Technique Note: Application of positive matrix factor analysis in
heterogeneous kinetics studies utilizing the mixed-phase relative
rates technique
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23 Abstract:

The mixed-phase relative rate approach for determining aerosol particle organic 24 heterogeneous reaction kinetics is often performed utilizing mass spectral tracers as a 25 26 proxy for particle phase reactant concentration. However, sometimes this approach 27 may be influenced by signal contamination from oxidation products during the experiment. In the current study, the mixed-phase relative rates technique has been 28 improved by combining a Positive Matrix Factor (PMF) analysis with electron 29 ionization Aerosol Mass Spectrometry (unit mass resolution), thereby removing the 30 31 influence of m/z fragments from reaction products on the reactant signals. To demonstrate the advantages of this approach, the heterogeneous reaction between OH 32 33 radicals and citric acid (CA) was investigated using a photochemical flow tube coupled to a compact time-of-flight aerosol mass spectrometer (C-ToF-AMS). The 34 measured heterogeneous rate constant (k_2) of citric acid toward OH was 35 $(3.31\pm0.29)\times10^{-12}$ cm³ molecule⁻¹ s⁻¹ at 298 K and (30 ± 3) % RH and was several 36 37 times greater than the results utilizing individual m/z fragments. This phenomenon was further evaluated for particulate-phase organophosphates (TPhP, TDCPP, and 38 TEHP), leading to k_2 values significantly larger than previously reported. The results 39 suggest that heterogeneous kinetics can be significantly underestimated when the 40 structure of the products is highly similar to the reactant and when a non-molecular 41 tracer is measured with a unit mass resolution aerosol mass spectrometer. The results 42 also suggest that the heterogeneous lifetime of organic aerosol in models can be 43

44	overestimated due to underestimated OH uptake coefficients. Finally, a comparison of
45	reported rate constants implies that the heterogeneous oxidation of aerosols will be
46	dependent upon a number of factors related to the reaction system, and that a single
47	rate constant for one system cannot be universally applied under all conditions.
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67 **1. Introduction**

68 Reaction kinetics data provide key parameters for both air quality and climate models. They are required to compute the trace gas and particle matter (PM) content 69 70 of the atmosphere (Kolb et al., 2010) and to evaluate the atmospheric lifetime and fate for individual species. Organic particles make up 10-90 % of the global submicron 71 particle mass in the lower troposphere (Zhang et al., 2011), and is comprised of 72 various reactive organic species, which are subject to atmospheric heterogeneous 73 74 oxidation. Previous studies have found that heterogeneous reactions with OH in particular, can lead to an increase in density, CCN activation (George and Abbatt, 75 2010) and optical extinction (Cappa et al., 2011) of organic particulate matter. 76 77 Therefore, there is a growing interest in understanding not only the mechanism of PM transformation through heterogeneous reactions including oxidation, but also 78 determining the rates at which organic aerosols are chemically transformed in the 79 atmosphere. 80

To this end, Donahue et al. (Donahue et al., 2005) and Hearn and Smith (Hearn and Smith, 2006) developed a mixed-phase relative rate technique for measuring organic PM component heterogeneous reaction kinetic rate constants. In this method, the rate constant of the compound of interest is determined from the decrease of its particle phase relative concentration as a function of oxidant exposure. The oxidant levels are simultaneously estimated via the measured loss of a gas phase reference compound after applying the known second-order rate constant (k_2) toward the 88 oxidant. In this approach the rates of chemical change are given by,

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$$-\frac{dc_{A}}{dt} = k_{2,A}c_{A}c_{Ox}$$
 (1)
90 $-\frac{dc_{R}}{dt} = k_{2,R}c_{R}c_{Ox}$ (2)

where c_A , c_R and c_{Ox} are the particle phase concentration of the compound of interest 91 92 (A), the gas phase concentration of the reference compound (R) and oxidant (molecules cm⁻³) respectively, while $k_{2,A}$ and $k_{2,R}$ are the second-order rate constant of 93 A and R to the oxidant (cm³ molecule⁻¹ s⁻¹). A relative rate constant (k_r) (ie: particle 94 phase reaction rate of A, relative to the gas phase rate of R) can be derived by dividing 95 96 Eq. (1) by Eq. (2). The derivation of k_r provides a means to obtain heterogeneous kinetic data without the need to know the absolute concentration of the oxidant. The 97 differential and integral forms for the relative rates technique are shown as Eq. (3) and 98 99 (4),

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$$\frac{dc_A}{c_A} = \frac{k_{2,A}}{k_{2,R}} \frac{dc_R}{c_R} = k_r \frac{dc_R}{c_R}$$
 (3)

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$$\log \frac{c_{\rm A}}{c_{\rm A,0}} = k_{\rm r} \log \frac{c_{\rm R}}{c_{\rm R,0}}$$
 (4)

from which the relative rate constant (k_r) , is the slope of the line derived by plotting the logarithmic relative concentration of A against that of R (relative to initial conditions; $c_{A,0}$). The second-order heterogeneous rate constant of the compound of interest $(k_{2,A})$ towards the oxidant may then be calculated using the obtained k_r and the known $k_{2,R}$ (ie: $k_{2,A} = k_r \times k_{2,R}$).

Using this method, a number of studies have quantified the uptake coefficients of O₃, OH, Cl, and NO₃ on various organic particles, and the corresponding second order rate constants for the degradation of organic compounds (Hearn and Smith, 2006;George et al., 2007;Lambe et al., 2007;McNeill et al., 2007;McNeill et al.,
2008;Smith et al., 2009;Kessler et al., 2010;Renbaum and Smith, 2011;Kessler et al.,
2012;Liu et al., 2012;Sareen et al., 2013).

Although gas chromatograph mass spectrometry (GC-MS) has been widely used 113 in the kinetics studies (Weitkamp et al., 2008a; Weitkamp et al., 2008b; Lambe et al., 114 115 2009; Isaacman et al., 2012), quantifying the particle phase loss of an organic 116 compound in such studies often relies upon aerosol mass spectrometry techniques to monitor specific particle phase reactant ions of interest in semi-real time. Aerosol 117 mass spectrometry instruments utilizing high resolution detection and soft ionization 118 119 techniques, such as chemical ionization (Aerosol CIMS) (Hearn and Smith, 2006;McNeill et al., 2007;McNeill et al., 2008;Renbaum and Smith, 2011;Sareen et 120 121 al., 2013) and vacuum ultraviolet photo-ionization (VUV-ATOFMS)(Liu et al., 2012), have been utilized to measure the concentration of the target organic compounds in 122 particles. However, Aerosol Time-of-Flight or Quadrupole Mass Spectrometry 123 (ToF-AMS or Q-AMS) employing electronic ionization (EI; 70 eV) as an ion source 124 remains the prevalent instrument used in such organic particle experiments. In 125 utilizing this approach, a specific fragment (usually the fastest-decaying ions in the 126 spectrum) is often chosen as a tracer for the particle phase compound of interest. For 127 example, m/z 297 has been selected as a tracer for bis(2-ethylhexyl) sebacate (BES) 128 (George et al., 2007), m/z 71 for hexacosane (Lambe et al., 2007), m/z 113 for 129 squalane (Smith et al., 2009), m/z 104 and 144 for erythritol and levoglucosan 130 (Kessler et al., 2010), and m/z 152, 68 and 98 for 1,2,3,4-butanetetracarboxylic acid, 131

132 citric acid and tartaric acid (Kessler et al., 2012) respectively.

However, the use of EI in conjunction with a particle vaporizer in the AMS 133 results in heavy fragmentation for organic compounds due to the high energy 134 associated with the EI source (70 eV) and the high temperature (~873 K) of the 135 vaporizer (Jayne et al., 2000; Allan et al., 2003). Under such conditions, the tracer m/z 136 137 fragment is prone to interferences due to (1) the fragmentation of larger ions and/or molecules and (2) fragments from particle phase oxidation products. Both can 138 contribute to the tracer m/z signal, sometimes leading to an insensitive or nonlinear 139 140 response of the tracer m/z to the concentration of the target reactant during oxidation. The same may also be true for the m/z for the molecular ion should one exist. In 141 particular, it is true if the structure of the product is highly similar to the reactant and 142 143 when the tracer is measured with a unit-mass resolution (UMR) aerosol mass spectrometer. Although it is often assumed that the chosen tracer ion does not 144 contribute significantly to the mass spectra of any possible oxidation products or vice 145 versa (Kessler et al., 2010), this is not always the case. In our previous work, we 146 observed that the magnitude of the second order heterogeneous rate constant (k_2) 147 increases as a function of increasing m/z of the fragment chosen as a tracer of the 148 parent molecule (Liu et al., 2014). The same trend has also been observed for the OH 149 oxidation of ambient biogenic secondary organic aerosol (SOA) (Slowik et al., 2012). 150 This suggests an interference from the fragments selected, and points to the necessity 151 to separate the signals of the compound of interest, from other compounds (products 152 and/or fragment) for kinetic studies. 153

In the current study, we improve the mixed-phase relative rate technique used for 154 studies of the heterogeneous oxidation of organic aerosol (OA) using positive matrix 155 factorization (PMF) analysis of UMR-AMS derived kinetic data. Heterogeneous 156 kinetics of citric acid (CA) toward OH oxidation was studied in a photo-chemical 157 flow tube coupled to an Aerodyne C-ToF-AMS and an Ionicon Analytik High 158 159 Resolution Proton Transfer Reaction Mass Spectrometer (PTR-ToF-MS). As it was applied to heterogeneous oxidation of ambient biogenic SOA (Slowik et al., 2012), 160 PMF analysis was used to successfully deconvolve the full mass spectra of the 161 162 reactant from the potential oxidation products, hence allowing proper accounting of the time evolution of reactant concentrations during photochemical oxidation. 163

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2. EXPERIMENTAL DETAILS

165 2.1 Flow tube experiments. A detailed schematic representation of the experimental system utilized in this study has been described elsewhere (Liu et al., 2014). Briefly, 166 organic particles (citric acid) were generated via atomization (model 3706, TSI), dried 167 through a diffusion drier and size-selected with a differential mobility analyzer (DMA) 168 (model 3081, TSI). The dried, monodispersed CA particles were introduced into the 169 170 flow tube reactor and exposed to differing OH concentrations. OH radicals were produced by the photolysis of O_3 at 254 nm in the presence of water vapor. O_3 was 171 generated by passing zero air through an O₃ generator (OG-1, PCI Ozone Corp.). The 172 O₃ concentration in the reactor was measured using an O₃ monitor (model 205, 2B 173 Technologies) and ranged from 0-1000 ppbv. Relative humidity (RH) in the reactor 174 was held constant (30 ± 3) % by varying the ratio of wet to dry air used as an air source, 175

and was measured at the exit of the flow tube reactor. The temperature was held 176 constant at 298 K by circulating a temperature controlled fluid through the outer 177 jacket of the reactor. The residence time in the flow reactor was 52 s. The steady-state 178 OH exposures were varied from 0 to $\sim 7.0 \times 10^{11}$ molecules cm⁻³ s which was estimated 179 on the basis of the decay of methanol from (as a reference compound) its reaction 180 181 with OH. The decay of methanol from its reaction with OH was measured using the PTR-ToF-MS. The k_2 of methanol, 9.4×10^{-13} cm³ molecule⁻¹ s⁻¹, was used for the OH 182 exposure calculation (Atkinson and Arey, 2003). 183

184 OH radical reactions were performed in a custom-made reactor consisting of two electro-polished stainless steel cylinders with inner diameter of 7.3 cm. The first stage 185 contained static mixing elements (StaMixCo) to ensure that particles and gas phase 186 187 species were well mixed prior to entering the reaction region (second stage). Fluid dynamics simulations of the flow tube confirmed that particles and gas phase species 188 were well mixed in the reactor, with a uniform initial velocity profile. The size and 189 composition of the particles exiting the reactor were measured by a scanning mobility 190 191 particle sizer (SMPS, TSI) and an Aerodyne C-ToF-AMS (Drewnick et al., 2005)

Control experiments demonstrated that O₃ or 254 nm light exposure did not lead
to the decomposition of CA. Analytic grade CA (EM, Germany) was used as received.

- 194 18.2 M Ω water was used as solvent.
- 195 **2.2 PMF analysis and kinetics calculation**.

196 PMF is a multivariate factor analysis tool that decomposes a matrix of speciated197 sample data into two matrices, namely, factor contributions and factor profiles

198 (Paatero and Tapper, 1994), such that

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$$x_{ij} = \sum_p g_{ip} f_{pj} + e_{ij}$$
 (5)

Where *i* and *j* refer to row and column indices in the matrix, respectively, *p* is the number of factors in the solution, x_{ij} is an element of the $m \times n$ matrix *X* of measured data elements to be fit, and e_{ij} is the residual. Results are constrained so that no sample can have a negative source contribution. The PMF solution minimizes the object function *Q* (Eq.6), based upon the uncertainties (*u*) (Norris and Vedantham, 2008).

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$$Q = \sum_{i=1}^{n} \sum_{j=1}^{m} \left(\frac{e_{ij}}{u_{ij}}\right)^2$$
(6)

Its ability to separate the signals of a multi-component matrix has been well 207 established. PMF analysis has been widely used for source apportionment of ambient 208 209 particles in field measurements (Song et al., 2006; Yuan et al., 2006; Viana et al., 2008;Ulbrich et al., 2009;Liggio et al., 2010;Schwartz et al., 2010). Three secondary 210 organic aerosol factors (SOA1, SOA2, SOA3) have been identified for OH initiated 211 oxidation of laboratory SOA (George and Abbatt, 2010). Similarly, SOA factors have 212 also been successfully isolated in OH oxidation of ambient biogenic SOA (Slowik et 213 214 al., 2012). Therefore, the use of PMF for separating the reactants from the products in laboratory studies aimed at using the relative rates method for heterogeneous kinetic 215 studies would seem to be a reasonable approach. 216

The AMS data for CA oxidation from all experiments combined were used as input into the PMF Evaluation Toolkit (PET) v2.05 (Paatero, 1997;Paatero and Tapper, 1994;Ulbrich et al., 2009) to separate the signals of CA and the corresponding

220 oxidation products. In the AMS data, the *m* rows of *X* are ensemble average mass 221 spectra (MS) of typically tens of thousands of particles measured over each averaging 222 period (typically 2 min) and the *n* columns of *X* are the time series (TS) of each m/z223 sampled.

224 PMF analyses were done in the robust mode. The default convergence criteria were not modified. The Q values as a function of FPEAK from -1 to +1 were 225 examined (Reff et al., 2007). For the variables with signal-to-noise ratio (SNR) less 226 than 0.2 ("bad" variables) and downweight variables with SNR between 0.2 and 2 227 228 ("weak" variables), their error estimates were increased by a factor of 10 and 3, respectively, as recommended by Paatero and Hopke (Paatero and Hopke, 2003). In 229 this study, the SNR of all m/z fragments are larger than 0.2. The error values for m/z230 231 44, 18, 17 and 16 were multiplied by sqrt(4).

The extracted factor profiles (mass spectra for CA and the oxidation products) 232 were compared with the NIST mass spectrum of pure CA and that measured with the 233 C-ToF-AMS directly via atomization. The temporal concentration profiles (factor 234 contributions) of CA were further confirmed via comparison to the known 235 experimental conditions used for kinetics calculations (ie: zero OH exposure should 236 result in a CA factor contribution of 100 %). For comparison with the PMF results, 237 the kinetic rate constants (k_r) were also calculated using specific individual tracers of 238 CA at m/z 87, 129 and 147, separately. The k_r of CA toward methanol was calculated 239 according to Eq. (4). The k_2 of CA was further calculated with the known k_2 of 240 methanol and $k_{\rm r}$. 241

The reactive uptake coefficient of OH (γ_{OH}) with CA was calculated using the following formulation (Kessler et al., 2010;Worsnop et al., 2002;Kessler et al., 2012;Liu et al., 2012):

Where D_p is the surface-weight average particle diameter of unreacted particles (cm), ρ_{CA} is the density of CA (g cm⁻³), N_A is Avogadro's number, v_{OH} is the average speed of OH radicals in the gas phase (cm s⁻¹), M_{CA} is the molecular weight of CA (g mol⁻¹), φ is a correction factor for diffusion of OH from the gas phase to particle phase.

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251 **3.0 Results**

252 **3.1 PMF analysis of AMS data.**

To ensure that oxidation of CA in particles does not result in a PTR-ToF-MS response for methanol in the gas phase (thus compromising the OH radical reference measurement), the oxidation of pure CA was performed in the absence of methanol, with no gas phase methanol signal detected by the PTR-ToF-MS. The mass concentration of the OA measured with the AMS during oxidation is shown in Figure 1A, which was constant. The results of Figure 1A demonstrate that the aerosol source is adequately stable for kinetic studies to be performed.

A two factor solution from the PMF analysis accounts for 99.98 % of the variance of the data. When the number of factors is greater than 2, none of the obtained factors resembles that of pure CA, whose contribution should be approximately 100 % when OH is absent in the reactor. Figures 1B and C represent

the temporal variations of the typical 2-factor PMF solution of AMS data when CA is exposed to varying OH concentrations. The error bars indicate the rotational uncertainty in the PMF analysis. Three independent experiments were performed to test the response of CA signal to OH exposure (determined by O_3 concentration). In the first and the third experiments, OH exposure was stepped downwards (high to low OH) by changing the power of O_3 -generator with the same flow rate and RH, while the inverse sequence was performed in the second experiment.

As demonstrated in Figure 1B and C, in the absence of OH radical (labeled"0"), 271 factor 1 (Figure 1B) accounts for (94.7±0.9) % of the OA mass, while factor 2 (Figure 272 1C) contributes (6.2 ± 0.7) % of OA. This is consistent with the experimental 273 conditions of zero OH radical (ie: no oxidation), and suggests that factor 1 should be 274 275 assigned to the citric acid reactant. Impurities in the CA or the water used to atomize CA likely contributed to factor 2. When OH exposure was decreased in a step-wise 276 manner in the first and the third experiment (Figure 1B), the extracted factor 277 representative of CA (factor 1) increased synchronously, and is accompanied with a 278 decrease in factor 2. Therefore, factor 2 is interpreted as the OH oxidation products of 279 CA. This is consistent with the second experiment, where the inverse trend was 280 observed with a step-wise OH exposure increase. Based upon this evidence, we 281 conclude that changes in the time series of factors 1 and 2 extracted by PMF are 282 consistent with the expected response to OH exposures, namely, that higher OH 283 exposure resulted in a decrease in CA (factor 1) and an increase in the oxidation 284 products (factor 2). 285

286	The factor profiles (ie: mass spectra) extracted by PMF analysis are shown in
287	Figure 2. The main fragments of CA including m/z values 129 $(C_5H_5O_4^+)$ and 87
288	$(C_3H_3O_3^+)$ are present in factor 1 (Figure 2A). These fragments are in good agreement
289	with the NIST mass spectra of pure CA and the mass spectrum of pure CA particles
290	measured with the C-ToF-AMS (Figure 3). Figure 4 further compared the normalized
291	mass spectra of factor 1 and pure CA directly measured with the C-ToF-AMS. The
292	relative intensities for all ions of pure CA are linearly correlated with that of factor 1
293	with a slope of 0.985 and R of 0.9999. This further confirmed that factor 1 should be
294	assigned to unreacted CA. Figure 2C shows the difference mass spectra (factor 2 -
295	factor 1). Consumption of m/z values 147 ($C_5H_7O_5^+$), 129, 87, 85 ($C_4H_5O_2^+$) and 60
296	$(C_2H_4O_2^+)$ can be observed, which is consistent with the assignment that factor 2
297	belongs to oxidation products of CA. However, small changes in the relative
298	intensities of these peaks suggest that the structure of the oxidation products of CA are
299	likely similar to that of CA. For example, as shown in Figure 2A and B, the intensity
300	of m/z 129 and 87 in factor 2 are 0.0125 ± 0.0046 and 0.0218 ± 0.0013 compared to
301	0.0141±0.0046 and 0.0235±0.0013 in factor 1.

The changes of the relative concentrations of gas phase methanol and particle phase CA are shown in Figure 5. The signal of CA extracted by PMF analysis also responded to OH exposure as expected, when methanol was present in the gas phase, which is similar to that of Figure 1. The relative intensities of the typical tracers of CA at m/z 87, 129 and 147 are shown in Figure 5C. As shown in Figure 5 B and C, the drop in the PMF product factor is substantially greater than that of any of the

individual ions. In addition, the consumption of the smaller tracer (m/z 87) is 308 substantially lower than that of the larger ones (m/z values 129 and 147). For example, 309 the maximum consumption of CA extracted with PMF analysis is approximately 80 %, 310 in comparison to ~ 30 %, ~ 10 % and 5 % for m/z values 147, 129 and 87, respectively. 311 312 These results support the small differences in the mass spectra between the unreacted 313 CA and its oxidation products as shown in Figure 2. Furthermore, it suggests that the measured loss of these fragments, which were supposedly only derived from CA, had 314 in fact contributions from the fragmentation of the products of CA oxidation. This 315 316 ultimately would lead to an underestimation of the second order heterogeneous rate constant (or OH uptake coefficients) if these fragments were chosen as the proxies for 317 the particle phase concentration of CA. In particular, the difference between the 318 319 PMF-factor decay rate and the marker-ion decay rate is mathematically possible only when the two factors (reactants and products) are extremely similar. 320

3.2 Reaction kinetics. The saturation vapor pressure of CA at 298K is 1.6×10^{-7} Pa 321 (Huisman et al., 2013), thus 99.9% of CA should be present in the particle phase 322 under the current experimental conditions according to a partition model (Kroll and 323 Seinfeld, 2008; Pankow, 1994). Although new particle formation was observed with a 324 CPC in the experiments (at the exit of the reactor), it has no influence on the measured 325 mass concentration of OA due to the small particle size of the new particles. This is 326 well supported by the constant mass concentration of OA measured with the AMS 327 during oxidation experiments (Figure 1A). In addition, as pointed out in our previous 328 work (Liu et al., 2014), evaporation of CA from particles could potentially contribute 329

to the decreases in particle phase CA concentration observed as a function of OH exposure. If CA evaporation was at play, the derived reaction rates will be overestimated using either the present approach or the simpler methods of using single fragments. The evaporation of CA from the particle phase under these experimental conditions from control experiments is less than 0.005 % based upon an evaporation model (Jacobson, 2005). This implies that the observed changes in CA concentration in the particle phase were due to the particle phase reaction.

The relative rates (relative to initial conditions) for CA and methanol in these 337 experiments are shown in Figure 6. The logarithmic c/c_0 of CA both measured with 338 339 the tracers and extracted with PMF analysis linearly correlated to that of methanol with $R^2 > 0.95$. The derived relative rate constant based upon PMF analysis is 340 3.01±0.27, while it is 0.72±0.05 and 0.22±0.01 for m/z values 147 and 129, 341 respectively. Applying the k_2 value of methanol towards OH of 9.4×10^{-13} cm³ 342 molecule⁻¹ s⁻¹ at 298 K (Atkinson and Arey, 2003), the k_2 of CA is calculated as 343 $(2.83\pm0.25)\times10^{-12}$ using the PMF approach, or $(6.77\pm0.47)\times10^{-13}$ using the single 344 tracer at m/z 147 and $(2.02\pm0.01)\times10^{-13}$ cm³ molecule⁻¹ s⁻¹ using the single tracer at 345 m/z 129, respectively. The reaction between methanol and OH radicals occurs in the 346 gas phase, while for the CA oxidation it occurs in particle phase. Thus it is necessary 347 to correct for OH diffusion from the bulk gas phase to the particle phase. Applying a 348 diffusion correction utilizing a previously developed empirical formula (Fuchs and 349 1970;Worsnop et al., 2002;Widmann and 350 Sutugin, Davis, 1997), the diffusion-corrected k_2 is $(3.31\pm0.29)\times10^{-12}$ using the PMF approach, 351 and

 $(7.92\pm0.55)\times10^{-13}$ and $(2.36\pm0.01)\times10^{-13}$ cm³ molecule⁻¹ s⁻¹ using single tracers at m/z 352 147 and 129, respectively. The diffusion-corrected γ_{OH} is calculated as 2.74±0.24 353 using the PMF approach, and 0.66 ± 0.05 and 0.20 ± 0.01 using single tracers at m/z 147 354 and 129, respectively. The γ_{OH} for a number of different organic particles have 355 previously been measured, and are in the range of 0.3 - 2.0 (Kessler et al., 356 357 2010;George et al., 2007;Hearn and Smith, 2006;Lambe et al., 2007;Smith et al., 2009;Kessler et al., 2012). As pointed out by Hearn and Smith (2006), the large γ 358 implies that secondary radical reactions within the particles could play a significant 359 360 role in heterogeneous chemistry, particularly since gaseous citric acid in these studies is insignificant. 361

It should be pointed out that oxidant diffusion in the particle phase should lead to 362 363 a concentration gradient of oxidant and a negative impact on reaction kinetics (Donahue et al., 2005). However, as shown in Figure 6, this effect is negligible under 364 the current experimental conditions. Based upon the measured c/c0 and the initial 365 366 diameter of the CA particles, the maximum OH diffusion depth is approximately 25 nm. Given the residence time (τ) in this study (52 s), a significant OH concentration 367 gradient will exist in particle phase if the D_{OH} in CA particles is smaller than 1.2×10^{-17} 368 m² s⁻¹ ($D=l^2/\tau$) (Donahue et al., 2005). At the present time, the D_{OH} in CA particles is 369 unavailable. However, Price et al. (Price et al., 2014) have reported the diffusion of 370 D_2O in several organics (sucrose and levoglucosan) to be larger than $\sim 1 \times 10^{-16}$ m² s⁻¹ 371 even under dry condition. This implies that a gradient in OH concentration in the CA 372 particles is negligible under the current conditions. 373

374 **4. Discussion**

Kessler et al. (Kessler et al., 2012) have reported the k_2 of CA toward OH to be 375 $(4.3\pm0.8)\times10^{-13}$ cm³ molecule s⁻¹ at 308 K and 30 % RH with an Aerodyne HR-AMS. 376 In their work, the diameter of particles and RH were equivalent to the current work, 377 while their experimental temperature was 10 K higher. In addition, a m/z fragment of 378 379 68 was used as a tracer for CA in their work to derive the heterogeneous rate constant. 380 Conversely, no significant consumption of m/z 68 was observed in the current study. The lack of a m/z 68 fragment consumption here may be explained by the choice of 381 reaction conditions. In the work of Kessler et al., OH concentration exposure 382 $(0 \sim 7 \times 10^{12} \text{ molecule cm}^{-3} \text{ s})$ was approximately an order of magnitude higher than that 383 reported here. Recent evidence suggests that the product distribution during OA 384 385 oxidation greatly depends upon OH exposure levels (Wilson et al., 2012). Hence, it is possible that more oxidized products formed via multi-generational chemistry at high 386 OH were formed, which may have less of an influence on the signal of the chosen 387 tracer (m/z 68), and result in product AMS spectra which are significantly different 388 than that of the reactant thus mitigating the use of PMF (which was not the case here). 389 In studies of the OH oxidation of squalane (Sq) (Smith et al., 2009; Wilson et al., 390 2012), the first generation product (SqO) was the primary contributor to the products 391 when the OH exposure was the same as the highest OH level in the current study 392 $(7.0 \times 10^{11} \text{ molecules cm}^{-3} \text{ s})$, while higher generation products were predominant at 393 OH exposures was greater than $\sim 2 \times 10^{12}$ molecules cm⁻³ s. Although not directly 394 comparable, it is reasonable to assume that lower OH exposure in the current work 395

should lead primarily to the first generation products, which are highly similar to CA. 396 However, the formation of multi-generation products cannot be completely ruled out. 397 Secondly, the difference in OA and oxidant concentrations as well as timescale may 398 also have an influence on the product distribution. Thirdly, a high resolution 399 time-of-flight aerosol mass spectrometer (HR-ToF-AMS) was used in their work, 400 401 while a C-ToF-AMS with unit-mass resolution was used in this study. The higher mass resolution of the HR-ToF-AMS relative to a C-ToF-AMS, may further reduce 402 the influence of product fragments on m/z 68 (or others). Finally, differences in 403 temperature or other reaction conditions between experiments may also have led to 404 differences in the morphology of CA and subsequent differences in the reactivity of 405 CA. 406

407 Given the above discrepancy in the consumption of m/z 68, the fragments at m/z129 and 147 were used as tracers in this work. The measured k_2 of CA utilizing m/z 408 129 and 147 in this study is of the same order of magnitude as that reported in Kessler 409 et al. (2012). However, as shown in Figure 3C, the consumption of m/z 87 is much 410 lower than that of m/z 129. The apparent k_2 of CA based on m/z 87 is $(9.9\pm0.8)\times10^{-14}$ 411 cm³ molecule⁻¹ s⁻¹, and the diffusion-corrected k_2 is $(1.16\pm0.09)\times10^{-13}$ cm³ molecule⁻¹ 412 s^{-1} . This suggests that the derived rate constant greatly depends upon the size of the 413 tracer fragment, with larger fragments resulting in larger values of k_2 in this study. 414 This is consistent with previous work investigating the OH oxidation of tris-phenyl 415 phosphate (TPhP) (Liu et al., 2014) and ambient biogenic SOA (Slowik et al., 2012). 416 The k_2 of CA based upon PMF analysis is approximately an order of magnitude larger 417

than the Kessler result measured with the tracer at m/z 68, and 4.2 times greater than that calculated based upon m/z 147 in this study. The differences in product distributions that may arise between this and the work of Kessler et al., consistent with the fact that m/z 68 is not consumed in the current study, suggests that the PMF approach was likely required in this work to separate similar product and reactant spectra ultimately caused by lower OH exposure.

A number of factors may be responsible for the discrepancy between derived rate 424 constants. It has previously been observed that the presence of O₃ can inhibit the rate 425 426 of OH reaction, perhaps by reacting with OH radicals or by O₃ or intermediate species blocking surface active sites (Renbaum and Smith, 2011). A Langmuir-Hinshelwood 427 mechanism has been observed for the reaction of O₃ on organic surfaces (Pöschl, 428 429 2005). It has also been demonstrated that a higher concentration of gas phase reactant often leads to a lower uptake coefficient due to surface saturation (Ma et al., 2010 ;Li 430 et al., 2002). Differences in k_2 may also arise from the competition between reaction 431 products and reactants for available OH, or via the blocking or coating of the reactant 432 by products which would require liquid phase diffusion of OH to degrade the original 433 434 CA. In experiments with higher OH exposures (Kessler et al 2012) it is possible that significantly more product mass is mixed and/or coated onto the original particle thus 435 decreasing the perceived k_2 . Different timescales and concentrations of reactants 436 might also lead to different rate constants (Che et al., 2009). Finally, as pointed out 437 above, the differing reaction conditions may have led to a different CA morphology 438 and subsequent differences in the reactivity towards OH. The significant difference 439

between the reported rate constants highlights an important issue in heterogeneous
reactions of the atmosphere, and in the experiments trying to derive such kinetics. It
implies that the particle composition and/or morphology as determined by the reaction
conditions in the laboratory or the ambient atmosphere will have a large effect on the
OH kinetics.

445 Citric acid is a hydroxyl substituted poly carboxyl acid. Scheme 1 summarizes its possible fragmentation pathways. The typical mass peaks including m/z 147, 129, 87, 446 85 and 68 would result from this scheme and were indeed observed. The fragments at 447 m/z 129, 87, 85 and 68 are also likely from CA oxidation products fragments, and 448 449 hence their signal intensities may be highly influenced by products and/or larger fragments, in particular, when the oxidized products are highly similar to the reactant. 450 451 In some instances, oxidation products can exhibit similar fragmentation pathways as the reactants. This is likely the case for the smaller fragments of CA. For example, 452 scheme 2 illustrates the possible fragmentation of 453 pathways 2,3-dihydroxypropane-1,2,3-tricarboxylic acid, which is one of the possible products 454 455 from the OH oxidation of citric acid in terms of the general chemistry described by Atkinson et al. (Atkinson, 1986). As observed in Scheme 2, there are several pathways 456 leading to the fragment at m/z 87, implying that the decrease in the signal of m/z 87 457 due to CA oxidation is likely to be compensated by fragments from the oxidation 458 products. In addition, it is also possible to form fragments with the same m/z as the 459 parent citric acid if the dehydration reaction (the 6th path in Scheme 2) takes place 460 initially. Other possible reaction products might also play similar roles in the 461

462 fragments. This is highly possible when the product distribution contains products463 which are structurally similar to the reactant under low oxidant exposure conditions.



Scheme 1. Possible fragmentation pathways for citric acid.



468

469 Scheme 2. Possible fragmentation pathways for an oxidation product of citric acid in
470 terms of the general chemistry described by Atkinson et al. (Atkinson, 1986).

The current relative rate method based upon PMF analysis was used to re-analyze the heterogeneous oxidation kinetics of three organophosphate flame retardants found in ambient particles and reported previously (Liu et al., 2014). The k_2 values for TPhP, tris-1,3-dichloro-2-propyl phosphate (TDCPP) and tris-2-ethylhexyl phosphate (TEHP) utilizing the tracer and PMF approaches are summarized in Table 1. For TPhP, its molecular ion peak (M⁺;326) was chosen as a tracer; while the largest detectable fragments, i.e. m/z 381 and 323, were chosen for TDCPP (M⁺; 431) and TEHP (M⁺;

479 435), respectively. The typical evolution of the PMF factors of TPhP, TDCPP, and TEHP are shown in Figures S1-3. For TPhP, the measured k_2 values derived by both 480 methods are comparable within the experimental uncertainties, while k_2 of TDCPP 481 and TEHP based upon PMF analysis is 1.5 and 1.6 times larger than that using the 482 483 chosen tracers. The good agreement between methods for TPhP is likely due to the 484 fact that the molecular ion peak (M^+) is measurable for TPhP with the AMS, while it is not observable for TDCPP, TEHP and CA. Therefore, the influence of secondary 485 fragmentation from larger fragments has little influence on the signal of M⁺ for TPhP. 486 487 These results also demonstrate that a substantial underestimation of rate constants could result when a non-molecular ion tracer is used to monitor the particle phase 488 concentration of organic matter with UMR-AMS for heterogeneous kinetic studies. 489 490 The discrepancy between the tracer and PMF based methods for other compounds will depend upon a number of factors including: structure of products, OH exposure 491 level, particle morphology, and organic species competing OH reactions. 492

493

494 **5.0 Implications and Conclusions**

The measured k_2 for citric acid toward OH is $(3.31\pm0.29)\times10^{-12}$ cm³ molecule⁻¹ s⁻¹ at 298 K and 30 % RH. This value is at least 4.2 times greater than that calculated on the basis of atypical tracer m/z 147. Although the tracer and PMF approaches can at times agree (Kroll, 2014) and the tracer and molecular-ion approaches can sometimes agree as well (Smith et al., 2009), our results suggest that the heterogeneous kinetics of OA is underestimated when a non-molecular ion peak is 501 used as the tracer to measure the particle phase concentration of OA based on UMR-AMS. In model simulations, the reactive uptake coefficient of OH or other 502 503 radicals, which are calculated based upon k_2 , is an important parameter in evaluating the fate of OA during transport. The current results suggest that the lifetime of OA 504 505 estimated in models due to heterogeneous oxidation might be overestimated for a 506 reaction system where the products are highly similar to the reactant and the kinetic 507 data are derived by individual non-molecular m/z tracers of OA. The results also suggest that it may be necessary to revisit the kinetic data of other organic aerosol 508 509 components (and OH uptake coefficients) which have been derived using the relative 510 rates technique (George et al., 2007; Lambe et al., 2007) based on UMR-AMS. Finally, these results imply that the heterogeneous oxidation of aerosols will be dependent 511 512 upon a number of factors related to the reaction system, and that a single rate constant 513 for one system cannot be universally applied under all conditions. Future work is thus required to elucidate the chemical and physical parameters which control the OH 514 heterogeneous reaction kinetics and the associated need to apply PMF for a variety of 515 516 chemical systems. This may be best accomplished through systematic application of 517 the PMF approach to species with differing mass spectral characteristics, such as linear/branched alkanes, monocarboxylic acids and other oxygenates. As illustrated in 518 this study, the kinetics derived with PMF may differ from that derived with tracer ions, 519 with both based upon EI-AMS approaches. This highlights the usefulness of 520 measurements from CIMS, GC-MS and VUV-AMS, for the determination of 521 heterogeneous loss rates, since these instruments are more likely to retain the reactant 522

523 molecular information.

524

525 Supporting Information

- 526 Supplementary material related to this article is available online at:
- 527

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Table 1. Comparison of the measured k_2 values utilizing PMF and select m/z tracers,

	OA	Mean	$k_2(10^{12})$	$k_2(10^{12}) \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$		k _{2 PMF} /	
		$k_{r_{PMF}}$	$k_{2, \text{ obs}_PMF}$	$k_{2, t _PMF}$	k _{2, t_Tracer}	k_{2_Tracer}	M _{Tracer} /M
	TPhP	1.58±0.33	1.48±0.31	1.95±0.43	2.10±0.19 ^a	0.9	326/326
	TDCPP	1.20 ± 0.31	1.13±0.29	1.35±0.35	$0.92{\pm}0.09^{a}$	1.5	381/431
	TEHP	3.52 ± 0.65	3.31±0.61	4.25±0.78	2.70 ± 0.63^{a}	1.6	323/435
	CA	3.01±0.27	2.83±0.25	3.31±0.29	0.79 ± 0.06	4.2	147/192
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for organophosphate compounds and CA.

709 Figure captions

Figure 1. Changes in (A) total organic mass concentration, (B) the fraction of 710 711 unreacted citric acid derived by PMF and (C) products of citric acid oxidized by OH derived by PMF, as a function of relative experimental time. The values 1 - 6712 represent a step-wise O₃ concentration decrease, corresponding to decreased OH 713 exposure; 0 represents an O_3 concentration of zero. Experimental conditions are D_m : 714 200 nm, RH: 30±3 %, T: 298 K. 715 Figure 2. Normalized mass spectra of (A) citric acid (PMF factor 1), (B) citric acid 716 oxidation products (PMF factor 2), and (C) the difference mass spectrum (Factor 2 -717 718 Factor 1). The numbers in the upper two rows are the intensities of m/z 87 and 129,

- while negative values are shown in the bottom row. The red and green lines indicate anegative and positive value, respectively.
- Figure 3. Mass spectra (A) of CA from NIST database, (B) of pure CA measured withthe C-ToF-AMS.
- Figure 4. Comparison between the mass spectra of factor 1 from PMF analysis and pure CA directly measured by the C-ToF-AMS. The inset graph is the correlation of their corresponding signal intensities.
- Figure 5. Changes in the relative concentration of (A) methanol, (B) citric acid
- extracted with PMF analysis and (C) specific tracers measured with the AMS during
- the OH initiated oxidation of citric acid. Experimental conditions are $D_{\rm m}$: 140 nm, RH:
- $30 \pm 3\%$, T: 298 K. The values in the top row represent the OH exposures.
- Figure 6. Relative concentration of citric acid (c/c_0) as a function of the relative
- concentration of methanol based upon (A) PMF analysis, (B) m/z=129 and (C) m/z

732	147. Experimental conditions are $D_{\rm m}$: 140 nm, RH: 30±3 %, T: 298 K.
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Figure 1.







Figure 2.





Figure 4.



Figure 5.



Figure 6.