

Constraining condensed-phase formation kinetics of IEPOX-SOA

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Constraining condensed-phase formation kinetics of secondary organic aerosol components from isoprene epoxydiols

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Abstract

Isomeric epoxydiols from isoprene photooxidation (IEPOX) have been shown to produce substantial amounts of secondary organic aerosol (SOA) mass and are therefore considered a major isoprene-derived SOA precursor. Heterogeneous reactions of IEPOX on atmospheric aerosols form various aerosol-phase components or “tracers” that contribute to the SOA mass burden. A limited number of the reaction rate constants for these acid-catalyzed aqueous-phase tracer formation reactions have been constrained through bulk laboratory measurements. We have designed a chemical box model with multiple experimental constraints to explicitly simulate gas- and aqueous-phase reactions during chamber experiments of SOA growth from IEPOX uptake onto acidic sulfate aerosol. The model is constrained by measurements of the IEPOX reactive uptake coefficient, IEPOX and aerosol chamber wall-losses, chamber-measured aerosol mass and surface area concentrations, aerosol thermodynamic model calculations, and offline filter-based measurements of SOA tracers. By requiring the model output to match the SOA growth and offline filter measurements collected during the chamber experiments, we derive estimates of the tracer formation reaction rate constants that have not yet been measured or estimated for bulk solutions.

1 Introduction

The gas-phase photooxidation of isoprene (2-methyl-1,3-butadiene), the largest biogenic volatile organic compound (VOC) emitted worldwide (Guenther et al., 2012), yields isomeric isoprene epoxydiols (IEPOX) (Paulot et al., 2009). Subsequent acid-catalyzed multiphase chemistry of IEPOX is a significant source of secondary organic aerosol (SOA) mass (Lin et al., 2012; Surratt et al., 2010). In recent field studies, up to 50 % of summertime aerosol mass loadings in the southeastern United States have been attributed to SOA resulting from IEPOX heterogeneous reactions (Budisulistiorini et al., 2013, 2015; Lin et al., 2013b). Similar IEPOX-derived SOA influences are

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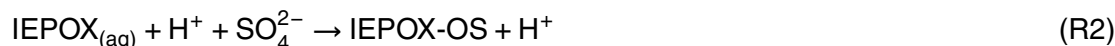
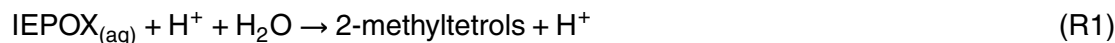
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expected in areas with large isoprene emissions, such as forests primarily composed of broad-leaf vegetation. As a significant SOA precursor, IEPOX has implications regarding potential climate forcing due to the scattering of incoming radiation and also impacts human health due to its large contribution to PM_{2.5} (particulate matter < 2.5 μm in diameter) mass (Chung and Seinfeld, 2002; Dockery et al., 1993).

Gas-phase IEPOX can partition to atmospheric aerosol surface area where it can react with aerosol liquid water and aerosol-phase constituents, including sulfate, nitrate, and organics, to form a variety of lower-volatility organic compounds that can remain in the aerosol and contribute to total aerosol mass. Because their presence establishes IEPOX as the precursor, the particle-phase products are referred to as IEPOX-SOA “tracers” (i.e., “molecular markers”). The efficiency of gas-phase IEPOX removal by aerosol surface area is thought to be largely a function of aerosol acidity and concentration of nucleophiles that can react with accommodated IEPOX by acid-catalyzed oxirane ring opening to yield the tracer compounds (Eddingsaas et al., 2010; Gaston et al., 2014; Nguyen et al., 2014; Piletic et al., 2013; Riedel et al., 2015; Surratt et al., 2007b). Products of the reactions have been proposed to include the 2-methyltetrols (2-methylthreitol and 2-methylerythritol) from addition of water, and the corresponding isomeric sulfate esters (IEPOX-OS) from sulfate addition (Reactions R1 and R2) (Claeys et al., 2004; Surratt et al., 2007a).



Products of nitrate addition, while observed less often, are also thought to be important in certain cases (Darer et al., 2011; Lin et al., 2012). Additional condensed-phase reactions are thought to form IEPOX-derived dimeric species (2-methyltetrol dimers, OS dimers), isomeric C₅-alkene triols, cyclodehydration products (3-methyltetrahydrofuran-3,4-diols (3-MeTHF-3,4-diols)), and higher order oligomers, which have also been identified in field and chamber studies (Lin et al., 2012, 2014, 2013b; Wang et al., 2005). In the aerosol phase, these oligomers or other high molecular weight aerosol species

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may be in dynamic equilibrium with low molecular weight tracers (i.e., equilibrium between monomers and oligomers) (Kolesar et al., 2015). The formation of unsaturated IEPOX-derived oligomers has been linked to brown carbon formation and therefore potential radiative forcing (Lin et al., 2014). General acids, such as bisulfate, can also

5 serve as oxirane ring-opening catalysts, though rates for such reactions tend to be significantly slower than rates for acid catalysis under the majority of aerosol conditions (Eddingsaas et al., 2010; Gaston et al., 2014).

To date, only the formation of IEPOX-derived 2-methyltetrols and/or organosulfates have been investigated through direct bulk kinetic measurements (Cole-Filipiak et al., 10 2010), the extension of bulk kinetic measurements of surrogate epoxides (Eddingsaas et al., 2010), and computational estimates (Piletic et al., 2013). While the tetrol and IEPOX-OS tracers are responsible for a sizeable fraction of IEPOX-derived SOA (Lin et al., 2013a, b), the remaining tracer formation reactions have yet to be examined, and accurate estimates would benefit SOA modeling efforts (Karambelas et al., 2014; 15 McNeill et al., 2012; Pye et al., 2013). Here we present an approach that combines chamber experiments, offline quantification of SOA tracers from filter samples using authentic standards, and modeling to estimate the formation reaction rate constants of IEPOX-derived SOA tracers whose formation rates are currently unknown. This has been done for a single seed aerosol system, acidified ammonium sulfate at low relative 20 humidity (RH), but the estimated rate coefficients are anticipated to be independent of the seed aerosol used.

2 Methods

2.1 Chamber experiments

Experiments were conducted under dark conditions in an indoor 10 m^3 Teflon smog 25 chamber at the University of North Carolina at Chapel Hill (UNC) (Lin et al., 2014; Riedel et al., 2015). Acidic ammonium sulfate seed aerosol was injected into the

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dry ($RH < 5\%$) chamber using a custom-built atomizer with an atomizing solution of $0.06\text{ M}(\text{NH}_4)_2\text{SO}_4$ and $0.06\text{ M}\text{H}_2\text{SO}_4$ until the desired total aerosol mass concentration was achieved. After seed injection, the chamber was left static for at least 30 min to ensure that the seed aerosol concentration was stable and uniformly mixed. IEPOX was then injected into the chamber for 2 h by passing $\sim 4\text{ L min}^{-1}$ of $\text{N}_{2(g)}$ through a glass manifold heated at $60\text{ }^\circ\text{C}$ containing $50\text{--}300\text{ }\mu\text{L}$ of a 100 mg mL^{-1} ethyl acetate solution of *trans*- β -IEPOX (Zhang et al., 2012), the predominant IEPOX isomer (Bates et al., 2014). The majority of the SOA mass growth occurred within the first hour of the injection period, and after 2 h, significant SOA growth had ceased.

Chamber aerosol number distributions, which were subsequently converted to total aerosol surface area and volume concentrations, were measured by a scanning electrical mobility system (SEMS v5.0, Brechtel Manufacturing Inc. – BMI) containing a differential mobility analyzer (DMA, BMI) coupled to a mixing condensation particle counter (MCPC Model 1710, BMI). Total volume concentration of seed aerosols was converted to total mass concentration assuming a density of 1.6 g mL^{-1} , in accord with aerosol thermodynamic model outputs described in more detail below, and SOA total volume concentration was converted to total mass concentrations assuming a density of 1.25 g mL^{-1} (Kroll et al., 2006). The chamber RH and temperature were monitored with a commercial RH/temperature probe (OM-62, Omega Engineering Inc.).

2.2 SOA tracer quantification

On completion of IEPOX injection, a filter sample was collected for analysis of the chamber-generated SOA. Aerosols were collected onto 46.2 mm Teflon filters (Part No.: SF17471, Tisch Scientific) in a stainless steel filter holder for 2 h at $\sim 15\text{ L min}^{-1}$ with a carbon strip denuder (Sunset Labs) upstream of the filter holder. Filters were stored in 20 mL scintillation vials at $-20\text{ }^\circ\text{C}$ prior to extraction and analysis. Denuder efficiency tests were performed by passing $\sim 500\text{ ppbv}$ of $\text{IEPOX}_{(g)}$ in $\text{N}_{2(g)}$ at low RH ($< 5\%$) through the denuder at 2 L min^{-1} . $\sim 80\%$ of IEPOX was removed from the sampling

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stream under these conditions, as measured by an iodide-adduct high-resolution time-of-flight chemical ionization mass spectrometer (HR-TOF-CIMS, Aerodyne Research Inc.) (Lee et al., 2014). The denuder is expected to be less efficient at the higher flow velocities and shorter residence times during filter collection.

As described in previous studies (Lin et al., 2012; Surratt et al., 2010), IEPOX-derived SOA components were extracted from filters with high-purity methanol prior to analysis. Analysis was performed on a gas chromatograph coupled to a mass spectrometer equipped with an electron ionization source (GC/EI-MS, Hewlett-Packard 5890 Series II GC coupled to a Hewlett-Packard 5971A MS) and an ultra-performance liquid chromatograph/high-resolution quadrupole time-of-flight mass spectrometer equipped with electrospray ionization (UPLC/ESI-HR-QTOFMS, Agilent 6500 Series). 2-Methyltetrols, C₅-alkene triols, 3-MeTHF-3,4-diols, and the IEPOX-derived dimer were quantified by GC/EI-MS with prior trimethylsilylation. GC/EI-MS calibrations were performed with authentic 2-methyltetrol and 3-MeTHF-3,4-diol standards (Budisulistiorini et al., 2015; Zhang et al., 2012). In the absence of authentic standards, the triols and dimer were assumed to have the same response factor as the 2-methyltetrols (Lin et al., 2012, 2013b). Aliquots of filter extracts were reconstituted in a 50 : 50 (v/v) methanol:water mixture from which the IEPOX-OS and IEPOX-derived dimer organosulfate (IEPOX-dimerOS) were quantified using UPLC/ESI-HR-QTOFMS operated in the negative ion mode. An authentic IEPOX-OS standard was used for calibration, and IEPOX-dimerOS was assumed to have the same response factor as the IEPOX-OS standard (Budisulistiorini et al., 2015).

2.3 Model setup and evaluation

Reaction kinetics of SOA generation were investigated with a zero-dimensional time-dependent chemical box model incorporating explicit aqueous-phase tracer formation. The model is initialized with the amount of *trans*- β -IEPOX added to the injection manifold and the measured seed aerosol total surface area and mass concentration. Estimates of the aqueous-phase molar concentrations of the inorganic seed

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aerosol species ($[H^+]$, $[H_2O]$, $[HSO_4^-]$, $[SO_4^{2-}]$) and the total volume of the aqueous phase were obtained from the Extended AIM Aerosol Thermodynamics Model III (AIM, <http://www.aim.env.uea.ac.uk/aim/aim.php>) (Clegg et al., 1998; Wexler and Clegg, 2002). The composition of the atomizer solution was used as the AIM inputs with a RH of 10 %, as AIM does not allow RH inputs < 10 %. As is typical with aerosol thermodynamic model calculations, the aerosol components were treated as a metastable solution thereby suppressing the formation of solid-phase species (Hennigan et al., 2015). Given the low chamber RH and the composition of the atomizer solution, the seed aerosol was highly acidic, and this assumption is likely valid (Cziczo et al., 1997; Seinfeld and Pandis, 2006). While some gas-phase measurements might be used to constrain aerosol thermodynamic models like AIM, such measurements (e.g., gas-phase ammonia) were unavailable for this study. Furthermore, the actual state of aerosols at low RH is difficult to represent in such models. As a consequence, estimates presented here may be limited by the ability of so-called “reverse mode” thermodynamic aerosol model calculations to appropriately represent the aerosols in the chamber.

A constant IEPOX-aerosol reaction probability (γ) of 0.021 was assumed over the course of modeled experiments, which is consistent with that measured for similar seed aerosol systems (Gaston et al., 2014; Riedel et al., 2015). The resulting pseudo-first order heterogeneous uptake rate coefficient (k_{het}) of IEPOX to the aerosol phase was then calculated by Eq. (1),

$$k_{het} = \frac{\gamma S_a \omega}{4} \quad (1)$$

where S_a is the total seed aerosol surface area concentration and ω is the mean molecular speed of gas-phase IEPOX. Once IEPOX has partitioned to the particle phase (IEPOX_(aq)) it is allowed to react with the aerosol constituents to form the SOA tracer species. In addition to Reactions (R1) and (R2), the model incorporates acid-catalyzed reactions to form C₅-alkene triols, 3-MeTHF-3,4-diols, IEPOX-dimer, and IEPOX-dimerOS – Reactions (R3)–(R6) below. The model also tracks the formation

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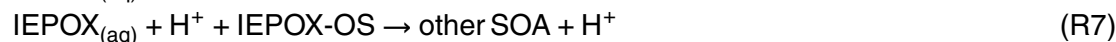
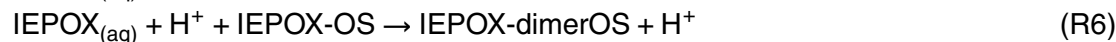
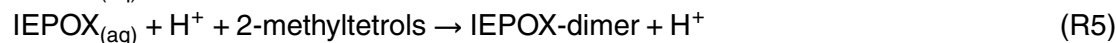
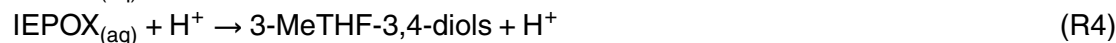
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of “other SOA” – defined as the difference between the chamber-measured SOA mass and the sum of the quantified tracer mass loadings – comprised of unidentified SOA products, mostly likely from acid-catalysis, as is the case for the other IEPOX tracers. Species comprising “other SOA” may be oligomers formed by acid-catalyzed coupling of tetrols or IEPOX-OS with IEPOX concomitant with reactive uptake (Lin et al., 2014). Since we are unable to differentiate the extent to which the “other SOA” is formed from the two pathways, the model assumes all of the “other SOA” is formed from reactions of IEPOX-OS with IEPOX (Reaction R7) and has a molecular weight of 334 g mol^{-1} , the same as that of IEPOX-dimerOS.



The coupled differential equations corresponding to the production and/or loss of $\text{IEPOX}_{(\text{g})}$, $\text{IEPOX}_{(\text{aq})}$, 2-methyltetrols, IEPOX-OS, C_5 -alkene triols, 3-MeTHF-3,4-diols, IEPOX-dimer, IEPOX-dimerOS, “other SOA”, HSO_4^- , and SO_4^{2-} are integrated over the entire IEPOX injection duration (2 h) or until the observed chamber SOA mass concentration had reached a maximum. Under the assumption that HSO_4^- is converted to SO_4^{2-} as SO_4^{2-} forms IEPOX-OS, the equilibrium ratio ($R_{\text{SO}_4} \equiv \text{SO}_4^{2-} / \text{HSO}_4^-$) is held constant. Additionally, a general first-order loss, Reaction (R8) from the formation of volatile products that do not contribute to the overall SOA mass, is applied to $\text{IEPOX}_{(\text{aq})}$.



This reaction lowers the molar SOA yield (φ_{SOA}) below unity. First-order wall-losses estimated for the chamber from a previous study are also applied to gas-phase IEPOX ($k_{\text{wall}} = 9.4 \times 10^{-5} \text{ s}^{-1}$) and all aerosol-phase species ($k_{\text{wall-aerosol}} = 1 \times 10^{-5} \text{ s}^{-1}$) (Riedel

et al., 2015). The rate of IEPOX injection into the chamber is simulated in the model by an exponential decay of IEPOX in the injection manifold. The decay constant (λ) was varied between 1×10^{-3} – $2 \times 10^{-3} \text{ s}^{-1}$ as a fitting parameter to better match the timescale of observed SOA growth. However, over the 2 h duration of the experiment, the value of the decay constant had a negligible effect on the final model-predicted SOA growth.

The complete set of differential equations used to track each individual species in the model is provided in Eqs. (2)–(12).

$$\frac{d[\text{IEPOX}_{(g)}]}{dt} = \lambda[\text{IEPOX}_{(\text{manifold})}] - k_{\text{het}}[\text{IEPOX}_{(g)}] - k_{\text{wall}}[\text{IEPOX}_{(g)}] \quad (2)$$

$$\begin{aligned} \frac{d[\text{IEPOX}_{(aq)}]}{dt} = & k_{\text{het}}[\text{IEPOX}_{(g)}] - k_{R1}[\text{IEPOX}_{(aq)}][\text{H}_2\text{O}][\text{H}^+] \\ & - k_{R2}[\text{IEPOX}_{(aq)}][\text{SO}_4^{2-}][\text{H}^+] - k_{R3}[\text{IEPOX}_{(aq)}][\text{H}^+] \\ & - k_{R4}[\text{IEPOX}_{(aq)}][\text{H}^+] - k_{R5}[\text{IEPOX}_{(aq)}][\text{H}^+][\text{tetrol}] \\ & - k_{R6}[\text{IEPOX}_{(aq)}][\text{H}^+][\text{IEPOX-OS}] - k_{R7}[\text{IEPOX}_{(aq)}][\text{H}^+][\text{IEPOX-OS}] \\ & - k_{R8}[\text{IEPOX}_{(aq)}] - k_{\text{wall-aerosol}}[\text{IEPOX}_{(aq)}] \end{aligned} \quad (3)$$

$$\frac{d[\text{tetrol}]}{dt} = k_{R1}[\text{IEPOX}_{(aq)}][\text{H}_2\text{O}][\text{H}^+] - k_{\text{wall-aerosol}}[\text{tetrol}] \quad (4)$$

$$\frac{d[\text{IEPOX-OS}]}{dt} = k_{R2}[\text{IEPOX}_{(aq)}][\text{SO}_4^{2-}][\text{H}^+] - k_{\text{wall-aerosol}}[\text{IEPOX-OS}] \quad (5)$$

$$\frac{d[\text{triol}]}{dt} = k_{R3}[\text{IEPOX}_{(aq)}][\text{H}^+] - k_{\text{wall-aerosol}}[\text{triol}] \quad (6)$$

$$\frac{d[\text{diolTHF}]}{dt} = k_{R4}[\text{IEPOX}_{(aq)}][\text{H}^+] - k_{\text{wall-aerosol}}[\text{diolTHF}] \quad (7)$$

$$\frac{d[\text{dimer}]}{dt} = k_{R5}[\text{IEPOX}_{(aq)}][\text{H}^+][\text{tetrol}] - k_{\text{wall-aerosol}}[\text{dimer}] \quad (8)$$

$$\frac{d[\text{dimerOS}]}{dt} = k_{R6}[\text{IEPOX}_{(\text{aq})}][\text{H}^+][\text{IEPOX-OS}] - k_{\text{wall-aerosol}}[\text{dimerOS}] \quad (9)$$

$$\frac{d[\text{other}]}{dt} = k_{R7}[\text{IEPOX}_{(\text{aq})}][\text{H}^+][\text{IEPOX-OS}] - k_{\text{wall-aerosol}}[\text{other}] \quad (10)$$

$$\frac{d[\text{HSO}_4^-]}{dt} = -k_{R2}[\text{IEPOX}_{(\text{aq})}][\text{H}^+][\text{HSO}_4^-] R_{\text{SO}_4} - k_{\text{wall-aerosol}}[\text{HSO}_4^-] \quad (11)$$

$$\begin{aligned} \frac{d[\text{SO}_4^{2-}]}{dt} = & k_{R2}[\text{IEPOX}_{(\text{aq})}][\text{H}^+][\text{HSO}_4^-] R_{\text{SO}_4} \\ & - k_{R2}[\text{IEPOX}_{(\text{aq})}][\text{H}^+][\text{SO}_4^{2-}] - k_{\text{wall-aerosol}}[\text{SO}_4^{2-}] \end{aligned} \quad (12)$$

Rate constants (k) for Reactions (R1)–(R8) were systemically varied until model output closely matched the offline tracer measurements. Initial values were assigned to k_{R1} – k_{R8} , and the model run in a continuous loop, varying each rate constant to minimize the sum of the squares of the differences between the filter measurements and model output, under the constraint that all $k > 0$. Implicitly, this approach assumes that tracer quantitations are robust, a correct representation of IEPOX-derived SOA speciation and mass loading, and that the filter collection and extraction efficiency are 100 %.

3 Results and discussion

3.1 Model output and comparison to chamber data

Five chamber experiments were performed with the low RH $(\text{NH}_4)_2\text{SO}_4 + \text{H}_2\text{SO}_4$ seed aerosol system. Table 1 lists initial chamber conditions, including seed aerosol surface area and mass loading and the mass of IEPOX placed in the injection manifold. Figure 1 shows aerosol mass data and the corresponding model simulation for one experiment (Exp. No. 1). The initial seed aerosol mass loading is $113 \mu\text{g m}^{-3}$, and IEPOX injection is initiated at experiment time (t) = 0. SOA mass growth is most rapid for 30 min

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post injection and slows thereafter, reaching a maximum total aerosol mass concentration of $\sim 275 \mu\text{g m}^{-3}$ at $t \approx 90$ min. The timescale of SOA growth for other experiments was similar to that in Fig. 1. Figure 2 shows the model-predicted aqueous-phase IEPOX concentration for Exp. No. 1. Despite the large amount of IEPOX injected into the chamber, the maximum predicted aqueous-phase IEPOX concentration reaches only 0.92 mol L^{-1} due to rapid formation of the SOA products. For all simulated experiments, the model reproduced the SOA growth well, both the rate and the maximum mass loading. Nevertheless, caution is necessary in interpreting the significance of this agreement since the model parameters are adjusted to maximize the agreement.

Figure 3 compares the modeled evolution of the SOA tracers in Exp. No. 1 to offline measurements of the corresponding tracers, and results for all experiments are summarized in Table 2. The tracer concentrations predicted by the model agree well with the filter measurements, differing by $< 5\%$ for all tracers.

The model also predicts significant titration of total aqueous inorganic sulfate species ($[\text{SO}_4^{2-}] + [\text{HSO}_4^-]$) over the course of each experiment due to the formation of IEPOX-OS, IEPOX-dimerOS, and “other SOA”. Sulfate loadings were predicted to drop 36, 28, and 27% for the 30, 15, and 5 mg IEPOX injections, respectively. Figure 4 shows the model-predicted sulfate titration for Exp. No. 1 in which sulfate loading drops from an initial value of ~ 95 to $\sim 60 \mu\text{g m}^{-3}$ at the conclusion of the model run. These titration levels closely match those reported in Surratt et al. (2007a) for a low- NO_x isoprene oxidation experiment with acidified ammonium sulfate seed aerosol.

3.2 Model-predicted tracer formation kinetics

The model-predicted tracer formation rate constants for Reactions (R1)–(R7) are given in Table 3. These are averaged over all experiments and the listed errors correspond to one standard deviation. While the aerosols are not a priori ideal solutions, comparison of the rate constants obtained in this study to those estimated from prior studies provides useful insights. Eddingsaas et al. (2010) determined the pseudo second-order formation constants for bulk solutions of *cis*-2,3-epoxybutane-1,4-diol and used

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the relationship between 2-methyl-2,3-epoxybutane and 2,3-epoxybutane reaction rate constants to estimate those for 2-methyl-2,3-epoxybutane-1,4-diol (β -IEPOX). For 2-methyltetrol formation, Pye et al. (2013) used the value estimated by Eddingsaas et al. (2010) and assumed a water concentration of 55 M in order to derive a third-order rate constant with an explicit water dependence. The resulting rate constants are $9 \times 10^{-4} \text{ M}^{-2} \text{ s}^{-1}$ for formation of 2-methyltetrol (Reaction R1) and $2 \times 10^{-4} \text{ M}^{-2} \text{ s}^{-1}$ for formation of IEPOX-OS (Reaction R2). A similar treatment can be applied to the pseudo second-order hydrolysis rate constant (2-methyltetrol formation) for a mixture of *cis*- and *trans*- β -IEPOX from Cole-Filipiak et al. (2010) to obtain a rate constant of $6.5 \times 10^{-4} \text{ M}^{-2} \text{ s}^{-1}$. Purely computational estimates of 5.3×10^{-2} and $5.2 \times 10^{-1} \text{ M}^{-2} \text{ s}^{-1}$ for 2-methyltetrol and IEPOX-OS, respectively, are also available for comparison (Piletic et al., 2013). Apart from the computational study, these rate constants are of the same order as those predicted by the model, $3.4 \pm 3.2 \times 10^{-4} \text{ M}^{-2} \text{ s}^{-1}$ for 2-methyltetrols and $4.8 \pm 3.4 \times 10^{-4} \text{ M}^{-2} \text{ s}^{-1}$ for IEPOX-OS, indicating that the model gives a reasonable representation of the kinetics of the multiphase process in light of the low RH, non-ideal conditions in the highly concentrated chamber aerosols.

Epoxide ring-opening reactions by general acids (i.e., bisulfate) have not been explicitly included in the model. The contribution is expected to be negligible as the branching ratio between the bisulfate and H^+ -catalyzed reaction channels is likely to heavily favor the H^+ channel. For example, in Exp. No. 1, $\sim 98\%$ of the epoxide ring-opening is predicted to proceed through the H^+ -catalyzed channel compared to that of bisulfate.

Aerosol surface area was held constant at initial seed aerosol levels over the course of a model run, and thus k_{het} is insensitive to additional surface area resulting from IEPOX-derived SOA (Riedel et al., 2015). However, the presence of organics such as polyethylene glycol have been shown to lower γ and therefore k_{het} (Gaston et al., 2014), and it is unclear whether the presence of IEPOX-derived SOA components would have a similar effect. A consequence of the constant surface area is that the model does not account for any possible slowing of the uptake rate resulting from increased aerosol

organic content. Measurements of γ on mixed and pure IEPOX-SOA would be required to resolve this question.

Given the estimates of the tracer formation rate constants, the calculated k_{het} , and the model output, φ_{SOA} can be estimated as the ratio of the sum of the tracer production rates over the IEPOX_(g) heterogeneous loss rate (Riedel et al., 2015). Averaged over the five experiments, $\varphi_{\text{SOA}} = 0.078 \pm 0.025$ (1σ), with the largest φ_{SOA} from the 5 mg IEPOX injections and the smallest φ_{SOA} from the 30 mg injections. The drop in φ_{SOA} with increased IEPOX injection mass is a function of the increased amount of “other SOA” measured in these experiments. The higher molecular weight assumed for the oligomeric products relative to the molecular weight of the tracers requires less IEPOX to be reacted in order to match the total SOA mass loadings, thus driving down φ_{SOA} . $\varphi_{\text{SOA}} = 0.078$ is similar to that predicted from an independent modeling approach which estimated the φ_{SOA} for this aerosol system at 0.1–0.12 (Riedel et al., 2015). These results indicate that the molar yield of SOA from IEPOX heterogeneous reactions is likely to be significantly < 1 for the majority of atmospheric conditions where aerosols are likely to contain more water and be less acidic than in this study.

3.3 Atmospheric implications

Figure 5 shows the model output after 6 h processing time, using as inputs the rate constants from Table 3 and initial atmospheric conditions which might be representative of a daytime summer urban/rural mixed air mass: 50 % RH, ~ 500 pptv gas-phase IEPOX, and $250 \mu\text{m}^2 \text{cm}^{-3}$ of ammonium bisulfate aerosol surface area, corresponding to an aerosol mass loading of $\sim 10 \mu\text{g m}^{-3}$. The model predicts $0.37 \mu\text{g m}^{-3}$ of total SOA with the bulk (77 %) being 2-methyltetrols, and minor amounts of IEPOX-OS (14 %), C₅-alkene triols (7 %), and 3-MeTHF-3,4-diols (2 %). The remaining tracers – IEPOX-dimer, IEPOX-dimerOS, and “other SOA” – are predicted to form in small amounts ($< 0.6 \text{ ng m}^{-3}$). Additionally, this simulation predicted no appreciable titration of total aqueous inorganic sulfate, suggesting that titration is unlikely to occur in atmo-

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spheric aerosols, and the rate of sulfated tracer formation is rarely, if ever, limited by the availability of aerosol sulfate.

The model IEPOX tracer loading predictions are in close correspondence to recent measurements in the southeastern United States. Analysis of tracers in ambient PM_{2.5} collected by high-volume sampling during summer 2010 in Yorkville, GA, determined that 2-methyltetrols (330 ng m⁻³), C₅-alkene triols (290 ng m⁻³), and IEPOX-OS (72 ng m⁻³) were major constituents, with minor amounts of 3-MeTHF-3,4-diols (27 ng m⁻³), IEPOX-dimerOS (5 ng m⁻³), and IEPOX-dimer (0.5 ng m⁻³) (Lin et al., 2012). IEPOX tracer mass loadings from analysis of high-volume PM_{2.5} samples collected at Look Rock, TN, in summer 2013 as part of the Southern Oxidant and Aerosol Study (SOAS) were also dominated by IEPOX-OS (169.5 ng m⁻³), 2-methyltetrols (163.1 ng m⁻³), and C₅-alkene triols (144.4 ng m⁻³), whereas 3-MeTHF-3,4-diols (4.4 ng m⁻³) and IEPOX-dimerOS (1.4 ng m⁻³) made only minor contributions (Budisulistiorini et al., 2015).

4 Concluding remarks

Attempts to replicate the chamber experiments at higher RH (50 %) resulted in large positive deviations (1.2–2.3-fold) in total IEPOX tracer mass loadings compared to measured total aerosol mass loadings by the SEMS-MCPC. This result precluded the extension of these kinetic studies to include humid conditions. A possible explanation for the enhancement of filter mass loadings could be subsequent reactions at the Teflon filter surface; however, appropriate controls are required to confirm such effects. The deviation in mass loadings at higher RH indicate that artifacts may be introduced into field and chamber measurements during filter collection even when sampling through a carbon strip denuder.

Low molecular weight tracers with significant vapor pressures may be detected as a result of decomposition of SOA products. Such a possibility would dictate caution in adopting the kinetic estimates presented here. The sum of these formation rates

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would likely represent an upper limit to the formation of such SOA species under the assumption that more than one tracer could potentially be formed from the degradation of these products. However, in the absence of evidence to the contrary, there is general agreement that tracers constitute a large fraction of IEPOX-SOA, and additional investigations are required prior to the proposal that certain SOA tracers represent decomposition products.

In summary, this study is a first approach at placing kinetic constraints on the formation of species that have been quantified in laboratory and field measurements but lack directly measured experimental rate constraints. While bulk solution rate constant estimates are desirable, such measurements pose a challenge when authentic standards are unavailable or when surrogates do not adequately represent the true compounds. Additionally, it is unclear that bulk-phase kinetics can approximate aerosol-phase reactions where non-ideal conditions likely play a role. The flexible approach described here may readily be extended to other SOA production systems known to have atmospheric importance.

This study approximates tracer branching ratios for the currently proposed SOA tracers resulting from IEPOX uptake, a necessary step to predict isoprene-derived SOA production in regional models that guide policy decisions. Additional laboratory studies to identify SOA products and elucidate formation mechanisms are important to ensure that both chamber and field measurements accurately reflect atmospheric processes. Modeling developed on the basis of such experimental systems can then be extended to large-scale models.

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opinions or conclusions of the TCEQ. The authors also thank Tianqu Cui and Sri Hapsari Budisulistiorini (UNC) and Felipe Lopez-Hilfiker (UW) for helpful discussions.

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Table 1. Summary of conditions for each chamber SOA experiment.

Exp. No.	IEPOX injected (mg)	Seed surface area ($\mu\text{m}^2 \text{cm}^{-3}$)	Seed mass ($\mu\text{g m}^{-3}$)
1	30	1480	113
2	30	1660	125
3	15	1200	76
4	5	800	59
5	5	800	57

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Table 2. Comparison of tracer mass loadings and model outputs for each chamber SOA experiment.

Exp. No.	Loading ($\mu\text{g m}^{-3}$)							
	Total SOA	2-Methyl-tetrols	IEPOX-OS	C ₅ -alkene triols	3-MeTHF-3,4-diols	IEPOX-dimer	IEPOX-dimerOS	Other SOA
1	170.00	39.13	16.97	12.01	15.05	0.40	1.45	84.99
model:	169.99	39.13	16.97	12.00	15.05	0.40	1.45	84.99
2	185.00	41.35	23.69	12.17	13.67	0.70	3.01	90.41
model:	185.01	41.35	23.69	12.18	13.67	0.70	3.02	90.41
3	131.00	34.01	13.25	35.31	3.68	3.59	4.01	37.15
model:	130.01	34.01	13.25	35.31	3.69	3.59	4.01	37.15
4	60.99	3.72	27.13	18.42	0.04	0.27	10.51	0.90
model:	60.98	3.72	27.13	18.42	0.04	0.27	10.51	0.90
5	63.00	3.97	27.44	19.36	0.10	0.25	9.05	2.83
model:	62.99	3.97	27.44	19.36	0.09	0.25	9.05	2.83

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Table 3. Model-predicted formation reaction rate constants for IEPOX-SOA tracers.

SOA tracer formed	k	Reaction
2-methyltetrols	$3.4 \pm 3.2 \times 10^{-4} \text{ M}^{-2} \text{ s}^{-1}$	(R1)
IEPOX-OS	$4.8 \pm 3.4 \times 10^{-4} \text{ M}^{-2} \text{ s}^{-1}$	(R2)
C ₅ -alkene triols	$8.8 \pm 3.8 \times 10^{-4} \text{ M}^{-1} \text{ s}^{-1}$	(R3)
3-MeTHF-3,4-diols	$2.6 \pm 3.5 \times 10^{-4} \text{ M}^{-1} \text{ s}^{-1}$	(R4)
IEPOX-dimer	$1.3 \pm 0.7 \times 10^{-5} \text{ M}^{-2} \text{ s}^{-1}$	(R5)
IEPOX-dimerOS	$6.8 \pm 4.6 \times 10^{-5} \text{ M}^{-2} \text{ s}^{-1}$	(R6)
other SOA	$5.7 \pm 6.9 \times 10^{-4} \text{ M}^{-2} \text{ s}^{-1}$	(R7)

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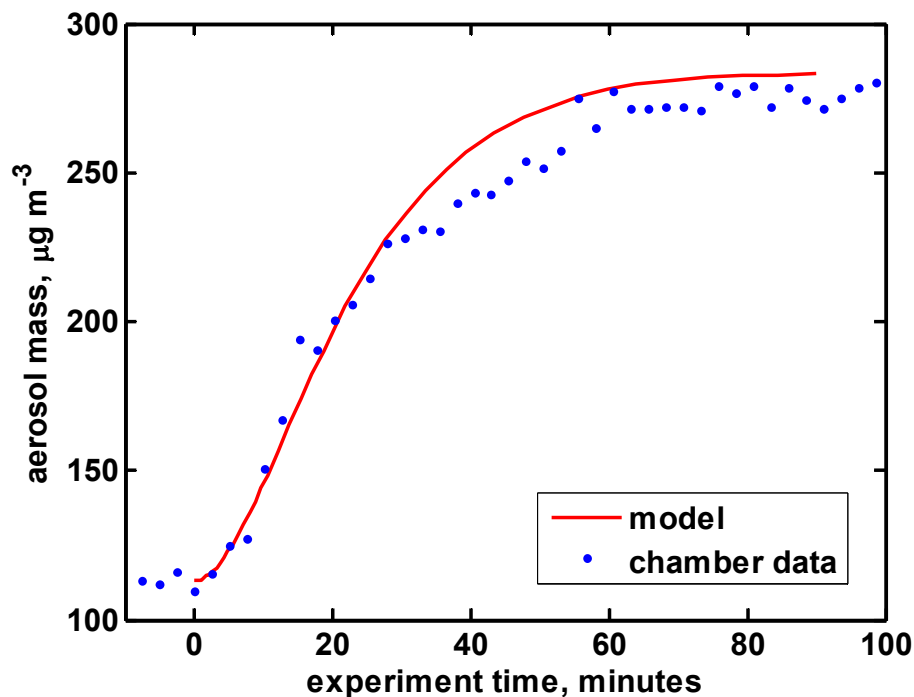


Figure 1. Aerosol mass loadings from IEPOX-SOA Exp. No. 1 and corresponding model output. IEPOX injection starts at experiment time $t = 0$ min.

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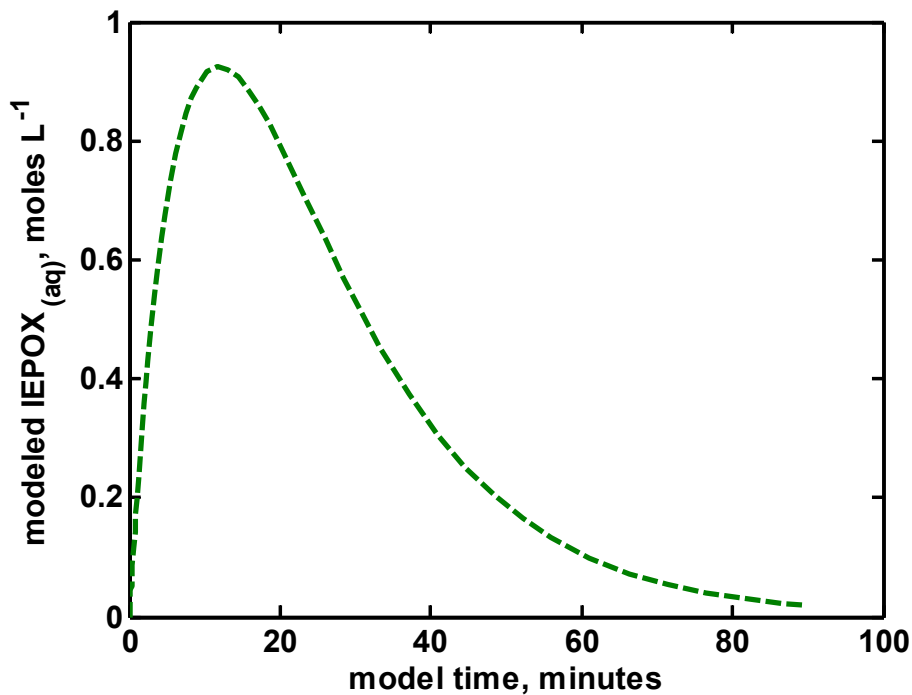


Figure 2. Model output of aqueous-phase IEPOX concentrations during Exp. No. 1 simulation.

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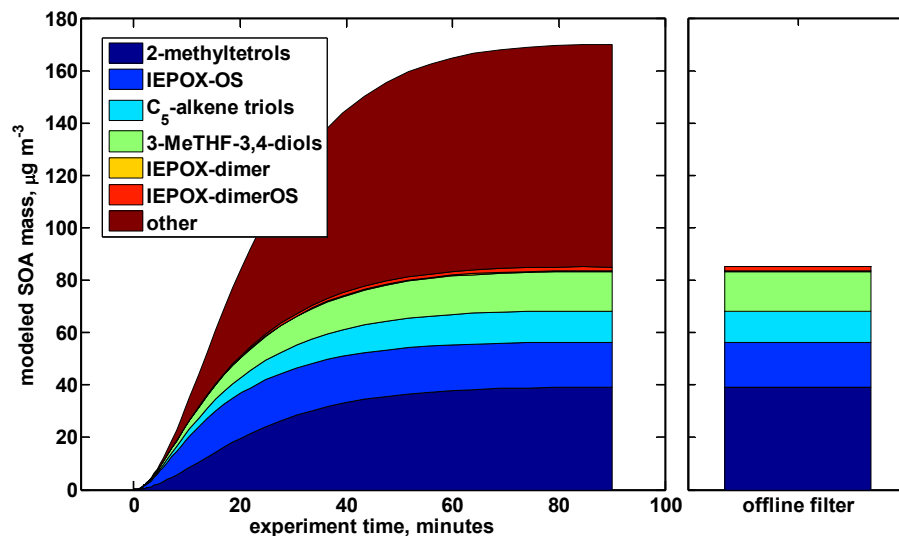


Figure 3. Model output of IEPOX-SOA tracers (left panel) and the associated filter-based tracer measurements (right panel) for Exp. No. 1. The “other SOA” is calculated as the difference between the chamber-measured aerosol mass loadings and the sum of the filter-based tracer loadings.

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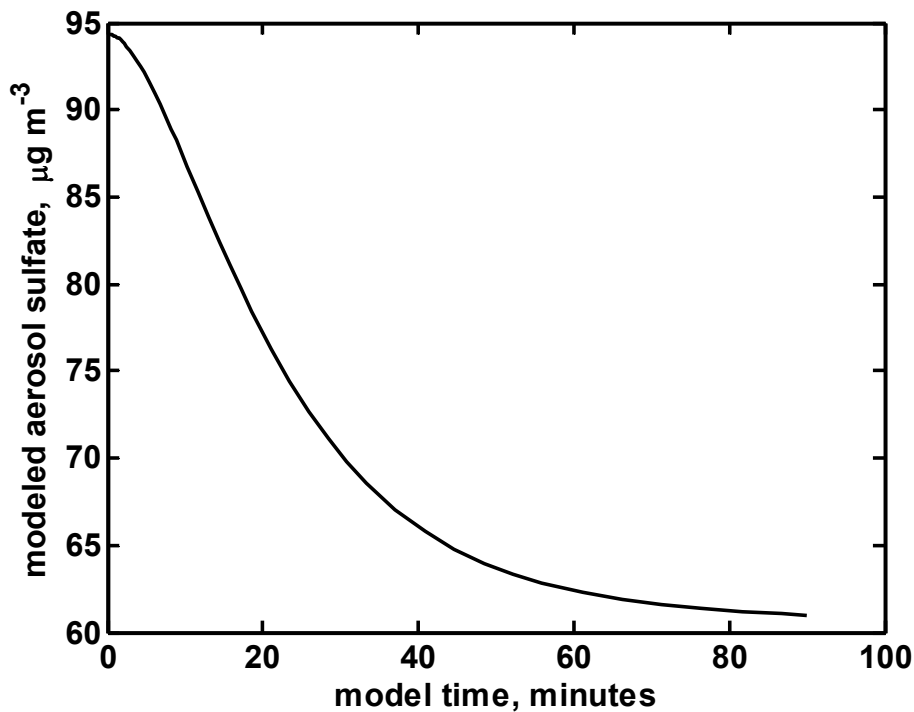


Figure 4. Model output of predicted titration of total inorganic aerosol sulfate ($[\text{SO}_4^{2-}] + [\text{HSO}_4^-]$) due to sulfated tracer formation during Exp. No. 1 simulation.

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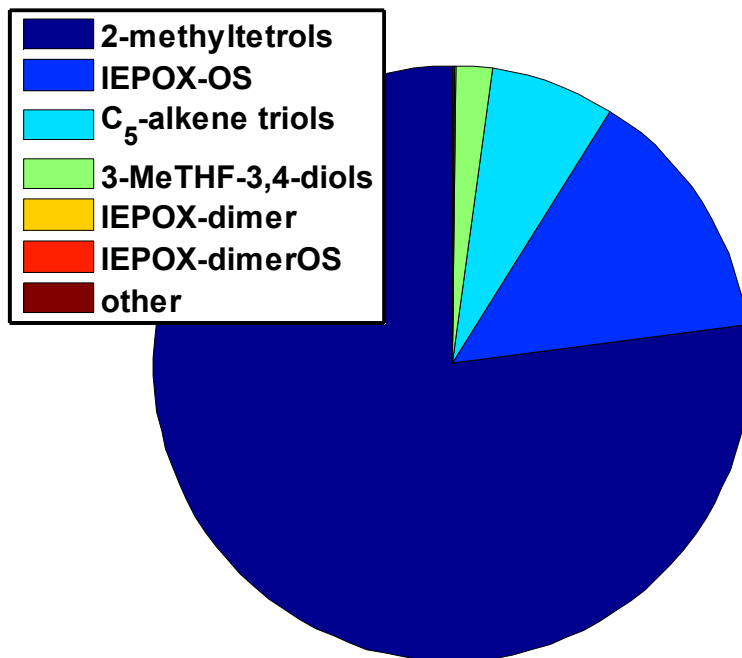
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Total predicted SOA mass = 0.37 $\mu\text{g m}^{-3}$

Figure 5. Model-predicted IEPOX-SOA tracer distribution and loadings for atmospherically relevant initial conditions.

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