9 nm. The physical  
2 parameters (i.e., slip length, surface tension, contact angle, and density) used in the simulation are  
3 listed in Table 2.

4 For each particle for which flow was observed, simulations were run using a half torus geometry,  
5 similar to the geometry observed in the experiments where flow was observed. The radius of the  
6 tube,  $R$ , in the half torus geometry and the radius of the hole,  $r$ , in the half torus geometry used in  
7 the simulations were based on the images recorded immediately after poking the particles with the  
8 needle. To determine viscosity for each particle, viscosity in the simulations was adjusted until  
9  $\tau_{\text{model, flow}}$  was within 1% of  $\tau_{\text{exp, flow}}$ .

10 In cases for which the particles cracked, simulations were run using a quarter-sphere model with  
11 one of the flat faces of the quarter sphere in contact with the substrate, similar to what was observed  
12 in the experiments (Renbaum-Wolff et al., 2013a). The diameter used for the quarter sphere was  
13 20  $\mu\text{m}$ . In this case we determined a lower limit to the viscosity by adjusting the viscosity in the  
14 simulation until the sharp edge of the quarter sphere model moved by 0.5  $\mu\text{m}$  within 5 hr. A value  
15 of 0.5  $\mu\text{m}$  was used since this amount of movement could be observed in the optical microscope  
16 experiments.

17

### 18 **3 Results**

19 Shown in Fig. 3 are the mean bead speeds of individual SOM samples (toluene 1, 2, 3, and 4)  
20 measured at different RH values between 60 and 90% RH (see Sect. 2.1). As the RH decreased  
21 from 89.9 to 60.7%, the average bead speed decreased by a factor of 22 from  $9.20 \times 10^{-4}$  to  $4.24 \times$   
22  $10^{-7} \mu\text{m} \cdot \text{ms}^{-1}$ . Sample-to-sample variation was less than the uncertainty in the measurements and,  
23 within uncertainty, the results for 60 - 100  $\mu\text{g} \cdot \text{m}^{-3}$  concentration agreed with the results for 600 -  
24 1000  $\mu\text{g} \cdot \text{m}^{-3}$  concentration.

25 Figure 4 shows the result of  $\tau_{\text{exp, flow}}$  as a function of RH for the different samples (toluene 5, 6, 7,  
26 and 8). The  $\tau_{\text{exp, flow}}$  increased from  $\sim 1$  s to  $\sim 2000$  s as RH decreased from 50 to 30% RH. The  $\tau_{\text{exp,}}$   
27  $\tau_{\text{flow}}$  variation from sample to sample was less than the variation within individual toluene samples  
28 with mass concentrations over the range studied (600-1000 and 60-100  $\mu\text{g} \cdot \text{m}^{-3}$ ), as shown in Fig.  
29 4.



1 Shown in Fig. 5 are the viscosities as a function of RH for toluene-derived SOM particles  
2 determined from the bead-mobility experiments (Sect. 2.2) and the poke-flow experiments in  
3 conjunction with the fluid simulation (Sect. 2.3). For the bead-mobility experiments, the viscosities  
4 were determined by the mean of bead speeds between 60 and 90% RH. The y-error bars indicate  
5 the 95% prediction intervals from the calibration line (Song et al., 2015). The x-error bars represent  
6 the uncertainty in the RH measurements. The viscosity of the SOM increases from  $\sim 0.2$  to  $\sim 129$   
7 Pa·s as RH decreases from 89.9 to 60.7%. As shown in Fig. 5, difference between the results for  
8 the 600-1000 and 60-100  $\mu\text{g}\cdot\text{m}^{-3}$  samples are less than the uncertainties in the measurements.

9 Also shown in Fig. 5 are the calculated viscosities of the toluene-derived SOM for RH < 50 %  
10 from the poke-flow experiments. The viscosity increases from approximately  $7.8 \times 10^3$  to  $6.3 \times$   
11  $10^6$  Pa·s as RH decreases from 47.3 to 30.5%. The uncertainty in the viscosity of approximately  
12 two orders of magnitude arises from the uncertainties in the physical parameters used in the  
13 simulations (i.e. slip length, surface tension, density and contact angle). Of these parameters, the  
14 slip length contributed the most to the uncertainty in the viscosity (Grayson et al., 2015a). For RH  
15 < 20 %, restorative flow did not occur over  $\sim 5$  hrs resulting in a lower limit to the viscosity of  $\sim 2$   
16  $\times 10^8$  Pa·s, similar to or greater than the viscosity of tar pitch ( $\sim 10^8$  Pa·s, Koop et al., 2011).

17

## 18 **4 Discussion**

19 Bateman et al. (2015) previously estimated the viscosity of toluene-derived SOM from particle  
20 rebound experiments. From their measurements they estimated a viscosity of 100 to 1 Pa·s for  
21 RHs between 60 and 80% with SOM mass concentrations of 30 - 50  $\mu\text{g}\cdot\text{m}^{-3}$  (green box in Fig. 5)  
22 in good agreement with our measurements.

23 Li et al. (2015) previously estimated the diffusion coefficient of carboxylic acids within toluene-  
24 derived SOM from measurements of reactive uptake of  $\text{NH}_3$ . They estimated a diffusion  
25 coefficient for carboxylic acids of  $10^{-13.5 \pm 0.5} \text{cm}^2\cdot\text{s}^{-1}$  for RHs between 35 and 45% using SOM mass  
26 concentrations of 44 to 125  $\mu\text{g}\cdot\text{m}^{-3}$ . If a hydrodynamic radius of 0.1 - 1.5 nm is assumed for the  
27 carboxylic acids (Li et al., 2015), viscosity of  $1 \times 10^4 - 2 \times 10^6$  Pa·s is calculated using the Stokes-  
28 Einstein equation (blue box in Fig. 5), consistent with our measurements. The good agreement  
29 between the current results and the results from Bateman et al. and Li et al. suggests that the

1 viscosity of the toluene-derived SOM is relatively insensitive to the particle mass concentrations  
2 at which the SOM is produced over the range of 30 to 1000  $\mu\text{g}\cdot\text{m}^{-3}$ .

3 The strong dependence of viscosity on RH shown in Fig. 5 can be understood by considering the  
4 hygroscopic nature of the SOM. To illustrate this point in Fig. 5 viscosity is also plotted versus  
5  $V_{\text{wet}}/V_{\text{dry}}$  of the SOM (secondary  $x$ -axis), where  $V_{\text{dry}}$  is the volume of SOM at 0% RH and  $V_{\text{wet}}$  is  
6 the volume of the SOM after taking up water at a given RH.  $V_{\text{wet}}/V_{\text{dry}}$  was calculated with the  
7 following equation (Petters and Kreidenweis, 2008; Pajunoja et al., 2015):

$$8 \quad V_{\text{wet}}/V_{\text{dry}} = \frac{\kappa}{\frac{100}{\text{RH}} - 1} + 1 \quad (\text{Eq. 1})$$

9 where  $\kappa$  is the hygroscopic parameter. A hygroscopic parameter of 0.15 was assumed, consistent  
10 with previous measurements for toluene-derived SOM (Ruiz et al., 2015). Equation (1) neglects  
11 the Kelvin effect, which is a reasonable assumption for the large particles used in our studies. Fig.  
12 5 illustrates that the water content (top  $x$ -axis) of the particles plays a key role in regulating the  
13 viscosity.

14 A liquid is defined as a material with a viscosity less than  $10^2$  Pa·s; a semisolid is defined as a  
15 material with a viscosity between  $10^2$  Pa·s and  $10^{12}$  Pa·s; and a solid is defined as a material with  
16 a viscosity greater than  $10^{12}$  Pa·s (Koop et al., 2011; Shiraiwa et al., 2011). As shown in Fig. 5,  
17 the viscosities of the SOM produced from toluene photo-oxidation correspond to liquid for  $\text{RH} >$   
18  $60\%$ , a semisolid for  $60\% < \text{RH} < 30\%$ , and a semisolid or a solid for  $\text{RH} < 20\%$ . Our results  
19 suggest a semisolid-to-liquid phase transition at an RH between 60 and 70%, in good agreement  
20 with Bateman et al. (2015) who suggested a semisolid-to-liquid phase transition of toluene-derived  
21 SOM particles in the range of 60 - 80% RH.

22 From the viscosities determined at  $295 \pm 1$  K and the Stokes-Einstein relationship (assuming a  
23 hydrodynamic radius of 0.4 nm for organic molecules within the toluene-derived SOM, Renbaum-  
24 Wolff et al., 2013a), we calculated the diffusion coefficients of large organic molecules,  $D_{\text{org}}$ ,  
25 within toluene-derived SOM (see secondary  $y$ -axis in Fig. 5).  $D_{\text{org}}$  ranges from  $\sim 3 \times 10^{-8}$  to  $\sim 2 \times$   
26  $10^{-15}$   $\text{cm}^2\cdot\text{s}^{-1}$  for RH from 90 to 30%. It is lower than  $\sim 3 \times 10^{-17}$   $\text{cm}^2\cdot\text{s}^{-1}$  for  $\text{RH} \leq 17\%$ . The Stokes-  
27 Einstein relation is not expected to predict with high accuracy the diffusion rates of small gas  
28 molecules such as OH, O<sub>3</sub>, NO<sub>x</sub>, NH<sub>3</sub>, and H<sub>2</sub>O and may be inaccurate near the glass transition

1 RH (Koop et al., 2011; Shiraiwa et al., 2011). However, the Stokes-Einstein relationship should  
2 give reasonable estimations of diffusion rates for large organic molecules for conditions not close  
3 to the glass transition temperature of the matrix (Champion et al., 2000; Koop et al., 2011; Shiraiwa  
4 et al., 2011; Power et al., 2013; Marshall et al., 2016).

5 Using the diffusion coefficients ( $D_{org}$ ), the mixing time by diffusion,  $\tau_{mixing}$ , of large organic  
6 molecules within a 200 nm SOM particle was calculated with the following equation, where  $d$  is  
7 the particle diameter (Shiraiwa et al., 2011; Bones et al., 2012; Renbaum-Wolff et al., 2013a):

$$8 \quad \tau_{mixing} = \frac{d^2}{4\pi^2 D_{org}} \quad (\text{Eq.2})$$

9 Here we are using 200 nm to represent a typical accumulation mode atmospheric particle, Shiraiwa  
10 et al. (2011). The concentration of the diffusing molecules anywhere in the particles deviates by  
11 less than  $e^{-1}$  from the homogeneously well-mixed case at times longer than  $\tau_{mixing}$ . The  $\tau_{mixing}$  values  
12 calculated with this procedure are indicated in Fig. 5 (secondary y-axis). At an RH of 45% or  
13 higher, the mixing times are short, approaching less than or equal to 0.1 h. At 30% RH the mixing  
14 times are between 0.1 and 5 h. At  $\text{RH} \leq 17\%$  the mixing time is longer than  $\sim 100$  h (lower limit of  
15 the arrows in Fig. 5).

16

## 17 **5 Atmospheric implications**

18 In the following, we use the mixing times calculated in the previous section to estimate the mixing  
19 times of large organic molecules in organic particulate matter over megacities. Several caveats  
20 should be kept in mind when applying the mixing times discussed earlier to particles over  
21 megacities. First, organic particulate matter over megacities is most likely more complicated than  
22 toluene-derived SOM. Toluene and other aromatics can account for a large fraction of nonmethane  
23 hydrocarbon emission in urban environments (Singh et al., 1985; Na et al., 2005; Suthawaree et  
24 al., 2012) and toluene and aromatics are thought to be one of the main sources of SOM particles  
25 in urban environments (Odum et al., 1997; Schauer et al., 2002a; 2002b; Vutukuru et al., 2006;  
26 Velasco et al., 2007; de Gouw et al., 2008; Velasco et al., 2009; Gentner et al., 2012; Liu et al.,  
27 2012; Hayes et al., 2015). Nevertheless, large alkanes and unspciated nonmethane organic gases  
28 also likely play a role in SOM formation in urban environments. Second, the toluene-derived SOM

1 was generated using relatively large mass concentrations of particles ( $60 - 1000 \mu\text{g}\cdot\text{m}^{-3}$ ). The good  
2 agreement between our results and the results from Bateman et al. (2015) and Li et al. (2015),  
3 which were carried out with a mass concentration of  $30 - 1000 \mu\text{g}\cdot\text{m}^{-3}$ , suggests that for toluene-  
4 derived SOM the viscosity is not strongly dependent on the mass concentration of organics used  
5 to generate the SOM, but additional studies are needed to confirm this. Third, as mentioned above,  
6 the Stokes-Einstein equation was used to estimate diffusion coefficients and hence mixing times,  
7 and this equation can underestimate diffusion coefficients close to the glass transition temperature.  
8 Due to these caveats, the analysis below should be considered as a starting point for understanding  
9 the mixing times of large organic molecules in organic particulate matter over megacities.  
10 Additional studies are needed to explore the implications of the caveats discussed above.

11 For this analysis we define megacity as a metropolitan area with a total population in excess of ten  
12 million people. Based on the Population Division Data Query (2014) of the United Nations  
13 (<http://esa.un.org/>), we selected the top 15 most populous cities (Tokyo, Delhi, Shanghai, Mexico  
14 City, São Paulo, Mumbai, Osaka, Beijing, New York, Cairo, Dhaka, Karachi, Buenos Aires,  
15 Kolkata, and Istanbul) which meet this criterion.

16 In order to determine  $\tau_{mixing}$  for organic particulate matter in megacities, information on the RH  
17 and temperature in the cities is needed. Fig. 6 gives information on RH and temperature in the 15  
18 most populous megacities obtained from NOAA's National Climatic Data Center (NCDC)  
19 ([www.ncdc.noa.gov](http://www.ncdc.noa.gov)). The figure shows boxplots of average afternoon (3:00 – 5:00 local time) RH  
20 and temperature from these cities for the years from 2004 – 2014. The afternoon (3:00 – 5:00 local  
21 time) was chosen for this analysis since this is the time of day when RH is typically the lowest. In  
22 the figure, the boxes represent the median, 25<sup>th</sup> and 75<sup>th</sup> percentiles and the whiskers show the 10<sup>th</sup>  
23 and 90<sup>th</sup> percentiles. In addition to RH, viscosity can depend strongly on temperature (Champion  
24 et al., 1997; Koop et al., 2011). For example, the viscosity of solutions of sucrose and water may  
25 increase by two to three orders of magnitude for a 10 K decrease in temperature close to the glass  
26 transition temperature (Champion et al., 1997). However, the effect of temperature on the  
27 viscosity of toluene-derived SOM has not been quantified. As a result, we have limited the current  
28 analysis to months when the median afternoon temperature is within 5 K of the temperatures used  
29 in the viscosity measurements (i.e. 290 to 300 K). The fact that the median afternoon temperature  
30 is often below 290 K, highlights the need for low-temperature viscosity measurements.

1 In the Fig. 6, we indicate with green shading cases when the afternoon RH (at the 10<sup>th</sup> percentile  
2 level) does not go below 45% RH and the median afternoon temperature is 290-300 K. The cases  
3 when the afternoon RH (at the 10<sup>th</sup> percentile level) does not go below 45 % RH are listed in Table  
4 3 (second column). At 45% RH the mixing time within toluene-derived SOM is short (i.e., less  
5 than or equal to 0.1 h). Figure 6 (green shading) and Table 3 suggest that, if the organic particulate  
6 matter over megacities is similar to the toluene-derived SOM in this study, in Tokyo, Shanghai,  
7 Sao Paulo, and Istanbul mixing times during certain periods of the year will be very short, and  
8 homogeneously well-mixed particles can be assumed.

9 In the Fig. 6, we indicate with red shading cases where the afternoon RH (at the 10<sup>th</sup> percentile  
10 level) is 17% or lower and the median afternoon temperature is 290-300K. The cases when the  
11 afternoon RH (at the 10<sup>th</sup> percentile level) is 17 % or lower are listed in Table 3 (third column). As  
12 mentioned above, at this RH, the mixing time within toluene-derived SOM is long (> 100 h), based  
13 on the viscosity measurements and Stokes-Einstein calculations. Fig. 6 (red shading) and Table 3  
14 (third column) suggest that if the organic particulate matter is similar to the toluene-derived SOM  
15 in this study, in Mexico City, Beijing, Cairo, and Karachi, the particles may not be well-mixed in  
16 the afternoon (3:00 – 5:00 local time) during certain times of the year.

17 Kleinman et al., (2009) studied the time evolution of aerosol size distributions and number  
18 concentrations of ambient particulate matter over the Mexico City plateau during the MILAGRO  
19 (Megacity Initiative: Local And Global Research Observations) field campaign conducted in  
20 March 2006. The particulate matter over Mexico City was primarily organic and as photochemical  
21 aging occurred, Kleinman and colleagues observed an increase in accumulation-mode volume due  
22 to an increase in the accumulation mode particles, not because of an increase in the average size  
23 of the accumulation mode. The condensing organic vapors from photooxidation of toluene and  
24 other anthropogenic VOCs over Mexico City are expected to be semivolatile (Shrivastava et al.,  
25 2013). However, Kleinman et al. showed that the observed evolution of aerosol size distribution  
26 was not consistent with a volume growth mechanism in which the semivolatile organic vapors are  
27 expected to readily diffuse within the accumulation mode substrate. This could indicate that the  
28 accumulation mode particles over Mexico City were highly viscous and did not reach equilibrium  
29 with large gas-phase organic molecules during the observation period. This observation is  
30 consistent with our experimental results that toluene-derived SOM is highly viscous at RH < 20%

1 and Fig. 6, which shows that the median RH in Mexico City often falls below 20% in March.  
2 However, it should be noted that the particulate matter over Mexico City is likely more chemically  
3 complex than the SOM used in this study.

4

## 5 **6 Conclusions**

6 We investigated the RH-dependent viscosities at room temperature of SOM particles produced  
7 from toluene photo-oxidation with the mass concentration of 60 – 1000  $\mu\text{g}\cdot\text{m}^{-3}$ . A bead-mobility  
8 technique showed the viscosities of the toluene-derived SOM increased from  $\sim 0.2$  to  $\sim 129$  Pa·s as  
9 RH decrease from 89.9 to 60.7%. This indicates that the toluene-derived SOM particles are a liquid  
10 at  $\text{RH} > 60\%$ . The RH range for liquid-to-semisolid is in good agreement with Bateman et al.  
11 (2015) who showed the liquid-to-semisolid phase transition of these particles in the range of 60-  
12 80% RH. A poke-flow technique combined with fluid simulations showed the viscosities increased  
13 from approximately  $7.8 \times 10^3$  to  $6.3 \times 10^6$  Pa·s as RH decreases from 47.3 to 30.5%. For  $\text{RH} \leq$   
14 17%, the viscosities of the SOM were greater than or equal to  $\sim 2 \times 10^8$  Pa·s, similar to or greater  
15 than the viscosity of tar pitch. This suggests that the toluene-derived SOM particles are a semisolid  
16 at  $20 < \text{RH} \leq 60\%$ , and a semisolid or a solid at  $\text{RH} \leq 17\%$ . Using the viscosity data and the Stokes-  
17 Einstein equation, the diffusion coefficients of large gas-phase organic molecules within the  
18 toluene-derived SOM particles were calculated to be  $\sim 3 \times 10^{-8}$  to  $\sim 2 \times 10^{-15}$   $\text{cm}^2 \text{s}^{-1}$  for RHs from  
19 89.9 to 30.5%, and is lower than  $\sim 3 \times 10^{-17}$   $\text{cm}^2 \text{s}^{-1}$  for  $\text{RH} \leq 17\%$ . Mixing time by diffusion of  
20 large organic molecules within 200 nm toluene-derived SOM particles was calculated to be less  
21 than 0.1 h at  $\text{RH} < 47.3\%$ , 0.5 - 5 h at 30.5% RH, and greater than  $\sim 100$  h at  $\text{RH} \leq 17\%$ .

22 To apply the results of the viscosities, diffusion coefficients, and mixing time of the toluene-  
23 derived SOM, we selected the top 15 most populous megacities. Based on the RH in the cities, and  
24 if the organic particulate matter in megacities is similar to the toluene-derived SOM in this study,  
25 in cities such as Tokyo, Shanghai, Sao Paulo and Istanbul, mixing times during certain periods of  
26 the year will be very short and homogeneously well-mixed particles can be assumed. On the other  
27 hand, for certain times of the year in Beijing, Mexico City, Cairo, and Karachi, mixing times of  
28 large organic molecules in organic particulate matter may be long ( $\geq 100$  hr), and the particles may

1 not be well mixed in the afternoon (3:00 – 5:00 local time) during certain times of the year. These  
2 results are summarized in Fig. 7.

3

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9

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1 Table 1. Experimental conditions for production and collection of toluene-derived SOM particles  
 2 using the oxidation flow reactor. Particles were collected onto hydrophobic substrates using an  
 3 electrostatic precipitator or a single stage impactor.

SOM sample name	Toluene conc. (ppm)	Ozone conc. (ppm)	SOM mass conc. during production ( $\mu\text{g m}^{-3}$ )	OFR flow rate ( $\text{L m}^{-1}$ )	Collection time (hr)	Collection method
For bead-mobility experiments						
Toluene 1	$1.0 \pm 0.1$	$30 \pm 3$	600-1000	$7.0 \pm 0.5$	48	Electrostatic precipitator
Toluene 2	$1.0 \pm 0.1$	$30 \pm 3$	600-1000	$7.0 \pm 0.5$	48	Electrostatic precipitator
Toluene 3	$0.1 \pm 0.01$	$30 \pm 3$	60-100	$7.0 \pm 0.5$	12	Impactor
Toluene 4	$0.1 \pm 0.01$	$30 \pm 3$	60-100	$7.0 \pm 0.5$	19	Impactor
For poke-flow experiments						
Toluene 5	$1.0 \pm 0.1$	$30 \pm 3$	600-1000	$7.0 \pm 0.5$	96	Electrostatic precipitator
Toluene 6	$1.0 \pm 0.1$	$30 \pm 3$	600-1000	$7.0 \pm 0.5$	96	Electrostatic precipitator
Toluene 7	$0.1 \pm 0.01$	$30 \pm 3$	60-100	$7.0 \pm 0.5$	12.5	Impactor
Toluene 8	$0.1 \pm 0.01$	$30 \pm 3$	60-100	$7.0 \pm 0.5$	16	Impactor

4

5

1 Table 2. Physical parameters used to simulate material flow in the poke-flow experiments.  $R$  and  
 2  $r$  indicate the radius of a tube and the radius of an inner hole, respectively.

	Slip length (nm)	Surface tension (mN m <sup>-1</sup> )	Density (g cm <sup>-3</sup> )	Contact angle (°)
Values used to calculate lower limit	5 <sup>a</sup>	28 <sup>b</sup>	1.4 <sup>c</sup>	80 (if $r < 2R$ ), 100 (if $r > 2R$ )
Values used to calculate upper limit	10000 <sup>a</sup>	75 <sup>d</sup>	1.4 <sup>c</sup>	80 (if $r < 2R$ ), 100 (if $r > 2R$ )

3 <sup>a</sup>The range of slip length, which is the interactions between fluids and solid surfaces, is based on  
 4 literature data (Schnell, 1956; Churaev et al., 1984; Watanabe et al., 1999; Baudry et al., 2001;  
 5 Craig et al., 2001; Tretheway and Meinhart, 2002; Cheng and Giordano, 2002; Jin et al., 2004;  
 6 Joseph and Tabeling, 2005; Neto et al., 2005; Choi and Kim et al., 2006; Joly et al., 2006; Zhu et  
 7 al., 2012; Li et al., 2014).

8 <sup>b</sup>The lower limits of the surface tension of toluene-derived SOM were determined as 28 mN m<sup>-1</sup>,  
 9 the surface tension of liquid toluene at 293 K (Adamson and Gast, 1997).

10 <sup>c</sup>Ng et al., 2007

11 <sup>d</sup>The upper limits of the surface tension of toluene-derived SOM were determined as 75 mN m<sup>-1</sup>,  
 12 the surface tension of pure water at 293 K (Engelhart et al., 2008).

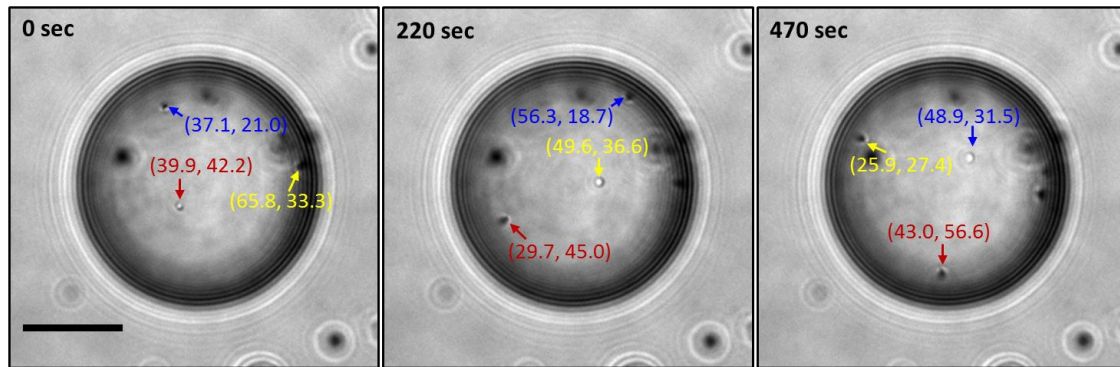
13 <sup>e</sup>Contact angle of the toluene-derived SOM on a substrate measured by 3-D fluorescence confocal  
 14 microscope ranged from 80 - 100°. The relationship of viscosity and contact angle depends on the  
 15 ratio of the radius of a tube,  $R$ , to the radius of an inner hole,  $r$  (Grayson et al., 2015a).

16

1 Table 3. Months when the afternoon RH in the 15 most populous megacities either does not go  
 2 below 45 % (at the 10<sup>th</sup> percentile level) or is 17% or lower (at the 10<sup>th</sup> percentile level) and the  
 3 median afternoon temperature is 290-300 K. “None” indicates that these criteria are not met for  
 4 any month.

Megacity	Months when the afternoon RH (at the 10 <sup>th</sup> percentile level) does not go below 45 %	Months when the afternoon RH (at the 10 <sup>th</sup> percentile level) is 17 % or lower
Tokyo	Jun and Sep.	none
Delhi	none	none
Shanghai	Jun. and Sep.	none
Mexico City	none	Jan. – May, Dec.
Sao Paulo	Jan.	none
Mumbai	none.	none
Osaka	none	none
Beijing	none	Apr. and May.
New York	none	none
Cairo	none	Mar. – Apr.
Dhaka	none	none
Karachi	none	Jan. And Dec.
Buenos Aires	none	none
Kolkata	none	none
Istanbul	Oct.	none

1

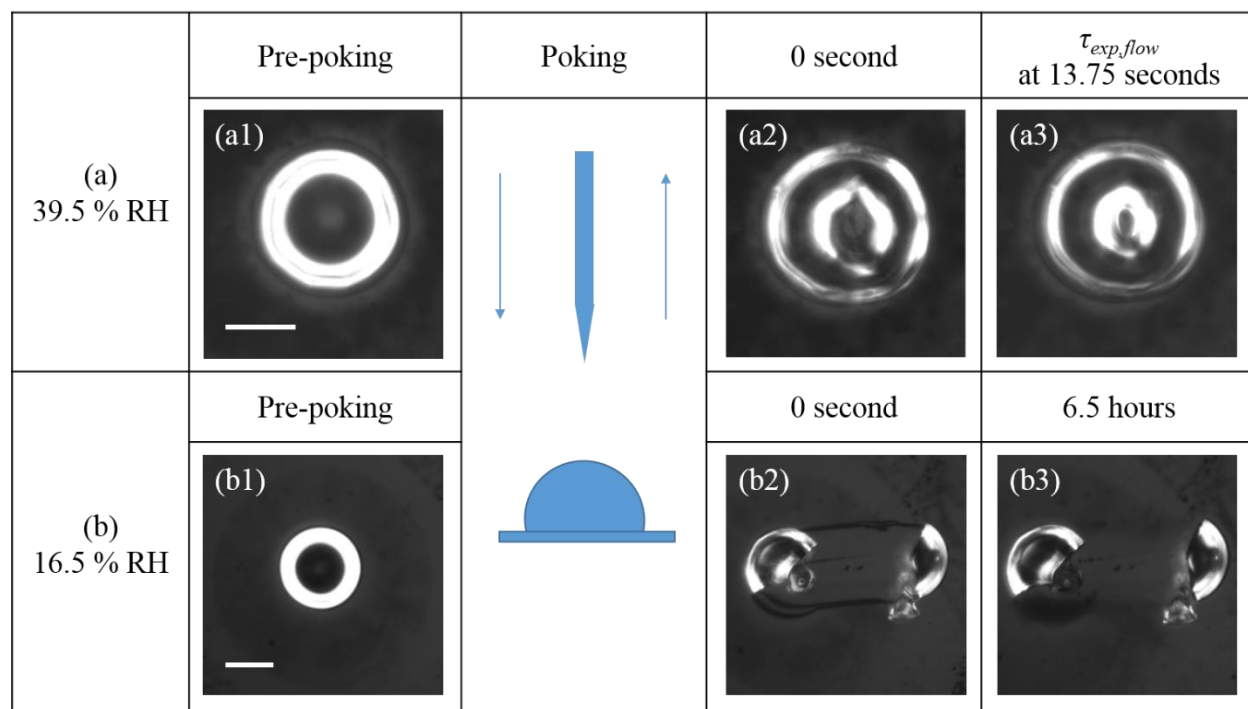


2

3 **Fig. 1.** Optical images from typical bead-mobility experiments for a toluene-derived SOM particle  
4 (Toluene sample 8 in Table 1) at 80% RH. Three different beads are labeled using colored arrows.  
5 The  $x$  and  $y$  coordinates of these beads are also indicated. Scale bar: 20  $\mu\text{m}$ .

6

7



1

2

3 **Fig. 2.** Optical images of pre-poking, poking, and post-poking from typical poke-flow experiments  
4 on toluene-derived SOM particles (toluene sample 6) at (a) 39.5% RH and (b) 16.5% RH. Panel  
5 a1 and b1; pre-poking, Panel a2 and b2: post-poking immediately after the needle has been  
6 removed (time set = 0 s), Panel a3; the experimental flow time,  $\tau_{exp,flow}$ , where the diameter of hole  
7 has decreased to 50% of its initial size, and Panel b3; particles shatter and do not flow over a period  
8 of 6.5 h. Size bar: 20  $\mu\text{m}$ .

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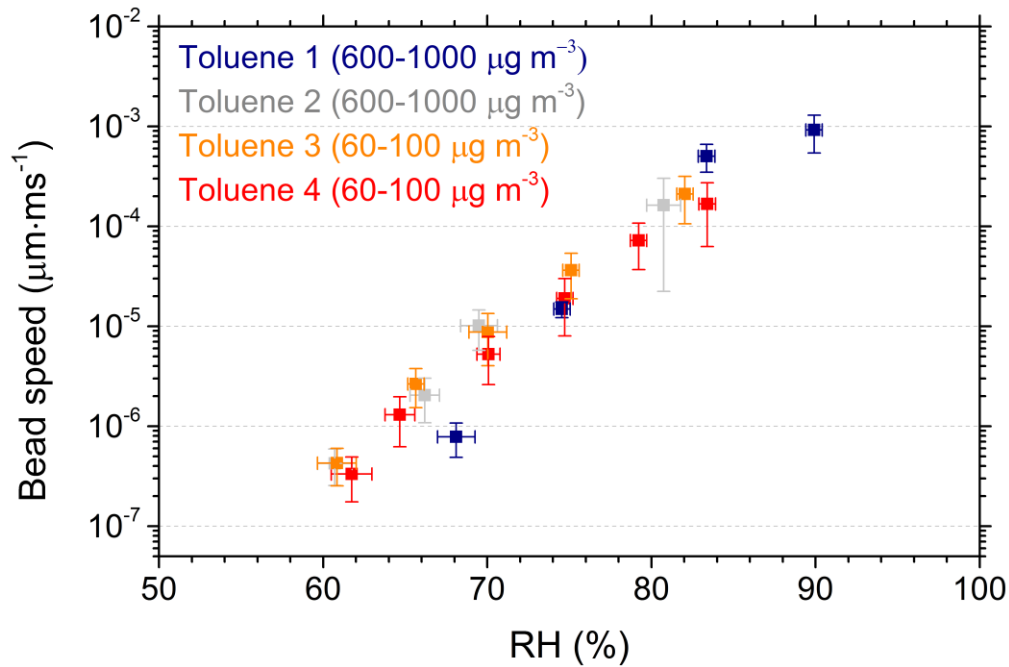
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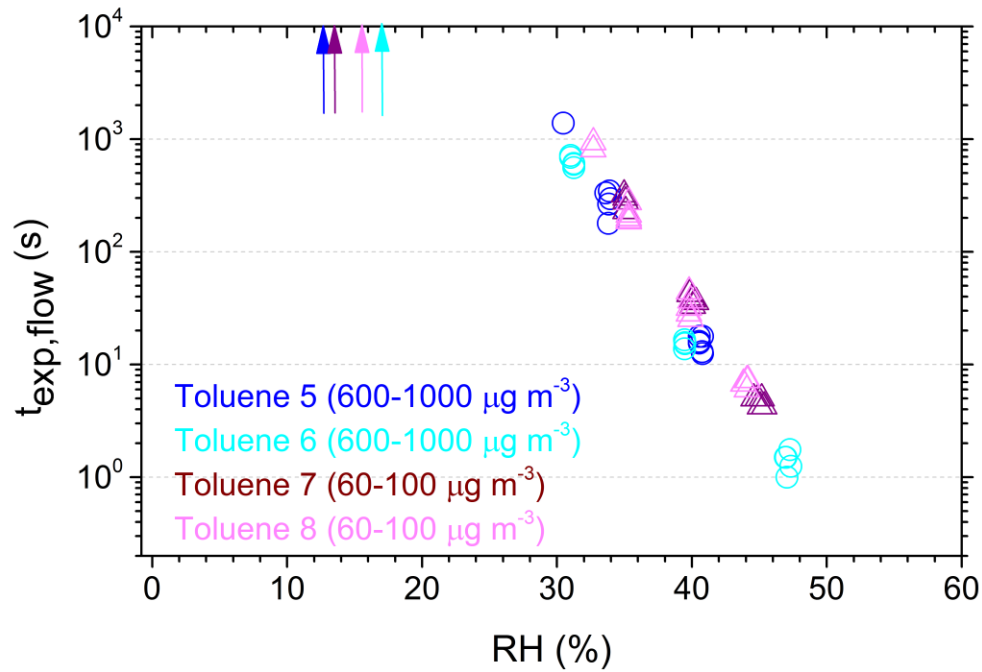
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2

3 **Fig. 3.** Measured average bead speeds as a function of RH for different SOM samples (Toluene 1,  
 4 2, 3, and 4, see Table 1). The bead speeds of 3 - 10 beads were used to determine a mean bead  
 5 speed. The  $x$ -error bars represent the uncertainty in the RH measurements and the range of RH  
 6 values in a given experiment. The  $y$ -error bars represent the standard deviation of the measured  
 7 bead speeds.

8





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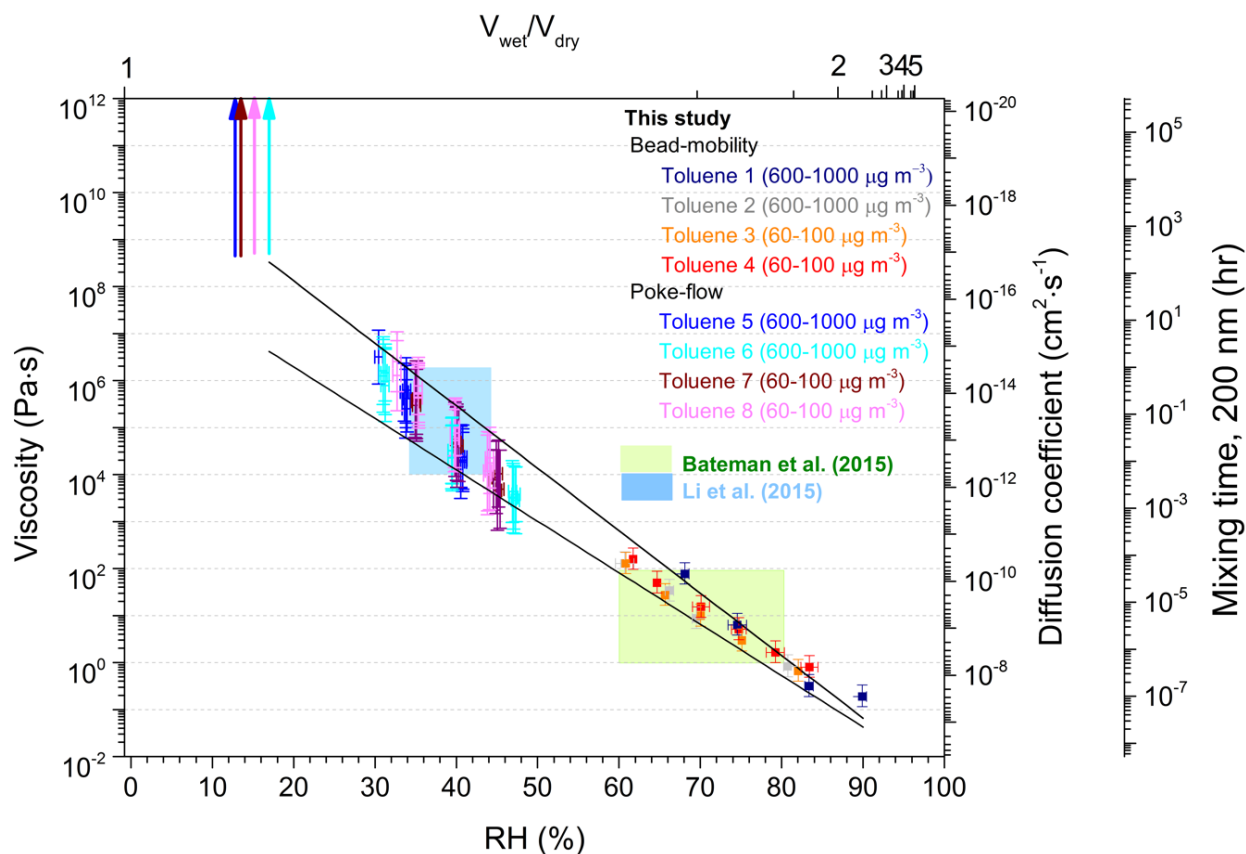
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3 **Fig. 4.** Results from poke-flow experiments.  $\tau_{\text{exp, flow}}$ , where the diameter of hole has decreased to  
 4 50% of its initial size, measured for the different samples (Toluene 5, 6, 7, and 8, see Table 1).

5 The arrows indicate particles shattered at the given RH.

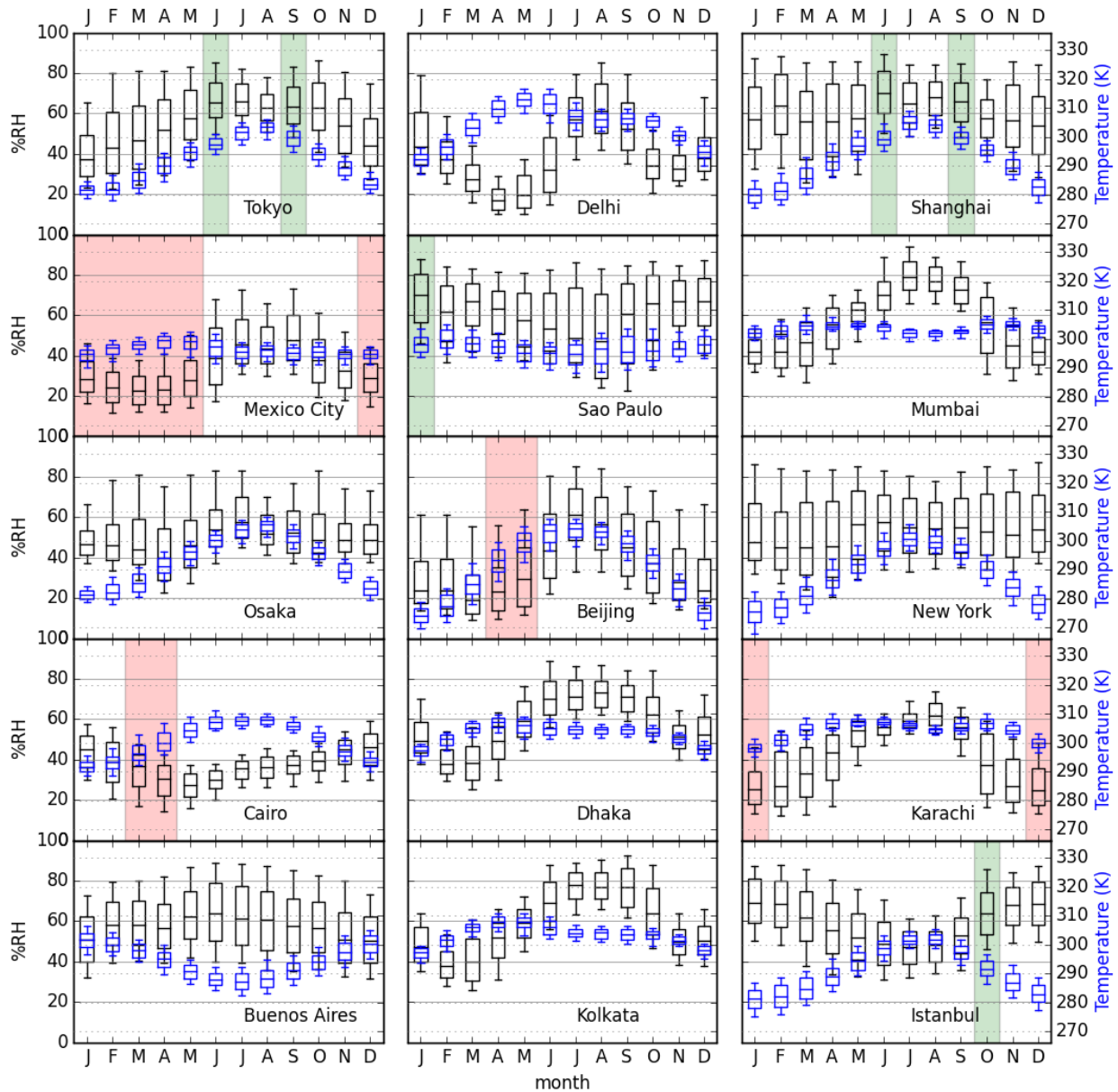
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1  
2  
3 **Fig. 5.** Viscosities of toluene-derived SOM particles as a function of RH. For RH > 60% the  
4 viscosities were determined from the mean bead speeds (see Fig. 3) and a calibration line (Song et  
5 al., 2015). The y-error bars for RH > 60% represent the 95% prediction intervals from the  
6 calibration line. For RH < 60% the viscosities were calculated from the  $\tau_{\text{exp, flow}}$  where y-error bars  
7 represent the calculated lower and upper limits of viscosity using the simulations. The x-error bars  
8 over the entire range of RH represent the range of RH values in a given experiments and the  
9 uncertainty in the RH measurements. The right y-axes present calculated diffusion coefficients of  
10 organic molecules in SOM using the Stoke-Einstein relation, and calculated mixing times within  
11 200 nm particles due to bulk diffusion using Eq. (2). The black lines represent linear fits for the  
12 RH vs. log(lower viscosities) ( $R^2 = 0.958$ ) and log(upper viscosities) ( $R^2 = 0.984$ ) from the entire  
13 data set excluding the RH where particles cracked. Viscosity of toluene-derived SOM particles  
14 from Bateman et al. (2015) (green box) and Li et al. (2015) (blue box) is also included. The

- 1 secondary  $x$ -axis shows  $V_{\text{wet}}/V_{\text{dry}}$  of the SOM, where  $V_{\text{dry}}$  is the volume of SOM at 0% RH and
- 2  $V_{\text{wet}}$  is the volume of the SOM after taking up water at a given RH.
- 3



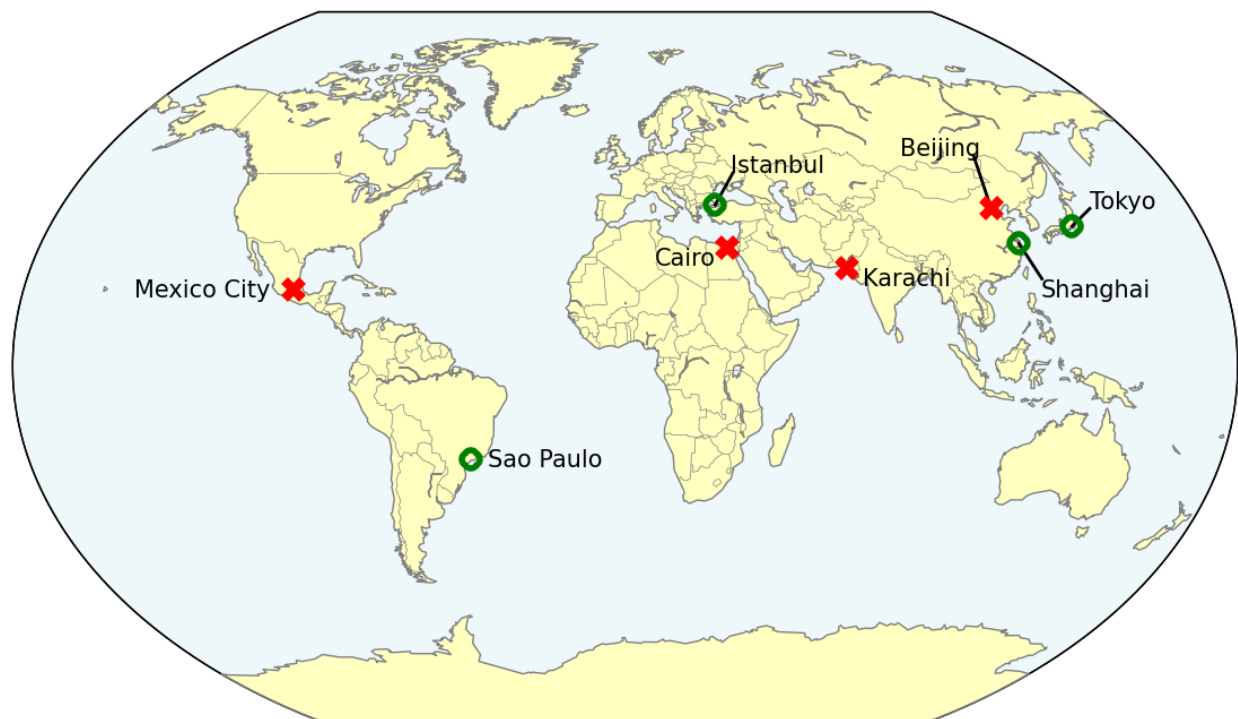
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4 **Fig. 6.** Monthly average RH and temperature for the megacities of Tokyo, Delhi, Shanghai,  
 5 Mexico City, São Paulo, Mumbai, Osaka, Beijing, New York, Cairo, Dhaka, Karachi, Buenos  
 6 Aires, Kolkata, and Istanbul. For the stations, afternoon averages RH values (3-5 pm local time)  
 7 were retrieved from NOAA's National Climate Data Center for the years from 2004 to 2014. Boxes  
 8 show the median, 25<sup>th</sup> and 75<sup>th</sup> percentiles of 3-hr averages and the whiskers show the 10<sup>th</sup> and

1 90<sup>th</sup> percentiles. Green shading indicates that the afternoon RH (at the 10<sup>th</sup> percentile level) does  
2 not go below 45% RH and the median afternoon temperature is 290–300K. Red shading indicates  
3 that the afternoon RH (at the 10<sup>th</sup> percentile level) is 17% or lower and the median afternoon  
4 temperature is 290–300K.

5



1

2

3 **Fig. 7.** Summary of conclusions reached after applying the results of the viscosities, diffusion  
4 coefficients, and mixing time of the toluene-derived SOM to the top 15 most populous megacities.  
5 Green circles indicates megacities where the afternoon RH at 10<sup>th</sup> percentile does not go below  
6 45 % RH and the median afternoon temperature is 290-300 K for certain times of the year. In  
7 these cases, well-mixed particles can be assumed. Red crosses indicates megacities where the  
8 afternoon RH at 10<sup>th</sup> percentile is 17 % or lower for certain times of the year and the median  
9 afternoon temperature is 290-300 K. In these cases, the particles may not be well-mixed in the  
10 afternoon for certain times of the year.