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Derivation of the stoichiometric coefficient of water (v_w) to account for water uptake by atmospheric aerosols

S. Metzger¹, B. Steil¹, J. E. Penner³, L. Xu³, and J. Lelieveld^{1,2}

¹Max Planck Institute for Chemistry, Mainz, Germany ²Energy, Environment and Water Research Centre, The Cyprus Institute, Nicosia, Cyprus ³Department of Atmospheric, Oceanic and Space Science, University of Michigan, Ann Arbor, Michigan, USA

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Correspondence to: S. Metzger (swen.metzger@mpic.de)

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Abstract

In this work we derive the effective stoichiometric coefficient of water (v_w), introduced by Metzger and Lelieveld, 2007 (ML07), from first principles. We give examples of the application of v_w in CPU efficient computations of the Deliquescence Relative Humid-

⁵ ity (DRH) and the water uptake of atmospheric aerosols, being important parameters in atmospheric chemistry and climate modeling. We show that the application of v_w in a gas/liquid/solid aerosol equilibrium partitioning model (EQSAM3) leads to results that are in excellent agreement with those of widely used thermodynamic (reference) models (E-AIM and ISORROPIA2) for various single salt solutions (NaCl, NH₄NO₃, (NH₄)₂SO₄, NH₄HSO₄, NaHSO₄) and the corresponding mixed solutions (including (NH₄)₃H(SO₄)₂ and Na₃H(SO₄)₂), notwithstanding the distinct different theoretical and numerical concepts on which these models are based.

1 Introduction

Metzger and Lelieveld, 2007 (ML07) introduced the effective stoichiometric coefficient ¹⁵ of water v_w in analogy to the stoichiometric coefficient of solutes to consistently account for the amount of water that is consumed during the hydration of solutes. This complements the traditional physical chemistry methods, considering that the amount of water is not normally considered in detail in the classical equilibrium thermodynamics based on chemical potentials and inferred activity coefficients. The use of v_w can have the ²⁰ important advantage of decreasing CPU requirements by efficiently computing comprehensive aerosol equilibrium thermodynamics in large-scale models of the atmospheric environment. However, the scientific concept was questioned in the public discussion of the application paper of Xu et al. (2009). To underscore that the new concept of

 $v_{\rm w}$ is scientifically sound and useful, we derive the effective stoichiometric coefficient of water ($v_{\rm w}$) from first principles. Moreover, we present results from a comparison of our Equilibrium Simplified Aerosol Model 3, EQSAM3 (ML07), applying $v_{\rm w}$, with the 10, 8165-8188, 2010

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reference thermodynamic models E-AIM (Wexler and Clegg, 2002) and ISORROPIA2 (Fountoukis and Nenes, 2007), the latter used in atmospheric chemistry-transport models.

In Sect. 2 we derive v_w and apply it in Sect. 3, in which we also provide example s calculations and present a model inter-comparison. We conclude in Sect. 4 with a brief summary and the context of the underlying concepts, while the key equations on which EQSAM3 is built and that are relevant for our applications are summarized in the appendix.

2 Derivation of v_w

Let us consider the following experiment, adding a solute to pure water. When the so-10 lution becomes saturated any excess of the solute will not dissolve and precipitate from the solution. The critical mass of the solute $m_{\rm s(solid)}$ [kg] that yields a saturated solution is related to the water mass m_w^o [kg], by the mass fraction solubility, which is defined as $w_{\rm s}[-]=m_{\rm s(solid)}$ [kg]/ $(m_{\rm s(solid)}$ [kg]+ $m_{\rm w}^{\rm o}$ [kg]). Considering for instance sodium chloride (NaCl_(cr)), where $w_{s(NaCl)}$ =26.47 [%] (at T=25 °C), a (dry=solid=crystalline) maximum 15 mass of $m_{s(solid)}=0.36$ [kg] can completely dissolve in a mass $m_w^o=1$ [kg] of pure water. Alternatively, if we consider 1 mole of NaCl_(cr), a mass of $m_{s(solid)} = n_s^{sat} M_s = 58.44$ [g] can dissolve in a mass $m_w^o = 1000 \text{ [g]} / n_s^{\text{sat}} = 162.33 \text{ [g]}$ of pure water. With these mass ratios the solution is saturated. n_s^{sat} denotes the number of moles of solute at saturation and corresponds to the solubility mass fraction w_s [-], which is the central parameter. Note 20 that we consider here the special case of a saturated solution in order to be able to derive v_{w} . However, once v_{w} is known, its use is not restricted to a saturated solution as it will be shown below.

The number of "free" water molecules decreases during dissolution, while the total ²⁵ water mass does not change, since some of the water molecules are "consumed" by

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the solute, either bound to the solute as a hydration shell, or by processes such as hydrolysis.

To describe this amount of "consumed" (bound) water (i.e. solvent) molecules, expressed as an equivalent of chemical stoichiometry, i.e. as a molar change, Metzger and Lelieveld (2007) (ML07) have introduced the symbol v_w , the "stoichiometric" coefficient of water. Note that v_w is analogous to the stoichiometric coefficient of the solute v_s , used in chemistry to express in how many moles an ion-pair can dissociate. For instance, strong electrolytes such as NaCl_(cr) dissociate practically completely in water so that 1 mole of NaCl_(cr) yields 1 mole of Na⁺_(aq) and 1 mole of Cl⁻_(aq), thus 1 mole of dry (crystalline) solute yields $v_s=2$ moles ions of electrolyte in solution.

Note that the stoichiometric coefficients (constants) v_w and v_s are dimensionless (scalars), and scale the number of moles of solute (and solvent) volume rather than e.g. adding (or subtracting) a number of moles or volume. The masses of the solute and the solvent do not change during dissolution and dissociation; only volumes change because the number of moles changes due to partial or complete dissociation. It is this proportionality that enables us to derive v_w .

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Since many solutes do not dissociate completely, we will use in the following the symbol v_w to distinguish between the fraction of water that is associated with an undissociated solute, and $v_w \pm$ for an \pm -ion-pair, e.g. salt solute, that effectively dissociates

- ²⁰ into v_e^{\pm} ions, i.e. v_e^{+} cations and v_e^{-} anions, with $v_e \pm = v_e^{+} + v_e^{-}$ and $v_w \pm = v_w^{+} + v_w^{-}$. Thus, the stoichiometric coefficient of water v_w^{\pm} expresses the fraction of water that is needed (e.g. for hydration) for each mole of solute to effectively dissociate into v_e^{+} cations and v_e^{-} anions. We can derive the stoichiometric coefficient of water v_w^{\pm} by considering for our experiment an osmosis system according to ML07. In a Pfeffer cell (Pfeffer, 1887),
- with two compartments expandable in height (with equal surfaces), the volumes can expand by exerting different pressures. The pressure difference is merely the result of solute dissolution and potential dissociation that causes the volume expansion and the consequent hydrostatic counter-pressure. A schematic is given in Fig. 1.

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Assume that both compartments are filled with a certain mass of pure water that corresponds to the saturation of 1 mole of solute (e.g. of NaCl_(cr) with the values given above), and that these volumes are separated through a membrane permeable only for water molecules but not for the solute molecules, independently whether these are

- ⁵ dissociated (hydrated) or not. Thus, adding e.g. the pure (crystalline) solute NaCl_(cr) to one (e.g. the left) compartment yields a concentration change (number of moles per volume) and a volume expansion, leading to two different height changes, Δh_{sol} and Δh_{w}^{o} , due to the number of v_{e}^{\pm} moles in which the solute effectively dissociates and due to v_{w}^{\pm} , the amount of water consumed during dissolution/dissociation.
- The volume changes due to (1) the added mass of the solute, and (2) due to the amount of water required to dissolve and/or dissociate the solute, and bound to the solute ions as a hydration shell. This volume change causes a flow of water through the membrane (here from right to left) to compensate for the amount of water bound to the ions of the dissociating solute, until all solute mass is dissolved and the solution (left compartment) is saturated.

At saturation the system is in equilibrium again with maximum changes in the volume of both compartments, ΔV_{sol} and ΔV_w^o , respectively. Note that the volume of the right (pure water) compartment merely changes because of a flow of water through the membrane (osmotic drag). This flow stops when the hydrostatic counter pressures, Δp_{sol} and Δp_w^o , that build up due to the volume expansion compensate the osmotic pressures, i.e. $\Pi_{sol} = \Delta p_{sol}$ and $\Pi_w = \Delta p_w^o$ (Fig. 1).

Thus, we distinguish between two volume changes:

1. A change of the pure water (reference) volume that provides information about the water amount that hydrates the solute, ΔV_w^o . Note that this is valid, both, when the water molecules condense from the gas phase (shown below based on the classical gas-solution analogy), thus changing an initial volume of water vapor, and when they are supplied by a reservoir such as the right compartment of Fig. 1.





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2. A change in the volume of the solution due to the additional solute and hydration, $\Delta V_{\rm sol}.$

Note that the volume change for (1) needs to be considered for pure water only, while the volume change (2) consists of three parts:

- ⁵ 1. A change of the volume due to the added mass of solute, $\Delta V_{s(dry)}^{o}$; this volume corresponds to the initial mass of the solute that does not change by the dissolution of a solute, e.g. due to solute hydration (which is not a chemical reaction);
 - 2. A change of the volume $\Delta V_{s(diss)}^{\pm}$ due to solute dissociation, expressed by the effective stoichiometric coefficient of the solute, $v_e^{\pm} = v_e^{+} + v_e^{-}$; (one mole of a single charged electrolyte (ion-pair) such as NaCl yields one mole, $v_e^{+} = 1$, of the of the cation $(Na_{(aq)}^{+})$ and one mole, $v_e^{-} = 1$, of the anion $(Cl_{(aq)}^{-})$. Thus, for NaCl at equilibrium, one mole of dry substance expands in volume into two moles in solution, $v_e^{\pm} = 2$.
 - 3. A change of the volume $\Delta V_{s,w(hyd)}^{\pm}$ due the amount of water that is bound to the solute ions, which drives the dissolution and potential dissociation, $v_w^{\pm} = v_w^{+} + v_w^{-}$.

The total volume change $\Delta V = \Delta V_{sol} + \Delta V_w^o$ is determined by the volume change of the solution $\Delta V_{sol} = \Delta V_{s(dry)}^o + \Delta V_{s(diss)}^{\pm} + \Delta V_{s,w(hyd)}^{\pm}$ and of pure water $\Delta V_w^o = \Delta m_w^o / \Delta \rho_w^o$. Thus, we can consider two associated changes in energy (of the solution and of pure water), i.e. the work done by the two compartments due to the volume changes, ΔV_{sol} and ΔV_w^o against the associated pressure changes ΔP_{sol} and ΔP_w^o , at temperature *T*,

i.e. $\Delta E_{sol}^{\pm} = \Delta (P_{sol} V_{sol})$ and $\Delta E_{w}^{o} = \Delta (P_{w}^{o} V_{w}^{o})$, for which we postulate:

 $\Delta E[\mathbf{J}] = \Delta E_{w}^{o} - \Delta E_{sol}^{\pm}[\mathbf{J}].$

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Let $\Delta E = \Delta(PV)$ denote the total change in energy (with potential changes in the heat content), i.e. the work by both compartments due to the effective dissociation of the



(1)

solute into v_e^{\pm} moles (considering one mole solute) and the changes in the pure water compartment due to v_w^{\pm} consumed moles of water.

At equilibrium $\Delta E = 0$, so that Eq. (1), expressed in terms of partial volume and pressure changes, dE = d(PV) = 0, yields with the product integration, d(PV) = dPV + dVP:

$$5 \quad dPV[J] + dVP[J] = 0.$$

Dividing Eq. (2) by $P[N/m^2]$ and $V[m^3]$ further yields (with $[J=Nm]=[Pa=N/m^2]$):

$$\frac{dP[N/m^2]}{P[N/m^2]} + \frac{dV[m^3]}{V[m^3]} = 0.$$
(3)

Integration over all partial changes in pressure and volume yields:

$$\int_{P}^{(\Delta P)} \frac{dP}{P} + \int_{V}^{(\Delta V)} \frac{dV}{V} = \ln\left(\frac{\Delta P}{P}\right) + \ln\left(\frac{\Delta V}{V}\right) = 0,$$
(4)

Equation (4) can be re-arranged into:

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$$\ln\left(\frac{\Delta P}{P} \cdot \frac{\Delta V}{V}\right) = 0,$$
(5)

with ΔP [Pa] and ΔV [m³] the total changes (relative to the initial state) in pressure and volume that correspond to the two shaded areas in Fig. 1 and *P* and *V* the equilibrium state after the addition of the solute.

These changes can be expressed in terms of the total mass change of the solution, $\Delta m[kg]$, caused by the addition of the solute mass $m_{s(solid)}[kg]$ to the left compartment, i.e. $\Delta m[kg]=m_{s(solid)}[kg]$. Adding $m_{s(solid)}[kg]$ causes a redistribution of the initial pure water mass $\Delta m_w^o[kg]$ from the right compartment; the water mass is conserved. Further, the gravitational acceleration $g[m/s^2]$ acts on both mass changes (of the solution and of the pure water).

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(2)

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We can therefore express the total pressure change $\Delta P[Pa]$ in terms of a change in the resulting total gravitational force ΔF_g [N]= $\Delta m[kg] \cdot g[m/s^2]$ that acts on both surface areas, $2A[m^2]$, i.e. $\Delta P[Pa] = \Delta F_g[N]/(2A[m^2])$. Analogously, we can express the resulting (total) pressure and volume of the solution at equilibrium in terms of the total mass of the solution, $m[kg] = m_w^o[kg] + m_{s(solid)}[kg]$ as $P[Pa] = m[kg] \cdot g[m/s^2] A^o[m^2]$ and $V[m^3] = A^o[m^2] \cdot h[m]$; with $A^o[m^2]$ the total surface area, and h[m] an associated height of the solution that corresponds to both compartments. If we express the total volume change as a change in height of both compartments $\Delta V[m^3] = 2A[m^2] \cdot \Delta h[m]$, with $\Delta h[m] = \Delta h_{sol}[m] + \Delta h_w^o[m]$, we can express Eq. (5) in terms of a dimensionless ratio of potential energies, i.e. the change relative to the potential energy of the solution:

$$\ln \left(\frac{\Delta m \cdot g}{2A} \cdot \frac{A^{\circ}}{m \cdot g} \cdot \frac{\Delta V}{V}\right) = \ln \left(\frac{\Delta m}{m} \cdot \frac{A^{\circ}}{2A} \cdot \frac{2A \cdot \Delta h}{A^{\circ} \cdot h}\right) = \ln \left(\frac{\Delta m}{m} \cdot \frac{\Delta h}{h}\right) = 0.$$
(6)

The total mass change $\Delta m = m_s$ of the system is related through the definition of solubility, $w_s = m_s/m$, to the associated change in the water mass, $\Delta m_w^o = w_s \cdot m_w^o$, by $\Delta m = \Delta m_w^o \cdot m_w^o / m_w$, with $m_w = m_w^o - \Delta m_w^o$ the remaining free water in the solution and the pure water compartment. The total mass of the system, $m = m_w^o + \Delta m$, can be additionally expressed as $m = m_w^o \cdot m_w^o / m_w$, so that the mass ratio of the total mass change to the total mass of the system can be expressed as $\Delta m/m = \Delta m_w^o / m_w^o = w_s$, and Eq. (6) yields:

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$$\ln\left(w_{\rm s}\cdot\frac{\Delta h}{h}\right) = 0. \tag{7}$$

²⁰ Since Eq. (7) depends on fractions rather than on the actual amounts of solute and water (due to w_s), we can consider molar changes to further express the change in height, Δh , relative to the height *h* that corresponds to the solution. Although both are not (yet) known, they depend (for molar changes) on the effective stoichiometric coefficients of the solute v_e^{\pm} and water v_w^{\pm} .





This becomes clearer by expressing the energy ratio of Eq. (5) in the terms of the ideal gas law, i.e. $\Pi \cdot V = \Delta n \cdot R \cdot T$, based on the gas-solution analogy according to van't Hoff (1887, 1897, 1901) and Einstein (1905). Note that this analogy was resolved after the historical dispute between van't Hoff and Rayleigh versus Kelvin and Gibbs, http://urila.tripod.com/evidence.htm).

Thus, if we consider the ratio of the two energy changes expressed in terms of the gas law:

$$\ln \left(\frac{\Pi_{\rm sol}}{\Pi_{\rm w}^{\rm o}}\right) = \ln \left(\frac{\Delta c_{\rm s} \cdot R \cdot T}{\Delta c_{\rm w}^{\rm o} \cdot R \cdot T}\right) = \ln \left(\frac{\Delta n_{\rm s} \cdot R \cdot T/V}{\Delta n_{\rm w}^{\rm o} \cdot R \cdot T/V}\right) = \ln \left(\frac{\Delta n_{\rm s}}{\Delta n_{\rm w}^{\rm o}}\right) = 0, \tag{8}$$

where $\Delta n_s = v_e^{\pm} \cdot n_s^{\circ}$ with $n_s^{\circ} = 1$ [mol] of (dry) solute that has been added to a corresponding mass of pure water to satisfy w_s [-] as described above, which yields an associated change of the pure water mass $\Delta m_w^{\circ} = \Delta n_w^{\circ} M_w = w_s \cdot m_w^{\circ}$; $\Delta c_s = \Delta n_s / V$ and $\Delta c_w^{\circ} = \Delta n_w^{\circ} / V$ are concentration changes, with V being the total volume of the system, so that the term *RT/V* cancels out. Note that these "energy changes" might be expressed instead as the osmotic pressures for each component, since *P* is not an energy.

¹⁵ On the other hand, Eqs. (7) and (8) are only satisfied if $w_s = \frac{h}{\Delta h}$ and $\Delta n_s = \Delta n_w^o$, since then the natural logarithm becomes zero, i.e. ln(1)=0, as required by Eqs. (7) and (8).

The height *h* of the solution is an average height of $\Delta h_{sol}[m]$ and $\Delta h_w^o[m]$ and proportional to both, v_e^{\pm} and to half of the total change $\Delta h[m]$, if divided by a certain scaling factor, i.e. $h = v_e^{\pm} \cdot \Delta h/(2h')$, so that the height ratio $\frac{\Delta h}{h}$ of Eq. (7) can be expressed as ²⁰ $\frac{\Delta h}{h} = \frac{2}{v_e^{\pm}} h'$, where the factor of 2 comes from the fact that v_e^{\pm} caused a total volume change of $2A\Delta h$.

Let us assume that this dimensionless scaling height \dot{h} has a density, volume and surface contribution, i.e. $\frac{\Delta V_{s,w(hyd)}^{\pm}}{\Delta A'} = \frac{\dot{h'} \cdot \dot{h'} \cdot \dot{h'}}{\dot{h'} \cdot \dot{h'}} \cdot \frac{1}{\dot{h'}^{-v_w^{\pm}}} = \frac{\dot{h'}^3}{\dot{h'}^{2-v_w^{\pm}}} = h^{'3/(2-v_w^{\pm})}$, which can be attributed to the binding of water molecules, with $\dot{h'}^{-v_w^{\pm}}$ an associated height of the bound water molecules. However, a density contribution remains as the final result of the mass and

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volume changes of Eq. (5), in accordance with Archimedes' principle, so that a mass ratio in hydrostatics can be expressed in terms of a density ratio (http://en.wikipedia. org/wiki/Buoyancy).

Therefore, we assume the dimensionless scaling height h' being an effective change 5 in density $\frac{\Delta h}{h} = \frac{2}{v_{a}^{\pm}} \cdot h' = \frac{2}{v_{a}^{\pm}} \cdot \frac{\rho_{w}^{o(2-v_{w}^{\pm})/3}}{\Delta \rho_{w}^{o}}$, relative to a unit change in the pure water density; expressed in SI-units, $\Delta \rho_{\rm w}^{\rm o} = 1 \left[\text{kg/m}^3 \right]$, where we interpret $\frac{2}{v_{\star}^{\circ}} \cdot \frac{\rho_{\rm w}^{o(2-v_{\rm w}^{\pm})/3}}{\Delta \rho_{\rm w}^{\circ}} = \frac{m_{\rm w}^{\circ}}{\Delta m_{\rm w}^{\circ}} = 1/w_{\rm s}$ as the reciprocal and dimensionless (although the ratio of density expressions might not be dimensionless) mass change to satisfy Eq. (7).

Equation (7) thus yields:

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$$\ln \left(w_{\rm s} \cdot \frac{2}{v_{\rm e}^{\pm}} \cdot \rho_{\rm w}^{o(2-v_{\rm w}^{\pm})/3} \right) = 0.$$
 (9)

And Eq. (9) can be rearranged into

$$\ln\left(\frac{2}{v_{\rm e}^{\pm}}w_{\rm s}\right) + (2 - v_{\rm w}^{\pm})/3 \cdot \ln\left(\rho_{\rm w}^{\rm o}\right) = 0.$$
(10a)

With the fractional density of pure water in SI-units, $\rho_w^o = 1000 \left[\text{kg/m}^3 \right]$ at $T_o = 277.15$ [K], we can express the dimensionless density ratio as $\ln(\rho_w^0) = \ln(1000) = 3\ln(10)$, so that we can write:

$$\ln\left(\frac{2}{v_{\rm e}^{\pm}}w_{\rm s}\right) + (2 - v_{\rm w}^{\pm}) \cdot \ln(10) = 0, \tag{10b}$$

and upon re-arranging, we can finally solve for v_w^{\pm}

$$v_{\rm w}^{\pm} = \ln \left(\frac{2}{v_{\rm e}^{\pm}}w_{\rm s}\right) / \ln (10) + 2.$$
 (10c)

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In accordance with the gas-solution analogy the value $R \cdot T_o = 2.304$ [KJ] is close to $\ln(10) = 2.303$ assuming a temperature for which pure water has a density of unity, $\rho_{w(pure)}^o = 1000$ [kg/m³], i.e. $T_o = 277.15$ [K], so that we can alternatively write:

$$v_{\rm w}^{\pm} = \ln \left(\frac{2}{v_{\rm e}^{\pm}}w_{\rm s}\right)/2.304 + 2.$$
 (10d)

⁵ Furthermore, the ratio of $\ln\left(\frac{2}{v_e^{\pm}}w_s\right)/\ln(10)$ can be further reduced to the decadal logarithm, i.e. $\log_{10}\left(\frac{2}{v_e^{\pm}}w_s\right)$, so that Eq. (10c) can be alternatively expressed as

$$v_{\rm w}^{\pm} = \log_{10} \left(\frac{2}{v_{\rm e}^{\pm}} \cdot w_{\rm s} \right) + 2.$$
 (10e)

Finally, by dropping the \pm -index which indicates the \pm -ion-pair, we may write:

$$v_{\rm w} = v_{\rm w,o} + \log_{10} \left(\frac{2}{v_{\rm e}} \cdot 1000 \cdot w_{\rm s} \right),$$
 (10f)

with Eq. (10f) being Eq. (19) of ML07, and their $v_{w,o} = -1$ indicating that each mole of solute "consumes" $\log_{10} \left(\frac{2}{v_e} \cdot 1000 \cdot w_s\right)$ moles of initially "free" water.

3 Application of v_w

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3.1 Calculations of v_w

With the above equations we can, for example, calculate v_w for the following compounds:

(A) NaCl,
$$w_s = 0.2647$$
, $v_e^{\pm} = 2$, $v_w^{\pm} = \frac{1}{2.303} \ln \left(\frac{2}{2}0.2647\right) + 2 = 1.423$.
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(B) NH₄NO₃,
$$w_s = 0.6805$$
, $v_e^{\pm} = 1.97$, $v_w^{\pm} = \frac{1}{2.303} \ln \left(\frac{2}{1.97} 0.6805\right) + 2 = 1.839$.

(C)
$$(NH_4)_2SO_4$$
, $w_s = 0.4331$, $v_e^{\pm} = 2.15$, $v_w^{\pm} = \frac{1}{2.303} \ln \left(\frac{2}{2.15}0.4331\right) + 2 = 1.605$.

Thus, these values (among other examples) based on Eq. (10c) are in agreement with those presented in Table 1a of ML07, based on Eq. (10f) i.e. their Eq. (19).

3.2 Comparison EQSAM3 with reference models

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In this section we present several examples for the application of v_w with respect to the DRH and the water uptake of atmospheric aerosols, being key parameters in atmospheric chemistry and climate modeling studies. Figure 2 presents the results of a model inter-comparison using the gas/liquid/solid aerosol equilibrium partitioning model EQSAM3 and the widely used and generally accepted thermodynamic models, E-AIM (Wexler and Clegg, 2002; http://www.aim.env.uea.ac.uk/aim/aim.php) and ISORROPIA2 (Fountoukis and Nenes, 2007).

Figure 2a–f show the results for various single salt solutions, i.e. NaCl, NH_4NO_3 , NH_4NO_3 [nmol], $(NH_4)_2SO_4$, NH_4HSO_4 , $NaHSO_4$, and Fig. 2g–h shows the results for the corresponding mixed solutions (including $(NH_4)_3H(SO_4)_2$ and $Na_3H(SO_4)_2$).

All solute concentrations were fixed to $1[\mu mol/m^3]$ except for Fig. 2d, where the solute concentrations were fixed to $1[nmol/m^3]$ to test the sensitivity against a different concentration. The aerosol water and the DRH predicted by EQSAM3 compare well with the predictions of E-AIM and ISORROPIA2 for all salt solutions. The only exception is the $1[nmol/m^3]$ case where ISORROPIA2 does not predict any NH₄NO₃. This is probably related to the equilibrium constant ($K_{eq(NH4NO3)}$) used for the NH₄NO_{3(s)}<==>NH_{3(g)}+HNO_{3(g)} equilibrium reaction, which prohibits the NH₄NO₃ formation due to its low value of 57.46[ppb²] in ISORROPIA2 (Fountoukis and Nenes, 2007). Note that the EQSAM3 version introduced in ML07 has been extended in this work by an option to account for $K_{eq(NH4NO3)}$ (exactly as used in ISORROPIA2); using 10, 8165-8188, 2010

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the temperature dependent *K*_{eq(NH4NO3)} yields the same result (not shown) as ISOR-ROPIA2, but differs from that of E-AIM. Note further that the DRH for the mixed solution is inferred from the same equations used to derive the DRH of single solutes (i.e. Eq. 21 and Sects. 4.1.5 and 4.1.9 of ML07; see also the summary of the EQSAM3 key equations given in the appendix) by using the mean values of the required thermodynamic parameters, i.e. the effective stoichiometric coefficients of the solutes and water of all single solutes in the mixed solution, their solubilities and molar masses. Although a few discrepancies occur at the phase transitions, the aerosol water uptake, which is central for our modeling purposes, is generally represented very accurately.

10 4 Discussion and conclusions

In this work we have detailed the concept of the effective stoichiometric coefficient of water (v_w), as introduced by ML07 to consistently account for the amount of water that is consumed during the hydration of solutes, in analogy to the stoichiometric coefficient of solutes. This concept has been questioned in the public discussion of an application paper by Xu et al. (2009), and we hope to have shown that this was unfounded.

- tion paper by Xu et al. (2009), and we hope to have shown that this was unfounded. The application potential has been corroborated by direct comparisons with the reference model E-AIM of Wexler and Clegg (2002). Our results indicate that our new method provides a valid alternative to traditional approaches in atmospheric equilibrium gas-aerosol partitioning modeling which are based on chemical potentials and inferred activity coefficients. The traditional solution algorithms require computationally
- comprehensive online or offline iterations (E-AIM and ISORROPIA-II, respectively) to compute the equilibrium composition of compounds in the solution.

The v_w -concept allows the gas/liquid/solid equilibrium partitioning of single or multiple charged electrolytes, including semi- or non-volatile compounds and partial dissociation of bi-sulfates, to be computed analytically, since the stoichiometric coefficient of water (v_w) contains a priori information of the water activity as it is based only on the so-





to mixed solutions may give insights into the basis of the so-called ZSR-relationship Zdanovskii-Stokes-Robinson (Stokes and Robinson, 1966), a widely used method in atmospheric modeling (including E-AIM and ISORROPIA2) to derive the water content of mixed solutions from the corresponding binary solutions upon the application of ⁵ empirical mixing rules.

Finally we note that the v_w -concept of ML07 goes back to Arrhenius' theory of partial dissociation (Arrhenius, 1887; Heyrovska, 1989), and van't Hoff's gas-solution analogy originally used to explain osmosis (van't Hoff, 1887). Interestingly, the work by van't Hoff on osmosis was initially disputed until Lord Rayleigh (1897) put van't Hoff's arguments on a firmer ground. One issue at that time was that Gibbs (1897) proposed an alternative analysis of the osmotic pressure in terms of chemical potentials, which has subsequently served as an essential element of textbooks about osmosis. Van't Hoff's and Rayleigh's original ideas were then disregarded in favor of theories making use of the Gibbs free energy and of chemical potentials. However, these theories must be

¹⁵ considered as equivalent in treating osmosis, and they do not provide the benefits of generality and rigor (http://urila.tripod.com/evidence.htm). Thus, based on the original ideas of Arrhenius, van't Hoff and Rayleigh, v_w builds on the concept of osmosis, analogously to the stoichiometric coefficients for solutes, to account on a molar basis for the amount of water consumed by hydration.

20 Appendix A

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Clarification of the EQSAM3 concept (ML07)

EQSAM3 solves the gas-liquid-solid partitioning analytically and non-iteratively upon calculation of the single solute concentrations from the compound's solubility and a newly introduced variable; the stoichiometric coefficient of water, v_w . This is a different approach compared to other equilibrium models, and previous EQSAM versions





(EQSAM, Metzger et al., 2002; EQSAM2, Metzger et al., 2006). The source code of EQSAM3 is available on request.

ML07 introduced v_w to represent the degree to which water is consumed or bound in processes such as solvation, hydration, hydrolysis or similar other processes that ⁵ consume water and which are associated with a chemical reaction. These processes are, apart from some exceptions (such as water chemically bound in minerals), usually neglected in the stoichiometrical notation of chemical reactions in solution, and hence, activity coefficients are needed. Instead, EQSAM3 does not require activity coefficients for non-volatile aqueous compounds. The use of v_w allows ML07 to deter-¹⁰ mine the amount of water associated with a dissolved solute without the use of activity coefficients.

EQSAM3 is based on 5 key equations, all of which are detailed in ML07, but a summary of each equation is given here for completeness. These equations are used to calculate:

- 1. The stochiometric coefficient of water
 - 2. The single solute molality (as a function of RH)
 - 3. The aerosol associated water mass (water uptake)
 - 4. The relative humidity of deliquescence (of single and mixed solutes)
 - 5. Activity coefficients (for semi-volatile species)
- ²⁰ These 5 key equations are outlined in this section.

A1 Stochiometric coefficient of water

EQSAM3 calculates the single solute concentrations from the compound's solubility and a newly introduced variable; the stoichiometric coefficient of water, v_w . ML07 introduced a relation for the dependence of v_w on the solubility:

$$v_{\rm w} = v_{\rm w,o} + \log (2/v_{\rm e} \times 1000 w_{\rm s}),$$



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(A1)

with w_s the solubility mass fraction, defined as mass of solute per total mass of the solution and with $v_{w,o} = -1$ indicating that each mole of solute "consumes" $\log_{10}\left(\frac{2}{v_e} \times 1000 w_s\right)$ moles of initially "free" water. Note that Eq. (A1) can be expressed in terms of an ±-ion-pair and the natural logarithm as:

with $v_{w,0}^{\pm}=2$ instead of $v_{w,0}=-1$, as it is derived in Sect. 2 from first principles.

A2 Single solute molality as a function of RH (water activity)

The introduction of the coefficient v_w allows generalization of the solute mole fraction and molality, which can be related to the solubility (ML07). Using the generalized ¹⁰ mole fraction instead of the (traditional) mole fraction has the advantage that we can directly express the single solute molality (of non-volatile compounds) as a function of RH without considering activity coefficients. In contrast, the (traditional) mole fraction and molality need to be corrected by activity coefficients to match measurements. The generalized mole fraction does not need such corrections.

¹⁵ The generalized mole fractions for solute and water at equilibrium are respectively expressed as

$$\tilde{x}_{\rm s} = v_{\rm e} n_{\rm s} / \left[v_{\rm w} n_{\rm w} + v_{\rm e} n_{\rm s} \right], \tag{A3a}$$

$$\tilde{x}_{w} = v_{w} n_{w} / [v_{w} n_{w} + v_{e} n_{s}].$$
 (A3b)

Equation (A3a, b) differ from their traditional definitions $x_s = n_s/[n_w + n_s]$ and $x_w = n_w/[n_w + n_s]$ only by the effective stoichiometric coefficients for the solute v_e and water v_w which account for solution non-ideality by partial or complete dissociation; n_s is the number of moles of solute that is dissolved in a solution with n_w the moles of solvent water.

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In accord with the traditional definition the sum of the generalized mole fractions yields unity, i.e. for a binary solution (one solute and water):

$$\tilde{x}_{\rm s} + \tilde{x}_{\rm w} = 1. \tag{A3c}$$

The activity of water in terms of the generalized mole fraction for water at equilibrium is

which can be expressed as

$$\tilde{x}_{w} = v_{w}n_{w}/[v_{w}n_{w} + v_{e}n_{s}^{o}] = 1/[1 + v_{e}n_{s}^{o}/v_{w}n_{w}] = RH,$$
(A4b)

and upon rearranging

$$n_{\rm s}^{\rm o}/n_{\rm w} = v_{\rm w}/v_{\rm e} \cdot (1/{\rm RH} - 1),$$
 (A5)

¹⁰ The single solute molality, $m_{\rm ss}$, is defined as the moles of solute per kilogram water, i.e.

$$m_{\rm ss} = 1000[g(H_2O)]/M_w[g/mol] \cdot n_s^o[mol]/n_w[mol] = 55.51 n_s^o/n_w[mol/kg(H_2O)],$$
 (A6)

where $55.51/n_w$ denotes the number of moles of water per kilogram and $M_w = 18.015[g/mol]$ is the molar mass of water; n_s^o denotes the initial num-¹⁵ ber of moles that effectively dissociates into $v_e n_s^o$ number of moles at equilibrium (saturation). Thus, the initial and non-equilibrium single solute molality, $m_{ss,sat}^{v_s^o} = n_s^o/n_w \cdot 55.51$ (with $v_s^o = 1$) yields at equilibrium the saturation molality $m_{ss,sat}^{v_e/v_w} = v_e/v_w n_s^o/n_w \cdot 55.51$, or the actually measured saturation activity, $a_{s,o}^{v_s^o} = a_{w(hyd),sat} = a_{ss,sat}^{v_e/v_w}$, with $n_s^o/n_w = m_{ss}^{v_s^o}/55.51 \Rightarrow v_e/v_w n_s^o/n_w = m_{ss,sat}^{v_e/v_w}/55.51$. Note that ²⁰ if $v_e/v_w \neq 1$ the units for the solute molality in these equations would not be balanced in the traditional and chemical potential based approaches, but this is ignored in this model. stoichiometric coefficient of water





Substitution in Eq. (A5) yields, by considering that

$$n_{\rm s}^{\rm o}/n_{\rm w} = m_{\rm ss}^{v_{\rm s}^{\rm o}}/55.51 \Rightarrow m_{\rm ss,sat}^{v_{\rm e}/v_{\rm w}}/55.51 = v_{\rm w}/v_{\rm e} \cdot (1/{\rm RH} - 1),$$
 (A7)

so that we can express Eq. (A6) in terms of RH and the effective stoichiometric coefficients for the solute v_e and water v_w , i.e.

$${}_{5} m_{\rm ss,sat} = \left[v_{\rm w} / v_{\rm e} \cdot 55.51 \cdot \left(1 / \rm{RH} - 1 \right) \right]^{v_{\rm w} / v_{\rm e}}.$$
(A8)

Equation (A8) is the basic formulation of ML07 (their Eq. 20) from which all further equations used in EQSAM3 can be expressed as a function of RH, v_e and v_w .

Note that $m_{ss,sat}^{v_e/v_w}$ directly follows from the example reaction:

$$v_{s}^{o} \text{NaCl}_{(cr)} + v_{w}^{o,\pm} \text{H}_{2} \text{O} \Leftrightarrow v_{e}^{\pm} \text{NaCl}_{(aq)}^{\pm} \cdot v_{w}^{\pm} \text{H}_{2} \text{O}$$

$$v_{e}^{\pm} \text{NaCl}_{(aq)} + v_{w}^{\pm} \text{H}_{2} \text{O} \Leftrightarrow v_{e} + \text{Na}_{(aq)}^{+} \cdot v_{w}^{+} \text{H}_{2} \text{O} + v_{e}^{-} \text{Cl}_{(aq)}^{-} \cdot v_{w}^{-} \text{H}_{2} \text{O}$$

$$(\text{R1})$$

¹⁰ when we explicitly include water. Considering only the dissolution of a pure compound, which potentially dissociates effectively (either partly or completely) into v_e^+ cations and v_e^- anions, with $v_e^{\pm} = v_e^+ + v_e^-$, a certain amount $v_w^{\pm} = v_w^+ + v_w^-$ of water will be stoichiometrically consumed by (or bound to) the solute that drives the dissolution and potential dissociation. Since the dissolution and potential dissociation does not change the initial ¹⁵ amount of the solute (no chemical reaction), and since the amount of water consumed is associated with the solute (or its ions), the associated concentration of the water bound to the solute must equal the hydrated solute concentration (both relative to the free water), so that with $a_{s,o}^{v_s^0} = a_{w(hyd),\pm} = a_{s,\pm}^{v_e^+/v_w^+}$ as above.

Thus, the concentration at equilibrium (after dissolution and potential dissociation) is higher by the exponent v_w^{\pm}/v_e^{\pm} than the initial solute concentration $a_s^{v_s^\circ}=55.51v_s^\circ n_s^\circ/(v_w^\circ n_w)$ (not being in equilibrium), with $v_s^\circ=1$ and $v_w^\circ=1$ for the stoichiometrical notation (which is usually neglected). Or in other words, the amount of water bound to the solute decreases the amount of remaining "free" water in the solution so

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that the amount of $v_s^o v_e^{\pm} = v_s^o (v_e^+ + v_e^-)$ dissolved and potentially dissociated solute "sees" a reduced water activity by the exponent v_w^{\pm}/v_e^{\pm} , i.e. $a_{s\pm}^{v_s^{\pm}/v_w^{\pm}} = 55.51v_s^{\pm}n_s^o/(v_w^{\pm}n_w^{\pm})$, with n_s^o always dissolved in 1 l of solution (for the molarity scale), or 1000 g of water (for the molality scale), i.e. $n_w^o = 1000[g]/18.015[g/mol] = 55.51[mol]$. n_w denotes the number of moles of "free" water for the initial solution containing $v_s^o n_s^o$ moles of solute, n_w^{\pm} denotes the number of moles of "free" water for the saturated solution (at equilibrium) containing actually $v_s^o v_e^{\pm} n_s^o$ moles of solute, but with $n_w^{\pm} = n_w^o - n_w^{\pm}$ fewer moles of "free" water n_w^{\pm} .

A3 Aerosol water mass (water uptake)

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The water mass associated with a single solute in an atmospheric aerosol is calculated from Eq. (A8) by:

$$m_{\rm w,sat} = n_{\rm s}/m_{\rm ss,sat} = n_{\rm s}/\left(v_{\rm w}/v_{\rm e} \cdot 55.51 \cdot (1/{\rm RH} - 1)\right)^{v_{\rm w}/v_{\rm e}},$$
 (A9)

Equation (A9) equals Eq. (22) of ML07; $m_{w,sat}$ is the water mass associated with n_s moles of dissolved single solute in a saturated aerosol phase. The total mass of water in an aerosol is then obtained by adding up the (partial) water masses (obtained from Eq. (A9)) of all solutes dissolved in the aqueous phase, but only for compounds those RH is above the compound's relative humidity of deliquescence (RHD).

A3.1 Relative humidity of deliquescence of single solutes (single solutions)

The RHD of a compound can be calculated using Eq. (A8) if the single solute molality at saturation ($m_{ss,sat}$) is used that can be e.g. directly obtained from the solubility mass fraction, i.e. $m_{ss,sat}=1000/M_s/(1/w_s-1)$. Rearranging Eq. (A8) and solving for RHD, gives the expression:

RHD =
$$\left(v_{\rm e} / v_{\rm w} \cdot m_{\rm ss,sat}^{v_{\rm e} / v_{\rm w}} / 55.51 + 1 \right)^{-1}$$
, (A10)

with 55.51[mol/kg(H_2O)]. Equation (A10) equals Eq. (21) of ML07. Tables of RHD calculated using this formula compared to measurements are given in ML07.



A3.2 Relative humidity of deliquescence of mixed solutes (mixed solutions)

The MRHD that corresponds to a mixed solution is inferred from the same equations used to derive the RHD of single solutes, i.e. (A10) (or Eq. 21 and Sects. 4.1.5 and 4.1.9 of ML07) by using the mean values of the relevant thermodynamic properties, i.e. the effective stoichiometric coefficients of the solutes (\bar{v}_e) and water (\bar{v}_w) of all single solutes in the mixed solution, their solubilities and molar masses need to derive the mean

molality at saturation ($\bar{m}_{ss,sat}$).

MRHD = $(\bar{v}_{e}/\bar{v}_{w}\cdot\bar{m}_{ss\,sat}^{\bar{v}_{e}/\bar{v}_{w}}/55.51+1)^{-1}$,

A4 Activity coefficients

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¹⁰ In EQSAM3 activity coefficients are not needed for non-volatile species, but they are required for the calculation of the gas-aerosol partitioning of semi-volatile species. The mean ion pair activity coefficient, γ_s^{\pm} , of a volatile compound is obtained by substitution of the single solution molality, i.e. Eq. (A8), into Eq. (14–16) of ML07. Note that according to ML07 and as mentioned above, Eq. (14–16) yields unity for a pure compound ¹⁵ dissolution (e.g. associated hydration but no chemical reaction), so that upon use of the standard definition of the activity i.e., $a_s^{V_s} = (m_{ss}\gamma_s^{\pm})^{V_s}$ (Robinson and Stokes, 1965), we find, by accounting for the charge density of the solution, ξ_s , (Metzger et al., 2002) and the ratio of the water and solute density, ρ_w/ρ_s

$$\gamma_{\rm s}^{\pm} = \rho_{\rm w}/\rho_{\rm s} \cdot \left({\rm RH}^{-v_{\rm w}/v_{\rm e}}/\left[v_{\rm w}/v_{\rm e}\cdot55.51\cdot\left(1/{\rm RH}-1\right)\right]^{v_{\rm w}/v_{\rm e}}\right)^{2/\xi_{\rm s}}.$$
 (A12)

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(A11)



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Fig. 1. Sketch of a Pfeffer cell: left compartment solution, right compartment pure water.

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Fig. 2. Water uptake of atmospheric aerosols for various single and mixed salt solutions.

