Supplement of

Formation kinetics and mechanisms of ozone and secondary organic aerosols from photochemical oxidation of different aromatic hydrocarbons: dependence on NOx and organic substituents

Hao Luo et al.

Correspondence to: Taicheng An (ante99@gdut.edu.cn)

The copyright of individual parts of the supplement might differ from the article licence.
1 Experimental setting of instrument

The gas in the reactor were inhaled into the drift tube of Proton Transfer Reaction-Time of Flight-Mass Spectrometry (PTR-ToF-MS, Ionicon Analytik, Austria) through a 1.5 m long heated PEEK tube (80 °C) with a flow rate of 30 ml min⁻¹. The key factors of the drift tube conditions were set as following: drift pressure of 2.3 mbar, 80 °C and voltage at 600 V, corresponding to E/N ratio approximately 130 Td (1 Td=10⁻¹⁷ V cm²). The PTR-TOF-MS was operated using protonated water (H₃O⁺) as the reagent ion.

2 Calculation methodology

The yield of products can be calculated by the following formula:

\[ \gamma_{\text{(product)}} = \frac{\Delta_{\text{(product)}}}{\Delta_{\text{(AH)}}} \]  

(S1)

which \( \gamma \) is the yield of a single AH product; \( \Delta_{\text{(product)}} \) is the concentration of individual AH product when peak O₃ concentration occurs; \( \Delta_{\text{(AH)}} \) is the reaction amount of AH when O₃ peak occurs during the experiment.

All experiments were conducted under UV light without aerosol seeds. And the aerosol particles were corrected by the wall loss. The yield calculation formula of SOA is shown as following:

\[ \gamma_{\text{(SOA)}} = \frac{\Delta_{\text{(particle mass concentration)}}}{\Delta_{\text{(AH)}}} \]  

(S2)

\( \gamma \) (SOA) is the yield of SOA; \( \Delta_{\text{(particle mass concentration)}} \) is the corrected particle mass concentration after peak O₃ concentration; \( \Delta_{\text{(AH)}} \) is the reaction amount of the AH after peak O₃ concentration.

In two-product semi-empirical model, the SOA yield is defined as the ratio of produced aerosols to reacted AHs \(^1\):

\[ \frac{\Delta_{\text{(particle mass concentration)}}}{\Delta_{\text{(AH)}}} \]
\[ \gamma_{\text{SOA}} = \Sigma \gamma_i(\text{SOA}) = M_0 \Sigma \left( \alpha_i \frac{K_{\text{om},i}}{1 + K_{\text{om},i} M_0} \right) \] (S3)

\( \gamma_{\text{SOA}} \) is the yield of SOA, \( M_0 \) is the total mass concentration of organic matter, \( \alpha_i \) and \( K_{\text{om},i} \) are the stoichiometric coefficient and the partition coefficient of species \( i \).

In this model, these two products represent a class of low vapor pressure compounds and a class of high vapor pressure compounds, respectively. The two-product empirical model divides SOA into high-volatility and low-volatility, where \( \alpha_i \) and \( K_{\text{om},i} \) are the fitting parameters and are determined by the minimum sum of squares of the residuals. SOA mass concentration is calculated by the volume concentration of SOA measured by SMPS. According to previous studies, the aerosol density of aromatic hydrocarbons ranges from 1.24 to 1.51 g cm\(^{-3}\). In this study, the aerosol density of aromatic hydrocarbons is selected as 1.4 g cm\(^{-3}\) to calculate the mass concentrations of SOA produced from AH-NO\(_x\) photooxidation in the peak O\(_3\) time. All SMPS data were obtained after wall loss correction.
Table S1. Typical Experimental conditions of this study for nine AHs.

<table>
<thead>
<tr>
<th>AHs</th>
<th>VOC/ppb</th>
<th>NOx/ppb</th>
<th>VOC/NOx ratio</th>
<th>RH/%</th>
<th>T/K</th>
</tr>
</thead>
<tbody>
<tr>
<td>Benzene</td>
<td>2000</td>
<td>160.2</td>
<td>12.48</td>
<td>&lt; 5</td>
<td>303 ± 1</td>
</tr>
<tr>
<td>Toluene</td>
<td>1048</td>
<td>162.0</td>
<td>6.47</td>
<td>&lt; 5</td>
<td>303 ± 1</td>
</tr>
<tr>
<td>Ethylbenzene</td>
<td>1050</td>
<td>162.4</td>
<td>6.47</td>
<td>&lt; 5</td>
<td>303 ± 1</td>
</tr>
<tr>
<td>m-Xylene</td>
<td>889</td>
<td>172.1</td>
<td>5.17</td>
<td>&lt; 5</td>
<td>303 ± 1</td>
</tr>
<tr>
<td>o-Xylene</td>
<td>1052</td>
<td>159.8</td>
<td>6.58</td>
<td>&lt; 5</td>
<td>303 ± 1</td>
</tr>
<tr>
<td>p-Xylene</td>
<td>1040</td>
<td>157.2</td>
<td>6.42</td>
<td>&lt; 5</td>
<td>303 ± 1</td>
</tr>
<tr>
<td>123-TMB</td>
<td>956</td>
<td>171.4</td>
<td>5.58</td>
<td>&lt; 5</td>
<td>303 ± 1</td>
</tr>
<tr>
<td>124-TMB</td>
<td>1010</td>
<td>169.5</td>
<td>5.96</td>
<td>&lt; 5</td>
<td>303 ± 1</td>
</tr>
<tr>
<td>135-TMB</td>
<td>1040</td>
<td>164.2</td>
<td>6.33</td>
<td>&lt; 5</td>
<td>303 ± 1</td>
</tr>
</tbody>
</table>

Table S2. Range of VOC/NOx ratio in our work and previous studies during O3 formation.

<table>
<thead>
<tr>
<th>AHs</th>
<th>Range of VOC/NOx ratio</th>
<th>Source</th>
</tr>
</thead>
<tbody>
<tr>
<td>123-TMB</td>
<td>3.19-3.69</td>
<td>Luo et al., 2019</td>
</tr>
<tr>
<td>Toluene</td>
<td>1.60-4.90</td>
<td>Li et al., 2018</td>
</tr>
<tr>
<td>m-xylene</td>
<td>0.10-15.00</td>
<td>Xu et al., 2015</td>
</tr>
<tr>
<td>Nine AHs</td>
<td>1.00-13.70</td>
<td>This study</td>
</tr>
</tbody>
</table>
Figure S1. The concentration variation of intermediates formed from photochemical oxidation of benzene (2110 ppb), ethylbenzene (1060 ppb), m-xylene (889 ppb), o-xylene (1160 ppb), p-xylene (1040 ppb), 123TMB (824 ppb), 124TMB (935 ppb) and 135TMB (913 ppb).
Figure S2. O₃ formation curve of benzene (a), ethylbenzene (b), m-xylene (c), o-xylene (d), p-xylene (e), 123TMB (f), 124TMB (g) and 135TMB (h) photochemical oxidation under different VOC/NOₓ ratio.
Figure S3. Nanoparticle distribution from benzene photochemical oxidation varied with time at different VOC/NOx ratio (the initial concentrations of NOx were in the range of 151.5 to 165.7 ppb).
Figure S4. Nanoparticle distribution from ethylbenzene photochemical oxidation varied with time at different VOC/NO$_x$ ratio (the initial concentrations of NO$_x$ were in the range of 151.1 to 176.6 ppb).
**Figure S5.** Nanoparticle distribution from m-xylene photooxidation varied with time at different VOC/NOx ratio (the initial concentrations of NOx were in the range of 169.7 to 173.6 ppb).
Figure S6. Nanoparticle distribution from o-xylene photooxidation varied with time at different VOC/NOₓ ratio (the initial concentrations of NOₓ were in the range of 157.1 to 166.4 ppb).
Figure S7. Nanoparticle distribution from p-xylene photooxidation varied with time at different VOC/NO\textsubscript{x} ratio (the initial concentrations of NO\textsubscript{x} were in the range of 157.2 to 166.9 ppb).
Figure S8. Nanoparticle distribution from 123TMB photooxidation varied with time at different VOC/NO\textsubscript{x} ratio (the initial concentrations of NO\textsubscript{x} were in the range of 167.3 to 178.4 ppb).
**Figure S9.** Nanoparticle distribution from 124TMB photooxidation varied with time at different VOC/NO\textsubscript{x} ratio (the initial concentrations of NO\textsubscript{x} were in the range of 164.4 to 170.3 ppb).
Figure S10. Nanoparticle distribution from 135TMB photooxidation varied with time at different VOC/NO\textsubscript{x} ratio (the initial concentrations of NO\textsubscript{x} were in the range of 157.4 to 169.7 ppb).

Figure S11. The yield of SOA generated by photochemical oxidation of AHs varies with VOC/NOx ratio.

Figure S12. The variation trend of SOA yield generated by photochemical oxidation of different AHs (square: benzene; circle: toluene; upper triangle: ethylbenzene; lower triangle: m-xylene; diamond: o-xylene; left triangle: p-xylene; right triangle: 123TMB; hexagon: 124TMB; pentacle: 135TMB)
Figure S13. The concentration variation of produced intermediates from photochemical oxidation of different AHs.
Figure S14. Concentration comparison of produced intermediates from photochemical oxidation of different AHs with or without NOx.
Figure S15. The (a) concentration and (b) yield of products in the gas phase generated by the photochemical oxidation of benzene changed with the trend of VOC/NO\textsubscript{x} ratio.

Figure S16. The (a) concentration and (b) yield of products in the gas phase generated by the photochemical oxidation of ethylbenzene changed with the trend of VOC/NO\textsubscript{x} ratio.
**Figure S17.** The (a) concentration and (b) yield of products in the gas phase generated by the photochemical oxidation of m-xylene changed with the trend of VOC/NO\textsubscript{x} ratio.

**Figure S18.** The (a) concentration and (b) yield of products in the gas phase generated by the photochemical oxidation of o-xylene changed with the trend of VOC/NO\textsubscript{x} ratio.
Figure S19. The (a) concentration and (b) yield of products in the gas phase generated by the photochemical oxidation of p-xylene changed with the trend of VOC/NO \(_x\) ratio.

Figure S20. The (a) concentration and (b) yield of products in the gas phase generated by the photochemical oxidation of 123TMB changed with the trend of VOC/NO \(_x\) ratio.
Figure S21. The (a) concentration and (b) yield of products in the gas phase generated by the photochemical oxidation of 124TMB changed with the trend of VOC/NO$_x$ ratio.

Figure S22. The (a) concentration and (b) yield of products in the gas phase generated by the photochemical oxidation of 135TMB changed with the trend of VOC/NO$_x$ ratio.
Figure S23. The concentration variation of (a) m87 and (b) m111 formed from different AH photochemical oxidation in the presence of NOx.

Reference


