

1 CCN activation of fumed silica aerosols mixed with soluble 2 pollutants

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14 **Abstract:**

15 Particle-water interactions of completely soluble or insoluble particles are fairly well
16 understood but less is known of aerosols consisting of mixtures of soluble and insoluble
17 components. In this study, laboratory measurements were performed to investigate cloud
18 condensation nuclei (CCN) activity of silica particles mixed with ammonium sulphate (a salt),
19 sucrose (a sugar) and bovine serum albumin known as BSA (a protein). The agglomerated
20 structure of the silica particles was investigated using measurements with a Differential
21 Mobility Analyzer (DMA) and an Aerosol Particle Mass Analyzer (APM). Based on these data,
22 the particles were assumed to be compact agglomerates when studying their CCN activation
23 capabilities. Furthermore, the critical supersaturations of particles consisting of pure and mixed
24 soluble and insoluble compounds were explored using existing theoretical frameworks. These
25 results showed that the CCN activation of single component particles was in good agreement
26 with Köhler and adsorption theory based models when the agglomerated structure was
27 accounted for. For mixed particles the CCN activation was governed by the soluble
28 components, and the soluble fraction varied considerably with particle size for our wet-
29 generated aerosols. Our results confirm the hypothesis that knowing the soluble fraction is the
30 key parameter needed for describing the CCN activation of mixed aerosols, and highlight the

31 importance of controlled coating techniques for acquiring a detailed understanding of the CCN
32 activation of atmospheric insoluble particles mixed with soluble pollutants.

33

34 **Keywords:** Silica, CCN activation, Mixture aerosols

35 **1 Introduction**

36 The atmosphere of the Earth is composed of gases and suspended liquid and solid aerosol
37 particles of different size, shape, and chemical composition. Atmospheric aerosols have several
38 important impacts on the environment. First, at high concentrations in urban areas, they are a
39 health hazard to the respiratory system causing millions of premature deaths every year
40 (Mackay and Mensah, 2004; Pope and Dockery, 2006; Pope et al., 2009). Second, they scatter
41 and absorb solar and thermal radiation and thereby directly influence the heat balance of the
42 Earth and thus the climate (McCormick and Ludwig, 1976; Haywood and Boucher, 2000;
43 Ramanathan et al., 2001) Third, they act as cloud condensation nuclei (CCN) and ice nuclei
44 (IN). Hence, they alter the microphysical properties of clouds and thereby indirectly affect the
45 climate (Twomey, 1974; Albrecht, 1989; Lohmann and Feichter, 2005). Fourth, atmospheric
46 surface and condensed-phase chemistry can occur in the aerosol phase (Ravishankara, 1997;
47 Seinfeld and Pandis, 2006).

48 Aerosol-cloud interactions represent the largest uncertainty in predictions of the future
49 climate (IPCC, 2013). To reduce this uncertainty we need to improve our understanding of the
50 activation of aerosol particles to cloud droplets. In general, the ability of aerosol particles to act
51 as CCN depends on their composition, size and structure (Kumar et al., 2011a). Besides soluble
52 aerosol particles, insoluble particles like soot, mineral dust, and silica can act as CCN –
53 particularly if they are coated with hygroscopic material (Kumar et al., 2009).

54 During atmospheric transport and aging, originally insoluble particles may acquire
55 soluble species like $(\text{NH}_4)_2\text{SO}_4$ (ammonium sulphate) on their surfaces (Levin et al., 1996). In
56 such cases, the threshold supersaturation of cloud droplet activation substantially decreases
57 when water adsorbs onto the slightly soluble particles giving rise to the process of adsorption
58 activation (Saathoff et al., 2003; Hings et al., 2008). Thus, the presence of soluble species on
59 insoluble particle surfaces can enhance water-particle interactions and CCN activity of the
60 particles. Several recent studies have focused on the CCN activation of insoluble and mixed
61 soluble-insoluble particles, leading to the development of new theoretical frameworks for
62 describing the relevant phenomena. The developed theories are often based on multilayer
63 adsorption models and account for the curvature effects of the particles. One of these theories
64 introduced by Sorjamaa and Laaksonen (2007) combined FHH (Frenkel, Halsey and Hill)
65 adsorption isotherms and traditional Köhler theory to describe the equilibrium growth of
66 insoluble particles. Sorjamaa and Laaksonen (2007) showed that adsorption could help wettable
67 insoluble compounds to activate in the atmosphere. Thereafter, Kumar et al. (2009) developed

68 a cloud droplet formation parameterization where the CCN constitute an external mixture of
69 soluble aerosol, that follows Köhler theory, and insoluble aerosol, that follows FHH adsorption
70 activation theory (FHH-AT). They tested the new parameterization by comparing it to a
71 numerical cloud model and found a good agreement between the parameterization and the
72 model. Later Kumar et al. (2011a) reported laboratory measurements of CCN activity and
73 droplet activation kinetics of aerosols dry generated from clays, calcite, quartz, silica and desert
74 soil samples. They used FHH adsorption activation theory for describing fresh dust CCN
75 activity and found that the adsorption activation theory describes fresh dust CCN activity better
76 than Köhler theory. Afterward, Kumar et al. (2011b) studied particle size distributions, CCN
77 activity, and droplet activation kinetics of wet generated aerosols from mineral particles and
78 introduced a new framework of CCN activation of dust containing a soluble salt fraction, based
79 on a combination of the traditional Köhler and FHH adsorption theories. Henning et al. (2010)
80 on the other hand, studied agglomerated soot particles coated with levoglucosan and ammonium
81 sulphate, and concluded that traditional Köhler theory was sufficient to describe the CCN
82 activation of these mixed particles – as long as the amount of soluble material in the particles
83 was known (see also Stratmann et al., 2010). Despite these pioneering studies, CCN activation
84 measurements of partly insoluble particles containing a soluble fraction are still scarce.

85 Combustion processes result in emissions of different types of anthropogenic
86 nanoparticles. Flame-made (fumed) silica (SiO_2) particles, mainly produced in flame reactors,
87 are among these kind of particle types (Scheckman et al., 2009). Recently, fumed silica particles
88 have been taken into consideration due to their industrial importance (Scheckman et al., 2009;
89 Keskinen et al., 2011). In this study we use fumed silica particles as an experimental model to
90 investigate the CCN activation of the insoluble and partly soluble particles and the applicability
91 of the current theoretical frameworks developed to describe this phenomenon. Furthermore,
92 since the presented theories generally assume that the insoluble particles are spherical, the
93 agglomerated structure of the silica particles could cause uncertainties in the CCN activation
94 parameterizations. Taking into account the shape characterization of aggregated silica particles
95 may overcome these uncertainties. Different studies have recently focused on parameterizing
96 the structure of aggregated particles, especially silica agglomerates (Fuchs, 1964; DeCarlo et
97 al., 2004; Virtanen et al., 2004; Biskos et al., 2006; Scheckman et al., 2009).

98 The main aims of this study are: 1) measuring the CCN activity of pure and mixed
99 soluble-insoluble particles, 2) analysing and comparing the experimental results with
100 theoretical calculations using the existing frameworks and 3) connecting the mass analysis and

101 shape characterization of agglomerated silica particles to the existing theoretical frameworks to
102 gain a better understanding of the structure effects of these particles. Laboratory measurements
103 on the particle size distribution, mass, morphology and CCN activation of insoluble fumed
104 silica mixed with different amounts of soluble materials have been conducted. Furthermore, the
105 experimental CCN activity results are compared to theoretical calculations using the framework
106 introduced by Kumar et al. (2011b), and the distribution of soluble material on wet-generated
107 particle populations was discussed.

108

109 **2 Experimental setup**

110 Pure soluble or insoluble and mixed soluble-insoluble particles were generated and analysed in
111 this study. The investigated mixed particles consisted of fumed silica (Degussa, Aerosil-90) as
112 the insoluble part and three different hygroscopic components as the soluble part. The first
113 hygroscopic component was ammonium sulphate which is a water-soluble inorganic salt with
114 high hygroscopicity (Table 1); the second one was sucrose which is a sugar, i.e. a water-soluble
115 organic; the third one was bovine serum albumin (BSA) which is a large water-soluble protein
116 with molecular dimensions of approximately $4 \times 4 \times 14$ nm (Sugio et al., 1999; Jeyachandran
117 et al., 2010) . The SiO_2 used in the experiments was hydrophilic fumed silica, with a specific
118 surface area of $90 \text{ m}^2/\text{g}$ and purity of $\geq 99.8\%$ from Evonik Industries. Ammonium sulphate
119 and BSA were purchased from Sigma-Aldrich, and sucrose was purchased from VWR
120 International BVBA. All chemicals had purities higher than 99%.

121 Figure 1 shows a schematic of the experimental setup used in this study. Pure silica and
122 pure soluble particles as well as mixed particles made of silica and soluble species were
123 produced using the atomization-drying method described in Keskinen et al. (2011). Particles
124 were generated by an aerosol generator (Model 3076, TSI Inc., USA) after dissolving materials
125 in de-ionized water (Model Maxima LS., USF Elga Ltd.) with the production resistivity $> 10 \text{ M}\Omega\text{-}$
126 cm and TOC concentration < 5 ppb. The solute content in the water suspension was 0.06 wt%.
127 For mixed particles, the ratios of soluble components to silica were 1:19, 1:9 and 1:3, implying
128 that the fractions of soluble species were expected to be 5%, 10% and 25% of total particulate
129 mass in the atomized solution. We use the term solution, despite the fact that the insoluble silica
130 particles were suspended in the water (instead of dissolved).

131 After the particles had been produced they were fed into a diffusion drier (Fig. 1)
132 consisting of a porous tube surrounded by silica gel (Rotronic AG, model HC2-C04), resulting

133 in a relative humidity (RH) below 5% and they were neutralized using a charge neutralizer.
134 Thereafter particle number size distributions were measured using a Scanning Mobility Particle
135 Sizer (SMPS). The SMPS system was composed of an electrostatic classifier, which included
136 a Differential Mobility Analyzer (DMA) (Model 3071; TSI, Inc.) to bin the particles according
137 to electrical mobility, and an ultrafine Condensation Particle Counter (CPC Model 3025; TSI,
138 Inc.) to count the size-binned particles exiting the DMA.

139 Simultaneously, size-resolved CCN activity of the generated particles was measured
140 using a CCN counter (CCNc; Droplet Measurement Technologies Inc.) (Roberts and Nenes,
141 2005) (Fig.1). Before entering the CCNc, particles were size classified by a DMA, of the same
142 model as the DMA used in the SMPS. The CCNc operates by supersaturating sample air to the
143 point where the CCN become detectable particles. Humidified sheath air ($454 \text{ cm}^3 \text{ min}^{-1}$)
144 surrounds the sample flow ($45.4 \text{ cm}^3 \text{ min}^{-1}$) in the CCN column to hold it in the centre of the
145 column in the region of maximum supersaturation. The ratio of the flows was around 1 part of
146 sample air to 10 parts of sheath air and the total flow rate was $500 \text{ cm}^3 \text{ min}^{-1}$. The
147 supersaturation in the column could be varied between 0.1% and 1.5%. The total number
148 concentration of the particles entering the CCNc was measured by a CPC (Model 3772; TSI,
149 Inc.) and the number of activated droplets was counted by an Optical Particle Counter (OPC)
150 over 20 size bins in the diameter range from 0.75 to $10 \mu\text{m}$.

151 The effect of the silica particle morphology on activation was investigated by measuring
152 the mass of size classified particles by Aerosol Particle Mass Analyzer (APM) (model APM-
153 3600; Kanomax Inc.) (Fig. 1) (McMurry et al., 2002; Park et al., 2003a and 2003b). The APM
154 provides a direct relationship between the applied voltage, rotation speed, and particle mass
155 (Liu et al., 2012). Therefore, by measuring the outlet number concentration of the APM
156 corresponding to different applied voltages of the instrument, it was possible to measure the
157 mass distribution of the size selected particles. For each APM voltage, the downstream number
158 concentration was measured by a CPC (Model 3772; TSI, Inc.) (Fig. 1). From the voltage
159 corresponding to the highest concentration the average particle mass was calculated using the
160 following equation (McMurry et al., 2002; Park et al., 2003b):

$$161 \quad m = \frac{qV}{r^2 \omega^2 \ln(r_2/r_1)} \quad (1)$$

162 where m is the particle mass, ω is the APM angular speed, V is the applied voltage, q is the
163 particle charge, and r_1 , r_2 and r are the inner, outer and rotating radius of the instrument,
164 respectively.

165

166 **3 Theoretical frameworks**

167 **3.1 Non-sphericity of particles**

168 Particle shape can affect the physical dimensions of the particle in terms of the surface available
169 for water vapour to adsorb onto, as well as for the effective curvature determining the Kelvin
170 effect (see e.g. Kumar et al., 2011a). In the case of highly non-spherical or porous particles the
171 conversion between the electrical mobility (the quantity measured with the SMPS system) and
172 the available surface area or particle volume and density is not straight-forward. As mentioned
173 above, we used measurements of particle mass for the pure silica agglomerates to complement
174 the information about the mobility of these particles.

175 Two parameters, the dynamic shape factor and fractal dimension have been widely used
176 to characterize non-sphericity of aerosol particles. Dynamic shape factor is defined as the ratio
177 of the drag force on the agglomerated particles to the drag force on the volume equivalent
178 spherical particles (χ' , volume-based shape factor) or to the drag force on the mass equivalent
179 spherical particles (χ , mass-based shape factor) (DeCarlo et al., 2004; Kelly and McMurry,
180 1992). The fractal dimension (D_f) is the coordination number in the aggregate and links
181 properties like surface area of a particle to the scale of the measurements (Hinds, 1999; Ibaseta
182 and Biscans, 2010). These parameters are applicable to quantify the morphology of
183 agglomerated particles.

184 The mass-based shape factor is defined as (Kelly and McMurry, 1992):

$$185 \chi = \frac{d_b}{d_{me}} \cdot \frac{C(d_{me})}{C(d_b)} \quad (2)$$

186 where d_b and d_{me} are mobility diameter and mass equivalent diameter, while $C(d_b)$ and
187 $C(d_{me})$ are the corresponding Cunningham slip correction factors. The slip correction factors
188 are given by (Kulkarni, et al., 2011):

$$189 C(d_i) = 1 + \frac{2\lambda}{d_i} \left(1.142 + 0.558 \exp \left(-0.999 \frac{d_i}{2\lambda} \right) \right) \quad (3)$$

190 where λ is the mean free path of the gas molecules and d_i corresponds to either of d_{me} or d_b .
191 The mass equivalent diameter (d_{me}) was calculated using the following equation (Kelly and
192 McMurry, 1992):

$$193 d_{me} = \left(\frac{6m}{\pi\rho_p} \right)^{1/3} \quad (4)$$

194 where ρ_p is the material density of the silica particle (see Table 1)

195 To calculate the volume and surface equivalent diameters (d_{ve} and d_{se}) of the silica
 196 particles, which will be required to estimate the CCN capability of these particles, in addition
 197 to the mobility and mass data, knowledge on the volume-based shape factor (χ') is also required
 198 (see DeCarlo et al., 2004 and Kumar et al. 2011a for details):

$$199 \quad \frac{d_{ve}}{C(d_{ve})} = \frac{d_b}{\chi \cdot C(d_b)} \quad (5)$$

$$200 \quad d_{se} = \frac{3\chi d_{ve} - d_b}{2} \quad (6)$$

201 In this regard two limiting assumptions can be made. The first one is to assume compact
 202 agglomerates with nearly spherical shape and internal voids. In this case the mobility and
 203 volume equivalent diameters are approximately equal ($\chi'=1$) and also equal to the surface
 204 equivalent diameter, but larger than the mass equivalent diameter, i.e. $d_b = d_{ve} = d_{se} > d_{me}$.
 205 The particle density is in this case lower than the pure silica material density, but equal to the
 206 effective density. The second assumption is to approximate the silica particles as chain-like
 207 agglomerates with no internal voids, for which mass and volume equivalent diameters are equal
 208 ($\chi = \chi'$), but smaller than surface equivalent and mobility diameters, i.e. $d_{ve} = d_{me} < d_{se}$ and
 209 d_b . In this case the particle density would be the same as the pure silica material density but
 210 higher than the effective density.

211 The fractal dimension (D_f) of the silica particles provides further insight on their
 212 sphericity (Boldridge, 2010; DeCarlo et al., 2004; Keskinen et al., 2011): for perfect spheres
 213 $D_f=3$ and for line-like structures $D_f = 1$.

214 The fractal dimension of the pure silica particles was determined using the scaling law
 215 for effective density versus mobility diameter (Skillas et al., 1998, 1999):

$$216 \quad \rho_e \propto d_b^{(D_f-3)} \quad (7)$$

217 where ρ_e is the particle effective density. ρ_e was estimated using the following equation
 218 (Virtanen et al., 2004):

$$219 \quad \rho_e = m / (\pi d_b^3 / 6) \quad (8)$$

220 where m is the mass of the particles determined using APM (Eq. 1).

221

222

223

224

225 3.2 CCN activation of soluble particles

226 κ -Köhler theory (Petters and Kreidenweis, 2007) was used to estimate the critical
227 supersaturation of pure ammonium sulphate, sucrose and BSA particles. The saturation ratio
228 (S) is expressed as:

$$229 \quad S = \frac{d_p^3 - d_{dry}^3}{d_p^3 - d_{dry}^3(1-\kappa)} \exp\left(\frac{4\sigma_w M_w}{RT\rho_w d_p}\right) \quad (9)$$

230 where σ_w is the water surface tension, ρ_w is the water density, M_w is the molar mass of water, R
231 is the universal gas constant, T is the temperature, d_{dry} is the dry particle diameter, d_p is the
232 droplet diameter and κ is the hygroscopicity parameter of soluble particles.

233 The supersaturation (s) is equal to $(S-1)$ and is expressed as a percentage. The maximum
234 value of the supersaturation is called critical supersaturation (s_c) – similar definition naturally
235 holding for critical saturation ratio S_c as well. Thus, at the critical point:

$$236 \quad \left. \frac{ds}{dd_p} \right|_{d_p=d_c} = 0 \quad (10)$$

237 where d_c is called the critical diameter. The κ values for pure soluble particles were extracted
238 from previous studies or, in the case of BSA, derived by applying the following relation
239 introduced by Petters and Kreidenweis (2007) to our observations of the critical
240 supersaturations of the pure soluble particles:

$$241 \quad \kappa = \frac{4A^3}{27d_{dry} \ln^2 S_c} \quad (11)$$

242 where S_c is the saturation ratio at the critical point, $A = \frac{4\sigma_w M_w}{RT\rho_w}$, $\sigma = 0.072 \text{ J/m}^2$, $T = 298.15 \text{ K}$, M_w
243 $= 0.018 \text{ kg/mol}$ and $\rho_w = 1000 \text{ kg/m}^3$.

244 The pure soluble particles were assumed to be compact and spherical, and thus the
245 mobility diameter was used as the d_{dry} in Eqs. 9-11.

246

247 3.3 CCN activation of insoluble silica

248 The critical supersaturation of pure silica particles was calculated using FHH adsorption theory
249 (Sorjamaa and Laaksonen, 2007, Kumar et al., 2009 and Kumar et al., 2011a). In this case the
250 relationship between water supersaturation s and particle size can be expressed as:

$$251 \quad s = \frac{4\sigma_w M_w}{RT\rho_w d_p} - A_{FHH} \left(\frac{d_p - d_{dry}}{2d_{H_2O}} \right)^{-B_{FHH}} \quad (12)$$

252 where d_{H_2O} ($= 2.75 \text{ \AA}$) is the diameter of the water molecule, and A_{FHH} and B_{FHH} are the FHH
 253 adsorption isotherm parameters. The first and second terms on the right hand side of Eq. 12
 254 correspond to the contributions from the Kelvin and adsorption effects, respectively.

255 In the literature, different values of the parameters A_{FHH} and B_{FHH} for silica particles have
 256 been reported. Kumar et al. (2011a) obtained the values 2.95 and 1.36 for A_{FHH} and B_{FHH} of
 257 quartz silica, respectively, and Keskinen et al. (2011) assigned values of 4.82 and 2.16 for A
 258 and B for non-agglomerated fumed silica particles (Degussa, Aerosil-300) with the diameter of
 259 8 and 10 nm.

260 To yield a reasonable estimate of the surface available for adsorption, the surface
 261 equivalent diameter of the pure silica particles was used as d_{dry} in Eq. 12.

262

263 3.4 CCN activation of mixed soluble and insoluble particles

264 Kumar et al. (2011b) used adsorption activation theory assuming that the particles are spheres
 265 and presented a model describing mixed particles with an insoluble and a soluble fraction. They
 266 introduced the following relation between water supersaturation, particle size and composition:

$$267 \quad s = \frac{4\sigma_w M_w}{RT\rho_w d_p} - \frac{\varepsilon_s d_{dry}^3 \kappa}{(d_p^3 - \varepsilon_i d_{dry}^3)} - A_{FHH} \left(\frac{d_p - \varepsilon_i^{1/3} d_{dry}}{2d_{H_2O}} \right)^{-B_{FHH}} \quad (13)$$

268 where ε_i and $\varepsilon_s = 1 - \varepsilon_i$ are the insoluble and soluble volume fractions in the dry particles and κ
 269 is the hygroscopicity parameter of the soluble part. A_{FHH} and B_{FHH} are the FHH adsorption
 270 isotherm parameters of the insoluble part, which is assumed to interact with the water through
 271 adsorption onto its surface.

272 To estimate the average insoluble volume fractions of the mixed particles, the following
 273 relation was used:

$$274 \quad \varepsilon_i = \frac{m_i/\rho_i}{m_i/\rho_i + m_s/\rho_s} \quad (14)$$

275 where m_i and m_s are the insoluble and soluble mass fractions in the total mixed aerosol
 276 population, and ρ_i and ρ_s are the densities of the insoluble and soluble parts, respectively. The
 277 bulk densities of the used components are listed in Table 1.

278 In the second term of Eq. 13 the volume equivalent diameter was used as d_{dry} , while the
 279 surface equivalent diameter was assumed to represent the d_{dry} in the last term.

280

281 **4 Results and discussion**

282 **4.1 Particle size distributions**

283 The SMPS measurements yielded the average number size distributions for silica particles
284 mixed with $(\text{NH}_4)_2\text{SO}_4$, sucrose and BSA (Fig. 2). Figure 2a displays average number size
285 distributions for particles made of pure fumed silica, pure $(\text{NH}_4)_2\text{SO}_4$ and particles made of
286 silica and different amounts of $(\text{NH}_4)_2\text{SO}_4$. As is evident in the figure, size distributions of
287 particles generated from pure silica or pure $(\text{NH}_4)_2\text{SO}_4$ are unimodal while size distributions of
288 particles generated from the silica- $(\text{NH}_4)_2\text{SO}_4$ mixtures are bimodal. The mean mobility
289 diameter is ~ 30 nm for the pure $(\text{NH}_4)_2\text{SO}_4$ particles, and approximately 150 nm for the pure
290 silica particles. The first mode of the bimodal size distributions, associated with particles
291 generated from the aqueous bulk mixtures, is centered at a diameter of less than 30 nm. The
292 second mode, with lower number concentration, is centered at approximately 150 nm. Fig. 2b
293 shows the average number size distributions of particles made of sucrose and silica. Particles
294 made of pure sucrose have a mean diameter of approximately 50 nm. Size distributions
295 associated with particles generated from the silica-sucrose mixtures are bimodal (Fig. 2b); the
296 first mode centered at a diameter of less than 50 nm and the second mode centered at a diameter
297 of about 150 nm. Similarly, Fig. 2c shows the average SMPS number size distributions of
298 particles made of silica and BSA. These data are comparable with previous two measurements
299 in Figs 2a-b. The particles made of the large BSA protein have a mean diameter of about 75
300 nm. The mode associated with particles made of a mixture of BSA and silica is centered at
301 about 150 nm.

302 In the case of mixed aerosols, the particles in the first mode of the bimodal size
303 distributions are likely pure soluble particles, while the second mode of the bimodal distribution
304 curves represents silica particles mixed with soluble species. Hence, when analysing the
305 activation behaviour of mixed particles we omitted the CCNc data of the smallest particles by
306 subtracting their contribution from the CCN numbers and restricted our analysis to particle sizes
307 larger than 100 nm.

308 To estimate the average soluble volume (mass) fractions in the mixed particles, we
309 calculated the fraction of soluble material lost to the first pure mode of the particle size
310 distributions and subtracted it from the total soluble mass. In this regard, we fitted log-normal
311 distribution curves to the number size distributions associated with particles from the mixtures
312 and estimated the volume and mass distributions related to each particle number size

313 distribution. Hereupon, it was possible to estimate the fraction of total soluble mass remaining
314 in the first mode of the bimodal size distributions for each mixture, and the fraction of the total
315 soluble mass which was mixed with silica (Table 2). By multiplying this fraction with the
316 soluble mass fraction in the bulk mixture we gained an estimate of the real average soluble mass
317 fraction in the mixed/coated particles excluding the portion of the pure soluble particles. As is
318 evident from Table 2, the overall mass losses of the soluble material from the first mode are
319 small, and 87-100% of the total soluble masses were mixed with silica particles.

320

321 **4.2 Mass analysis and size characterization of pure and mixed silica particles**

322 Since fumed silica particles are agglomerates, mass analysis of the pure silica particles could
323 help us to get a better understanding of their shape (see Sect. 3.1). As an example, Figure 3a
324 shows the observed average number concentrations of 100 nm size-selected silica particles (by
325 DMA) for different APM voltages. A log-normal distribution was fitted to provide the voltage
326 value corresponding to the peak of the distribution. After determining the mass of size selected
327 particles using Eq. 1, the effective density of the silica particles was estimated (Eq. 3). The
328 APM measurements were performed for two different rotation speeds of the APM (3000 and
329 5000 rpm). The achieved effective particle densities using these two rotation speeds are
330 presented in Fig. 3b. There is only a small difference in effective density between the two
331 different speeds, giving confidence in the results. Figure 3c displays the mass-based shape
332 factor (χ) of silica particles for different mobility diameters. χ is clearly larger than 1 and
333 increases by increasing mobility diameter. This indicates that internal voids and/or irregularities
334 of the particles increase with increasing particle diameter (Kelly and McMurry, 1992).

335 The fractal dimension of the silica particles was estimated using the slopes of the curves
336 in Fig. 3b and Eq. 6 yielding D_f values of 2.54 and 2.55 for the 3000 and 5000 rpm rotation
337 speeds, thus suggesting closer to spherical rather than rod- or chain-like structures. The fitted
338 D_f values are also close to the value ($D_f=2.57$) reported by Keskinen et al. (2011) and Ibaseta
339 and Biscans (2010) ($D_f=2$ to 2.5) for fumed silica (Degussa, Aerosil-300 and -200,
340 respectively). We therefore expect the silica particles to be better represented by the “compact
341 agglomerates” assumption and applying this assumption ($\chi'=1$, see Sect. 3.1), the volume and
342 surface equivalent diameters used in all the CCN activity calculations were thus approximated
343 with the mobility diameters.

344 The mass analysis results were only available for the pure silica particles. When analysing
345 the CCN activation data for the mixed particles, we assumed that the effective density of the
346 silica in the mixed particles was similar to the effective density of the pure silica particles. The
347 physical meaning of this assumption would be that the silica present in the mixed particles
348 would contain the same volume of voids per unit silica mass as the pure particles. Furthermore,
349 when calculating the critical supersaturations using Eq. 13 the adsorption term was calculated
350 using the surface equivalent diameter d_{se} as d_{dry} and the solubility term using the volume
351 equivalent diameter d_{ve} as d_{dry} , which in our case, by compact agglomerates assumption d_{ve}
352 $= d_{se} = d_b$.

353

354 **4.3 CCN activation results**

355 Before analysing the CCN activity of the generated particles, all the activation curves were
356 charge-corrected using the procedure introduced by Moore et al. (2010). The ratio of the
357 corrected CCN and CN (Condensation Nuclei, measured by CPC) time series thus determines
358 the activated fraction (also referred to as activation ratio) of the specified particles (Kumar et
359 al., 2011a). Furthermore, as described in Sec. 4.3.2, for the mixed particles the contributions of
360 the smaller completely soluble particle mode (see Fig. 2) were subtracted from the CCN
361 concentrations. Finally all the activation curves used in the further analysis were normalized
362 using a correction factor derived from the ammonium sulphate (AS) experiments, assuming that
363 AS activation probability reaches unity at high supersaturations. In the cases where the
364 normalization with the AS data would have produced CCN/CN values larger than unity, the
365 value was set to unity instead.

366

367 **4.3.1 CCN behavior of pure components**

368 Figure 4 shows the activation ratio dependence on supersaturation for 120 nm (mobility
369 diameter) pure silica, BSA, sucrose and ammonium sulphate particles. A sigmoid curve was
370 fitted to each set of activation ratio data. Critical supersaturation (s_c) is often associated with
371 the supersaturation where 50% of the particles are CCN activated – equivalent to a CCN/CN-
372 ratio of 50%, and we will follow this convention although the two are not necessarily equal
373 when the CCN/CN curve is not a step function. As expected, $(\text{NH}_4)_2\text{SO}_4$ particles, which are
374 the most hygroscopic particles investigated in this study (see κ values in Table 1), activated at
375 lower supersaturations than was the case for sucrose, silica and BSA particles. The pure silica

376 particles, which are insoluble and non-hygroscopic, exhibited the highest critical
377 supersaturation of the investigated compounds (Fig. 4).

378 Figure 5 displays activation ratio against supersaturation for pure silica particles of
379 different mobility diameters. As is evident from Fig. 5, the critical supersaturation decreases
380 with increasing particle diameter. Experimentally and theoretically determined critical
381 supersaturations of pure silica particles as a function of particle mobility diameter are shown in
382 Fig. 6. Previously, the values for FHH adsorption parameters (Eqs. 10 and 12) of different
383 types of silica have been determined by Kumar et al. (2011a) (quartz), and Keskinen et al.
384 (2011) (Fumed silica, Aerosil-300). To compare our results to these studies, we fitted the FHH
385 adsorption parameters for the pure silica particles (Fumed silica, Aerosil-90). A_{FHH} and B_{FHH}
386 values of 2.50 and 1.62 explain our results on the activation diameter vs. critical supersaturation
387 (Fig. 6), although the fits were difficult to constrain uniquely. Our results are closer to those
388 reported by Keskinen et al. (2011) than Kumar et al. (2011a), but the A_{FHH} and B_{FHH} values are
389 close to those reported by Kumar et al. (2011a). This highlights the sensitivity of the fits to
390 adsorption parameters, reflecting the fact that our data set is not sufficient for constraining any
391 physical or chemical phenomena behind these values. In particular, the parameter A_{FHH} ,
392 describing the interactions of the first monolayer with the adsorbent surface, seems to be
393 difficult to constrain based on the CCN activation data. This is perhaps not surprising as at the
394 point of activation the rapid condensation of water might relatively soon destroy the information
395 of the very first steps of the adsorption / monolayer formation. For the parameter B_{FHH} , on the
396 other hand, the fits seem to reproduce relatively robust values. CCN activation measurements
397 are probably not the best approach for yielding accurate data of the physical phenomena behind
398 the adsorption parameters – as a lot of information has already been lost at the point where the
399 CCN are activated and detected – but should be rather regarded as a valuable source of
400 information on the processes limiting atmospheric cloud droplet formation. It should also be
401 pointed out that the quartz silica (Kumar et al., 2011a) is not as hydrophilic as fumed silica
402 which probably affects the critical supersaturation. Furthermore, the FHH adsorption
403 parameters in Keskinen et al. (2011) study were fitted for only 8 and 10 nm fumed silica
404 particles which were most likely spherical and thus potentially not fully representative of the
405 agglomerated particles that we used. Impurity of the silica could also affect the results even
406 though the deionized water was used in all studies. To conclude, the experimental results for s_c
407 of pure silica particles were in good agreement with theoretical calculations using FHH
408 adsorption isotherm and small deviations were only observed for larger diameters.

409 To estimate the critical supersaturations of pure soluble particles, κ -Köhler theory (Eqs.
410 9 and 10) was applied. Table 1 lists κ values of the soluble materials used in this study. The
411 ability for ammonium sulphate particles to act as CCN has been widely studied (e.g. Garland,
412 1969; Kreidenweis et al., 2005; Hiranuma et al., 2011), and here we employed the previously-
413 reported hygroscopicity (κ) values (Petters and Kreidenweis, 2007), given the relatively good
414 agreement between the κ value fitted to our results (0.78) and the literature values. The κ value
415 for pure sucrose was extracted from Ruehl et al. (2010), which was also in reasonable agreement
416 with the value 0.08 that best described our results. For the pure BSA particles κ was calculated
417 based on Eq. 11 using the CCN activation results of pure BSA particles in this study. The
418 experimentally and theoretically determined critical supersaturations for pure $(\text{NH}_4)_2\text{SO}_4$, BSA
419 and sucrose particles are shown in Fig. 7. Indeed, κ -Köhler theory results using the literature
420 values for the hygroscopicity parameter were in good agreement with the experimentally
421 determined critical supersaturations of pure soluble particles.

422

423 **4.3.2 CCN behavior of the mixtures**

424 Here we present the CCN activation results of co-synthesized silica particles mixed with
425 $(\text{NH}_4)_2\text{SO}_4$, sucrose or BSA considering the determined total soluble fractions in the mixed
426 particle population from Table 2.

427 The activation ratio curves were determined for different diameters of mixed particles
428 and different ratios of soluble to insoluble materials. For mixed particles the activation ratio
429 curves were modified by subtracting the contributions of the smaller completely soluble particle
430 from the CCN and CN concentrations using the following procedure: First, the contribution of
431 pure soluble particles to the total number of CN for each size were estimated by fitting two log-
432 normal modes to the size distributions such as those shown in Fig. 2. The pure soluble mode
433 was then subtracted from the CN data for each size to yield an estimate of the total numbers of
434 mixed CN. Second, using the CCN/CN ratios of the pure soluble particles (shown for 120 nm
435 in Fig. 4) we could estimate the number of CCN originating from pure CN at each mobility
436 diameter and supersaturation. Subtracting this from the total number of CCN, we could yield
437 an estimate for the CCN/CN ratio for the mixed particles. Figure 8 represents the activation
438 ratio curves for 150 nm (mobility diameter) pure and mixed particles. Although both the raw
439 data (unnormalized) and the normalized curves are shown for completeness, only the

440 normalized data was used in the follow-up analysis. It can be seen that the normalization
441 procedure caused only very small adjustments to the 50% points inferred from the curves.

442 Figure 8a shows the activation probabilities of mixed silica-(NH₄)₂SO₄ particles. The
443 critical supersaturation (corresponding to CCN/CN=50%) is higher for pure silica particles than
444 for the particles with soluble material. Evidently, the pure (NH₄)₂SO₄ particles have the lowest
445 critical supersaturation. Furthermore, the critical supersaturation decreases when the fraction of
446 soluble material in the particles increases, and the CCN/CN curves are shallower (i.e. further
447 from a step function) for the mixed as compared with the pure particles. The same behavior can
448 be observed in Fig. 8b for 150 nm silica particles mixed with sucrose. Pure sucrose particles
449 were activated at a supersaturation of 0.22% which is comparable to previous studies (e.g.
450 Rosenorn et al., 2006). s_c decreases with increasing sucrose ratio in the mixed particles, similar
451 to what was observed for ammonium sulphate in Fig. 8a. In the case of particles containing
452 BSA, however, a different behavior was observed: s_c was higher for particles made of 5% and
453 10% BSA than for particles made of pure silica (Fig. 8c). The reason for this behavior is not
454 clear but it is known that adsorption of BSA on silica can affect the structural properties of
455 BSA. As was explained by Larsericsdotter et al. (2005), for soft proteins such as BSA the
456 structural stability decreases when adsorption onto other materials occurs. On the other hand,
457 the BSA can also affect the agglomerate structure of the mixed particles – for instance through
458 more compact agglomerates with increasing BSA concentrations (see e.g. Kiselev et al., 2010
459 and Stratmann et al., 2010 for discussion on effects of coating on agglomerate compactness).
460 However, it is also possible that this effect is solely due to different distribution of the soluble
461 materials as a function of particle size for the different bulk solution compositions, which is
462 discussed in detail below.

463 To estimate the soluble mass fractions (ω_s) in the coated/mixed particles required for the
464 application of Eq. 13, the total amount of soluble material was first estimated by fitting log-
465 normal size distributions to the observed size distributions (Sect. 4.1). The dashed lines in Fig.
466 9 show the theoretical critical supersaturations (using Eq. 13) of particles consisting of a
467 mixture of silica and ammonium sulphate assuming soluble volume fractions (ε_s) corresponding
468 to these constant ω_s (see Table 2 and the dashed lines of the inset in
469 Fig. 9) with changing diameter. These theoretical values of critical supersaturations are mostly
470 lower than the observed critical supersaturations (stars), and the size-dependence of the critical
471 supersaturation is not captured by the theory. We observed the same (although less pronounced)
472 behavior for silica particles mixed with sucrose and BSA (Figs. 10 and 11). In all three cases,

473 the observed critical supersaturations were higher than expected from the model by Kumar et
474 al. (2011b) using constant soluble mass fractions. The calculations are very sensitive to the κ
475 values and the deviation between experimental and estimated s_c for mixed particles increases
476 with increasing hygroscopicity. The largest deviations were observed for particles mixed with
477 $(\text{NH}_4)_2\text{SO}_4$, which is more hygroscopic ($\kappa=0.61$) than the other compounds, and the smallest
478 deviations were observed for silica particles mixed with BSA which has the lowest
479 hygroscopicity ($\kappa=0.01$). The adsorption term contribution to the critical supersaturation in Eq.
480 13 was generally minor: $<0.72\%$ for silica + $(\text{NH}_4)_2\text{SO}_4$, $<3.8\%$ for silica + sucrose and $<7\%$
481 for silica + BSA of the total (Kelvin + solubility + adsorption) contribution for all the studied
482 compositions and supersaturations. The theoretical predictions were thus dominated by the
483 Kelvin and solubility effects – similarly to the case of soot agglomerates studied by Henning et
484 al (2010).

485 The small contribution of the adsorption term to the theoretical predictions combined with
486 the shallow activation ratio curves (see Fig. 8) suggest that the reason for the apparent
487 discrepancy between the theoretical and the observed critical supersaturations is a non-constant
488 distribution of the soluble material with varying particle size. This explanation seems
489 particularly feasible taking into account the good agreement between the experiments and
490 theory for the pure particles, and the fact that the particle generation method (atomization and
491 drying of aqueous solutions) does not allow for controlling the ratio of soluble to insoluble
492 materials at a given particle size – only for the overall aerosol population. To yield further
493 insight into this, we estimated the distribution of the soluble material by fitting size-dependent
494 ε_s distributions to the CCN/CN vs. s_c curves (e.g. Fig. 8) using Eq. 13 – thus assuming that all
495 the mixed particles that activate at a given supersaturation interval contain a specific soluble
496 volume (mass) fraction. It is worthwhile to note that the ε_s determined this way correspond to
497 the surface or volume equivalent diameters (linked to the particle mass through the modified
498 silica density including internal voids, see Sect. 3), and is thus not directly comparable to the
499 mass fractions in the atomized solution.

500 The s_c (defined as the 50% point in the CCN/CN curves) vs. mobility diameter results
501 obtained through the fitting procedure are shown by the solid lines in Figs. 9-11, and the
502 resulting soluble mass fractions ω_s corresponding to the ε_s fitted to the 50% points in the
503 CCN/CN curves as a function of particle size are shown as the solid lines in the insets. The
504 results suggest a very uneven distribution of the soluble material as a function of particle size:
505 the small particles contain considerably higher fractions of soluble material than the larger ones,

506 and the effect increases with the amount of soluble material. In the case of BSA (Fig. 11), the
507 different mixture compositions lie relatively close to each other in terms of their critical
508 supersaturations – making it difficult to constrain the soluble contents of these particles.
509 However, it seems clear that at the small particle sizes (< 150 nm) the particle population is
510 dominated by pure BSA particles. At sizes between 150 and 250 nm, on the other hand,
511 extremely low BSA-content is required to reproduce the observed critical supersaturations. This
512 is of course also visible in Fig. 8c, where the mixtures with low BSA-content seem to activate
513 at even higher supersaturations than pure silica. The exact reason for this is not clear, but the
514 effect of BSA on silica particle structure (e.g. density etc.) could be speculated upon.

515 While the size-dependent ω_s shown in Figs. 9-11 correspond to the points at which 50%
516 of the CN activate as CCN for a given particle diameter and supersaturation, the ω_s values vary
517 even for a given particle size – as indicated by non-step function shape of the activation curves
518 in Fig. 8. An example distribution of the soluble mass as deduced from the CCN/CN vs. s_c data
519 (Fig. 8) using Eq. 13 is shown in Fig. 12 for the 150 nm mobility diameter mixed particles. The
520 figure shows that for each mixture, there is an uneven distribution of soluble mass fraction in
521 the particles of a given size. In all cases, there is a large number of particles with very low
522 soluble mass fractions (less than initial bulk solution) and the composition of the size-selected
523 particles is not constant. Similar conclusions were drawn by Dusek et al. (2006) for soot
524 particles coated by NaCl. When compared to the mass fractions in the atomized solution, it can
525 be seen that only in the case of sucrose the distribution peaks at soluble mass fractions similar
526 to the original solution, while the mixtures containing ammonium sulphate and BSA have
527 widely varying compositions.

528

529 **5 Summary and conclusions**

530 In this study, the CCN activation of pure and mixed particles of silica and soluble compounds
531 (AS, sucrose and BSA) was investigated. Furthermore, the morphology and effective density
532 of silica particles were investigated based on APM measurements. In addition, size distributions
533 of the sampled particles were measured using a SMPS. Then non-sphericity of the particles was
534 investigated by applying APM measurements and estimating mass-based dynamic shape factors
535 and fractal dimensions of pure silica particles. Assuming that our pure and mixed silica particles
536 are compact agglomerates, which is the most reasonable assumption for our silica particles with
537 fractal dimension of 2.54-2.55 close to the spherical particles with fractal dimension of three,

538 the surface and volume equivalent diameters become identical to the mobility diameter of these
539 particles. The SMPS results showed that the particles generated from pure compounds resulted
540 in unimodal size distributions, while the particles generated from mixtures were associated with
541 bimodal size distributions. The first peak of the bimodal size distribution indicated that also the
542 mixture generated some pure soluble particles. The size distributions allowed us to estimate the
543 total soluble vs. insoluble mass fractions present in the mixed particle population.

544 CCN activity measurements were conducted in various supersaturations up to 1.5%, and
545 activation ratio curves were determined for the evaluated particles. Afterward, the experimental
546 data were compared to theoretical values using adsorption theory (e.g. Sorjamaa and
547 Laaksonen, 2007) for the pure silica particles, κ -Köhler-theory (Petters and Kreidenweis, 2007)
548 for the pure soluble particles, and a model describing mixtures of soluble and insoluble
549 components introduced by Kumar et al. (2011b). The CCN activation of pure soluble and
550 insoluble particles was in good agreement with κ -Köhler theory and adsorption theory. For
551 mixed particles, however, the observed critical supersaturations were higher than those
552 expected from the model by Kumar et al. (2011b), if constant soluble and insoluble mass
553 fractions were assumed for the whole mixed particle population. This indicates that the particles
554 were less hygroscopic than expected, indicating an uneven distribution of the soluble material
555 in the aerosol size distribution. As the calculations were governed by the soluble mass (volume)
556 fraction in the particles instead of adsorption effects, we could use the experimental critical
557 supersaturations to estimate size-dependent distribution of the soluble material in the mixed
558 particles. For particles > 150 nm in mobility diameter the soluble fractions were smaller and for
559 particles < 150 nm mostly larger than in the total mixed particle population – indicating that the
560 soluble material preferentially accumulated to particles < 150 nm, independent of the exact
561 identity of the soluble species. If the uneven distribution of the soluble material was accounted
562 for, the framework by Kumar et al. (2011b) could be successfully used to describe the CCN
563 activation of insoluble particles mixed with soluble pollutants.

564 Our results indicate that knowing the fraction of soluble material (instead of the
565 adsorption properties of the surfaces) is the key prerequisite for describing the CCN activation
566 of silica mixed with soluble pollutants – at least for the relatively large soluble fractions studied
567 here. Furthermore, our results indicate that well-defined descriptions of the coating processes
568 are crucial for elucidating the phenomena governing the CCN activation of insoluble particles
569 mixed with soluble compounds. We also conclude that although the model by Kumar et al.
570 (2011b) was originally introduced for fresh dust coated by a layer of soluble salt after ageing,

571 it gives a reasonable estimate of the potential importance of adsorption as compared with the
572 bulk solubility of the mixed soluble-insoluble particles.

573

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579

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735

736 Table 1: Thermodynamic properties of components used in this study.

	Molar mass (g/mol)	Density (g/cm³)	Solubility in water (Mass%)	κ
(NH₄)₂SO₄	132.14 ^a	1.77 ^a	43.3 ^a	0.61 ^e
Sucrose	342.3 ^a	1.58 ^a	67.1 ^a	0.084 ^f
BSA	66500 ^b	1.362 ^b	60 ^d	0.013 ^g
SiO₂	60.08 ^a	2.16 ^c	-	-

737 ^a Haynes et al. (2013)

738 ^b Mikhailov et al. (2004)

739 ^c Grayson (1985)

740 ^d Shiraiwa et al. (2011)

741 ^e Petters and Kreidenweis (2007)

742 ^f Ruehl et al. (2010)

743 ^g This work

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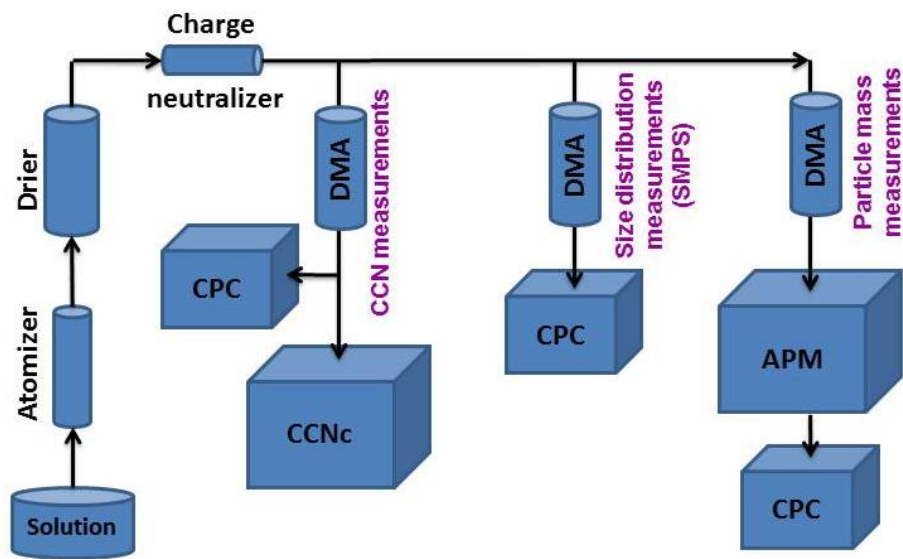
745 Table 2: The total soluble fraction of the solute masses in the bulk mixtures, the fraction of total
 746 soluble mass mixed with silica, the average soluble mass fraction of the mixed particles
 747 (calculated from particle size distributions, see text for details).

Soluble mass fraction in the bulk mixture (%)	Fraction of total soluble mass mixed with silica (%)			Total soluble mass fraction in the mixed particles (%)		
	Silica+ (NH ₄) ₂ SO ₄	Silica+ sucrose	Silica+ BSA	Silica+ (NH ₄) ₂ SO ₄	Silica+ sucrose	Silica+ BSA
25	92	98	87	23.4	24.6	22.5
10	88	99	99	8.9	9.9	9.9
5	87	99	~100	4.4	4.9	~5

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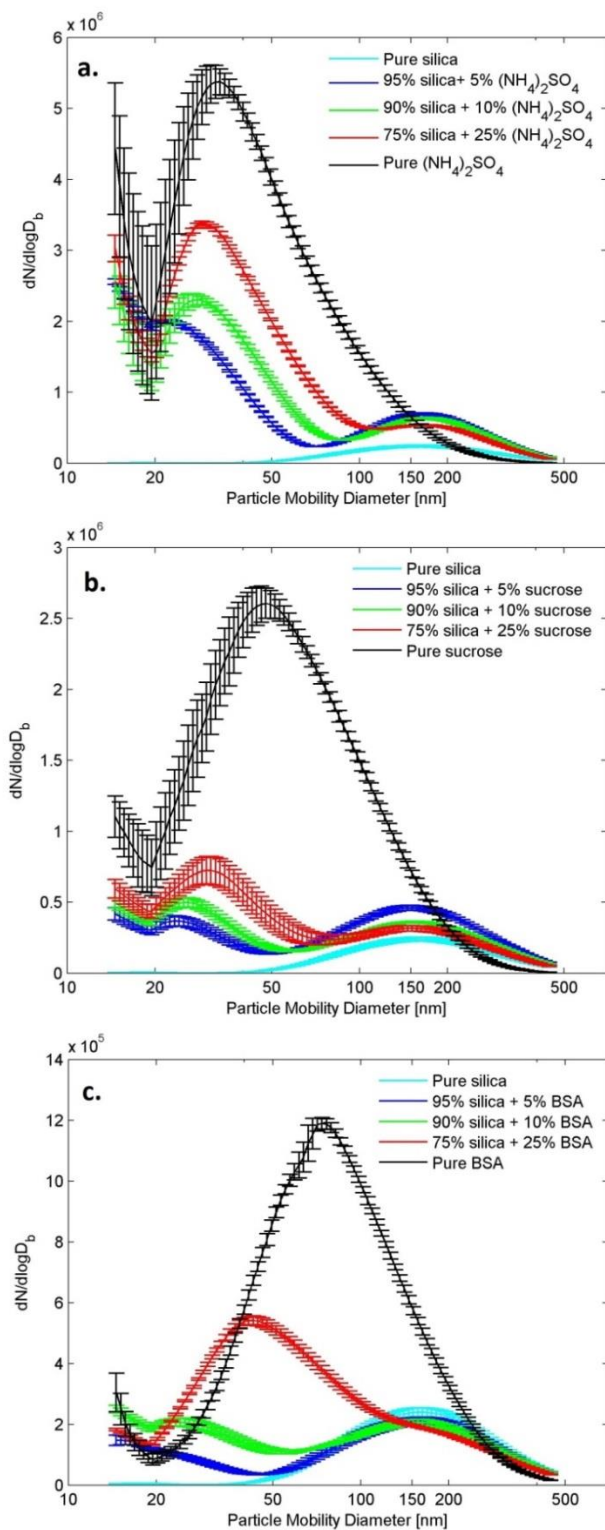
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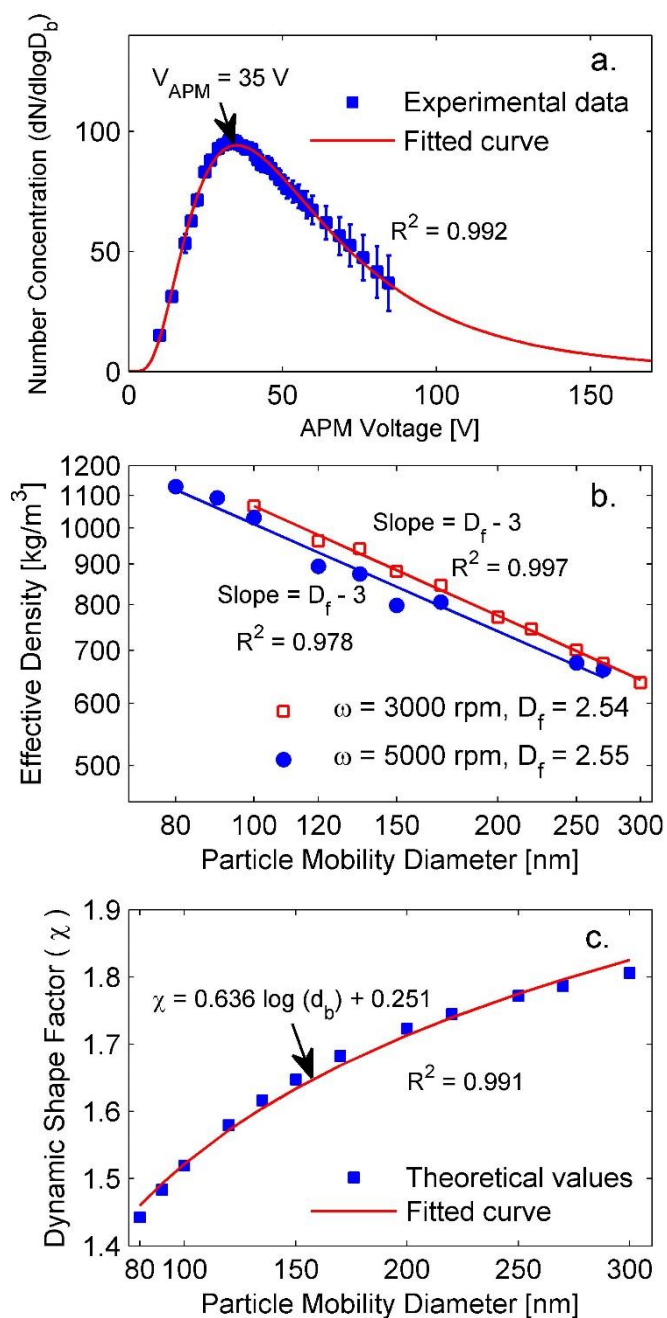
752 Fig. 1: Schematic of the experimental set up and three types of measurements: CCN activity
753 measurements, size distribution measurements by SMPS and particle mass analyzing by APM.

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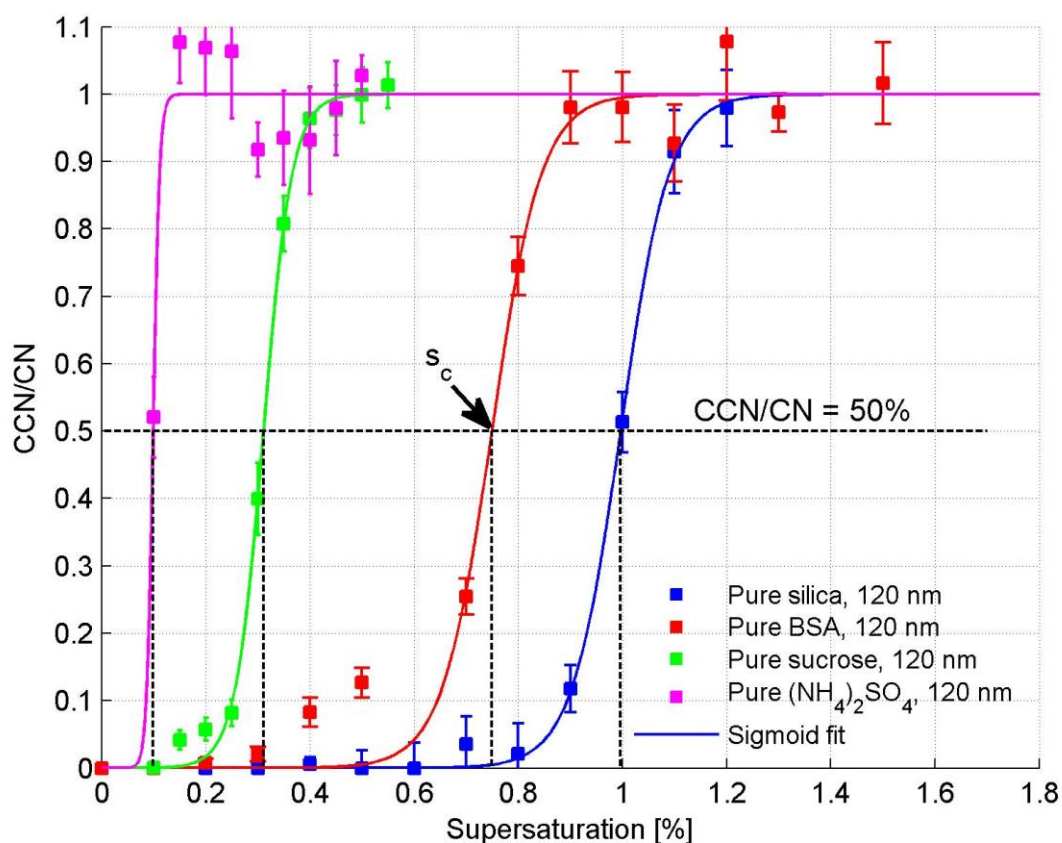
755

756 Fig. 2: Average particle number size distributions (SMPS) for silica particles mixed with **(a)**
 757 $(\text{NH}_4)_2\text{SO}_4$, **(b)** sucrose and **(c)** BSA. Each average size distribution is based on at least 70
 758 individual size distributions, and the error bars represent the standard deviation of the
 759 measurements.



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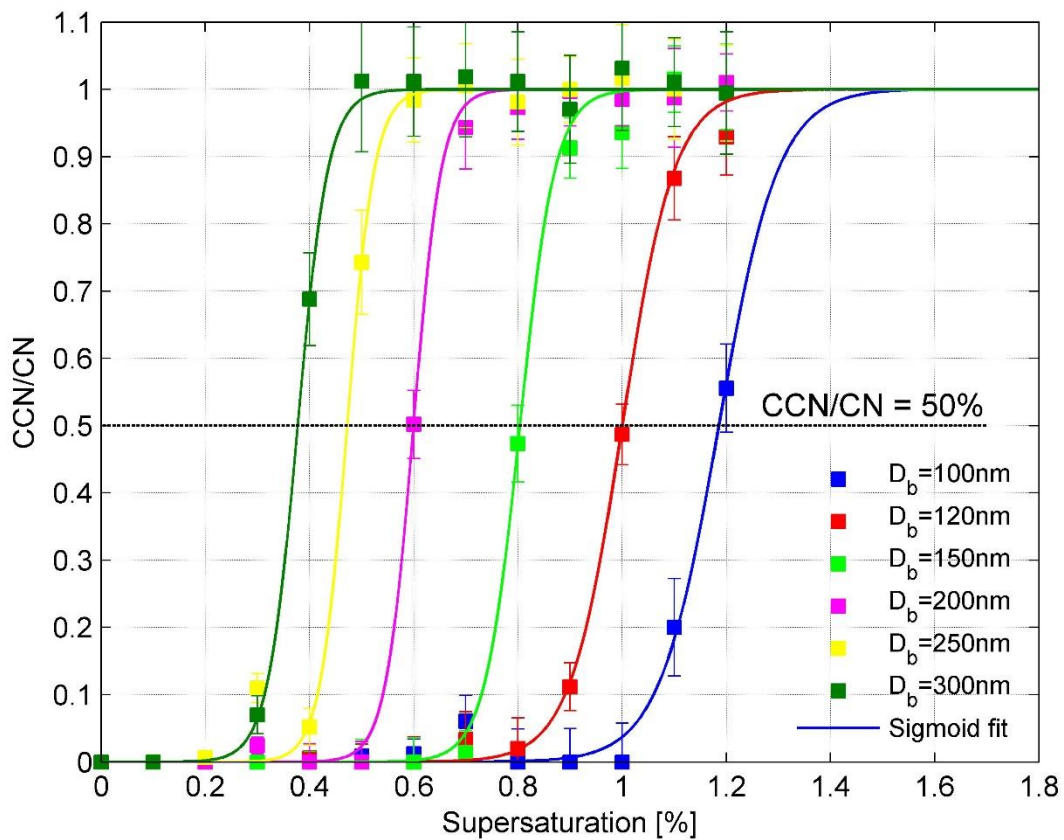
761 Fig. 3: **(a)** Average number concentration of 100 nm (mobility size) pure silica particles
 762 downstream the APM and at a rotation speed of the APM of 3000 rpm. The number
 763 concentrations were averaged over one minute for each APM voltage, and the error bars
 764 represent the standard deviation of about 60 measurements recorded under the same conditions.
 765 **(b)** Effective density of silica particles for different mobility diameters and two different
 766 rotation speeds of the APM (3000 and 5000 rpm). The fitted fractal dimensions are 2.54 and
 767 2.55, respectively. **(c)** Mass-based shape factor versus electrical mobility diameter for silica
 768 particles.



769

770 Fig. 4: The average activation ratio of pure soluble or insoluble particles with the mobility
 771 diameter of 120 nm at different supersaturations. Error bars represent the standard deviation
 772 of the activation efficiency of about 20 measurements corresponding to each supersaturation
 773 of the instrument. Critical supersaturation s_c is defined as the point where the activation ratio
 774 is equal to 50%.

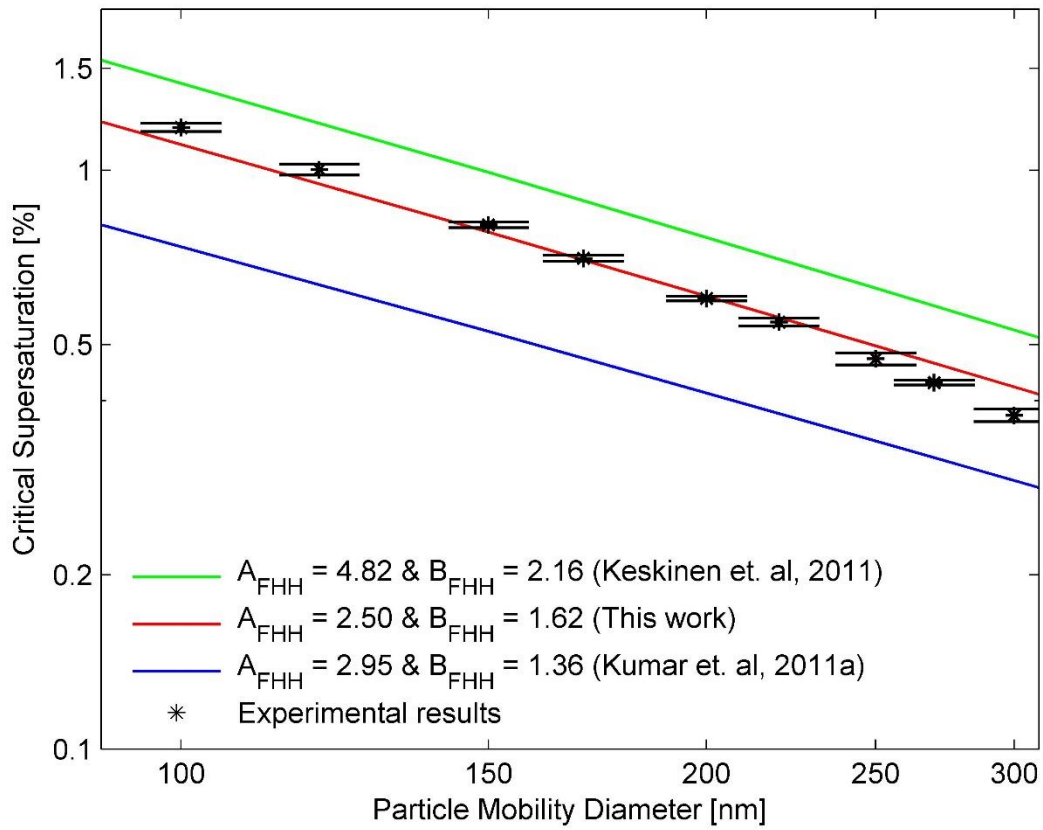
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777 Fig. 5: The average activation ratio versus supersaturation for different mobility diameters of
 778 silica particles. Error bars represent the standard deviation of the measured activation efficiency
 779 as a result of about 20 measurements corresponding to each supersaturation of the instrument.

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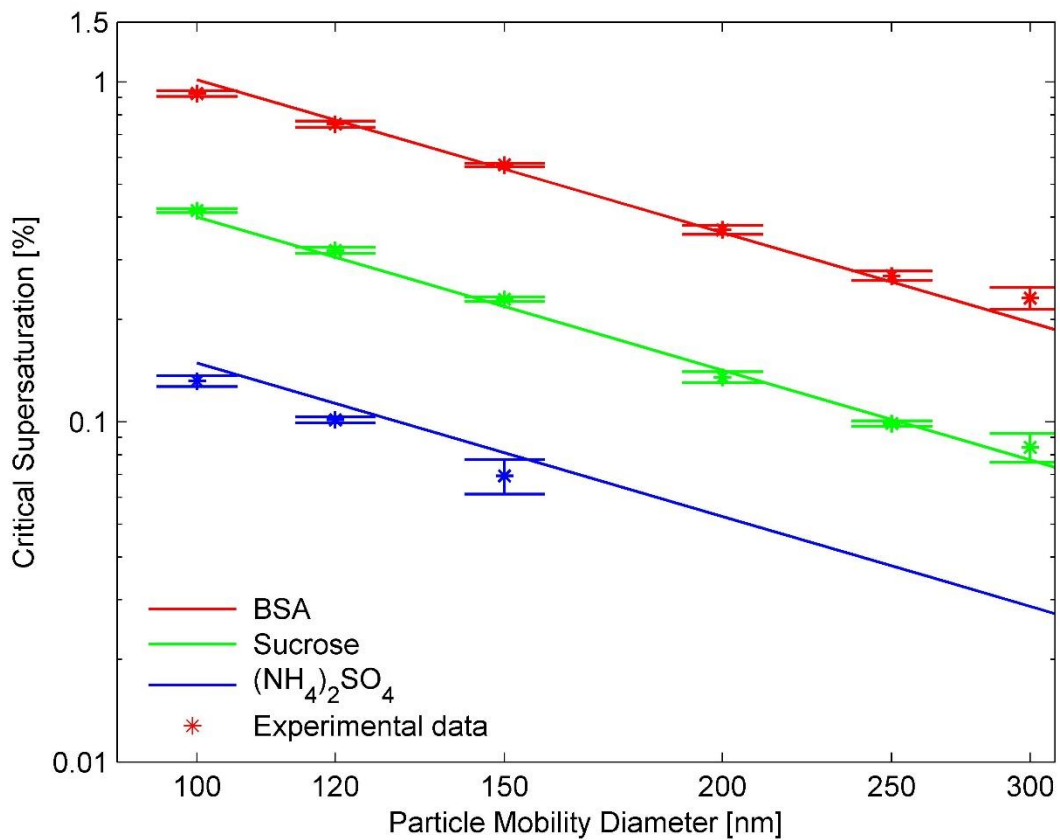


781

782 Fig. 6: Critical supersaturations against activation mobility diameter of pure silica particles with
 783 different FHH adsorption isotherm parameters from different studies compared to experimental
 784 results. Error bars represent the minimum vs. maximum values of supersaturation to estimate
 785 the s_c corresponding to each d_b .

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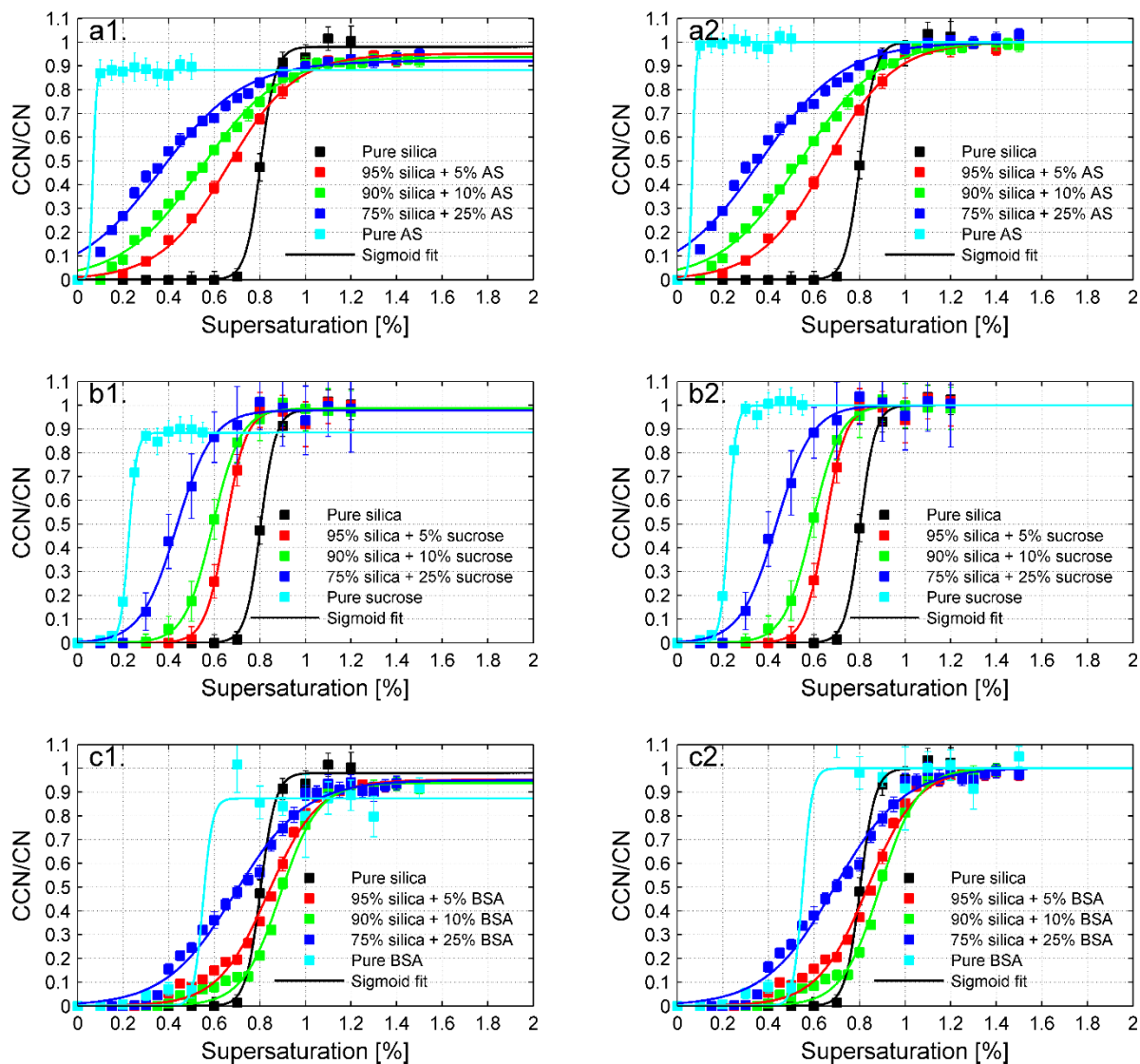
789 Fig. 7: Experimental and theoretical critical supersaturations of pure (NH₄)₂SO₄, sucrose and
 790 BSA particles for different mobility diameters based on κ -Köhler theory. Error bars represent
 791 the minimum vs. maximum values of supersaturation to estimate the s_c corresponding to each
 792 d_b .

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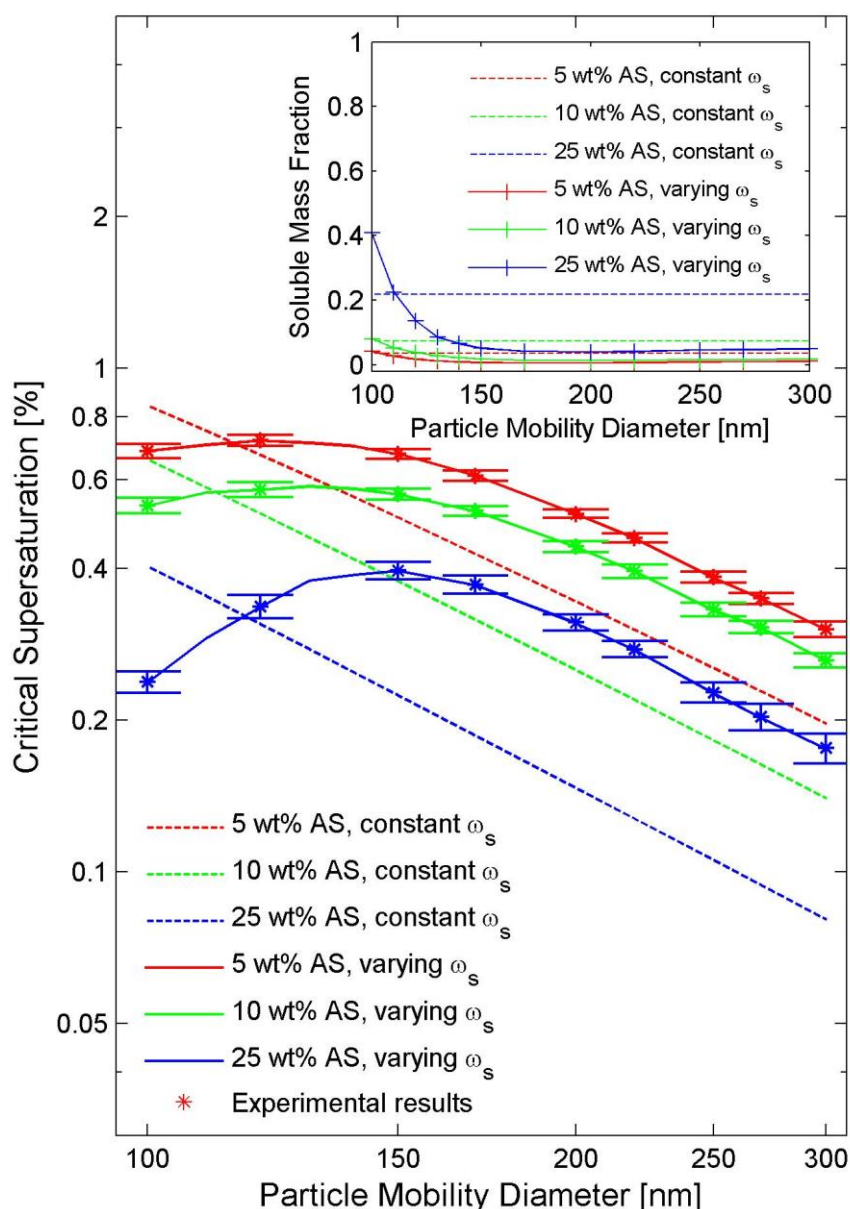
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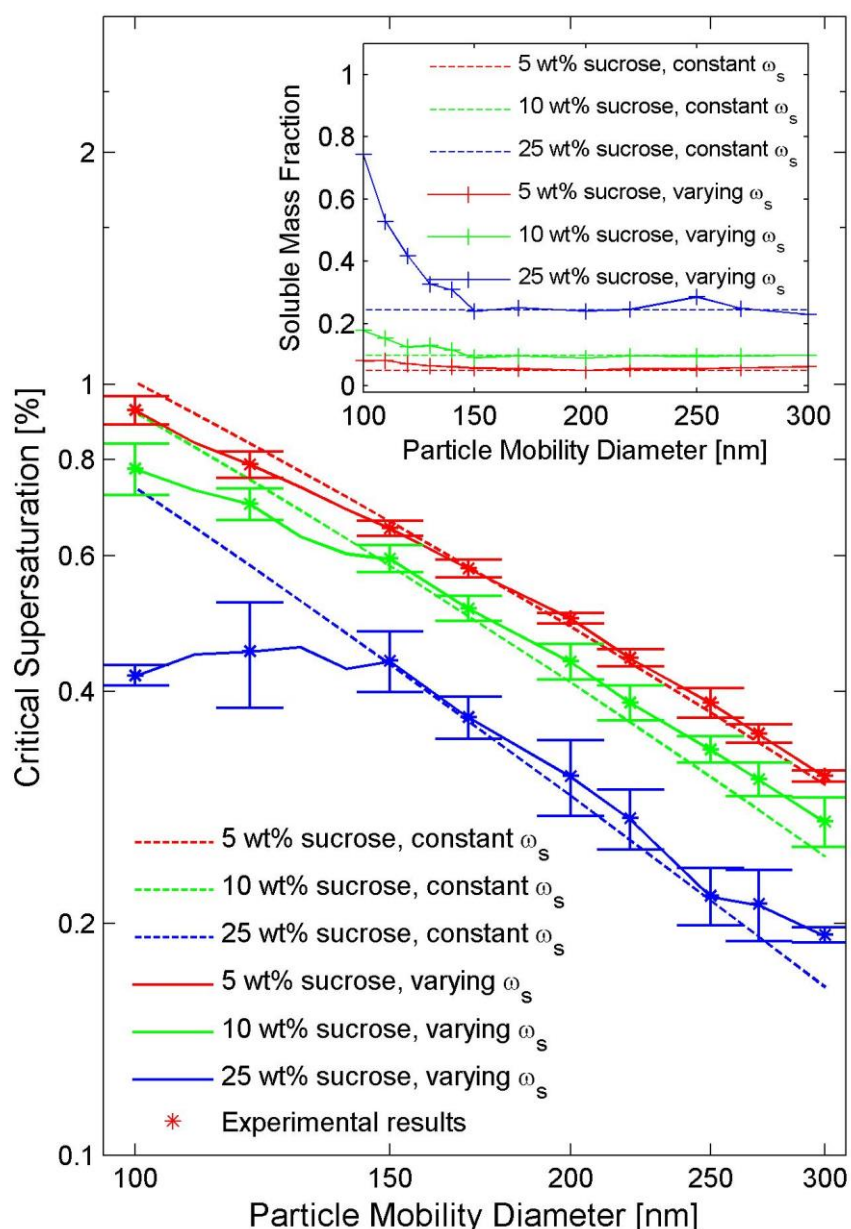


797
 798 Fig. 8: (a) Activation ratio curves for different supersaturations of silica + $(\text{NH}_4)_2\text{SO}_4$ particles
 799 of 150 nm mobility diameter, (b) Activation ratio curves for different supersaturations of silica
 800 + sucrose particles of 150 nm mobility diameter, (c) Activation ratio curves for different
 801 supersaturations of silica + BSA particles of 150 nm mobility diameter. The activation curves
 802 on the left side (subplots a1-c1) represent the unnormalized data, while the activation curves on
 803 the right side (subplots a2-c2) show the normalized ones. Error bars represent the standard
 804 deviation of the measured activation efficiency as a result of about 20 measurements
 805 corresponding to each supersaturation of the instrument.



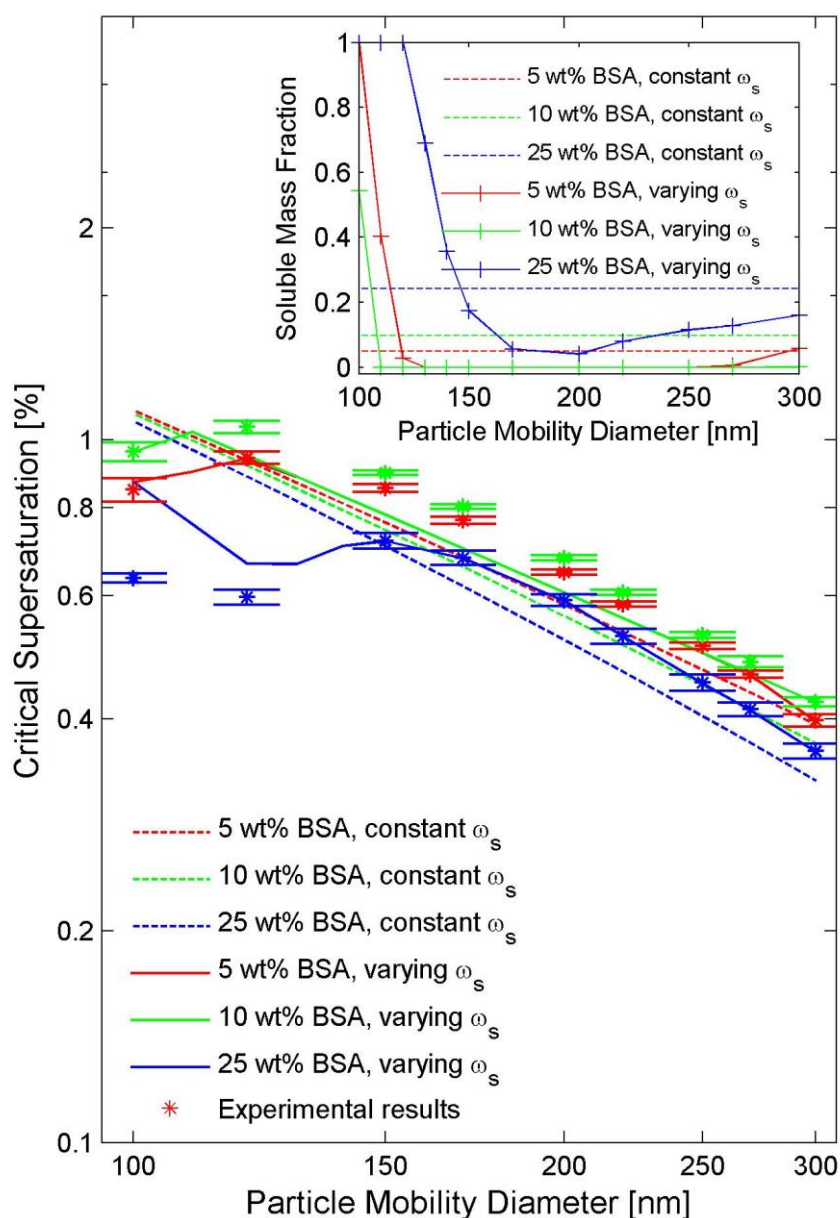
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807 Fig. 9: Experimental and theoretical critical supersaturations for mixed silica + $(\text{NH}_4)_2\text{SO}_4$ (AS)
 808 particles for different particle mobility diameters using the model by Kumar et al. (2011b).
 809 Dashed lines represent calculated critical supersaturations based on an assumption of constant
 810 soluble mass fractions (ω_s) with changing diameter and solid lines show the critical
 811 supersaturations based on the size-dependent soluble mass fractions. Error bars represent the
 812 minimum vs. maximum values of supersaturation to estimate the s_c corresponding to each
 813 mobility diameter. The inset represents assumed constant soluble mass fractions as well as size-
 814 dependent ones corresponding to the 50% points in the CCN/CN curves for different size vs.
 815 supersaturation pairs of mixed silica + $(\text{NH}_4)_2\text{SO}_4$ particles.



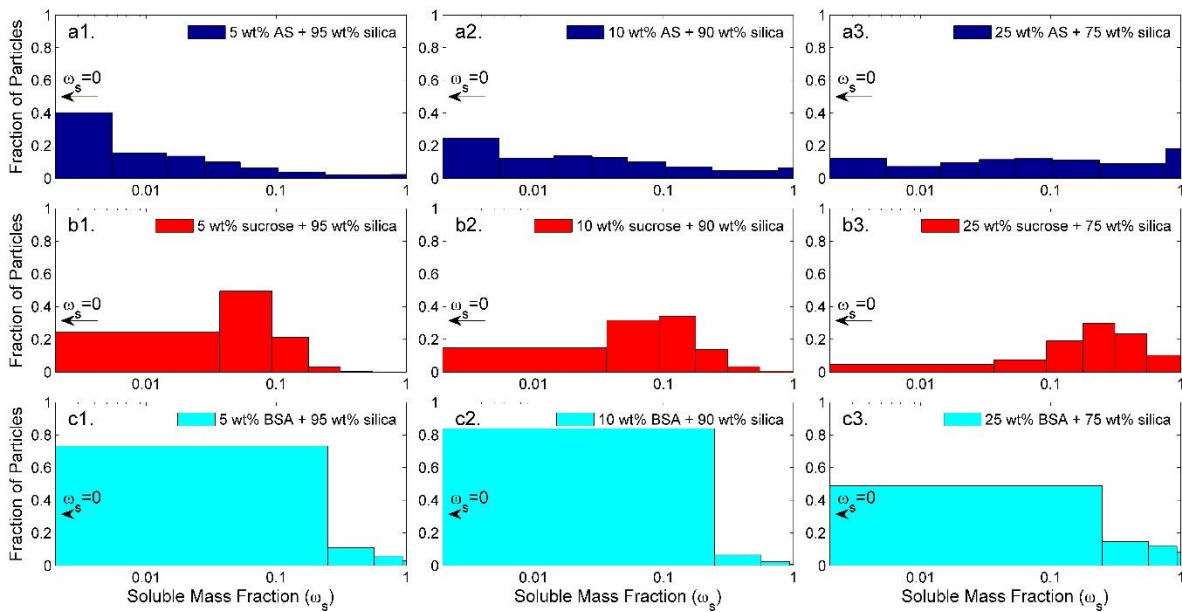
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817 Fig. 10: Experimental and theoretical critical supersaturations for mixed silica + sucrose
 818 particles for different particle mobility diameters using the model by Kumar et al. (2011b).
 819 Dashed lines represent calculated critical supersaturations based on an assumption of constant
 820 soluble mass fractions (ω_s) with changing diameter and solid lines show the critical
 821 supersaturations based on the size-dependent soluble mass fractions. Error bars represent the
 822 minimum vs. maximum values of supersaturation to estimate the s_c corresponding to each
 823 mobility diameter. The inset represents assumed constant soluble mass fractions as well as size-
 824 dependent ones corresponding to the 50% points in the CCN/CN curves for different size vs.
 825 supersaturation pairs of mixed silica + sucrose particles.



826

827 Fig. 11: Experimental and theoretical critical supersaturations for mixed silica + BSA particles
 828 for different particle mobility diameters using the model by Kumar et al. (2011b). Dashed lines
 829 represent calculated critical supersaturations based on an assumption of constant soluble mass
 830 fractions (ω_s) with changing diameter and solid lines show the critical supersaturations based
 831 on the size-dependent soluble mass fractions. Error bars represent the minimum vs. maximum
 832 values of supersaturation to estimate the s_c corresponding to each mobility diameter. The inset
 833 represents assumed constant soluble mass fractions as well as size-dependent ones
 834 corresponding to the 50% points in the CCN/CN curves for different size vs. supersaturation
 835 pairs of mixed silica + BSA particles.



836

837 Fig. 12: The distribution of soluble material on 150 nm (mobility diameter) particles in the
 838 mixed particles made of **(a1-3)** silica + $(\text{NH}_4)_2\text{SO}_4$ (AS), **(b1-3)** silica + sucrose, **(c1-3)** silica +
 839 BSA. Note that the smallest solubility bin extends down to zero, i.e. particles consisting of pure
 840 silica.