

Changes to manuscript ms-nr acp-2015-903

Modelling and Measurements of Urban Aerosol Processes on the Neighbourhood Scale in Rotterdam, Oslo and Helsinki

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Dear Prof Rob MacKenzie,

We highly appreciate the reviews of our manuscript ms-nr acp-2015-903 that we received from Prof Roy M. Harrison and two anonymous referees. We have replied to their comments in the Open Discussion. We have addressed all specific comments in the revised manuscript as will be described below. We carefully considered the concerns of the two anonymous referees and the comments of Prof Harrison and his co-workers in our revision of the manuscript.

Below follows: (1) the point-by-point replies to the three reviewers, (2) a list of relevant changes in the manuscript, and (3) the revised manuscript with changes highlighted.

Our responses to reviewers have been written in [blue font](#).

Figure, table, section, and page numbers in the replies below refer to the revised manuscript which has been sent along with this response.

Referee #1

1. Line 15 of the Abstract. "It was not necessary to model the nucleation of the gas-phase vapors..." This sentence created immediate concern (suggestion nucleation had been neglected) until I read further into the manuscript to understand fully. I suggest adding a short sentence after this to say why, i.e. post tail-pipe emissions were considered.

The sentence will be changed to: "By choosing concentrations and particle size distributions at roadside as starting point of the computations, nucleation of gas-phase vapors from the exhaust has been regarded as post tail-pipe emission, avoiding the need to include nucleation in the process analysis."

2. Line 22 of pg 35168. "The traffic volume at Bentinckplein, which is a street canyon..." The measurement PN in Street canyons is affected by the circulation of air within the canyon whether it passes across the traffic before passing over the sampler or whether it passes over the sampler first before the traffic. This is dependent on the wind direction across the canyon. Was this taken into account?

When modelling the hourly contribution from road traffic emissions to the sampler location in Rotterdam at the Bentinck street location, the hourly average wind direction was indeed taken into account.

The following sentence will be added on p. 35168: "Hourly averaged wind direction was used to select campaign data that was directly influenced by the traffic emissions in the street."

3. Line 21 of pg 35171 "The mean traffic-related size..." Three distinct modes are described with mean diameters 17, 85 and 250nm. Are these peak fitted modes and if so please specify how you fitted them.

Three-modal fit has been done with the MAFOR model; the procedure is explained in section 2.2 of the manuscript. This information will be added.

4. Lines 1-10 of pg 35184. In the conclusions the inaccuracies of the simplified treatment of the coagulation process was discussed, which did not account for the coagulation between size categories. How does the accuracy improve as the number of size categories is increased, eg X2 and X4?

We note here that the discussion of the accuracy of the derived simplified parameterizations of dry deposition and coagulation involving three size categories of PNC only elaborates on uncertainties with respect to the solution obtained from the fully size-resolved MAFOR model with 120 size sections. Uncertainties due to the neglect of fractal geometry and van der Waals forces as well as uncertainties due to inaccurate measurement of dry deposition velocities, as pointed out by Referee #2, are not included in the error of the simplified parameterization. The accuracy of the developed parameterization improves when the number of size categories is increased since the error due to neglecting intra-modal coagulation is reduced. For a parameterization with six categories of PNC the deviation to the reference solution with 120

size sections is only up to 5 %. Further increasing the number of size categories is expected to give even better accuracy however is not considered to be practical for the implementation in urban dispersion models.

The following sentence will be added to section 3.7 "The recommended simplified parameterizations of aerosol processes" in the revised manuscript: "Increasing the number of PNC size categories is expected to reduce the error due to neglecting coagulation between size categories. A parameterization with six PNC categories resulted in a deviation to the reference solution by only up to 5 % (Table S3). In addition the parameterization is uncertain due to assumptions about particle shape, neglecting van der Waals forces as well as inaccurate measured dry deposition velocities. It is however not affected by the specific treatment of dilution in the idealized scenarios because the simplified PNC parameterization was derived with only one aerosol process activated."

A table with obtained with required data for implementation of the 6-category parameterization will be included in the Supplement (new Table S3).

5. Table 3 pg35193 The average PN concentration for Helsinki LIPIKA Case 1 (186100 cm⁻³) is much higher than the other sites, what is the explanation for this?

We thank Referee #1 for finding this mistake. The high value of 186 100 particle cm⁻³ was measured with the mobile laboratory "Sniffer", while driving on Itäväylä, in 9 m distance from the center line of the two-direction highway, and not as erroneously written in Table 3, at 65 m distance from roadside. The measured value in 9 m distance from the roadside was 129 600 particles cm⁻³. This is the correct value, which has also been used in the calculations. Table 3 and Figure S1 will be corrected accordingly.

6. Figure 4A. The size development of the size spectra for Oslo Winter UFP - Oslo shows the nucleation mode being diluted. It would be useful to have had a third intermediate size distribution collected half way between the roadside and background to fit the model through. Is there a possibility that there could be nanoparticle loss by evaporation, rather than coagulation processes? (ref M. Dall'Osto et al Atmos. Chem. Phys., 11, 6623-6637, 2011).

We agree that intermediate sampling positions in 100-1000 m distance between the roadside and the background site would have been of great value to determine possible evaporation of exhaust particles.

We give a detailed evaluation on the possibility of loss by evaporation in our response to the Comment by Prof Harrison and co-workers.

The title of section 3.4 will be changed from "Effect of condensation of n-alkanes" to "Effect of condensation and evaporation of organic compounds".

The following text on findings from Dall'Osto et al. (2011) and Harrison et al. (2016) will be added in section 3.4:

"Model simulations of the idealized scenario suggest that evaporation could be an important process, altering the particle size distribution in urban micro-environments, if the semi-volatile vapor and also the nanoparticles forming post-emission were assumed to have the same or higher volatility as the n-alkane C22. Dall'Osto et al. (2011) analyzed observations of particle size distributions from London and reported a reduction in the size of nucleation mode particles during advection from a major highway into the cleaner environment of a park, indicating evaporative loss of semi-volatile constituents during travel times of around 5 min. Harrison et al. (2016), for the same location, found most rapid evaporation to occur at higher wind speeds, associated with shorter travel times, but cleaner air."

Prof Harrison and co-workers

1. We have a basic conceptual disagreement with the way in which condensation/evaporation processes have been considered in this work and would also like to highlight the very confusing information provided by the authors in relation to this aspect. To set the context, one needs first to consider the tailpipe to kerbside dilution process. The raw exhaust gases contain predominantly graphitic soot-carbon particles and the vapour of hydrocarbons deriving from unburnt fuel and lubricating oil. During the immediate dilution and cooling of the exhaust gases, semi-volatile hydrocarbons become supersaturated and condense which causes the formation of the nucleation mode seen in roadside air (Charron and Harrison, 2003) as well some condensational growth of the larger particles with a solid carbon core which typically exhibit a mode at around 70 nm in roadside air (Harrison et al., 2011 and many other published studies). Our conceptual view of this system is that because of the large surface area available for condensation, the semi-volatile organic compounds reach an equilibrium between vapour and the condensed phase. Consequently, we see no reason for further condensational growth by hydrocarbon condensation unless there is another source of vapour or a reduction in ambient temperature causing further supersaturation.

The concept regarding condensation and evaporation between roadside and ambient environment applied in our study is based on the work of Zhang and Wexler (Zhang and Wexler, 2004; Zhang et al. 2004).

Hundreds of condensable organic vapors could form in vehicle exhaust with varying concentrations. Determination of their physicochemical parameters such as bulk-phase vapor pressure, molar volume and surface tension, required for modelling, poses an enormous challenge. Due to the lack of composition measurements at roadside, we had to assume a lumped, average composition for the condensable material in the gas-phase. In the applied approach, the effective behavior of condensable organic vapors with respect to changes of the

particle number concentration and the particle size distribution was modeled by introducing two different volatility classes: C22 representing semi-volatile vapors and C28 representing low-volatile vapors. This has been mentioned in section 2.1, page 35162, lines 9-11.

For the included roadside locations and campaigns, concentration of n-alkanes and other condensable organic vapors have not been measured and therefore it is not known whether they were in equilibrium with the (bulk) particle phase or not. Such measurements are still rare and not complete regarding the full volatility spectrum of condensable organic vapors. Based on theoretical considerations, Zhang and Wexler (2004) concluded that during the second dilution stage, between roadside and a few hundred meters distant from the road, particles can still grow by condensation, although with decreasing growth rates when the air parcel moves away from the road.

We have assumed that gas-phase organic compounds at roadside are in excess, even after the first dilution stage between tailpipe and roadside, potentially enabling further growth in accordance with the study by Zhang et al. (2004) that shows growth of sub-6nm particles until 30-90 m downwind. It was also assumed that the roadside concentration of condensable organic vapors is several orders higher than their concentration in the urban background. In fact, the background concentration of C22 and C28 had been set to zero in our study, forcing maximum dilution of the condensing vapors.

The following text will be added in section 2.1:

“The concept regarding condensation and evaporation between roadside and ambient environment applied in this study is based on the work of Zhang and Wexler (Zhang and Wexler, 2004; Zhang et al. 2004). The effective behavior of condensable organic vapors from vehicular exhaust with respect to changes of the particle number concentration and the particle size distribution was modeled by introducing two different volatility classes: the n-alkane $C_{22}H_{46}$ (abbreviated as C22) representing semi-volatile vapors and the n-alkane $C_{28}H_{58}$ (abbreviated as C28) representing low-volatile vapors.”

Subsequent to section 2.2, the term “n-alkanes”, meaning representatives of two volatility classes, will be replaced by “condensable organic vapors”.

2. In models such as that used by Karl et al., the determinant of whether nucleation mode particles shrink by evaporation or grow by condensation is the ambient vapour pressure of the semi-volatile hydrocarbons. In this context, the selection of a concentration by Karl et al. appears to be rather superficial. This is explained in their Supplementary Information which summarises total VOC concentrations (excluding VOC with less than four carbon atoms and benzene) measured in London, Copenhagen, Hamburg and Helsinki, but does not consider measured concentrations of the specific C22 and C28 n-alkanes used in the calculation. Additionally, the Supplementary Information is extremely confusing in that it uses the statement “assuming that 5-10% of the VOCs react to form condensable gas-phase products, a concentration range of 0.4-4 ppbv is obtained using the available VOC measurements”. This leaves doubt as to whether the

condensation process is assumed to involve the VOCs themselves or their oxidation products.

The applied aerosol dynamics model makes no assumption regarding equilibrium. If the gas-phase concentration of an organic compound is below the saturation concentration, the compound will evaporate from the particles, if it is above the saturation concentration, the compound will condense to the particles. During the road-to-ambient process, some compounds may continue condensing, while others begin evaporating, depending on the relative magnitude of their vapor pressures. In addition, the vapor pressure of the model compounds C22 and C28 is further modified by their molar fraction in the particle phase, according to Raoult's law, and by their molar volume and surface tension according to the Kelvin effect. This in particular has an impact on the growth or shrinkage of particles in the nucleation mode.

We agree that the estimation of 5-10 % conversion of VOC into condensable organic compounds is not relevant for the roadside, since the figure refers to the oxidative conversion yield of reactive hydrocarbons, such as toluene and alkenes. At roadside, the "fast" photochemical equilibrium will be dominating while the photochemical reactivity of VOC is generally reduced.

The estimation of the 5-10% conversion was removed from the Supplementary Information.

The following text will be added to section 2.2 to better explain the applied concept regarding condensation and evaporation:

"The applied aerosol dynamics model makes no assumption regarding the equilibrium between organic vapor and the condensed phase at the roadside. If the gas-phase concentration of an organic compound is below the saturation concentration, the compound will evaporate from the particles, if it is above the saturation concentration, the compound will condense to the particles. During the road-to-ambient process, some compounds may continue condensing, while others begin evaporating, depending on the relative magnitude of their vapor pressures. In addition, the vapor pressure of the model compounds C22 and C28 is further modified by their molar fraction in the particle phase, according to Raoult's law, and by their molar volume and surface tension according to the Kelvin effect."

3. The abstract of the paper refers to "condensation and evaporation of organic vapours emitted by vehicles" which suggests that it is the n-alkanes themselves, in which case it is wholly unclear what the 5-10% figure refers to. This leads the authors somewhat mysteriously to use initial concentrations of 0.25 ppb of C22 and 0.25 ppb of C28 for the reference case but they then conduct sensitivity tests in the range 1-4 ppb of each compound. There seems to be no justification whatever for these numbers. In the UK atmosphere, we have measured concentrations of vapour phase n-C22H46 of 3.97 ng m⁻³ (0.31 ppt) and n-C28H58 of 1.03 ng m⁻³ (0.06 ppt) at a roadside site (Harrad et al., 2003).

C22 and C28 are thought to be representative of the non-oxidized condensable material in the gas-phase of the vehicle exhaust. It has already been clarified in the manuscript that the concentrations do not refer to the individual chemical species, but are intended to represent the total concentration of two volatility classes. It was decided to keep the initial concentrations at 0.25 ppb of C22 and 0.25 ppb of C28 (i.e. in total 0.5 ppb), potentially allowing for continued growth downwind the road. This is not unreasonable since for instance the particle size distribution from the SAPPHIRE Case I campaign shows a clear increase of the nucleation mode diameter between roadside measurement and background measurement. It is noted that Pohjola et al. (2007) obtained best fit between modeled and measured particle size distribution on a distance scale of 125 m near a major road in Helsinki when using roadside concentrations of one condensable organic vapor of the order of 10^{10} molecules cm^{-3} (ca. 0.4 ppb).

Mandalakis et al. (2002) reported a total n-alkane (C14 - C33) concentration of 50.43 ng m^{-3} in the vapor phase and of 38.65 ng m^{-3} in the particulate phase, from measurements in the urban center of Athens (Greece). C14 - C23 n-alkanes were mainly in the vapor phase while C25 - C33 n-alkanes were mainly in the particulate phase; C24 was equally present in both phases. Summing up vapor concentrations for C14 - C23 and particulate phase concentrations for C25 - C33 and the phase averaged concentration for C24 gave a concentration of total condensable n-alkanes of 73.5 ng m^{-3} , corresponding to 5.1 ppt when using the averaged molecular weight of C22 and C28. Similar total n-alkane concentrations were reported by Harrad et al. (2003) for an urban traffic site (Birmingham, UK), by Doskey and Andren (1986) for a rural site (North Wisconsin, WI, USA), and by Pietrogrande et al. (2011) for a suburban site (particulate phase only, Augsburg, Germany). Total n-alkane concentrations were several times higher at an urban industrial site (Prato, Italy) in a study by Cincinelli et al. (2007). Total n-alkane concentrations were more than one order of magnitude higher at an urban site in China (Bi et al., 2002). Although a concentration of 5 ppt of condensable n-alkanes seems to be typical for the urban environment, higher concentrations may occur. Other condensable organic compounds such as PAH, n-alkanols, and dicarboxylic acids are also emitted from vehicles and may contribute to the total concentration of condensable organic vapors at the roadside, represented by C22 and C28 in our study.

The sensitivity tests in the range 1-4 ppb (for the sum of C22 and C28, not for each compound as suggested by the Prof Harrison) were now replaced by a test series with smaller concentrations for the sum of C22 and C28, stepwise decreasing by one order of magnitude between 500 ppt (i.e. 0.5 ppb, reference case) and 5 ppt, closer to the reported measurements of the sum of n-alkanes available for condensation. Since evaporation depends on the volatility of the nanoparticles in the exhaust post-emission, the OC fractions in the modeled nucleation mode were changed to 100% C22 in an additional test. Results from the new tests on condensation and evaporation were added to section 3.4. Two new figures (Figures S3 and S4) showing the particle number and mass size distributions in 240 m distance from roadside for Helsinki LIPIKA and for UFP-Oslo Winter with different concentrations of condensable organic vapors will be included in the Supplement.

The following text will be added to section 2.2:

“For the included campaigns, gas-phase concentration of n-alkanes and other condensable organic compounds have not been measured at the roadside locations. Measurements of n-alkane vapor concentrations in urban environments indicate typical concentrations of 5 ppt for the sum of the n-alkanes, but higher concentrations may occur (for more details see section S2 in the Supplement). Pohjola et al. (2007) obtained best fit between modeled and measured particle size distribution on a distance scale of 125 m near a major road in Helsinki when using roadside concentrations of one condensable organic vapor of the order of 10^{10} molecules cm^{-3} (ca. 0.4 ppb). Based on this, initial concentrations of 0.25 ppb C22 and 0.25 ppb C28 were used in the reference case (all campaigns and dispersion conditions). The background concentration of C22 and C28 was set to zero, forcing maximum dilution of the condensable organic vapors during travel of the air parcel away from the roadside.”

The above description of reported n-alkane measurements will be included in Section S2 of the Supplementary Information.

4. This leaves open the question of why Karl et al. achieved a better fit to the measured data for Oslo during low dispersion conditions when assuming condensational growth, and why the data from the other sites do not imply an evaporation process during transport from roadside. In our view, the most likely explanation is that the experimental studies used comparisons between roadside and urban background sites and that further emissions of vehicle pollutants occurred between those sites which are not taken account of in the modelling approach used. This would serve to maintain the concentrations of vapour, hence suppressing the evaporation process. Alternatively, oxidised VOC (or other compounds) provided a source of condensable material.

We do not exclude alternative explanations for the diameter increase of nucleation mode particles between roadside and background measurements during the Oslo UFP Winter campaign. Vehicle emissions models suggest that in cold climates the majority of volatile organic compounds (VOC) emitted by vehicles occur during engine cold starts. Vehicle emissions of hydrocarbons from gasoline vehicles during cold start might be up to 35 times higher at -20°C than at room temperature (Weilenmann et al., 2009). It is possible that oxidation of extra-emitted VOC from gasoline vehicles provided an additional source of condensable material during the travel between roadside and the neighborhood.

The alternative explanations given by Harrison and co-workers will be included in the discussion of the Oslo winter case in section 3.4 and in the new section 3.6 “Uncertainties of the aerosol treatment in the idealized scenario”.

Weilenmann, M., Favez, J.-Y., and Alvarez, R.: Cold-start emissions of modern passenger cars at different low ambient temperatures and their evolution over vehicle legislation categories, *Atmos. Environ.*, 43, 2419-2429, 2009.

5. In other words, $H_{m,0}$ indicates the initial volume of the plume and H_m indicates the final volume of the plume. In consequence, the ratio, $H_{m,0}/H_m$, implies the volume fraction taken by the initial plume at the final stage. At the travel time of 30 min (e.g. for the

results shown in Table 4), the plume is overwhelmingly taken by the background air (99.86% for 'efficient dispersion', 99.05% for 'moderate dispersion', and 88.6% for 'inefficient dispersion' calculated from Equation (1)) – see table below. Even for the travel time of 10 min, these percentages are already very high (99.6%, 98.4%, and 85.8% for the three weather conditions, respectively).

We thank Prof Harrison and co-workers for compiling the ratio $H_{m,0}/H_m$ for 10 min, 20 min and 30 min in form of a table in their short comment.

Exponential decay observed for the total PN concentration during dispersion of the particles between 1 m from road to several hundred meters from road, is dominated by the atmospheric dilution. Lähde et al. (2014) demonstrated that an exponential dilution function, $c(x) = B + D \exp(kx)$ can be applied to various PN roadside dispersion studies. Although relative concentrations of the background (B) and of the emission source (D) differed, the decay coefficient k was similar for all sites. This confirms the result of our study, that for efficient dispersion conditions between roadside and neighborhood scale, total PN can be modelled as passive tracer.

Lähde, T., Niemi, J. V., Kousa, A., Rönkkö, T., Karjalainen, P., Keskinen, J., Frey, A., Hillamo, R., and Pirjola, L.: Mobile particle and NO_x emission characterization at Helsinki downtown: comparison of different traffic flow areas, *Aerosol and Air Quality Research*, 14, 1372-1382, doi: 10.4209/aaqr.2013.10.0311, 2014.

6. It is entirely unclear whether the model collects further emissions during the travel; we assume it does not (otherwise, a specification of emission rate and composition and particle size distribution etc. should be described). These effectively lead to an approximate modelling of aerosol evolution of the background air. The results shown in Table 4, for example, have little influence from the initial traffic emissions.

No additional emissions are collected during transport from roadside to ambient in this idealized scenario. The background concentration of particles has an essential influence on the dilution time scale. The scenario calculations are constrained by the measured background particle concentration and size distribution. If there had been other sources of ultrafine particles between the roadside and the urban background, these are integrated in the shape of the particle size distribution of the urban background, which is imposed on the calculated aerosol evolution of the model.

Table 4 is intended to illustrate the relative importance of the different aerosol dynamics processes, in changing the total particle number concentration between roadside and the neighborhood scale, assuming no additional emissions and a homogeneous underlying surface.

The obtained percentage changes of PN due to aerosol dynamics (coagulation and dry deposition) are comparable to those found previously with urban dispersion models.

The following sentence will be added in section 2.2.:

“No additional emissions of particles or vapors are collected during transport from roadside to ambient in this idealized scenario.”

7. In addition, it is not entirely clear how to derive the initial plume height, $H_{m,0}$, which is not described as part of fitting method (only for a and b). It is odd to have higher values for more stable conditions as shown in Table 1 and no justification is given for it. This is important for an examination of percentages of air from the initial emitted plume and from the entrained background air as discussed above.

Wind speed and direction are important in determining the dispersion of ultrafine particles near busy roads. Zhu et al. (2002) observed a linear dependence of the total particle number concentration on wind speeds, 30 m downwind of a motorway in Los Angeles. With increasing wind speed the atmospheric dilution effect will be stronger. Therefore wind speed was included to characterize the dispersion cases of our study. Wind speed U , perpendicular to the road, was 1.0 m/s, 3.0 m/s, and 4.0 m/s, respectively, for the inefficient dispersion, moderate dispersion, and efficient dispersion cases; indicated in Table 1 of the manuscript.

The initial stage of the exhaust plume was described with the simple plume dispersion model by Vignati et al. (1999). This was done independently before the actual scenario calculation. We apologize that the derivation of $H_{m,0}$ has not been mentioned in the manuscript.

The expression by Vignati et al. (1999) for the evolution of the plume cross section was applied.

Where S is the cross sectional area of the plume or, in more statistically oriented way, it can be interpreted as being proportional to the variance of the Gaussian plume distribution. S_0 is the size of the plume at the exhaust pipe (assumed to be equal to the cross-sectional area of the exhaust pipe, here using a radius of 0.020 m), $\sigma_w(0)$ is the initial entrainment velocity at $t = 0$ and u_0 is the initial exhaust gas velocity. The proportionality constant α is given a value of 0.1, which corresponds to typical levels of mechanically induced turbulence (Berkowicz et al., 1997). For $\sigma_w(0)$ a value of 0.25 m s^{-1} was adopted (Fig. 6 in Kastner-Klein et al., 2000), typical for traffic on working days between 8 a.m. and 7 p.m. in situations where traffic-induced turbulence dominates. For the initial exhaust gas velocity u_0 a value of 0.23 m s^{-1} typical for light-duty vehicles was taken (Kurkela et al., 1994). Further, t is the time from the release, here expressed as $t = x/U$. A fixed distance from the release point of $x_{st} = 9 \text{ m}$ was chosen for the PN measurement, resulting in an arrival time t_{st} at the measurement location which differs for different wind speeds. Solving the above expression for the initial plume height at roadside, assuming circular plume cross-section, gives $H_{m,0}$.

For the wind speeds 1.0 m/s, 3.0 m/s and 4.0 m/s we obtained an initial plume height, $H_{m,0}$, of 2.6 m, 0.9 m, and 0.7 m at the roadside ($H_{m,0}$ values are now given with one significant decimal).

Description will be added as new section S1 in the Supplementary Materials.

Vignati, E., Berkowicz, R., Palmgren, F., Lyck, E., and Hummelshøj, P.: Transformations of size distributions of emitted particles in streets, *Science of the Total Environment*, 235, 37-49, 1999.

Berkowicz, R., Hertel, O., Sørensen, N. N., and Michelsen J. A.: Modelling air pollution from traffic in urban areas. In: Perkins, R. J., Belcher, S. E., editors, Flow and dispersion through groups of obstacles, Oxford: Clarendon Press, 121-141, 1997.

Kastner-Klein, P., Berkowicz, R., and Plate, E. J.: Modelling of vehicle induced turbulence in air pollution studies for streets, Int. Journal of Environment and Pollution, 14(1-6), 496-507, doi: 10.1504/IJEP.2000.000573, 2000.

Kurkela, J., Valmari, T., and Kauppinen, E.: The 14.9.-15.9.1994 particulate phase measurements of a bus diesel engine, VTT Aerosol Research Group Publications, Espoo, 18pp. (in Finnish), 1994.

Referee #2

1. Several fundamental assumptions seem to ignore processes that could make major qualitative differences in the results.

1.a. Given the relatively large contribution of diesels to the vehicle fleets, and in port cities such as Rotterdam, marine vessels their attendant fleet of lorries, the contribution from fractal agglomerates would seem to be much too high to ignore. Ignoring these particles and their very different behavior appears to be capable of introducing a significant error. The distribution data seem to imply significant contributions from diesel particles for some sites (such as Rotterdam) which have few very small particles. At the very least this the magnitude of the potential error from this omission should be estimated. Possibly differences between the sites could be used to better constrain MAFOR.

Model calculations for the idealized scenario assumed that all particles are spherical. Treatment of aggregates of soot as fractal particles increases the coagulation rate. The effect of fractal geometry on coagulation will be taken into account in the revised manuscript by considering the effect on radius, diffusion coefficient and the Knudsen number in the Brownian collision kernel, following the approach described by Jacobson and Seinfeld (2004).

Jacobson, M. Z. and Seinfeld, J. H.: Evolution of nanoparticle size and mixing state near the point of emission, Atmos. Environ., 38, 1839-1850, 2004.

For the treatment of fractal geometry of soot particles in MAFOR the coagulation kernel was modified by assuming that the collision radius is equal to the fractal (outer) radius.

Where $n_s = v_i/v_s$ is the number of primary spherules in the soot aggregate, v_i is the volume of the aggregate, treated as if it were spherical, r_s is the radius of spherules and v_s is the volume of

a spherule that makes up the aggregate, and D_f is the fractal dimension. Soot particle density was corrected as explained in Lemmetty et al. (2008).

Lemmetty, M., Rönkkö, T., Virtanen, A., Keskinen, J., and Pirjola, L.: The effect of sulphur in diesel exhaust aerosol: Models compared with measurements, *Aerosol Sci. Technol.*, 42, 916-929, 2008.

The effect of fractal geometry of soot aggregates can only be of significance for those campaigns or locations where coagulation has been identified as an important process. Rotterdam showed the highest contribution of coagulation to PN losses under moderate dispersion conditions (see Table 4 of the original manuscript), but unfortunately particles with $D_p < 10$ nm have not been measured in that campaign. Due to the dominant contribution of dilution to PN losses at all sites, and the competition between coagulation and dry deposition with respect to the loss of nanoparticles ($D_p < 25$ nm), which made up the largest PN fraction at roadside (except at Rotterdam), it is not possible to better constrain the coagulation process in the model.

The description of the treatment of fractal geometry in MAFOR will be added in the new section 3.5 “Effect of fractal geometry of soot particles and van der Waals forces”.

1.b. Ignoring van der Waals forces leads to underestimation of coagulation rates that is of order a factor of two for the smaller particles (10s of nm). This will make a very substantial difference in the outcome of the calculations, and one that cannot be ignored.

The effect of van der Waals forces on coagulation is usually treated in combination with viscous forces (Jacobson and Seinfeld, 2004), which both affect primarily the small particles. Van der Waals forces are weak dipole-dipole attractions in uncharged, nonpolar molecules caused by random fluctuations in the electron cloud. Viscous forces are fluid mechanical interactions arising from the fact that velocity gradients induced by a particle approaching another particle in a viscous medium affect the motion of the other particle. Viscous forces retard the rate of van der Waals force enhancement in the continuum regime. It has been shown that van der Waals forces can enhance the coagulation rate of small particles by up to a factor of five (Jacobson and Seinfeld, 2004). However the degree of enhancement depends on the Hamaker constant A which is specific for the van der Waals properties of each substance. Jacobson and Seinfeld (2004) used a value of $A/k_B T = 200$ (k_B is the Boltzmann constant and T is the air temperature), which gave plausible enhancement for the coagulation of soot particles. However, for some values of the Hamaker constant there is an overall retardation of the coagulation rate in the continuum regime due to viscous forces. In the kinetic regime, coagulation is always enhanced due to the absence of viscous forces. The uncertainty related to the Hamaker constant was the reason for not including the effect of van der Waals forces in the original manuscript.

A simplified treatment of the van der Waals enhancement combined with retardation by viscous forces was considered sufficient to evaluate the possible uncertainty introduced into

our study by neglecting the two interactions. A correction factor $V_{E,ij}$ due to van der Waals and viscous forces was applied to the Brownian collision kernel in the MAFOR model.

Based on Fig. 3 in Jacobson and Seinfeld (2004), three regimes of enhancement were distinguished in the implementation, depending on the value of the particle pair Knudsen number, Kn_p , of two colliding particles with radius r_i and r_j :

Where λ_p is the effective mean free path of an individual particle.

The three cases for the correction factor are approximated.

Clearly, $V_{E,ij}$ for values of the particle pair Knudsen number greater than 1.0 depends on the radius ratio of the two colliding particles and can range from 1.0 to 5.0 for ratios between 50 and 1, when $A/k_B T = 200$ is used. A value (enhancement factor) of 3.0 was chosen which corresponds to a radius ratio of about 5, e.g. describing the collision of a 5 nm-particle with a 25 nm-particle, relevant for the studied size distributions at roadside. The applied correction value is higher than the factor of two suggested by the reviewer.

A brief description of the treatment of van der Waals forces and viscous interactions in MAFOR will be added in the new section 3.5 “Effect of fractal geometry of soot particles and van der Waals forces”. A detailed description is given in the new Supplement section S3 (“Modification of the Brownian coagulation kernel to approximate van der Waals forces and viscous interactions”).

1.c The parameterizations and resulting rate estimates for dry deposition in the literature span more than an order of magnitude, and the calculations in this manuscript appear to be toward the high end. The manuscript would be much more useful and enlightening if it were to address this large source of uncertainty as well. Possibly the data again could be used to constrain dry deposition parameterization schemes. But at least this needs to be addressed directly as a source of uncertainty.

Measurements of dry deposition velocities of particles for one particular surface type generally vary by approximately one order of magnitude for a given particle size range of a half logarithmic decade (e.g. for different grassland and forest types; Fig. 12 in Petroff et al., 2008). The typical mean measured deposition velocity values are within $0.1\text{--}1.0\text{ cm s}^{-1}$ for vegetated surfaces in the 0.1 and $1.0\text{ }\mu\text{m}$ particle size range (Zhang et al., 2001). Average dry deposition velocities were in the range of $0.2\text{--}0.9\text{ cm s}^{-1}$ in the studied campaigns for the reference case parameterization “KS2012 Urban”, well within the range reported by Zhang et al. (2001).

Petroff, A., Mailliat, A., Amielh, M., and Anselmet, F.: Aerosol dry deposition on vegetative canopies. Part II: A new modelling approach and applications, *Atmos. Environ.*, 42, 3654-3683.

Zhang, L., Gong, S., Padro, J., and Barrie, L.: A size-segregated particle dry deposition scheme for an atmospheric aerosol module, *Atmos. Environ.*, 35, 549-560, 2001.

For size-dependent dry deposition velocities to typical urban surfaces: asphalt, roof bricks, concrete tile, and gravel only limited measurements exist. For these slightly rough surfaces, the

measurement uncertainty is expected to be similar as for field measurements of vegetated surfaces (i.e. one order of magnitude) due to the difficulties of the measurements and different methods and assumptions during different measurement studies.

However, the span of literature values is smaller than the span between the upper line (“H2012, High Roughness”) and lower line (“H2012, Low Friction”) in our Figure 2 (size-dependent dry deposition velocity) which can be interpreted as the uncertainty range of tested dry deposition parameterizations.

The uncertainty due to available dry deposition measurements has to be distinguished from the uncertainty due to treating the underlying urban surface as homogeneous in the idealized scenario. The latter uncertainty can however be eliminated when the respective surface type is considered in the urban models, for example by using look-up tables of the size-dependent dry deposition velocity for each relevant surface (or land use) type.

Due to the dominant contribution of dilution to PN losses at all sites, and the competition between dry deposition and coagulation with respect to the loss of nanoparticles ($D_p < 25$ nm), which made up the largest PN fraction at roadside (except at Rotterdam), it is not possible to better constrain the dry deposition process in the model.

The following text will be added to the new section 3.6 (“Uncertainties of the aerosol treatment in the idealized scenario”): “Measurements of dry deposition velocities of particles for one particular surface type generally vary by one order of magnitude for a given particle size range of a half logarithmic decade (e.g. for different grassland and forest types; Petroff et al., 2008). Dry deposition velocities for total PN ($0.2\text{--}0.9$ cm s⁻¹), calculated with the reference case parameterization “KS2012 Urban”, correspond to the reported range of measured deposition velocity values.”

1.d The authors completely ignore additional emissions sources that happen between the roadside site and the “background” site. How does this effect the uncertainties on the estimates?

We have already clarified in our reply to the Comment by Prof Roy M. Harrison and co-workers, that no additional emissions are collected during transport from roadside to ambient in the idealized scenario. Additional sources of ultrafine particles between the roadside site and the background site, i.e. downwind of the roadside, would also influence the particle size distribution that has been measured at the urban background site. In principle, particles emitted from additional sources on the travel path are integrated in the shape of the average size distribution of the urban background site. However, if there are strong emissions of ultrafine particles on the way, the momentary particle size distribution might strongly be changed resulting in somewhat different results at 3600 m distance than without extra emissions. However, since we don't have emission inventories available, the more accurate simulations could not be performed.

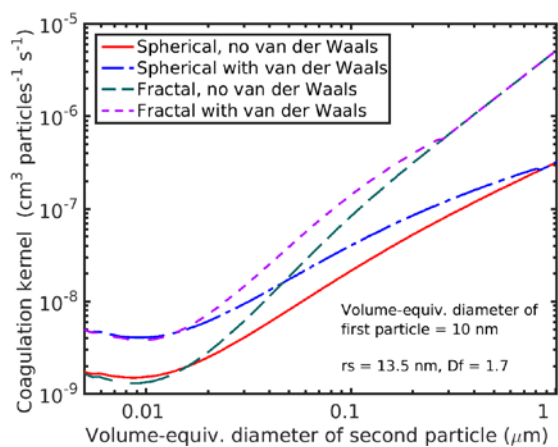
Figure 4 shows that the modeled particle size distribution converges with the measured size distribution at the urban background site after a distance of 3600 m from the roadside site

under moderate dispersion conditions. Therefore momentary fluctuations in the dilution rate due to additional emissions during the travel path are expected to have a small effect on the effective total PN loss.

1.e Both the van der Waals and the diesel agglomerate issue have effects that goes in only one direction, and we know which direction that is. Further, it is possible to estimate (bracket) the size of most of the effects. In this situation, the authors need to address the size of the potential effects, and also include in their analysis the fact that both 1.a and 1.b skew the results in a single direction (unless fractal agglomerates behave like spheres and van der Waals forces do not exist, but there is abundant evidence to the contrary in both cases). The dry deposition uncertainty can go in either direction, but also results in large uncertainties. 1.d may be a smaller effect.

The combination of the two effects, fractal geometry of soot aggregates (1.a), and van der Waals forces together with viscous interactions (1.b), substantially enhanced the loss of nanoparticles during advection of the exhaust plume from roadside to the neighborhood scale. The effect of fractal particles is now taken into account using the fractal parameters $r_s = 13.5$ nm and $D_f = 1.7$ given by Jacobson and Seinfeld (2004). In addition, fractal parameters from the study by Lemmetty et al. (2008), $r_s = 2.5$ nm and $D_f = 2.5$, were also tested. Figure C1 shows how the consideration of van der Waals forces assuming either spherical or fractal geometry of aggregates enhances the coagulation kernel for the collision with a 10-nm particle (volume-equivalent diameter), as implemented in the MAFOR model. Figure C1 will be included as Figure S5 in the Supplement.

a)



b)

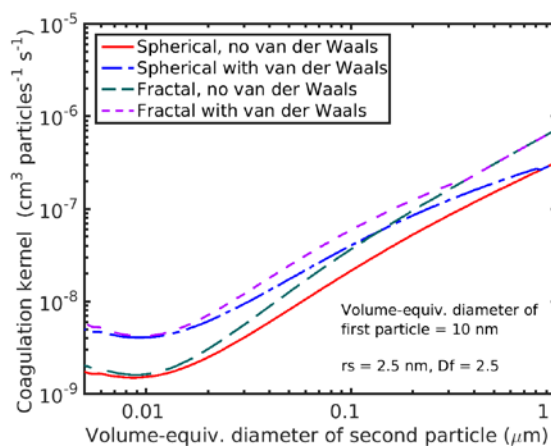


Figure C1: Brownian coagulation when the volume-equivalent diameter of the first particle is 10 nm and the volume-equivalent diameter of the second particle varies from 5 to 1000 nm: a) fractal geometry ($r_s = 13.5$ nm, $D_f = 1.7$) adapted from Jacobson and Seinfeld (2004), b) fractal geometry ($r_s = 2.5$ nm, $D_f = 2.5$) adapted from Lemmetty et al. (2008). The four curves account for when particles are spherical or fractal and when van der Waals and viscous forces (parameterized as described in section S3) are or are not included.

The size distribution of Helsinki MMEA was chosen to demonstrate the two effects in a scenario simulation since it was found that coagulation is a relevant process and a high fraction of

nanoparticles was present at the roadside site. Coagulation contributed ca. 10% to PN losses after 600 m distance. Taking into account the fractal geometry as well as van der Waals and viscous forces doubled the contribution of coagulation to PN losses, resulting in a 15% higher loss of total PN compared to the reference simulation. Figure C2 shows how the modeled size distribution after 600 m distance from the roadside was affected by the two effects, assuming inefficient dispersion conditions. Figure C2 will be included as Figure S6 in the Supplement.

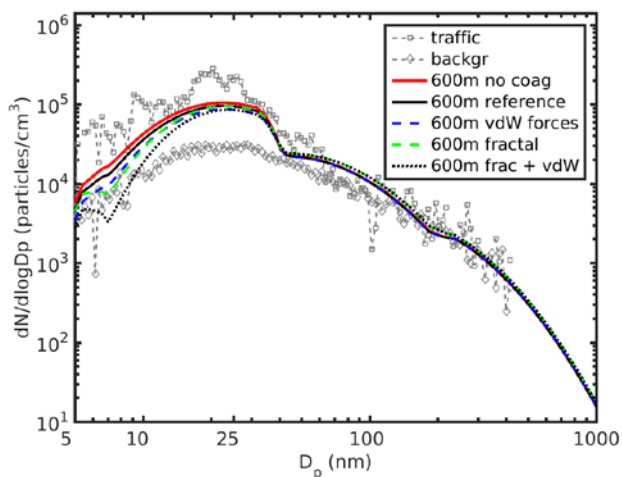


Figure C2: Sensitivity of the modeled size distribution to the effects of fractal geometry and van der Waals forces combined with viscous forces in campaign Helsinki-MMEA for inefficient dispersion. Modeled number size distributions ($dN/d\log D_p$ in particles cm^{-3}) 600 m downwind for reference case, i.e. spherical particles, coagulation by Brownian motion only (black line), case with coagulation of spherical particles enhanced by van der Waals and viscous forces (blue dashes), case with fractal geometry (green dashes) according to Jacobson and Seinfeld (2004), and case with coagulation of fractal particles enhanced by van der Waals and viscous forces (black dots). Red curve shows the modeled size distribution for the case without coagulation.

The uncertainty of coagulation by not considering fractal geometry (1.a) and by not considering van der Waals forces and viscous interactions (1.b) is addressed in our reply to point 3 of the reviewer.

The uncertainty due to the literature span of dry deposition values (1.c) was estimated in relation to the reference case by increasing and decreasing the “KS2012 Urban” deposition velocity by a factor 2 and 1/5, respectively.

The uncertainty due to additional emissions of particles on the travel path between the roadside site and the background site (1.d) was estimated in relation to the reference case by uniformly decreasing the dilution rate for all particles by 5%.

The following text with respect to point 1.a and point 1.b will be added in the new section 3.5 (“Effect of fractal geometry of soot particles and van der Waals forces”): “The effect of van der Waals forces and viscous interactions as well as fractal geometry on the Brownian collision kernel is shown in Figure S5. Parameters of the fractal geometry adapted from Jacobson and Seinfeld (2004), $r_s = 13.5$ nm and $D_f = 1.7$, resulted in stronger enhancement of the coagulation

rate for collisions with a 10 nm particle than the parameters ($r_s = 2.5$ nm and $D_f = 2.5$) adapted from Lemmetty et al. (2008).”

The following text with respect to the effect of point 1.a and point 1.b on the modelled size distributions will be added in the new section 3.5: “The combination of both effects substantially enhanced the loss of nanoparticles in the simulation of the evolution of the roadside aerosol. For Helsinki MMEA, inefficient dispersion conditions, the enhancement was similar for the two effects, separately, i.e. spherical particles with van der Waals and viscous forces versus fractal particles (Figure S6). The combined effect increased the loss of total PN by 15% compared to the reference simulation (coagulation of spherical particles by Brownian motion) in 600 m distance from the road.”

2. All studies considering the effects of particle dynamics in emissions to the atmosphere struggle with the issue that dilution is responsible for the majority of the changes observed in particle concentrations and size distributions (see also comments from Prof. Harrison and co-workers). This means researchers are trying to tease out the small effects of coagulation/condensation/deposition (and evaporation?) when the vast majority of the aerosol evolution is caused by dilution, not any of the other processes.

2.a. First, the manuscript would be more clear if the contribution of dilution to the final concentrations was included explicitly.

The contribution of dilution to the final concentrations (after 30 min travel time) for each dispersion case will be included explicitly in Table 4.

2.b. The test applied to verify the MAFOR is working – start out with near roadway air, dilute with background air and arrive at the background concentration profiles needs to be tested for sensitivity to processes other than dilution, and to the dilution scheme as well. The bugger with this type of analysis is that the model needs to meet quite high standards to be able to verify parameterizations for dry deposition, condensation and coagulation. And even then, given the uncertainties for the minor processes, it is hard.

The primary goal of this study was to identify aerosol dynamic processes that are able to compete with dilution and to quantify the associated PN losses on the neighborhood scale. Validation of the MAFOR model was not intention of the study, despite the good agreement with the measured particle size distribution at the urban background sites. PN losses by dilution are overwhelming and the relatively small contribution from aerosol processes has to be carefully evaluated. Evaluation of different parameterizations of individual aerosol processes would only be possible with several intermediate sampling positions in 100-1000 m distance downwind between the roadside and the background site. However, the current study tried to include different urban settings, exhibiting different traffic conditions and different sampling periods, in order to arrive at a generally applicable simple parameterization for modelling PN concentrations in urban models.

Coagulation by Brownian motion is treated in a physical accurate manner in the model hence does not require verification in a field study. Different empirical parameterizations of size-

dependent dry deposition rates, which were compared in the present study, show considerable spread, resulting in three different time scale estimates for use in the simplified parameterization. Condensation and evaporation are treated as physical process but important constraints such as measurements of gas-phase and particle-phase concentrations of semi-volatile and low-volatile compounds are lacking.

3. The estimates of all processes need well founded error bars, or at the very least a hard-headed discussion of uncertainties. This will go a long way to addressing comments 1. And 2. If done well, it will make the manuscript much better.

We agree with the reviewer’s suggestion to perform a rigorous analysis of uncertainties associated with each aerosol dynamic process, and also for the dilution parameterization applied in the idealized scenarios. This will help to highlight the need for more investigations of certain aerosol dynamic processes in future.

An uncertainty analysis was performed to quantify the errors associated with the determination of the contribution of the respective atmospheric processes to the change of total PN. Errors were determined based on simulations for the mean traffic-related particle distribution (obtained from a fit of MAFOR to the average of the size distribution curves for all traffic sites) under inefficient dispersion conditions after 30 min travel time. Figure C3 depicts the percentage contribution to total PN losses, together with the error bars for aerosol processes, additional emissions, and the dilution scheme. Figure C3 will be included as Figure 6 in the revised manuscript.

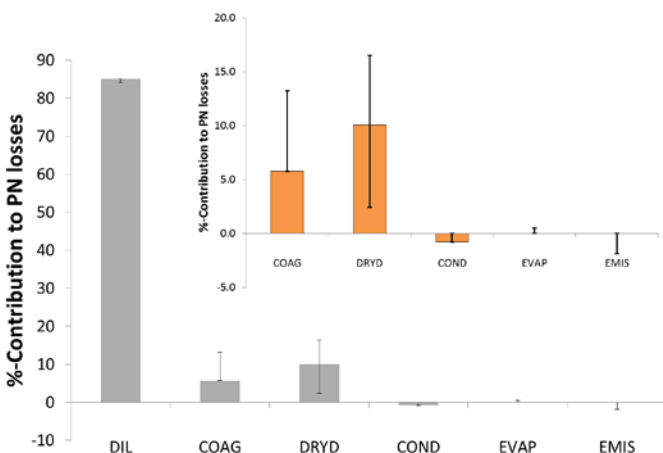


Figure C3: Contribution of processes to the percentage change of PN concentrations between roadside station and neighborhood environment, and their associated uncertainty depicted as error bars. Inset magnifies the contribution and uncertainty of the aerosol processes and additional emissions of particles.

The following sentences will be added to the new section 3.6 (“Uncertainties of the aerosol treatment in the idealized scenario”).

With respect to coagulation: “Fractal geometry parameters of Jacobson and Seinfeld (2004) were chosen for the evaluation of the uncertainty of the coagulation process. The combined effect of fractal geometry and van der Waals plus viscous interactions was taken into account,

resulting in an error of +130%, roughly corresponding to a doubling of the contribution of coagulation to PN losses between roadside station and the neighborhood.”

With respect to dry deposition: “Here, dry deposition velocity was scaled by factor 2 and 1/5 to evaluate the uncertainty of the dry deposition process due to literature span of measured velocities. This resulted in an error margin from -76% to +64% for the contribution from dry deposition.”

With respect to condensation and evaporation: “For the mean traffic-related particle distribution, evaporation contributed 0.3 % to PN losses when assuming 0.005 ppb C22 + C28 and 100% C22 in <10 nm particles. Condensation and evaporation are uncertain processes due to the lack of measurements of the gas-phase and particle phase concentrations of condensable compounds at the roadside station. Oxidation of VOC from vehicular emissions may provide an additional source of condensable material on the neighborhood scale. However, oxidized VOC in the background air are expected to condense on the particles of the accumulation mode, increasing their volume, rather than changing PN concentrations.”

With respect to additional emissions: “Additional emissions of particles on the travel path between the roadside station and the background were not considered in the idealized scenario. Since the dilution process in the model simulations was constrained with the measured size distribution at the background, the influence of additional particle emissions has been implicitly taken into account. However, if there are strong emission sources of ultrafine particles on the way, the momentary particle size distribution might be perturbed. The error due to fluctuations of the dilution rate caused by additional emissions was estimated to be -2 %.”

With respect to the dilution scheme: “The main uncertain parameter in the applied dilution scheme [Eqs. (1) and (2)] is the initial plume height at the roadside, $H_{m,0}$. Doubling $H_{m,0}$ resulted in a small error (-1%) of the contribution of dilution to PN losses.”

4. P 35184 Given the uncertainties in coagulation resulting not just from not interacting size bins but also the assumptions in comment 1, the claim of dry deposition rates within 10% seems optimistic.

The paragraph on page 35184 refers to the accuracy of the simplified PN parameterization as compared to the fully size-resolved aerosol dynamics and also to the potential improvements of the parameterization, not to the uncertainty of the modeled aerosol dynamic processes. The formulation in the original manuscript was ambiguous and will be corrected. Furthermore, concluding remarks from the uncertainty analysis of the aerosol dynamic processes (point 3) will be added to the Conclusions.

The sentence “The parameterization of aerosol processes can predict particle number concentrations between roadside and the urban background within an inaccuracy of 10%.” will be changed to “The parameterization of dry deposition and coagulation can predict total particle number concentrations between roadside and the urban background within an inaccuracy of 10%, compared to simulations with the fully size-resolved MAFOR model.”

The following text will be added to the Conclusions:

“Computation of the aerosol evolution between the roadside station and the neighborhood environment involved several assumptions and uncertain parameters. Due to the lack of measurements of the gas-phase and particle phase concentrations of semi-volatile compounds during the studied campaigns, the contributions from condensation and evaporation of condensable vapors emitted with the vehicle exhaust to PN changes are uncertain. Due to the wide span of measured deposition velocities in literature, the contribution from dry deposition to PN losses has an uncertainty range from -76% to +64%. The removal of nanoparticles by coagulation is further enhanced when considering the fractal nature of soot aggregates and the combined effect of van der Waals and viscous interactions. Taking into account these effects doubles the contribution of coagulation to PN losses between roadside and neighborhood.”

The following text will be added to the Abstract:

“The error of the contribution from dry deposition to PN losses due to the uncertainty of measured deposition velocities ranges from -76% to +64%. The removal of nanoparticles by coagulation enhanced considerably when considering the fractal nature of soot aggregates and the combined effect of van der Waals and viscous interactions”

List of relevant changes in the ms

Relevant text changes:

1. Condensation and evaporation of organic vapors

We address the concern by Prof Harrison and co-workers regarding the applied concept for condensation and evaporation of organics between the roadside site and the urban background site by adding the following text in section 2.1 (Pg. 6 lines 9-15): “The concept regarding condensation and evaporation between roadside and ambient environment applied in this study is based on the work of Zhang and Wexler (Zhang and Wexler, 2004; Zhang et al. 2004). The effective behavior of condensable organic vapors from vehicular exhaust with respect to changes of the particle number concentration and the particle size distribution was modeled by introducing two different volatility classes: the n-alkane $C_{22}H_{46}$ (abbreviated as C22) representing semi-volatile vapors and the n-alkane $C_{28}H_{58}$ (abbreviated as C28) representing low-volatile vapors.”

Further it was added in section 2.2 (Pg. 9 line 13-22):

“The applied aerosol dynamics model makes no assumption regarding the equilibrium between organic vapor and the condensed phase at the roadside. If the gas-phase concentration of an organic compound is below the saturation concentration, the compound will evaporate from the particles, if it is above the saturation concentration, the compound will condense to the particles. During the road-to-ambient process, some compounds may continue condensing, while others begin evaporating, depending on the relative magnitude of their vapor pressures. In addition, the vapor pressure of the model compounds C22 and C28 is further modified by their molar fraction in the particle phase, according to Raoult’s law, and by their molar volume and surface tension according to the Kelvin effect.”

In order to justify the use of 0.5 ppb of condensable organic vapors in the reference case the following paragraph was added in section 2.2 (Pg. 9 line 23 to Pg. 10 line 5):

“For the included campaigns, gas-phase concentration of n-alkanes and other condensable organic compounds have not been measured at the roadside locations. Measurements of n-alkane vapor concentrations in urban environments indicate typical concentrations of 5 ppt for the sum of the n-alkanes, but higher concentrations may occur (for more details see section S2 in the Supplement). Pohjola et al. (2007) obtained best fit between modeled and measured particle size distribution on a distance scale of 125 m near a major road in Helsinki when using roadside concentrations of one condensable organic vapor of the order of 10^{10} molecules cm^{-3} (ca. 0.4 ppb). Based on this, initial concentrations of 0.25 ppb C22 and 0.25 ppb C28 were used in the reference case (all campaigns and dispersion conditions). The background concentration of C22 and C28 was set to zero, forcing maximum dilution of the condensable organic vapors during travel of the air parcel away from the roadside.”

In order to clarify the use of C22 and C28 as two volatility classes that represent semi-volatile and low-volatile condensable organic vapors, the term “n-alkanes” was replaced by “condensable organic vapors” where appropriate in the ms.

A description of reported n-alkane measurements was included in Section S2 of the Supplementary Information. The estimation of the 5-10% conversion of VOC into condensable organic compounds was removed from the Supplementary Information.

The title of section 3.4 was changed from "Effect of condensation of n-alkanes" to "Effect of condensation and evaporation of organic compounds".

The sensitivity tests in the range 1-4 ppb were replaced by a test series with smaller concentrations for the sum of C22 and C28, stepwise decreasing by one order of magnitude between 500 ppt (i.e. 0.5 ppb, reference case) and 5 ppt, closer to the reported measurements of the sum of n-alkanes available for condensation. Results from the new tests on condensation and evaporation were added to section 3.4. Two new figures (Figures S3 and S4) showing the particle number and mass size distributions in 240 m distance from roadside for Helsinki LIPIKA and for UFP-Oslo Winter with different concentrations of condensable organic vapors were included in the Supplement.

Since evaporation depends on the volatility of the nanoparticles in the exhaust post-emission, the OC fractions in the modeled nucleation mode were changed to 100% C22 in an additional test. The result from this test for UFP-Oslo Winter was added in section 3.4 (Pg. 23 line 6-21). Regarding the possibility of evaporation to occur in the idealized scenario, the following was added in section 3.4 (Pg. 23 line 28 to Pg. 24 line 7):

"Model simulations of the idealized scenario suggest that evaporation could be an important process, altering the particle size distribution in urban micro-environments, if the semi-volatile vapor and also the nanoparticles forming post-emission were assumed to have the same or higher volatility as the n-alkane C22. Dall'Osto et al. (2011) analyzed observations of particle size distributions from London and reported a reduction in the size of nucleation mode particles during advection from a major highway into the cleaner environment of a park, indicating evaporative loss of semi-volatile constituents during travel times of around 5 min. Harrison et al. (2016), for the same location, found most rapid evaporation to occur at higher wind speeds, associated with shorter travel times, but cleaner air."

2. Effects of van der Waals forces and fractal geometry

The first main concern of Referee #2 was that important processes were ignored in the idealized scenario which could qualitatively change the relevance of the different aerosol processes. In response to this concern, (1) the effect of treating aggregates of soot as fractal particles and (2) the effect of van der Waals forces, which both mainly act on the removal of nanoparticles, were included in the model to provide an estimate of the error when these effects were not taken into account. The effect of the fractal shape of soot aggregates was

account in the revised manuscript by considering the effect on radius, diffusion coefficient and the Knudsen number in the Brownian collision kernel, following the approach described by Jacobson and Seinfeld (2004). A simplified treatment of the van der Waals enhancement combined with retardation by viscous forces was included to evaluate the possible uncertainty introduced into our study by neglecting the two interactions. A correction factor due to van der Waals and viscous forces was applied to the Brownian collision kernel in the MAFOR model.

The description of the treatment of fractal geometry and correction for van der Waals / viscous interactions in MAFOR was added in the new section 3.5 “Effect of fractal geometry of soot particles and van der Waals forces”. A detailed description of the correction for van der Waals/ viscous interactions is given in the new Supplement section S3 (“Modification of the Brownian coagulation kernel to approximate van der Waals forces and viscous interactions”).

3. Uncertainty analysis

The second main concern of Referee #2 was that the sensitivity to processes other than dilution is small, so that the model has to meet high standards to be able to verify the included parameterizations of dry deposition, condensation, and coagulation. We argue that the primary goal of the study was to identify those aerosol dynamic processes that are able to compete with dilution and to quantify the associated PN losses on the neighborhood scale. The current study includes different urban settings, exhibiting different traffic conditions and different sampling periods, in order to arrive at a generally applicable simple parameterization for modelling PN concentrations in urban models. Due to lack of data, such as measured composition of gas-phase and particle phase concentrations of semi-volatile and low-volatile compounds, and lack of intermediate measurement positions, the campaign data could not be used to evaluate the aerosol processes in the MAFOR model.

The third main concern of Referee #2 is that the uncertainties of the involved processes have not been assessed. Following this concern, an uncertainty analysis was performed to quantify the errors associated with the determination of the contribution of the respective atmospheric processes to the change of total PN concentration between the roadside site and the background site. Errors were determined based on simulations for the mean traffic-related particle distribution (obtained from a fit of MAFOR to the average of the size distribution curves for all traffic sites) under inefficient dispersion conditions after 30 min travel time. Under inefficient dispersion conditions, aerosol processes are most relevant compared to dilution and therefore the associated errors can be determined with higher accuracy.

A new section 3.6 (“Uncertainties of the aerosol treatment in the idealized scenario”) was added in the revised manuscript to report the results from the uncertainty analysis.

The following text was added to the Conclusions (Pg. 32 line 3-13):

“Computation of the aerosol evolution between the roadside station and the neighborhood environment involved several assumptions and uncertain parameters. Due to the lack of

measurements of the gas-phase and particle phase concentrations of semi-volatile compounds during the studied campaigns, the contributions from condensation and evaporation of condensable vapors emitted with the vehicle exhaust to PN changes are uncertain. Due to the wide span of measured deposition velocities in literature, the contribution from dry deposition to PN losses has an uncertainty range from -76% to +64%. The removal of nanoparticles by coagulation is further enhanced when considering the fractal nature of soot aggregates and the combined effect of van der Waals and viscous interactions. Taking into account these effects doubles the contribution of coagulation to PN losses between roadside and neighborhood.”

The following text was added to the Abstract:

“The error of the contribution from dry deposition to PN losses due to the uncertainty of measured deposition velocities ranges from -76% to +64%. The removal of nanoparticles by coagulation enhanced considerably when considering the fractal nature of soot aggregates and the combined effect of van der Waals and viscous interactions”

Tables:

Table 3.

The measured average PN concentration for Helsinki LIPIKA Case 1 in this table was corrected.

Table 4.

The percentage contribution of dilution to PN concentration changes between the roadside station and the neighborhood environment was added for all campaigns and dispersion conditions.

Table S3.

A new table, Table S3, providing the parameter values of dry deposition and coagulation required for implementation of a PNC parameterization with six size categories was included in the Supplement.

Figures:

Figure 1.

The illustration of the idealized scenario was slightly modified to be in accordance with the description of the initial plume stage given in the new section S1 of the Supplement (“Approximation of the initial plume height at roadside”).

Figure 6.

A new figure, Figure 6, was included in the revised manuscript. It displays the contribution of processes to the percentage change of PN concentrations between roadside station and neighborhood environment, and their associated uncertainty depicted as error bars.

Figure S1.

The measured average PN concentration for Helsinki LIPIKA Case 1 in this figure was corrected.

Figure S3.

A new figure, Figure S3, was included in the Supplement, showing the sensitivity of the modeled particle number and mass size distributions to changes of the concentration of condensable organic vapors (sum of C22 and C28) and composition of particles in campaign Helsinki LIPIKA for moderate dispersion conditions.

Figure S4.

A new figure, Figure S4, was included in the Supplement, showing the sensitivity of the modeled particle number and mass size distributions to changes of the concentration of condensable organic vapors (sum of C22 and C28) and composition of particles in campaign Oslo UFP-Oslo Winter for inefficient dispersion conditions.

Figure S5.

A new figure, Figure S5, was included in the Supplement, showing the effect of van der Waals forces and viscous interactions as well as fractal geometry on the Brownian collision kernel. Two parameter sets of the fractal geometry were tested: from Jacobson and Seinfeld (2004), with $r_s = 13.5$ nm and $D_f = 1.7$, and from Lemmetty et al. (2008), with $r_s = 2.5$ nm and $D_f = 2.5$.

Figure S6.

A new figure, Figure S6, was included in the Supplement, showing the sensitivity of the modeled particle number size distribution to the effects of fractal geometry and van der Waals forces combined with viscous forces in campaign Helsinki-MMEA for inefficient dispersion conditions.

Modelling and measurements of urban aerosol processes on the neighborhood scale in Rotterdam, Oslo and Helsinki

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Abstract. This study evaluates the influence of aerosol processes on the particle number (PN) concentrations in three major European cities on the temporal scale of one hour, i.e. on the neighborhood and city scales. We have used selected measured data of particle size distributions from previous campaigns in the cities of Helsinki, Oslo and Rotterdam. The aerosol transformation processes were evaluated using an aerosol dynamics model MAFOR, combined with a simplified treatment of roadside and urban atmospheric dispersion. We have compared the model predictions of particle number size distributions with the measured data, and conducted sensitivity analyses regarding the influence of various model input variables. We also present a simplified parameterization for aerosol processes, which is based on the more complex aerosol process computations; this simple model can easily be implemented to both Gaussian and Eulerian urban dispersion models. Aerosol processes considered in this study were (i) the coagulation of particles, (ii) the condensation and evaporation of ~~n-alkane~~two organic vapors, and (iii) dry deposition. The chemical transformation of gas-phase compounds was not taken into account. ~~It was not necessary to model the~~ By choosing concentrations and particle size distributions at roadside as starting point of the computations, nucleation of gas-phase vapors ~~as the computations were started with roadside conditions from the exhaust has been regarded as post tail-pipe emission, avoiding the need to include nucleation in the process analysis.~~ Dry deposition and coagulation of particles were identified to be the most important aerosol dynamic processes that control the evolution and removal of parti-

cles. The error of the contribution from dry deposition to PN losses due to the uncertainty of measured deposition velocities ranges from -76 % to +64 %. The removal of nanoparticles by coagulation enhanced considerably when considering the fractal nature of soot aggregates and the combined effect of van der Waals and viscous interactions. The effect of condensation and evaporation of organic vapors emitted by vehicles on particle numbers and on particle size distributions was examined. Under inefficient dispersion conditions, condensational growth ~~contributed significantly~~ might contribute to the evolution of PN from roadside to the neighborhood scale. The simplified parameterization of aerosol processes can predict particle number concentrations between roadside and the urban background with an inaccuracy of $\sim 10\%$, compared to the fully size-resolved MAFOR model.

1 Introduction

Motor vehicle exhaust emissions constitute the major source of ultrafine particle (UFP, < 100 nm in aerodynamic diameter) pollution in urban environments (Harrison et al., 2011; Morawska et al., 2008; Pey et al., 2009; Johansson et al., 2007). Ultrafine particles can contain toxic contaminants, such as transition metals, polycyclic aromatic hydrocarbons (PAHs), and other particle-bound organic compounds, which may be responsible for initiating local lung damage, when the particles deposit on the epithelial surfaces (Lighty et al., 2000). Biodistribution studies suggest translocations of UFP

from the respiratory system to other organs including liver, heart and the central nervous system, in which they can cause adverse health effects (Oberdörster et al., 2005; Kleinman et al., 2008; Kreyling et al., 2013). In urban environments, ultrafine particles make the most significant contribution to total particle number (PN) concentrations, but only a small contribution to particulate matter (PM) mass. Hence, reliable information on the number concentrations, together with the size distributions, is needed to better assess the health effects of urban particulate pollution.

The exposure of the population in urban areas to particles may be assessed by modelling the spatial distribution of particles emitted from road transport and other sources in various micro-environments (e.g., Soares et al., 2014). Kumar et al. (2011) reviewed aerosol process modelling on urban and smaller scales. Aerosol dynamic models (which are commonly Lagrangian-type process models) have been used to model the spatial and temporal evolution of ultrafine particles in the initial vehicle exhaust plume during the first seconds after emission (e.g. Vignati et al., 1999; Pohjola et al., 2003, 2007). These models can be used to study the further evolution of the plume, if they will be coupled to an urban dispersion model. Particles emitted from road transport, as they are transported from the emission sources, are subject to complex dilution processes (turbulence generated by moving traffic, atmospheric turbulence) and transformation processes (nucleation, coagulation, condensation, evaporation, deposition, and heterogeneous chemical reactions), acting on different time scales. Aerosol dynamic processes continuously change the number and size distribution, after the particles have been released into air.

Clearly, dilution is an important process influencing PN concentrations and the spatial distributions in cities (e.g. Zhang et al., 2004; Pohjola et al., 2007; Keuken et al., 2012). An exhaust parcel emitted from the tailpipe of a vehicle first experiences fast dilution by the strong turbulence generated by moving traffic between tailpipe to roadside (Rao et al., 2002; Zhang and Wexler, 2004). On the neighborhood scale in the city, the parcel of exhaust is advected through a network of streets, over and around several buildings. On the city scale, the pollutant plume can extend vertically up to twice the average building height above the city's surface layer, and its dispersion becomes independent of the specific effects of individual buildings (Kumar et al., 2011).

The main aims of the present study are (i) the quantification of the impacts of relevant aerosol processes on the neighborhood and city scales and (ii) the derivation of a reasonably accurate, simplified parameterization of the most important aerosol processes, to be used in urban air quality models. The study is part of the European Union funded research project TRANSPHORM (Transport related Air Pollution and Health impacts – Integrated Methodologies for Assessing Particulate Matter). A related paper by Kukkonen et al. (2015) presents atmospheric dispersion modelling of particle number concentrations in the five target cities of

the TRANSPHORM project, as well as on a European scale, and evaluates the predicted results against available measured concentrations. In the present model study, we have used the results of measurements from a campaign in Rotterdam, initiated by the TRANSPHORM project, and those from previous campaigns in Helsinki and Oslo. Our aims are to quantify the influence of selected individual aerosol processes for each measurement campaign and to inter-compare the relative contribution of the processes to PN changes in the selected campaigns and cities.

2 Materials and methods

2.1 Aerosol process model MAFOR

In order to study the relevance of aerosol dynamics on the fate of PN emitted from traffic in urban areas, the evolution of the particle size distribution with increasing distance from the roadside was modeled using the multicomponent aerosol dynamics model MAFOR (Karl et al., 2011). MAFOR uses a fixed sectional grid to represent the particle size distribution with size bins evenly distributed on a logarithmic scale. MAFOR has been evaluated against laboratory chamber data (Karl et al., 2012) and PN measurements at a motorway (Keuken et al., 2012); it has also been shown to compare well with the sectional aerosol dynamics model AEROFOR (Pirjola and Kulmala, 2001).

Aerosol processes considered in this study were condensation and evaporation of [n-alkanes](#) [organic vapors](#), coagulation of particles due to Brownian motion, and dry deposition (particle deposition in contact with the street surface and other urban structures). In this study 120 size bins were used in the MAFOR model, to represent the aerosol size distribution ranging from particle diameters from 1 nm to 1 μ m.

Particles were assumed to be spherical and possible effects of the fractal geometry were disregarded; the exact shape and morphology of particles was not measured in the addressed campaigns. The various aerosol dynamical processes were treated by calculation of the temporal variation of the particle number concentration and the mass concentrations of each chemical component within each size section. Mass transfer of gas molecules to particles was calculated using the Analytical Predictor of Condensation scheme (Jacobson, 1997).

The coagulation coefficients of particles that are smaller than 50 nm in diameter might be enhanced due to Van der Waals forces and viscous interactions; however, these were neglected, due to the large uncertainties involved in the modelling of such processes. Further, effects of turbulent shear on coagulation between exhaust particles can be neglected for the time scale from roadside to ambient (Zhang and Wexler, 2004).

Dry deposition of particles was modelled according to Kouznetsov and Sofiev (2012), which accounts for the physical properties of both the air flow and the surface, as well as

the physical properties of the particle size. In this approach rough surfaces are characterized by two length scales: the aerodynamic roughness and the so-called collection scale, which incorporates the effective size of collectors and a ratio of the airflow velocity at the top of the roughness elements to the friction velocity. Alternatively, MAFOR provides a treatment to calculate size-dependent deposition rates according to Schack et al. (1985) and Hussein et al. (2012).

~~Two different n-alkanes (i.e., The concept regarding condensation and evaporation between roadside and ambient environment applied in this study is based on the work of Zhang and Wexler (Zhang and Wexler, 2004; Zhang et al., 2004). The effective behavior of condensable organic vapors from vehicular exhaust with respect to changes of the particle number concentration and the particle size distribution was modeled by introducing two different volatility classes: the n-alkane C₂₂H₄₆ and) were used to represent vehicular exhaust gases with different volatilities, which (abbreviated as C22) representing semi-volatile vapors and the n-alkane C₂₈H₅₈ (abbreviated as C28) representing low-volatile vapors. Both organic compounds can condense or evaporate to or from particles during their transport downwind from the road. Vapor pressure of n-alkanes as function of temperature was adopted from the work by Lemmon and Goodwin (2000).~~

Carbonaceous aerosol in MAFOR is separated into (i) elemental carbon (EC_p) from primary emissions, treated as a non-volatile substance, and (ii) organic carbon (OC_p), treated as a volatile substance. In this study, organic carbon is assumed to be composed of organic acid (for background OC_p) and the two n-alkanes (originated from vehicles). The organic fraction in the nucleation mode below 10 nm diameter was composed by 100% of C28 in the roadside aerosol. A density of 1200 kg m⁻³ (Virtanen et al., 2002) was used for EC_p. The density of OC_p was calculated as the weighted average of the densities of the organic compounds.

2.2 Modelling of the dilution of exhausts

MAFOR is a one-dimensional model; it is therefore necessary to couple it to a dispersion model, to simulate combined atmospheric dispersion and transformation processes. In order to approximate atmospheric dispersion, we used a simplified treatment of dilution of particle numbers. This procedure implies the assumption of a well-mixed state within each cross-wind cross-section of the plume. The assumption of a well-mixed state may overestimate the influence of the processes responsible for the temporal decrease of the PN, due to the non-linear nature of the involved processes (condensation and coagulation). Model runs were performed with different dispersion conditions to address the influence of aerosol processes for a wide range of meteorological dispersion regimes.

Emissions from traffic sources commonly contribute to particle size distributions with distinct modes, i.e. nucleation, Aitken, accumulation, and coarse mode. Formation of new liquid particles in the exhaust by nucleation of gases, such as sulfuric acid and semi-volatile organic substances, occurs during the first milliseconds (Kittelson, 1998) after release of the exhaust into the ambient air. On-road measurements by Rönkkö et al. (2007) confirmed that the nucleation mode was already present after 0.7 s residence time in the atmosphere. Thus, it is practical to regard nucleation as a process that has already occurred, when one considers roadside concentrations. The evolution of vehicular emissions from the engine to the roadside concentrations were not considered in this study, as we used the particle size distributions measured at the roadside locations as a starting point.

Idealized scenarios were set up for the study of relevant aerosol processes (i.e. the dry deposition, the growth by condensation of gases and the coagulation of particles) and dilution by background air (see Fig. 1).

We used a simple horizontal particle dilution parameterization, following the numerical power function $y = a \times x^{-b} = a \times (Ut)^{-b}$, where x (in m) is the distance from the roadside and U is the horizontal wind speed perpendicular to the road. The height of the air parcel (plume height), H_m (in m), containing the exhaust emissions, as function of time t (in s) during its travel away from the roadside at a specific wind speed was defined by:

$$H_m(t) = \sqrt{H_{m,0}^2 + \left(a \times (10^{-3} \times Ut)^b\right)^2} \quad (1)$$

Where $H_{m,0}$ is the initial plume (or air parcel) height at the roadside. The particle dilution rate for use in the aerosol model was obtained by derivation of the above mentioned numerical power function as function of time. The change of particle number concentration, N (in particles cm⁻³), in size section i due to dilution with background air is:

$$\left. \frac{dN_i}{dt} \right|_{\text{dilution}} = -\frac{b}{t} (N_i - N_{\text{bg},i}) \quad (2)$$

Where $N_{\text{bg},i}$ is the number concentration of background particles in the same size bin. No additional emissions of particles or vapors are collected during transport from roadside to ambient in this idealized scenario.

Dilution parameters a and b that are used in Eqs. (1) and (2) for moderate dispersion conditions were derived from a fit of the modelled total number concentration to measured number concentration in different distances (below 100 m) from a major highway in Helsinki (LIPIKA campaign, case 10; Fig. 5 in Pohjola et al., 2007). It was assured that the PN change in the distance up to 100 m was solely due to dilution with background air. Best fit was obtained with parameter values $a = 40$ and $b = 0.5$. For neutral conditions, the values $a = 86.49$ and $b = 0.923$ were reported for dispersion downwind of a motorway (Petersen, 1980). Similar values were adopted for efficient dispersion conditions

in this study ($a = 80.0$ and $b = 0.90$). For inefficient dispersion conditions, a and b were chosen to be typical for atmospheric situations with inversion and stagnant air. [Details on the approximation of initial plume height, \$H_{m,0}\$, at the roadside are provided in section S1 of the Supplementary Materials.](#) Table 1 provides an overview of the set of meteorological and dilution parameters that were tested in sensitivity studies.

The model simulations were started by assuming an initial chemical composition of the aerosol at the respective roadside traffic site and urban background site. Chemical composition of the urban background aerosol was estimated based on the measured $PM_{2.5}$ and the mass fractions of the chemical components in $PM_{2.5}$. Composition of the nucleation, Aitken, accumulation and coarse modes was estimated based on mass fractions for the urban background of Helsinki (Pohjola et al., 2007). Then mass concentrations of the respective lognormal modes were distributed over the discrete size sections of the model. The aerosol composition of the traffic-influenced aerosol at the traffic station was approximated by adding mass concentrations of OC_p and EC_p (from vehicle exhaust emissions) to the mass concentrations of the background aerosol. Fixed modal $OC_p : EC_p$ ratios were used (nucleation mode: 100 : 0, Aitken mode: 80 : 20, accumulation mode 1: 40 : 60, accumulation mode 2: 60 : 40) based on the mass composition of vehicle exhaust particle emissions (Pohjola et al., 2007). Finally, the initial model number size distribution was fitted to the observed number size distribution at the traffic site for each of the campaigns, by variation of the geometric-mean mass diameter (by $\pm 30\%$) and the geometric standard deviation (within the range 1.5–2.0) in each lognormal mode.

[The applied aerosol dynamics model makes no assumption regarding the equilibrium between organic vapor and the condensed phase at the roadside. If the gas-phase concentration of an organic compound is below the saturation concentration, the compound will evaporate from the particles, if it is above the saturation concentration, the compound will condense to the particles. During the road-to-ambient process, some compounds may continue condensing, while others begin evaporating, depending on the relative magnitude of their vapor pressures. In addition, the vapor pressure of the model compounds C22 and C28 is further modified by their molar fraction in the particle phase, according to Raoult's law, and by their molar volume and surface tension according to the Kelvin effect.](#)

[For the included campaigns, gas-phase concentration of n-alkanes and other condensable organic compounds have not been measured at the roadside locations. Measurements of n-alkane vapor concentrations in urban environments indicate typical concentrations of 5 ppt for the sum of the n-alkanes, but higher concentrations may occur \(for more details see section S2 in the Supplement\). Pohjola et al. \(2007\) obtained best fit between modeled and measured particle size distribution on a distance scale of](#)

[125 m near a major road in Helsinki when using roadside concentrations of one condensable organic vapor of the order of \$10^{10}\$ molecules \$cm^{-3}\$ \(ca. 0.4 ppb\). Based on this, initial concentrations of 0.25 ppb C22 and 0.25 ppb C28 were used in the reference case \(all campaigns and dispersion conditions\). The background concentration of C22 and C28 was set to zero, forcing maximum dilution of the condensable organic vapors during travel of the air parcel away from the roadside.](#)

Additional sensitivity tests were carried out to address uncertainties in the modelling with respect to (i) dry deposition of particles to urban surfaces and, (ii) assumptions about the roadside concentrations of condensable organic vapors (represented as n-alkanes). [Details on the sensitivity test for condensable organic vapors are given in Sect. S1 in the Supplement.](#), (iii) [the fractal geometry of soot particles and](#) (iv) [the enhancement of coagulation through van der Waals and viscous forces.](#)

2.3 The effect of different surface types on the dry deposition of particles

As the air parcel containing vehicle exhaust leaves street scale, it can be assumed to be advected through a network of streets, and over and around buildings, defined as the neighborhood scale with a characteristic length scale of 1–2 km. On the neighborhood scale, geometrical features dominate mean flow and mixing. Effects caused by buildings and other structures are disregarded in this study. Instead the flow was assumed to have a long fetch over a statistically homogeneous surface. However, different average surface types may have an impact on dry deposition of particles. In a series of tests the sensitivity of PN changes were studied, caused by dry deposition on various surface types and roughness conditions. Table 2 provides a summary of relevant parameters for dry deposition used in the reference case (all campaigns and dispersion conditions) and in the sensitivity tests (selected campaigns).

The parameterization used in the reference runs is thought to represent dry deposition to typical urban surfaces, i.e. streets and buildings (urban case). Values for friction velocity near surface, u^* , and roughness height, z_0 , used in the urban case were adopted from the work of Ketzel and Berkowicz (2004). Sensitivity tests for dry deposition were performed for the campaigns in Rotterdam and Oslo using the dilution parameters for moderate dispersion conditions.

The methodology by Kouznetsov and Sofiev (2012) considers Brownian diffusion, interception, inertial impaction and gravitational settling as mechanisms for dry deposition to rough surfaces. They define a collection length scale to characterize the properties of rough surfaces. This collection length depends on the ratio U_{top}/u^* (U_{top} is the wind speed at top of the canopy, i.e. at height z_C) and to the effective collector size, d_{col} , of the canopy. The methodology by Hussein et al. (2012) is a three-layer deposition model for-

mulation with Brownian and turbulent diffusion, turbophoresis and gravitational settling as the main particle transport mechanisms to rough surfaces. Hussein et al. (2012) introduced the effective surface roughness length F^+ to relate roughness height and the peak-to-peak distance between its roughness elements. For a hydraulically smooth surface, F^+ approaches zero. Parameters z_0 , z_C and d_{col} are only used in the concept of Kouznetsov and Sofiev (2012) while F^+ is only used in the concept of Hussein et al. (2012). Size-dependent dry deposition velocities of particles were calculated with two different methodologies: The methodology of Kouznetsov and Sofiev (2012) (short: KS2012) was applied in the reference case for all simulations. In addition the methodology of Hussein et al., 2012 (short: H2012) was applied for all cases in the sensitivity test.

Figure 2 shows size-dependent dry deposition velocity of particles for the different cases listed in Table 2 for the two methodologies. The curve “KS2012 Urban” (thick black line) represents the parameterization used in the reference runs of this study. Dry deposition velocities calculated by H2012 for the urban case (“H2012 Urban”) agree with “KS2012 Urban” within a factor of 3 as function of particle diameter. Results from the KS2012 methodology were not sensitive to changes of friction velocity within a range ($0.27\text{--}1.33\text{ m s}^{-1}$) typical for the urban environment.

A large discrepancy between the two methodologies was found for deciduous forest (green area with forest). H2012 closely matches measured dry deposition velocities over a beech forest by Pryor (2006) when using $F^+ = 2.25$. Kouznetsov and Sofiev (2012) state that their parameterization offsets measured data for broad-leaf forests by 2–3 orders, unless using a very small collector size ($d_{col} < 0.2\text{ cm}$). However, their parameterization is in close agreement with one wind tunnel measurement for $1\text{ }\mu\text{m}$ particle deposition on natural oak branches by Reinap et al. (2009). It should be kept in mind that “KS2012 Forest” does not necessarily represent realistic dry deposition rates to forests and was rather included as lower limit for particle deposition from the KS2012 method in urban environments.

2.4 Experimental data from the measurement campaigns

We have used the measured particle number size distributions at a traffic station and at an urban background (UB) station, during campaigns in the cities Oslo, Rotterdam and Helsinki. The included campaign datasets were:

1. Rotterdam 2011, TRANSPHORM. Traffic site Bentinckplein and urban background location Zwartewaalstraat (6–19 May 2011) at Rotterdam, and the regional background station at Cabauw in the Netherlands (February–November 2011).

2. Oslo 2008, UFP-Oslo. Traffic site Smestad and urban background location Sofienberg park (12 December 2007 to 17 April 2008).
3. Helsinki, SAPPHERE case I. Traffic site at Herttoniemi and urban background location at Kumpula, Helsinki, 23–28 August 2003 (Hussein et al., 2007).
4. Helsinki, SAPPHERE case II. Traffic site at Herttoniemi and urban background location at Kumpula, Helsinki, 9–11 February 2004 (Hussein et al., 2007).
5. Helsinki LIPIKA. Traffic site at Herttoniemi and urban background location at Saunalahti bay, Helsinki, 17–20 February 2003 (Pirjola et al., 2006; Pohjola et al., 2007).
6. Helsinki, MMEA. Traffic site at Mannerheimintie and urban background location at Lääkärinkatu, Helsinki, 13–14 December 2010 (Pirjola et al., 2012).

The measured data for roadside and urban background in the TRANSPHORM campaign at Rotterdam, in the UFP-Oslo (“Measurements of ultrafine particles in Oslo”) campaign at Oslo, and in the SAPPHERE campaigns in Helsinki was obtained simultaneously. Whereas in the LIPIKA and the MMEA campaigns in Helsinki the measured data was obtained with the mobile laboratory “Sniffer” (e.g., Pirjola et al., 2004) at various locations during each measurement day. Quality control (QC) procedures in the measurement campaigns at Helsinki are described in the cited literature. Table 3 compiles the information on the size distribution data from the different campaigns in Rotterdam, Oslo, and Helsinki. In order to obtain an average size distribution for the respective traffic station and urban background station, either median or mean of measured time series of size distributions ($dN/d\log(D_p)$) were calculated, as specified in Table 3. A comparison of measured total PN concentrations between campaigns is shown in Fig. S1 (Supplement).

In Rotterdam, particle measurements were performed at the regional background station at Cabauw near Rotterdam and a traffic location at less than 5 m from the roadside (Bentinckplein) by two Scanning Mobility Particle Sizer (SMPS) instruments: one SMPS 3080 covering size diameters (D_p) 10–480 nm and a CPC 3775 (TSI Inc.) with a 50 % cut-off at 4 nm, and one SMPS 3034 with D_p 10–470 nm and a CPC 3010 (TSI Inc.) with a 50 % cut-off at 7 nm. The comparability of both SMPS was tested by parallel measurements, which resulted in a correlation coefficient (r^2) of 0.96. The results of the PNC measurements were corrected for the difference in comparability between both instruments. [Hourly averaged wind direction was used to select campaign data that was directly influenced by the traffic emissions in the street.](#) The traffic volume at Bentinckplein, which is a street canyon (width: 50 m; height: 12 m) was 35 000 vehicles per 24 h with 4 % trucks and buses. The urban background location Zwartewaalstraat in Rotterdam total

PN concentrations were measured by a Condensation Particle Counter (TSI 3007). The entire monitoring period at the regional background site was from February until December 2011. QC procedures were derived from the European Super-sites for Atmospheric Aerosol Research (EUSAAR) project (Asmi et al., 2011). These involved inter-comparison studies of monitoring instruments, 2-weekly checking of the sampling flow and annual calibration of the PN monitors by the manufacturer.

In Oslo, PN concentration and particle size distributions were measured at two stations in the municipality of Oslo for a four month period in winter 2008, using a Grimm 565 Environmental Wide Range Aerosol Spectrometer system (<http://www.GRIMM-Aerosol.com>). This system combines a Grimm 190 aerosol spectrometer OPC (Optical Particle Counter), and a scanning mobility particle sizer with a condensation particle counter (SMPS+C). The entire system in principle covers the range from 5 nm to 30 μm . Instruments were calibrated by the manufacturer prior to installation on site. Weekly zero filter test and other maintenance was carried out according to the manufacturers guide. In addition to automatic QC in the Grimm software, data from the two sites was compared and aligned with other air quality data from the respective sites. For the analysis of the Oslo campaign, only data from the SMPS was used and the smallest size bin was discarded. The traffic station (Smestad) was at a busy road with an average daily traffic (ADT) of around 50 000 vehicles. The traffic signal at the urban background station (Sofienberg park) showed a continuous shift of the size distribution peak towards larger sizes with decreasing air temperature, i.e. the maximum of the size distribution is shifted from 16 nm at 6 °C to 26 nm at -10 °C. Size distribution data measured at -8 to -12 °C was used as a separate dataset, UFP-Oslo Winter. The complete dataset from the period December 2007 to April 2008 is referred to as UFP-Oslo Tav.

For Helsinki, two cases from the SAPPHERE campaign, one case from the LIPIKA campaign (both at Herttoniemi), and one case at the city center from the MMEA campaign (Pirjola et al., 2012) were included. The roadside station near the highway Itäväylä at Herttoniemi is located about 6 km east of the center of Helsinki in a suburban area, with substantial local traffic. Particle measurements were performed with a differential mobility particle sizer (DMPS) at the background station and with a twin SMPS at the traffic site. Particle measurements during the LIPIKA campaign were conducted by Sniffer at various locations near the highway Itäväylä (Pirjola et al., 2006). The highway consists of six lanes, three lanes to both directions (total width of three lanes: 12 m), and a 6 m wide central grass area between the lanes to both directions, with a speed limit of 80 km h⁻¹. Particle size distributions in the range of 7 nm to 10 μm (aerodynamic diameter) were measured by Electrical Low Pressure Impactor (ELPI, Dekati Ltd.; 12 channels). Nucleation mode particles were measured with high size resolution by a Hauke

type SMPS (20 channels); measured size range was 3–50 nm (mobility diameter). The study period included 14 cases of measurements downwind of the highway Itäväylä from wind sector 1 (northwestern wind; Pirjola et al., 2006). The daily traffic density varied between 32 000–54 000 vehicles per day. Based on the traffic density information for year 2001, the vehicle fleet on the highway was composed of 85 % light duty vehicles (of which 11 % were diesel), 12 % vans (of which about 84 % diesel), and 4 % heavy duty vehicles (Hussein et al., 2007).

During the MMEA campaign (Pirjola et al., 2012) the mobile laboratory “Sniffer” was driving along the main street Mannerheimintie (MA) at the city center of Helsinki. MA is about 40 m wide and surrounded by 21 m tall buildings at both sides. The daily traffic flow was 36 300 vehicles day⁻¹ (of which ca. 10 % were heavy duty diesel vehicles). On 13–14 December 2010, the northeastern wind was perpendicular to MA, allowing traffic exhaust to be diluted freely between the buildings as in open environments. During rush hours, “Sniffer” was stopping around 10 min at 8, 28 and 56 m distances from the driving lane of MA downwind. Particle size distribution was measured by two SMPS (size ranges: 3–60 and 10–420 nm). The urban background particles were measured while Sniffer was standing at Lääkärinkatu, 300 m north from the measurement sites at MA.

A summary of the meteorological and dispersion conditions for the different campaigns is given in Table S1 in the Supplement. Measured meteorological data was not directly used in the model study of idealized scenarios, but are considered to be important for discussing the relevance of aerosol dynamical processes compared to dilution under real world conditions.

3 Results

3.1 Traffic-related particle size distributions in the campaigns

Measured PN concentrations based on hourly averages or 10 min averages (in case of the LIPIKA and MMEA campaigns) showed a wide range of PN concentrations (20 000–100 000 particles cm⁻³) for the traffic sites considered, depending on the season of the year, traffic density, and distance from the road. Size distributions of the measured datasets at the traffic sites from all campaigns were normalized by the measured total PN concentrations (Fig. 3). We have also calculated the average values of the size distribution curves for all traffic sites, denoted as “mean of traffic sites” (black curve in Fig. 3). This size distribution is considered to be representative for the traffic-influenced roadside aerosol in the considered cities.

The “mean of traffic sites” distribution is characterized by a fraction of ultrafine particles (D_p : 10–100 nm) and accumulation mode (Acc) particles (D_p : 100–500 nm) of

80 and 4 %, respectively, while 16 % of the particles were below 10 nm. SAPPHIRE Case I had the highest fraction of < 10 nm particles (38 %); in Rotterdam < 10 nm particles were not measured. For the other campaigns fraction of < 10 nm particles was in the range 6–19 %. The fraction of ultrafine particles was 60 % for SAPPHIRE Case I and 74–87 % for all other campaigns. The fraction of Acc particles was smallest for the SAPPHIRE campaigns (≈ 1 %), and between 4 and 9 % for the other campaigns in Helsinki and Oslo.

~~The~~ From a three-modal fit to the mean traffic-related size distribution ~~shows with the MAFOR model (following the procedure described in section 2.2)~~ three distinct modes with mean diameter at 17 nm, 85 nm, and 250 nm, respectively, were obtained. The measured average size distributions from the campaigns LIPIKA and MMEA in Helsinki, as well as UFP-Oslo Tav exhibited a similar shape as the mean traffic-related size distribution. The distribution of SAPPHIRE Case II also resembled the constructed distribution but did not show significant particle numbers with diameter > 100 nm. Ultrafine particles measured at the traffic sites in the campaigns were most likely from fresh vehicle exhaust emissions. Particles emitted from diesel engines are usually in the size range 20–130 nm (e.g., Kittelson, 1998), somewhat larger than those emitted from gasoline engines, typically being in the range 20–60 nm (Harris and Maricq, 2001; Ristovski et al., 2006). Comparing campaigns in Helsinki, MMEA size distribution peaked at 20–40 nm, while LIPIKA and SAPPHIRE size distributions peaked at 8–25 nm. The higher fraction of heavy duty diesel vehicles at Mannerheimintie (10 %) compared to highway Itäväylä (4 %) could be one possible reason for the peak at relatively larger sizes in MMEA. Different driving conditions may also have contributed to the difference in peaks; at Mannerheimintie rush hour limited the speed to 20–25 km h⁻¹ with stop-and-go driving, whereas at Itäväylä vehicles could drive 60–80 km h⁻¹ very fluently.

The peak of the size distribution for UFP-Oslo Winter was below 10 nm and for Helsinki SAPPHIRE Case II the peak was below 20 nm. Both campaigns were during winter in Northern Europe; ambient temperature in UFP-Oslo Winter ranged from -12 to -8 °C and SAPPHIRE Case II ranged from -15 to -4 °C. The relative increase of nanoparticle numbers in cold conditions may be the result of increased nucleation of semi-volatile compounds post-emission and decreased saturation ratio of the condensing vapors that tend to enhance initial particle growth. It has also been reported that particle emission from light duty diesel vehicles are influenced by low ambient temperatures during the vehicle cold-start (Mathis et al., 2005). However, the primary effect of a cold environment on vehicle cold-start is a number increase of semi-volatile nucleation mode particles, not of the solid particles in the exhaust (Maricq, 2007).

Accumulation mode particles have a longer lifetime in the atmosphere, it is therefore likely that they are either a result

from ageing processes on the urban time scale or that they are from short-range or long-range transport of aerosols. Since the size distribution measurements were carried out at traffic sites at distances of a few meters from busy roads, the measured aerosols are expected to be mainly influenced by primary traffic emissions. However, for the campaigns at Rotterdam and Oslo, measurements were not always downwind from the traffic emissions, and could be influenced also by other local particle sources and secondary pollution from local traffic.

The number size distribution at Rotterdam showed an exceptionally broad peak mode at 30–70 nm and a large fraction of Acc particles. Other sources, such as emissions from harbor activities and refineries situated in the harbor area, could have contributed to the relatively high fraction of Acc particles at Bentinckplein. Average wind direction during the Rotterdam campaign was from southwest, from the direction of the harbor area “Nieuw Mathenesse”. At an average wind speed of 3.6 m s⁻¹, the travel time of particles from the harbor and refineries to the traffic site was about 15 min. Ships emit large amounts of particles larger than 20 nm, which consist of soot and volatile material (e.g. Fridell et al. 2008; Petzold et al., 2008; Kasper et al., 2007). Number size distributions of ship emissions in the ports of Helsinki and Turku (Finland) measured by “Sniffer” showed peaks at around 20–30 and 80–100 nm (Pirjola et al., 2014).

Truck traffic in the harbor during loading/unloading of ships also leads to increased particle numbers (Pirjola et al., 2014). Measurements downwind of a harbor at Rotterdam showed that 61 % of the PN concentration was in the size range 25–100 nm while it was 48 % downwind of a motorway (Keuken et al., 2012). Condensation of vapors onto particles emitted from ships during their transport to the traffic site might explain the relatively high number concentration of Acc particles in the Rotterdam campaign. We note that the measured PN concentration of Acc particles in Rotterdam was similar as in Oslo but lower than during the LIPIKA and MMEA campaigns in Helsinki.

3.2 Comparison of the model predictions against the campaign measurements

The evolution of the particle size distribution as function of time up to one hour for all the cases, and by definition, following increasing distance from the roadside (idealized scenario, Sect. 2.2), was studied with the aerosol dynamics box model and compared to measured size distributions data from the respective campaigns. Figure 4 and Fig. S2 in the Supplement show the comparison of modelled number size distributions from the idealized scenarios and the measured number size distribution at the roadside and at the urban background site for campaigns at Oslo, Rotterdam, and Helsinki. As the air parcel containing vehicle exhaust leaves street scale it is assumed to be advected over a homogenous surface in the neighborhood with a length scale of a few kilometers and

further to the city scale. In the model, initial particle concentrations in all size bins were diluted with background air containing particles with a size distribution that matched the measured size distribution at the urban background site.

The modelled number size distribution calculated for moderate dispersion conditions after ~ 10 min of travel time, corresponding to a distance of 3600 m from the roadside, was generally in good agreement with the size distribution measured at the urban background site. Dilution was the dominant process changing the size distribution between roadside and urban background, as shown by the continuous decrease of concentrations with time. For the campaigns Helsinki SAPPHIRE Case I (Fig. 4c) and Case II (Fig. S2c in the Supplement), as well as Helsinki MMEA (Fig. 4d) the maximum of the particle size distribution was moved to larger diameter. For instance, the modelled size distribution in Helsinki SAPPHIRE Case I showed an increase of the nucleation mode peak diameter from 10 to 18 nm within a distance of 3600 m. This behavior can be explained by dilution transforming the shape of the roadside distribution into the (prescribed) shape of the urban background distribution. UFP-Oslo Winter (Fig. 4a) shows signs of growing small particles by condensation, with peak diameter moving from ca. 5 to 8 nm.

Model simulations using different wind speed and dilution parameters, representative for different dispersion conditions (efficient, moderate, inefficient dispersion; as given in Table 1), were performed for each campaign. The contribution of the various aerosol dynamic processes to the change of total PN at a given travel time was derived by switching off the respective aerosol process in the model calculation. The percentage PN change due to a specific aerosol dynamic process was obtained by division of the total PN change with the total PN change when all processes were considered (PN change defined as difference between initial total particle number and total particle number after a certain travel time). Table 4 summarizes the PN change after 30 min of travel time due to each selected aerosol process, [and also to dilution](#), in each of the campaigns for efficient, moderate and inefficient dispersion conditions. The considered aerosol processes accounted for PN concentration changes of up to 20 % after 10 min and up to ~ 30 % after 30 min (Fig. 5), respectively.

According to the results shown in Table 4, coagulation and dry deposition were relevant aerosol dynamic processes for particle removal in the Rotterdam campaign whereas dry deposition was the predominant aerosol process in the Oslo campaign. Due to identical dispersion conditions and wind speeds used in the comparison, the observed difference is attributed to the different shapes of the initial size distribution measured at the roadside station and the background particle size distributions. The larger fraction of particles with diameter > 25 nm measured at Rotterdam (accounting for 73 % of total PN) explains the higher relevance of coagulation compared to the Oslo campaign. Particles with larger diameter

more efficiently scavenge the small (< 25 nm diameter) particles by coagulation.

For the LIPIKA and MMEA campaigns coagulation was the most important aerosol process for particle removal during low wind speed. The size distributions for LIPIKA and MMEA (green and cyan lines in Fig. 3a) peak in a size range between 10–40 nm diameter and show a higher fraction of Acc particles than the SAPPHIRE distributions. Obviously, coagulation becomes a relevant PN loss process once large numbers of particles below 50 nm diameter from vehicle exhaust emissions (e.g. ca. $92\,000$ particles cm^{-3} at roadside, LIPIKA) are accompanied by a significant PN fraction of larger particles, which originate either from other local sources or from secondary particle formation within the urban area. These results are in agreement with the ones by Kerminen et al. (2007) who estimated that the lower and upper limits for the inter-modal coagulation time scale during the rush hours were 15–20 and 60–80 min, respectively. During the night, the inter-modal coagulation time scale was 2–3 times that during the rush hours (Kerminen et al., 2007).

The contribution of dry deposition and coagulation to total PN losses is comparable to those determined in previous measurements and model studies. City scale modelling studies with a multi-plume aerosol dynamics and transport model indicated that coagulation and dry deposition can cause total PN losses of 15–30 % between roadside measurement and urban background measurement in Copenhagen (Ketznel and Berkowicz, 2005). Gidhagen et al. (2005), using an urban dispersion model that included aerosol dynamics in Stockholm, concluded that in terms of time-averaged PN concentration, dry deposition may yield particle number losses of up to 25 % in certain locations, while coagulation contributed little to PN losses. During particle peak episodes the removal by dry deposition and coagulation was more substantial (Gidhagen et al., 2005).

Condensation and evaporation of vapors as such is not expected to change the total number concentrations, however can modify the particle size distributions and particle volume. In this study a significant increase of PN (by up to 8 % after 30 min travel time) was evident under inefficient dispersion conditions, when condensation was considered in addition to coagulation and dry deposition. The reason could be the competition between condensation and coagulation. As the air parcel moves away from the roadside, condensation of [n-alkane-condensable organic](#) vapors leads to rapid growth of small particles to larger diameters at which they are less affected by coagulation loss. In addition, dry deposition velocity decreases with increasing diameter between 1 and 100 nm. Hence particles grown by condensation of [n-alkanes-condensable organic vapors](#) will be less affected by deposition.

Aerosol dynamics are less relevant under conditions with efficient dispersion. When efficient dispersion occurs in the urban canopy, dilution by background air is the only effective process reducing PN concentration with distance from

the roadside. In such situations (dilution parameters: $a = 80$, $b = 0.9$) aerosol processes account for PN concentration changes of less than 3 % after 10 min and PN concentration changes of less than 6 % after 30 min, hence modelling of PN as passive tracer is adequate. According to the previously published model study at the Dutch motorway A16; the particle size distribution at $D_p > 40$ nm is not further altered by aerosol processes after a distance of 1000 m from the roadside (Keuken et al., 2012). The distance where the PN level reaches background concentrations depends on dispersion conditions. Background PN levels were reached approximately (within an accuracy of ± 5 %) after 1740, 900, and 160 m in distance from the road for inefficient, moderate, and efficient dispersion conditions, respectively, in box model simulations using the Rotterdam campaign data.

3.3 Effect of dry deposition of particles to different surface types

The sensitivity of modelled PN concentrations towards dry deposition of particles on various surface types and roughness conditions were studied in the campaigns Rotterdam TRANSPHORM and UFP-Oslo Tav under moderate dispersion conditions. Two different deposition methodologies, KS2012 and H2012 (detailed description in Sect. 2.3), were applied. Results from the sensitivity tests are summarized in Table S2 in the Supplement.

Between different KS2012 cases, calculated dry deposition velocity, ν_d , spanned about one order of magnitude for all particle diameters. Case “KS2012 Urban” corresponded to the surface characteristics of typical urban environments, i.e. streets and buildings, as used for the reference model runs with MAFOR. KS2012 parameterization was not sensitive to changes of friction velocity or roughness length within a typical urban range of values: reducing friction velocity (case “Low friction”) or increasing roughness length (case “High roughness”) resulted in negligible (≤ 0.1 %) change of PN loss due to dry deposition compared to case “Urban”. Over grassland and forest, modelled PN concentration changes due to dry deposition were smaller by 30 and 50 %, respectively, than over urban surfaces.

Using the deposition methodology H2012 for case “Urban” resulted in 40–50 % lower PN losses by dry deposition compared to KS2012. Between different H2012 cases calculated ν_d spans about two orders of magnitude for accumulation mode particles (D_p 100–1000 nm) which can be attributed to the fact that surface roughness becomes a dominant factor in collecting aerosol particles efficiently for that particle size range, where neither diffusion nor inertial processes are significant processes. H2012 parameterization was very sensitive to changes of friction velocity or roughness length. The contribution of dry deposition to PN changes varied by roughly a factor of 5 for Rotterdam and by a factor of 3–4 for Oslo due to changing roughness conditions.

It has been evident in the literature (e.g., Guha, 1997), that surface roughness can increase ν_d by up to two orders of magnitudes, in the size range between particle diffusion regime and diffusion-impaction regime, compared to a smooth surface. This behavior is reflected by the H2012 parameterization, but not by the KS2012 parameterization.

3.4 Effect of condensation and evaporation of n-alkane organic compounds

~~The effect of condensation of two n-alkanes with varying gas-phase concentrations on total PN concentration and on the size distribution was tested. Variation of the roadside mixing ratio of n-alkanes between 1–4 changed the total PN concentration after 30 travel time by less than 1.55 at the most, for the campaigns Rotterdam, UFP-Oslo Tav, UFP-Oslo Winter, and Helsinki LIPIKA under moderate dispersion conditions. Therefore, PN concentration can be considered invariant to variations of the concentration of condensable vapors within the above mentioned concentration range, if dispersion is sufficiently efficient.~~

Inspection of the modelled evolution of number size distributions in simulations of ~~LIPIKA-Helsinki LIPIKA (moderate dispersion)~~ revealed that variation of ~~n-alkane organic vapor~~ concentration mainly affected the nucleation mode. ~~Roadside n-alkane concentration of 1 and 3 caused an increase of the nucleation mode diameter from 5 to 5.2 and 7~~ Compared to a simulation without condensation and evaporation, the reference case with 0.5, respectively, ~~in a ppb condensable organic vapors (sum of C22 and C28 gas-phase concentration with ratio 50:50) did not significantly change the number size distribution in a distance of 240 m from the road compared to a simulation without condensation (Fig. S3a) but doubled the mass of 10 nm particles (Fig. S3b). When the concentration of condensable organic vapors was reduced to 0.05 ppb or below, condensation became completely negligible.~~ Our sensitivity results are qualitatively in line with the study of Pohjola et al. (2007) who, based on measured PN data and the aerosol dynamics model MONO32 (Pirjola et al., 2003), found that the influence of condensation on PN concentrations was negligible on a distance scale of 200 m near a major road in Helsinki. For example, presence of a condensable organic compound with ~ 0.4 ppb increased the diameter in the two smallest particle size modes by only 14 and 1.9 %, respectively (Pohjola et al., 2007).

An extreme case to test the relevance of condensing n-alkane vapor and its effect on traffic-related size distributions was the Oslo Winter data (Fig. 4a). Under inefficient dispersion conditions, modelled total PN concentration in UFP-Oslo Winter was 2 ~~and 10~~ % higher after a distance of 240 m with 0.5 ~~and 3 n-alkane, respectively,~~ ppb ~~condensable organic vapors,~~ compared to a simulation without condensation. ~~The growth rate of particles with $D_p < 10$ Growth of particles by condensation caused a shift~~

of the nucleation mode diameter from 5.9 to 8.8 nm was ~ 12 for 0.5 n-alkane (Fig. S4a), thus increasing the survival probability of the very small particles. Two factors enhanced the effect of n-alkane condensation on the changing size distribution: first, the low temperature causing low vapor pressure (a factor of 90 smaller than at 10 °C) and second, the high fraction of initially present particle numbers with diameter below 10 nm. Growth of particles by condensation of n-alkanes caused a shift of the size distribution to larger diameters, thus increasing the survival probability of very small particles. For lower concentrations of condensable organic vapors, 0.05 ppb and 0.005 ppb, no significant particle growth was found (mass size distribution in Fig. S4b). Evaporation of particles < 10 nm diameter occurred at 0.005 ppb, when changing the organic fraction of nucleation mode particles to 100% C22, i.e. assuming higher volatility of vehicular nanoparticles that formed post-emission. Interestingly, the evaporated material partly re-condensed to particles with diameter > 100 nm within 240 m distance from the roadside (blue dashed line in Fig. S4a and Fig. S4b).

The growth of small particles ($D_p < 10$ nm) at 0.5 ppb condensable organic vapors to larger sizes within a distance of 240 m in campaign UFP-Oslo Winter corroborates the finding in a curbside study by Zhang et al. (2004) at two freeways in Los Angeles, that a large number of emitted sub-6 nm particles can grow substantially 30–90 m downwind. However, it cannot be excluded that downwind emissions of vehicle pollutants or oxidized volatile organic compounds (VOC) contributed to the observed growth.

Model simulations of the idealized scenario suggest that evaporation could be an important process, altering the particle size distribution in urban micro-environments, if the semi-volatile vapor and also the nanoparticles forming post-emission were assumed to have the same or higher volatility as the n-alkane C22. Dall'Osto et al. (2011) analyzed observations of particle size distributions from London and reported a reduction in the size of nucleation mode particles during advection from a major highway into the cleaner environment of a park, indicating evaporative loss of semi-volatile constituents during travel times of around 5 min. Harrison et al. (2016), for the same location, found most rapid evaporation to occur at higher wind speeds, associated with shorter travel times, but cleaner air.

3.5 Effect of fractal geometry of soot particles and van der Waals forces

Model calculations for the idealized scenario assumed that all particles are spherical. However, soot particles emitted from diesel vehicles are fractal-like aggregates consisting of nano-sized primary spherules. The effect of fractal geometry on coagulation was taken into account by considering the effect on radius, diffusion coefficient and the Knudsen

number in the Brownian collision kernel. In order to test how fractal geometry of soot particles affects the modeled particle size distribution and PN concentrations, the coagulation kernel in MAFOR was modified by assuming that the collision radius is equal to the fractal (outer) radius, r_f , defined as (Jacobson and Seinfeld, 2004):

$$r_{f,i} = r_s \times n_{s,i}^{1/D_f} \quad (3)$$

Where $n_s = v_i/v_s$ is the number of primary spherules in the soot aggregate, v_i is the volume of the aggregate, treated as if it were spherical, r_s is the radius of spherules and v_s is the volume of a spherule that makes up the aggregate, and D_f is the fractal dimension. Soot particle density was corrected as explained in Lemmetty et al. (2008).

Van der Waals forces and viscous interactions affect the coagulation rate of small particles. It has been shown that van der Waals forces can enhance the coagulation rate of particles with diameter < 50 nm by up to a factor of five (Jacobson and Seinfeld, 2004). To evaluate how neglecting the two forces affected the particle size distribution evolution, a correction factor $V_{E,i,j}$ accounting for van der Waals and viscous forces was applied to the Brownian collision kernel, $K_{i,j}^B$, for the collision of particle of size bin i with particles of size bin j in the MAFOR model:

$$K_{i,j}^{corr} = K_{i,j}^B \times V_{E,i,j} \quad (4)$$

It is referred to section S3 in the Supplement for details of the implementation. The effect of van der Waals forces and viscous interactions as well as fractal geometry on the Brownian collision kernel is shown in Figure S5. Parameters of the fractal geometry adapted from Jacobson and Seinfeld (2004), $r_s = 13.5$ nm and $D_f = 1.7$, resulted in stronger enhancement of the coagulation rate for collisions with a 10 nm particle than the parameters ($r_s = 2.5$ nm and $D_f = 2.5$) adapted from Lemmetty et al. (2008).

The combination of both effects substantially enhanced the loss of nanoparticles in the simulation of the evolution of the roadside aerosol. For Helsinki MMEA, inefficient dispersion conditions, the enhancement was similar for the two effects, separately, i.e. spherical particles with van der Waals and viscous forces versus fractal particles (Fig. S6). The combined effect increased the loss of total PN by 15% compared to the reference simulation (coagulation of spherical particles by Brownian motion) in 600 m distance from the road.

3.6 Uncertainties of the aerosol treatment in the idealized scenario

Computation of the aerosol evolution between the roadside station and the neighborhood environment with the idealized

scenarios involves several assumptions and uncertain parameters. An uncertainty analysis was performed to quantify the errors associated with the determination of the contribution of the respective atmospheric processes to the change of total PN. Errors were determined based on simulations for the mean traffic-related particle distribution (section 3.1) under inefficient dispersion conditions after 30 min travel time (Figure 6).

Fractal parameters of Jacobson and Seinfeld (2004) were chosen for the evaluation of the uncertainty of the coagulation process. The combined effect of fractal geometry and van der Waals plus viscous interactions was taken into account, resulting in an error of +130 %, roughly corresponding to a doubling of the contribution of coagulation to PN losses between roadside station and the neighborhood.

Measurements of dry deposition velocities of particles for one particular surface type generally vary by one order of magnitude for a given particle size range of a half logarithmic decade (e.g. for different grassland and forest types; Petroff et al., 2008). Dry deposition velocities for total PN ($0.2\text{--}0.9\text{ cm s}^{-1}$), calculated with the reference case parameterization “KS2012 Urban”, correspond to the reported range of measured deposition velocity values. Here, dry deposition velocity was scaled by factor 2 and 1/5 to evaluate the uncertainty of the dry deposition process due to literature span of measured velocities. This resulted in an error margin from -76% to $+64\%$ for the contribution from dry deposition.

For the mean traffic-related particle distribution, evaporation contributed 0.3 % to PN losses when assuming 0.005 ppb C22 + C28 and 100 % C22 in $< 10\text{ nm}$ particles. Condensation and evaporation are uncertain processes due to the lack of measurements of the gas-phase and particle phase concentrations of condensable compounds at the roadside station. Oxidation of VOC from vehicular emissions may provide an additional source of condensable material on the neighborhood scale. However, oxidized VOC in the background air are expected to condense on the particles of the accumulation mode, increasing their volume, rather than changing PN concentrations.

Additional emissions of particles on the travel path between the roadside station and the background were not considered in the idealized scenario. Since the dilution process in the model simulations was constrained with the measured size distribution at the background, the influence of additional particle emissions has been implicitly taken into account. However, if there are strong emission sources of ultrafine particles on the way, the momentary particle size distribution might be perturbed. The error due to fluctuations of the dilution rate caused by additional emissions was estimated to be -4% .

The main uncertain parameter in the applied dilution scheme [Eqs. 1 and 2] is the initial plume height at the

roadside, $H_{m,0}$. Doubling $H_{m,0}$ resulted in a small error (-1%) of the contribution of dilution to PN losses.

It is concluded that errors due to the design of the scenario (dilution scheme, additional emissions) are relatively small compared to the magnitude of the potential contribution of coagulation and dry deposition to total PN losses between roadside station and the neighborhood environment.

3.7 The recommended simplified parametrizations of aerosol processes

As a first step of the implementation of a treatment of aerosol processes in urban air quality models, a separation of PN to various size categories is required. Three particle number concentration (PNC) categories were defined, as follows: PNC₁ ($8.5\text{ nm} < D_p < 25\text{ nm}$; “Nucleation mode”), PNC₂ ($25\text{ nm} < D_p < 100\text{ nm}$; “Aitken mode”), and PNC₃ ($100\text{ nm} < D_p < 500\text{ nm}$; Acc). The upper boundary of 500 nm is justified because the contribution of large particles (defined here as $> 500\text{ nm}$) to total PN concentration from vehicular exhaust is negligible.

A first-order rate law for PNC in the three size categories (index k) was derived for number concentration change with time due to dry deposition:

$$\ln\left(\frac{\text{PNC}_k}{\text{PNC}_{k,0}}\right) = -\frac{\overline{v_{d,k}}}{H_m} \times t \quad (5)$$

Where $\text{PNC}_{k,0}$ is initial concentration. The average dry deposition velocity $\overline{v_{d,k}}$ was determined by fitting a linear regression model to the time series of modelled PNC₁, PNC₂, and PNC₃, from a MAFOR run initialized with the size distribution “mean of traffic sites” (see Sect. 3.1) and dry deposition as only process.

In Eulerian models, dry deposition of particles can be implemented according to:

$$\left.\frac{d\text{PNC}_k}{dt}\right|_{\text{depo}} = -\text{PNC}_k \frac{\overline{v_{d,k}}}{H_{\text{grid}}} \quad (6)$$

Here H_{grid} is the depth of the lowest grid level. Table 5 provides average dry deposition velocity derived from the fit to Eq. (35). If applying the parameterization in a Gaussian model then the deposition velocity is usually used to influence the reflection parameter (α) for the reflected plume, e.g. using the following equation (Hanna et al., 1982):

$$\alpha_k(x) = 1 - \frac{2\overline{v_{d,k}}}{\nu_t + \overline{v_{d,k}} + (Uh - \nu_t x) \times \sigma_z^{-1} \left(\frac{d\sigma_z}{dx}\right)} \quad (7)$$

Where h is the effective plume rise and σ_z is the vertical dispersion coefficient. Gravitational settling velocity ν_t in Eq. (57) can be neglected (set to zero) since only particle sizes below 500 nm are relevant for determining PN concentrations.

Coagulation of particles can be implemented, rate according to:

$$\left. \frac{d\text{PNC}_k}{dt} \right|_{\text{coag}} = -\text{PNC}_k \times (\overline{K_{\text{coag},k}} \times \text{PNC}_k^0) \quad (8)$$

Where $\overline{K_{\text{coag},k}}$ (in units $\text{cm}^3 \text{s}^{-1}$) is the average coagulation coefficient in a size category k derived from MAFOR calculations, provided in Table 5. The expression in Eq. (68) neglects the production terms of coagulation. The superscript 0 indicates the number concentration at the start of the time step calculation in Eulerian models. For Gaussian models this is the calculated concentration before the inclusion of the decay rate due to any physical and chemical processes considered for PNC.

Dry deposition and coagulation terms are applied separately for the three PNC classes. This means that coagulation between different size categories is not calculated explicitly with the parameterization. However, inter-modal coagulation is partly taken into account through the average coagulation coefficient derived from a model calculation that included coagulation between all size bins. Since the average coagulation coefficient of a given size category depends on the number concentrations in the other size categories, the predicted coagulation loss for PNC_1 and PNC_2 of roadside size distributions that differ from the size distribution "mean of traffic sites" will be somewhat inaccurate.

The accuracy of the presented parameterization for aerosol processes for prediction of PN concentrations is limited by three factors: first, by the averaging of process parameters over a certain size range; second by the simplified treatment of coagulation; and third by neglecting condensation and evaporation. The uncertainty of the parameterization was studied by comparison with PN concentrations resulting from a detailed aerosol dynamics calculation with MAFOR as reference. For the case "mean of traffic sites", calculated total PNC after 10 min travel time deviated from the reference solution by only 1 %, implying that the error introduced by size-averaged process parameters is negligible. When applying the parameterization to campaign data, the deviation of the total PNC to the reference solution was up to 10 %. UFP-Oslo Winter was excluded from the evaluation due the obvious influence of condensation as shown in Sect. 3.4. Increasing the number of PNC size categories is expected to reduce the error due to neglecting coagulation between size categories. A parameterization with six PNC categories resulted in a deviation to the reference solution by only up to 5 % (Table S3). In addition the parameterization is uncertain due to assumptions about particle shape, neglecting van der Waals forces as well as inaccurate measured dry deposition velocities. It is however not affected by the specific treatment of dilution in the idealized scenarios because the simplified PNC parameterization was derived with only one aerosol process activated.

Results of PN concentration modelling for Oslo using the simplified parameterization for dry deposition and coagulation in the Eulerian urban dispersion model EPISODE (Slørdal et al., 2003) are presented in Kukkonen et al. (2015).

4 Conclusions

We have evaluated the significance of aerosol processes during the atmospheric transport of particles on a timescale of one hour, i.e., from the roadside to the neighborhood scale, based on measurement campaigns and modelling in three European major cities. Most of the previous studies have been based on the results of one specific measurement campaign. Our analysis included size distribution data from several campaigns that were performed in different urban settings (street canyon, highway, and suburban main road), exhibiting different traffic characteristics and dispersion conditions, at different times of the year. Monitoring was done with stationary or mobile platforms, and size distributions were measured with various aerosol instruments. An advantage of this study is therefore that the results and conclusions about the relevance of aerosol processes do not depend critically on the specific conditions in terms of emissions, meteorology, and dispersion of a single campaign.

We have used the one-dimensional multicomponent aerosol dynamics model MAFOR to predict PN concentrations and number size distributions. We coupled this one-dimensional model with a simplified treatment of the dilution of particle numbers. Three dispersion cases that are common for northern and central Europe were simulated, ranging from stagnant conditions to efficient dispersion. Despite the simple representation of atmospheric dispersion, size distributions predicted by the aerosol model after approximately 10 min of travel time ($U = 3 \text{ m s}^{-1}$) compared well with the size distributions measured at the respective urban background sites.

A limitation of this study was that the chemical transformation of gas phase compounds was not taken into account. It was not necessary to evaluate the nucleation of gas-phase vapors to form new particles, as the model simulations of this study were started at roadside conditions (instead of the exit of the tailpipes of vehicles). It was investigated how condensational growth might influence the shape of the particle size distribution between roadside and the neighborhood scale. Condensational growth did not substantially affect the temporal evolution of the PN concentrations in the presence of efficient and moderate dispersion conditions. The present study shows that growth by condensation can increase the survival probability of very small particles. Condensation removes the smallest particles ($D_p < 15 \text{ nm}$; Ketzler and Berkowicz, 2004) from the size distribution by growing them to larger sizes, which are less affected by removal through dry deposition and coagulation. **However, a significant increase of An increase of the PN concentra-**

tion was found between roadside and the neighborhood scale due to condensational growth under inefficient dispersion conditions. This result differs from that in some previous studies, which stated that the total number concentration between roadside and ambient is not substantially influenced by condensation and evaporation (e.g., Ketznel and Berkowicz, 2004).

It was found that dry deposition and coagulation of particles were generally relevant for PN concentrations on timescales of the neighborhoods. However, as expected, these processes were less relevant in efficient dispersion conditions. The relative relevance of coagulation compared to dry deposition depended on the concentrations of nanometer size particles (< 50 nm).

Coagulation is especially important for the removal of nanoparticles, in this study defined as particles of the sizes 8–25 nm, which accounted for 70 % of the total PN of the mean traffic-related aerosol. ~~The timescale of coagulation is similar to that of dry deposition for the nanoparticles.~~

The typical time scale of dry deposition of particles with 8–25 nm diameter in the urban environment using different deposition schemes was 0.5–3 h. Average dry deposition velocities were in the range of 0.2–0.9 cm s⁻¹; ~~this range is similar with the range of 0.6–0.9 cm s⁻¹ estimated by Ketznel and Berkowicz (2004).~~ Large differences between the two considered deposition schemes were evident for very rough urban surfaces and for forests. Most of the urban environmental surfaces are rough, and the influence of surface roughness on the dry deposition seems to be pronounced, especially for those particles that are not deposited efficiently by diffusion and inertial processes (Hussein et al., 2012). A future refinement of the ~~dry-deposition-parameterization~~ parameterization of dry deposition for use in urban models (Eq. (6)) should take into account the dependence of the deposition velocity on the underlying urban surface. The lack of measurements of deposition velocities for ultrafine particles to various urban surfaces currently impedes such a refinement.

A simple parameterization of dry deposition and coagulation for urban air quality models was derived. The parameterization of ~~aerosol processes can predict dry deposition and coagulation can predict total~~ particle number concentrations between roadside and the urban background within an inaccuracy of ~ 10 %. ~~The main source of inaccuracy is the simplified treatment of coagulation, which does not explicitly account for coagulation between size categories., compared to simulations with the fully size-resolved MAFOR model.~~ Inclusion of more PN data ~~form from~~ other traffic sites and cities might improve the overall accuracy of the parameterization. Potentially, the process of condensational growth might be included in the framework of the current PN parameterization. However, new particle formation events in the urban background air, frequently associated with a prominent nucleation mode with peak diameter $D_p < 10$ nm (Hussein

et al., 2014), probably cannot be sufficiently accurately represented by such a simplified parameterization.

Computation of the aerosol evolution between the roadside station and the neighborhood environment involved several assumptions and uncertain parameters. Due to the lack of measurements of the gas-phase and particle phase concentrations of semi-volatile compounds during the studied campaigns, the contributions from condensation and evaporation of condensable vapors emitted with the vehicle exhaust to PN changes are uncertain. Due to the wide span of measured deposition velocities in literature, the contribution from dry deposition to PN losses has an uncertainty range from -76 % to +64 %. The removal of nanoparticles by coagulation is further enhanced when considering the fractal nature of soot aggregates and the combined effect of van der Waals and viscous interactions. Taking into account these effects doubles the contribution of coagulation to PN losses between roadside and neighborhood.

Mitigation policies for ultrafine particle pollution in the future would require the need for operational modelling of PN on urban scales. The presented simplified parameterization can be implemented in both Gaussian and Eulerian models. However, it would be recommendable to evaluate such modelling systems against measured PN data in various urban settings.

Code availability

The computer code of the MAFOR aerosol dynamics model, version 1.8, can be made available upon request (contact: Matthias Karl on email matthias.karl@hzg.de). The code is written in FORTRAN 90.

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Table 1. Meteorological and dilution parameters used in the numerical computations on the evolution of the particle size distribution and PN between roadside and neighborhood time scales. Notation: U = wind speed at a height of 10 m, H_m = initial plume height at the roadside station, a , b = Parameters of the particle dilution parameterization ($y = a \times x^{-b}$, where x is the distance from roadside in meter). The moderate dispersion conditions were used for the reference case.

Dispersion cases	Wind speed	Initial plume	Dilution parameter	
	U [m s ⁻¹]	$H_{m,0}$ [m]	a	b
Moderate dispersion	3.0	0.88 <u>0.9</u>	40.0	0.5
Efficient dispersion	4.0	0.67 <u>0.7</u>	80.0	0.9
Inefficient dispersion	1.0	2.59 <u>2.6</u>	20.0	0.2

Table 2. Dry deposition of particles to urban surfaces. Parameter values used in the modelling of the reference case (all campaigns) and in the sensitivity cases for the dry deposition process. Notation: u^* = friction velocity, z_0 = roughness height, d_{col} = effective collector size, z_C = canopy height, F^+ = effective roughness length. Values for F^+ were adopted from Hussein et al. (2012) for corresponding surface and vegetation types.

Case	Surface type	u^* [cm s ⁻¹]	z_0 [m]	d_{col} [cm]	z_C [m]	F^+ [-]
Urban	Street and building	133	0.13	0.20	10.0	0.55
Low friction	Street and building	27	0.13	0.20	10.0	0.55
High roughness	Street and building	133	1.00	0.20	10.0	1.60
Green area without trees	Grassland	36	0.01	0.40	0.20	0.50
Green area with forest	Deciduous forest	75	1.00	1.00	12.0	2.25

Table 3. Campaign number size distribution data used in this study. Notation: RT = roadside traffic site, ST = street canyon traffic site, UB = urban background, RB = regional background.

City	Campaign / case	Time period	Classification of location	Name of station	Data averaging method	Average total PN [particles cm ⁻³]	References
Rotterdam	TRANSPHORM	6–19 May 2011	Suburban	Bentickplein (ST)	Mean	20 300	This Study
				Zwartewaalstraat (UB)	$dN/d\log(D_p)$	14 100	
				Cabauw (RB)		10 200 ^a	
Oslo	UFP-Oslo	12 Dec 2007	Suburban	Smestad (RT)	Mean	24 000	This Study
		– 17 Apr 2008		Sofienberg park (UB)	$dN/d\log(D_p)$ ^b	9300	
Helsinki	SAPPHIRE case I	23–28 Aug 2003	Suburban	Highway Itäväylä, Herttoniemi (RT) at 65 m distance Kumpula (UB)	Median $dN/d\log(D_p)$ ^c	32 000 7200	Hussein et al., 2007
Helsinki	SAPPHIRE case II	9–11 Feb 2004	Suburban	Highway Itäväylä, Herttoniemi (RT) at 65 m distance Kumpula (UB)	Median $dN/d\log(D_p)$ ^c	55 100 11 300	Hussein et al., 2007
Helsinki	LIPKA case I	17 Feb 2003	Suburban	Highway Itäväylä, Herttoniemi (RT) at 65 m distance Saunalahti bay, Herttoniemi (UB)	1 data record (10 min average) $dN/d\log(D_p)$	486 129 <u>400 600</u> 13 400	Pirjola et al., 2006 and Pohjola et al., 2007
Helsinki	MMEA	9–11 Feb 2004	Suburban	Mannerheimintie (ST), Herttoniemi (RT) at 0 m (or 8 m) distance	1 data record (10 min average)	51 000 (25 800)	Pirjola et al., 2012
				Lääkärintkatu (UB)	Mean $dN/d\log(D_p)$	13 700	

^a Annual average (2011) at Cabauw.

^b Weekdays, between 6 a.m. and 3 p.m.

^c Excluding night-time between 10 p.m. to 6 a.m.

Table 4. Contribution of aerosol-processes coagulation (Coag), dry deposition (Dry dep) and condensation (Cond) and dilution (Dil) to percentage change of PN concentration (%) between roadside station and neighborhood environment after 30 min transport time for different dispersion conditions (i.e. $(\Delta\text{PN}_{\text{process}}/(\text{PN}(\text{initial}) - \text{PN}(\text{end}))) \times 100\%$; with $\Delta\text{PN}_{\text{process}}$ being the change due to aerosol-dynamic processes the respective process after 30 min).

City and campaign	Efficient dispersion				Moderate dispersion				Inefficient dispersion			
	Coag	Dry dep	Cond	Dil	Coag	Dry dep	Cond	Dil	Coag	Dry dep	Cond	Dil
Rotterdam TRANSPHORM	4.7	0.9	0.0	94.4	7.5	4.3	-0.1	88.4	12.9	16.6	-0.9	71.4
Oslo UFP-Oslo Tav	0.5	0.4	0.0	99.1	0.8	2.6	-0.1	96.8	4.1	15.1	-2.9	83.7
Oslo UFP-Oslo Winter	0.5	0.4	0.0	99.1	0.8	2.8	-0.1	96.5	4.4	16.8	-5.9	84.7
Helsinki SAPHIRE Case I	0.4	0.3	0.0	99.3	0.7	3.2	0.0	96.1	4.6	18.3	-4.5	81.6
Helsinki SAPHIRE Case II	0.7	0.4	0.0	98.8	1.2	2.4	0.0	96.3	7.3	14.8	-3.0	80.9
Helsinki LIPIKA	1.1	0.2	0.0	98.7	2.2	1.0	-0.1	95.9	12.5	8.7	-1.1	79.9
Helsinki MMEA	1.3	0.3	0.0	98.5	2.2	1.6	-0.1	96.2	12.0	9.2	-1.0	79.8
All campaigns												
Range (min-max)	0.4-4.7	0.2-0.9	0.0	94.4-99.3	0.7-7.5	1.0-4.3	-0.1-0.0	88.4-96.8	4.1-12.9	8.7-18.3	-5.9- -0.9	71.4-84.7

City and campaign	All dispersion conditions			
	Coag	Dry dep	Cond	Dil
Rotterdam TRANSPHORM	4.7-12.9	0.9-16.6	-0.9-0.0	71.4-94.4
Oslo UFP-Oslo Tav	0.5-4.1	0.4-15.1	-2.9-0.0	83.7-99.1
Oslo UFP-Oslo Winter	0.5-4.4	0.4-16.8	-5.9-0.0	84.7-99.1
Helsinki SAPHIRE Case I	0.4-4.6	0.3-18.3	-4.5-0.0	81.6-99.3
Helsinki SAPHIRE Case II	0.7-7.3	0.4-14.8	-3.0-0.0	80.9-98.9
Helsinki LIPIKA	1.1-12.5	0.2-8.7	-1.1-0.0	79.9-98.7
Helsinki MMEA	1.3-12.0	0.3-9.2	-1.0-0.0	79.8-98.5
All campaigns				
Range (min-max)	0.4-12.9	0.2-18.3	-5.9-0.0	71.4-99.3

Table 5. Data required for the implementation of the PNC parameterization for dry deposition according to three different methodologies and for coagulation. Typical urban times scales for dry deposition (τ_{depo}) and for coagulation (τ_{coag}) is given as reference. MAFOR uses a large number of bin sizes so the extracted coefficients for the three size categories are based on an integral/average over a number of bins in the model. The initial size distribution ratio is the PN fraction in each PNC category for the “mean of traffic sites” distribution. Dry deposition velocity and time scale was calculated with three different methods: KS2012 (Kouznetsov and Sofiev, 2012), H2012 (Hussein et al., 2012), and S1985 (Schack et al., 1985).

Size category	Size ranges [nm]	Initial size distr. ratio [-]	ν_d			K_{coag} [cm ³ s ⁻¹]	τ_{depo}			
			KS2012 [cm s ⁻¹]	H2012 [cm s ⁻¹]	S1985 [cm s ⁻¹]		KS2012 [h]	H2012 [h]	S1985 [h]	τ_{coag} [h]
PNC ₁	8.5–25	0.70	0.53	0.20	0.87	4.51×10^{-9}	1.1	2.8	0.6	1.9
PNC ₂	25–100	0.29	0.12	0.08	0.19	3.10×10^{-9}	4.7	6.7	2.9	6.6
PNC ₃	100–500	0.01	0.02	0.07	0.03	8.82×10^{-10}	24	8.5	17	589

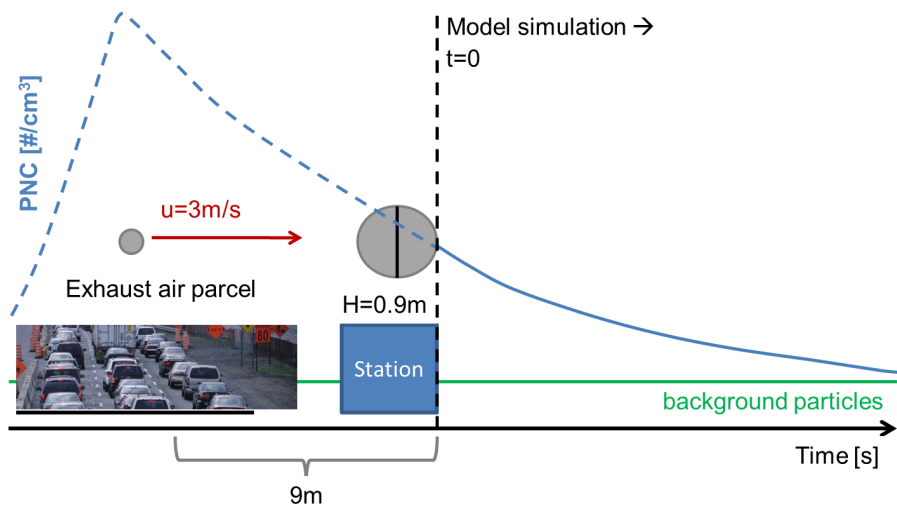


Figure 1. Idealized scenario for model simulations with MAFOR to study aerosol processes between roadside and neighborhood scale. Model simulations start at the point where the exhaust parcel (plume height typically 0.880,9 m) has approached the roadside traffic station. The simulations are initialized with PN concentration and size distribution measured at roadside. Particle concentrations in the exhaust air are diluted by background air with constant PN concentration.

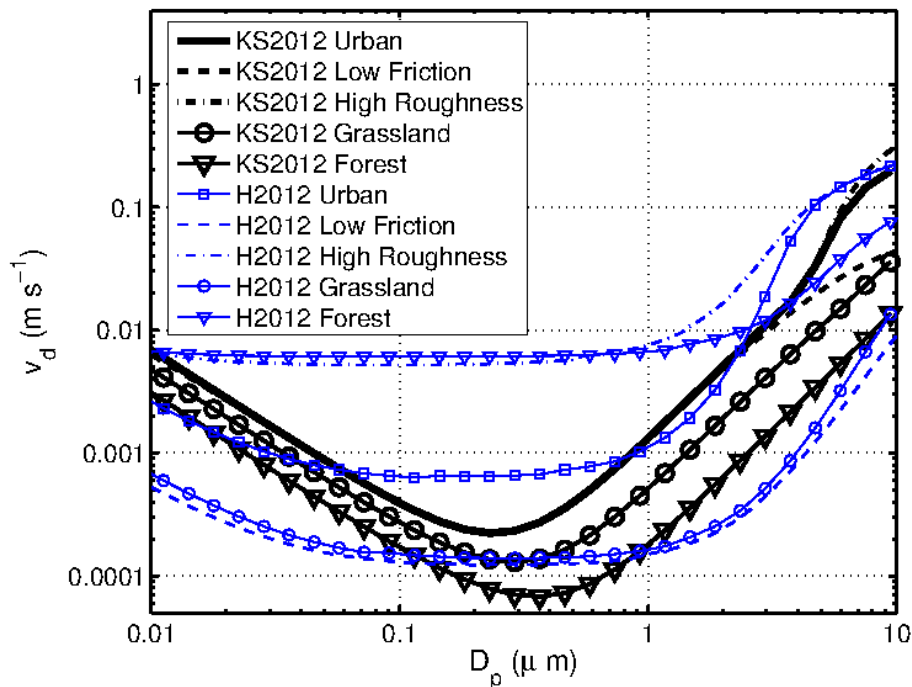


Figure 2. Dry deposition velocity, v_d (in m s^{-1}) as function of particle diameter D_p (in μm), using a particle density of 1400 kg m^{-3} . The results with the model of Kouznetsov and Sofiev (2012) (KS2012) are shown as black lines and the results with the model of Hussein et al. (2012) (H2012) are shown as blue lines. The curve of “KS2012 Urban” (thick black line) represents the dry deposition parameterization that is used in all model runs with MAFOR. The curves for cases “KS2012 Low Friction” (dashed black line) and “KS2012 High Roughness” (dash-dotted black line) partly overlay with the curve for “KS2012 Urban”.

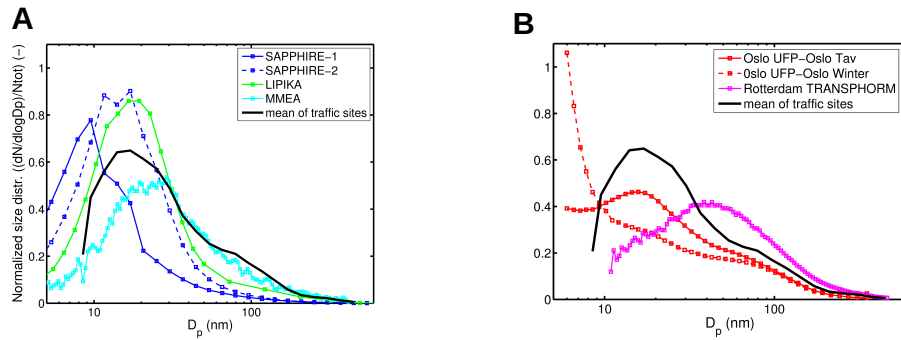


Figure 3. Measured size distribution data normalized to total PN concentration at different traffic stations: **(a)** Helsinki SAPHIRE Case I, Helsinki SAPHIRE Case II, Helsinki LIPIKA, Helsinki MMEA, and **(b)** Oslo Smestad Tav case, Oslo Smestad Winter case, Rotterdam Bentinckplein. Urban background concentrations have not been subtracted. The “mean of traffic sites” curve (solid black line) was constructed based on the mean of the size distribution curves for all traffic sites (Bentinckplein, Smestad, Itäväylä, Mannerheimintie) in all campaigns, after synchronization of the size bin diameters. The “mean of traffic sites” curve is displayed in both panels **(a, b)**.

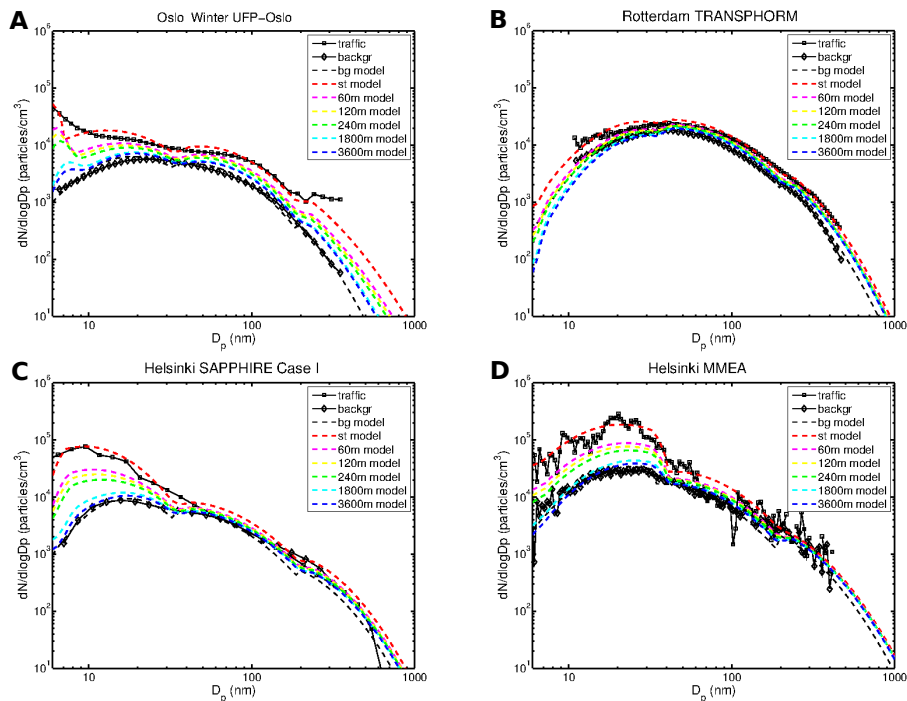


Figure 4. Size distributions ($dN/d\log D_p$ in particles cm^{-3}) downwind of roads in selected campaigns: **(a)** Oslo, UFP-Oslo Winter, **(b)** Rotterdam, **(c)** Helsinki SAPHIRE Case I, and **(d)** Helsinki MMEA. The plots show the measured distribution at roadside (black squares connected by line), the measured distribution at urban background (black diamonds connected by line), the initial model distribution (roadside: dashed red line, background: dashed black line) and the modelled distributions (resulting for moderate dispersion conditions) at distances of 60, 120, 240, 1800, and 3600 m, respectively. Size distributions are shown with a lower size cut-off at 6 nm.

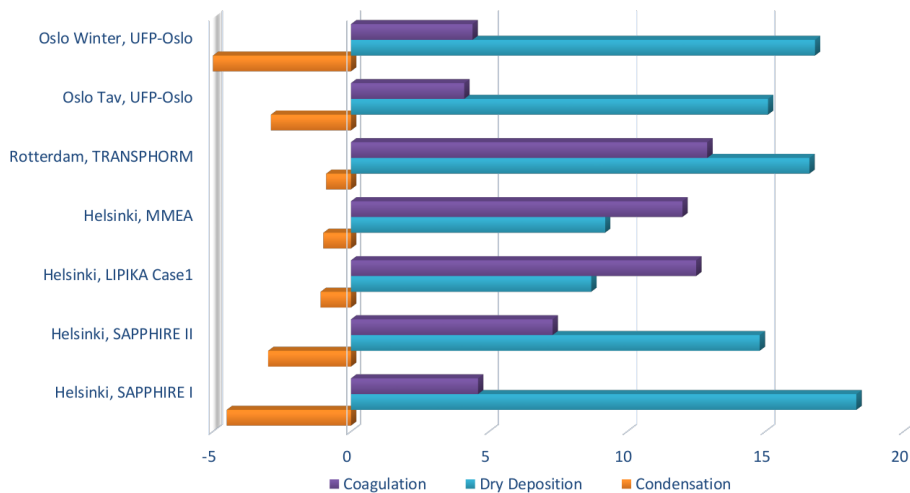


Figure 5. Contribution of aerosol processes to the percentage change of PN concentration (%) between roadside station and neighborhood environment for inefficient dispersion conditions after 30 min transport time [in all campaigns](#).

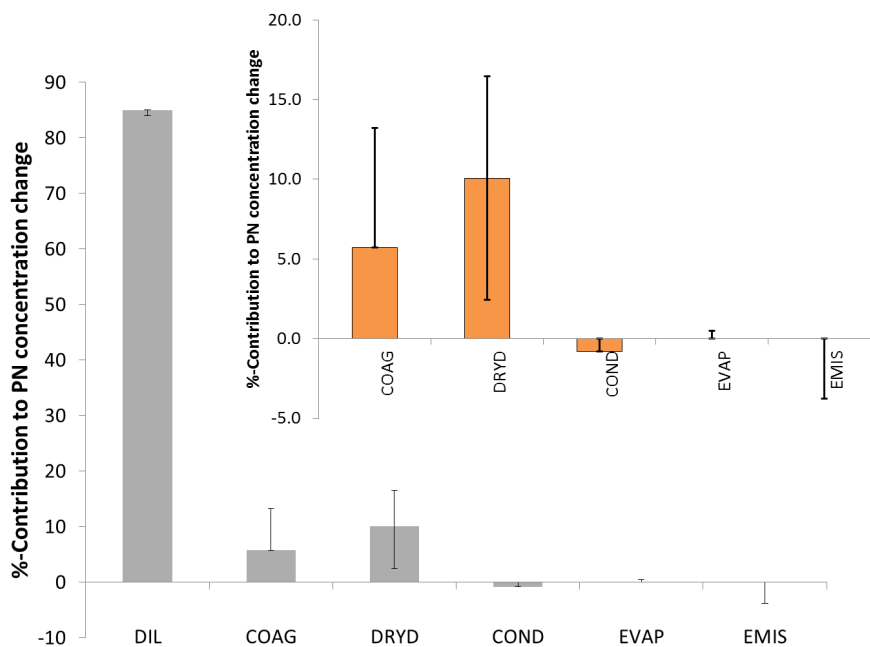


Figure 6. [Contribution of processes to the percentage change of PN concentrations between roadside station and neighborhood environment, and their associated uncertainty depicted as error bars. Inset magnifies the contribution and uncertainty of the aerosol processes and additional emissions of particles.](#)