

## 1 Online Supporting Information.

- 2 1) Differences with Ball et al
- 3 2) Variation of Mixing Region temperature
- 4 3) Measured [H<sub>2</sub>SO<sub>4</sub>] vs. QA
- 5 4) Long time monitoring of NBC
- 6 5) Differential Mobility Analyzer. Particle sizes.
- 7 6) More data sets for particle vs. MS ion ratio or QA .
- 8 7) Ammonia and amine additions.
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- 10 9) Contamination Episode.
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12

### 13 1 Differences with Ball et al.

14 There are significant differences with the procedure of Ball et al. and it is assumed that these  
15 differences have little effect on the results. They are listed here for completeness. As noted in  
16 the text, Q<sub>A</sub>, the N<sub>2</sub> flow rate over the sulfuric acid reservoir was varied to attain variations in  
17 H<sub>2</sub>SO<sub>4</sub> content: also, the small tube carrying this flow was ~ 29 °C whereas in Ball et al. it was  
18 maintained at 60 °C.

19 There was also (i) a higher pressure, 1 atm vs. 0.8 atm, and (ii) a larger mass flow rate, 6 sLpm  
20 vs. 5 sLpm. The overall effects of (i) and (ii) result in an average flow velocity that is similar to  
21 that of Ball et al. Buoyancy driven convection is expected to be similar.

22 There was no (iii) periodic rinsing of the flow reactor with de-ionized water as was done by Ball  
23 et al. Rinsing the flow reactor was not done because it would be exposed to room air which is  
24 not desirable. The reproducibility of the results supports this decision. However, at one point  
25 the dry N<sub>2</sub> flow line (Teflon) was T-ed into to introduce an amine to this flow (and thus the  
26 mixing region); upon withdrawing the amine, particle count rates subsided quickly but plateaued  
27 after a few days at ~300 s<sup>-1</sup> for NBC, indicating the line became contaminated with the amine  
28 (normal NBC conditions yield particle count rates of ~ 20 s<sup>-1</sup>.) This line was removed from the  
29 system, rinsed with a 10<sup>-3</sup> M HCl solution and then deionized water, dried and replaced  
30 whereupon NBC conditions yielded a typical particle count rate of 15 s<sup>-1</sup>.

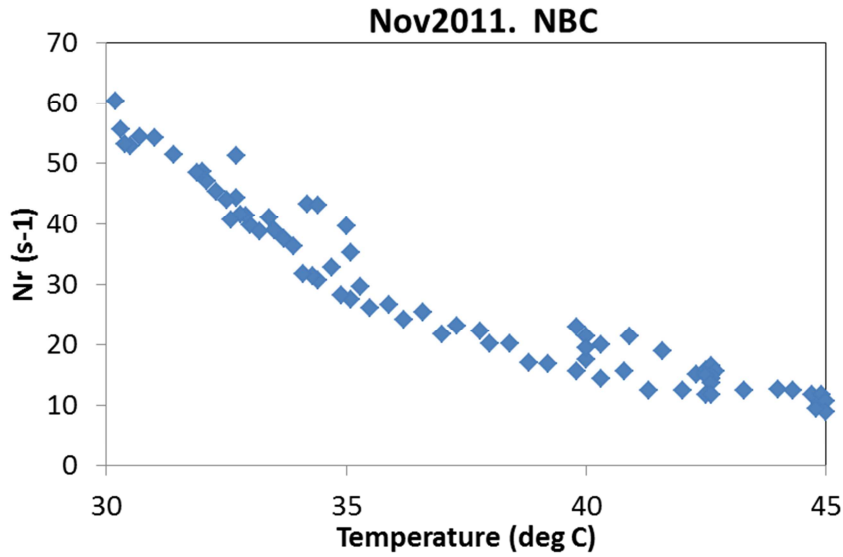
1 The chemical ionization mass spectrometer (iv) had an ion drift region (aka Hanson, 2005, ion  
2 molecule reaction times of  $\sim 1$  ms set by electric fields) rather than a flow arrangement (aka  
3 Eisele and Tanner, 1993, ion molecule reaction times of  $\sim 1$  s set by gas flows) and (v) ammonia  
4 was introduced below the mixing region rather than in it. The drift arrangement (iv) is less  
5 sensitive than the flow arrangement but  $[\text{H}_2\text{SO}_4]$  is more readily calculated in the absence of  
6 calibrations. Nonetheless, both systems are passive monitors of sulfuric acid and should yield  
7 equivalent results. The differences in ammonia introduction methods means that a direct  
8 comparison between the ammonia addition experiments should be made with caution.

9 The nucleation time (vi) here of 8 s is different than that used by Ball et al. of 4 s which was  
10 based on a 4 cm/s flow velocity over the  $\sim 15$  cm nucleation zone length. A more refined  
11 estimate here was obtained by using their Figure 3(a) data and noting that a 4 cm/s speed applies  
12 to 1/3 of this length, 2.5 cm/s applies to the middle third, and 1 cm/s applies to the top portion.  
13 The sum of times in these portions of the nucleation zone is about 8 s, which is assigned a large  
14 uncertainty of +100%, -50%. Further exploration of the time for nucleation in a flow reactor will  
15 be done with fluid dynamics simulations.

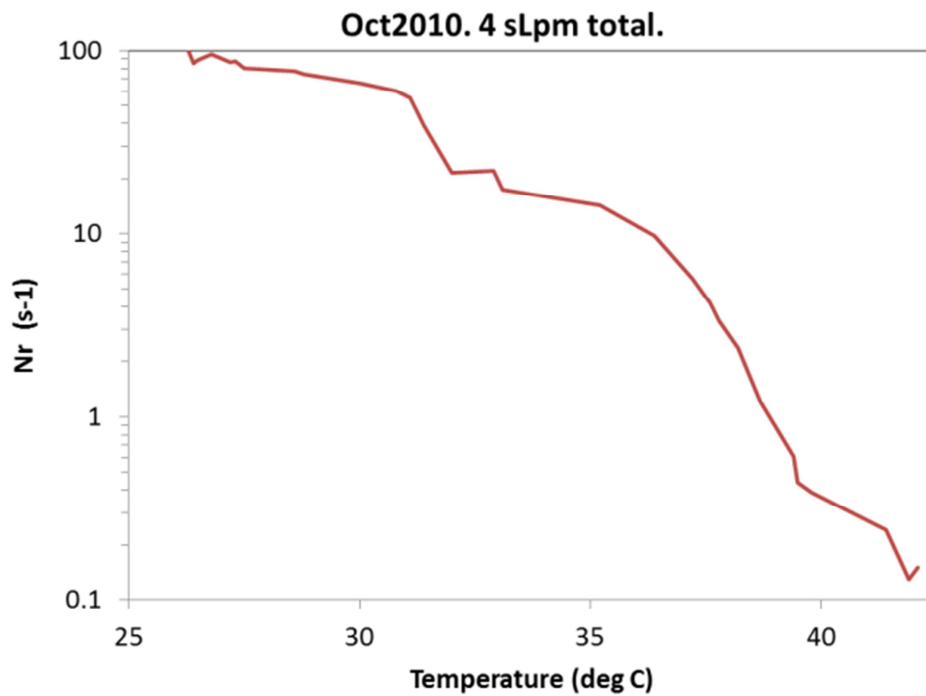
16 Finally, the particle inlet here did not extend into cooled section of the flow reactor which is  
17 believed to lead to a high variability in the present measurements.

## 18 **2 Variation of mixing region temperature.**

19 Temperature of the mixing region was varied over the range of 30 to 45 C and particle numbers  
20 decreased considerably as temperature increased. This is due to suppression of nucleation in the  
21 mixing region, and to a lesser extent, changes in flow patterns in the transition and nucleation  
22 regions. This is shown in Fig A1(a) for NBC and a set of data taken  $\sim 13$  months earlier (b), a  
23 few weeks after the system was initially assembled and at a total flow rate of 4 sLpm. A much  
24 stronger dependence on mixing region temperature is exhibited in Fig. A1b. The stronger effect  
25 may be due to the lower flow rate and also to contaminants that may be present initially in the  
26 system. Further experimentation on this effect with N bases present in the mixing region are  
27 planned.



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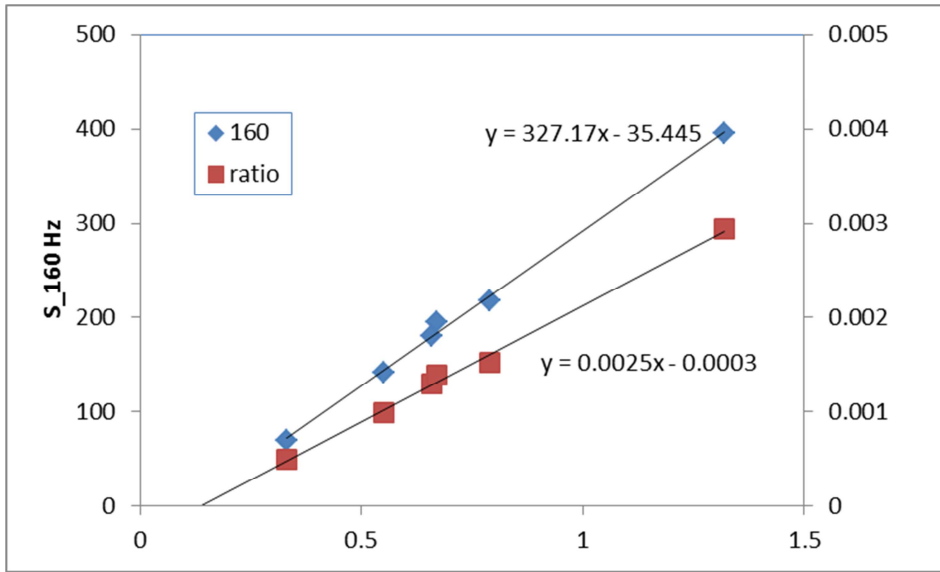
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3 Fig. A1. Variation of particle counts as a function of mixing region temperature. Results of the  
 4 particle number versus mixing region temperature performed in (a) Nov 2011 and (b) Oct 2010.

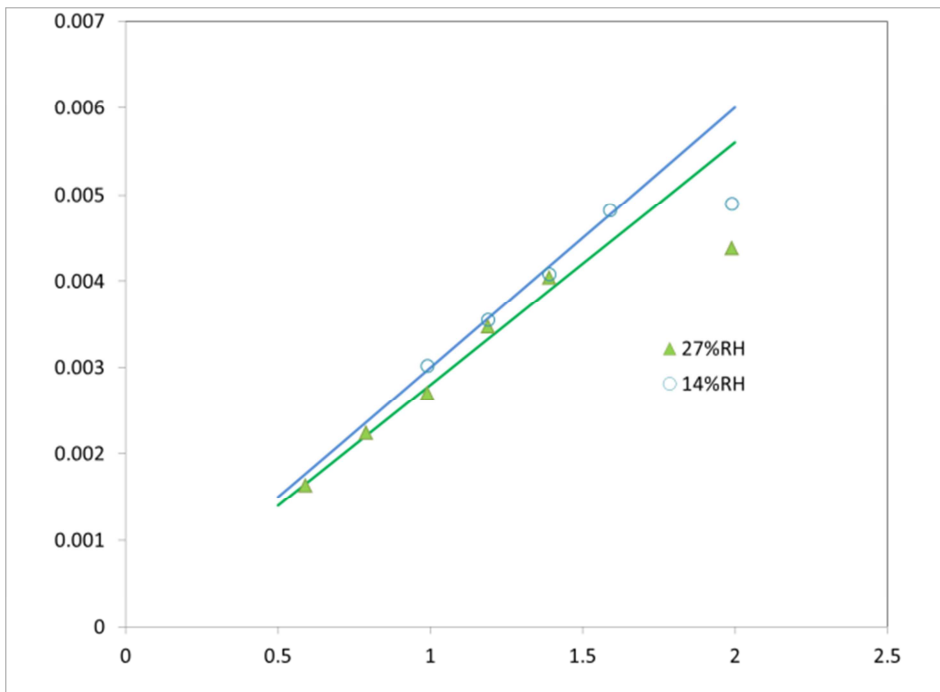
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### 6 3 Mass spectrometer detection vs QA, flow rate through sulfuric acid reservoir.

7 Shown in Fig. A2 (a) and (b) are the ion signals for sulfuric acid versus flow rate. A linear  
 8 relationship is shown. Evident in fig. A2b, deviations from this relationship occurs for flows  
 9 higher than about 1.6 sLpm.



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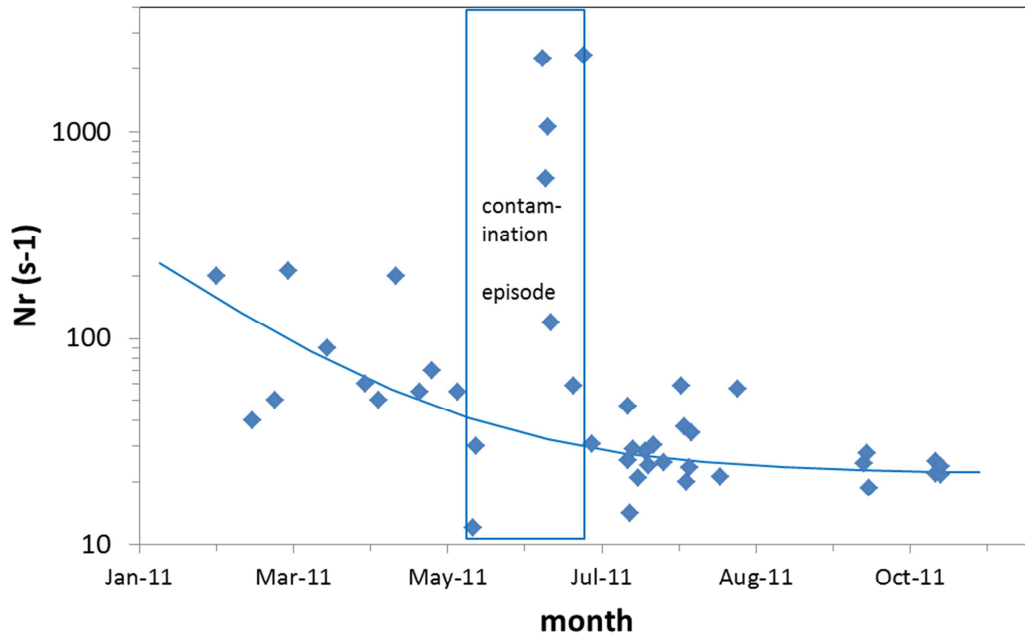
3 Figure A2. Variation with  $Q_A$  of the raw signal at 160 u ( $\text{HSO}_4^- \cdot \text{HNO}_3$ ) and the ratio of signals  
 4 for the  $\text{HSO}_4^-$  core ions and the  $\text{NO}_3^-$  core reactant ions.

5

#### 6 4 Nr for NBC conditions for 10 months.

7 A plot of measured count rates with time for NBC is shown in Figure A3. A general  
 8 downwards trend is exhibited: an exponential decay with a constant is plotted as a suggested  
 9 time dependency. A contamination episode is indicated during the months of May and June

1 2011 which is explained below. Note that the large spikes in early June are due to heating of  
 2 contaminated lines that were then cleaned or replaced.



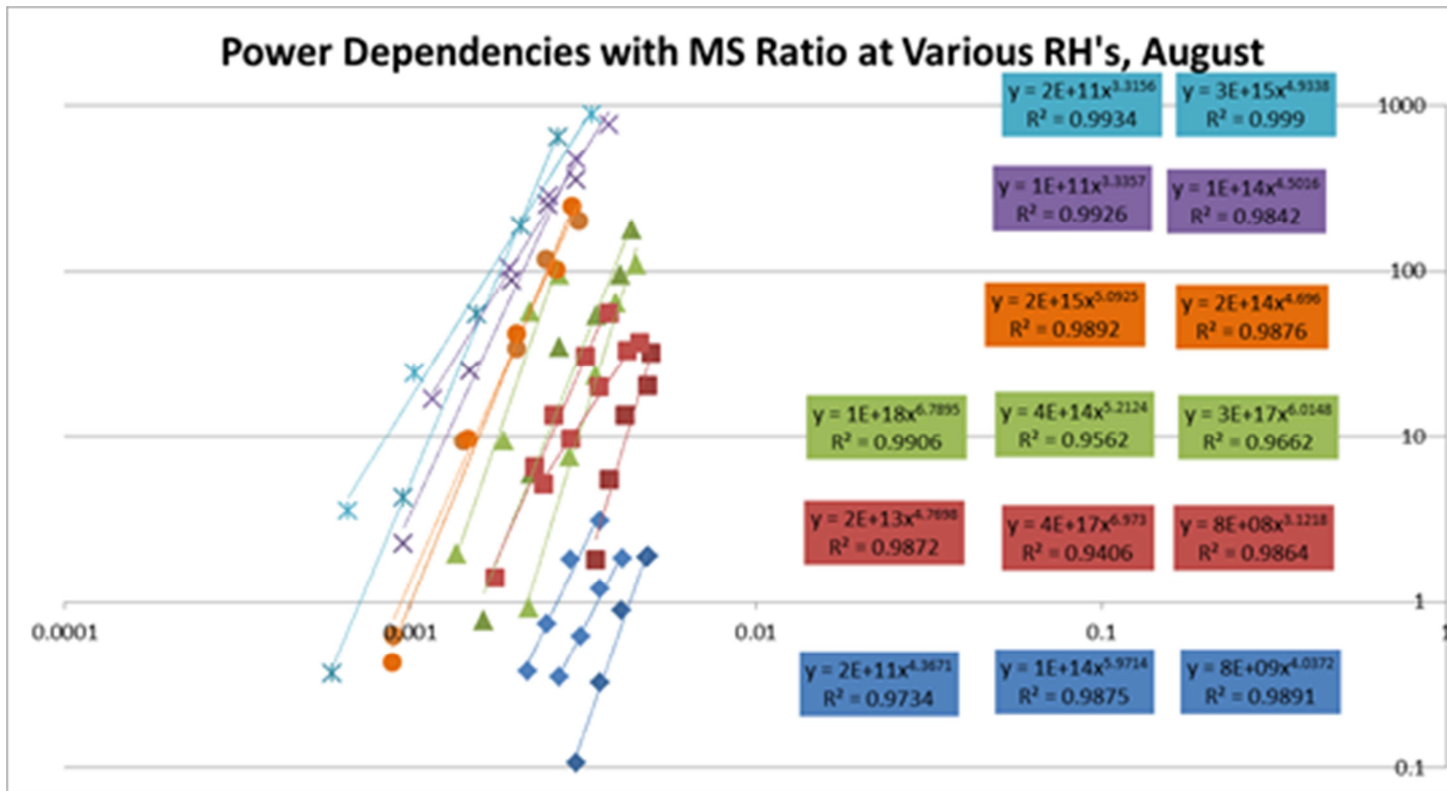
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4 Figure A3. Nr versus date, for 10 mos. Beginning in late Jan-11, NBC conditions were chosen  
 5 with total flow rate of 6 sLpm and  $T_{\text{H}_2\text{SO}_4}$  reservoir = 30 C.

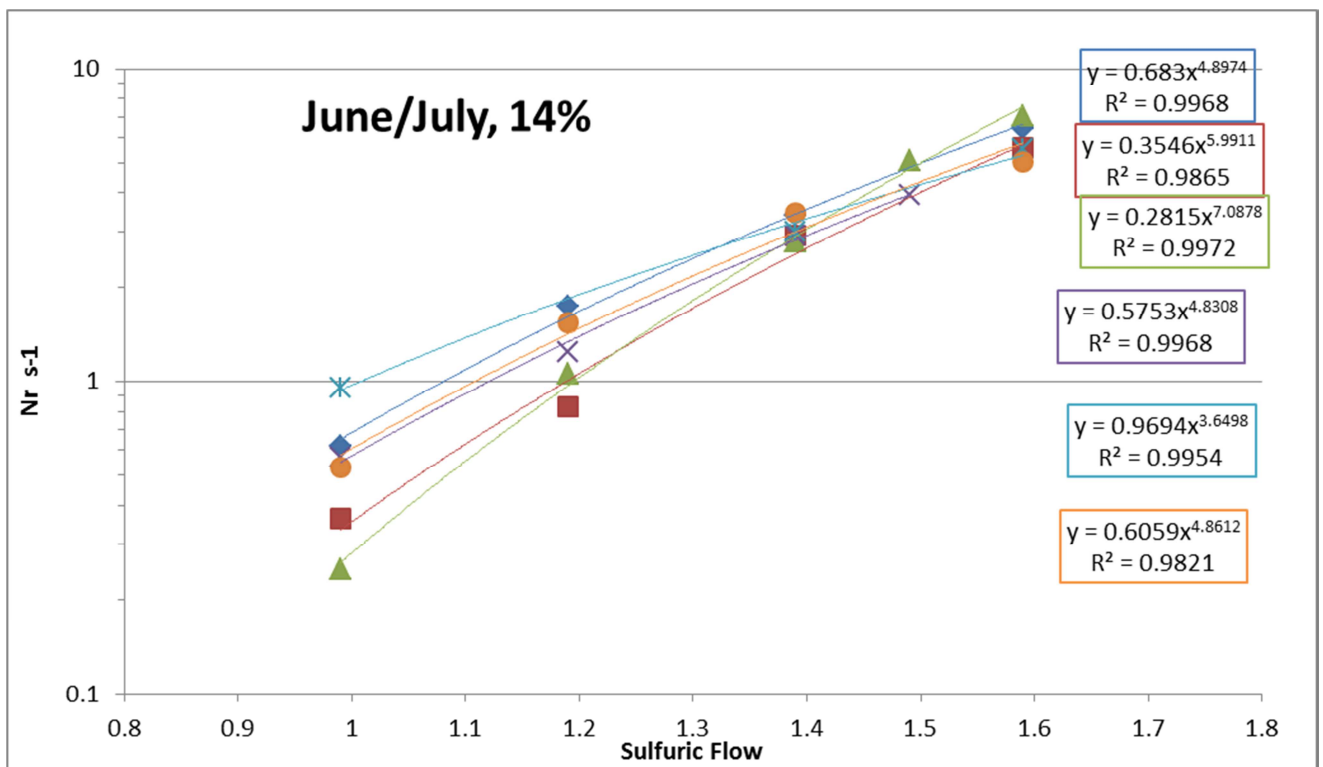
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### 7 **5 Representative data sets for Nr vs.both MS ion ratio and QA,**

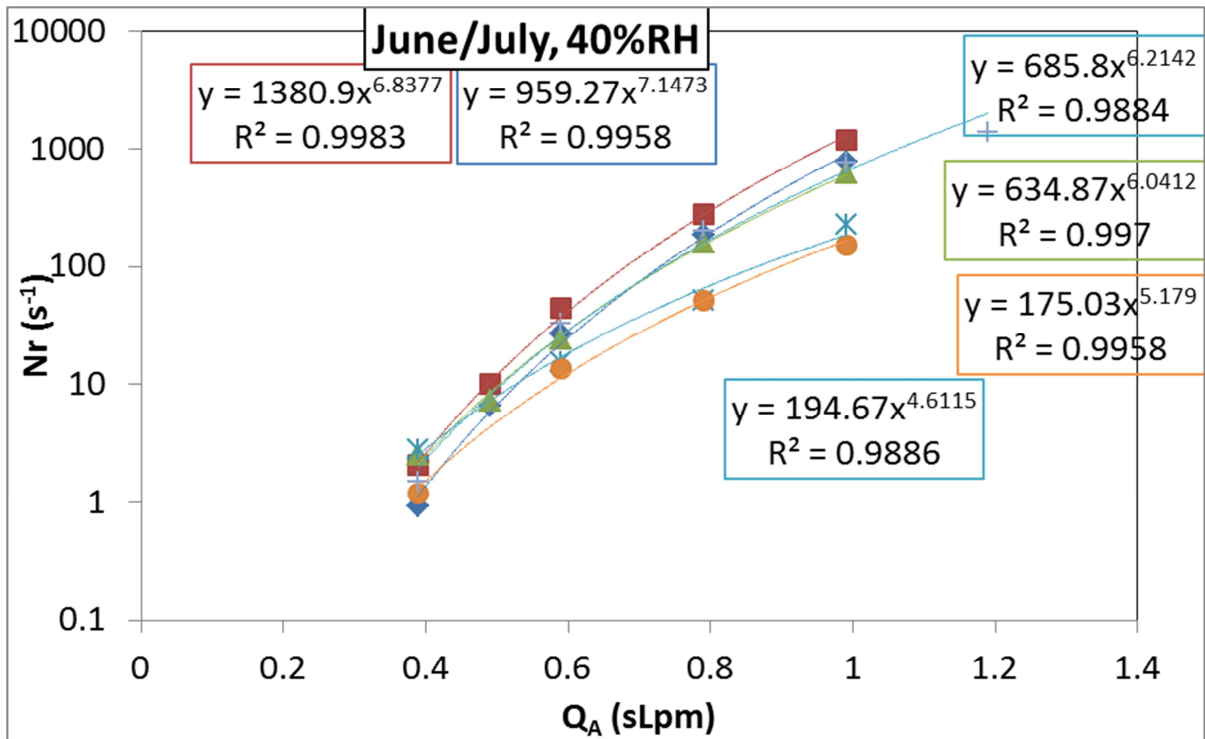
8 A plot representative of the scatter of particle count rate vs. ion ratio from negative ion AmPMS  
 9 is shown in Figure A4. This is all the data for the month of August, 2011. For June and July  
 10 2011, AmPMS was generally not operational and this data it plotted with Nr vs.  $Q_A$  (for  $Q_A$  1.5  
 11 sLpm and less) in FigA5: (a) 14 % RH and (b) 40% RH.

1  
2

3 Figure A4. Nr plotted versus MS ion ratio for a range of relative humidities: dark blue, 14%; red,  
4 20 %; green, 27%; orange, 40%; purple, 54%; turquoise, 68 %.



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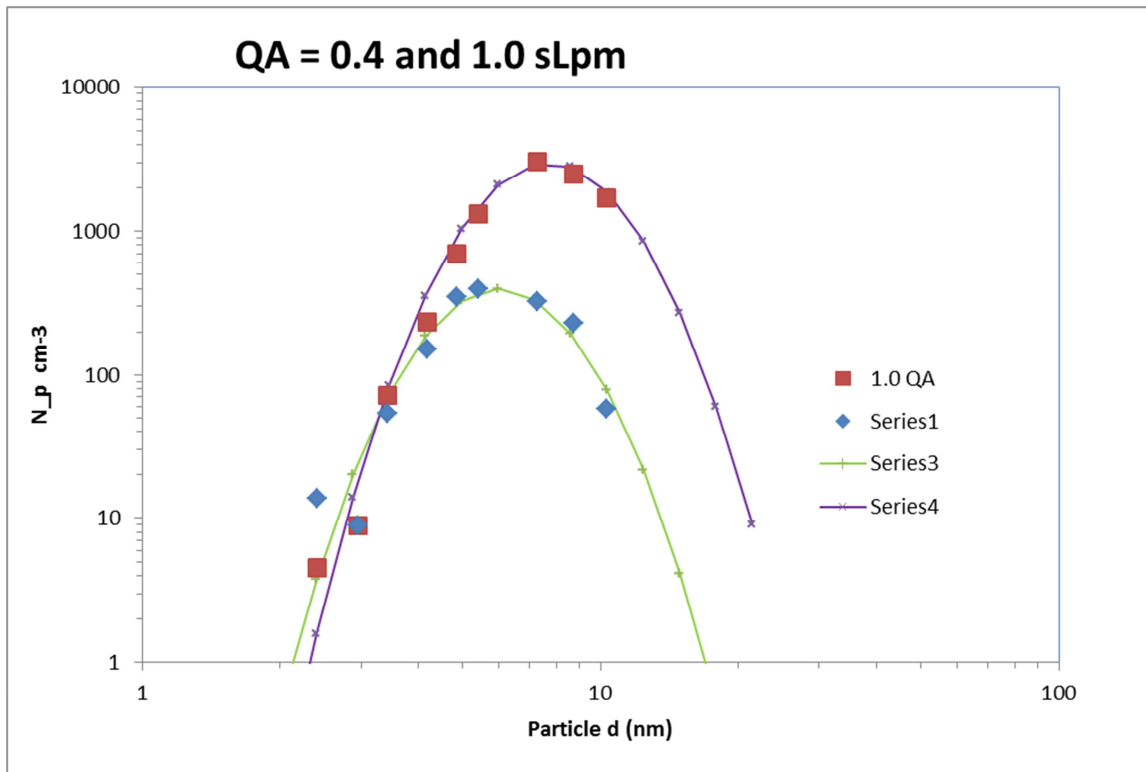
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2 Figure A5. Nr plotted versus  $Q_A$  at (a) 14 % rh and (b) 40% RH.

3

4 **6 Particle Sizes.**

5 The particle size distributions for  $Q_A = 1$  and 0.4 sLpm are shown in Figure A6. These two sets  
 6 of conditions represent typical and low sulfuric acid concentrations respectively. Particle  
 7 charging efficiency of Fuchs [1964] and long DMA loss equation of Birmili et al. [1997] were  
 8 applied. The log normal particle distributions are shown and have peak diameters of 6 and 7.7  
 9 nm and  $\ln\sigma$  was 0.25-to-0.3. Even though the charging of nanoparticles by the custom-built  
 10 charger has not been evaluated and the particle sampling lines may cause additional particle  
 11 losses, this measurement shows that the particle sizes are well above the detection threshold of  
 12 the instrument, about 2 nm in diameter.



1  
2 Figure A6. Particle size distributions for two different sulfuric acid levels. A rough conversion  
3 of the vertical axis,  $N_r$ , to  $dN/d\ln D$  can be done by multiplying by the ratio of sheath to aerosol  
4 flows [Stolzenburg and McMurry, 2008] (sheath flow was 7.2 sLpm and the aerosol flow was  
5 1.3 sLpm.)

6 As discussed in the text, Kuang et al. [2012] presented modified conditions for UCPCs where the  
7 saturator temperature of the UCPC can be increased, increasing the detection efficiency of  
8 nanoparticles of 2 nm diameter and smaller. To test if the particles detected here are of this size,  
9 different saturator temperatures were used at NBC. It was found that when the saturator  
10 temperature was increased (and condenser flow was increased), the particle number density did  
11 not change, however the pulse heights (i.e., channel number from Maestro) decreased. The pulse  
12 heights correspond to the size of the particles after growth with butanol, which did not affect the  
13 detected number of particles. This observation that the temperature of the saturator has no direct  
14 effect on the number density of particles that are detectable indicates that they are likely to be of  
15 a significantly greater size than the  $\sim 2$  nm diameter cut point that Kuang et al. presented.

16



## 1 **7 Ammonia and amine additions.**

### 2 **7.1 Effect of 10 ppqv of base.**

3 A decrease in the vapor pressure of  $\text{H}_2\text{SO}_4$  due to base would increase the stability of  $\text{H}_2\text{SO}_4$  in  
4 the critical cluster. This can be estimated using the E-AIM website (Clegg et al., 1998.) At 30 %  
5 RH and a 0.3-to-1  $\text{NH}_4^+$  to sulfate ratio (suppressing formation of ammonium bisulfate) the  
6 equivalent  $\text{NH}_3$  and  $\text{H}_2\text{SO}_4$  mixing ratios at 1 atm total pressure are about 10 and 7 ppqv,  
7 respectively. Because this is close to that for  $\text{H}_2\text{SO}_4$  vapor over neat  $\text{H}_2\text{SO}_4\text{-H}_2\text{O}$  solution at 30  
8 % RH (9.7 ppqv), this level of ammonia would probably not significantly affect nucleation.  
9 With methyl amine (Ge et al. 2011b) in the  $\text{H}_2\text{SO}_4\text{-H}_2\text{O}$  calculations, a one to one mole ratio of  
10 methyl amine to sulfuric acid at 30 % RH gives equivalent mixing ratios (1 atm total pressure) of  
11 2.4 ppqv for  $\text{H}_2\text{SO}_4$  and ~10 ppqv for methyl amine. Note: in the current implementation there  
12 are important assumptions regarding the amine's activity coefficients in sulfuric acid solutions  
13 (S. Clegg, 2011, private communication.) Nonetheless, the suppression of  $\text{pH}_2\text{SO}_4$  due to base is  
14 likely to be less in small clusters than for bulk solutions, and therefore only a modest effect on  
15 particle formation is expected due to the presence of 10 ppqv levels of  $\text{NH}_3$  while a significant  
16 effect for methyl amine at 10 ppqv levels cannot be ruled out.

### 17 **7.2 Other experimental considerations.**

18 The ~30 pptv level of amine added at the top port gave extremely high  $N_r$  for  $Q_A=1$  such that  
19 live time was reduced to essentially 0 and thus  $N_p$  could not be reliably monitored. For the base  
20 addition experiments therefore, the  $\text{N}_2$  flow over the bulk sulfuric acid was set to 0.4 sLpm for  
21 these 27 % RH measurements: this being the lowest sulfuric acid level used in any neat  
22 experiment (i.e., at 40 % to 68 % RH.)

23 Different addition methods (for example, 1.7 mm ID vs. 4 mm ID inlet tubes) resulted in  
24 significantly different  $N_r$  for nominally the same amine mixing ratios. The variability here was  
25 most likely due to how well the base was mixed into the main flow: a smaller ID tube has a  
26 stronger jet, which can go across the flow reactor and interact rapidly with the wall. This was  
27 verified in an experiment where a constant amount of methyl amine was introduced at the bottom  
28 of the flow reactor with varying amounts of  $\text{N}_2$  flow through the inlet. The measured amine  
29 concentration of 3 to 17 pptv with AmPMS depended on inlet tube flow rate as it varied from 10  
30 to 150 STP  $\text{cm}^3/\text{min}$ ; above ~ 40 STP  $\text{cm}^3/\text{min}$  it decreased strongly. The maximum observed

1 level of ~17 pptv is consistent with the calculated amount added, 25 pptv. Amine and ammonia  
2 addition and calibrations will be discussed in forthcoming papers (Panta et al., Carlson et al.,  
3 *manuscripts in preparation.*)  
4

## 5 **8 Previous work on amines/ammonia.**

6 Enhancement factors (EF) for ammonia and amines are convenient for quantifying and reporting  
7 their effects on nucleation. It is defined as the ratio of particles formed in the presence of added  
8 base to that in the absence of added base.

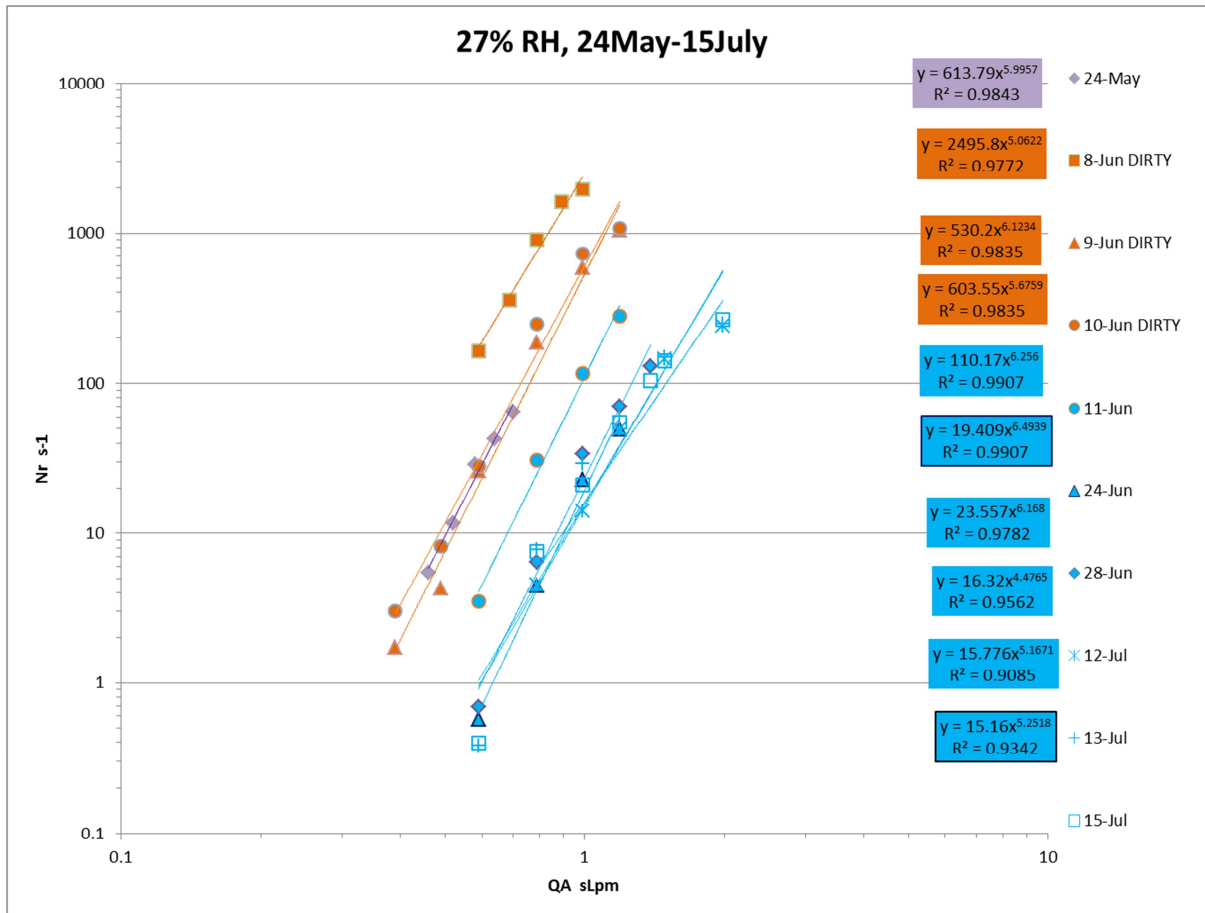
9 For NH<sub>3</sub> for example, Kirkby et al. [2011] report EF of ~100 for 70 pptv NH<sub>3</sub> (6 pptv H<sub>2</sub>SO<sub>4</sub> and  
10 38 % RH); Ball et al. [1999] show an EF of ~20 for an estimated NH<sub>3</sub> of ~3 pptv (+200/-67 %) at  
11 15 % RH and ~1000 pptv H<sub>2</sub>SO<sub>4</sub>; Berndt et al. [2010] report EFs up to 100 for 50000 pptv at low  
12 RH but less than 10 at 47 % RH. Benson [2010, 2011] report EF of 10 or less for 20000 pptv for  
13 RH values of 15 % and higher. These values are much lower than the ~ 10<sup>3</sup> to 10<sup>5</sup> values  
14 reported here for 3 to 45 pptv, respectively, for ~ 200 pptv [H<sub>2</sub>SO<sub>4</sub>]<sub>NZ</sub>. The differences of the  
15 present results with Ball et al. can be explained because of differing H<sub>2</sub>SO<sub>4</sub> levels; at lower  
16 H<sub>2</sub>SO<sub>4</sub> EF due to NH<sub>3</sub> will increase according to theory (Coffman and Hegg). The studies that  
17 used very large ammonia levels that saw very low EFs could be due to the presence of  
18 contaminants in their system: as discussed in the text and by Kirkby et al. [2011] and Benson et  
19 al. [2011].

20 Comparisons of the present measurements to the predictions for ammonia's effect on nucleation  
21 seem to indicate that the predictions either overestimate nucleation rates or EFs. The Coffman  
22 and Hegg [1995] predictions show EFs of ~100 and 1000 for 1 and 5 pptv respectively (for 75 %  
23 RH and 200 pptv H<sub>2</sub>SO<sub>4</sub>) however nucleation rates are predicted to be ~10<sup>10</sup> to 10<sup>15</sup> cm<sup>-3</sup> s<sup>-1</sup>.  
24 Korhonen et al. [1999] suggest an EF of ~ 10<sup>14</sup> at 2 pptv (52 % RH and 109 H<sub>2</sub>SO<sub>4</sub>) and J = 10<sup>5</sup>  
25 cm<sup>-3</sup> s<sup>-1</sup> and Napari et al. [2002] an EF of 10<sup>8</sup> for 2 pptv (using 0.1 pptv as the binary nucleation  
26 rate) with J = 10<sup>4</sup> cm<sup>-3</sup> s<sup>-1</sup>. The enhancement factor reported here is in better agreement with the  
27 theoretical treatment of Coffman and Hegg [1995] however the measured nucleation rate of 5  
28 cm<sup>-3</sup> s<sup>-1</sup> is very much lower (a factor of 10<sup>9</sup> or greater) than they predict. Although the EF of  
29 Korhonen et al. and Napari et al. deviate significantly from the current measurement, their  
30 predicted rates are somewhat closer, factors of only 10<sup>3</sup>-10<sup>4</sup> too large.

31

## 1 9 Contamination Episode.

2 For a period of time there was an unknown contaminant in the system, evidenced by a sharp rise  
 3 in particle numbers, to almost uncountable levels for periods of tens of minutes during heating of  
 4 suspected contaminated lines. To investigate further the effect this contaminant had on the  
 5 experiment, several power dependencies were taken at 27% RH while particle numbers remained  
 6 above normal NBC. They decreased day after day as the contaminant was slowly eliminated  
 7 from the system, and normal levels for NBC were achieved in about a ten days. While particle  
 8 numbers were high and as they decreased, the power dependency did not vary (Figure A7). It is  
 9 concluded that the unknown contaminant “X” changed only the total number of particles, not the  
 10 power dependency on  $H_2SO_4$ , and by extension the number of  $H_2SO_4$  in the critical cluster. The  
 11 mass spectrometer system was not operational for most of this episode.



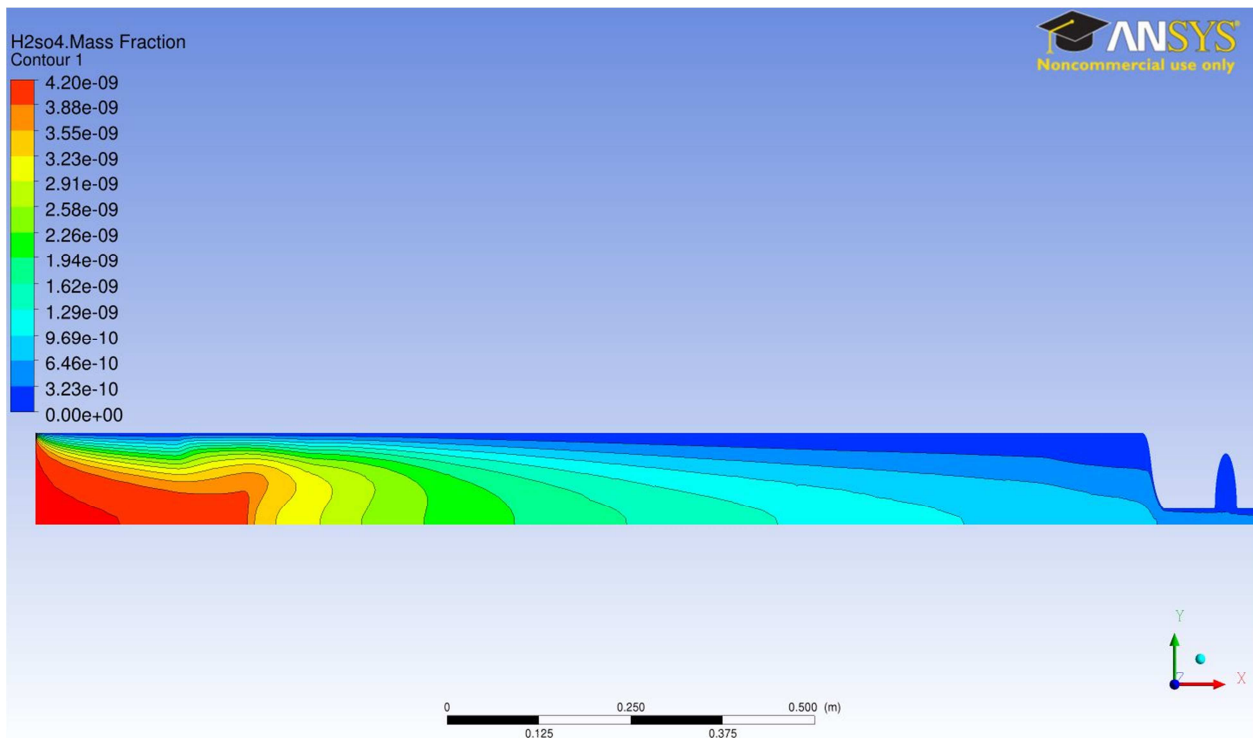
12  
 13 Figure A7. Nr and power dependencies at 27% RH. During contamination episode. Data for  
 14 May 24th, June 8th to 11th all show enhanced levels of particle number but power dependencies  
 15 were not appreciably affected.

16

1 **10 Computational Fluid Dynamics: [H<sub>2</sub>SO<sub>4</sub>]<sub>NZ</sub> versus measured [H<sub>2</sub>SO<sub>4</sub>].**

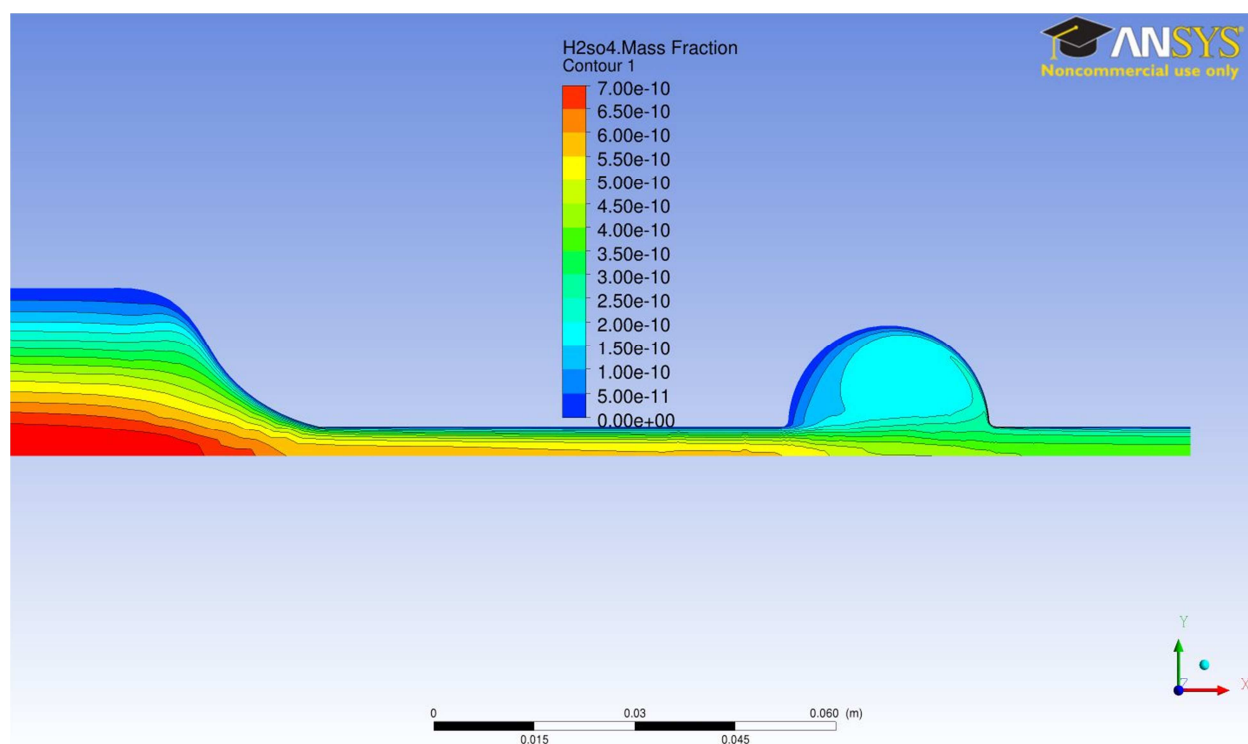
2 Shown in Figure A8 and A9 are contour plots of the mass fraction of H<sub>2</sub>SO<sub>4</sub> in a 2D simulation  
 3 of the flow reactor. The diffusion coefficient for H<sub>2</sub>SO<sub>4</sub> in N<sub>2</sub> was taken from Hanson and Eisele  
 4 [2000]. Thermal properties of the gas mixtures are very close to those used by Herrman et al.  
 5 [2010]. A complete description of the model is being prepared (Panta et al., [2012], manuscript  
 6 in preparation.)

7



8

9 Figure A8. Mass fraction contours of H<sub>2</sub>SO<sub>4</sub>. Axis of symmetry is at the bottom, vertical  
 10 coordinate is multiplied by ten. Nucleation zone is about 1/3 down the tube with an average  
 11 mass fraction of  $2 \times 10^{-9}$  for H<sub>2</sub>SO<sub>4</sub>.



1  
2 Figure A9. Blowup of mass spectrometer detection region in the middle of the small sphere of  
3 radius 1.5 cm. Average  $\text{H}_2\text{SO}_4$  mass fraction is about  $3 \times 10^{-10}$  in the ion drift region.

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## 8 References

9 Clegg, S. L., Brimblecombe, P., A. S. Wexler (1998) A thermodynamic model of the system  $\text{H}^+\text{-NH}_4^+$ -  
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12 Eisele, F.L., and Tanner, D. J.: Measurement of the gas phase concentration of  $\text{H}_2\text{SO}_4$  and methane  
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