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**Application of positive matrix factor analysis in heterogeneous kinetics studies utilizing the mixed-phase relative rates technique**

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22 **Abstract:**

23 The mixed-phase relative rate approach for determining aerosol particle organic  
24 heterogeneous reaction kinetics is often performed utilizing mass spectral tracers as a  
25 proxy for particle phase reactant concentration. However, sometimes this approach  
26 may be influenced by signal contamination from oxidation products during the  
27 experiment. In the current study, the mixed-phase relative rates technique has been  
28 improved by combining a Positive Matrix Factor (PMF) analysis with electron  
29 ionization Aerosol Mass Spectrometry (unit mass resolution), thereby removing the  
30 influence of m/z fragments from reaction products on the reactant signals. To  
31 demonstrate the advantages of this approach, the heterogeneous reaction between OH  
32 radicals and citric acid (CA) was investigated using a photochemical flow tube  
33 coupled to a compact time-of-flight aerosol mass spectrometer (C-ToF-AMS). The  
34 measured heterogeneous rate constant ( $k_2$ ) of citric acid toward OH was  
35  $(3.31 \pm 0.29) \times 10^{-12} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$  at 298 K and (30 $\pm$ 3) % RH and was several  
36 times greater than the results utilizing individual m/z fragments. This phenomenon  
37 was further evaluated for particulate-phase organophosphates (TPhP, TDCPP, and  
38 TEHP), leading to  $k_2$  values significantly larger than previously reported. The results  
39 suggest that heterogeneous kinetics can be significantly underestimated when the  
40 structure of the products is highly similar to the reactant and when a non-molecular  
41 tracer is measured with a unit mass resolution aerosol mass spectrometer. The results  
42 also suggest that the heterogeneous lifetime of organic aerosol in models can be  
43 overestimated due to underestimated OH uptake coefficients. Finally, a comparison of

44 reported rate constants implies that the heterogeneous oxidation of aerosols will be  
45 dependent upon a number of factors related to the reaction system, and that a single  
46 rate constant for one system cannot be universally applied under all conditions.

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## 66 **1. Introduction**

67       Reaction kinetics data provide key parameters for both air quality and climate  
68 models. They are required to compute the trace gas and particle matter (PM) content  
69 of the atmosphere (Kolb et al., 2010) and to evaluate the atmospheric lifetime and fate  
70 for individual species. Organic particles make up 10-90 % of the global submicron  
71 particle mass in the lower troposphere (Zhang et al., 2011), and is comprised of  
72 various reactive organic species, which are subject to atmospheric heterogeneous  
73 oxidation. Previous studies have found that heterogeneous reactions with OH in  
74 particular, can lead to an increase in density, CCN activation (George and Abbatt,  
75 2010) and optical extinction (Cappa et al., 2011) of organic particulate matter.  
76 Therefore, there is a growing interest in understanding not only the mechanism of PM  
77 transformation through heterogeneous reactions including oxidation, but also  
78 determining the rates at which organic aerosols are chemically transformed in the  
79 atmosphere.

80       To this end, Donahue et al. (Donahue et al., 2005) and Hearn and Smith (Hearn  
81 and Smith, 2006) developed a mixed-phase relative rate technique for measuring  
82 organic PM component heterogeneous reaction kinetic rate constants. In this method,  
83 the rate constant of the compound of interest is determined from the decrease of its  
84 particle phase relative concentration as a function of oxidant exposure. The oxidant  
85 levels are simultaneously estimated via the measured loss of a gas phase reference  
86 compound after applying the known second-order rate constant ( $k_2$ ) toward the  
87 oxidant. In this approach the rates of chemical change are given by,

88  $-\frac{dc_A}{dt} = k_{2,A}c_Ac_{Ox}$  (1)

89  $-\frac{dc_R}{dt} = k_{2,R}c_Rc_{Ox}$  (2)

90 where  $c_A$ ,  $c_R$  and  $c_{Ox}$  are the particle phase concentration of the compound of interest  
 91 (A), the gas phase concentration of the reference compound (R) and oxidant  
 92 (molecules  $\text{cm}^{-3}$ ) respectively, while  $k_{2,A}$  and  $k_{2,R}$  are the second-order rate constant of  
 93 A and R to the oxidant ( $\text{cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$ ). A relative rate constant ( $k_r$ ) (ie: particle  
 94 phase reaction rate of A, relative to the gas phase rate of R) can be derived by dividing  
 95 Eq. (1) by Eq. (2). The derivation of  $k_r$  provides a means to obtain heterogeneous  
 96 kinetic data without the need to know the absolute concentration of the oxidant. The  
 97 differential and integral forms for the relative rates technique are shown as Eq. (3) and  
 98 (4),

99  $\frac{dc_A}{c_A} = \frac{k_{2,A}}{k_{2,R}} \frac{dc_R}{c_R} = k_r \frac{dc_R}{c_R}$  (3)

100  $\log \frac{c_A}{c_{A,0}} = k_r \log \frac{c_R}{c_{R,0}}$  (4)

101 from which the relative rate constant ( $k_r$ ), is the slope of the line derived by plotting  
 102 the logarithmic relative concentration of A against that of R (relative to initial  
 103 conditions;  $c_{A,0}$ ). The second-order heterogeneous rate constant of the compound of  
 104 interest ( $k_{2,A}$ ) towards the oxidant may then be calculated using the obtained  $k_r$  and the  
 105 known  $k_{2,R}$  (ie:  $k_{2,A} = k_r \times k_{2,R}$ ).

106 Using this method, a number of studies have quantified the uptake coefficients of  
 107  $\text{O}_3$ , OH, Cl, and  $\text{NO}_3$  on various organic particles, and the corresponding second order  
 108 rate constants for the degradation of organic compounds (Hearn and Smith,  
 109 2006; George et al., 2007; Lambe et al., 2007; McNeill et al., 2007; McNeill et al.,

110 2008;Smith et al., 2009;Kessler et al., 2010;Renbaum and Smith, 2011;Kessler et al.,  
111 2012;Liu et al., 2012;Sareen et al., 2013).

112 Although gas chromatograph mass spectrometry (GC-MS) has been widely used  
113 in the kinetics studies (Weitkamp et al., 2008a;Weitkamp et al., 2008b;Lambe et al.,  
114 2009;Isaacman et al., 2012), quantifying the particle phase loss of an organic  
115 compound in such studies often relies upon aerosol mass spectrometry techniques to  
116 monitor specific particle phase reactant ions of interest in semi-real time. Aerosol  
117 mass spectrometry instruments utilizing high resolution detection and soft ionization  
118 techniques, such as chemical ionization (Aerosol CIMS) (Hearn and Smith,  
119 2006;McNeill et al., 2007;McNeill et al., 2008;Renbaum and Smith, 2011;Sareen et  
120 al., 2013) and vacuum ultraviolet photo-ionization (VUV-ATOFMS)(Liu et al., 2012),  
121 have been utilized to measure the concentration of the target organic compounds in  
122 particles. However, Aerosol Time-of-Flight or Quadrupole Mass Spectrometry  
123 (ToF-AMS or Q-AMS) employing electronic ionization (EI; 70 eV) as an ion source  
124 remains the prevalent instrument used in such organic particle experiments. In  
125 utilizing this approach, a specific fragment (usually the fastest-decaying ions in the  
126 spectrum) is often chosen as a tracer for the particle phase compound of interest. For  
127 example,  $m/z$  297 has been selected as a tracer for bis(2-ethylhexyl) sebacate (BES)  
128 (George et al., 2007),  $m/z$  71 for hexacosane (Lambe et al., 2007),  $m/z$  113 for  
129 squalane (Smith et al., 2009),  $m/z$  104 and 144 for erythritol and levoglucosan  
130 (Kessler et al., 2010), and  $m/z$  152, 68 and 98 for 1,2,3,4-butanetetracarboxylic acid,  
131 citric acid and tartaric acid (Kessler et al., 2012) respectively.

132        However, the use of EI in conjunction with a particle vaporizer in the AMS  
133 results in heavy fragmentation for organic compounds due to the high energy  
134 associated with the EI source (70 eV) and the high temperature (~873 K) of the  
135 vaporizer (Jayne et al., 2000; Allan et al., 2003). Under such conditions, the tracer m/z  
136 fragment is prone to interferences due to (1) the fragmentation of larger ions and/or  
137 molecules and (2) fragments from particle phase oxidation products. Both can  
138 contribute to the tracer m/z signal, sometimes leading to an insensitive or nonlinear  
139 response of the tracer m/z to the concentration of the target reactant during oxidation.  
140 The same may also be true for the m/z for the molecular ion should one exist. In  
141 particular, it is true if the structure of the product is highly similar to the reactant and  
142 when the tracer is measured with a unit-mass resolution (UMR) aerosol mass  
143 spectrometer. Although it is often assumed that the chosen tracer ion does not  
144 contribute significantly to the mass spectra of any possible oxidation products or vice  
145 versa (Kessler et al., 2010), this is not always the case. In our previous work, we  
146 observed that the magnitude of the second order heterogeneous rate constant ( $k_2$ )  
147 increases as a function of increasing m/z of the fragment chosen as a tracer of the  
148 parent molecule (Liu et al., 2014). The same trend has also been observed for the OH  
149 oxidation of ambient biogenic secondary organic aerosol (SOA) (Slowik et al., 2012).  
150 This suggests an interference from the fragments selected, and points to the necessity  
151 to separate the signals of the compound of interest, from other compounds (products  
152 and/or fragment) for kinetic studies.

153        In the current study, we improve the mixed-phase relative rate technique used for

154 studies of the heterogeneous oxidation of organic aerosol (OA) using positive matrix  
155 factorization (PMF) analysis of UMR-AMS derived kinetic data. Heterogeneous  
156 kinetics of citric acid (CA) toward OH oxidation was studied in a photo-chemical  
157 flow tube coupled to an Aerodyne C-ToF-AMS and an Ionicon Analytik High  
158 Resolution Proton Transfer Reaction Mass Spectrometer (PTR-ToF-MS). As it was  
159 applied to heterogeneous oxidation of ambient biogenic SOA (Slowik et al., 2012),  
160 PMF analysis was used to successfully deconvolve the full mass spectra of the  
161 reactant from the potential oxidation products, hence allowing proper accounting of  
162 the time evolution of reactant concentrations during photochemical oxidation.

## 163 **2. EXPERIMENTAL DETAILS**

164 **2.1 Flow tube experiments.** A detailed schematic representation of the experimental  
165 system utilized in this study has been described elsewhere (Liu et al., 2014). Briefly,  
166 organic particles (citric acid) were generated via atomization (model 3706, TSI), dried  
167 through a diffusion drier and size-selected with a differential mobility analyzer (DMA)  
168 (model 3081, TSI). The dried, monodispersed CA particles were introduced into the  
169 flow tube reactor and exposed to differing OH concentrations. OH radicals were  
170 produced by the photolysis of O<sub>3</sub> at 254 nm in the presence of water vapor. O<sub>3</sub> was  
171 generated by passing zero air through an O<sub>3</sub> generator (OG-1, PCI Ozone Corp.). The  
172 O<sub>3</sub> concentration in the reactor was measured using an O<sub>3</sub> monitor (model 205, 2B  
173 Technologies) and ranged from 0-1000 ppbv. Relative humidity (RH) in the reactor  
174 was held constant (30±3) % by varying the ratio of wet to dry air used as an air source,  
175 and was measured at the exit of the flow tube reactor. The temperature was held



176 constant at 298 K by circulating a temperature controlled fluid through the outer  
177 jacket of the reactor. The residence time in the flow reactor was 52 s. The steady-state  
178 OH exposures were varied from 0 to  $\sim 7.0 \times 10^{11}$  molecules  $\text{cm}^{-3}$  s which was estimated  
179 on the basis of the decay of methanol from (as a reference compound) its reaction  
180 with OH. The decay of methanol from its reaction with OH was measured using the  
181 PTR-ToF-MS. The  $k_2$  of methanol,  $9.4 \times 10^{-13}$   $\text{cm}^3$  molecule $^{-1}$  s $^{-1}$ , was used for the OH  
182 exposure calculation (Atkinson and Arey, 2003).

183 OH radical reactions were performed in a custom-made reactor consisting of two  
184 electro-polished stainless steel cylinders with inner diameter of 7.3 cm. The first stage  
185 contained static mixing elements (StaMixCo) to ensure that particles and gas phase  
186 species were well mixed prior to entering the reaction region (second stage). Fluid  
187 dynamics simulations of the flow tube confirmed that particles and gas phase species  
188 were well mixed in the reactor, with a uniform initial velocity profile. The size and  
189 composition of the particles exiting the reactor were measured by a scanning mobility  
190 particle sizer (SMPS, TSI) and an Aerodyne C-ToF-AMS (Drewnick et al., 2005)

191 Control experiments demonstrated that O<sub>3</sub> or 254 nm light exposure did not lead  
192 to the decomposition of CA. Analytic grade CA (EM, Germany) was used as received.

193 18.2 MΩ water was used as solvent.

## 194 **2.2 PMF analysis and kinetics calculation.**

195 PMF is a multivariate factor analysis tool that decomposes a matrix of speciated  
196 sample data into two matrices, namely, factor contributions and factor profiles  
197 (Paatero and Tapper, 1994), such that

198  $x_{ij} = \sum_p g_{ip} f_{pj} + e_{ij}$  (5)

199 Where  $i$  and  $j$  refer to row and column indices in the matrix, respectively,  $p$  is the  
200 number of factors in the solution,  $x_{ij}$  is an element of the  $m \times n$  matrix  $X$  of measured  
201 data elements to be fit, and  $e_{ij}$  is the residual. Results are constrained so that no  
202 sample can have a negative source contribution. The PMF solution minimizes the  
203 object function  $Q$  (Eq.6), based upon the uncertainties ( $u$ ) (Norris and Vedantham,  
204 2008).

205  $Q = \sum_{i=1}^n \sum_{j=1}^m \left( \frac{e_{ij}}{u_{ij}} \right)^2$  (6)

206 Its ability to separate the signals of a multi-component matrix has been well  
207 established. PMF analysis has been widely used for source apportionment of ambient  
208 particles in field measurements (Song et al., 2006; Yuan et al., 2006; Viana et al.,  
209 2008; Ulbrich et al., 2009; Liggiio et al., 2010; Schwartz et al., 2010). Three secondary  
210 organic aerosol factors (SOA1, SOA2, SOA3) have been identified for OH initiated  
211 oxidation of laboratory SOA (George and Abbatt, 2010). Similarly, SOA factors have  
212 also been successfully isolated in OH oxidation of ambient biogenic SOA (Slowik et  
213 al., 2012). Therefore, the use of PMF for separating the reactants from the products in  
214 laboratory studies aimed at using the relative rates method for heterogeneous kinetic  
215 studies would seem to be a reasonable approach.

216 The AMS data for CA oxidation from all experiments combined were used as  
217 input into the PMF Evaluation Toolkit (PET) v2.05 (Paatero, 1997; Paatero and Tapper,  
218 1994; Ulbrich et al., 2009) to separate the signals of CA and the corresponding  
219 oxidation products. In the AMS data, the  $m$  rows of  $X$  are ensemble average mass

220 spectra (MS) of typically tens of thousands of particles measured over each averaging  
221 period (typically 2 min) and the  $n$  columns of  $X$  are the time series (TS) of each  $m/z$   
222 sampled.

223 PMF analyses were done in the robust mode. The default convergence criteria  
224 were not modified. The  $Q$  values as a function of FPEAK from -1 to +1 were  
225 examined (Reff et al., 2007). For the variables with signal-to-noise ratio (SNR) less  
226 than 0.2 (“bad” variables) and downweight variables with SNR between 0.2 and 2  
227 (“weak” variables), their error estimates were increased by a factor of 10 and 3,  
228 respectively, as recommended by Paatero and Hopke (Paatero and Hopke, 2003). In  
229 this study, the SNR of all  $m/z$  fragments are larger than 0.2. The error values for  $m/z$   
230 44, 18, 17 and 16 were multiplied by  $\sqrt{4}$ .

231 The extracted factor profiles (mass spectra for CA and the oxidation products)  
232 were compared with the NIST mass spectrum of pure CA and that measured with the  
233 C-ToF-AMS directly via atomization. The temporal concentration profiles (factor  
234 contributions) of CA were further confirmed via comparison to the known  
235 experimental conditions used for kinetics calculations (ie: zero OH exposure should  
236 result in a CA factor contribution of 100 %). For comparison with the PMF results,  
237 the kinetic rate constants ( $k_r$ ) were also calculated using specific individual tracers of  
238 CA at  $m/z$  87, 129 and 147, separately. The  $k_r$  of CA toward methanol was calculated  
239 according to Eq. (4). The  $k_2$  of CA was further calculated with the known  $k_2$  of  
240 methanol and  $k_r$ .

241 The reactive uptake coefficient of OH ( $\gamma_{OH}$ ) with CA was calculated using the

242 following formulation (Kessler et al., 2010; Worsnop et al., 2002; Kessler et al.,  
243 2012; Liu et al., 2012):

$$244 \quad \gamma_{\text{OH}} = \frac{2D_p \rho_{\text{CA}} N_A}{3v_{\text{OH}} M_{\text{CA}}} \varphi k_2 \quad \text{Eq (7)}$$

245 Where  $D_p$  is the surface-weight average particle diameter of unreacted particles (cm),  
246  $\rho_{\text{CA}}$  is the density of CA ( $\text{g cm}^{-3}$ ),  $N_A$  is Avogadro's number,  $v_{\text{OH}}$  is the average speed  
247 of OH radicals in the gas phase ( $\text{cm s}^{-1}$ ),  $M_{\text{CA}}$  is the molecular weight of CA ( $\text{g mol}^{-1}$ ),  
248  $\varphi$  is a correction factor for diffusion of OH from the gas phase to particle phase.

249

## 250 **3.0 Results**

### 251 **3.1 PMF analysis of AMS data.**

252 To ensure that oxidation of CA in particles does not result in a PTR-ToF-MS  
253 response for methanol in the gas phase (thus compromising the OH radical reference  
254 measurement), the oxidation of pure CA was performed in the absence of methanol,  
255 with no gas phase methanol signal detected by the PTR-ToF-MS. The mass  
256 concentration of the OA measured with the AMS during oxidation is shown in Figure  
257 1A, which was constant. The results of Figure 1A demonstrate that the aerosol source  
258 is adequately stable for kinetic studies to be performed.

259 A two factor solution from the PMF analysis accounts for 99.98 % of the  
260 variance of the data. When the number of factors is greater than 2, none of the  
261 obtained factors resembles that of pure CA, whose contribution should be  
262 approximately 100 % when OH is absent in the reactor. Figures 1B and C represent  
263 the temporal variations of the typical 2-factor PMF solution of AMS data when CA is

264 exposed to varying OH concentrations. The error bars indicate the rotational  
265 uncertainty in the PMF analysis. Three independent experiments were performed to  
266 test the response of CA signal to OH exposure (determined by O<sub>3</sub> concentration). In  
267 the first and the third experiments, OH exposure was stepped downwards (high to low  
268 OH) by changing the power of O<sub>3</sub>-generator with the same flow rate and RH, while  
269 the inverse sequence was performed in the second experiment.

270 As demonstrated in Figure 1B and C, in the absence of OH radical (labeled“0”),  
271 factor 1 (Figure 1B) accounts for (94.7±0.9) % of the OA mass, while factor 2 (Figure  
272 1C) contributes (6.2±0.7) % of OA. This is consistent with the experimental  
273 conditions of zero OH radical (ie: no oxidation), and suggests that factor 1 should be  
274 assigned to the citric acid reactant. Impurities in the CA or the water used to atomize  
275 CA likely contributed to factor 2. When OH exposure was decreased in a step-wise  
276 manner in the first and the third experiment (Figure 1B), the extracted factor  
277 representative of CA (factor 1) increased synchronously, and is accompanied with a  
278 decrease in factor 2. Therefore, factor 2 is interpreted as the OH oxidation products of  
279 CA. This is consistent with the second experiment, where the inverse trend was  
280 observed with a step-wise OH exposure increase. Based upon this evidence, we  
281 conclude that changes in the time series of factors 1 and 2 extracted by PMF are  
282 consistent with the expected response to OH exposures, namely, that higher OH  
283 exposure resulted in a decrease in CA (factor 1) and an increase in the oxidation  
284 products (factor 2).

285 The factor profiles (ie: mass spectra) extracted by PMF analysis are shown in

286 Figure 2. The main fragments of CA including m/z values 129 ( $C_5H_5O_4^+$ ) and 87  
287 ( $C_3H_3O_3^+$ ) are present in factor 1 (Figure 2A). These fragments are in good agreement  
288 with the NIST mass spectra of pure CA and the mass spectrum of pure CA particles  
289 measured with the C-ToF-AMS (Figure 3). Figure 4 further compared the normalized  
290 mass spectra of factor 1 and pure CA directly measured with the C-ToF-AMS. The  
291 relative intensities for all ions of pure CA are linearly correlated with that of factor 1  
292 with a slope of 0.985 and R of 0.9999. This further confirmed that factor 1 should be  
293 assigned to unreacted CA. Figure 2C shows the difference mass spectra (factor 2 –  
294 factor 1). Consumption of m/z values 147 ( $C_5H_7O_5^+$ ), 129, 87, 85 ( $C_4H_5O_2^+$ ) and 60  
295 ( $C_2H_4O_2^+$ ) can be observed, which is consistent with the assignment that factor 2  
296 belongs to oxidation products of CA. However, small changes in the relative  
297 intensities of these peaks suggest that the structure of the oxidation products of CA are  
298 likely similar to that of CA. For example, as shown in Figure 2A and B, the intensity  
299 of m/z 129 and 87 in factor 2 are  $0.0125 \pm 0.0046$  and  $0.0218 \pm 0.0013$  compared to  
300  $0.0141 \pm 0.0046$  and  $0.0235 \pm 0.0013$  in factor 1.

301 The changes of the relative concentrations of gas phase methanol and particle  
302 phase CA are shown in Figure 5. The signal of CA extracted by PMF analysis also  
303 responded to OH exposure as expected, when methanol was present in the gas phase,  
304 which is similar to that of Figure 1. The relative intensities of the typical tracers of CA  
305 at m/z 87, 129 and 147 are shown in Figure 5C. As shown in Figure 5 B and C, the  
306 drop in the PMF product factor is substantially greater than that of any of the  
307 individual ions. In addition, the consumption of the smaller tracer (m/z 87) is

308 substantially lower than that of the larger ones (m/z values 129 and 147). For example,  
309 the maximum consumption of CA extracted with PMF analysis is approximately 80 %,   
310 in comparison to ~30 %, ~10 % and 5 % for m/z values 147, 129 and 87, respectively.  
311 These results support the small differences in the mass spectra between the unreacted  
312 CA and its oxidation products as shown in Figure 2. Furthermore, it suggests that the  
313 measured loss of these fragments, which were supposedly only derived from CA, had  
314 in fact contributions from the fragmentation of the products of CA oxidation. This  
315 ultimately would lead to an underestimation of the second order heterogeneous rate  
316 constant (or OH uptake coefficients) if these fragments were chosen as the proxies for  
317 the particle phase concentration of CA. In particular, the difference between the  
318 PMF-factor decay rate and the marker-ion decay rate is mathematically possible only  
319 when the two factors (reactants and products) are extremely similar.

320 **3.2 Reaction kinetics.** The saturation vapor pressure of CA at 298K is  $1.6 \times 10^{-7}$  Pa  
321 (Huisman et al., 2013), thus 99.9% of CA should be present in the particle phase  
322 under the current experimental conditions according to a partition model (Kroll and  
323 Seinfeld, 2008; Pankow, 1994). Although new particle formation was observed with a  
324 CPC in the experiments (at the exit of the reactor), it has no influence on the measured  
325 mass concentration of OA due to the small particle size of the new particles. This is  
326 well supported by the constant mass concentration of OA measured with the AMS  
327 during oxidation experiments (Figure 1A). In addition, as pointed out in our previous  
328 work (Liu et al., 2014), evaporation of CA from particles could potentially contribute  
329 to the decreases in particle phase CA concentration observed as a function of OH

330 exposure. If CA evaporation was at play, the derived reaction rates will be  
331 overestimated using either the present approach or the simpler methods of using  
332 single fragments. The evaporation of CA from the particle phase under these  
333 experimental conditions from control experiments is less than 0.005 % based upon an  
334 evaporation model (Jacobson, 2005). This implies that the observed changes in CA  
335 concentration in the particle phase were due to the particle phase reaction.

336 The relative rates (relative to initial conditions) for CA and methanol in these  
337 experiments are shown in Figure 6. The logarithmic  $c/c_0$  of CA both measured with  
338 the tracers and extracted with PMF analysis linearly correlated to that of methanol  
339 with  $R^2 > 0.95$ . The derived relative rate constant based upon PMF analysis is  
340  $3.01 \pm 0.27$ , while it is  $0.72 \pm 0.05$  and  $0.22 \pm 0.01$  for  $m/z$  values 147 and 129,  
341 respectively. Applying the  $k_2$  value of methanol towards OH of  $9.4 \times 10^{-13} \text{ cm}^3$   
342  $\text{molecule}^{-1} \text{ s}^{-1}$  at 298 K (Atkinson and Arey, 2003), the  $k_2$  of CA is calculated as  
343  $(2.83 \pm 0.25) \times 10^{-12}$  using the PMF approach, or  $(6.77 \pm 0.47) \times 10^{-13}$  using the single  
344 tracer at  $m/z$  147 and  $(2.02 \pm 0.01) \times 10^{-13} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$  using the single tracer at  
345  $m/z$  129, respectively. The reaction between methanol and OH radicals occurs in the  
346 gas phase, while for the CA oxidation it occurs in particle phase. Thus it is necessary  
347 to correct for OH diffusion from the bulk gas phase to the particle phase. Applying a  
348 diffusion correction utilizing a previously developed empirical formula (Fuchs and  
349 Sutugin, 1970; Worsnop et al., 2002; Widmann and Davis, 1997), the  
350 diffusion-corrected  $k_2$  is  $(3.31 \pm 0.29) \times 10^{-12}$  using the PMF approach, and  
351  $(7.92 \pm 0.55) \times 10^{-13}$  and  $(2.36 \pm 0.01) \times 10^{-13} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$  using single tracers at  $m/z$



352 147 and 129, respectively. The diffusion-corrected  $\gamma_{\text{OH}}$  is calculated as  $2.74 \pm 0.24$   
353 using the PMF approach, and  $0.66 \pm 0.05$  and  $0.20 \pm 0.01$  using single tracers at  $m/z$  147  
354 and 129, respectively. The  $\gamma_{\text{OH}}$  for a number of different organic particles have  
355 previously been measured, and are in the range of 0.3 – 2.0 (Kessler et al.,  
356 2010; George et al., 2007; Hearn and Smith, 2006; Lambe et al., 2007; Smith et al.,  
357 2009; Kessler et al., 2012). As pointed out by Hearn and Smith (2006), the large  $\gamma$   
358 implies that secondary radical reactions within the particles could play a significant  
359 role in heterogeneous chemistry, particularly since gaseous citric acid in these studies  
360 is insignificant.

361 It should be pointed out that oxidant diffusion in the particle phase should lead to  
362 a concentration gradient of oxidant and a negative impact on reaction kinetics  
363 (Donahue et al., 2005). However, as shown in Figure 6, this effect is negligible under  
364 the current experimental conditions. Based upon the measured  $c/c_0$  and the initial  
365 diameter of the CA particles, the maximum OH diffusion depth is approximately 25  
366 nm. Given the residence time ( $\tau$ ) in this study (52 s), a significant OH concentration  
367 gradient will exist in particle phase if the  $D_{\text{OH}}$  in CA particles is smaller than  $1.2 \times 10^{-17}$   
368  $\text{m}^2 \text{s}^{-1}$  ( $D = l^2/\tau$ ) (Donahue et al., 2005). At the present time, the  $D_{\text{OH}}$  in CA particles is  
369 unavailable. However, Price et al. (Price et al., 2014) have reported the diffusion of  
370  $\text{D}_2\text{O}$  in several organics (sucrose and levoglucosan) to be larger than  $\sim 1 \times 10^{-16} \text{m}^2 \text{s}^{-1}$   
371 even under dry condition. This implies that a gradient in OH concentration in the CA  
372 particles is negligible under the current conditions.

#### 373 **4. Discussion**

374 Kessler et al. (Kessler et al., 2012) have reported the  $k_2$  of CA toward OH to be  
375  $(4.3\pm 0.8)\times 10^{-13}$  cm<sup>3</sup> molecule s<sup>-1</sup> at 308 K and 30 % RH with an Aerodyne HR-AMS.  
376 In their work, the diameter of particles and RH were equivalent to the current work,  
377 while their experimental temperature was 10 K higher. In addition, a m/z fragment of  
378 68 was used as a tracer for CA in their work to derive the heterogeneous rate constant.  
379 Conversely, no significant consumption of m/z 68 was observed in the current study.  
380 The lack of a m/z 68 fragment consumption here may be explained by the choice of  
381 reaction conditions. In the work of Kessler et al., OH concentration exposure  
382  $(0\sim 7\times 10^{12}$  molecule cm<sup>-3</sup> s) was approximately an order of magnitude higher than that  
383 reported here. Recent evidence suggests that the product distribution during OA  
384 oxidation greatly depends upon OH exposure levels (Wilson et al., 2012). Hence, it is  
385 possible that more oxidized products formed via multi-generational chemistry at high  
386 OH were formed, which may have less of an influence on the signal of the chosen  
387 tracer (m/z 68), and result in product AMS spectra which are significantly different  
388 than that of the reactant thus mitigating the use of PMF (which was not the case here).  
389 In studies of the OH oxidation of squalane (Sq) (Smith et al., 2009; Wilson et al.,  
390 2012), the first generation product (SqO) was the primary contributor to the products  
391 when the OH exposure was the same as the highest OH level in the current study  
392  $(7.0\times 10^{11}$  molecules cm<sup>-3</sup> s), while higher generation products were predominant at  
393 OH exposures was greater than  $\sim 2\times 10^{12}$  molecules cm<sup>-3</sup> s. Although not directly  
394 comparable, it is reasonable to assume that lower OH exposure in the current work  
395 should lead primarily to the first generation products, which are highly similar to CA.

396 However, the formation of multi-generation products cannot be completely ruled out.  
397 Secondly, the difference in OA and oxidant concentrations as well as timescale may  
398 also have an influence on the product distribution. Thirdly, a high resolution  
399 time-of-flight aerosol mass spectrometer (HR-ToF-AMS) was used in their work,  
400 while a C-ToF-AMS with unit-mass resolution was used in this study. The higher  
401 mass resolution of the HR-ToF-AMS relative to a C-ToF-AMS, may further reduce  
402 the influence of product fragments on  $m/z$  68 (or others). Finally, differences in  
403 temperature or other reaction conditions between experiments may also have led to  
404 differences in the morphology of CA and subsequent differences in the reactivity of  
405 CA.

406 Given the above discrepancy in the consumption of  $m/z$  68, the fragments at  $m/z$   
407 129 and 147 were used as tracers in this work. The measured  $k_2$  of CA utilizing  $m/z$   
408 129 and 147 in this study is of the same order of magnitude as that reported in Kessler  
409 et al. (2012). However, as shown in Figure 3C, the consumption of  $m/z$  87 is much  
410 lower than that of  $m/z$  129. The apparent  $k_2$  of CA based on  $m/z$  87 is  $(9.9 \pm 0.8) \times 10^{-14}$   
411  $\text{cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$ , and the diffusion-corrected  $k_2$  is  $(1.16 \pm 0.09) \times 10^{-13} \text{ cm}^3 \text{ molecule}^{-1}$   
412  $\text{s}^{-1}$ . This suggests that the derived rate constant greatly depends upon the size of the  
413 tracer fragment, with larger fragments resulting in larger values of  $k_2$  in this study.  
414 This is consistent with previous work investigating the OH oxidation of tris-phenyl  
415 phosphate (TPhP) (Liu et al., 2014) and ambient biogenic SOA (Slowik et al., 2012).  
416 The  $k_2$  of CA based upon PMF analysis is approximately an order of magnitude larger  
417 than the Kessler result measured with the tracer at  $m/z$  68, and 4.2 times greater than

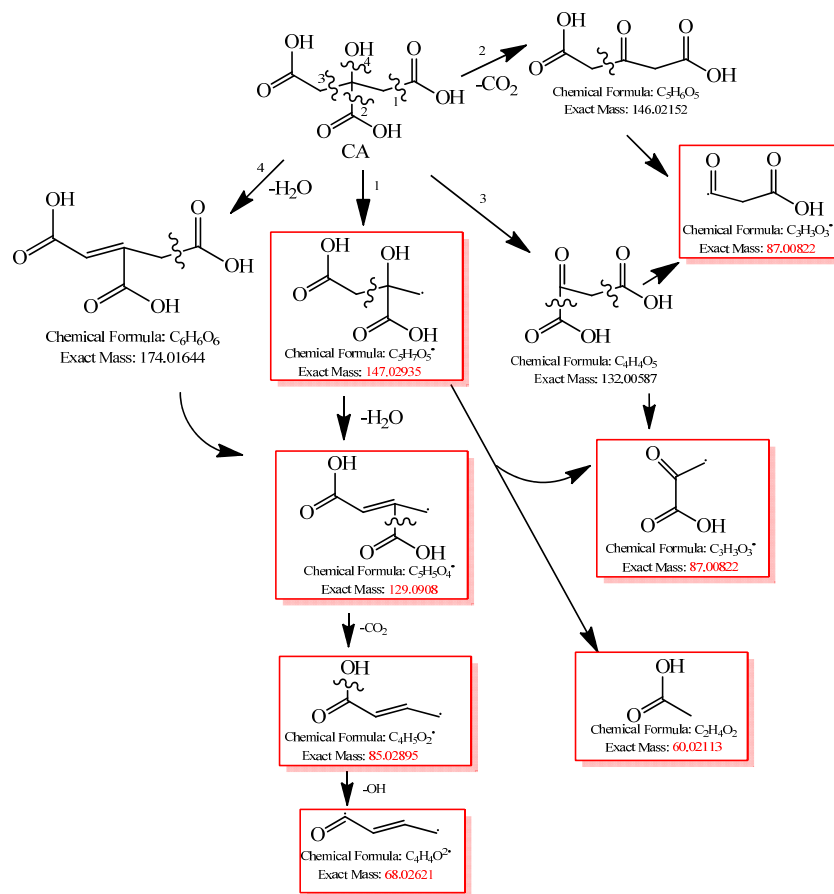
418 that calculated based upon  $m/z$  147 in this study. The differences in product  
419 distributions that may arise between this and the work of Kessler et al., consistent  
420 with the fact that  $m/z$  68 is not consumed in the current study, suggests that the PMF  
421 approach was likely required in this work to separate similar product and reactant  
422 spectra ultimately caused by lower OH exposure.

423 A number of factors may be responsible for the discrepancy between derived rate  
424 constants. It has previously been observed that the presence of  $O_3$  can inhibit the rate  
425 of OH reaction, perhaps by reacting with OH radicals or by  $O_3$  or intermediate species  
426 blocking surface active sites (Renbaum and Smith, 2011). A Langmuir-Hinshelwood  
427 mechanism has been observed for the reaction of  $O_3$  on organic surfaces (Pöschl,  
428 2005). It has also been demonstrated that a higher concentration of gas phase reactant  
429 often leads to a lower uptake coefficient due to surface saturation (Ma et al., 2010 ;Li  
430 et al., 2002). Differences in  $k_2$  may also arise from the competition between reaction  
431 products and reactants for available OH, or via the blocking or coating of the reactant  
432 by products which would require liquid phase diffusion of OH to degrade the original  
433 CA. In experiments with higher OH exposures (Kessler et al 2012) it is possible that  
434 significantly more product mass is mixed and/or coated onto the original particle thus  
435 decreasing the perceived  $k_2$ . Different timescales and concentrations of reactants  
436 might also lead to different rate constants (Che et al., 2009). Finally, as pointed out  
437 above, the differing reaction conditions may have led to a different CA morphology  
438 and subsequent differences in the reactivity towards OH. The significant difference  
439 between the reported rate constants highlights an important issue in heterogeneous

440 reactions of the atmosphere, and in the experiments trying to derive such kinetics. It  
441 implies that the particle composition and/or morphology as determined by the reaction  
442 conditions in the laboratory or the ambient atmosphere will have a large effect on the  
443 OH kinetics.

444 Citric acid is a hydroxyl substituted poly carboxyl acid. Scheme 1 summarizes its  
445 possible fragmentation pathways. The typical mass peaks including  $m/z$  147, 129, 87,  
446 85 and 68 would result from this scheme and were indeed observed. The fragments at  
447  $m/z$  129, 87, 85 and 68 are also likely from CA oxidation products fragments, and  
448 hence their signal intensities may be highly influenced by products and/or larger  
449 fragments, in particular, when the oxidized products are highly similar to the reactant.  
450 In some instances, oxidation products can exhibit similar fragmentation pathways as  
451 the reactants. This is likely the case for the smaller fragments of CA. For example,  
452 scheme 2 illustrates the possible fragmentation pathways of  
453 2,3-dihydroxypropane-1,2,3-tricarboxylic acid, which is one of the possible products  
454 from the OH oxidation of citric acid in terms of the general chemistry described by  
455 Atkinson et al. (Atkinson, 1986). As observed in Scheme 2, there are several pathways  
456 leading to the fragment at  $m/z$  87, implying that the decrease in the signal of  $m/z$  87  
457 due to CA oxidation is likely to be compensated by fragments from the oxidation  
458 products. In addition, it is also possible to form fragments with the same  $m/z$  as the  
459 parent citric acid if the dehydration reaction (the 6<sup>th</sup> path in Scheme 2) takes place  
460 initially. Other possible reaction products might also play similar roles in the  
461 fragments. This is highly possible when the product distribution contains products

462 which are structurally similar to the reactant under low oxidant exposure conditions.

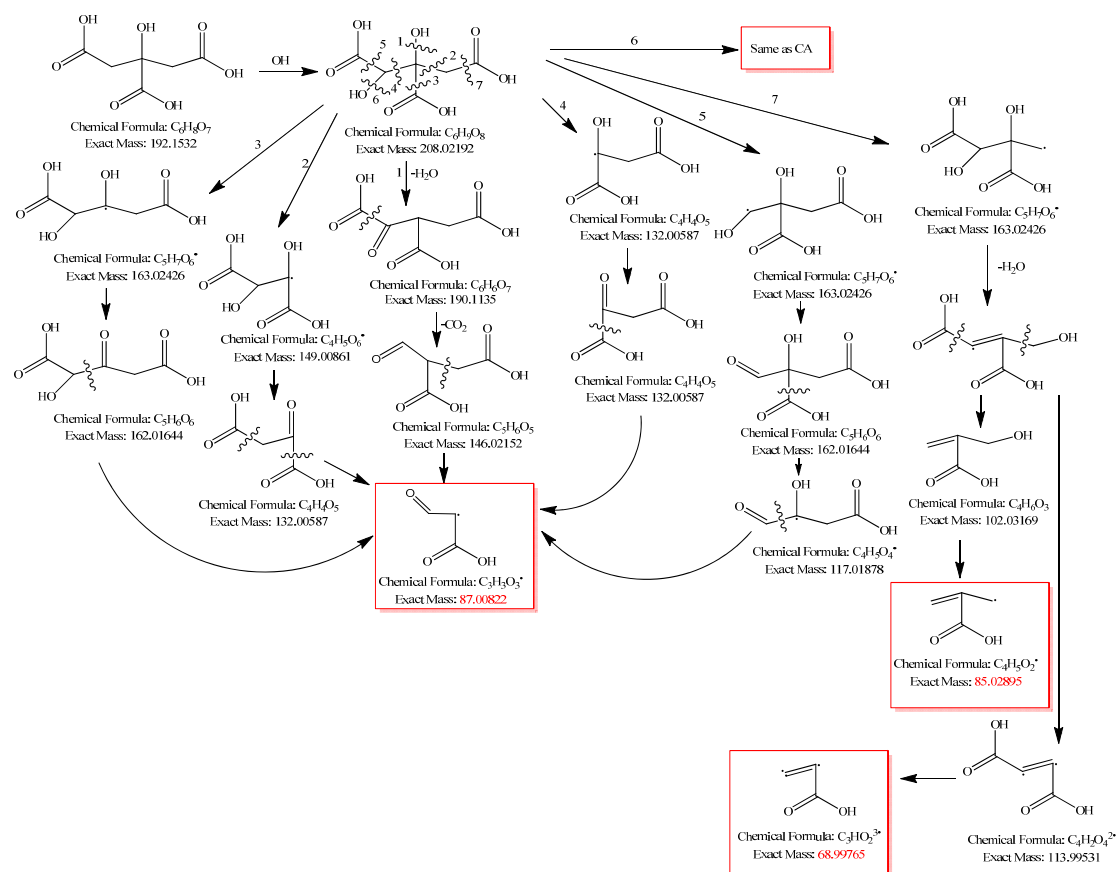


463

464

Scheme 1. Possible fragmentation pathways for citric acid.

465



478 435), respectively. The typical evolution of the PMF factors of TPhP, TDCPP, and  
479 TEHP are shown in Figures S1-3. For TPhP, the measured  $k_2$  values derived by both  
480 methods are comparable within the experimental uncertainties, while  $k_2$  of TDCPP  
481 and TEHP based upon PMF analysis is 1.5 and 1.6 times larger than that using the  
482 chosen tracers. The good agreement between methods for TPhP is likely due to the  
483 fact that the molecular ion peak ( $M^+$ ) is measurable for TPhP with the AMS, while it  
484 is not observable for TDCPP, TEHP and CA. Therefore, the influence of secondary  
485 fragmentation from larger fragments has little influence on the signal of  $M^+$  for TPhP.  
486 These results also demonstrate that a substantial underestimation of rate constants  
487 could result when a non-molecular ion tracer is used to monitor the particle phase  
488 concentration of organic matter with UMR-AMS for heterogeneous kinetic studies.  
489 The discrepancy between the tracer and PMF based methods for other compounds  
490 will depend upon a number of factors including: structure of products, OH exposure  
491 level, particle morphology, and organic species competing OH reactions.

492

## 493 **5.0 Implications and Conclusions**

494 The measured  $k_2$  for citric acid toward OH is  $(3.31 \pm 0.29) \times 10^{-12} \text{ cm}^3 \text{ molecule}^{-1}$   
495  $\text{s}^{-1}$  at 298 K and 30 % RH. This value is at least 4.2 times greater than that calculated  
496 on the basis of atypical tracer  $m/z$  147. Although the tracer and PMF approaches can  
497 at times agree (Kroll, 2014) and the tracer and molecular-ion approaches can  
498 sometimes agree as well (Smith et al., 2009), our results suggest that the  
499 heterogeneous kinetics of OA is underestimated when a non-molecular ion peak is



500 used as the tracer to measure the particle phase concentration of OA based on  
501 UMR-AMS. In model simulations, the reactive uptake coefficient of OH or other  
502 radicals, which are calculated based upon  $k_2$ , is an important parameter in evaluating  
503 the fate of OA during transport. The current results suggest that the lifetime of OA  
504 estimated in models due to heterogeneous oxidation might be overestimated for a  
505 reaction system where the products are highly similar to the reactant and the kinetic  
506 data are derived by individual non-molecular m/z tracers of OA. The results also  
507 suggest that it may be necessary to revisit the kinetic data of other organic aerosol  
508 components (and OH uptake coefficients) which have been derived using the relative  
509 rates technique (George et al., 2007; Lambe et al., 2007) based on UMR-AMS. Finally,  
510 these results imply that the heterogeneous oxidation of aerosols will be dependent  
511 upon a number of factors related to the reaction system, and that a single rate constant  
512 for one system cannot be universally applied under all conditions. Future work is thus  
513 required to elucidate the chemical and physical parameters which control the OH  
514 heterogeneous reaction kinetics and the associated need to apply PMF for a variety of  
515 chemical systems. This may be best accomplished through systematic application of  
516 the PMF approach to species with differing mass spectral characteristics, such as  
517 linear/branched alkanes, monocarboxylic acids and other oxygenates. As illustrated in  
518 this study, the kinetics derived with PMF may differ from that derived with tracer ions,  
519 with both based upon EI-AMS approaches. This highlights the usefulness of  
520 measurements from CIMS, GC-MS and VUV-AMS, for the determination of  
521 heterogeneous loss rates, since these instruments are more likely to retain the reactant

522 molecular information.

523

## 524 **Supporting Information**

525 Supplementary material related to this article is available online at:

526

## 527 **Acknowledgements**

528 This research was funded by the Chemicals Management Plan (CMP) and the Clean

529 Air Regulatory Agenda (CARA).

## 530 **Literature Cited:**

531 Allan, J. D., Jimenez, J. L., Williams, P. I., Alfarra, M. R., Bower, K. N., Jayne, J. T., Coe, H., and  
532 Worsnop, D. R.: Quantitative sampling using an Aerodyne aerosol mass spectrometer 1. Techniques of  
533 data interpretation and error analysis, *J. Geophys. Res.*, 108, 4090, 10.1029/2002jd002358, 2003.

534 Atkinson, R.: Kinetics and Mechanisms of the Gas-Phase Reactions of the Hydroxyl Radical with  
535 Organic Compounds under Atmospheric Conditions, *Chem. Rev.*, 85, 69-201, 1986.

536 Atkinson, R., and Arey, J.: Atmospheric Degradation of Volatile Organic Compounds, *Chem. Rev.*, 103,  
537 4605-4638, 2003.

538 Cappa, C. D., Che, D. L., Kessler, S. H., Kroll, J. H., and Wilson, K. R.: Variations in organic aerosol  
539 optical and hygroscopic properties upon heterogeneous OH oxidation, *J. Geophys. Res.*, 116, D15204,  
540 10.1029/2011jd015918, 2011.

541 Che, D. L., Smith, J. D., Leone, S. R., Ahmed, M., and Wilson, K. R.: Quantifying the reactive uptake  
542 of OH by organic aerosols in a continuous flow stirred tank reactor, *Phys. Chem. Chem. Phys.*, 11,  
543 7885-7895, 10.1039/b904418c, 2009.

544 Donahue, N. M., Robinson, A. L., Hartz, K. E. H., Sage, A. M., and Weitkamp, E. A.: Competitive  
545 oxidation in atmospheric aerosols: The case for relative kinetics, *Geophys. Res. Lett.*, 32, L16805,  
546 10.1029/2005gl022893, 2005.

547 Drewnick, F., Hings, S. S., DeCarlo, P., Jayne, J. T., Gonin, M., Fuhrer, K., Weimer, S., Jimenez, J. L.,  
548 Demerjian, K. L., Borrmann, S., and Worsnop, D. R.: A New Time-of-Flight Aerosol Mass  
549 Spectrometer (TOF-AMS)—Instrument Description and First Field Deployment, *Aerosol Sci. Technol.*,  
550 39, 637-658, 2005.

551 Fuchs, N. A., and Sutugin, A. G.: *Highly Dispersed Aerosols*, Butterworth-Heinemann, Newton, MA,  
552 1970.

553 George, I. J., Vlasenko, A., Slowik, J. G., Broekhuizen, K., and Abbatt, J. P. D.: Heterogeneous  
554 oxidation of saturated organic aerosols by hydroxyl radicals: uptake kinetics, condensed-phase products,  
555 and particle size change, *Atmos. Chem. Phys.*, 7, 4187-4201, 2007.

556 George, I. J., and Abbatt, J. P. D.: Chemical evolution of secondary organic aerosol from OH-initiated

557 heterogeneous oxidation, *Atmos. Chem. Phys.*, 10, 5551-5563, 2010.

558 Hearn, J. D., and Smith, G. D.: A mixed-phase relative rates technique for measuring aerosol reaction  
559 kinetics, *Geophys. Res. Lett.*, 33, L17805, 10.1029/2006gl026963, 2006.

560 Huisman, A. J., Krieger, U. K., Zuend, A., Marcolli, C., and Peter, T.: Vapor pressures of substituted  
561 polycarboxylic acids are much lower than previously reported, *Atmos. Chem. Phys.*, 13, 6647-6662,  
562 10.5194/acp-13-6647-2013, 2013.

563 Isaacman, G., Chan, A. W. H., Nah, T., Worton, D. R., Ruehl, C. R., Wilson, K. R., and Goldstein, A. H.:  
564 Heterogeneous OH Oxidation of Motor Oil Particles Causes Selective Depletion of Branched and Less  
565 Cyclic Hydrocarbons, *Environ. Sci. Technol.*, 46, 10632-10640, 10.1021/es302768a, 2012.

566 Jacobson, M. Z.: *Fundamentals of Atmospheric Modeling*, Cambridge University Press, 2005.

567 Jayne, J. T., Leard, D. C., Zhang, X., Davidovits, P., Smith, K. A., Kolb, C. E., and R. Worsnop, D.:  
568 Development of an Aerosol Mass Spectrometer for Size and Composition Analysis of Submicron  
569 Particles, *Aerosol Sci. Technol.*, 33, 49-70, 2000.

570 Kessler, S. H., Smith, J. D., Che, D. L., Worsnop, D. R., Wilson, K. R., and Kroll, J. H.: Chemical  
571 Sinks of Organic Aerosol: Kinetics and Products of the Heterogeneous Oxidation of Erythritol and  
572 Levoglucosan, *Environ. Sci. Technol.*, 44, 7005-7010, 10.1021/es101465m, 2010.

573 Kessler, S. H., Nah, T., Daumit, K. E., Smith, J. D., Leone, S. R., Kolb, C. E., Worsnop, D. R., Wilson,  
574 K. R., and Kroll, J. H.: OH-Initiated Heterogeneous Aging of Highly Oxidized Organic Aerosol, *J. Phys.*  
575 *Chem. A*, 116, 6358-6365, 10.1021/jp212131m, 2012.

576 Kolb, C. E., Cox, R. A., Abbatt, J. P. D., Ammann, M., Davis, E. J., Donaldson, D. J., Garrett, B. C.,  
577 George, C., Griffiths, P. T., Hanson, D. R., Kulmala, M., McFiggans, G., P'oschl, U., Riipinen, I., Rossi,  
578 M. J., Rudich, Y., Wagner, P. E., Winkler, P. M., Worsnop, D. R., and Dowd, C. D. O.: An overview of  
579 current issues in the uptake of atmospheric trace gases by aerosols and clouds, *Atmos. Chem. Phys.*, 10,  
580 10561-10605, 2010.

581 Kroll, J. H., and Seinfeld, J. H.: Chemistry of secondary organic aerosol: Formation and evolution of  
582 low-volatility organics in the atmosphere, *Atmos. Environ.*, 42, 3593-3624, 2008.

583 Lambe, A. T., Zhang, J. Y., Sage, A. M., and Donahue, N. M.: Controlled OH radical production via  
584 ozone-alkene reactions for use in aerosol aging studies, *Environ. Sci. Technol.*, 41, 2357-2363,  
585 10.1021/es061878e, 2007.

586 Lambe, A. T., Miracolo, M. A., Hennigan, C. J., Robinson, A. L., and Donahue, N. M.: Effective Rate  
587 Constants and Uptake Coefficients for the Reactions of Organic Molecular Markers (n-Alkanes,  
588 Hopanes, and Steranes) in Motor Oil and Diesel Primary Organic Aerosols with Hydroxyl Radicals,  
589 *Environ. Sci. Technol.*, 43, 8794-8800, 10.1021/es901745h, 2009.

590 Li, P., Al-Abadleh, H. A., and Grassian, V. H.: Measuring heterogeneous uptake coefficients of gases on  
591 solid particle surfaces with a Knudsen Cell reactor: complications due to surface saturation and gas  
592 diffusion into underlying layers., *J. Phys. Chem. A*, 106, 1210-1219, 2002.

593 Liggio, J., Li, S. M., Vlasenko, A., Sjostedt, S., Chang, R., Shantz, N., Abbatt, J., Slowik, J. G.,  
594 Bottenheim, J. W., Brickell, P. C., Stroud, C., and Leaitch, W. R.: Primary and secondary organic  
595 aerosols in urban air masses intercepted at a rural site, *J. Geophys. Res.-Atmos.*, 115, D21305,  
596 doi:10.1029/2010JD014426., D21305  
597 10.1029/2010jd014426, 2010.

598 Liu, C., Zhang, P., Wang, Y., Yang, B., and Shu, J.: Heterogeneous Reactions of Particulate  
599 Methoxyphenols with NO<sub>3</sub> Radicals: Kinetics, Products, and Mechanisms, *Environ. Sci. Technol.*, 46,  
600 13262-13269, 2012.

601 Liu, Y., Liggio, J., Harner, T., Jantunen, L., Shoeib, M., and Li, S.-M.: Heterogeneous OH initiated  
602 oxidation: A possible explanation for the persistence of organophosphate flame retardants in air,  
603 *Environ. Sci. Technol.*, 48, 1041-1048, 2014.

604 Ma, J., Liu, Y., and He, H.: Degradation kinetics of anthracene by ozone on mineral oxides, *Atmos.*  
605 *Environ.*, 44, 4446-4453, 2010

606 McNeill, V. F., Wolfe, G. M., and Thornton, J. A.: The Oxidation of Oleate in Submicron Aqueous Salt  
607 Aerosols: Evidence of a Surface Process, *J. Phys. Chem. A*, 111, 1073-1083, 2007.

608 McNeill, V. F., Yatavelli, R. L. N., Thornton, J. A., Stipe, C. B., and Landgrebe, O.: Heterogeneous OH  
609 oxidation of palmitic acid in single component and internally mixed aerosol particles: vaporization and  
610 the role of particle phase, *Atmos. Chem. Phys.*, 8, 5465-5476, 10.5194/acp-8-5465-2008, 2008.

611 Norris, G., and Vedantham, R.: EPA positive matrix factorization (PMF) 3.0 fundamentals & user guide,  
612 U.S. Environmental Protection Agency, [www.epa.gov](http://www.epa.gov), 2008.

613 Pöschl, U.: Atmospheric Aerosols: Composition, Transformation, Climate and Health Effects, *Angew.*  
614 *Chem. Int. Ed.*, 44, 7520-7540, 2005.

615 Paatero, P., and Tapper, U.: Positive matrix factorization: a nonnegative factor model with optimal  
616 utilization of error estimates of data values, *Environmetrics* 5, 111-126, 1994.

617 Paatero, P.: Least squares formulation of robust non - negative factor analysis, *Chemom. Intell. Lab.*  
618 *Syst.*, 37, 23-35, doi:10.1016/S0169-7439(96)00044-5., 1997.

619 Paatero, P., and Hopke, P. K.: Discarding or downweighting highnoise variables in factor analytic  
620 models, *Anal. Chim. Acta*, 490, 277-289, 2003.

621 Pankow, J. F.: An absorption-model of gas-particle partitioning of organic compounds in the  
622 atmosphere, *Atmos. Environ.*, 28, 185-188, 1994.

623 Price, H. C., Murray, B. J., Mattsson, J., O'Sullivan, D., Wilson, T. W., Baustian, K. J., and Benning, L.  
624 G.: Quantifying water diffusion in high-viscosity and glassy aqueous solutions using a Raman isotope  
625 tracer method, *Atmos. Chem. Phys.*, 14, 3817-3830, 10.5194/acp-14-3817-2014, 2014.

626 Reff, A., Eberly, S. I., and Bhave, P. V.: Receptor modeling of ambient particulate matter data using  
627 positive matrix factorization: Review of existing methods, *J. Air Waste Manage.*, 57, 146-154, 2007.

628 Renbaum, L. H., and Smith, G. D.: Artifacts in measuring aerosol uptake kinetics: the roles of time,  
629 concentration and adsorption, *Atmos. Chem. Phys.*, 11, 6881-6893, 10.5194/acp-11-6881-2011, 2011.

630 Sareen, N., Moussa, S. G., and McNeill, V. F.: Photochemical Aging of Light-Absorbing Secondary  
631 Organic Aerosol Material, *J. Phys. Chem. A*, 117, 2987-2996, 2013.

632 Schwartz, R. E., Russell, L. M., Sjostedt, S. J., Vlasenko, A., Slowik, J. G., Abbatt, J. P. D., Macdonald,  
633 A. M., Li, S. M., Liggio, J., Toom-Sauntry, D., and Leitch, W. R.: Biogenic oxidized organic  
634 functional groups in aerosol particles from a mountain forest site and their similarities to laboratory  
635 chamber products, *Atmos. Chem. Phys.*, 10, 5075-5088, 10.5194/acp-10-5075-2010, 2010.

636 Slowik, J. G., Wong, J. P. S., and Abbatt, J. P. D.: Real-time, controlled OH-initiated oxidation of  
637 biogenic secondary organic aerosol, *Atmos. Chem. Phys.*, 12, 9775-9790, 10.5194/acp-12-9775-2012,  
638 2012.

639 Smith, J. D., Kroll, J. H., Cappa, C. D., Che, D. L., Liu, C. L., Ahmed, M., Leone, S. R., Worsnop, D.  
640 R., and Wilson, K. R.: The heterogeneous reaction of hydroxyl radicals with sub-micron squalane  
641 particles: a model system for understanding the oxidative aging of ambient aerosols, *Atmos. Chem.*  
642 *Phys.*, 9, 3209-3222, 10.5194/acp-9-3209-2009, 2009.

643 Song, Y., Zhang, Y., Xie, S., Zeng, L., Zheng, M., Salmon, L. G., Shao, M., and Slanina, S.: Source  
644 apportionment of PM<sub>2.5</sub> in Beijing by positive matrix factorization, *Atmos. Environ.*, 40, 1526-1537,

645 2006.  
646 Ulbrich, I. M., Canagaratna, M. R., Zhang, Q., Worsnop, D. R., and Jimenez, J. L.: Interpretation of  
647 organic components from Positive Matrix Factorization of aerosol mass spectrometric data, *Atmos.*  
648 *Chem. Phys.*, 9, 2891-2918, 2009.  
649 Viana, M., Kuhlbusch, T. A. J., Querol, X., Alastuey, A., Harrison, R. M., Hopke, P. K., Winiwarter, W.,  
650 Vallius, A., Szidat, S., Prevot, A. S. H., Hueglin, C., Bloemen, H., Wahlin, P., Vecchi, R., Miranda, A. I.,  
651 Kasper-Giebl, A., Maenhaut, W., and Hitzenberger, R.: Source apportionment of particulate matter in  
652 Europe: A review of methods and results, *J. Aerosol. Sci.*, 39, 827-849, 10.1016/j.jaerosci.2008.05.007,  
653 2008.  
654 Weitkamp, E. A., Hartz, K. E. H., Sage, A. M., Donahue, N. M., and Robinson, A. L.: Laboratory  
655 measurements of the heterogeneous oxidation of condensed-phase organic molecular makers for meat  
656 cooking emissions, *Environ. Sci. Technol.*, 42, 5177-5182, 2008a.  
657 Weitkamp, E. A., Lambe, A. T., Donahue, N. M., and Robinson, A. L.: Laboratory Measurements of the  
658 Heterogeneous Oxidation of Condensed-Phase Organic Molecular Makers for Motor Vehicle Exhaust,  
659 *Environ. Sci. Technol.*, 42, 7950-7956, 10.1021/es800745x, 2008b.  
660 Widmann, J. F., and Davis, E. J.: Mathematical models of the uptake of ClONO<sub>2</sub> and other gases by  
661 atmospheric aerosols, *J. Aerosol. Sci.*, 28, 87-106, 1997.  
662 Wilson, K. R., Smith, J. D., Kessler, S. H., and Kroll, J. H.: The statistical evolution of multiple  
663 generations of oxidation products in the photochemical aging of chemically reduced organic aerosol,  
664 *Phys. Chem. Chem. Phys.*, 14, 1468-1479, 10.1039/c1cp22716e, 2012.  
665 Worsnop, D. R., Morris, J. W., Shi, Q., Davidovits, P., and Kolb, C. E.: A chemical kinetic model for  
666 reactive transformations of aerosol particles, *Geophys. Res. Lett.*, 29, 1996, 10.1029/2002gl015542,  
667 2002.  
668 Yuan, Z. B., Yu, J. Z., Lau, A. K. H., Louie, P. K. K., and Fung, J. C. H.: Application of positive matrix  
669 factorization in estimating aerosol secondary organic carbon in Hong Kong and its relationship with  
670 secondary sulfate, *Atmos. Chem. Phys.*, 6, 25-34, 10.5194/acp-6-25-2006, 2006.  
671 Zhang, Q., Jimenez, J., Canagaratna, M., Ulbrich, I., Ng, N., Worsnop, D., and Sun, Y.: Understanding  
672 atmospheric organic aerosols via factor analysis of aerosol mass spectrometry: a review, *Anal. Bioanal.*  
673 *Chem.*, 401, 3045-3067, 10.1007/s00216-011-5355-y, 2011.  
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689 **Table 1.** Comparison of the measured  $k_2$  values utilizing PMF and select m/z tracers,  
 690 for organophosphate compounds and CA.

OA	Mean $k_{r\_PMF}$	$k_2 (10^{12}) \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$			$k_{2\_PMF}/$ $k_{2\_Tracer}$	$M_{Tracer}/M^+$
		$k_{2, \text{obs\_PMF}}$	$k_{2, \text{t\_PMF}}$	$k_{2, \text{t\_Tracer}}$		
TPhP	1.58±0.33	1.48±0.31	1.95±0.43	2.10±0.19 <sup>a</sup>	0.9	326/326
TDCPP	1.20±0.31	1.13±0.29	1.35±0.35	0.92±0.09 <sup>a</sup>	1.5	381/431
TEHP	3.52±0.65	3.31±0.61	4.25±0.78	2.70±0.63 <sup>a</sup>	1.6	323/435
CA	3.01±0.27	2.83±0.25	3.31±0.29	0.79±0.06	4.2	147/192

691 a.(Liu et al., 2014)

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708 **Figure captions**

709 **Figure 1.** Changes in (A) total organic mass concentration, (B) the fraction of  
710 unreacted citric acid derived by PMF and (C) products of citric acid oxidized by OH  
711 derived by PMF, as a function of relative experimental time. The values 1 – 6  
712 represent a step-wise O<sub>3</sub> concentration decrease, corresponding to decreased OH  
713 exposure; 0 represents an O<sub>3</sub> concentration of zero. Experimental conditions are  $D_m$ :  
714 200 nm, RH:  $30 \pm 3$  %, T: 298 K.

715 **Figure 2.** Normalized mass spectra of (A) citric acid (PMF factor 1), (B) citric acid  
716 oxidation products (PMF factor 2), and (C) the difference mass spectrum (Factor 2 –  
717 Factor 1). The numbers in the upper two rows are the intensities of m/z 87 and 129,  
718 while negative values are shown in the bottom row. The red and green lines indicate a  
719 negative and positive value, respectively.

720 **Figure 3.** Mass spectra (A) of CA from NIST database, (B) of pure CA measured with  
721 the C-ToF-AMS.

722 **Figure 4.** Comparison between the mass spectra of factor 1 from PMF analysis and  
723 pure CA directly measured by the C-ToF-AMS. The inset graph is the correlation of  
724 their corresponding signal intensities.

725 **Figure 5.** Changes in the relative concentration of (A) methanol, (B) citric acid  
726 extracted with PMF analysis and (C) specific tracers measured with the AMS during  
727 the OH initiated oxidation of citric acid. Experimental conditions are  $D_m$ : 140 nm, RH:  
728  $30 \pm 3$  %, T: 298 K. The values in the top row represent the OH exposures.

729 **Figure 6.** Relative concentration of citric acid ( $c/c_0$ ) as a function of the relative  
730 concentration of methanol based upon (A) PMF analysis, (B) m/z=129 and (C) m/z

731 147. Experimental conditions are  $D_m$ : 140 nm, RH:  $30 \pm 3$  %, T: 298 K.

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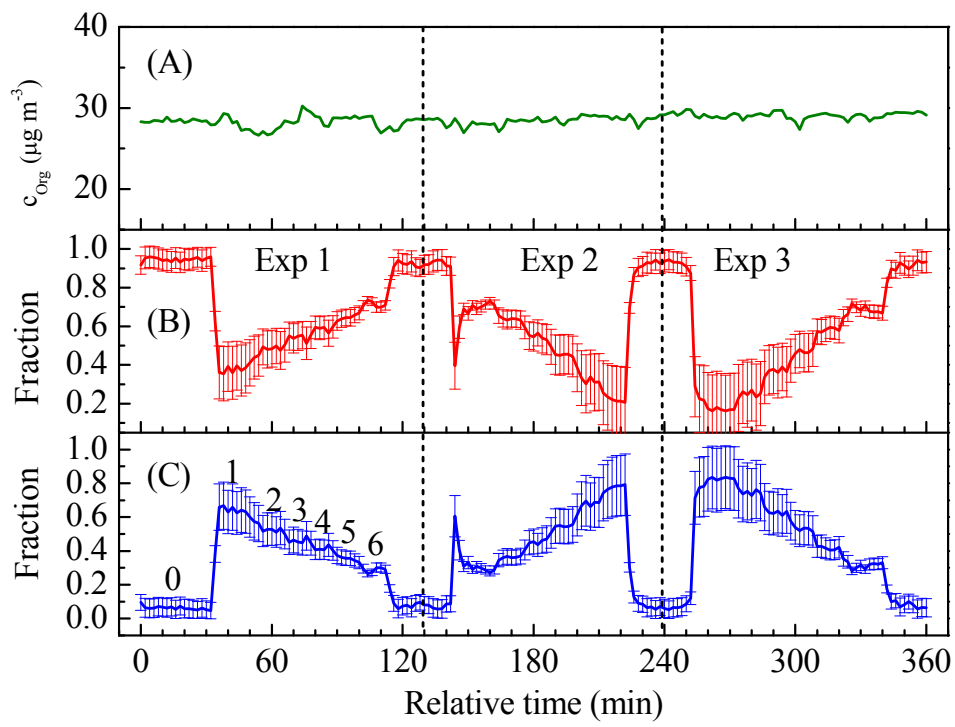
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**Figure 1.**

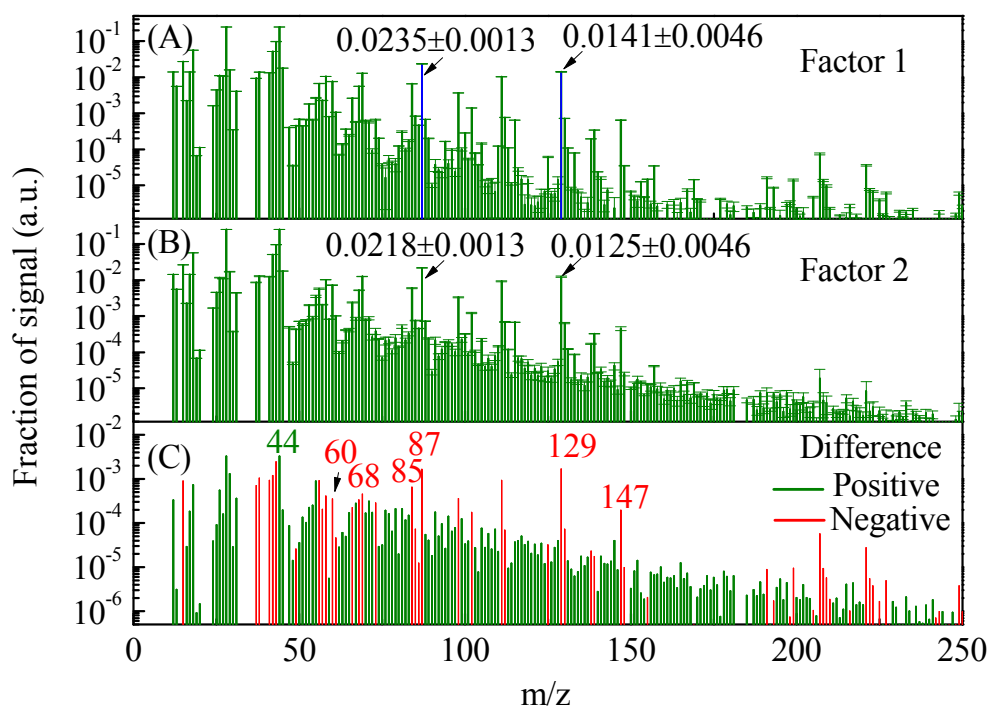
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**Figure 2.**

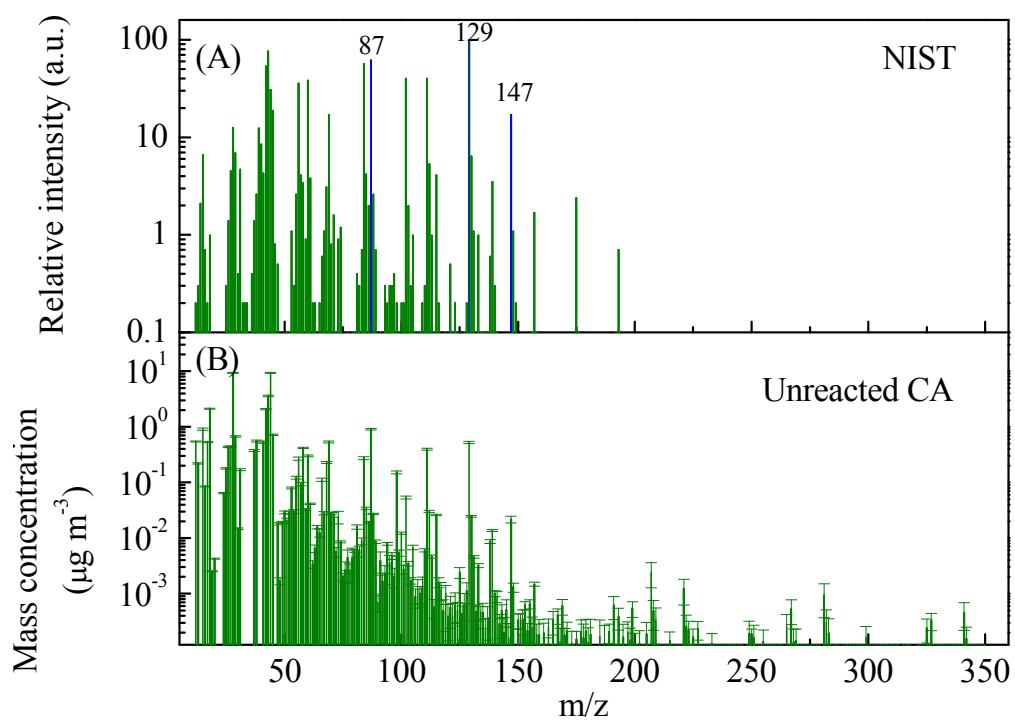


Figure 3.

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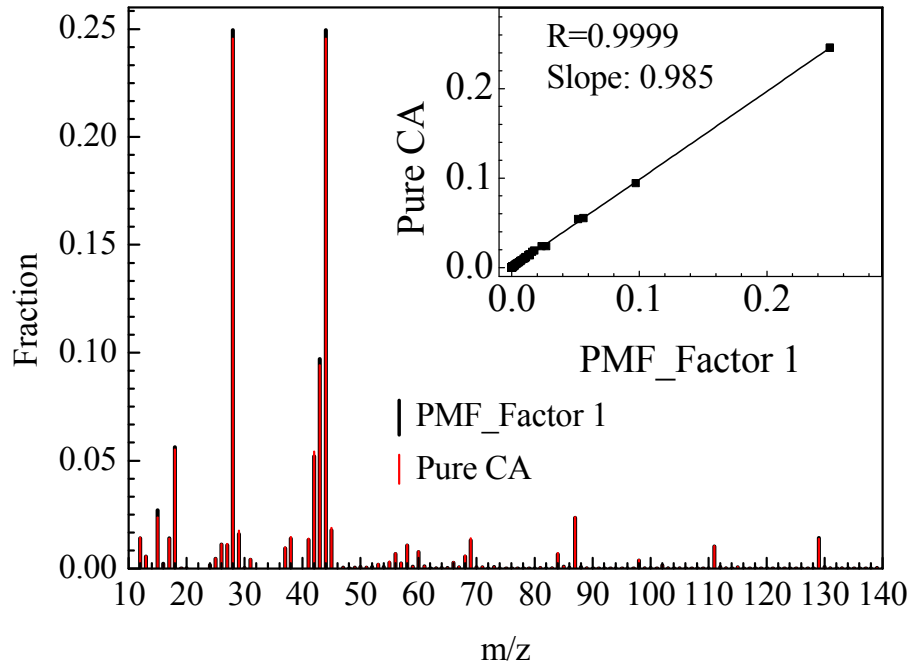
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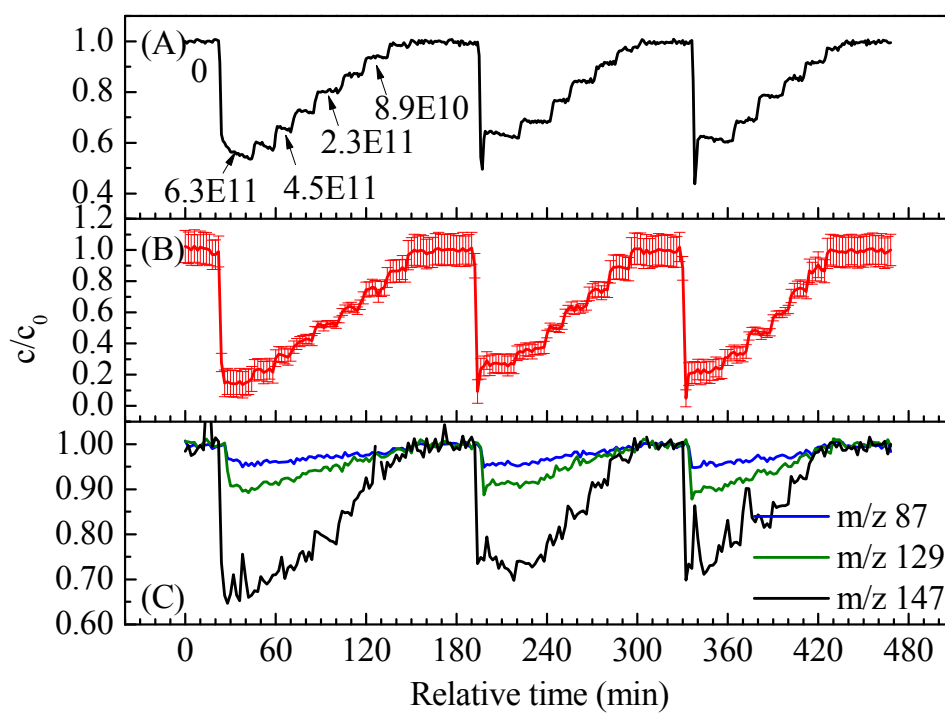
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**Figure 4.**



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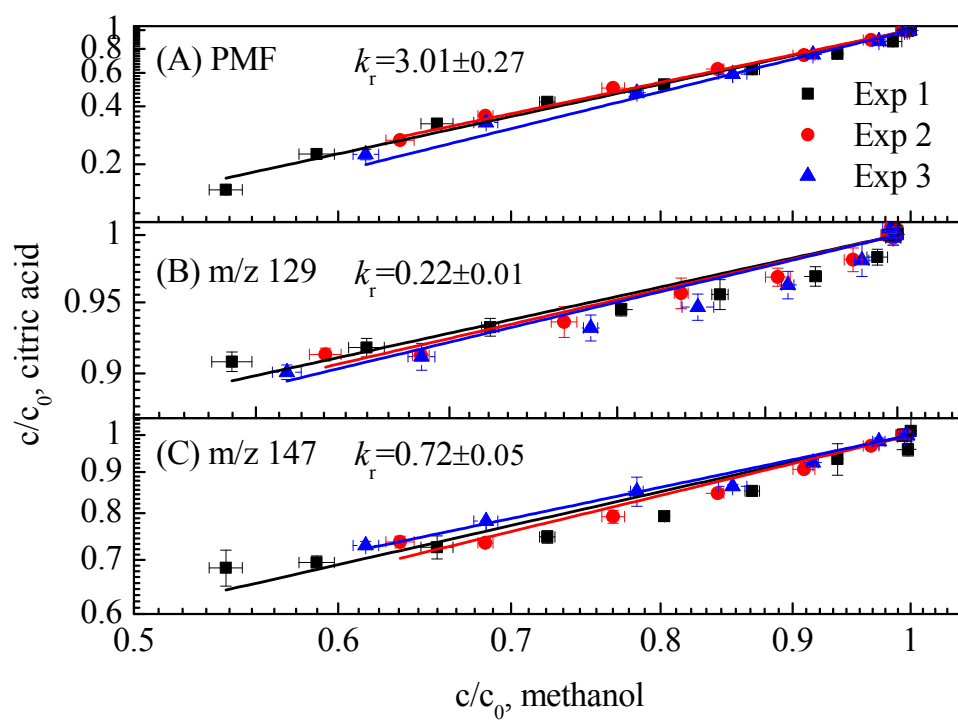
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**Figure 5.**



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**Figure 6.**