

1 **Formation of secondary aerosols from gasoline vehicle**
2 **exhaust when mixing with SO₂**

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26 **Abstract**

27 Sulfur dioxide (SO₂) can enhance the formation of secondary aerosols from biogenic
28 volatile organic compounds (VOCs), but its influence on secondary aerosol formation
29 from anthropogenic VOCs, particularly complex mixtures like vehicle exhaust,
30 remains uncertain. Gasoline vehicle exhaust (GVE) and SO₂, a typical pollutant from
31 coal burning, are directly co-introduced into a smog chamber, in this study, to
32 investigate the formation of secondary organic aerosols (SOA) and sulfate aerosols
33 through photooxidation. New particle formation was enhanced while substantial
34 sulfate was formed through the oxidation of SO₂ in the presence of high concentration
35 of SO₂. Homogenous oxidation by OH radicals contributed a negligible fraction to the
36 conversion of SO₂ to sulfate, and instead the oxidation by stabilized Criegee
37 intermediates (sCIs), formed from alkenes in the exhaust reacting with ozone,
38 dominated the conversion of SO₂. After 5 h of photochemical aging, GVE's SOA
39 production factor revealed an increase by 60–200% in the presence of high
40 concentration of SO₂. The increase could principally be attributed to acid-catalyzed
41 SOA formation as evidenced by the strong positive linear correlation ($R^2 = 0.97$)
42 between the SOA production factor and in-situ particle acidity calculated by AIM-II
43 model. A high-resolution time-of-flight aerosol mass spectrometer (HR-TOF-AMS)
44 resolved OA's relatively lower oxygen-to-carbon (O:C) (0.44 ± 0.02) and higher
45 hydrogen-to-carbon (H:C) (1.40 ± 0.03) molar ratios for the GVE/SO₂ mixture, with a
46 significantly lower estimated average carbon oxidation state (OS_c) of -0.51 ± 0.06 than
47 -0.19 ± 0.08 for GVE alone. The relative higher mass loading of OA in the experiments

48 with SO₂ might be a significant explanation for the lower SOA oxidation degree.

49 1. Introduction

50 Sulfate and organic aerosols (OA) can lead to serious and complex air pollution
51 ([Parrish and Zhu, 2009](#)) as the main components of fine particles or PM_{2.5}, conveying
52 negative effects on human health ([Nel, 2005](#)). Sulfate and OA additionally affect
53 radiative forcing on a global scale ([Andreae et al., 2005](#); [Shindell et al., 2009](#)). Thus, a
54 detailed understanding of the magnitude and formation pathways of sulfate and OA is
55 critical to formulate control strategies and to accurately estimate their impact on air
56 quality and climate. Complications often arise due to missing or underestimated
57 oxidation pathways of sulfur dioxide (SO₂) ([Berglen et al., 2004](#)), the precursor of
58 sulfate, and the unclear formation mechanisms of secondary organic aerosols (SOA)
59 ([de Gouw et al., 2005](#); [Heald et al., 2005](#); [Johnson et al., 2006](#); [Volkamer et al., 2006](#)),
60 accounting for a large fraction of OA ([Zhang et al., 2007](#)).

61 Recent smog chamber studies have demonstrated that the amount of SOA formed
62 from dilute gasoline vehicle exhaust often exceeds primary OA (POA) ([Nordin et al.,](#)
63 [2013](#); [Platt et al., 2013](#); [Gordon et al., 2014](#); [Liu et al., 2015](#)). Aromatic hydrocarbons
64 were found to be vital SOA precursors in gasoline vehicle exhaust. Up to 90% of SOA
65 from idling Euro 1–4 vehicle exhaust could be attributed to aromatics ([Nordin et al.,](#)
66 [2013](#); [Liu et al., 2015](#)). [Gordon et al. \(2014\)](#) concluded that traditional precursors
67 could fully explain the SOA production from old vehicles with model years prior to
68 1995. Emitted primarily from coal-fired power plants and coal-burning boilers, SO₂,
69 when mixed with gasoline vehicle exhaust containing the precursors for secondary
70 nitrates and organic aerosols, NO_x and aromatics, may react, complicating the

71 formation of sulfate and SOA. Alkenes present in gasoline vehicle exhaust can react
72 with ozone to form stabilized Criegee intermediates (sCIs), recently considered to
73 significantly oxidize SO₂ and influence sulfate formation (Mauldin et al., 2012; Welz
74 et al., 2012). On the other hand, recent smog chamber simulations indicated that SO₂
75 could enhance SOA formation from typical biogenic precursors, such as
76 monoterpenes and isoprene through acid-catalyzed reactions (Edney et al., 2005;
77 Kleindienst et al., 2006; Jaoui et al., 2008), but the influence of acid-catalyzed
78 reactions on SOA formation from aromatics still remains debatable (Cao and Jang,
79 2007; Ng et al., 2007). Combinations of several pure chemicals, additionally, are not
80 fully representative of SO₂ mixing with vehicle exhaust containing thousands of
81 gaseous and particle-phase components (Gordon et al., 2014) in the formation of
82 secondary aerosols under real atmospheric conditions. Till present no reports are
83 available about the influence of SO₂ on secondary aerosol formation from complex
84 vehicle exhaust.

85 Here we directly introduced pipe exhaust from light-duty gasoline vehicles
86 (LDGV) and SO₂ into a smog chamber with a 30 m³ Teflon reactor (Wang et al.,
87 2014), to study the production of secondary aerosols: the influence of LDGV exhaust
88 on SO₂ oxidation to form sulfate aerosols and reciprocally that of SO₂ on SOA
89 formation from primary organics in LDGV exhaust.

90 **2. Materials and methods**

91 **2.1 Vehicles and fuel**

92 In Europe, vehicle emissions are classified by “Euro Standards”, currently ranging

93 from Euro 1 to Euro 6. China implemented the Euro 1, Euro 2, Euro 3 and Euro 4
94 emission standards in 2000, 2004, 2007 and 2012 for LDGVs and the Euro 5 standard
95 will be implemented in 2018. Three LDGVs were utilized in this study, one Euro 1
96 and two Euro 4 vehicles. They are all port fuel injected vehicles with model years
97 ranging from 2002 to 2011. Further vehicle details are listed in [Table 1](#). All vehicles
98 were fueled with Grade 93# gasoline, which complies with the Euro III gasoline fuel
99 standard. Details of the gasoline composition can be found elsewhere ([Zhang et al.,](#)
100 [2013](#)).

101 **2.2 Smog chamber experiments**

102 Six photochemical experiments with LDGV exhaust were conducted in a 30 m³
103 indoor smog chamber at Guangzhou Institute of Geochemistry, Chinese Academy of
104 Sciences (GIG-CAS). Details of the smog chamber were described by [Wang et al.](#)
105 ([2014](#)). Briefly, black lamps (1.2m-long, 60W Philips/10R BL, Royal Dutch Philips
106 Electronics Ltd, The Netherlands) are used as a light source, providing a NO₂
107 photolysis rate of 0.49 min⁻¹. Two Teflon-coated fans are installed inside the reactor
108 to guarantee thorough mixing of the introduced gas species and particles within 120
109 seconds. Temperature and relative humidity in the reactor were controlled at
110 approximately 25 °C and 50%, respectively. A schematic of the experiment setup is
111 presented in [Fig. 1](#). Eight thermocouples are placed between the enclosure and the
112 reactor walls to control the temperature. The temperature inside the reactor (T9) was
113 measured by Siemens QFM2160 (Siemens AG, Germany). Vehicles were first
114 operated on-road to warm up the three-way catalysts for a minimal half an hour prior

115 to introducing the vehicle exhaust. Idling vehicle exhaust was then introduced directly
116 by two oil-free pumps (Gast Manufacturing, Inc, USA) into the reactor at a flow rate
117 of 40 L min⁻¹. Losses of volatile organic compounds (VOCs) and particles in the
118 transfer lines were estimated to be less than 5% (Liu et al., 2015). Prior to each
119 experiment, the chamber was evacuated and filled with purified dry air for at least 5
120 times, then the reactor was flushed with purified dry air for a minimal 48 h until no
121 residual hydrocarbons, O₃, NO_x, or particles were detected in the reactor. The exhaust
122 in the reactor was diluted by a factor of 13–94 compared to the tailpipe.

123 SO₂ was injected by a gas-tight syringe following introduction of exhaust to
124 create a mixing ratio of SO₂ in the reactor of approximately 150 ppb during three
125 experiments with the three vehicles. Experiments without additional SO₂ were also
126 conducted for each vehicle to compare and additional NO was added to adjust the
127 VOC/NO_x ratios (ppb/ppb) to between 4.9 and 10.8 (Table 2). VOC/NO_x ratios in
128 experiments with the same vehicle were similar with initial concentrations of NO_x
129 ranging from 300.8 to 458.5 ppb. After more than half an hour of primary
130 characterization, the exhaust was exposed to black light continuously for 5 h. The
131 formed SOA was characterized for another 2 to 3 h after the black lamps were
132 switched off to correct the particles wall loss. OH precursor and seed particles were
133 not introduced in this study.

134 An array of instruments was used to characterize gas and particle phase
135 compounds in the reactor. Gas phase NO_x, O₃ and SO₂ were measured with dedicated
136 monitors (EC9810, 9841T, Ecotech, Australia, and Thermo Scientific Model 43iTLE,

137 USA). The detection limit and accuracy of the SO₂ instrument are 0.2 ppb and ±1 %,
138 respectively. Methane and CO concentrations were determined using a gas
139 chromatography (Agilent 6980GC, USA) with a flame ionization detector and a
140 packed column (5A Molecular Sieve 60/80 mesh, 3 m × 1/8 inch) (Zhang et al., 2012).
141 CO₂ was analyzed with a HP 4890D gas chromatography (Yi et al., 2007). Gas phase
142 organic species were measured with a Mode 7100 preconcentrator (Entech
143 Instruments Inc., USA) coupled with an Agilent 5973N gas chromatography-mass
144 selective detector/flame ionization detector/electron capture detector (GC-MSD/FID,
145 Agilent Technologies, USA) (Wang and Wu, 2008, Zhang et al., 2010, 2012, 2013)
146 and a commercial proton-transfer-reaction time-of-flight mass spectrometer
147 (PTR-TOF-MS, Model 2000, Ionicon Analytik GmbH, Austria) (Lindinger et al.,
148 1998; Jordan et al., 2009). C₂-C₃ and C₄-C₁₂ hydrocarbons were measured by GC-FID
149 and GC-MSD, respectively. PTR-TOF-MS was used to determine the time-resolved
150 concentrations of VOCs such as aromatics. The decay curve of toluene was used to
151 derive the average hydroxyl radical (OH) concentration during each experiment.

152 Particle number concentrations and size distributions were measured with a
153 scanning mobility particle sizer (SMPS, TSI Incorporated, USA, classifier model
154 3080, CPC model 3775). An aerosol density of 1.4 g cm⁻³ was assumed to convert the
155 particle volume concentration into the mass concentration (Zhang et al., 2005). A
156 high-resolution time-of-flight aerosol mass spectrometer (HR-TOF-MS, Aerodyne
157 Research Incorporated, USA) was used to measure the particle chemical compositions
158 and nonrefractory PM mass (Jayne et al., 2000; DeCarlo et al., 2006). The instrument

159 was operated in the high sensitivity V-mode and high resolution W-mode alternatively
160 every two minutes. The toolkit Squirrel 1.51H was used to obtain time series of
161 various mass components (sulfate, nitrate, ammonium and organics). We used the
162 toolkit Pika 1.1H to determine the average element ratios of organics, including H:C,
163 O:C, and N:C (Aiken et al., 2007, 2008). The contribution of gas-phase CO₂ to the
164 m/z 44 signal was corrected with measured CO₂ concentrations. The HR-TOF-MS
165 was calibrated using 300 nm monodisperse ammonium nitrate particles.

166 A summary of initial experimental conditions and final results is presented in
167 Table 2 and Table 3, respectively. Total wall-loss corrected OA varied from 17.8 to
168 91.4 µg m⁻³, which spans the typical urban PM concentrations in heavy polluted
169 megacities with poor air quality. POA concentrations of the experiments ranged from
170 0.13 to 0.31 µg m⁻³ and are negligible compared with the formed SOA. Initial mixing
171 ratios of non-methane hydrocarbons (NMHCs) in the reactor were between 2.2 and
172 4.3 ppm, much higher than typical urban conditions. The average OH concentrations
173 during photo-oxidation ranged from 0.73 to 1.29 × 10⁶ molecules cm⁻³, approximately
174 5 times lower than that during summer daytime (Seinfeld and Pandis, 1998). Initial
175 concentrations of the reactants were maintained as similar as possible for the same
176 vehicle, though initial NMHCs, NO_x and average OH concentrations are different
177 from typical urban conditions, so all changes in SOA mass could be attributed to the
178 effects of SO₂.

179 **2.3 SOA production factors**

180 SOA production factor (PF) (mg kg⁻¹) is calculated on a fuel basis:

$$181 \quad PF = 10^6 \cdot [SOA] \cdot \left(\frac{[\Delta CO_2]}{MW_{CO_2}} + \frac{[\Delta CO]}{MW_{CO}} + \frac{[\Delta HC]}{MW_{HC}} \right)^{-1} \cdot \frac{\omega_C}{MW_C} \quad (1)$$

182 where $[\Delta CO_2]$, $[\Delta CO]$, and $[\Delta HC]$ are the background corrected concentrations of
 183 CO_2 , CO and the total hydrocarbons in the reactor in $\mu g\ m^{-3}$; $[SOA]$ is the
 184 concentration of wall-loss corrected SOA in $\mu g\ m^{-3}$; MW_{CO_2} , MW_{CO} , MW_{HC} , and
 185 MW_C are the molecular weights of CO_2 , CO , HC and C . ω_C (0.85) is the carbon
 186 intensity of the gasoline (Kirchstetter et al., 1999). Total hydrocarbons measured in
 187 this study include methane and C_2 - C_{12} hydrocarbons. The carbon content of each
 188 hydrocarbon was respectively calculated and then summed in Eq. (1).

189 2.4 Determination of OH concentration

190 Decay of toluene measured by PTR-TOF-MS is used to determine the average OH
 191 concentration during each experiment. Changes in the toluene concentration over time
 192 can be expressed as:

$$193 \quad \frac{d[toluene]}{dt} = -k \cdot [OH] \cdot [toluene] \quad (2)$$

194 where k is the rate constant for the reaction between toluene and OH radical. The
 195 value of k is obtained from the Master Chemical Mechanism version 3.3 or MCM
 196 v3.3 (<http://www.chem.leeds.ac.uk/MCM>) (Jenkin et al., 2003). Assuming a constant
 197 OH concentration during an experiment, we can integrate Eq. (2) to get Eq. (3):

$$198 \quad \ln\left(\frac{[toluene]_0}{[toluene]_t}\right) = k \cdot [OH] \cdot t \quad (3)$$

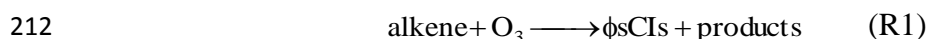
199 So by plotting $\ln([toluene]_0/[toluene]_t)$ versus time t , we can obtain a slope that equals
 200 $k \times [OH]$. The average OH concentration is then calculated as:

$$201 \quad [OH] = \frac{slope}{k} \quad (4)$$

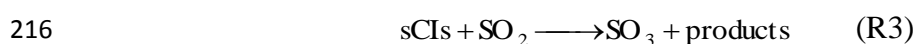
202 Average OH concentrations were determined when the black lamps were on.
 203 Segmented OH concentrations were also estimated and listed in [Table S1](#) in the
 204 Supplement for experiments with the addition of SO₂. Similar concentrations of sCIs
 205 were determined in subsequent section 2.5 when average and segmented OH
 206 concentrations were respectively used for the same experiment.

207 **2.5 Determination of the steady state concentration of sCIs**

208 Ozonolysis of alkenes will form a primary ozonide through a 1,3-cycloaddition of
 209 ozone across the olefinic bond. The primary ozonide then rapidly decomposes to two
 210 carbonyl compounds, called excited CIs, which can be stabilized by collision to form
 211 sCIs ([Heard et al., 2004](#); [Johnson and Marston, 2008](#)).



213 where ϕ represents the yield of sCIs from ozonolysis of alkenes. The four main losses
 214 of sCIs are reactions with H₂O, SO₂ and NO₂ and unimolecular decomposition.



219 The steady state concentration of sCIs will be

$$220 \quad \text{sCIs}_{\text{steady state}} = \frac{\phi K_{R1} [\text{O}_3] [\text{alkene}]}{K_{R2} [\text{H}_2\text{O}] + K_{R3} [\text{SO}_2] + K_{R4} [\text{NO}_2] + K_{R5}} \quad (5)$$

221 where K_{R1} is the rate coefficient for the ozonolysis of alkene; K_{R2} , K_{R3} , K_{R4} and K_{R5}
 222 represent the rate constant for reactions of sCIs with H₂O, SO₂, NO₂ and

223 decomposition, respectively. This equation was widely used to predict the steady state
224 concentration of sCIs in the atmosphere (Welz et al., 2012; Newland et al., 2015).

225 The steady state concentration of sCIs throughout the entire experiment was
226 estimated in this study. The production rate of sCIs was dependent on both the
227 concentrations and composition of alkenes in the exhaust. Detailed gas-phase
228 mechanisms of alkenes from the MCM v3.3 were run to determine the time-resolved
229 concentrations of sCIs in the experiments. The concentrations of alkenes included in
230 the model and the category of sCIs are presented in Table 4. N-alkenes and branched
231 alkenes respectively contributed 89.9%-93.0% and 7.0%-10.1% of the alkenes, with
232 ethene and propene as two main components accounting for 66.8%-81.3%. Only the
233 gas-phase mechanisms of alkenes were included in the model, with the concentrations
234 of OH radicals, SO₂, O₃ and NO₂ constrained to measured concentrations. Thus, the
235 neglect of alkanes and aromatics would not influence the steady state concentrations
236 of sCIs, as was confirmed by running the models including alkanes and aromatics.
237 K_{R2} , K_{R3} , K_{R4} and K_{R5} for CH₂OO, CH₃CHOO, and (CH₃)₂COO used in the model
238 were listed in Table 5. The rate coefficients for other sCIs including C₂H₅CHOO,
239 C₃H₇CHOO, C₂H₅(CH₃)COO and (CH₃)₂CHCHOO reacted with H₂O, SO₂, NO₂ and
240 their unimolecular decomposition were assumed to be same as CH₂OO. This
241 assumption seems reasonable as the precursors of C₂H₅CHOO, C₃H₇CHOO,
242 C₂H₅(CH₃)COO and (CH₃)₂CHCHOO contributed only a small portion of alkenes in
243 this study. The yields of CH₂OO, CH₃CHOO, and (CH₃)₂COO used in the model were

244 0.37, 0.38 and 0.28, respectively, while yields of other sCIs were assumed to be same
245 as CH₂OO.

246 **2.6 Wall loss corrections**

247 The loss of particles and organic vapors onto the reactor walls must be accounted for
248 to accurately quantify the SOA production. A detailed discussion of these corrections
249 can be found elsewhere (Liu et al., 2015). The loss of particles onto the walls was
250 treated as a first-order process (McMurry and Grosjean, 1985). The wall-loss rate
251 constant was determined separately for each experiment by fitting the SMPS and
252 AMS data with first-order kinetics when UV lamps were switched off. By applying
253 this rate to the entire experiment, we use the same method as Pathak et al. (2007) to
254 correct the wall loss of the particles. The wall loss of particles is a size-dependent
255 process, therefore, the presence of nucleation would influence wall loss correction of
256 the particles due to the rapid loss of nucleation mode particles. As shown in a previous
257 study, particle wall loss rates could not be accurately quantified for the particles
258 generated in the nucleation event (Keywood et al., 2004). The impact of the
259 nucleation event on wall-loss estimate is considered to be negligible as less than 5%
260 of the particle mass is in the nucleation mode twenty minutes after nucleation for all
261 experiments in this study.

262 Wall deposition of organic vapors can lead to the underestimation of SOA
263 production (Matsunaga and Ziemann, 2010; X. Zhang et al., 2014, 2015). Wall
264 deposition of a compound has recently been established as related with its volatility
265 (Zhang et al., 2015). The extent that wall deposition of organic vapors impacts on

266 SOA production depends on the competition of organic vapors depositing onto walls
267 and suspended particles. Here, we assumed that gas-particle partitioning of organic
268 vapors dominated their wall depositions and thus organic vapors were considered to
269 only partition onto suspended particles.

270 As the collection efficiency of sulfate in the HR-TOF-AMS can vary due to the
271 coating of OA onto sulfate, we used AMS data combined with SMPS data to derive
272 the time-resolved concentrations of OA, sulfate, ammonium and nitrate. The emission
273 of black carbon (BC) from LDGVs was negligible according to a previous study (Liu
274 [et al., 2015](#)), thus the ratio of OA to inorganic aerosols from the AMS was used to
275 split the total particle mass measured by SMPS into the mass of OA, sulfate,
276 ammonium and nitrate (Gordon [et al., 2014](#); Liu [et al., 2015](#)).

277 **3. Results and discussion**

278 **3.1 Formation of sulfate**

279 [Fig. 2](#) shows the temporal evolution of gas- and particle-phase species during the
280 photochemical aging of emissions from vehicle III with and without adding SO₂. NO
281 was injected to adjust the VOC/NO_x ratio at approximately time = -0.25 h for both
282 experiments. After the black lamps were switched on, NO was rapidly consumed in
283 less than 1 h. Mass concentrations of secondary aerosols rapidly ascended following
284 photooxidation with or without SO₂ for approximately 1 h, stabilizing after
285 approximately 4 h of photo-oxidation ([Figs. 2, 3, and 4](#)). Substantial sulfate was
286 formed synchronously with OA for experiments with SO₂ with the maximum particle
287 number concentrations at 5.4–48 times of those without SO₂ ([Table 1, Fig. 5](#)),

288 indicating enhanced new particle formation (NPF) when adding SO₂. As the precursor
289 of sulfuric acid (H₂SO₄), SO₂ at higher concentrations would lead to additional
290 formation of H₂SO₄, thereby increasing the nucleation rates and total particle number
291 concentrations (Sipila et al., 2010). The S-bearing organic fragments C_xH_yO_zS
292 determined by HR-TOF-AMS can be used as marker ions to quantify organosulfates
293 (Huang et al., 2015). In this study the fragments C_xH_yO_zS were almost not appreciable.
294 Using the methods of Huang et al. (2015), we estimated the mass ratio of
295 organosulfates to sulfate was less than 0.5%. Thus the formation of organosulfates
296 could be negligible in this study.

297 Substantial nitrates were formed for vehicles I and II (Figs. 3a and 4a) and could
298 be attributed to ammonium or organic nitrates. The identification of ammonium and
299 organic nitrates may be obtained from the NO⁺/NO₂⁺ ratio, which is typically
300 substantially higher for organic nitrates compared with ammonium nitrate (Farmer et
301 al., 2010; Sato et al., 2010). The NO⁺/NO₂⁺ ratios for experiments I-2 and II-2 were
302 1.99-2.60, within the range 1.08-2.81 for ammonium nitrate (Farmer et al., 2010; Sato
303 et al., 2010), suggesting that nitrates detected in the two experiments could be
304 attributed to ammonium nitrate. Ammonium nitrate was likely formed by reactions of
305 nitric acid formed from NO_x oxidation and ammonia, which is substantially higher in
306 China's LDGV exhaust (Liu et al., 2014). The NO⁺/NO₂⁺ ratios for experiments with
307 SO₂ were 3.9-5.0, significantly higher than ratios measured for ammonium nitrate and
308 also similar to ratios for organic nitrates (3.82-5.84) from the photo-oxidation of
309 aromatic hydrocarbons (Sato et al., 2010), indicating organic nitrates dominated

310 nitrate formation in these experiments. High concentration of SO₂ suppressed the
311 formation of ammonium nitrate in experiments with SO₂ as NH₃ was liable to react
312 with sulfuric acid rather than nitric acid (Pathak et al., 2009).

313 Formation rates of sulfate, derived from the differential of concentration-time
314 plots of sulfate, exhibited burst increases at the initial stage of sulfate formation and
315 then decreased to near zero 5 h after sulfate formation initiated (Fig. 6a). The
316 maximum formation rate of sulfate in experiments I-2, II-2 and III-2 was 61.5, 21.6
317 and 113 μg m⁻³ h⁻¹, respectively, extremely higher than the rate of 0.17–0.37 ppbv h⁻¹
318 (0.73–1.59 μg m⁻³ h⁻¹ under NTP condition) through gas-phase oxidation of SO₂
319 during the daytime in the Pearl River Delta (PRD) region of China in the summer of
320 2006 (Xiao et al., 2009), and also more than ten times higher than the maximum
321 sulfate formation rate of 4.79 μg m⁻³ h⁻¹ observed at an urban site in Beijing during
322 the Beijing Olympic Games in 2008 (Zhang et al., 2011). The formation rate of sulfate
323 was related to the concentrations of SO₂ and OH, which were respectively
324 approximately 7 times higher and 2-16 times lower than those in the study of Xiao et
325 al. (2009). Significant differences of sulfate formation rates between chamber and
326 ambient observations could, however, indicate that there might be other processes
327 dominating the oxidation of SO₂ rather than gas-phase oxidation by OH in this study.

328 SO₂ was typically deemed to be oxidized by OH radicals through homogeneous
329 reactions in gas-phase (Calvert et al., 1978), or by H₂O₂ and O₃ through in-cloud
330 processes in aqueous-phase (Lelieveld and Heintzenberg, 1992) that, however, could
331 be negligible in this study due to RH of approximate 50%. As shown in Fig. 7, the

332 loss rate of SO₂ through homogeneous reactions with OH radicals in the three
333 experiments ranged from 0.0023 to 0.0034 h⁻¹, accounting for only 2.4%–4.6% of the
334 total loss rate of SO₂. The initial concentrations of alkenes in the experiments with
335 SO₂ varied from 248 to 547 ppb, contributing 7.7%–23.5% of the total NMHCs. The
336 high content of alkenes in the exhaust might form a mass of sCIs through the reaction
337 with ozone. Recent studies indicated the rate coefficient of CH₂OO with SO₂ was 50
338 to 10000 times larger than that used in tropospheric models (Welz et al., 2012). The
339 oxidation of SO₂ by sCIs may be as significant as that by OH radicals in the
340 atmosphere. The oxidation rate of SO₂ for experiments I-2 and III-2, through the
341 reactions with sCIs, was calculated to be 0.065 ± 0.029 h⁻¹ and 0.042 ± 0.020 h⁻¹ (Fig. 7),
342 respectively, accounting for 66.9% and 61.4% of the total loss rate of SO₂.
343 Considering the variability of sCIs throughout the entire experiment, we concluded
344 that sCIs were virtually responsible for the oxidation of SO₂ in experiments I-2 and
345 III-2. The oxidation rate of SO₂ through the reactions with sCIs for the experiment
346 II-2 was estimated to be 0.028 ± 0.015 h⁻¹, contributing 31.5% of the total loss rate of
347 SO₂. The unexplained loss of SO₂ might be a result of heterogeneous oxidation in the
348 presence of LDGV exhaust containing massive aerosols and gaseous species. He et al.
349 (2014) found that SO₂ could react with NO₂ on the surface of mineral dust to promote
350 the conversion of SO₂ to sulfate. As shown in Fig. 5, the initial particle number for
351 vehicle II was approximately 5000 cm⁻³, nearly 40-50 times higher than those for
352 vehicle I and III, providing larger aerosol surface areas for the oxidation of SO₂ by
353 NO₂. However, quantification of SO₂ oxidation by NO₂ on the surface of existing

354 aerosols is difficult due to the lack of reaction rate constant (He et al., 2014). We
355 speculate that the reaction between SO₂ and NO₂ on the surface of existing aerosols
356 might explain the difference between the total loss rate of SO₂ and the sum of sCIs
357 and OH oxidation for vehicle II.

358 3.2 SOA production

359 Fuel-based SOA production factors (PF), expressed as SOA production in milligram
360 (mg) after 5 h photooxidation of LDGV exhaust emitted when per kilogram (kg)
361 gasoline was burned, all increased substantially when adding SO₂, 60%–200% above
362 that without SO₂ (Fig. 8a), although the selected cars' emission standards varied from
363 Euro-I to Euro-IV. The in-situ particle acidities at the time when SOA formation rate
364 peaks were calculated as H⁺ concentrations based on AIM-II model H⁺–NH₄⁺–SO₄²⁻–
365 NO₃⁻–H₂O with gas-aerosol partitioning disabled
366 (<http://www.aim.env.uea.ac.uk/aim/model2/model2a.php>) (Clegg et al., 1998; Wexler
367 and Clegg, 2002). Inputs to the model include temperature, RH, [SO₄²⁻], [NO₃⁻],
368 [NH₄⁺] and [H⁺]_{total}, calculated based on ion balance. SO₄²⁻, NH₄⁺ and NO₃⁻
369 contributed virtually all of the aerosol phase ions mass in this study, thus determining
370 the aerosol acidity. Though other ions (i.e., Ca²⁺, Mg²⁺, K⁺ and Na⁺) had negligible
371 influence on the aerosol acidity, it is worth noting that the reported values of H⁺ may
372 be the upper bound. The in-situ particle acidities with the addition of SO₂ were 1.6–
373 3.7 times as high as those without the addition of SO₂ (Table 3). This elevated particle
374 acidity could largely explain the higher PFs of SOA from LDGV exhaust with SO₂,
375 supported by the strong positive linear correlations ($R^2 = 0.965$, $P < 0.01$) between

376 SOA PFs and the in-situ particle acidities (Fig. 8b). Aromatic hydrocarbons are vital
377 SOA precursors in gasoline vehicle exhaust (Nordin et al., 2013; Gordon et al., 2014;
378 Liu et al., 2015). The influence of particle acidity on SOA formation from aromatics
379 is still debatable. Cao and Jang (2007) found that the presence of acid seeds with $[H^+]$
380 concentrations of 240-860 nmol m^{-3} significantly increased the SOA yields from
381 oxidation of toluene and 1,3,5-trimethylbenzene compared with yields using neutral
382 seed aerosols. However, Ng et al. (2007) observed no influence of particle acidity on
383 SOA yields from the aromatics possibly due to the low content of aerosol water. SOA
384 production from gasoline vehicle exhaust was enhanced in this study, even at a low
385 level of $[H^+]$ concentrations ranging from 7.4 to 27.1 nmol m^{-3} . Gas-phase oxidation
386 products of aromatic hydrocarbons in the exhaust, like multifunctional carbonyl
387 glyoxal, would be transformed more rapidly to low volatility products through
388 acid-catalyzed heterogeneous reactions (Jang et al., 2002; Cao and Jang, 2007) and
389 thus caused increasing SOA production. Aerosol water is needed for the hydration of
390 carbonyls and therefore it influences the acid-catalyzed reactions. Liquid water
391 content (LWC) in this study was not measured but predicted by the AIM-II model,
392 with an average value of $5.5 \pm 4.5 \mu\text{g m}^{-3}$ when SOA formation rate peaks, ensuring
393 the occurrence of acid-catalyzed reactions. Fig. 9 shows the ion intensity of fragment
394 m/z 88 that can arise only from a glyoxal oligomer (Liggio et al., 2015). The scatter of
395 the data might be due to the low intensity of m/z 88. However, the experiment with
396 the addition of SO_2 , with higher particle acidity, exhibited relatively higher m/z 88
397 intensity. This indicated the important role of acid-catalyzed heterogeneous reactions

398 in SOA formation from gasoline vehicle exhaust. A photo-oxidation experiment of
399 exhaust from vehicle I in the presence of ammonium sulfate seeds ($53.3 \mu\text{g m}^{-3}$) with
400 RH of 59% (Table 2) was conducted to explore the effect of sulfate on SOA formation
401 as particle acidity is typically driven by sulfate. The SOA production factor was 22.2
402 mg kg^{-1} fuel, comparable with 26.2 mg kg^{-1} fuel for experiment I-1, indicating that
403 sulfate may not directly influence SOA production. Thus, the SOA production was
404 indeed dependent on the particle acidity.

405 The addition of SO_2 may vary the vapor wall loss rate and influence the
406 estimation of SOA production. The wall accommodation coefficient ($\alpha_{w,i}$), governing
407 the extent of wall deposition of a compound i , was observed to be inversely dependent
408 on its effective saturation concentration C_i^* (X. Zhang et al., 2015). Partitioning
409 coefficients for different C_i^* ranging from 0.01 to $10^6 \mu\text{g m}^{-3}$ were calculated using
410 gas-particle partitioning theory (Donahue et al., 2006) (Table 6). Partitioning
411 coefficients for experiments with and without the addition of SO_2 mainly exhibited
412 big differences for C_i^* bins of 10 and $100 \mu\text{g m}^{-3}$ with $\alpha_{w,i}$ calculated to be 3.1×10^{-7}
413 and 2.0×10^{-7} , respectively. The wall loss rate for C_i^* bin of $10 \mu\text{g m}^{-3}$ would then be
414 approximately 50% higher than that for C_i^* bin of $100 \mu\text{g m}^{-3}$ assuming a linear
415 relation between wall loss rate and $\alpha_{w,i}$ (X. Zhang et al., 2015). An increase of 50% in
416 wall loss rate would lead to 11.5% higher vapor loss to walls when assuming the wall
417 loss rate to be $2.0 \times 10^{-5} \text{ s}^{-1}$, similar to a product of the photo-oxidation of toluene.
418 Thus, biases of vapor wall loss rates due to the addition of SO_2 may have negligible
419 influence on estimation of SOA production. Recent studies indicated that the presence

420 of high concentrations of seed aerosols might decrease the loss of organic vapors to
421 the walls and thus increase the SOA formation (Kroll et al., 2007; X. Zhang et al.,
422 2014, 2015). However, comparable SOA PFs for experiments with and without seed
423 aerosols observed in this study indicated the negligible impact of seed aerosols on
424 SOA production. Cocker III et al. (2001) also observed that the presence of
425 ammonium sulfate seed aerosols had no impact on SOA formation from the
426 photo-oxidation of m-xylene and 1,3,5-trimethylbenzene .

427 SOA formation rates, derived from the differential of concentration-time plots of
428 SOA, exhibited similar trends as sulfate with a burst increase at the initial stage of
429 SOA formation (Fig. 6b). The average SOA formation rates for vehicles I, II and III
430 with SO₂ were 1.1, 1.2 and 4.4 times as high as those without SO₂, respectively,
431 although the maximum rate for vehicle II with SO₂ was lower. Here we particularly
432 focused on the burst increase stage of SOA and sulfate, which may be related to fast
433 increase of PM_{2.5} and occurrence of haze (He et al., 2014). Fig. 10 shows the
434 correlation between SOA formation rate and particle acidity. Plotted data
435 corresponded to data selected from Fig. 6 when SOA formation rate was higher than
436 zero to when the rate reached the maximum value. Significant linear correlations
437 ($P < 0.05$, $R^2 > 0.88$) between SOA formation rate and particle acidity during this stage
438 for experiments with SO₂ suggest that acid-catalyzed heterogeneous reactions might
439 play an important role in the rapid formation of SOA (Jang et al., 2002). The fitted
440 slopes for vehicle I, II and III were 3.96, 0.82 and 3.14, respectively, suggesting other
441 factors, including alkene abundance, may influence the SOA formation rate. The

442 initial concentration of alkenes for experiments I-2, II-2 and III-2 was 547 ppb, 248
443 ppb and 353 ppb, respectively, consistent with the variation of the slopes. Higher
444 alkene content would increase the formation rate of sCIs, which could rapidly oxidize
445 SO₂ to sulfuric acid, thus influence the aerosol acidity.

446 **3.3 Oxidation state**

447 After 5 h of photo-oxidation, SOA's molar ratios of oxygen-to-carbon (O:C) and
448 hydrogen-to-carbon (H:C) resolved by HR-TOF-AMS, were plotted on a Van
449 Krevelen diagram (Heald et al., 2010) in Fig. 11. Concentrations of POA were lower
450 than 0.5 μg m⁻³, typically regarded as not appreciable (Presto et al., 2014) and
451 insufficient to determine the initial H:C and O:C, thus only SOA data were plotted on
452 the diagram. Relatively lower O:C (0.44±0.02) and higher H:C (1.40±0.03) for the
453 mixture of SO₂ and exhaust were observed than those for exhaust alone. The
454 oxidation state of carbon (OS_c), estimated from O:C and H:C, can be used to describe
455 the chemistry and oxidative evolution of atmospheric organic aerosols (Kroll et al.,
456 2011). Further calculated OS_c revealed an average lower level of -0.51±0.06 for SOA
457 formed from LDGV exhaust with SO₂ when compared to that of -0.19±0.08 without
458 SO₂, with all within or near the OS_c range of -0.5–0 for semi-volatile OOA (SV-OOA)
459 (Aiken et al., 2008). The relatively lower OS_c with SO₂ indicated a lower oxidation
460 degree of SOA. A difference in H:C and O:C for m-xylene SOA with neutral and
461 acidic seed particles was not observed by Loza et al. (2012), thus acid-catalyzed
462 heterogeneous reactions may not influence the oxidation degree of SOA in this study.
463 Shilling et al. (2009) observed a lower O:C of SOA formed from the dark ozonolysis

464 of α -pinene at a higher mass loading of organic aerosols and suggested that
465 compounds partitioning into the particle phase at lower loadings were more
466 oxygenated. Kang et al. (2011) also observed that the oxidation degree of OA
467 decreased rapidly as the OA mass concentration increased for the same amount of OH
468 exposure. Given that the average OH concentrations were similar for the same vehicle
469 (Table 2), the relative higher mass loading of OA in the experiments with SO₂ may
470 lead to the lower O:C and thus decrease the oxidation degree of OA. The O:C ratios
471 were observed to decrease 0.1 with an increase of approximately 50 $\mu\text{g m}^{-3}$ of OA
472 concentrations for m-xylene and p-xylene (Kang et al., 2011). However, in this study
473 the slope was 0.1 $\Delta\text{O:C}$ for approximately 26 $\mu\text{g m}^{-3}$ ΔOA . The differences may be
474 due to that some other precursors other than aromatics contributed to SOA formation
475 from gasoline vehicle exhaust (Liu et al., 2015).

476 The slope of -0.87 (Fig. 11) for the mixture of SO₂ and exhaust, slightly higher
477 than those for exhaust alone (Liu et al., 2015), indicates that SOA formation in these
478 experiments is a combination of carboxylic acid and alcohol/peroxide formation
479 (Heald et al., 2010; Ng et al., 2011). The slope of -0.87 and intercept of approximately
480 1.8 are similar to the observation for ambient data with a slope of approximately -1
481 and intercept approximately 1.8 (Heald et al., 2010), suggesting that SOA chemistry
482 for the mixture of SO₂ and gasoline vehicle exhaust is atmospheric relevant.

483 **4. Conclusions**

484 A series of chamber experiments investigating the formation of secondary aerosols
485 from the mixture of SO₂ and gasoline vehicle exhaust were conducted. The high

486 content of alkenes in gasoline vehicle exhaust formed numerous sCIs, dominating the
487 formation of sulfate while elevated particle acidity, resulting from the formation of
488 sulfuric acid, enhanced SOA production from the gasoline vehicle exhaust. We
489 concluded that SO₂ and gasoline vehicle exhaust can enhance each other in forming
490 secondary aerosols. High concentration of SO₂ and high levels of aerosol acidity
491 combined with rapid increase of LDGVs in heavily polluted cities such as Beijing
492 (Pathak et al., 2009; He et al., 2014) might consequently worsen the air quality in the
493 absence of stricter control strategies on emissions of SO₂ and vehicle exhaust.
494 Previous studies indicated that high content of alkenes in China's gasoline oil was
495 damaging for the control of ozone in ambient air (Y. Zhang et al., 2013, 2015). Our
496 results suggested that the incomplete combustion of gasoline with high content of
497 alkenes might also induce the formation of sCIs, facilitating the production of
498 secondary aerosols. The limit of alkenes content in China was lowered to 24% by
499 volume in the newly established Level V gasoline fuel standard from 28% by volume
500 in the Level IV gasoline fuel standard. This limit remains substantially higher when
501 compared to those in USA or in Europe, and in particular, 6 times that in California,
502 USA. Thus, limiting the content of alkenes in China's gasoline might benefit the
503 control of both ozone and secondary aerosols.

504

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799 **Table 1.** Detailed information of the three LDGVs.

ID	Emission standard class	Vehicle	Model year	Mileage (km)	Displacement (cm ³)	Power (kW)	Weight (kg)
I	Euro4	Golf	2011	25000	1598	77	1295
II	Euro4	Sunny	2011	9448	1498	82	1069
III	Euro1	Accord	2002	237984	2298	110	1423

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802

803 **Table 2.** Summary of the initial conditions during the photooxidation of LDGV
 804 exhaust.

Exp # ^a	OH ($\times 10^6$ molecules cm^{-3})	T (°C)	RH (%)	VOC /NO _x	NMHCs (ppbv)	NO (ppbv)	NO ₂ (ppbv)	SO ₂ (ppbv)
I-1	0.88	25.0±0.8	52.9±2.0	9.3	2896	300.6	9.5	8.6
I-2	1.19	25.5±0.3	53.6±2.5	7.7	2323	281.4	19.5	151.8
I-3 ^b	1.45	23.9±0.9	59.0±4.1	7.9	2447	300.0	10.2	8.9
II-1	1.29	24.6±0.5	52.5±1.7	10.8	4313	374	24.7	9
II-2	1.08	24.2±0.7	55.9±2.5	9	3220	356	2.6	151.9
III-1	0.73	24.1±0.6	57.0±2.0	6	2582	431	0.6	9.2
III-2	0.79	24.3±0.3	57.9±1.2	4.9	2243	454.6	3.9	154.1

805 ^a Photooxidation experiments of LDGV exhaust named with I, II and III refers to different
 806 vehicles.

807 ^b Ammonium sulfate ($53.3 \mu\text{g m}^{-3}$) was introduced as seed aerosols.

808

809 **Table 3.** Summary of the final results during the photooxidation of LDGV exhaust.

Exp #	POA ($\mu\text{g m}^{-3}$)	SOA ($\mu\text{g m}^{-3}$)	Sulfate ($\mu\text{g m}^{-3}$)	Ammonium ($\mu\text{g m}^{-3}$)	Nitrate ($\mu\text{g m}^{-3}$)	Particle number (cm^{-3}) ^a	[H ⁺] ^b (nmol m^{-3})
I-1	0.31	77.6	0.7	17.1	65.9	85182	12.5
I-2	0.21	91.2	67.5	17.6	6.1	563705	21.9
II-1	0.28	30.7	-	2.6	5.6	7427	10.4
II-2	0.13	37.3	38.1	9.7	1.9	357673	16.5
III-1	0.17	17.6	-	0.1	0.7	116143	7.4
III-2	0.23	77	76.7	19.2	5.3	630620	27.1

810 ^a Maximum particle number concentrations were without wall loss corrections.

811 ^b The concentration of H⁺ in particle phase shown here was the value when the SOA formation rate
 812 reached the maximum during each experiment.

813

814 **Table 4.** Concentrations of alkenes included in the model and the category of sCIs.

Species	Concentration (ppb)			sCIs
	I-2	II-2	III-2	
ethene	333.1	113.8	202.0	CH ₂ OO
propene	95.8	50.3	52.6	CH ₂ OO, CH ₃ CHOO
1-butene	30.9	49.1	13.1	CH ₂ OO, C ₂ H ₅ CHOO
cis-2-butene	7.6	4.8	7.1	CH ₃ CHOO
trans-2-butene	9.9	6.4	9.6	CH ₃ CHOO
1-pentene	3.8	0.3	3.1	CH ₂ OO, C ₃ H ₇ CHOO
cis-2-pentene	5.2	1.2	5.2	CH ₃ CHOO, C ₂ H ₅ CHOO
trans-2-pentene	8.5	2.6	9.4	CH ₃ CHOO, C ₂ H ₅ CHOO
2-methyl-1-butene	11.9	5.4	12.4	CH ₂ OO, C ₂ H ₅ (CH ₃)COO
3-methyl-1-butene	2.4	0.8	2.4	CH ₂ OO, (CH ₃) ₂ CHCHOO
2-methyl-2-butene	17.8	10.9	22.7	CH ₃ CHOO, (CH ₃) ₂ COO
cis-2-hexene	0.8	0	1.5	CH ₃ CHOO, C ₃ H ₇ CHOO

815

816

817 **Table 5.** Summary of the final results during the photooxidation of LDGV exhaust.

Stabilized CIs	$10^{15} K_{R2}$ ($\text{cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$)	$10^{11} K_{R3}$ ($\text{cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$)	$10^{12} K_{R4}$ ($\text{cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$)	K_{R5} (s^{-1})
CH ₂ OO	0.025 ^a	3.9 ^b	7.0 ^b	0 ^c
CH ₃ CHOO	7.0 ^d	4.55 ^d	2.0 ^d	67.5 ^e
(CH ₃) ₂ COO	2.1 ^c	2.4 ^c	2.0 ^c	151 ^c

818 ^a (Ouyang et al., 2013); ^b (Welz et al., 2012); ^c (Newland et al., 2015); ^d (Taatjes et al., 2013);

819 ^e Average of K_{R5} from Fenske et al. (2000) and Newland et al. (2015).

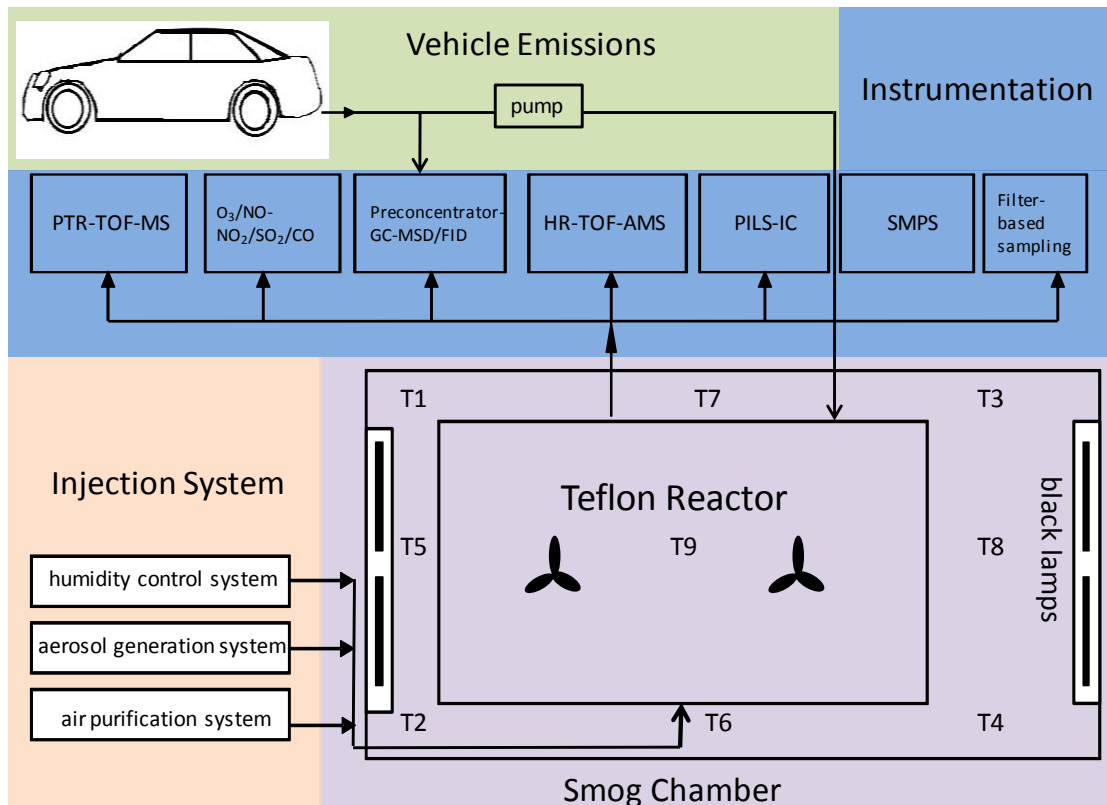
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821 **Table 6.** Partitioning coefficients for different C_i^* calculated using gas-particle
 822 partitioning theory.

$\log_{10} C_i^*$ ($\mu\text{g m}^{-3}$)	I-1	I-2	II-1	II-2	III-1	III-3
-2	1.000	1.000	1.000	1.000	0.999	1.000
-1	0.999	0.999	0.997	0.997	0.994	0.999
0	0.987	0.989	0.968	0.974	0.946	0.987
1	0.886	0.901	0.754	0.789	0.638	0.885
2	0.437	0.477	0.235	0.272	0.150	0.435
3	0.072	0.084	0.030	0.036	0.017	0.071
4	0.008	0.009	0.003	0.004	0.002	0.008
5	0.001	0.001	0.000	0.000	0.000	0.001
6	0.000	0.000	0.000	0.000	0.000	0.000

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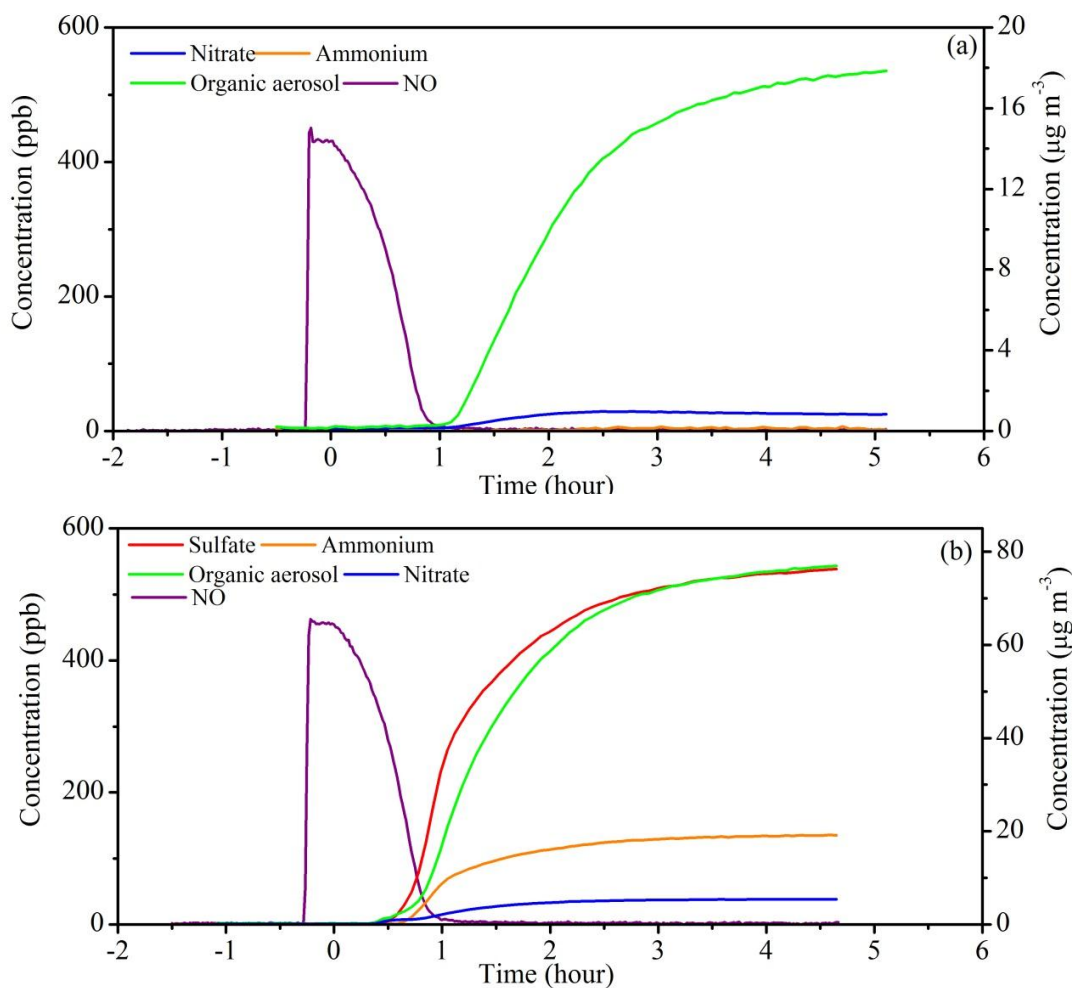
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826 **Fig. 1.** Schematic of the GIG-CAS smog chamber facility and vehicle exhaust
 827 injection system.

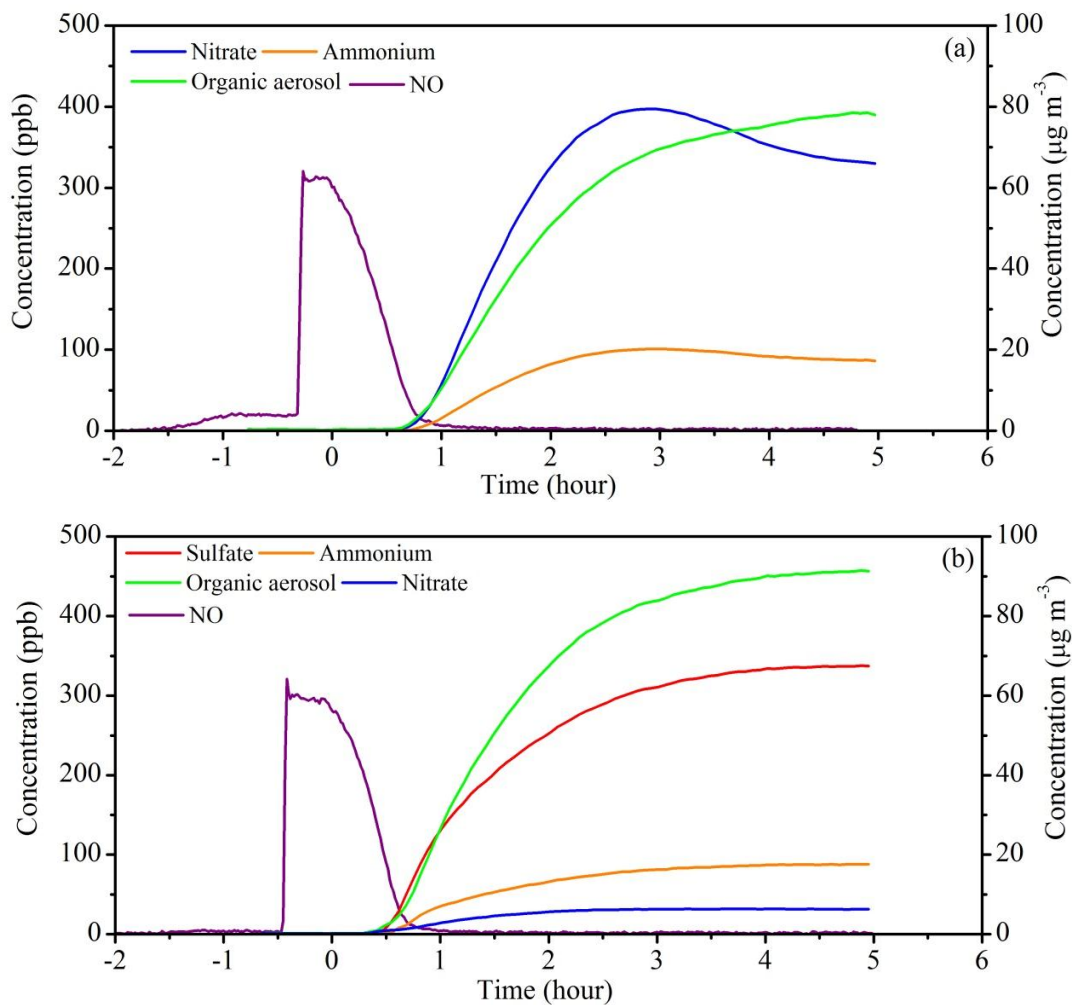
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830 **Fig. 2.** Concentration–time plots of NO (left-y axis) and particle–phase species
 831 (right-y axis) during the photochemical aging of emissions from vehicle III. (a)
 832 Without SO_2 , and (b) with SO_2 . The concentrations of particle-phase species are
 833 wall-loss corrected. At time =0 h, the black lamps were turned on.

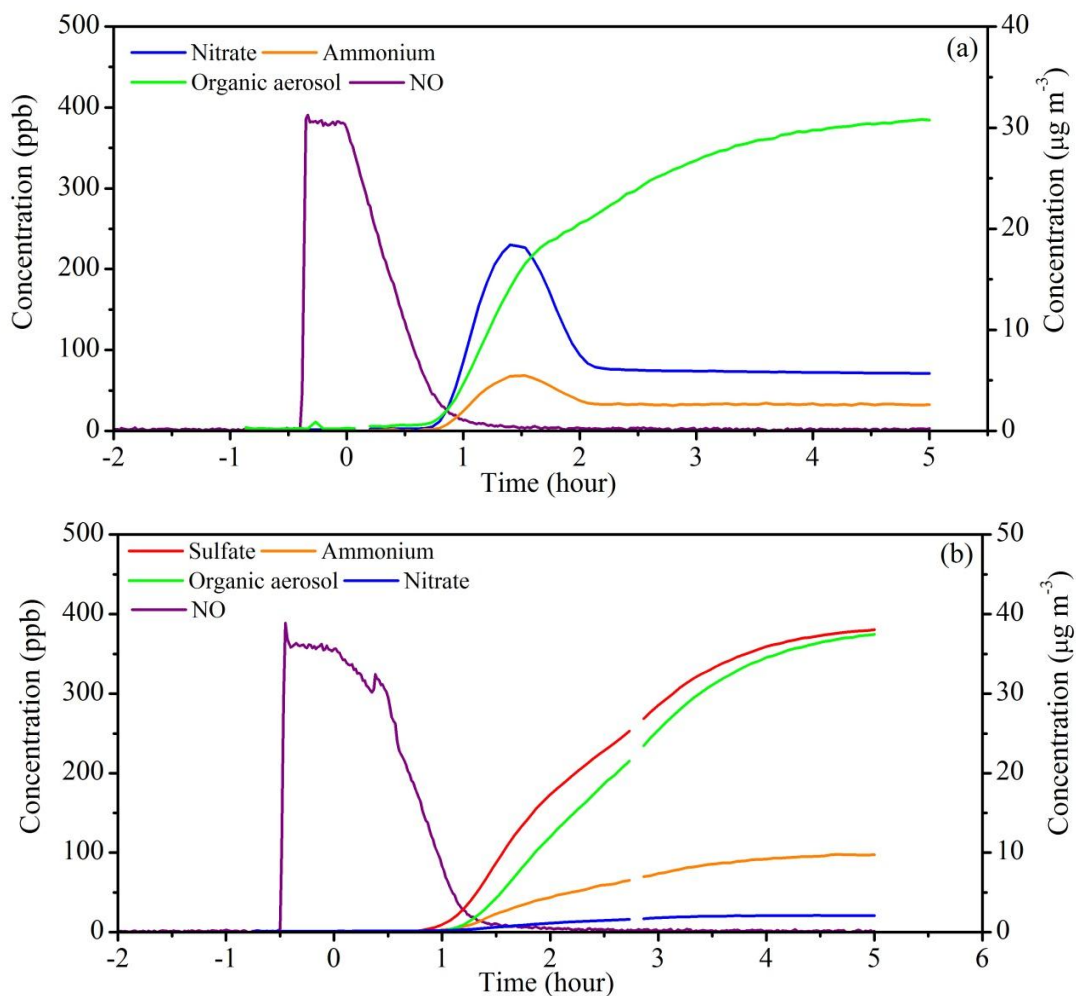
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836 **Fig. 3.** Concentration–time plots of NO (left-y axis) and particle–phase species
 837 (right-y axis) during the photochemical aging of emissions from vehicle I. (a) Without
 838 SO_2 , and (b) with SO_2 . The concentrations of particle-phase species are wall-loss
 839 corrected. At time =0 h, the black lamps were turned on.

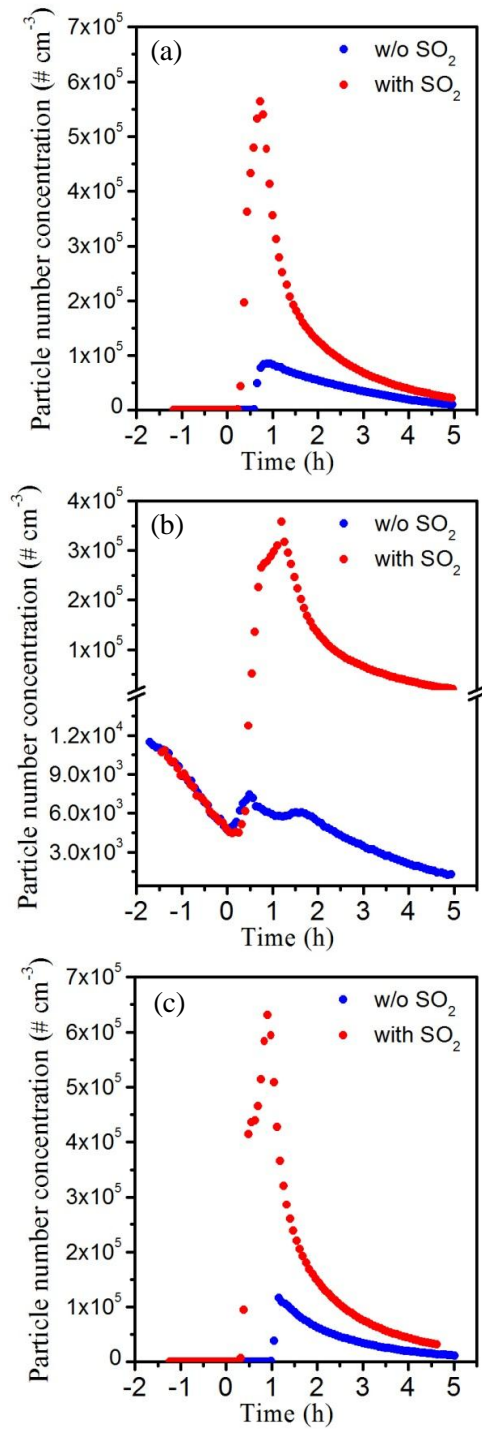
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842 **Fig. 4.** Concentration–time plots of NO (left-y axis) and particle–phase species
 843 (right-y axis) during the photochemical aging of emissions from vehicle II. (a)
 844 Without SO_2 , and (b) with SO_2 . The concentrations of particle-phase species are
 845 wall-loss corrected. At time =0 h, the black lamps were turned on.

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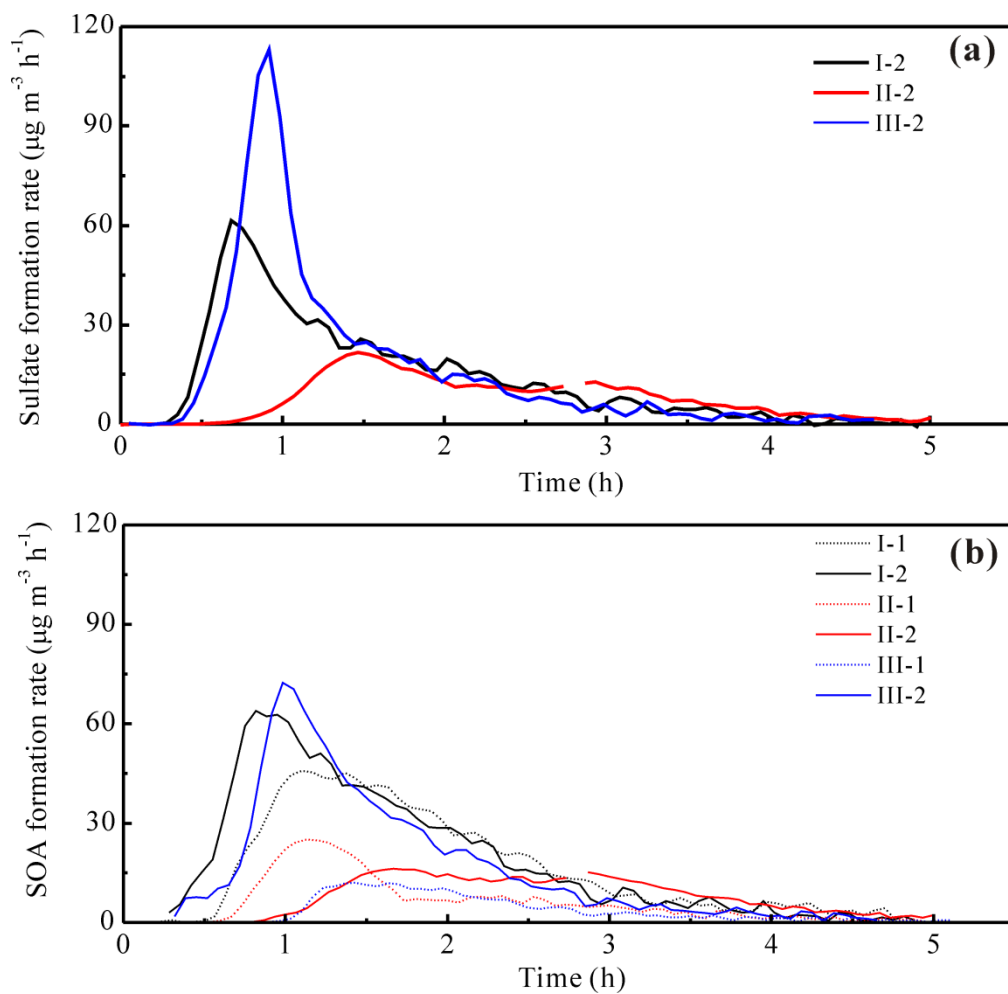
848 **Fig. 5.** Evolution of particle number concentrations during the aging experiments of

849 LDGV exhaust for vehicle I (a), II (b) and III (c). At time =0 h, the black lamps were

850 turned on. W/o SO₂ and with SO₂ in the figures represent experiments without and

851 with adding SO₂, respectively.

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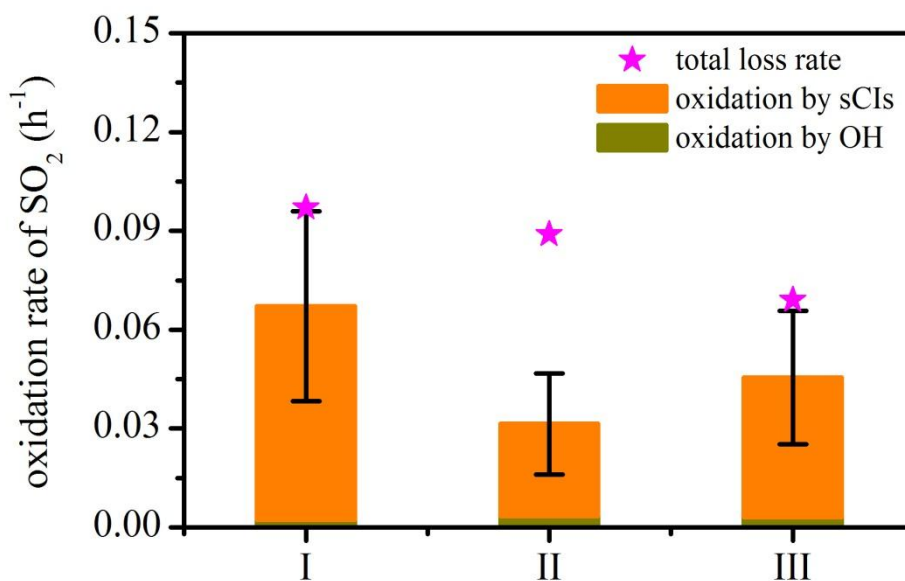


853

854 **Fig. 6.** Sulfate formation rates (a) and SOA formation rates (b) as a function of time

855 during the photooxidation of LDGV exhaust.

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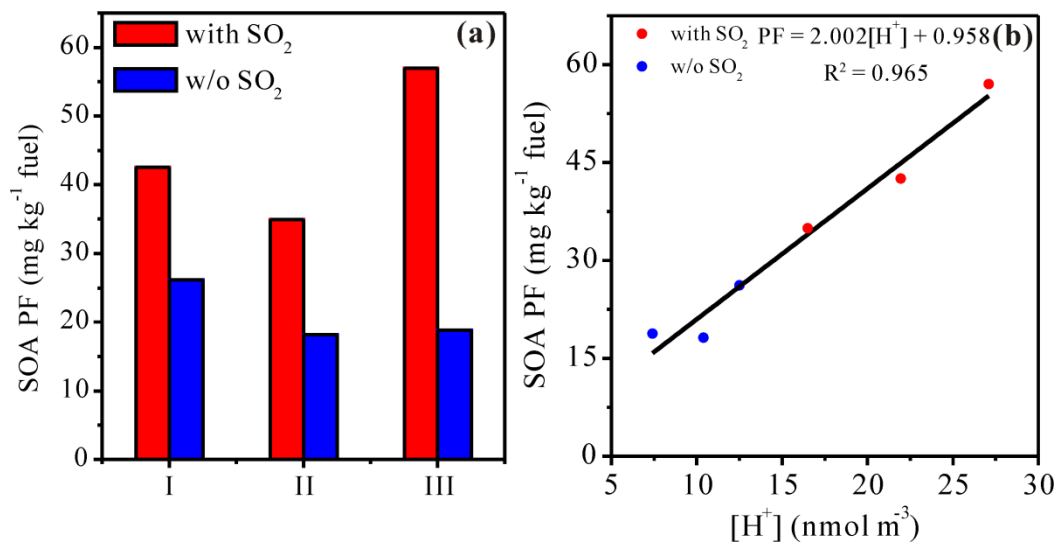


857

858 **Fig. 7.** The oxidation rate of SO₂ during the photooxidation of LDGV exhaust with
 859 SO₂. The loss rates of SO₂ reacting with OH radicals and sCIs were calculated by
 860 multiplying the reaction rate coefficients derived from the MCM v3.3 by the average
 861 OH concentration and estimated sCIs concentration, respectively. Error bars represent
 862 the standard derivation (1σ) of the oxidation rate of SO₂ by sCIs throughout the whole
 863 experiment.

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866

867 **Fig. 8.** SOA production factor (PF) and its relationship with particle acidity. **(a)** SOA

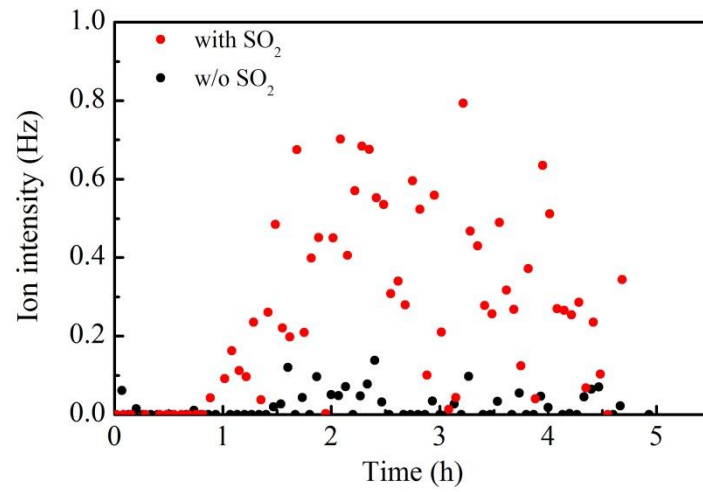
868 PF after 5 h of photochemical aging of exhaust from different LDGVs with and

869 without additional SO₂. **(b)** SOA PF as a function of in-situ particle acidity. The

870 concentration of H⁺ in particle phase shown here was the value when the SOA

871 formation rate reached the maximum during each experiment.

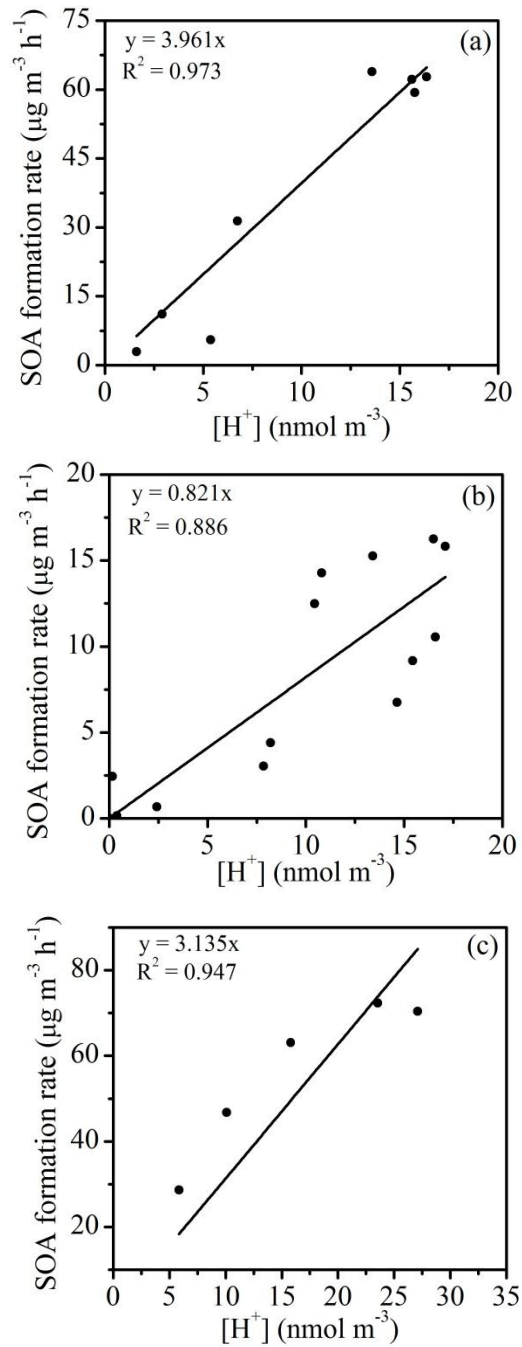
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874 **Fig. 9.** Time evolution of m/z 88 during the aging of LDGV exhaust from vehicle III.

875

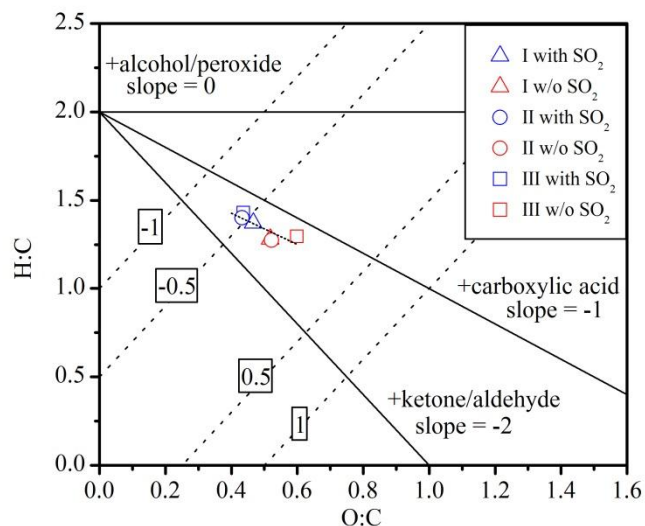


876

877 **Fig. 10.** SOA formation rate as a function of in-situ particle acidity ($[\text{H}^+]$) for vehicle
 878 I (a), vehicle II (b) and vehicle III (c) with adding SO_2 . Plotted data were selected
 879 from when SOA formation rate was higher than zero to when the rate reached the
 880 maximum value.

881

882



883

884 **Fig. 11.** O:C vs. H:C of SOA formed from LDGV exhaust with and without additional
 885 SO₂ at the end of each experiment. Blue and red symbols represent data with and
 886 without additional SO₂, respectively. The dashed lines represent estimated average
 887 carbon oxidation states of -1, -0.5, 0.5 and 1 (Kroll et al., 2011). The black lines
 888 represent the addition of functional groups to an aliphatic carbon (Heald et al., 2010).