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Comparative study of the effect of water on the heterogeneous reactions of carbonyl sulfide on the surface of α -Al₂O₃ and MgO

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Abstract

The heterogeneous reaction on mineral dust was considered as a new sink of OCS in the troposphere. Here we compared the heterogeneous reactions of carbonyl sulfide (OCS) on the surface of α -Al₂O₃ and MgO and the effect of water on the reactions 5 at 300 K using Knudsen cell – mass spectrometry, diffuse reflectance infrared Fourier transform spectroscopy, and temperature programmed reactions. H₂S and CO₂ were found to be hydrolysis products of OCS on both α -Al₂O₃ and MgO at ambient temperature. At low water vapor pressure, when water vapor pressure in the Knudsen cell reactor increased from 2.3×10^{-6} to 6.8×10^{-6} Torr, the initial true uptake coefficient of OCS on α -Al₂O₃ decreased from 4.70×10⁻⁷ to 3.59×10⁻⁷; while it increased from 10 5.19×10^{-7} to 6.48×10^{-7} on MgO under the same conditions. At high relative humidity, the observed uptake coefficients of OCS on α -Al₂O₃ and MgO decreased from 4.63×10^{-6} to 1.00×10^{-6} and from 9.72×10^{-5} to 7.68×10^{-5} , respectively, when RH increased from 0.07 to 0.67 which corresponding to 1.7-15.9 Torr of water vapor pressure. In the RH region of 0.17–0.67, the average observed uptake coefficient of OCS 15 on α -Al₂O₃ and MgO was equal to 8.34±2.19×10⁻⁷ and 8.19±0.48×10⁻⁵, respectively. The restrictive effect of water on the heterogeneous reaction of OCS on the surface of α -Al₂O₃ and MgO was found to be related to competitive adsorption between water and OCS molecules; while the promotive effect of water on the heterogeneous reaction of OCS on the surface of MgO at low coverage was ascribed to the formation of 20 surface hydroxyl groups. When the environmental RH was greater than the RH of the monolayer, which occurred readily at the typical relative humidity of the troposphere, liquid membrane formed on the mineral dusts, especially, the basic liquid membrane formed on the basic component of mineral dusts may be the primary contributor to the

²⁵ heterogeneous hydrolysis of OCS in the troposphere.

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1 Introduction

Carbonyl sulfide (OCS) is the most abundant sulfur compound in the atmosphere and, in the troposphere, has a rather uniform mixing ratio of approximately 500 pptv (Watts, 2000). The oxidation of OCS in the stratosphere is an important source of stratospheric
⁵ sulfate aerosol (SSA) during non-volcanic periods (Crutzen, 1976; Engel and Schmidt, 1994; Turco et al., 1980). SSA plays an important role in the Earth's radiation balance (Andreae et al., 1997; Craf, 2004; Turco et al., 1980) and stratospheric ozone chemistry (Solomon et al., 1993). Therefore, much interest has been drawn to the sources and sinks of OCS. In particular, it is important to investigate the tropospheric sinks of OCS
¹⁰ because these sinks are not only related to the source of SSA but also to the global chemical cycle of OCS in the atmosphere.

Oxic soils, vegetation, photolysis, and oxidation by OH and O are the primary sinks of OCS in the atmosphere (Kettle et al., 2002; Montzka et al., 2007; Watts, 2000). In past decades, heterogeneous reactions of trace gases on atmospheric particulate

- ¹⁵ matter (APM) have received much attention. Several atmospheric modeling studies have shown that APM often acts as a sink for certain species (Dentener et al., 1996; Jacob, 2000; Usher, 2003b). Mineral dust, which mainly originates from arid and semiarid regions having a global source strength of ~1000–3000 Tg year⁻¹ (Dentener et al., 1996), is one of the most important contributors to the loading of APM. Recently, a few
- ²⁰ studies demonstrated that heterogeneous reactions of OCS can occur on APM, and on mineral oxides including Al_2O_3 , SiO_2 , Fe_2O_3 , CaO, MgO, MnO₂ and the mixture of Fe_2O_3 and NaCl under ambient conditions (Chen et al., 2007; He et al., 2005; Liu et al., 2006, 2007a, b; Wu et al., 2004, 2005). Although the same intermediate (i.e., hydrogen thiocarbonate, HSCO₂⁻) was observed, the pathways of heterogeneous reactions
- of OCS still require further study. For example, some researchers have proposed a heterogeneous oxidation mechanism (Chen et al., 2007; He et al., 2005; Liu et al., 2006; Wu et al., 2004, 2005), while recently we found that heterogeneous hydrolysis of OCS can also occur on MgO (Liu et al., 2007a). Nonetheless, information on the kinetics of

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the heterogeneous reaction of OCS on mineral oxides is limited. We recently reported uptake coefficients of OCS on MgO (Liu et al., 2008a), α -Al₂O₃ and γ -Al₂O₃ (Liu et al., 2008b). All of these studies were performed under dry conditions. However, the typical relative humidity (RH= P/P_0 , where P_0 is the saturated vapor pressure of liquid water) ⁵ in the troposphere is between 0.20 and 0.90 (Al-Abadleh et al., 2005; Carlos-Cuellar et al., 2003). The presence of adsorbed water undoubtedly plays a vital role in the heterogeneous reaction of trace gases, such as HNO₃, O₃ and SO₂ etc., on mineral dust (Al-Abadleh et al., 2005; Roscoe and Abbatt, 2005). Nevertheless, the affect of water

¹⁰ α -Al₂O₃ and MgO are typical constituents of mineral dust and are widely used as model oxides for the study of trace gases heterogeneous reactions. In this work, diffuse reflectance infrared Fourier transform spectroscopy (DRIFTS), Knudsen cell mass spectrometry (KCMS), and temperature-programmed reactions (TPR) were used to investigate the effect of water on the heterogeneous reactions of OCS on α -Al₂O₃ and MgO. Our results demonstrate that catalytic hydrolysis of OCS can take place on the

on the reaction mechanism and kinetics of OCS on mineral dust remains uncertain.

¹⁵ MgO. Our results demonstrate that catalytic hydrolysis of OCS can take place on the surface of both α -Al₂O₃ and MgO under ambient conditions and that adsorbed water on mineral dust influences this reaction greatly. The mechanism and the atmospheric implications for the effect of water on the heterogeneous reactions of OCS on mineral oxides are also discussed.

20 2 Experimental methods and data evaluation

2.1 Materials

The α -Al₂O₃ sample was prepared from boehmite (AlOOH, supplied by Shandong Alumina Corporation) by calcining at 1473 K. The MgO sample (A.R.) used in this experiment was supplied by the Haizhong Chemical Plant in Tianjin. All other chemicals were used without further purification. These included: Carbonyl sulfide (OCS, 2%, OCS/N₂, Scott Specialty Gases Inc.), N₂ and O₂ (99.999% purity, Beijing AP BEIFEN

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Gases Inc.), and C₂H₅OH (99.7%, Beijing Chemicals Factory).

2.2 Characterization of samples

The X-ray powder diffraction pattern was collected from 10 to 90° 2θ on a D/max-RB automatic powder X-ray diffractometer using Cu K α irradiation. The Al₂O₃ sample calcined at 1473 K was identified as α -Al₂O₃ with the three main peaks at 35.0°, 43.0°,

57.0°, and the MgO sample was identified to be periclase with the three main 2θ peaks at 42.9°, 62.3°, and 78.6°.

Nitrogen Brunauer-Emmett-Teller (BET) physisorption measurement was performed using a Micromeritics ASAP 2000 automatic instrument. The specific surface area of α -Al₂O₃ and MgO samples was measured to be 12.0 m² g⁻¹ and 14.6 m² g⁻¹, respectively.

2.3 Experimental methods

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2.3.1 KCMS experiments

A homemade Knudsen cell-mass spectrometer, described in detail elsewhere (Liu et ¹⁵ al., 2008a, b), was used to measure the uptake coefficients of OCS at low water vapor pressures in the reactor. Briefly, the particle samples were dispersed evenly on a sample holder with alcohol and then dried at 393 K for 2 h. The pretreated samples and reactor chamber were evacuated at 323 K for 6 h to reach a base pressure of approximately 5.0×10^{-7} Torr. The sample cover was closed after the system was cooled to 300 K. OCS (1.51%) balanced with simulated air (21% O₂ and wet 79% N₂) in which the water vapor was introduced through a saturated water generator by a N₂ stream, was introduced into the reactor chamber through a leak valve. The RH in the feed gas was controlled by the ratio of dry air to wet N₂ and was measured using a hygrometer (Center 314) with a relative error of ±1.5%. Prior to the uptake experi-

ments, the system was passivated with the feed gas for 150 min to a steady-state of

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quadrupole mass spectrometer (QMS) signal established as the sample was isolated from the gas by the sample cover. Uptake of OCS on all samples was performed with an average OCS partial pressure of $5.3\pm0.3\times10^{-6}$ Torr, which is equivalent to $1.7\pm0.2\times10^{11}$ molecules cm⁻³ or 7.0 ± 0.3 ppb.

⁵ For steady-state uptake, the uptake coefficients at different water vapor pressures were calculated using the Knudsen cell equation (Underwood, 2000):

$$\gamma_{\rm obs} = \frac{A_h}{A_g} \frac{(I_0 - I)}{I} \tag{1}$$

where γ_{obs} is the observed uptake coefficient, A_h is the effective area of the escape aperture (m²), A_g is the geometric area of the sample holder (m²), and I_0 and I are the mass spectral intensities with the sample holder closed and open, respectively. The effective area of escape aperture, A_h , was measured according to previously described methodology (Liu et al., 2008a, b). As for multilayer powder samples, to consider the contribution of underlying layers of sample to the uptake coefficient, the true uptake coefficient, γ_t , was calculated from:

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$$\gamma_t = \text{slope} \cdot \left(\frac{A_s}{S_{\text{BET}}}\right)$$

where *slope* is the slope of the plot of γ_{obs} versus the sample mass in the linear region (kg⁻¹), A_s is the geometric area of the sample holder (m²), and S_{BET} is the specific surface area of the particle sample (m² kg⁻¹) (Liu et al., 2008a, b; Underwood et al., 2000, 2001).

20 2.3.2 TPR experiments

The instantaneous experiments for the heterogeneous reaction of OCS on mineral oxides were performed with a TPR apparatus. This apparatus consists of a temperatureprogrammed tube oven and a QMS (Hiden HPR20). One quartz tube was used as

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a sample tube, and another was used as a by-pass tube. The powder samples with 20-40 meshes (0.5 g) in the sample tube were pretreated in 100 mLmin^{-1} of simulated air at 573 K for 1 h. After the sample cooled to room temperature (r.t.), the two ends of the sample tube were closed, and 1000 ppmv of OCS in simulated air with a total flow rate of 100 mLmin^{-1} was introduced into the by-pass tube. The mass channels including m/z=60 (OCS), 44 (CO₂), and 34 (H₂S) were monitored online with the QMS. Until the steady-state of QMS signal intensity was established, the feed gas was shifted between the sample and by-pass tubes several times. Then, the TPR experiment was performed at 20 K min⁻¹ from r.t. to 430 K as the feed gas passed through the sample tube.

2.3.3 DRIFTS experiments

The apparent reaction rate constants at high RH for the heterogeneous reactions of OCS on α -Al₂O₃ and MgO were measured with a DRIFTS reactor in a closed system. In situ DRIFTS spectra were recorded on a NEXUS 670 (Thermo Nicolet Instrument Corporation) Fourier transform infrared spectrometer (FTIR) equipped with an in situ diffuse reflection chamber and a high sensitivity mercury cadmium telluride (MCT) detector cooled by liquid N₂. The infrared spectra were collected and analyzed by a computer with OMNIC 6.0 software. All spectra reported here were recorded at a resolution of 4 cm⁻¹ for 100 scans. The volume of the reactor chamber in the closed system

²⁰ was 30 mL.

The oxide sample (~10 mg) was finely ground and placed into a ceramic crucible in the in situ chamber. Before the DRIFTS measurement, the sample was pretreated in the in situ chamber at 573 K in 100 mL min⁻¹ of simulated air (79% N₂ and 21% O₂) for 2 h. After the pretreated sample cooled to 300 K, the reference spectrum was collected.

The oxide sample was then exposed to wet air with different RH for 20 min. The RH in the feed gas was controlled and measured as described for the KCMS experiment. After 1000 ppmv of OCS balanced with simulated wet air was introduced into the reactor for 3 min, the inlet and outlet of the reactor chamber were closed promptly. The



infrared spectra in the closed system were collected automatically by a computer. The concentration of OCS in the reactor was calibrated with standard OCS gas. From the decrease in concentration of gaseous OCS in the closed system, the apparent quasi first-order reaction rate constants were obtained:

$$5 \ln \frac{c_{\text{OCS},t}}{c_{\text{OCS},0}} = kt$$
(3)

where $c_{\text{OCS},t}$ and $c_{\text{OCS},0}$ are the concentrations of OCS at *t* s and 0 s, respectively, *k* is the apparent reaction rate constant (s⁻¹), and *t* is the reaction time (s). The observed uptake coefficients were calculated by Eqs. (4) and (5) (Li et al., 2006; Ullerstam et al., 2003):

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$$\gamma_{\rm obs} = \frac{k}{Z \cdot A_s}$$

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$$Z = \sqrt{\frac{8R \cdot T}{\pi \cdot M}} \cdot \frac{1}{4V}$$

where γ_{obs} is the observed uptake coefficient, *k* is the apparent reaction rate constant (s⁻¹), *V* is the reactor chamber volume (m³), *Z* is the collision frequency, A_s is the reactive surface area (m²), *T* is the temperature (K), *R* is the ideal gas constant (J mol⁻¹ K⁻¹), and *M* is the molecular weight of the OCS molecule (kg mol⁻¹).

To investigate the adsorption behavior of water on the model oxides, the infrared spectra and adsorptive isothermal curves of water on oxides were also measured using DRIFTS. Pretreated samples were exposed to wet air with different RH at 300 K for 20 min to establish an adsorption equilibrium. The infrared spectra at equilibrium were collected, and the original spectra were converted using the Kubelka-Munk function (Sirita et al., 2007). The K-M value of OH vibrational stretch (3700–2500 cm⁻¹) was used to denote the adsorptive capacity of water on mineral oxides.

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(5)





3 Results

3.1 Comparative study of the heterogeneous reaction of OCS on the surface of $\alpha\text{-Al}_2\text{O}_3$ and MgO

Figure 1 shows typical uptake profiles of OCS and water on α -Al₂O₃ and MgO at 300 K, s as measured by KCMS. The partial pressures of OCS and water vapor in the Knudsen cell reactor were 5.3×10^{-6} and 5.8×10^{-6} Torr, respectively. As shown in Fig. 1a, when the pretreated samples were exposed to the feed gas, the QMS signal intensity of OCS (m/z=60) decreased dramatically and was followed by a quick saturation process within 100 s on α -Al₂O₃. An apparent steady-state of uptake on the time scale of this experiment was then guickly reached. However, the QMS signal intensity of OCS 10 (m/z=60) on MgO came to a steady-state gradually within 1000 s (Fig. 1b). The quick saturation was ascribed to desorption of adsorbed OCS, while the steady-state uptake was related to the consumption of OCS by the heterogeneous reaction. Therefore, it can be deduced from Fig. 1a and b that desorption of OCS on the surface of α -Al₂O₃ was prominent while the heterogeneous reaction was weak. As shown in Fig. 1c and d, the signal intensity of water vapor also decreased when the same sample was exposed to the feed gas. The signal intensity of water vapor on α -Al₂O₃ increased gradually with exposure time, while continuous uptake of water was observed on MgO. These results demonstrate that α -Al₂O₃ and MgO can take up OCS and water simultaneously by adsorption and heterogeneous reaction at ambient temperature. 20

To investigate the surface and gaseous products during the heterogeneous processes of OCS on α -Al₂O₃ and MgO, DRIFTS and TPR experiments were performed. As described in Sect. 2.3, the sample was pretreated in the in situ chamber at 573 K in 100 mL min⁻¹ of simulated air (79% N₂ and 21% O₂) for 2 h. The RH in the feed gas was measured to be 0.07. Figure 2 shows the surface species formed on α -Al₂O₃ and MgO at 300 K after 10 min in the closed system after the pretreated samples were exposed to 1000 ppmv of OCS balanced with air. The cutoffs below 1200 cm⁻¹ in Fig. 2a and 900 cm⁻¹ in Fig. 2b were not shown because of the strong lattice vibrational ab-

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sorption of the samples. The absorption bands shown in Fig. 2 were assigned based on values found in the literatures (Table 1). As shown in Fig. 2a, surface hydroxyl (-OH) was consumed and gaseous carbon dioxide (CO₂), surface carbonic acid (H₂CO₃), bicarbonate (HCO₃⁻), thiocarbonate (HSCO₃⁻), carbonate (CO₃²⁻) and sulfate (SO₄²⁻) were formed on α -Al₂O₃. These results are similar to the previously described heterogeneous oxidation of OCS on γ -Al₂O₃ (He et al., 2005; Liu et al., 2006), suggesting that the heterogeneous oxidation of OCS may also occur on α -Al₂O₃. In Fig. 2b, apart from the above species, sulfur species including physisorbed sulfur dioxide (SO₂), surface sulfite or bisulfite (SO₃²⁻/HSO₃⁻), and surface hydrogen sulfide (-SH) were also

- ¹⁰ observed. A band at 2578 cm⁻¹ caused by adsorption of surface -SH was also observed and is shown enlarged in the insert graph in Fig. 2b. The formation of surface -SH implies that gaseous hydrogen sulfide (H_2S) may be formed during the heterogeneous reaction of OCS on the surface of MgO. However, this hypothesis needs to be further tested. It should be noted that the relative intensity between gaseous CO₂
- and surface HCO_3^- in Fig. 2a is much higher than that in Fig. 2b. This could be due to the fact that the basicity of MgO is stronger than that of α -Al₂O₃, which leads to low gaseous concentrations of CO₂ and high surface concentrations of HCO_3^- .

Figure 3a illustrates the change in QMS signal intensity in the heterogeneous reaction of OCS on MgO at 300 K. When the MgO sample was exposed to 1000 ppmv of

- ²⁰ OCS balanced with air, the signal intensity of OCS (m/z=60) decreased initially, and then quickly came to a steady-state due to saturation of adsorption. At the same time, the signal intensities of CO₂ (m/z=44) and H₂S (m/z=34) increased. When the feed gas was shifted to the by-pass tube (background), the QMS signals of these compounds quickly returned to their corresponding baselines. This indicates that H₂S is
- ²⁵ also one of the gaseous products of the heterogeneous reaction of OCS on MgO, which supports the spectroscopic results presented in Fig. 2b and is also consistent with the results of the Knudsen cell study (Liu et al., 2008a). However, for the heterogeneous reaction of OCS on α -Al₂O₃, no changes in the QMS signals of OCS, CO₂, or H₂S in the flow system were apparent under the same reaction conditions, although the for-





mation of gaseous CO_2 and surface HCO_3^- were easily measured in the closed system (Fig. 2a). These contrary phenomena could be explained by the differential signals detected by QMS in the flow system and the integrated signal of DRIFTS in the closed system; however, the characteristic absorption band of -SH was also not observed. These results imply that the reaction of OCS on α -Al₂O₃ may differ from that on MgO. It should be noted that the uptake of OCS by α -Al₂O₃ at steady-state was much lower

than that by MgO (see Fig. 1), indicating a lower reaction rate. The lack of gaseous H_2S or surface -SH could be ascribed to the low yield of H_2S on α -Al₂O₃ at r.t., which was lower than the detectable limit of our apparatus. Therefore, TPR experiments were performed to increase the reaction rate and to confirm whether H_2S was formed during the heterogeneous reaction of OCS on the surface of α -Al₂O₃.

When 1000 ppmv of OCS in air passed through 0.5 g of α -Al₂O₃ or MgO samples and the temperature was increased, the concentration of OCS decreased, and the concentration of CO₂ and H₂S increased (Fig. 3c and d). However, the concentration of OCS (*m*/*z*=60), CO₂ (*m*/*z*=44), and H₂S (*m*/*z*=34) did not change with temperature when the feed gas passed through the by-pass tube. These date suggest that the quartz tube did not catalyze the oxidation or hydrolysis of OCS and that OCS did not

decompose under our experimental conditions. These results clearly demonstrate that H_2S is a gaseous product of the heterogeneous reaction of OCS on α -Al₂O₃ and that hydrolysis of OCS also occurs on α -Al₂O₃. The heterogeneous reaction of OCS on the surface of α -Al₂O₃ and MgO is be described by Reaction (R1).

 $OCS + H_2O \rightarrow H_2S + CO_2$

3.2 Effect of water on the heterogeneous hydrolysis of OCS on the surface of α -Al₂O₃ and MgO

As shown in Fig. 1, the uptake of water and OCS occurred synchronously when the samples were exposed to the feed gas, followed by hydrolysis reactions of OCS on the surface of α -Al₂O₃ and MgO. Because water is one of the reactants, it should have a



(R1)

fundamental effect on the reaction kinetics. Therefore, the reaction kinetics at different water vapor pressures was studied using KCMS and DRIFTS. Figure 4 shows the true uptake coefficient (γ_t) of OCS on α -Al₂O₃ and MgO under different water vapor pressures at 300 K. The partial pressure of water vapor in the Knudsen cell reactor was in the range of 2.5×10^{-6} – 6.8×10^{-6} Torr. As shown in Fig. 4, the γ_t of OCS on α -Al₂O₃ at both the initial (Ini) and steady-states (SS) decreased under conditions of increased water vapor pressure in the Knudsen cell reactor; diametrically opposed effects oc-

curred on MgO. This suggests that water significantly suppressed the adsorption and heterogeneous reaction of OCS on the surface of α -Al₂O₃ under these experimental conditions. However, water promoted the adsorption and heterogeneous reaction of OCS on the surface of MgO. The linear regression between γ_t and water vapor pressure (P_{H_2O}) can be expressed as follows:

for α -Ål₂O₃,

5

$$V_t(\text{Ini}) = 5.4 \times 10^{-7} - 0.032 \times P_{\text{H}_2\text{O}}, R = 0.937;$$

¹⁵
$$\gamma_t(SS) = 1.1 \times 10^{-7} - 0.013 \times P_{H_2O}, R = 0.999;$$

for MgO,

$$\gamma_t(\text{Ini}) = 3.5 \times 10^{-7} + 0.044 \times P_{\text{H}_2\text{O}}, R = 0.858;$$

$$\gamma_t(SS) = -8.9 \times 10^{-8} + 0.054 \times P_{H_2O}, R = 0.939.$$

In the Knudsen cell reactor, low pressure must be maintained to avoid molecular collisions between gases (Underwood et al., 2000, 2001); the maximal value in our system was 3.5×10^{-4} Torr. Even though pure water vapor was introduced into the reactor chamber, the pressure achieved was still much lower than the water vapor pressure found in the atmosphere. Therefore, the effect of water on the heterogeneous reactions of OCS on the surface of α -Al₂O₃ and MgO at relative humidity values representative of the troposphere was investigated using DRIFTS. The initial concentration of OCS in the

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feed gas was held at 1000 ppmv. The relative humidity in the feed gas was in the range of 0.07–0.67, which corresponds to 1.7–15.9 Torr of water vapor pressure. Figures 5a and 6a show the time-dependent logarithmic decline in the concentration of OCS on α -Al₂O₃ and MgO at 300 K in the closed system. The apparent reaction rate constants were calculated according to Eq. (3); all correlation coefficients were greater than 0.99. Subsequently, the corresponding γ_{obs} were calculated using Eqs. (4) and (5). Because the probe depth for OCS molecules in the powder samples could not be obtained in the DRIFTS experiments, the geometric area of the sample holder (0.20 cm²) was used. The relationship between the γ_{obs} and the RH in the feed gas is shown in Figs. 5b and 6b.

As shown in Fig. 5b, the γ_{obs} of OCS on α -Al₂O₃ decreased sharply with the increase of RH in the region of 0.07–0.17. The maximal γ_{obs} was 7.38×10⁻⁶ at a RH of 0.07. When the RH increased to 0.17, γ_{obs} remained at a constant value (3.58±0.19×10⁻⁶), which was slightly higher than the background value (2.74×10⁻⁶) caused by adsorption or reaction on the surface of the reactor chamber. However, as shown in Fig. 6b, the γ_{obs} of OCS on MgO decreased slowly from 9.99×10⁻⁵ at a RH of 0.07 to 7.95×10⁻⁵ at a RH of 0.67. The average value of γ_{obs} between the RH values of 0.17 and 0.67 was 8.46±0.42×10⁻⁵, which was ~30 times higher than the background value. When the contribution of the background to the uptake coefficients was subtracted, the observed uptake coefficients of OCS on α -Al₂O₃ and MgO decreased from 4.63×10⁻⁶ to 1.00×10^{-6} and from 9.72×10^{-5} to 7.68×10^{-5} , respectively. The average observed uptake coefficient of OCS on α -Al₂O₃ and MgO was equal to $8.34\pm2.19\times10^{-7}$ and $8.19\pm0.48\times10^{-5}$ between the RH values of 0.17 and 0.67, respectively.





4 Discussion

4.1 Catalytic hydrolysis of OCS on the surface of α -Al₂O₃ and MgO

Most studies of OCS reactions in the troposphere have focused on the heterogeneous oxidation of OCS on the surface of alumina etc. (Chen et al., 2007; He et al., 2005; 5 Liu et al., 2006; Wu et al., 2004, 2005), and the hydrolysis pathway has not been elucidated due to the absence of reaction products such as H_2S . In those studies, FTIR was mainly used to investigate the reaction process; however, the sensitivity of infrared absorbance for surface -SH or gaseous H_2S is much lower than that for CO₂. In our studies, the slope of the increased signal intensity of H_2S with temperature was smaller than that of CO₂ (Fig. 3c and d). This could be ascribed to the oxidation of 10 gaseous H₂S or surface -SH to other sulfur species with high oxidation states including gaseous SO₂, surface SO₂²⁻/HSO₃⁻ and SO₄²⁻. These oxidized species were observed in this study (Fig. 2) and in previous works (Chen et al., 2007; He et al., 2005; Liu et al., 2006; Wu et al., 2004, 2005). Therefore, gaseous CO₂ is more easily observed than gaseous H₂S or surface -SH when using FTIR. In our previous work, we reported 15 the production of H₂S for the reaction of OCS on the surface of MgO using DRIFTS (Liu et al., 2007a) and KCMS (Liu et al., 2008a). Desorption of H₂S was also observed after the heterogeneous reaction of OCS on the surface of α -Al₂O₃ using KCMS (Liu et al., 2008b). Additionally, H₂S and CO₂ were observed as the gaseous products for the catalytic hydrolysis of OCS on γ -Al₂O₃ at ambient temperature (Rhodes et al., 2000; 20 West et al., 2001). Therefore, we conclude that, similar to reaction on the surface of MgO, heterogeneous hydrolysis of OCS on the surface of α -Al₂O₃ also occurs at ambient temperature.

In Fig. 1, the uptake profiles of OCS on α -Al₂O₃ and MgO can be classified into two stages – the quick recover stage and the steady-state stage. Because the uptake experiments were performed under steady-state conditions, the change in OCS intensity can be described according to the conservation of mass by Eq. (10) when the sample

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was exposed to the reactant gas:

$$-\frac{dn_g}{dt} = -k'dI = k_{ads}n_g(1-\theta) - k_{des}N_a + k_hN_a$$
(10)

where n_g is the number of gaseous molecules of OCS in the Knudsen cell reactor (molecule), *t* is time (s), *k'* is a constant, *I* is the signal intensity of OCS measured ⁵ by mass spectrometer (a.u.), k_{ads} is the apparent rate constant for adsorption of OCS (s⁻¹), k_{des} is the apparent rate constant for desorption of OCS (s⁻¹), k_h is the apparent rate constant for the heterogeneous reaction of OCS (s⁻¹), θ is the coverage of OCS on oxide samples (= N/N_a^*), N_a^* is the saturated coverage of OCS on oxide samples (molecules), and N_a is the number of OCS molecule adsorbed on the oxide samples 10 at a given time (molecules).

Therefore, because θ was almost equal to zero at the initial time, the OCS signal decreased to its lowest intensity when the sample cover was removed. The signal intensity of OCS then gradually recovered because the contribution of desorption became prominent with the increase of θ (Fig. 1). If there was no catalytic reaction (k_h =0), the OCS signal would eventually recover to baseline due to the balance between adsorption and desorption. However, as shown in Fig. 1, a steady-state consumption of OCS was observed. As discussed above, gaseous and surface products were also

detected. Therefore, it can be concluded that the hydrolysis of OCS on the surface of α -Al₂O₃ and MgO is a catalytic reaction. In Fig. 1, the steady-state consumption of OCS on MgO (Fig. 1b) was much larger than that on α -Al₂O₃ (Fig. 1a). This suggests that the apparent reaction rate constant (k_h) of OCS on MgO is greater than that on α -Al₂O₃. Therefore, compared to α -Al₂O₃, the slow recovery rate of the OCS signal on MgO (Fig. 1b) can be ascribed to the compensatory effect of the catalytic reaction to desorption of OCS. This relationship is well described by Eq. (10).

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4.2 Mechanism for the effect of water on the heterogeneous reactions of OCS on the surface of α -Al₂O₃ and MgO.

As shown in Figs. 4a and 5b, adsorbed water on α -Al₂O₃ prominently restricted the adsorption and heterogeneous reaction of OCS at low water vapor pressures and at high relative humidity. These data indicate that water and OCS compete for the same adsorption site on α -Al₂O₃. On the surface of MgO, adsorbed water promoted the adsorption and heterogeneous reaction of OCS at low water pressures (Fig. 4b), but had the opposite effect at high relative humidity (Fig. 6). Therefore, the effect of water on the heterogeneous reaction or adsorption of OCS on the surface of MgO appears

to utilize different reaction mechanisms under conditions of low water vapor pressures versus high humidity conditions.

In previous work, hydrogen thiocarbonate $(HSCO_2^-)$ was determined to be the crucial intermediate for the heterogeneous oxidation and hydrolysis of OCS on mineral oxides; $HSCO_2^-$ is formed via the reaction of OCS with surface -OH on mineral oxides (He et al.,

- ¹⁵ 2005; Hoggan et al., 1994; Liu et al., 2006, 2007a). Additionally, we found that surface -OH contributes to not only the formation of HSCO₂ but also to the decomposition of HSCO₂ (Liu et al., 2007a). In Fig. 2, the consumption of hydroxyl was also observed. Therefore, the content and properties of surface hydroxyl groups of mineral oxides should be important in these reactions.
- On the base of synchrotron-based photoemission spectroscopy, low energy electron diffraction studies and high-level theoretical simulations, it was found that water molecules could dissociate and react with a low concentration of defective sites on mineral surfaces at very low vapor pressures (Brown Jr., 2001; Eng et al., 2000; Hass et al., 1998; Liu et al., 1998a, 1998b). For example, water molecules react relatively fast with surface defects (corners, edge-step sites, and point defects) on MgO to form surface -OH when the water vapor pressure is less than 3×10⁻⁵ Torr. When the water vapor pressure is greater than 10⁻⁴ Torr, dissociative chemisorption of water on terrace sites occurs (Liu et al., 1998a, 1998b). The formation of surface -OH at 3700 cm⁻¹ on MgO





at low water coverage was also confirmed using FTIR (Foster et al., 2002). Thus, below 0.05 RH, the reaction between water and MgO can be described by Reaction (R2) (Al-Abadleh et al., 2005):

 $MgO + H_2O \rightarrow Mg(OH)_2$

- In our experiment, the water vapor pressures in the Knudsen cell reactor were lower than 3×10⁻⁵ Torr. The number of surface hydroxyl groups on MgO would likely increase with water vapor pressure due to the dissociative chemisorption of adsorbed water. As shown in Fig. 4b, adsorbed water promoted the adsorption and heterogeneous reaction of OCS on the surface of MgO at low water pressures.
- ¹⁰ As for α -Al₂O₃, it was also shown that hydroxylation occurred during the conversion of corundum to gibbsite (Al(OH)₃) according to Reaction (R3) (Al-Abadleh and Grassian, 2003; Eng et al., 2000; Hass et al., 1998):

 $AI_2O_3 + 3H_2O \rightarrow 2AI(OH)_3$

Although a rather high initial sticking coefficient of 0.1 has been measured for H_2O on α -Al₂O₃ at 300 K, the sticking coefficient was found to decrease exponentially with increasing water coverage (Elam et al., 1998). After the surface is fully hydroxylated, additional water can only be physisorbed on the hydroxyl layer on both α -Al₂O₃ and MgO (Elam et al., 1998; Liu et al., 1998b). Because surface -OH is the reactive site for the heterogeneous reaction of OCS, the formation of surface -OH should promote the reaction while the molecular adsorption of water on surface -OH should suppress this reaction. Theoretically, the uptake coefficients on both α -Al₂O₃ and MgO (shown in Fig. 4) should increase initially and then decrease with the increased water vapor pressures. However, this turning point was not observed, which may be due to limitations of our experiment conditions. It should be pointed out that the α -Al₂O₃ sample used in our experiment may have already been partially hydroxylated, which would lead to a turn-

ing point that occurs at low water vapor pressures. Therefore, in Figs. 4a, 5b and 6b, the decrease in the uptake coefficients of OCS on α -Al₂O₃ and MgO under conditions

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(R2)

(R3)

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of increased water vapor pressure can be explained by competitive adsorption of H_2O and OCS on surface -OH. This assumption is well-supported by the consumption of surface -OH during the adsorption of pure water vapor on α -Al₂O₃ and MgO.

As shown in Fig. 7, when the pretreated samples were exposed to water vapor at different RH, negative bands of surface -OH at 3734 cm⁻¹ on α -Al₂O₃ and 3755 cm⁻¹ on MgO were observed. The bands at 3417, 3219, and 1637 cm⁻¹ on α -Al₂O₃ (as well as 3418, 3230, and 1630 cm⁻¹ on MgO) were assigned to the v_{as} (HOH), v_s (HOH) and δ (HOH) of adsorbed water, respectively (Al-Abadleh et al., 2005). Obviously, the frequencies of the hydroxyl groups consumed by water in Fig. 7 are the same as those consumed by the reaction of OCS in Fig. 2. This suggests that OCS and H₂O have the same adsorption site on both α -Al₂O₃ and MgO.

In Fig. 7, the insert graphs show the variations in the amount of surface -OH consumed by water at different RH. The consumption of surface -OH (A) with RH in Fig. 7 is directionally identical to the corresponding observed uptake coefficient of OCS with RH (Figs. 5h and 6h). At RH between 0.07 and 0.07 the absenced uptake coefficient

¹⁵ RH (Figs. 5b and 6b). At RH between 0.07 and 0.27, the observed uptake coefficient of OCS on α -Al₂O₃ and MgO decreased almost linearly with increased consumption of surface hydroxyl (*A*) by the adsorbed water (shown in Fig. 8). The linear equations are as follows:

$$\gamma_{\rm obs} = 8.10 \times 10^{-6} - 4.86 \times 10^{-6} \times A, \ \alpha - Al_2O_3, \ R = 0.997;$$
 (11)

$$\gamma_{\rm obs} = 1.02 \times 10^{-4} - 4.76 \times 10^{-6} \times A$$
, MgO, $R = 0.866$.

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Although the apparent activity of the heterogeneous reaction of OCS on MgO is much higher than that on α -Al₂O₃, the slope in Eq. (11) is almost equal to that in Eq. (12). This demonstrates that the decrease in γ_{obs} is quantitatively related to the amount of surface hydroxyl groups consumed by adsorbed water regardless of the type of mineral oxide.

It is well known that, depending on the RH value, monolayer and multilayers of water can adsorb to the surface of minerals. To measure the relative humidity of one mono-

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(12)



layer (RH_{ML}) of water and to understand the effect of water on the heterogeneous reaction of OCS on the surface of α -Al₂O₃ and MgO at high RH, the adsorption isotherm curves of water on these oxides were investigated. The number of adsorbed water layers was assumed to be in direct proportion to the integrated K-M value of the stretch vibration (3700–2500 cm⁻¹) of surface adsorbed water (Sirita et al., 2007). Therefore, the coverage of adsorbed water on α -Al₂O₃ and MgO was quantified by generating adsorption isotherm curves according to a three-parameter Type III BET fit, as shown in Eq. (13) (Goodman et al., 2001):

$$\frac{\text{KM}}{\text{KM}_{\text{ML}}} = \left(\frac{c\text{RH}}{1 - \text{RH}}\right) \left(\frac{1 - (n+1)\text{RH}^{n} + n\text{RH}^{n+1}}{1 + (c+1)\text{RH} - c\text{RH}^{n+1}}\right)$$
(13)

- ¹⁰ where KM is the integrated K-M value of adsorbed water in the region of 3700– 2500 cm^{-1} , KM_{ML} is the integrated K-M value of adsorbed water at one monolayer, *c* is a temperature-dependent constant, *n* is the maximum number of layers of adsorbed water, and RH is the relative humidity. The adsorption isotherm curves of water on α -Al₂O₃ and MgO at 300 K are shown in Fig. 9.
- ¹⁵ One monolayer of water adsorbed on α -Al₂O₃ and MgO occurred at a RH of 0.37 and 0.30, respectively (Fig. 9). These values are higher than those reported in the literature (Goodman et al., 2001). The difference might be due to the sample origins or to the surface cleanliness of the samples. As discussion above, when water vapor pressure exceeds the corresponding RH_{ML}, multilayer adsorption of water should take place on mineral oxides, and the surface -OH should be consumed completely.
- Therefore, uptake of OCS should not be observed at high relative humidity. However, as shown in Figs. 5b and 6b, when RH exceeded the corresponding RH_{ML} , the uptake coefficients of OCS on the samples remained higher than that measured in the background experiment. In particular, the average value of γ_{obs} on MgO in the RH region
- ²⁵ between 0.47 and 0.67 was 29 times as that of the background value. This indicates that the liquid membrane of water on α -Al₂O₃ and MgO might also contribute to the heterogeneous hydrolysis of OCS. In our previous work, we found that the heteroge-





neous reaction of OCS on the surface of mineral oxides is related to the basicity of the oxide (Liu et al., 2007b). The base catalytic hydrolysis of OCS in aqueous solutions has also been widely investigated (Amararene and Bouallou, 2004). It is well known that the basicity of MgO is higher than that of α -Al₂O₃. The pH value of slurry for 1.0 g

⁵ of MgO in 20.0 mL water was measured to be 10.7, while that for α -Al₂O₃ was 9.1. Therefore, the observed uptake coefficients of OCS on MgO at high RH were much higher than that on α -Al₂O₃. At the typical relative humidity, water could not wet the oxides (Foster et al., 2002). Therefore, the surface basicity of the liquid membrane formed on mineral dust would be higher than the value measured in slurry. Conse-10 quently, it is reasonable to deduce that the liquid membrane formed on atmospheric particulate matter, especially the basic components, should be the primary contributor to heterogeneous reactions of OCS in the atmosphere.

5 Conclusions and atmospheric implications

In this work, the heterogeneous reactions of OCS on the surface of α -Al₂O₃ and MgO were studied using KCMS, DRIFTS, and TPR. We found that hydrolysis of OCS lead-15 ing to the formation of H₂S and CO₂ could occur on the surface of both α -Al₂O₃ and MgO at ambient temperature. The reaction kinetics was influenced significantly by adsorbed water on the surface of α -Al₂O₃ and MgO. At low water vapor pressure (<6.8×10⁻⁶ Torr), the uptake coefficients of OCS on MgO increased with increases in water vapor pressure in the feed gas due to the formation of surface hydroxyl groups; 20 these surface hydroxyl groups were confirmed to be the sites for the heterogeneous reaction of OCS on the surface of mineral oxides. However, at high coverage, adsorbed water on the surface hydroxyl groups led to a decrease in the uptake coefficients. For α -Al₂O₃, adsorbed water suppressed the heterogeneous hydrolysis of OCS at both low and high water vapor pressures due to the competitive adsorption of H₂O and 25 OCS on surface hydroxyl groups. At high relative humidity, the decrease in the uptake coefficients was in proportion to the amount of surface hydroxyl groups consumed by

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adsorbed water on α -Al₂O₃ and MgO. The uptake coefficients of OCS on MgO at high relative humidity remained higher than that of both α -Al₂O₃ and the background due to the contribution of basic liquid membrane of water on MgO.

- Hydrolysis is regarded as the most important universal reaction in the atmospheric (Ravishankara, 1997), and much work has been done regarding the hydrolysis of gaseous species on ice surfaces (Abbatt, 2003). Mineral dust has also been found to be an important constituent of atmospheric particulate matter (Dentener et al., 1996). The adsorption and oxidation of inorganic compounds including SO₂, NO_x, O₃, and HNO₃ on the surface of mineral dust have been well investigated (Usher et al., 2003a).
- However, under typical atmospheric conditions (298 K and 0.50–0.60 RH), about 3– 4 monolayers of water adsorb on mineral dust (Eng et al., 2000). This membrane of liquid formed on the surface of mineral dust imparts particulate matter with a capacity to heterogeneously hydrolyze trace gases. These studies mentioned above demonstrate that heterogeneous oxidation on mineral oxides may be a new sink of OCS in the tro-
- posphere. Here we found that mineral dust catalyzes the heterogeneous hydrolysis of OCS, which may be a tropospheric sink for OCS. However, water adsorbed on mineral dust appeared to restrict the heterogeneous hydrolysis of OCS at a typical relative humidity in the troposphere. Nevertheless, the hydrolysis of OCS on mineral dust should not be ignored even if the RH is higher than RH_{ML}. Liquid membranes of high basic-20 ity that formed on mineral dust are likely primary contributors to the heterogeneous
- hydrolysis of OCS and sinks for OCS in the troposphere.

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Species	Absorbance bands	Oxides	Ref.
OCS(g)	2071, 2052	α -Al ₂ O ₃ and MgO	Tubergen et al. (2000)
$CO_2(g)$	2363, 2338	α -Al ₂ O ₃ and MgO	He et al. (2005)
-OH(a)	3737 3755	α-Al ₂ O ₃ MgO	Peri and Hannan. (1960)
$H_2CO_3(a)$	1683 1681	α-Al₂O₃ MgO	Al-Hosney et al. (2004)
$HCO_3^-(a)$	3623, 1635 3618, 1659, 1409, 1225	α-Al₂O₃ MgO	Lavalley (1996)
CO ₃ ²⁻ (a)	1534 1584, 1545	α-Al ₂ O ₃ MgO	Baltrusaitis et al. (2006)
-SH(a)	2578	MgO	Datta and Cavell (1985)
SO ₂ (a)	1333	MgO	Ullerstam et al. (2003)
$HSCO_2^-(a)$	1578 1273	α-Al ₂ O ₃ MgO	He et al. (2005) Liu et al. (2007a)
SO ₄ ²⁻ (a)	1384 1138	α-Al₂O₃ MgO	Li et al. (2006)
SO ₃ ²⁻ /HSO ₃ ⁻ (a)	1084, 1030, 950	MgO	

Table 1. Assignment of the absorbance bands shown in Fig. 2.

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Fig. 1. Typical uptake profiles of OCS and water on α -Al₂O₃ and MgO at 300 K. (a) and (b) for OCS; (c) and (d) for water measured by Knudsen cell – mass spectrometry. The partial pressures of OCS and water in the Knudsen cell reactor were 5.3×10^{-6} and 5.8×10^{-6} Torr, respectively.







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Fig. 3. Gaseous products for the heterogeneous reactions of OCS on the surface of α -Al₂O₃ and MgO measured by temperature programmed reaction. **(a)** 1000 ppmv of OCS balanced with simulated air passing through 0.5 g MgO at 300 K; **(b–d)** temperature-programmed reaction of 1000 ppmv of OCS balanced with simulated air on back ground, α -Al₂O₃ and MgO, respectively. The temperature rate was 20 K min⁻¹.



Fig. 4. Effect of water on heterogeneous reactions of OCS at low water vapor pressure. (a) on α -Al₂O₃; (b) on MgO measured by Knudsen cell – mass spectrometry. The average partial pressure of OCS in the Knudsen cell reactor was kept at $5.3\pm0.3\times10^{-6}$ Torr, and that of water vapor was 2.5×10^{-6} - 6.8×10^{-6} Torr.

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Fig. 6. Effect of water on the heterogeneous reaction of OCS on MgO at high relative humidity calculated from the data of DRIFTS. The initial concentration of OCS in the feed gas was kept at 1000 ppmv.

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(b) 3418 3230 0.6 (a) 3417 3219 grated area a-Al₂O₃ 0-4 MgO Integrated area 3780-3720 cm 3781-3691cm 1637 0.6 3734 3755 $1630^{0.0}$ 0.4 0.6 0.8 RH Absorbance 2:0 Absorbance 5:0 Absorb 0.0 0.2 0.4 0.6 0.8 1.0 0.95 Absorbance RH 0.95 0.4 0.2 0.0 RH 0.05 0.0 RH 0.05 3500 2500 2000 3000 1500 3000 2500 2000 3500 1500 1000 Wavenumber (cm⁻¹) Wavenumber (cm⁻¹)



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Integrated area of surface hydroxyl consumed by adsorbed water

Fig. 8. Correlation between the observed uptake coefficients and amount of surface hydroxyl (*A*) consumed by water at different RH in the region of 0.07–0.27.







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