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1 **Introduction**

2 The hygroscopicity of aerosol particles plays a critical role in visibility degradation,  
3 cloud formation, radiative forcing and thereby regional and global climate (Sloane and  
4 Wolff, 1985; Charlson et al., 1992; Pandis et al., 1995; Heintzenberg and Charlson, 2009;  
5 Shi et al., 2012). Also, the hygroscopic properties of aerosol determine which fraction of  
6 aerosol particles can act as cloud condensation nuclei (CCNs) and thus contribute to the  
7 aerosol indirect effect (Pilinis et al., 1995; McFiggans, 2006; Hallquist et al., 2009).  
8 Moreover, water uptake by aerosol particles influences their health effects, as reported in  
9 epidemiological studies (Pöschl, 2005). Therefore, understanding the interactions  
10 between water vapor and aerosol particles, as well as the related physicochemical  
11 processes in the atmosphere is of great significance.

12 Biomass burning is one of the important sources of anthropogenic atmospheric  
13 aerosols and also leads to the emission of greenhouse gases. The annual globally burned  
14 land area is in the range of 3 to 3.5 million square kilometers, resulting in emissions  
15 amounting to  $2.5 \times 10^9$  kg carbon per year (van der Werf et al., 2006; Schultz et al., 2008).  
16 Particles in biomass burning smoke enriched with hygroscopic organic and inorganic  
17 constituents are suggested to act as efficient cloud condensation nuclei (Novakov and  
18 Corrigan, 1996; Petters et al., 2009; Rissler et al., 2010; Dusek et al., 2011; Frosch et al.,  
19 2011). In the Amazon basin, for example, the CCN concentration in the dry season is one  
20 order of magnitude higher than in the wet season due to biomass burning (Roberts et al.,  
21 2001; Carrico et al., 2008; Hening et al., 2010). In addition, the aerosol indirect climatic  
22 effects resulting from increased cloud condensation nuclei concentrations are expected to  
23 be very important in tropical regions, particularly in the regions with very high biomass

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24 burning emissions (Roberts et al., 2001; Carrico et al., 2008; Hening et al., 2010).  
25 Increased CCN concentrations may lead to reduced average cloud droplet radii and  
26 associated with this, likely an enhanced negative radiative forcing of affected clouds  
27 (Roberts et al., 2003; Lohmann and Feichter, 2005; Dinar et al., 2006a, b, 2007; Carrico  
28 et al., 2008). Several groups have reported that a significant portion of particles in  
29 biomass burning (from 11 % to as high as 99 % by mass) consists of water-soluble  
30 organic carbon (WSOC) (Ruellan et al., 1999; Novakov and Corrigan, 1996; Narukawa et  
31 al., 1999; Hoffer et al., 2006; Iinuma et al., 2007; Fu et al., 2009; Claeys et al., 2010;  
32 Dusek et al., 2011; Psichoadaki and Pandis, 2013). For example, Andreae et al. (2002)  
33 studied the chemical composition of the WSOC fraction of particles generated by  
34 biomass burning and divided these detected WSOC into three different classes: (1)  
35 neutrals (N), (2) monocarboxylic and dicarboxylic acids (MDA), and (3) polycarboxylic  
36 acids (PA). Further, Artaxo et al. (2002) have suggested organic surrogate compounds  
37 representing size-resolved WSOC chemical composition for the dry and wet seasonal  
38 periods of their field campaign in Rondônia, Amazonia. On the basis of chemical  
39 structure, these surrogate compounds can be represented approximately by: levoglucosan,  
40 4-hydroxybenzoic acid, and humic acid (Hoffer et al., 2006). Sampled WSOC typically  
41 contain the size distribution and a wide range of chemical species that are expected to  
42 show rather different water solubilities, and different effect on the hygroscopic growth  
43 factors of aerosol particles from biomass burning (Mochida and Kawamura, 2004; Biokos  
44 et al., 2006; Rissler et al., 2010; Jung et al., 2011). However, for a variety of WSOC  
45 compounds, it is not well known what the deliquescent relative humidity (DRH) of the  
46 pure compound is, which determines if it can exhibit substantial water uptake at moderate

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47 RH or not least as long as crystallization took place at dry conditions (followed by a  
48 hydration trajectory). Some organic components that show a small solubility in pure  
49 water (i.e., these require a large volume of water to be extracted and labeled as a WSOC),  
50 may have a DRH close to 100 % RH, which is not accessible in our hydration  
51 experiments (RH probed up to ~ 90 % RH). All these factors are of great importance in  
52 determining the CCN activity of biomass burning particles.

53 Previous laboratory studies have addressed the effects of organic surrogate compounds  
54 from biomass burning on the hygroscopic properties of mixed organic-inorganic aerosol  
55 particles containing inorganic salts (Chan and Chan, 2003; Mochida and Kawamura,  
56 2004; Brooks et al., 2004; Gysel et al., 2004; Chan et al., 2005; Svenningsson et al., 2005,  
57 2006; Koehler et al., 2006; Badger et al., 2006; Dinar et al., 2007; Sjogren et al., 2007;  
58 Carrico et al., 2008; Mikhailov et al. 2008, 2009; Hatch et al., 2009; Pope et al., 2010;  
59 Zamora et al., 2011; Dusek et al., 2011; Frosch et al., 2011; Zamora and Jacobson, 2013).

60 Studies about the hygroscopicity of individual organic compounds characteristic to  
61 biomass burning aerosol particles were performed by Mochida and Kawamura (2004).  
62 Their results showed that the hygroscopic diameter growth factors of levoglucosan  
63 aerosol particles are 1.23 at 80 % relative humidity (RH), while 4-hydroxybenzoic acid  
64 does not show any hygroscopic growth up to 95% RH when starting with dry particles.  
65 Water uptake by humic acid and mixtures of humic materials with ammonium sulfate  
66 were determined using a HTDMA setup by Brooks et al. (2004). They showed that the  
67 presence of humic acid affects the water uptake of mixed particles containing ammonium  
68 sulfate + humic acid. However, actual biomass burning aerosols are typically much more  
69 complex in terms of composition. The hygroscopicity of biomass burning aerosols likely

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70 depends on the mixing of a diversity of organic compounds with inorganic constituents  
71 during different time periods in the field (Decesari et al., 2006).

72 In this work, the hygroscopic properties of relevant organic compounds from biomass  
73 burning are determined by the HTDMA technique. Using this experimental technique, we  
74 also study the influence of the organic surrogate compounds on the water uptake behavior  
75 of mixed organic-inorganic aerosols containing ammonium sulfate. Moreover, mixtures  
76 of several the organic components with ammonium sulfate, mimicking more complex  
77 particles observed in the atmosphere are investigated to determine the influence of  
78 organic compounds on the overall particle hygroscopicity. In addition, we use the  
79 Zdanovskii-Stokes-Robinson (ZSR) relation (Stokes and Robinson, 1966), the Extended  
80 Aerosol Inorganic Model (E-AIM) (Clegg et al., 1992; Clegg et al., 2001; Clegg and  
81 Seinfeld, 2006; available online: <http://www.aim.env.uea.ac.uk/aim/aim.php>), and the  
82 Aerosol Inorganic-Organic Mixtures Functional groups Activity Coefficients  
83 (AIOMFAC) model (Zuend et al., 2008, 2011) to predict the hygroscopic growth of  
84 mixed aerosol particles and provide comparisons to our experimental findings.

85

## 86 **2 Experimental and modeling methods**

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### 88 **2.1 HTDMA instrument setup and experimental protocol**

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90 A schematic of our HTDMA setup is presented in Fig. 1. The HTDMA setup is  
91 comprised of three main components: (1) the aerosol particle generation section, (2) the  
92 particles sizing and humidification system and (3) a relative humidity control system.  
93 Polydispersed sub-micrometer particles are generated using an atomizer (MSP 1500,

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94 MSP) from bulk solutions (0.1 wt %) with different mass fractions of organic and  
95 inorganic species with deionised water (EASY Pure® I UF ultrapure water system, 18.2  
96 MΩ cm), assuming that the compositions of the mixed aerosols remain the same as that  
97 of the solution used in the atomizer. The aerosol particles pass through three silica gel  
98 diffusion dryers (SDD) and a Nafion gas dryer (Perma Pure Inc., USA), bringing the  
99 particles to a dry state ( $RH_1 < 5\%$ ). The dry aerosols are subsequently charged and then  
100 enter the first differential mobility analyzer (DMA1), where a near-monodisperse  
101 distribution of particles of the desired dry diameter ( $D_0$ ) of  $100 \pm 1$  nm is selected. After  
102 size selection, aerosols are pre-humidified in a Nafion conditioner tube, and then flow  
103 into a second Nafion tube at the set relative humidity,  $RH_2$ , of a growth factor  
104 measurement. the residence time of aerosol flow before entering into DMA2 is about 5 s  
105 in the humidification section. This residence time may be insufficient for some organic  
106 compounds to reach equilibrium at the high RH because of the very low accommodation  
107 coefficient (Kerminen, 1997; Ha and Chan, 2001; Zhang and Chan, 2000; Peng and Chan,  
108 2001; Chan et al., 2005). For example, for those coated with organic layers,  $MgSO_4$ ,  
109 sodium pyruvate, glutaric acid and asparagine. They need more long residence time to  
110 reach equilibrium. Finally, the number size distributions for the humidified aerosols are  
111 measured using the second DMA (DMA2) coupled with a condensation particle counter  
112 CPC (Model 1500, MSP). The relative humidity of the DMA2 sheath flow,  $RH_3$ , is  
113 measured using a dew point hygrometer (Michell, UK), with an uncertainty of  $\pm 0.08\%$   
114 RH. To allow the aerosol to equilibrate at the specified RH, we ensure that  $RH_3$  is equal  
115 to  $RH_2$ . In addition, critical orifices were used to regulate the sheath flows, which were  
116 both recirculated using closed-loop arrangements (Jokinen and Makela, 1997).

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## 118 **2.2 Theory and modeling methods**

119 The mobility-diameter growth factor is calculated as the ratio of mobility a particle  
120 established after exposure to a set RH level (mobility-diameter after humidification) to  
121 the reference mobility of the dry aerosol particles (at  $RH < 5\%$ ). Hygroscopic diameter  
122 growth factors,  $GF(RH) = D(RH)/D_0$ , where  $D(RH)$  is the particles diameter at a specific  
123 RH and  $D_0$  the diameter at dry conditions ( $RH < 5\%$ ),  $D_0$  is often taken as the initial  
124 mode diameter of the aerosol ( $D_{h,dry}$ ) at dry conditions,  $RH < 5\%$  selected by DMA1. In  
125 addition, following the definition of Mikhailov et al. (2004, 2008, 2009), a reference  
126 diameter  $D_0$  can be defined as being the minimum diameter ( $D_{h,min}$ ) observed while  
127 following an experimental protocol. The values of this minimum diameter and initial dry  
128 diameter are summarized in Table 2 (for set dry RH3 below  $5\%$  RH in the HTDMA  
129 operation) and measured hygroscopic growth factor of compounds presented in Fig. 2. In  
130 addition, hydroscopic diameter growth factors are based on these reference minimum  
131 diameters for the pure components are predicted using different thermodynamic models  
132 and mixing rules. In each model, we assume that these particles are spherical. As a  
133 consequence, the predicated mobility equivalent diameter is equal to the volume  
134 equivalent diameter of a sphere.

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### 136 **2.2.1 GF data fit**

137 An expression proposed by Dick et al. (2000) is used to present the relationship between  
138 water activity,  $a_w$  and  $GF(RH)$  for particles of individual compounds:

$$GF = \left[ 1 + \left( a + b * a_w + c * a_w^2 \right) \frac{a_w}{1 - a_w} \right]^{\frac{1}{3}} \quad (1)$$

$$RH / 100\% = a_w \times K_e \quad (2)$$

$$K_e = \exp \left\{ \frac{4\sigma_{sol}M_w}{RT\rho_w D_p} \right\} \quad (3)$$

Here  $a_w$  is the bulk water activity (mole fraction basis) at the composition of the solution droplet corresponding to gas phase RH at equilibrium with a bulk solution,  $\sigma_{sol}$  is the surface tension of the solution,  $M_w$  is the molecular weight of water,  $\rho_w$  is the density of pure water at  $T$ ,  $R$  is the universal gas constant,  $T$  is the temperature,  $D_p$  is the sphere-equivalent mobility particle diameter, and  $K_e$  is the so-called Kelvin correction factor term accounting for the droplet curvature.

The simplest assumption is that the Kelvin factor is equal to 1 (i.e., neglecting the droplet curvature effect), applicable to the large particles, however, for 100 nm diameter particles, ignoring the Kelvin effect at a given RH level and measured growth factor, leads to an error in the corresponding bulk solution equivalent water activity of about 1 - 2 % (Kreidenweis et al., 2005; Koehler et al., 2006). In this work, we have corrected all HTDMA GF data by evaluating the Kelvin term (Eq. 3) for the retrieved droplet size at a certain RH to obtain the corresponding water activity for comparison with models. The coefficients  $a$ ,  $b$ , and  $c$  of Eq. (1) are determined by fitting Eq. (1) to  $GF$  vs.  $a_w$  values obtained by using Eq. (2) with measured GF data at known experimental RH level. Equation (1) is appropriate to describe continuous water uptake behavior of particles with a reference diameter at dry conditions (i.e., with  $GF = 1.0$  at  $RH = 0\%$ ).

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### 160 2.2.2 GF predictions by ZSR

161 Assuming that the water uptake for each of the components of mixed particles can be  
162 treated independently at a given RH, i.e., the assumption of the Zdanovskii, Stokes,  
163 Robinson mixing rule, and that the partial volumes of individual components/phases are  
164 additive, the  $GF$  of a mixture,  $GF_{\text{mix}}(\text{RH})$ , can be estimated from the  $GF_j$  of the pure  
165 components  $j$  and their respective volume fractions,  $\varepsilon_j$ , in the mixture (Malm and  
166 Kreidenweis, 1997):

$$167 \quad GF_{\text{mix}} = \left[ \sum_j \varepsilon_j (GF_j)^3 \right]^{\frac{1}{3}} \quad (4)$$

168

### 169 2.2.3 GF prediction by E-AIM

170 E-AIM is a thermodynamic equilibrium model used for calculating gas/liquid/solid  
171 partitioning, widely used in the community. This model includes density predictions for  
172 aerosol systems containing inorganic and organic components in aqueous solutions. This  
173 allows for better consideration of non-ideal mixing effects on solution density, and hence  
174 particle diameter at different RH. The group-contribution method UNIFAC (UNIversal  
175 quasi-chemical Functional group Activity Coefficients) (Fredenslund et al., 1975; Hansen  
176 et al., 1991), can be used within the E-AIM model to predict activity coefficients in  
177 aqueous solutions of multifunctional organic compounds (Clegg et al., 2001). However,  
178 the standard UNIFAC model (Fredenslund et al., 1975; Hansen et al., 1991) is usually not  
179 appropriate for organic components in which two strongly polar groups are separated by  
180 less than four carbon atoms giving rise to intramolecular interactions, such as hydrogen  
181 bonding between certain polar groups. Some specific interaction parameters of UNIFAC  
182 were revised by Peng et al (2001). The use of these modified UNIFAC parameters

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183 improves the prediction of the water activity of dicarboxylic acids and  
184 hydroxy-di-carboxylic and -tricarboxylic acids. These modified UNIFAC parameters can  
185 also be chosen for calculations within the E-AIM model. The use of E-AIM model for  
186 mixed organic-inorganic systems has been described in a range of papers (Hanford et al.,  
187 2008; Clegg and Seinfeld, 2006; Hanford et al., 2008; Pope et al., 2010a; Yeung and  
188 Chan, 2010).

189 We applied the E-AIM model to obtain the equilibrium state of aqueous mixtures and  
190 predict the  $GF$  as a function of RH. The water uptake by the organic components is  
191 estimated by choice with either the standard UNIFAC model or the modified UNIFAC  
192 model with certain interaction parameters by Peng et al. (2001) UNIFAC-Peng as part of  
193 the E-AIM model. Both flavours of UNIFAC have been applied for certain systems  
194 studied in this work.

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#### 196 **2.2.4 $GF$ prediction by AIOMFAC**

197 The AIOMFAC model by Zuend et al. (2008, 2011) is a thermodynamic  
198 group-contribution model designed to calculate activity coefficient covering inorganic,  
199 organic, and organic-inorganic interactions in aqueous solutions over a wide  
200 concentration range. Like the optional choice in the E-AIM model, AIOMFAC also  
201 includes a modified UNIFAC model. In addition, AIOMFAC includes long-range and  
202 middle-range molecular interaction contributions based on a semi-empirical Pitzer-type  
203 model expression to explicitly account for interactions between inorganic ions and  
204 organic functional groups (plus water) in mixed solutions. This model has been  
205 successfully applied to a variety of thermodynamic equilibrium calculations, including

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206 the consideration of liquid-liquid phase separation and the deliquescence of ammonium  
207 sulfate (e.g., Zuend et al., 2010; Song et al., 2012; Zuend and Seinfeld, 2012; Shiraiwa et  
208 al., 2013).

209 In this study, we use a thermodynamic equilibrium model based on AIOMFAC (Zuend  
210 and Seinfeld, 2012; Shiraiwa et al., 2013) which assumes that all components are in a  
211 liquid or amorphous (viscous) solution, potentially exhibiting liquid-liquid phase  
212 separation in a certain RH range – except for ammoniums sulfate, which, as an option, is  
213 allowed to form a crystalline phase in equilibrium with the remaining solution (to  
214 represent the efflorescence and deliquescence hysteresis behavior of the inorganic salt  
215 depending on the mode of hydration/dehydration and starting RH in computations).  
216 Liquid-liquid phase equilibria are predicted using the algorithm of Zuend and Seinfeld  
217 (2013). However, the formation of solid (crystalline) organic phases is not generally  
218 considered at this point since in actual complex organic aerosols, the formation of  
219 crystalline organic phases is likely suppressed (Marcolli et al., 2004). Thus, in the context  
220 of this study, where solid organic phases may be present in some of the systems, the  
221 model will not be applicable – at least not to as part of the hydration branch of a humidity  
222 cycle. As an exception, we apply the model for the mixed systems of 4-hydroxybenzoic  
223 acid and ammoniums sulfate also in a mode where the assumption is made that the  
224 organic component is solid and insoluble over the whole RH range considered (this  
225 allows for better comparison with the experimental findings). Since this thermodynamic  
226 model predicts the water content (mole fraction of water) of a mixture in equilibrium with  
227 the gas phase at a given RH level, mass growth factors can be calculated directly.  
228 However, to compute diameter growth factors, assumptions about the density of different

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229 mixture components and non-ideal mixing effects on solution density need to be made.  
230 Here we use the simplified assumption of additive component volumes, while accounting  
231 for differences between the density of solid ammonium sulfate and dissolved aqueous  
232 ammonium sulfate using pure component molar volume data reported by Lienhard et al.  
233 (2012).

234

### 235 **2.2.5 Ideal solution growth factor**

236 The water activity of an ideal solution containing a nonvolatile, non-electrolyte  
237 component is equal to the mole fraction of water ( $x_w$ ) (activity coefficients of unity). Thus,  
238 in the case of an ideal solution, we can estimate the water activity of liquid particles  
239 directly from the knowledge of water content in term of  $x_w$ . Solutions comprising  
240 electrolyte components, such as ammonium sulfate or sulfuric acid, are usually strongly  
241 deviating from an ideal solution due to substantial dissolution (dissociation) of the  
242 electrolytes and non-ideal interaction between ions, water, and organic compounds.  
243 Therefore, water activities of mixed organic-inorganic systems may substantially differ  
244 from a prediction by an ideal solution assumption (e.g., Zuend et al., 2011).

245 In this study, the ideal solution growth factor is used to explore its use as a simple  
246 approach to describe the hygroscopic diameter growth factor of pure components and  
247 mixtures, e.g. for ammonium sulfate and mixed particles. Since hygroscopic diameter  
248 growth factor measurements using the HTDMA are on volume basis, the ideal solution  
249  $GF$  is calculated using mole fractions by the equation:

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$$GF = \left[ \frac{\sum_j \left( x_j M_j \frac{1}{\rho_j} \right)}{\sum_{j \neq w} \left( x_j M_j \frac{1}{\rho_j} \right)} \right]^{\frac{1}{3}} \quad (5)$$

250 Here,  $x_j$ ,  $M_j$ , and  $\rho_j$  are mole fraction, molar mass and mass density of component  $j$ ,  
 251 respectively. The sum in the numerator of Eq. (3) goes over all components including  
 252 water, while the sum in the denominator goes over all components except for water ( $j \neq w$ ;  
 253 “dry” conditions). Note that when dissociated electrolyte components are present in the  
 254 liquid mixtures, the mole fractions in Eq. (3) have to be calculated as mole fractions with  
 255 respect to completely dissociated electrolytes (or an applicable degree of dissociation).  
 256 Equation (3) is more likely applicable when water and the solute components are in a  
 257 liquid solution, i.e., no solid /phases present. In addition, it is assumed that the partial  
 258 molar volumes of organics and water in solution are equal to those of the respective pure  
 259 liquid components.

260

## 261 **3 Results and discussion**

### 262 **3.1 GF of single solute systems**

263 The hygroscopic behavior of ammonium sulfate aerosol close to room temperature is well  
 264 understood and has been characterized by several groups (Gysel et al., 2002; Kreidenweis  
 265 et al., 2005; Biskos et al., 2006a, b). We can use it as a reference substance to calibrate  
 266 the HTDMA setup because of its well-known deliquescent point (80 % RH at 294.8 K)  
 267 (Onasch et al., 1999).

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269 Fig. 2a. presents growth factors with respect to  $D_0 = D_{h,dry}$  and  $D_0 = D_{h,min}$  ammonium  
270 sulfate particles from low to high RH . The measured growth factor of ammonium sulfate  
271 is  $1.45 \pm 0.01$  at 80% RH after deliquescence. The data agree well with values measured  
272 by Gysel et al. (2002) and Wise et al. (2003), for example, the GF of AS is 1.45 at 24.9  
273 °C as measured by Wise et al. (2003). In addition, the effects of particle shape/porosity  
274 restructuring on hygroscopic behavior of AS particles investigated are rather small  
275 (Mikhailov et al., 2004, 2008, 2009). The hygroscopic growth experiments for pure AS  
276 are also in good agreement with the prediction from the E-AIM model and the  
277 AIOMFAC model. Here, both models correctly account for the solid, crystalline state of  
278 AS in the RH range before the deliquescence at  $\sim 80$  % RH for the conditions of a  
279 hydration experiment. Slight differences between these two thermodynamic models,  
280 which both account very well for the non-ideal solution behavior of AS, are due to  
281 different conversions of mass growth to diameter growth factors by the models. The  
282 E-AIM model includes a composition dependent solution density model, while the  
283 AIOMFAC-based model simply assumes volume additivity (see discussion in Section  
284 3.2). However, assuming an ideal solution, without consideration of the solid state and  
285 mixing effects on solution density, its prediction for AS results in higher than measured  
286 hygroscopic growth, also for  $RH > 80$  %. Therefore, aside from the solid-to-liquid phase  
287 transition, the water activity in concentrated solution also deviates from ideality.

288 As shown in Fig. 2b, levoglucosan aerosol particles show continuous water uptake  
289 from low to high RH, and no deliquescence phase transition is observed, in excellent  
290 agreement with the behavior reported by Mochida and Kawamura et al. (2004) and  
291 Svenningsson et al. 2006. The measured *GF* at 80 % RH is  $1.17 \pm 0.01$ , which is similar

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292 to a result from the literature (Mochida and Kawamura, 2004), which report a growth  
293 factor of levoglucosan of 1.18 at 80 % RH. Also, the measured hygroscopic growth  
294 factors are reasonably consistent with those estimated from the standard UNIFAC model  
295 within the E-AIM model, the AIOMFAC model, ideal solution theory, and the fitted  
296 expression Eq. (1). At higher RH, deviations between the different models become more  
297 significant for a good estimate of the actual *GF*. The measurements also suggest that  
298 levoglucosan absorbs a small amount of water even at 5% RH, and that it remains liquid  
299 over the full range of RH potentially rather viscous at lower RH. However, another  
300 possible explanation for slight water uptake of levoglucosan could be that nanoparticles  
301 produced by crystallization at very low RH contain volume and surface defects (porosity,  
302 polycrystalline state), which may facilitate water adsorption followed by absorption  
303 starting already at low relative humidity (Mikhailov et al., 2008, 2009). This possibility  
304 cannot be ruled out by our measurements, but the observation, which do not show a  
305 deliquescence step, would suggest that such an effect could only take place with a  
306 gradual deliquescence in the levoglucosan system. Zuend et al. (2011) discuss the case of  
307 AIOMFAC predictions for levoglucosan and its mixtures with different inorganic  
308 electrolytes. They state that the molecular structure of levoglucosan with several polar  
309 functional groups in close vicinity leads to less accurate model predictions for solutions  
310 containing this compound. The same is true for UNIFAC model predictions and is  
311 therefore a well-known limitation of these models for this particular system, explaining  
312 the observed deviations between model curves and measurements.

313 As can be seen from Fig. 2c, humic acid aerosol particles show a slight increase in  
314 *GF* from 10 % RH to 70 %. Above 70% RH, the particles start to take up increasingly

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315 more water toward high RH. The effects of microscopic restructuring on the water uptake  
316 of humic acid aerosol particles are relatively the same small, comparable with those of  
317 ammonium sulfate and levoglucosan aerosol particles. A similar tendency had been  
318 observed by Brooks et al. (2004), However, a contrasting phenomenon was observed by  
319 Zamora and Jacobson (2013); no hygroscopic growth of humic acid particles was  
320 observed over the full range of RH in their study. Due to the lack of detailed physical and  
321 chemical information about the used humic acid, the  $GF$  of humic acid particles are only  
322 presented with a data fit based on Eq. (1). The determined fit parameters are listed in  
323 Table 2. For model calculations with E-AIM and AIOMFAC, the chemical structure or at  
324 least the type and relative abundance of functional groups needs to be known, which is  
325 not the case for the humic acid particles.

326 The hygroscopic growth curves for 4-hydroxybenzoic acid are presented in Fig. 2d. No  
327 hygroscopic growth (within error) was observed below 90 % RH. Measured hygroscopic  
328 diameter growth factors with respect to  $D_{h,min}$  are above 1.0, and are close to 1.0 toward  
329 high RH (the minimum diameter was found at the highest RH measured). The main  
330 reasons for the observation of smaller particles at higher RH is likely the restructuring  
331 and/or partial evaporation of particles at higher relative humidity in the hydration mode.  
332 The measured hygroscopic diameter growth factor with respect to  $D_{h,dry}$  show of course  
333 the same slight decrease in particles diameter with increasing RH. with this definition of  
334 the reference diameter leading to GF smaller than 1.0 at higher RH, which is consistent  
335 with previous experiments by another group (Mochida and Kawamura, 2004). The  
336 reasons for the decrease in particle diameter are not fully understood, but the same  
337 behavior is reported by Shi et al. (2012) for particles consisting of ammonium sulfate +

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338 benzoic acid. On the basis of Transmission electron microscopy (TEM) image analysis,  
339 they attribute the diameter decrease to the microscopic restructuring of solid particles  
340 with increasing RH, which may affect the particle mobility diameter. Therefore, a similar  
341 effect could be responsible for the observations from our experiments. Another potential  
342 reason for a decrease in apparent diameter could be the partial evaporation of  
343 semivolatile organics from the aerosol particles in the HTDMA (here: 4-hydroxybenzoic  
344 acid, pure liquid vapour pressure  $p^{0,L} = 8.11 \times 10^{-4}$  Pa at 298.15 K, Booth et al. (2012)), an  
345 effect that is also known for certain volatile inorganic particles (e.g.,  $\text{NH}_4\text{NO}_3$ )  
346 (Lightstone et al., 2000; Hersey et al., 2013). In order to probe hysteresis effects of  
347 4-hydroxybenzoic acid during hydration and dehydration processing of the aerosol,  
348 another experiment was conducted for 4-hydroxybenzoic acid. First, the  
349 4-hydroxybenzoic acid aerosol particles were passed through a water supersaturation  
350 humidifier (RH of above 100 %), followed by drying to the different RH setpoints (90 %  
351 to 5 % RH). No obvious diameter changes other than potential restructuring effects were  
352 observed in this experiment. A possible reason is that the particles deliquesce in the  
353 oversaturation humidifier, but that their efflorescence occurs above 90 % RH, likely even  
354 above 97 % RH by their efflorescence (Mochida and Kawamura, 2004). A second  
355 possible issue could be that the residence time in the humidifier section (~ 5 s) of our  
356 HTDMA setup is too short for 100 nm 4-hydroxybenzoic acid particle to fully deliquesce.  
357 Our observations of this very limited solubility of 4-hydroxybenzoic acid, and hence, a  
358 high DRH are in agreement with the experimental data of Mochida and Kawamura (2004)  
359 for this system. Obviously, the observed results are different from the GF curves  
360 predicted by the ideal solution theory, the AIOMFAC model, and the UNIFAC-Peng

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361 (within E-AIM) model. For these predictions hydration mode, starting with particles at 0  
362 % RH, the applied models assume that the organic component is present in the liquid  
363 state and that solid organic phases are not present. However, the experimental data  
364 indicate that 4-hydroxybenzoic acid is solid and remains solid in the range from 5 % to  
365 90 % RH for a hydration experiment. Hence, the shown model predictions clearly deviate  
366 from the measurements due to the unfavourable assumption of a liquid solution and not  
367 because of a general limitation of the models for describing growth factors of the aqueous  
368 4-hydroxybenzoic acid. Would the models account for a solid organic phases, the  
369 predicted GF would be 1.0 throughout the showed experimental RH range with  
370 deliquescence of the organic crystal expected to occur at an RH value greater than 90 %.  
371 Indeed, the model curves may well capture the water uptake/loss behavior prior to  
372 crystallization for the case of a dehydration experiment starting at very high RH ( $\sim 100$   
373 %) with liquid particles becoming supersaturated, metastable solution as RH is decreased  
374 below the deliquescence point).

### 375 **3.2 Mixed systems: ammonium sulfate + levoglucosan**

376 The measured water uptake by 100 nm particles consisting of different mixtures of  
377 ammonium sulfate + levoglucosan with dry mass ratios of 3:1, 1:1, and 1:3, shown in Fig.  
378 3, present a reduction in the *GF* at  $RH > 80\%$  with increasing levoglucosan mass fraction  
379 and therefore decreasing AS content. For example, the growth factors are 1.30, 1.30, and  
380 1.28 at 80 % RH, respectively, relative to the *GF* of 1.45 of pure AS particles at 80 % RH.  
381 there is a clear shift in the full deliquescence of AS at  $RH \sim 80\%$  RH to lower RH with  
382 increasing levoglucosan mass fraction, which indicates the levoglucosan aerosol particles  
383 have significant effect on the deliquescence of ammonium sulfate. And with increasing

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384 levoglucosan mass fraction, the smoothing of hygroscopic behavior is obvious. this  
385 phenomenon was observed for mixtures of ammonium sulfate and succinic acid, malonic  
386 acid, monomethylammonium sulfate (MMAS), dimethylammonium sulfate (DMAS) by  
387 previous studies (e.g., Zaedini et al., 2008; Hämer et al., 2002; Qiu and Zhang, 2013). For  
388 example, Qiu and Zhang (2013) observed that particles consisting of 10 wt % MMAS, or  
389 DMAS and ammonium sulfate exhibit a moderate growth by water uptake in the RH  
390 range of 40 - 70 % RH. In addition, the hygroscopicity of internal mixtures of ammonium  
391 sulfate aerosol and levoglucosan with core-shell and well-mixed mixing structures were  
392 performed by Maskey et al. (2014) using HTDMA technique. They showed that the GF  
393 of the well-mixed particles was higher than that of the core-shell particles with the same  
394 fraction volume.

395 The experimental hygroscopic growth results for AS + levoglucosan mixtures are  
396 compared with four models predictions. The E-AIM model with standard UNIFAC is in  
397 relatively good agreement with the measured hygroscopic growth factors, but slightly  
398 overestimating the water uptake at  $RH < \sim 70\%$ . Especially in the case of the 1 : 1  
399 mixtures of AS: levoglucosan (by mass), the E-AIM model includes a composition  
400 dependent solution density model, (i.e., solution density depends on water content and  
401 therefore RH), while the AIOMFAC-based model does not include such a sophisticated  
402 treatment. The AIOMFAC model assumes linear additivity of pure component liquid or  
403 solid volumes/density to estimate the droplet diameter at a given RH. A possible reason  
404 for small differences between the model predictions is that E-AIM model provides  
405 droplet volume output based on density predictions of the aqueous system at different  
406 compositions (Clegg and Wexler, 2011a, b), while the other two models use a simpler

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407 volume additivity approach. We attribute a small effect on predicted GF curves due to  
408 different density treatment in E-AIM and the AIOMFAC-based model based on a  
409 comparison of E-AIM and AIOMFAC-based predicted mass growth factors and diameter  
410 growth factors for pure ammonium sulfate shown in Fig. 7.. In the case of predicted mass  
411 growth factors of ammonium sulfate, both models agree very well with each other,  
412 indicating the slight differences in predicted diameter growth factors must be due to the  
413 different way the conversion from particle mass to particle volume is done in the two  
414 models. In addition, for the levoglucosan + AS mixtures, the AIOMFAC-based model  
415 predicts a liquid-liquid phase separation between 80 % and ~ 90 % RH for the hydration  
416 conditions. The E-AIM model does not predict a phase separation and estimates a higher  
417 miscibility between the inorganic and organic components, which seems to be in better  
418 agreement with the experimental data. This is the major reason for the differences  
419 between the two model predictions regarding the diameter growth factors above AS  
420 deliquescence in case of the levoglucosan + AS system. In addition, the E-AIM model  
421 predicts a slightly higher mutual solubility of AS and levoglucosan at  $RH < 80\%$  in  
422 comparison to AIOMFAC, which leads to more dissolution of AS and associated with  
423 that, to a large water uptake at RH below full deliquescence. Regarding the ideal solution  
424 curve without consideration of a solid AS phase, the ideal curve approaches better with  
425 the measured GFs with increasing mass fraction of levoglucosan, which is a consequence  
426 of a reduced effect and less abrupt deliquescence transition of ammonium sulfate in the  
427 mixtures with higher levoglucosan mass fraction. The ZSR model is based on  
428 hygroscopic growth factors of ammonium sulfate and levoglucosan derived from E-AIM  
429 predictions for AS and fitted *GF* curve (Eq. 1) for levoglucosan. At RH above 80 %, the

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430 ZSR model is in relatively good agreement with the measured particle hygroscopicities  
431 when accounting for measurement error. However, due to the nature of the classical ZSR  
432 model used, the mutual solubility of AS in aqueous levoglucosan solution at  $RH < 80\%$   
433 below full AS deliquescence is not considered, i.e., the water uptake of organic and  
434 inorganic components is treated separately and no dissolution effects are accounted for.  
435 At those lower RH conditions, this leads to the largest deviations from experimental data  
436 for the ZSR predictions in comparison to the two other models.

### 437 **3.3 Mixed systems: ammonium sulfate + humic acid**

438 Hygroscopic behavior of 100 nm particles containing ammonium sulfate + humic acid  
439 with dry mass ratios of 3:1, 1:1, 1:3, shown in Fig.4, present a reduction in  $GF$  at  $RH >$   
440  $80\%$  with increasing mass fraction of HA (decreasing AS content). For instance, the  
441 measured growth factors are 1.30, 1.21, and 1.18 at  $80\%$  RH after full AS deliquescence  
442 for the particles containing 25 wt%, 50 wt% and 75 wt% HA (dry composition)  
443 compared to a growth factor of 1.45 for pure, deliquesced AS particles at  $80\%$  RH.  
444 Adding HA causes the mixed particles to start to take up a small amount of water before  
445 the complete deliquescence of AS, indicating HA aerosol particles have a litter effect on  
446 the deliquescence of AS. A similar tendency had been observed by Brooks et al. (2004)  
447 for mixtures containing HA and AS, which exhibit a size growth prior to  $80\%$  RH.  
448 Hygroscopic growth factors referring to the water uptake contribution by HA in the ZSR  
449 relation are obtained from the fitted growth curve of pure HA particles (Eq. 1). As for the  
450 humic acid + AS system, E-AIM predictions of the growth factors of pure AS are used in  
451 the ZSR relation here. The resulting ZSR prediction agrees relatively well with the  
452 measured hygroscopic growth of the different mixtures. Also qualitatively, when

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453 comparing the three mixtures, the ZSR prediction reproduces the lower *GF* of the 3:1  
454 AS:HA particles at RH < 80 % least amount of HA and then by contrast the higher *GF*  
455 for RH > 80 % due to a large water uptake contribution from AS after deliquescence.  
456 Model predictions using the E-AIM and AIOMFAC could not be performed for this  
457 system because of the lack of knowledge about the actual molecular structure of the  
458 humic acid samples used.

### 459 **3.4 Mixed systems: ammonium sulfate + 4-hydroxybenzoic acid**

460 Figure 5 shows the measurement and model predictions for particles consisting of  
461 ammonium sulfate + 4-hydroxybenzoic acid with dry mass ratios of 3:1, 1:1, 1:3, A *GF*  
462 reduction from panels (a) to (c) at high relative humidity is mainly due to an increasing  
463 mass fraction of 4-hydroxybenzoic acid. For example, the measured growth factors are  
464 1.31, 1.26, and 1.10 at 80 % RH after full AS deliquescence for the particles containing  
465 25 wt%, 50 wt%, and 75 wt% 4-hydroxybenzoic acid (dry mass percentages),  
466 respectively. Hygroscopic behavior of mixed 4-hydroxybenzoic acid - AS particles is  
467 found to be essentially unaffected by the presence of 4-hydroxybenzoic acid.  
468 4-hydroxybenzoic acid aerosol particles have no influence on the deliquescence point of  
469 ammonium sulfate with the low water solubility. Similar phenomenon was observed for  
470 mixtures of ammonium sulfate and organics containing glutaric, pinonic acid, and  
471 phthalic acid with low water solubility by Cruz and Pandis 2000 and Hamer et al. 2002  
472 However, the *GF* of such particles differ from pure AS particles due to the different basis  
473 of normalization dry diameter includes insoluble organic phase for the same dry size  
474 particles class. The ZSR relation agrees very well with the measured hygroscopic growth  
475 for mixed particles within measurement error due to fitted hygroscopic growth factors for

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476 4-hydroxybenzoic acid are used as input for the ZSR relation (Eq. 2). For the case of  
477 particles containing AS and 4-hydroxybenzoic acid, the ideal solution curves shows a  
478 large deviation from measured  $GFs$ , partly because of the solid organic phase, but it is  
479 also obvious that such mixtures deviate from ideal behavior. As in the case of binary  
480 4-hydroxybenzoic acid + water system (Fig. 2d), for the mixed systems with ammonium  
481 sulfate (Fig. 5), E-AIM model predictions are referring to a system where the organic  
482 component remains liquid at all RH, i.e., without consideration of a solid organic phase  
483 that is most likely present during these hydration experiments. However, the  
484 crystallization and dissolution of ammonium sulfate is considered by the two  
485 thermodynamic models. Hence, the systematic offset observed when comparing model  
486 results and measurements in Fig. 5 is mainly due to incorrect model assumptions for  
487 these organic-inorganic mixtures. In the case of the AIOMFAC model prediction a solid  
488 organic phase is assumed, i.e., it is assumed that the organic growth factor contribution  
489  $GF(4\text{-hydroxybenzoic acid}) = 1.0$  for the whole RH range, the resulting particle growth  
490 prediction is still a bit higher than the measured hygroscopic particle growths above 80 %  
491 RH. This is largely explained by the fact that the measurement indicate  $GF < 1.0$  at RH  
492  $\approx 80\%$  and above, potentially due to particles morphology effects, which then presents  
493 a systematic offset between measurements and model prediction. Microscopical particle  
494 morphology restructuring and associated size changes of solid particles at moderate to  
495 high RH levels have been found in other experiments too. An interesting, yet contrasting  
496 phenomenon was observed by Sjogren et al. (2007). They investigated different mixtures  
497 of ammonium sulfate + adipic acid in the RH range from  $\sim 5\%$  to  $\sim 95\%$  using  
498 HTDMA instruments and an electrodynamic balance (EDB). In addition, Sjogren et al.

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499 (2007) studied the morphology of samples of their mixed aerosols containing solid  
500 (insoluble) adipic acid using scanning electron microscopy (SEM). Growth factors  
501 indicating significant water uptake at RH below the full deliquescence of AS and  
502 systematic deviations from ZSR predictions observed are explained by Sjogren et al.  
503 (2007) as a result of morphological effects, including an inverse Kelvin effect, leading to  
504 enhanced particle growth factors due to water uptake into cracks, veins and pores of  
505 polycrystalline solids. In contrast, our observations indicate a shrinking of  
506 4-hydroxybenzoic acid containing particles with increasing RH or at least a decrease of  
507 their mobility-equivalent diameters.

### 508 **3.5 Mixtures of biomass burning organic surrogate compounds with ammonium** 509 **sulfate**

510 The water soluble organic carbon (WSOC) fraction in biomass burning aerosol is mainly  
511 composed of neutral compounds, a large fraction of which consisting of sugar-like  
512 compounds such as levoglucosan, mannosan and D-glucose. Levoglucosan, a major  
513 pyrolysis product of cellulose and hemicellulose, contributes substantially (16 %-31 % by  
514 mass) to the total organic fraction in PM<sub>2.5</sub> (Mochida and Kawamura, 2004; Iinuma et al.,  
515 2007; Claeys et al., 2010; Engling et al., 2013; Samburova et al., 2013). In general, MDA  
516 have been identified as pyrolysis products of lignin, which is a major constituent of  
517 woods (Mochida and Kawamura, 2004; Hoffer et al., 2006; Iinuma et al., 2007; Fu et al.,  
518 2009; Dusek et al., 2011; Psichoadaki and Pandis, 2013). We use 4-hydroxybenzoic acid  
519 to represent as a surrogate the MDA fraction; The polyacidic (PA) fraction of organic  
520 compounds is found in all samples of biomass burning aerosols (Decesari et al., 2006).  
521 Using the H-NMR technique for aerosol analysis of samples from the Po valley in Italy

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522 more than 40% of the water soluble organic carbon was identified as PA having  
523 molecular structures similar to humic materials (HMs) (Decesari et al., 2002; Fuzzi et  
524 al., 2001; Dinar et al., 2006a, b, 2007; Pope et al., 2010; Zamora et al., 2011; Fors et al.,  
525 2010). Therefore, organic surrogate compounds (levoglucosan, 4-hydroxybenzoic acid,  
526 and humic acid) have been proposed to represent the composition of WSOC on the basis  
527 of speciation methods and functional groups analysis (Decesari et al., 2006). The effects  
528 of such organic surrogate compounds on the hygroscopic behavior of mixed  
529 organic-inorganic particles containing also ammonium sulfate are measured and  
530 discussed in following. We use the relative abundances of the three model compound  
531 classes based on the chemical composition analysis of atmospheric particles reported by  
532 the Decesari et al. (2006). The chemical compositions of two distinct mixtures are given  
533 in Table 2. Mix-bio-dry and mix-bio-wet are compositions typical of biomass burning  
534 aerosols in the two different seasons (dry and wet) in the Amazon basin near Rondônia,  
535 Brazil (Decesari et al., 2006).

### 536 **3.5.1 Water uptake of mix-bio-dry and mix-bio-wet particles**

537 The hygroscopic behavior of mix-bio-dry particles in terms of  $GF$  is presented in Fig. 6a.  
538 Mixtures of organic surrogate compounds and AS in these dry season model particles do  
539 not show any growth below 65 % RH. However, mix-bio-dry particles begin to take up  
540 water at 65% RH and show steep growth between 75 % and 80 % RH, where the partial  
541 deliquescence of AS contributes increasingly to the water uptake and, hence, the overall  
542 growth factor. Similar water uptake behavior prior to full AS deliquescence has been  
543 reported by Zardini et al. (2008) and Wu et al. (2011) for different organic + ammonium  
544 sulfate mixed aerosol systems. The E-AIM model prediction for mixtures consisting of

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545 ammonium sulfate + levoglucosan with a comparable dry mass percentage ratio of 68  
546 wt%: 26 wt% is in relatively good agreement with the measured growth factors above 75  
547 % RH, this reveals that levoglucosan, as part of the mixture of organic biomass burning  
548 organic surrogate compounds, largely contributes to the water uptake of mixtures  
549 containing organic surrogate compounds and ammonium sulfate before the deliquescence  
550 of AS. The ZSR model curve is calculated on the basis of the growth factors of the pure  
551 components: for AS using E-AIM, for levoglucosan, 4-hydroxybenzoic acid and humic  
552 acid using the fitted expression (Eq. 1). The ZSR prediction tends to agree well with the  
553 water uptake investigated at RH above 80 % RH, while large deviations are found for the  
554 range between 0 % and 80 % RH, for similar reasons as discussed for the AS +  
555 levoglucosan systems (Fig. 3 and related text).

556 The hygroscopic behavior of mix-bio-wet particles is shown in Fig. 6b. In contrast to  
557 mix-bio-dry particles, mix-bio-wet aerosols show little water uptake below 80 % RH.  
558 This result is expected given the lower mass fraction of hygroscopic organics (e.g., only  
559 9.2 wt % levoglucosan) in the mix-bio-wet particles. The observed hygroscopic behavior  
560 of mixed organic-inorganic aerosols of other HTDMA studies on biomass burning  
561 aerosols published in the literature, e.g, Wu et al. (2011), cannot be compared directly to  
562 our measurements, because the samples and organic : inorganic ratios are different.  
563 However, the work by Wu et al. (2011) shows that other mixtures containing AS and  
564 organic acids found in biomass burning aerosol from Brazil, show significant water  
565 uptake at relative humidities below 80 %, similar to our mix-bio-dry case. In addition, the  
566 E-AIM model prediction for mixtures consisting of AS and levoglucosan by mass  
567 percentage ratio of 87 wt% : 9.2 wt% is in good agreement with the measured growth

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568 curve, which indicates that levoglucosan mainly contributes to the hygroscopic behavior  
569 of the organic aerosol fraction of the mixtures consisting of biomass burning model  
570 organics and AS. Also, due to the limited water uptake prior to AS deliquescence in the  
571 mix-bio-wet case, the ZSR prediction results in a good description of the measured  
572 growth curve.

573 To summarize, the hygroscopic growth factor of mixed organic + ammonium sulfate  
574 particles is affected by the presence and relative composition of organic surrogate  
575 compounds from biomass burning. For example, the growth factors during humidification  
576 of mixed particles composed of model organics and AS at 80 % RH are 1.35 for  
577 representative dry season aerosols and 1.37 for wet season aerosols. These growth factors  
578 are lower than the  $GF$  of 1.45 for pure AS particles, which is of course expected given  
579 the lower hygroscopicity of the organic components and the general finding that water  
580 uptake contributions according to Eq. (2) usually describes a mixture's  $GF$  quite well.  
581 The measured  $GF$  values of our biomass burning model systems are similar to the ones  
582 reported by Jung et al. (2011) for biomass burning aerosols sampled in Ulaanbaatar,  
583 Mongolia, for which the  $GF$  were found to be between 1.30 and 1.35 at 80 % RH during  
584 hydration. Effects of organic surrogate compounds on the deliquescence behavior of AS  
585 are found with increasing mass fraction of hygroscopic organic surrogate compounds,  
586 particularly levoglucosan, from aerosol mixtures representing the wet and dry seasons in  
587 the Amazon basin. In the case of dry period aerosols with an enhanced mass fraction of  
588 organic surrogate compounds, a smoothing of the hygroscopic behavior is observed,  
589 likely due to the continuous water uptake by levoglucosan and partial dissolution and  
590 additional water uptake by ammonium sulfate. This result is similar to the observed

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591 behavior in simple, binary mixtures of levoglucosan + AS, suggesting that  
592 4-hydroxybenzoic acid and HA show little to no effect on the hygroscopic behavior of  
593 mixed particles during a hydration experiment starting at dry conditions.

#### 594 **4 Conclusions**

595 According to field studies reported in the literature, aerosol particles from biomass  
596 burning events always contain a variety of inorganic and organic compounds. Different  
597 compositions of these aerosol particles have a significant influence on their  
598 physicochemical properties, in particular hygroscopic behavior. Differences regarding  
599 aerosol number concentration and particle composition were observed for the dry and wet  
600 seasons in the Amazon and other regions (Artaxo et al., 2002; Decesari et al., 2006;  
601 Rissler et al., 2006). In this work, we focused on three organic compounds (levoglucosan,  
602 4-hydroxybenzoic acid, and humic acid) to represent common compound classes from  
603 biomass burning. These organics are also representative of three different water uptake  
604 characteristics. Hygroscopic growth measurement for the two-component organic + AS  
605 particles show that certain organic compounds can have an important influence on the  
606 overall particle diameter growth factor and the partial deliquescence of AS, e.g., mixtures  
607 of levoglucosan with AS. With increasing mass fraction of levoglucosan, a clear shift of  
608 the onset of AS deliquescence to lower RH is occurring, which also leads to an overall  
609 more smooth looking hygroscopic growth factor curve. In contrast, 4-hydroxybenzoic  
610 acid and humic acid show no obvious effect on the deliquescence RH of AS. Also, due to  
611 the limited solubility of these two organic compounds, the hygroscopic growth factors at  
612 RH below 95 %, as measured, are reduced relative to that of pure AS particles.

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613 Mixtures of organic surrogate compounds with AS, representing atmospheric aerosols  
614 from biomass burning were made, with chemical compositions determined on the basis of  
615 different organic and inorganic component fractions observed for the dry and the wet  
616 period in the Amazon basin. The most striking difference in measured hygroscopic  
617 growth curves comparing the two seasons is due to presence of different amounts of  
618 levoglucosan as surrogate compound, implying that highly oxidized organic compounds  
619 like levoglucosan may play an important role in controlling the hygroscopic behavior of  
620 atmospheric particles at RH below the full deliquescence of inorganic salts, such as AS.  
621 Therefore, a main advantage of using organic surrogate compounds representing the  
622 complex WSOC fraction of biomass burning, aerosol is their use for laboratory  
623 experiments and associated evaluation and improvement of thermodynamic mixing  
624 models and parameterization for the predictions of hygroscopic behavior and CCN  
625 activity in atmospheric models.

626 This work focuses on the water uptake and deliquescence behavior of organic  
627 compounds from biomass burning sources and their influence on the water uptake of  
628 mixed organic-ammonium sulfate aerosol particles. Ambient biomass burning aerosol  
629 particles may undergo the humidity cycles depending on the RH history of an air parcel.  
630 Humidity cycles may possible lead to solid-liquid phase transition hysteresis with distinct  
631 deliquescence and efflorescence behavior of the organic components and  
632 organic-inorganic-mixtures. Associated changes of aerosol hygroscopicity of mixed  
633 particles similar to the multicomponent systems studies in this work will be a topic of  
634 studies in the future.

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1095 **Table 1.** Substances and their physical properties used in this work.

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Chemical compound	Chemical formula	Molar Mass [g mol <sup>-1</sup> ]	Density in solid and liquid state [g cm <sup>-3</sup> ]	Solubility g/100cm <sup>3</sup> H <sub>2</sub> O	Solution surface Tension [J m <sup>-2</sup> ]	Manufacture
Ammonium sulfate	(NH <sub>4</sub> ) <sub>2</sub> SO <sub>4</sub>	132.140	1.770 <sup>a</sup> , 1.550 <sup>b</sup>	74.400 (at 20°C)	0.072	Alfa Aesar, 99.95%
Levoglucozan	C <sub>6</sub> H <sub>10</sub> O <sub>5</sub>	162.100	1.618 <sup>c</sup> 1.512 <sup>d</sup>		0.073 <sup>e</sup> (0.01-10 mg/mL)	Aldrich, 99%
4-Hydroxybenzoic acid	C <sub>7</sub> H <sub>6</sub> O <sub>3</sub>	138.100	1.460 1.372 <sup>f</sup>	0.675(at 25 °C)	0.070 <sup>g</sup>	Alfa Aesar, 99.99%
Humic acids		NA	0.800 <sup>h</sup>	NA	0.073 <sup>i</sup>	Aldrich, 99%

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1098 <sup>a</sup> Clegg and Wexler (2011a);

1099 <sup>b</sup> Lienhard et al. (2012);

1100 <sup>c</sup> Tuckermann and Cammenga (2004);

1101 <sup>d</sup> Jedelský et al. (2000);

1102 <sup>e</sup> Kiss et al. (2005);

1103 <sup>f</sup> Yates III and Wandruszka (1999);

1104 <sup>i</sup> Mikhailov et al. (2008).

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1110 **Table 2.** Initial dry diameter ( $D_{h,dry}$ ) ( $RH < 5\%$ ) and minimum mobility diameter ( $D_{h,min}$ )  
1111 in hydration (h) mode of the HTDMA experiments.

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Aerosol type	$D_{h,dry}$ (nm)	$D_{h,min}$ (nm)
Ammonium sulfate	100.6	99.5
Levoglucosan	99.8	99.6
Humic acid	100.4	100.3
4-Hydroxybenzoic acid	100.2	95.0

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1134 **Table 3.** Coefficients (a, b, c) of the fitted growth curve parameterization to measured  
 1135 growth factor data using Eq. (1). Measured growth factors of  $D_0$  nm particles used in Eq.  
 1136 (1) were first corrected for the Kelvin effect.

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Chemical compounds	<i>a</i>	<i>b</i>	<i>c</i>
Levogluconan	0.45602	-0.69869	0.44755
4-Hydroxybenzoic acid	-0.14061	0.22767	-0.09526
$D_0 = D_{h,dry}$			
Humic acid	0.33579	-0.60172	0.40850

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1153 **Table 4.** The chemical composition of biomass-burning model mixtures studied, given as  
1154 mass percentages (wt %).

Mixture name	Ammonium sulfate	Levoglucosan	4-Hydroxybenzoic	Humic acid
Mix-bio-dry	68.0%	26.0%	3.0%	3.0%
Mix-bio-wet	87.2%	9.2%	1.5%	2.1%

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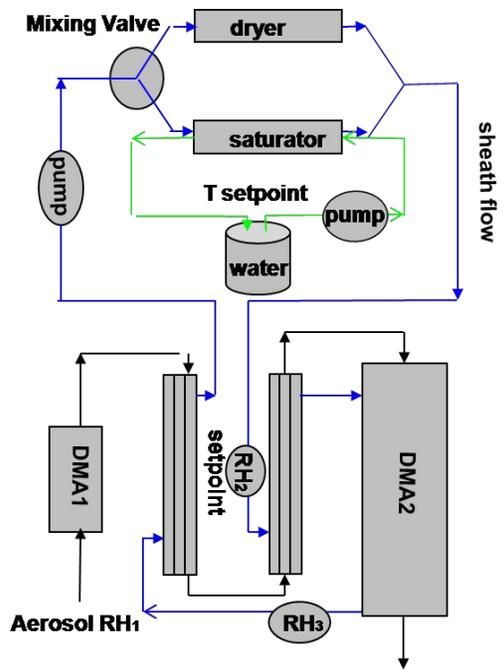
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Fig. 1. Schematic of the hygroscopicity tandem different mobility analyzer (HTDMA) system.

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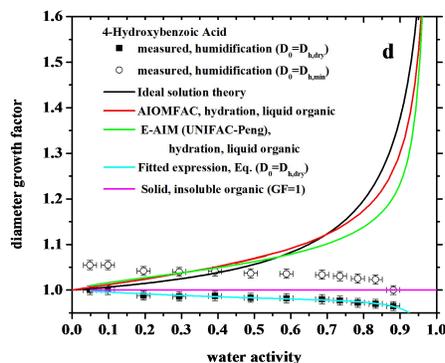
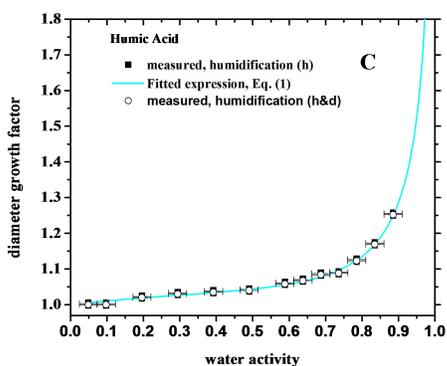
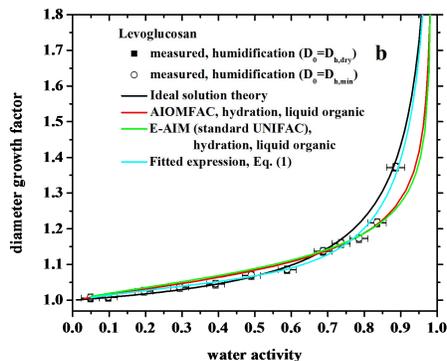
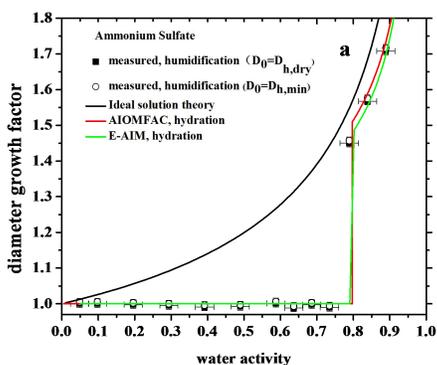
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1183 **Fig. 2.** Hygroscopic diameter growth factor (GF) for  $D_0$  (initial dry diameter RH < 5 %) aerosol particles.

1184 The measurements, model calculations, and fitted expression Eq. (1) represent conditions of particle growth

1185 during a hydration experiment from 5 % to 90 % RH at 298.15 K. Measured growth factors are corrected

1186 for the Kelvin effect and and therefore shown vs. water activity. Symbols: measured GF are shown with

1187 respect to  $D_0 = D_{h, dry}$  (black squares) or  $D_0 = D_{h\&d, min}$  (open circles). Systems: **(a)** ammonium sulfate **(b)**

1188 levoglucosan, **(c)** humic acid, and **(d)** 4-hydroxybenzoic acid.

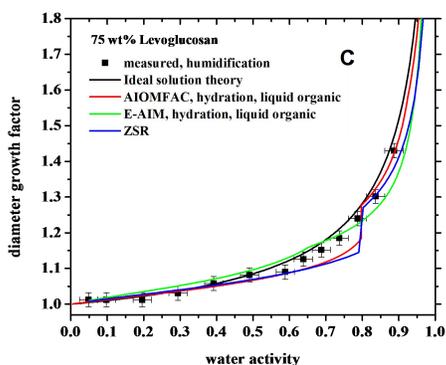
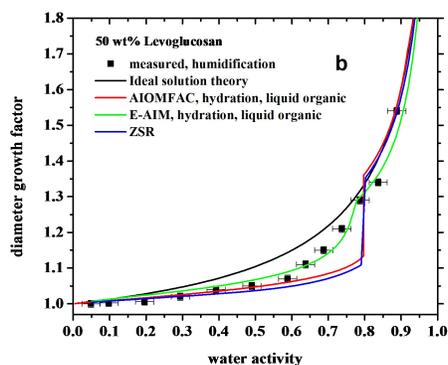
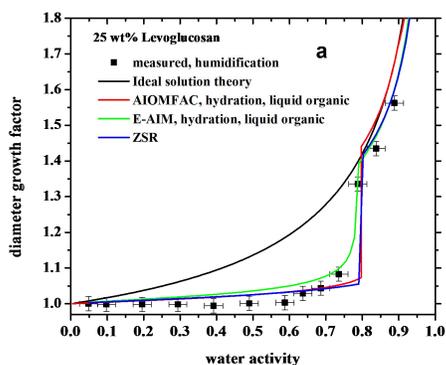
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1196 **Fig. 3.** Hygroscopic growth factors of aerosol particles containing mixtures of levoglucosan with  
 1197 ammonium sulfate at three different dry state mass fractions. The measurements and model calculations  
 1198 represent the particle growth during a hydration experiment from 5 % to 90 % RH at 298.15 K. Measured  
 1199 growth factors are corrected for the Kelvin effect and and therefore shown vs. water activity. Mass ratio of  
 1200 AS: Levoglucosan: **(a)** 3:1, **(b)** 1:1, **(c)** 1:3.

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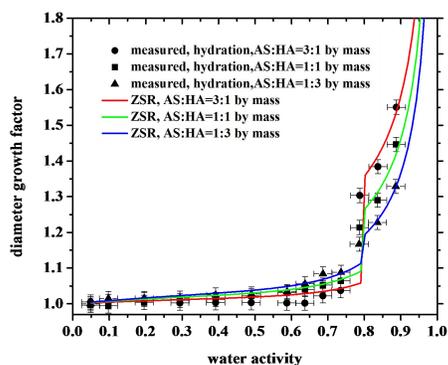
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1208 **Fig. 4.** Hygroscopic growth factors of aerosol particles containing mixtures of humic acid (HA) and  
 1209 ammonium sulfate at three different dry state mass ratios. The measurements and ZSR model calculations  
 1210 represent the particle growth during hydration experiments from 5 % to 90 % RH at 298.15 K. Measured  
 1211 growth factors are corrected for the Kelvin effect and and therefore shown vs. water activity.

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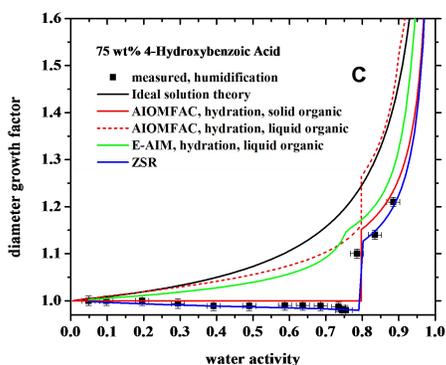
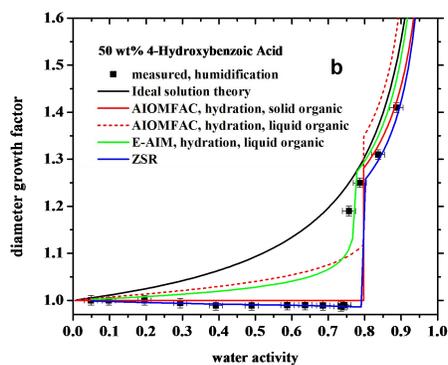
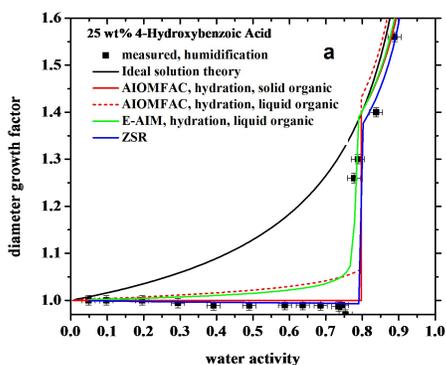
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1226 **Fig. 5.** Hygroscopic growth factors of aerosol particles containing mixtures of 4-hydroxybenzoic acid  
 1227 ammonium sulfate at three different dry mass ratios. The measurements and model calculations represent  
 1228 particle growth during hydration experiment from 5 % to 90 % RH at 298.15 K. Measured growth factors  
 1229 are corrected for the Kelvin effect and and therefore shown vs. water activity. Mass ratio of  
 1230 AS:4-Hydroxybenzoic Acid: **(a)** 3:1, **(b)** 1:1, **(c)** 1:3.

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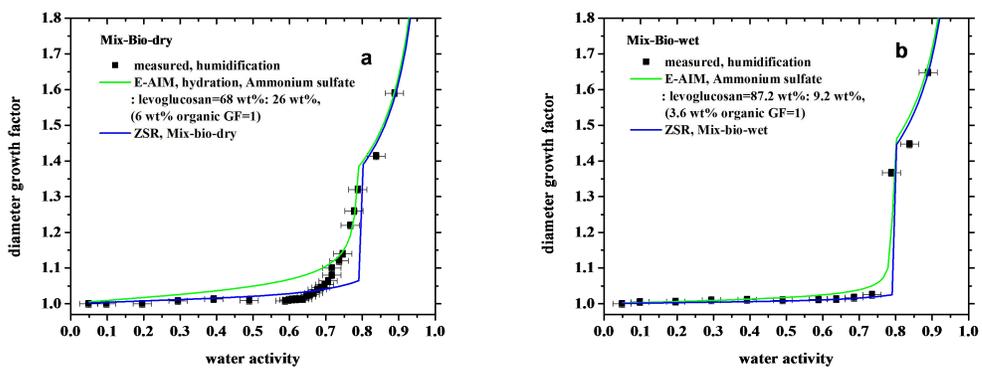
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1238 **Fig. 6.** Hygroscopic growth factors of 100nm (dry diameter) particles consisting of mixtures of organic  
 1239 surrogate compounds with ammonium sulfate representing particles of (a) dry and (b) wet seasonal periods  
 1240 in the Amazon . The measurements and model calculations describe the particle growth during hydration  
 1241 experiments from 5 % to 90 % RH at 298.15 K systems. Measured growth factors are corrected for the  
 1242 Kelvin effect and and therefore shown vs. water activity.

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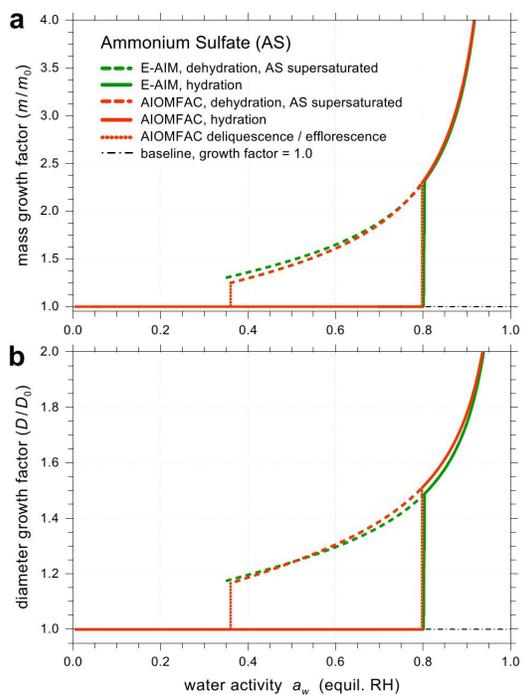
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1255 **Fig. 7.** Comparison of E-AIM and AIOMFAC-based mass growth factors (a) and growth diameter growth  
 1256 factors (b) for the binary ammonium sulfate + water system at 298.15 K.