



Supplement of

Prediction of secondary organic aerosol from the multiphase reaction of gasoline vapor by using volatility–reactivity base lumping

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Section S1. Gasoline fuel composition and its application to Carbon Bond 6



Figure S1. The GC-FID chromatogram of gasoline fuel.

Figure S1 illustrates the GC-FID chromatogram of gasoline vapor. To separate GC peaks, the oven temperature was held at 35 °C for 3 minutes and increased to 120 °C at 5 °C min⁻¹. The aromatic HC fraction to total hydrocarbons was about 30%. The reaction rate constants and gas mechanisms used in CB6r3 are as follows.

Aromatic HC	Reaction mechanisms	Rate constants	References ^{a)}
benzene	BENZENE + OH → 0.530*CRES + 0.352*BZO2 + 0.352*RO2 +	2.30×10 ⁻¹² e ^{-190.00/T}	CB6r31
	0.118*OPEN + 0.118*OH + 0.530*HO2 + BENZRO2		
toluene	TOL + OH → 0.180*CRES + 0.650*TO2 + 0.720*RO2 + 0.100*OPEN +	1.80×10 ⁻¹² e ^{340.00/T}	CB6r31
	0.100*OH + 0.070*XO2H + 0.180*HO2 + TOLRO2		
ethylbenzene	EBENZ + OH → 0.180*CRES + 0.650*TO2 + 0.720*RO2 +	7.00×10 ⁻¹²	MCM v3.3.1 ²
	0.100*OPEN + 0.100*OH + 0.070*XO2H + 0.180*HO2 + TOLRO2		
	$PAR + OH \rightarrow XPAR$	8.1×10 ⁻¹³	CB6r31
propylbenzene	PBENZ + OH → 0.180*CRES + 0.650*TO2 + 0.720*RO2 +	5.8×10 ⁻¹²	MCM v3.3.1 ²
	0.100*OPEN + 0.100*OH + 0.070*XO2H + 0.180*HO2 + TOLRO2		
	$2PAR + 2OH \rightarrow 2XPAR$	8.1×10 ⁻¹³	CB6r31
o-xylene	OXYL + OH → 0.155*CRES + 0.544*XLO2 + 0.602*RO2 +	1.36×10 ⁻¹¹	MCM v3.3.1 ²
	0.244*XOPN + 0.244*OH + 0.058*XO2H + 0.155*HO2 + XYLRO2		
m-xylene	MXYL + OH → 0.155*CRES + 0.544*XLO2 + 0.602*RO2 +	2.31 ×10 ⁻¹¹	MCM v3.3.1 ²
	0.244*XOPN + 0.244*OH + 0.058*XO2H + 0.155*HO2 + XYLRO2		
p-xylene	PXYL + OH → 0.155*CRES + 0.544*XLO2 + 0.602*RO2 +	1.43×10 ⁻¹¹	MCM v3.3.1 ²
	0.244*XOPN + 0.244*OH + 0.058*XO2H + 0.155*HO2 + XYLRO2		
TM123B	TM123B + OH → 0.155*CRES + 0.544*XLO2 + 0.602*RO2 +	3.27×10 ⁻¹¹	MCM v3.3.1 ²
	0.244*XOPN + 0.244*OH + 0.058*XO2H + 0.155*HO2 + XYLRO2		
	$PAR + OH \rightarrow XPAR$	8.1×10 ⁻¹³	CB6r3
TM124B	TM124B + OH → 0.155*CRES + 0.544*XLO2 + 0.602*RO2 +	3.25×10 ⁻¹¹	MCM v3.3.1 ²
	0.244*XOPN + 0.244*OH + 0.058*XO2H + 0.155*HO2 + XYLRO2		
	$PAR + OH \rightarrow XPAR$	8.1×10 ⁻¹³	CB6r31
TM135B	TM125B + OH → 0.155*CRES + 0.544*XLO2 + 0.602*RO2 +	5.67×10 ⁻¹¹	MCM v3.3.1 ²
	0.244*XOPN + 0.244*OH + 0.058*XO2H + 0.155*HO2 + XYLRO2		
	$PAR + OH \rightarrow XPAR$	8.1×10 ⁻¹³	CB6r31
ethyltoluenes	Treated as a OXYL + PAR		1
tetramethylbenzenes	Treated as a TM123B + PAR		1

Table S1. Reactions of aromatic HCs of this study with an OH radical and their rate constants

^{a)} 1: (Yarwood et al., 2010), 2: (Jenkin et al., 2012)

Section S2. Model parameters in the absence of gas-wall partitioning.

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S2.1. Near Explicit UNIPAR-GWP

The UNIPAR model was coupled with the Master Chemical Mechanism (MCM v3.3.1) to explicitly treat SOA formation by using individual chemical properties (i.e., molecular weight, O:C ratio, hydrogen bonding) of oxygenated products. The UNIPAR simulation was performed in the box model platform by using the Dynamically Simple Model

30 of Atmospheric Chemical Complexity (DSMACC)(Emmerson and Evans, 2009) platform integrated with the Kinetic PreProcessor (KPP)(Damian et al., 2002). The oxidation products from the MCM mechanisms were explicitly integrated with the UNIPAR model.

To assess the impact if gas-wall partitioning (GWP) on SOA formation, UNIPAR model was coupled with GWP model (UNIPAR-GWP). In UNIPAR-GWP, both gas-particle partitioning and GWP were kinetically treated by using the absorption rate constants (*kon*) and desorption rate constants (*koff*) of organic species *i*, in the *or*, *in*, and *w* phases. The SOA growth via in-particle chemistry was also kinetically treated as the second-order dimerization reaction of condensed organics with aerosol phase reaction rate constants ($k_{o,i}$ for organic phase and $k_{AC,i}$ for the inorganic phase).(Odian, 2004) The kinetic mechanisms associate with the oxidation product *i* were listed as:

1) Gas phase oxidation (MCM v3.3.1)

$$I_g + OH \xrightarrow{k_{OH,i}} I'_g$$

2) Gas-particle partitioning (into the organic phase)

$$I_g \xrightarrow{kon_{or,i}} I_{or}$$
$$I_{or} \xrightarrow{koff_{or,i}} I_g$$

3) Gas-particle partitioning (into the inorganic phase)

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$$I_g \xrightarrow{kon_{in,i}} I_{in}$$

$$I_{in} \xrightarrow{koff_{in,i}} I_g$$

4) Gas-wall partitioning (GWP)

$$I_g \xrightarrow{kon_{w,i}} I_w$$
$$I_w \xrightarrow{kof f_{w,i}} I_g$$

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5) In-particle chemistry (organic phase)

 2^{nd} order reaction

6) In-particle chemistry (inorganic phase)

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2^{nd} order reaction
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In this study, reversibility of oligomerization was not considered. Figure S2 illustrates the simple structure of UNIPAR-GWP.



Figure S2. The structure of the UNIPAR-GWP model, simulated to predict the impact of GWP on aromatic SOA formation. *C* denotes the concentration of the organic compound (*i*) in gas phase (g), organic phase (or), inorganic phase (in), and chamber wall phase (w). $C_{g,i}$ is simulated using the gas kinetic mechanisms (MCM v3.3.1). The gas-phase reactions, multiphase partitioning processes, and aerosol-phase reactions to form the SOA mass are integrated into a chemical solver under the Dynamically Simple Model of the Atmospheric Chemical Complexity (DSMACC)

The chemical properties were explicitly treated for partitioning processes. The physicochemical parameters of oxygenated products resulting from the MCM mechanism were obtained from individual species. For GWP, the physicochemical parameters (hydrogen bond donor (*H_{a,i}*), hydrogen bond acceptor (*H_{a,i}*), dipolarity/polarizability (*S_i*), and polarizability (*P_i*)) of *i* were obtained from PaDEL-descriptor (Yap, 2011) and applied to calculate the GWP parameter (Han and Jang, 2020). The gas-wall partitioning coefficient (*K_w*) and absorption rate constant (*kon_{w,i}*) are two important GWP parameters which can determine the deposition of organic vapor to the chamber wall. *K_w* is a unitless partitioning coefficient derived from the traditional partitioning coefficient by multiplying organic matter
absorbed on the chamber wall (*OM_{wall}*) (Han and Jang, 2020;Krechmer et al., 2016):

$$K_{w,i} = \frac{7.501 RTOM_{wall}}{10^9 MW_{OM} \gamma_{w,i} p_{L,i}^{\circ}}$$
(S1)

where MW_{OM} is the molecular weight of OM_{wall} and $\gamma_{w,i}$ is the activity coefficient of *i* in the wall phase. R (8.314 J mol⁻¹ K⁻¹) is the ideal gas constant, and T (K) is the temperature. $p_{L,i}^{\circ}$ denotes the vapor pressure of *i*. The absorption rate constant $(kon_{w,i})$ of *i* to the wall is expressed as a fractional loss rate with the accommodation coefficient $(\alpha_{wall,i})$ (McMurry and Grosjean, 1985) of *i* to the organic matter on the chamber wall:

$$kon_{w,i} = {A \choose v} \frac{\alpha_{wall,i}\overline{v}_i/4}{1 + \frac{\pi \alpha_{wall,i}\overline{v}_i}{8\sqrt{K_e D}}}$$
(S2)

where D ($1.0 \times 10^{-6} \text{ m}^2 \text{ s}^{-1}$) and K_e (0.12 s^{-1}) are the diffusion coefficient and the coefficient of eddy diffusion, respectively. \bar{v}_i is the gas molecules' mean thermal speed of *i*. A is the surface area and V is the volume of the chamber. The important parameters, activity coefficient of *i* to the wall ($\gamma_{w,i}$) to calculate K_w and accommodation coefficient ($\alpha_{wall,i}$) to calculate k_{on} , were estimated by applying a quantitative structure activity relationship (QSAR) employing

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organic vapors' physicochemical properties. QSAR models are semiempirically determined by using the experimental data that measured time series gas-phase concentrations of SVOCs in the UF-APHOR chamber to predict
$$\gamma_{w,i}$$
 and $\alpha_{wall,i}$:

$$\ln(\gamma_{w,i}) = 2.25e^{0.0007RH}H_{d,i} + 0.79e^{0.022RH}H_{a,i} + 0.13e^{0.0025RH}P_i - 6.54e^{0.0047RH}$$
(S3)

$$\ln(\alpha_{wall,i}) = -0.33H_{d,i} - 3.00H_{a,i} - 0.05P_i - 0.61S_i - 9.69$$
(S4)

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platform.

where $H_{d,i}$, $H_{a,i}$, S_i , and P_i indicate the hydrogen bond donor, hydrogen bond acceptor, dipolarity/polarizability, and polarizability, respectively (Abraham and McGowan, 1987;Abraham et al., 1991;Platts et al., 1999).

The UNIPAR-GWP model was limited to simulate individual compounds of data due to the complexity of mechanism, and thus it was applied to correct the SOA parameters for GWP bias. To improve the SOA parameters, aerosol phase reaction rate constant ($k_{o,i}$) was semiempirically determined by including the GWP mechanism to predict the SOA data generated from the UF-APHOR chamber.

S2.2. Simulation of aromatic SOA using UNIPAR-CB6r3

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The chamber experiments were conducted under various seed conditions, such as NS (non-seed), SA (sulfuric acid seeded), wAS (wet ammonium sulfate seeded), and SO₂, to test SOA parameters and evaluate the feasibility of the UNIPAR-CB6r3 model. Experimental conditions for each chamber experiment are summarized in the Table S2.

Precursor	Date ^a	Initial condition				_				
		HC (ppb)	NO _x (HONO) (ppb)	Seeded aerosol ^c (ppb or µg m- ³)	HC/NO _x (ppbC/ppb)	OM0 ^d (µg m ⁻³)	Y _{SOA} e (%)	RH ^f (%)	Temp. (K)	Figure
Benzene	05/31/20 W	515	680 (125)	-	4.2	5	3.8	37-99	295-321	2, S4(c)
	06/17/20 E	496	648 (134)	SA (50)	4.6	5	9.0	22-91	291-320	2
toluene	06/25/20 E	198	350(160)	-	5.0	2	2.6	21-70	296-321	2, S3(a), S4(a)
	02/23/2019 E	104	76 (76)	wAHS (250)	9.6	2	20.2	27-79	293-318	2, S4(b)
	02/23/2019 W	120	65(65)	wAS (350)	12.9	2	19.2	34-86	294-315	2, S4(b)
ethylbenzene	12/10/17 E ^b	131	363 (13)	SO ₂ (39)	2.7	3	10.1	20-83	271-298	2
	$12/10/17 \ W^{b}$	128	363 (15)	-	2.8	3	4.1	33-86	272-295	2
propylbenzene	03/28/18 E ^b	87	264 (36)	SO ₂ (54)	3.0	3	7.1	11-43	285-312	2, S4(f)
	03/28/18 W ^b	88	248 (33)	-	3.2	3	4.6	16-51	285-312	2, S4(f)
m-xylene	11/27/2018 E	114	272	SA (80)	3.4	2	6.0	31-90	277-297	2, S3(d), S4(e)
	11/27/2018 W	117	274	-	3.4	2	2.0	51-93	277-295	2, S4(e)
	10/28/2018 E	131	289	SA (70)	3.6	2	6.6	14-66	281-310	2, S3(b), S4(d)
o-xylene	10/28/2018 W	128	294	wAS (80)	3.5	2	4.0	36-93	282-310	2, S4(d)
	01/21/2019 E	121	86	SA (70)	11.3	2	11.6	15-70	271-299	2
p-xylene	01/21/2019 W	119	79	-	12.1	2	3.1	26-74	272-299	2
1,2,3TMB	9/25/2018 E	148	353	SA (50)	3.8	2	5.4	12-39	296-322	2
	9/25/2018 W	141	335	-	3.8	2	1.0	16-41	296-321	2
1,2,4TMB	9/8/2018 E	115	275	SA (70)	3.8	2	1.9	13-44	294-321	2, S3(e), S4(h)
	9/8/2018 W	115	269	-	3.8	2	0.9	19-50	295-319	2, S4(h)
1.3.5TMB	9/10/2019 E	210	600	-	3.2	5	1.1	13-40	296-322	2, S4(g)
1.5.511110	9/10/2019 W	211	617	SA (50)	3.1	5	3.4	23-50	297-319	2, S4(g)

Table S2. Experimental conditions of the chamber studies.

a. "E" or "W" that follows the experiment date represents the east or west chamber for the UF APHOR, respectively.

b. The SOA data obtained from (Zhou et al., 2019).

c. "SA", "wAS", or "wAHS" denotes that the experiment with sulfuric-acid aerosol, wet ammonium-sulfate aerosol, or wet ammonium-hydrogen sulfate aerosol is directly injected to the chamber, respectively. SO₂ (in the unit of ppb) was injected into the chamber to generate sulfuric acidic seeds under the sun light.

d. The pre-existing organic matter (OM₀) is determined based on the measured organic matter in the chamber before experiment and applied to the simulation for the initial condition.

e. SOA yield is estimated using $Y_{SOA} = \Delta OM_T / \Delta HC$. Yield in the table was estimated when SOA mass reached to the maximum over the course of the experiments. f. The accuracy of relative humidity (RH) is 5 %. The accuracy of temperature is 0.5 K.

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The time profiles of the simulated concentration of NO, NO₂, O₃, and aromatic HC with CB6r3 mechanism under the experimental conditions (Table S2) are illustrated in Fig. S3. The simulated aromatic SOA mass with UNIPAR-CB6r3 model under the experimental conditions (Table S2) is shown in Fig. S4.



Figure S3. Observed (symbol) and simulated (line) concentration of NO, NO₂, O₃, and HC for the photooxidation of individual aromatic HCs. The environmental conditions of the chamber experiment are described in Table S2.



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Figure S4. Observed (plot) and simulated (line) SOA mass in the chamber studies of aromatic HCs. The simulated OM_T (solid line) and OM_{AR} (dotted line) are illustrated. Particle loss of experimental data onto the chamber wall was corrected. The ranges of FS are presented for experiment under the acidic condition to indicate aerosol acidity over the course of the experiment. The error (9%) associated with SOA mass was estimated with the instrumental error originating from the OC/EC analyzer.

Overall, the simulated concentrations of aromatic SOA, NO, NO₂, O₃, and HC with UNIPAR-CB6r3 agrees with the observed values in the chamber studies.

Section S3. Sunlight intensities

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The sunlight intensity illustrated in Fig. S5 (a) was measured on 06/19/2015 in the UF-APHOR and applied as a reference sunlight intensity for the sensitivity and uncertainty tests. For the simulation of chamber experiment, the measured sunlight intensity was used. To illustrate the difference in sunlight intensities due to the seasonal variation, the measured sunlight intensities in March and December were illustrated in Figure S5 (b).



Figure S5. Time profile of sunlight intensity measured by total ultra-violet radiation (TUVR) in the UF-APHOR on 130 (a) 06/19/2015 for the reference sunlight intensity, and that on (b) 3/6/2019 and 12/5/2020 during the experiments.

Section S4. SOA simulation using CMAQ-AE7 aerosol module

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To compare the SOA simulation results between UNIPAR-CB6r3 and CMAQ-AE7, 2 gasoline SOA data generated in UF-APHOR in the absence of wet inorganic seed were simulated with both models. In CMAQ-AE7, the first order oligomerization reaction of organic species is included in gas mechanisms with the rate constant as 9.5×10⁻⁶ molecules s⁻¹ cm⁻³, while UNIPAR-CB6r3 treats the oligomerization as the second order self-dimerization reaction. In Fig. S6, the SOA simulation with CMAQ-AE7 is compared to the SOA data generated from the photooxidation of gasoline vapor. The simulated gasoline SOA using UNIPAR-CB6r3 is shown in Fig. 4 in the manuscript.





Figure S6. Simulation of gasoline SOA mass by using the CMAQ-AE7 module against SOA data generated without inorganic seed in the UF-APHOR chamber (Table 1).

Section S5. The list of the acronyms or abbreviations

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Table S3. The list of the acronyms and abbreviations.

Acronyms or abbreviation	Definition			
GWP	Gas-Wall Partitioning			
HC	Hydrocarbon			
	Quantitative Structure Activity Relationship			
QSAR RH	Relative Humidity			
OC	Organic carbon			
	The consumption of hydrocarbons			
[RO ₂]	The concentration of RO ₂			
[KO ₂]	The concentration of HO ₂			
	The stoichiometric coefficient of the lumping species i			
$\frac{\alpha_i}{OM_T}$	Total SOA mass			
OMP	The SOA mass generated via gas-particle partitioning			
OMAR	The SOA mass generated via gas particle partitioning The SOA mass generated via heterogeneous reactions in organic and inorganic phases			
0	Vapor pressure of the lumping species <i>i</i> (mmHg)			
$p_{L,i}$ MW_i	Molecular weight of the lumping species <i>i</i> (g/mol)			
$O: C_i$	Oxygen to carbon ratio of the lumping species <i>i</i>			
HB_i	Hydrogen bonding of the lumping species <i>i</i>			
R_i	Reactivity scale of the lumping species <i>i</i> in the aerosol phase			
	The gas concentration of lumping species <i>i</i> in the actosol phase			
$C_{g,i}$	The concentration of lumping species <i>i</i> partition onto the organic phase			
C _{or,i}	The concentration of lumping species <i>i</i> partition onto the organic phase			
C _{in,i}				
K _{or,i}	The partitioning coefficient of <i>i</i> into the organic phase			
K _{in,i}	The partitioning coefficient of <i>i</i> into the inorganic phase			
MW _{or}	The averaged molecular weight of OM _T (g mol ⁻¹)			
R	The ideal gas constant (8.314 J mol ⁻¹ K ⁻¹)			
Т	Temperature (K)			
MW _{in}	The averaged molecular weight of inorganic aerosol (g mol ⁻¹)			
Yor,i	The activity coefficient of <i>i</i> in organic phase			
γin,i	The activity coefficient of i in inorganic phase			
FS	Fractional sulfate Sulfuric acid			
AS SA	Ammonium sulfate			
$C'_{or,i}$	The concentration of <i>i</i> in the organic aerosol phase (mol L^{-1})			
	The concentration of <i>i</i> in the organic aerosol phase (mol L^{-1})			
$C'_{in,i}$				
k _{AC,i}	The reaction rate constant in the aqueous phase			
k _{o,i}	The reaction rate constant in the organic phase			
$pK_{BH_i^+}$	The protonation equilibrium constant			
X	The excess acidity			
a_w	The water activity			
[H ⁺]	The proton concentration			
C _{T,i}	The total concentration of <i>i</i>			
$C_{g,i}^*$	the effective saturation concentration of <i>i</i>			
OM ₀	The pre-existing OM concentration (mol m ⁻³)			
OM	The organic matter			
MW _{oli,i}	The molecular weight of the dimer (g mol ⁻¹).			
kon _w	The absorption rate constant of <i>i</i> into the chamber wall			
kof f _w	The desorption rate constant of <i>i</i> from the chamber wall			
LLPS	Liquid-liquid phase separation			
NS	No-seeded			

wAHS	Wet ammonium bisulfate
dAS	Dry ammonium sulfate
C _{SOA}	The aromatic SOA mass in the absence of GWP bias ($\mu g m^{-3}$)
C _{SOA,wall}	The aromatic SOA mass in the presence of GWP bias (μ g m ⁻³)
ERH	Efflorescence relative humidity
DRH	Deliquescence relative humidity

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