

Influence of atmospheric in-cloud aqueous-phase chemistry on the global simulation of SO_2 in CESM2

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Abstract. Sulfur dioxide (SO₂) is a major atmospheric pollutant and precursor of sulfate aerosols, which influences air quality, cloud microphysics, and climate. Therefore, better understanding the conversion of SO₂ to sulfate is essential to simulate and predict sulfur compounds more accurately. This study evaluates the effects of in-cloud aqueous-phase chemistry on SO₂ oxidation in the Community Earth System Model version 2 (CESM2). We replaced the default parameterized SO_2 aqueous-phase reactions with detailed HO_x , Fe, N, and carbonate chemistry in cloud droplets and performed a global simulation for 2014–2015. Compared with the observations, the results incorporating detailed cloud aqueousphase chemistry greatly reduced SO₂ overestimation. This overestimation was reduced by 0.1-10 ppbv (parts per billion by volume) in most of Europe, North America, and Asia and more than 10 ppbv in parts of China. The biases in annual simulated SO₂ mixing ratios decreased by 46%, 41%, and 22 % in Europe, the USA, and China, respectively. Fe chemistry and HO_x chemistry contributed more to SO_2 oxidation than N chemistry. Higher concentrations of soluble Fe and higher pH values could further enhance the oxidation capacity. This study emphasizes the importance of detailed in-cloud aqueous-phase chemistry for the oxidation of SO₂. These mechanisms can improve SO₂ simulation in CESM2 and deepen understanding of SO2 oxidation and sulfate formation.

1 Introduction

Sulfur dioxide (SO₂) is one of the major atmospheric pollutants. The anthropogenic emission of SO₂ is the greatest source, which includes mainly the combustion of fossil fuel in the power and steel industries (Buchard et al., 2014). Human health risks from SO2 have also been discovered and discussed in many studies (Kan et al., 2012; Tong et al., 2017; Chen et al., 2018). More importantly, SO₂ is the precursor of sulfate aerosols. Sulfate can be regarded as one of the core species in the atmosphere. First, it is one of the major components of fine particles (PM_{2.5}) which cause haze pollution and affect human health, especially in East and South Asia (Buchard et al., 2014; Chen et al., 2018; Quan et al., 2015; Geng et al., 2019). In addition, sulfate is also the main component of cloud condensation nuclei (CCN), which directly influences the formation of clouds and, thus, affects precipitation, solar radiation, and climate (He et al., 2015a; Tang et al., 2016). Moreover, sulfate itself is also one of the key species affecting radiative forcing, which directly influences climate change (J. Li et al., 2018; Pöschl and Shiraiwa, 2015; Xie et al., 2016). Therefore, only through a better understanding of SO₂, especially the process of its oxidation to sulfate, can we better understand sulfate and explore all the issues above (Hung et al., 2018).

 SO_2 can be oxidized to sulfate in multiple ways. On clear and sunny days, the gas-phase oxidation of SO_2 by OH radicals (•OH) is the dominant pathway (J. Li et al., 2018; Cheng et al., 2016). However, when relative humidity (RH) and PM_{2.5} increase on cloudy, foggy, or hazy days, solar radiation and photochemical reactions decrease dramatically, resulting in a sharp decrease in gaseous •OH and, thus, the gasphase oxidation of SO₂, especially in winter. Alternatively, the aqueous-phase oxidation of SO₂ becomes much more important because of the increase in atmospheric liquid water content (Cheng et al., 2016; Quan et al., 2015). Aqueousphase chemistry is an important part of atmospheric chemistry. Various physical and chemical parameters, such as the water content, ionic strength, and pH value, could directly affect the gas-aqueous mass transfer process and the reaction rates and then influence the relative contributions of various mechanisms (Elser et al., 2016; Ervens, 2015). For SO₂, the aqueous-phase oxidation of SO₂ by diverse oxidants can serve as the major sink of atmospheric SO₂. It accounts for nearly 80 % of global sulfate production, and more than half of sulfate production occurs in clouds (Harris et al., 2013; Huang et al., 2018). Specifically, there are several common oxidation pathways in the aqueous phase, such as oxidation by hydrogen peroxide (H₂O₂) and ozone (O₃; Tan et al., 2016; Hung et al., 2018). In recent years, increasing numbers of studies have focused on the catalytic effect of transition metal ions (TMIs) on the aqueous-phase oxidation of SO₂ (Tilgner et al., 2013; Alexander et al., 2009). In addition, oxidation by NO₂ has also received increasing attention (Xue et al., 2016).

Transition metals in dust particles are important sites for various reactions and affect the moisture absorption, light scattering, and nucleation process of clouds. Among these elements, Fe is one of the most important transition metals due to its high abundance and activity (Tang et al., 2016). Soluble Fe can act as an important catalyst in the Fenton reaction for the oxidation of SO₂ when dissolved into the aqueous phase. The Fenton reaction, which was first proposed by Henry J. H. Fenton in the 1890s, is one of the most important and widespread reactions in multiphase chemistry (Wiegand et al., 2017; Fenton, 1894; Pöschl and Shiraiwa, 2015). This reaction involves the production of •OH in the aqueous phase by the decomposition of H_2O_2 catalyzed by low-valence TMIs such as Fe^{2+} (Deguillaume et al., 2005; Herrmann et al., 2015). Different mechanisms have been developed to explain the first step of Fenton reactions. Of the best known pathways, two are (1) the OH radical mechanism (Fe²⁺ + H₂O₂ \rightarrow Fe³⁺ + •OH + OH⁻) developed by Haber and Weiss (1934) and (2) the non-OH radical mechanism (Fe²⁺ + H₂O₂ \rightarrow FeO²⁺ + H₂O) proposed by Bray and Gorin (Haber and Weiss, 1934; Bray and Gorin, 1932; Wiegand et al., 2017; Pöschl and Shiraiwa, 2015). The relative contributions of these two pathways differ under various conditions and remain controversial. A recent experimental study suggested that the non-OH radical mechanism is dominant under nearly neutral conditions (pH \approx 7), while the OH radical mechanism becomes more important under acidic conditions (Pang et al., 2011; Deguillaume et al., 2005; Wiegand et al., 2017; Pöschl and Shiraiwa, 2015; Bataineh et al., 2012). Then, all of these oxidative intermediates (i.e., Fe^{3+} , •OH, and FeO^{2+}) can further oxidize SO₂ to sulfate. In this way, Fe^{3+} and FeO^{2+} are reduced to Fe^{2+} , thus forming a complete redox cycle. Their concentrations and proportions are basically the same during the redox cycle, and a balance of catalysts is achieved (Deguillaume et al., 2005). The effects of soluble Fe on sulfate formation have been discussed in several studies (Gankanda et al., 2016). In addition, direct oxidation of SO₂ by O₂ might also be catalyzed by soluble Fe. In general, Fenton reactions could lead to faster radical recycling. The reaction rates of sulfate formation are enhanced with high Fe concentrations, especially when pH < 5 (Shao et al., 2019; Ervens, 2015; Huang et al., 2014; Tilgner et al., 2013).

On the other hand, a number of studies have also emphasized the important role of NO₂ in the oxidation of SO₂ (Ma et al., 2018; Tao et al., 2017; Huang et al., 2019). He et al. (2014) and Cheng et al. (2016) reported a missing source of SO₂ oxidation that can be explained by the synergistic effect between NO₂ and SO₂ in aerosol water and on mineral dust as follows: $2NO_2 + HSO_3^- + H_2O \rightarrow 3H^+ + 2NO_2^- + SO_4^{2-}$ (He et al., 2014; Cheng et al., 2016). Such a conversion of SO_2 by NO_2 is driven by a high pH value (e.g., pH > 5.5) and a high concentration of NO₂ (Wang et al., 2020; L. Li et al., 2018; Huang et al., 2019; He and He, 2020; He et al., 2018). Moreover, these studies have indicated that > 95 % of NO₂ converts to HNO_2/NO_2^- by hitting the surface of NaHSO₃ aqueous microjets to promote the aqueous-phase oxidation of SO₂ (Wang et al., 2020; L. Li et al., 2018). This pathway can explain the gaps in sulfate concentrations between simulations and observations from approximately 15 % to 65 % during haze days in winter (Zheng et al., 2020). However, other studies have suggested that the contribution of nitrogen chemistry to SO₂ oxidation is very limited. Au Yang et al. (2018) argued that the NO₂ oxidation pathway cannot explain the extreme concentrations of sulfate measured in urban aerosols (Au Yang et al., 2018). Only a minor (approximately 2%) fraction of heterogeneous sulfate formation occurs via the oxidation of SO₂ by NO₂ (Shao et al., 2019). The main reason is that the pH value is hardly ever high enough to maintain the efficiency of oxidation by NO₂ in aerosol or cloud water (Guo et al., 2017). For instance, aerosols collected from several urban areas in China (CN) were always acidic (even with the unusually high NH₃ emissions and concentrations in northern CN), suggesting that oxidation by NO₂ might not be very important in these regions (Li et al., 2020; He and He, 2020). In summary, the contribution of N chemistry to the aqueous-phase oxidation of SO₂ still needs further investigation.

Many studies have been conducted on the aqueous-phase oxidation of SO₂. Some laboratory studies have focused on the detailed mechanism, such as the radical processes involved in different pathways of the Fenton reaction (Wiegand et al., 2017; Bataineh et al., 2012) and the conversion of NO₂ to HNO₂ to oxidize SO₂ (He et al., 2014). Some studies

have paid more attention to the measurement and updating of kinetic parameters (Cwiertny et al., 2008; He et al., 2018; He and He, 2020). More importantly, modeling studies have made great progress in revealing the mechanism of SO₂ oxidation and sulfate formation in the aqueous phase (Bell et al., 2005). For instance, Herrmann et al. (2000) used a box model to investigate the detailed aqueous-phase radical mechanism for tropospheric chemistry (Herrmann et al., 2000). Huang et al. (2014) and Li et al. (2017) discussed the enhancement of sulfate formation by mineral aerosols in CN and improved the simulation of heterogeneous sulfate in the Weather Research and Forecasting (WRF)-Chem model (Huang et al., 2014; Li et al., 2017). J. Li et al. (2018) also improved the simulation of sulfate with the nested air-quality prediction modeling system (NAQPMS) model of oxidation of SO₂ by NO₂ on wet aerosols on haze days (J. Li et al., 2018). Shao et al. (2019) evaluated various heterogeneous mechanisms for sulfate aerosol formation in Beijing using the GEOS-Chem model (Shao et al., 2019). Bell et al. (2005) analyzed the effects of different SO₂ emission scenarios on radiative forcing and climate over East Asia (EA) using the Global Climate Model (GCM; Bell et al., 2005). Both Zheng et al. (2020) and Zheng et al. (2015) used the Community Multiscale Air Quality (CMAQ) model to explore heterogeneous chemistry for the formation of secondary inorganic aerosols and the contribution of nitrate photolysis to heterogeneous sulfate formation in CN on winter haze days, respectively (Zheng et al., 2020; Zheng et al., 2015). Zheng et al. (2015) used the WRF-CMAQ model to explain the crucial role of reactive N chemistry in aerosol water for sulfate formation during haze events in CN (Zheng et al., 2015). Nevertheless, there are still obvious shortcomings in these model studies. First of all, in long-term global climate simulations, studies focused on the spatiotemporal distribution of SO₂ concentrations are still insufficient. Most studies have evaluated only sulfate distribution and its climate impact. Very few studies have discussed the simulation of SO₂, and these few studies are only from the perspective of SO₂ emissions. In addition, although some studies have attempted to discuss different pathways of aqueous-phase oxidation of SO₂, most of them have merely adopted simplified mechanisms or even parameterization alone without introducing detailed radical mechanisms. On the other hand, several studies investigated the detailed aqueous-phase chemistry, but they did not analyze its influence on SO_2 but only discussed the influence on O_3 , •OH, or HO₂ (Herrmann et al., 2000; Jacob, 1986; Matthijsen et al., 1995; Jacob, 2000; Mao et al., 2013, 2017). Finally, the simulations of SO₂ in many studies are still highly overestimated (He et al., 2015b, a; Buchard et al., 2014; Hong et al., 2017; Georgiou et al., 2018; Wei et al., 2019; Flemming et al., 2015; Sha et al., 2019; X. Liu et al., 2012; Hedegaard et al., 2008), while others underestimate the concentration of sulfate (Xie et al., 2016; Goto et al., 2015; Bell et al., 2005; Lamarque et al., 2012; Pozzer et al., 2012; Guth et al., 2016; Wei et al., 2019; Geng et al., 2019; Kajino et al., 2012; Mathur, 2005; X. Liu et al., 2012; Sha et al., 2019; Zhang et al., 2012; Itahashi, 2018). All of these disadvantages indicate that the mechanism of SO_2 oxidation to sulfate is still not fully understood.

This study aims to examine the role played by detailed in-cloud aqueous-phase chemistry (not including chemical reactions on the surfaces of wet aerosols) on the capacity for oxidation of global SO₂ in the Community Earth System Model 2 (CESM2). We describe the CESM2 model, detailed cloud chemistry, and observational data in Sect. 2. The evaluation of SO₂ simulations with or without coupling detailed in-cloud aqueous-phase chemistry is given in Sect. 3. The contributions of different in-cloud aqueous-phase chemical mechanisms to the simulation of SO₂ are analyzed in Sect. 4. The key factors that affect the capacity for SO₂ oxidation are discussed in Sect. 5. Finally, the main conclusions are drawn in Sect. 6.

2 Methodology

2.1 Model description

The Community Earth System Model 2 (CESM2, v2.1.1), developed by the National Center for Atmospheric Research (NCAR; https://www.cesm.ucar.edu/models/cesm2/, last access: 16 December 2020), is used in this study (Emmons et al., 2020; Danabasoglu et al., 2020), configured with the Community Atmosphere Model version 4.0 (CAM4). The coupled chemistry in CAM4 is primarily based on the Model for Ozone and Related chemical Tracers, version 4 (MOZART-4), including 85 gas-phase species with bulk aerosols and detailed tropospheric chemistry with 196 gasphase reactions (Emmons et al., 2010; Lamarque et al., 2012). The default aerosol species simulated in this component set include sulfate, nitrate, ammonium, black carbon (BC), organic carbon (OC), secondary organic aerosol (SOA), dust, and sea salt. In this study, we develop a detailed aqueous-phase chemistry module for SO₂ oxidation fully coupled in the MOZART-4 chemistry.

The model is configured with a horizontal resolution of 0.95° (latitude) $\times 1.25^{\circ}$ (longitude) and 30 levels in the vertical direction from 993 (near-surface layer) to 3.6 hPa. The model is nudged by assimilated meteorological offline data from Modern-Era Retrospective analysis for Research and Applications, version 2 (MERRA-2, https://rda.ucar.edu/datasets/ds313.3/, last access: 20 July 2020), prepared with 14 meteorological variables (e.g., air temperature, surface pressure, specific humidity, and eastward and northward winds) to run CESM2 simulations. The meteorological data have a temporal resolution of 3 h.

All the emission inventories needed for MOZART-4 chemistry are obtained from the CESM database (https://svn-ccsm-inputdata.cgd.ucar.edu/trunk/inputdata/ atm/cam/chem/emis/CMIP6_emissions_1750_2015/, last

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access: 31 December 2020), which was developed for the Coupled Model Intercomparison Project (CMIP)6 projects (Feng et al., 2020). The inventories have been updated to 2015, which is the year of the simulation in this study. Meanwhile, the emission, dry deposition, and wet deposition processes of aerosol species are also guided by input files from CESM database (https: //svn-ccsm-inputdata.cgd.ucar.edu/trunk/inputdata/atm/cam/ chem/trop_mozart_aero/, last access: 31 December 2020; https://svn-ccsm-inputdata.cgd.ucar.edu/trunk/inputdata/ atm/cam/chem/emis/CMIP6_emissions_1750_2015_2deg/, last access: 31 December 2020) and the source codes of CESM2 (aero_model.F90, mo_drydep.F90, and wetdep.F90).

The variables related to the cloud properties used in this study are all from the Rasch and Kristjansson (RK) prognostic cloud microphysical processes. These variables include the liquid water content of clouds (LWC; liters of water per liter of air; hereafter $L_{water} L_{air}^{-1}$), volume fraction of clouds (F_{cld}), and radius of cloud droplets (r; microns; hereafter µm). They are directly obtained from the model simulation and directly or indirectly influence the incloud aqueous-phase chemistry. Among these variables, the simulated r ranges from 8 to $14 \,\mu\text{m}$, consistent with those in previous studies (Herrmann et al., 2000, 2015; Jacob, 1986; Matthijsen et al., 1995; J. Liu et al., 2012). Meanwhile, CESM2 simulates both large-scale stratiform clouds and convective clouds (i.e., shallow cumulus clouds and deep convective clouds). For each type of cloud, both water and ice are simulated. However, the SO₂ produced in convective clouds is assumed to be removed rapidly by convective precipitation. Thus, the contribution of SO₂ from shallow cumulus clouds and deep convective clouds is ignored. Only the LWC and F_{cld} of large-scale liquid stratiform clouds are employed in this study.

2.2 Mechanism of in-cloud aqueous-phase oxidation of SO₂

The detailed mechanism of in-cloud aqueous-phase oxidation of SO₂ is divided into the gas-aqueous-phase transfer process and aqueous-phase chemical mechanisms, as listed in Tables 1 and 2, respectively (see below). There are 32 (16 pairs of) gas-aqueous-phase transfer equilibria and 187 aqueous-phase reactions (only in cloud droplets and not on surfaces of wet aerosol), involving 46 new aqueous species in all. Specifically, the aqueous-phase reactions include 26 (13 pairs of) ionization equilibria and four different chemistry modules, which are HO_x chemistry, Fe chemistry, N chemistry, and carbonate chemistry. The aqueousphase oxidation of SO₂ by H₂O₂ and O₃ is included in the HO_x chemistry mechanism. The two pathways of the Fenton reaction are included in the Fe chemistry mechanism. The aqueous-phase oxidation of SO₂ by NO₂ is included in the N chemistry mechanism.

There are four parameters in every pair of gas–aqueousphase transfer equilibria. The two parameters in the transfer from the gas phase to the aqueous phase are the molar mass (grams per mole; hereafter g mol⁻¹) and mass accommodation coefficients of this species. The other two parameters in the transfer from the aqueous phase to the gas phase are Henry's law constants (moles per liter per atmosphere; hereafter M atm⁻¹) at 298 K (K_{H298}) and ΔH (joules per mole; hereafter J mol⁻¹)/R (joules per mole per Kelvin; hereafter J mol⁻¹ K⁻¹), where ΔH is the enthalpy of dissolution. The Henry's law constant $K_{\rm H}$ (M atm⁻¹) at any temperature T (Kelvin; hereafter K) in Eq. (1) can be calculated by Eq. (2) as follows:

$$[C_i] = K_{\rm H} \cdot P_i \tag{1}$$

$$K_{\rm H}(T) = K_{\rm H298} \cdot \exp\left(-\frac{\Delta H}{R}\left(\frac{1}{T} - \frac{1}{298}\right)\right),\tag{2}$$

where $[C_i]$ and P_i are aqueous-phase and gas-phase concentrations of species *i* in units of moles per liter of water (hereafter molL⁻¹_{water}) and atmosphere, respectively. On the other hand, the concentration of liquid water is a constant value of 55.6 (i.e., 1000/18) molL⁻¹. The initial concentration of soluble Fe(III) ([Fe³⁺]) is set to 5 µM, which refers to the urban conditions from the literature (Deguillaume et al., 2005; Mao et al., 2013; Jacob, 2000; Shao et al., 2019; Li et al., 2017; Herrmann et al., 2000; Matthijsen et al., 1995).

To facilitate the calculation of gas-phase and aqueousphase chemistry simultaneously, the methods used in Jacob (1986) and J. Liu et al. (2012) are applied in this study, which convert the units of concentrations and reaction rates in the aqueous phase to the same units as those used in gas-phase chemistry, as follows (Jacob, 1986; J. Liu et al., 2012):

$$[X_i] = 6.023 \times 10^{20} \cdot \text{LWC} \cdot [C_i], \tag{3}$$

where $[X_i]$ and $[C_i]$ are aqueous-phase concentrations of species *i* in units of molecules per cubic meter of air (hereafter molec. cm_{air}⁻³) and moles per liter of water (hereafter molL_{water}), respectively, and 6.023×10^{20} is the product of Avogadro constant (6.023×10^{23}) and unit conversion factor (10^{-3}) between values per liter of air (hereafter L_{air}⁻¹) and per cubic centimeter of air (hereafter cm_{air}⁻³). In this way, the chemical systems of both gas and aqueous phases can be numerically solved without distinction.

2.3 Model configuration

There are two main simulations conducted in this study. The first simulation (the *original* case) is conducted without any modification of the default CAM4 chemistry, with parameterized aqueous-phase oxidation reactions of SO₂ by H₂O₂ and O₃. In the second simulation (the *improved* case), since the F_{cld} is nonzero in most grids, two calculations are performed in a cloudy grid cell. In the cloudy part, the parameterized aqueous-phase reactions mentioned above are replaced by detailed in-cloud aqueous-phase chemistry, listed

No.	Reactions	k_1	<i>k</i> ₂	Reference
	Gas-aqueous-phase transfer			
1 ^{a, c}	$O_3(g) \rightarrow O_3$	48	0.05	Mirabel (1996)
2 ^b	$O_3 \rightarrow O_3(g)$	$1.1 imes 10^{-2}$	-2397	Hoffman and Calvert (1985);
				Pandis and Seinfeld (1989)
3 ^a	$HO_2(g) \rightarrow HO_2$	33	0.01	Hanson et al. (1992)
4 ^b	$HO_2 \rightarrow HO_2(g)$	9.0×10^{3}	0	Weinsteinlloyd and Schwartz (1991)
5 ^a	$OH(g) \rightarrow OH$	17	0.05	Herrmann et al. (2000)
6 ^b	$OH \rightarrow OH(g)$	25	-5280	Kläning et al. (1985)
7 ^a	$H_2O_2(g) \rightarrow H_2O_2$	34	0.23	Seinfeld and Pandis (2016)
8 ^b	$H_2O_2 \rightarrow H_2O_2(g)$	1.02×10^{5}	-6339	Lind and Kok (1994)
9 ^a	$SO_2(g) \rightarrow SO_2$	64	$[1 + \exp(14.7 - 3825/T)]^{-1}$	Boniface et al. (2000)
10 ^b	$SO_2 \rightarrow SO_2(g)$	1.2	-3157	Olson and Hoffmann (1989)
11 ^a	$CO_2(g) \rightarrow CO_2$	44	2×10^{-4}	Herrmann et al. (2000)
12 ^b	$CO_2 \rightarrow CO_2(g)$	3.11×10^{-2}	-2422	Chameides (1984)
13 ^a	$NH_3(g) \rightarrow NH_3$	17	0.04	Bongartz et al. (1995)
14 ^b	$NH_3 \rightarrow NH_3(g)$	60.7	-3921	Clegg and Brimblecombe (1990)
15 ^a	$HNO_3(g) \rightarrow HNO_3$	63	0.054	Davidovits et al. (1995)
16 ^b	$HNO_3 \rightarrow HNO_3(g)$	2.1×10^{5}	-8696	Lelieveld and Crutzen (1991)
17 ^a	$HCOOH(g) \rightarrow HCOOH$	46	0.012	Davidovits et al. (1995)
18 ^b	$HCOOH \rightarrow HCOOH(g)$	5.53×10^{3}	-5629	Khan and Brimblecombe (1992)
19 ^a	$CH_3COOH(g) \rightarrow CH_3COOH$	60	0.019	Davidovits et al. (1995)
20 ^b	$CH_3COOH \rightarrow CH_3COOH(g)$	5.50×10^{3}	-5894	Khan and Brimblecombe (1992)
21 ^a	$NO_3(g) \rightarrow NO_3$	62	4×10^{-3}	Kirchner et al. (1990);
				Rudich et al. (1996)
22 ^b	$NO_3 \rightarrow NO_3(g)$	0.6	0	Rudich et al. (1996)
23 ^a	$N_2O_5(g) \rightarrow N_2O_5$	108	3.7×10^{-3}	George et al. (1994)
24 ^b	$N_2O_5 \rightarrow N_2O_5(g)$	1.4	0	Herrmann et al. (2000)
25 ^a	$NO_2(g) \rightarrow NO_2$	46	2×10^{-4}	Shao et al. (2019)
26 ^b	$NO_2 \rightarrow NO_2(g)$	1.0×10^{-2}	-2518	Sander (1999);
	2 2 0			Pandis and Seinfeld (1989)
27 ^a	$HO_2NO_2(g) \rightarrow HO_2NO_2$	79	0.1	Jacob (1986)
28 ^b	$HO_2NO_2 \rightarrow HO_2NO_2(g)$	1×10^{5}	0	Herrmann et al. (2000)
29 ^a	$NO(g) \rightarrow NO$	30	0.1	Estimated
30 ^b	$NO \rightarrow NO(g)$	1.9×10^{-3}	-1460	Sander (1999);
	-			Pandis and Seinfeld (1989)
31 ^a	$O_2(g) \rightarrow O_2$	32	0.1	Estimated
32 ^b	$O_2 \rightarrow O_2(g)$	1.3×10^{-3}	0	Sander (1999)

Table 1. Gas-aqueous-phase transfer equilibria. (b) Aqueous-phase chemistry.

^a Reaction rate constant is $k = \frac{3D_g LWC}{\Lambda r^2}$. The unit is per second (hereafter s⁻¹). Gas-phase diffusion coefficient is $D_g = \frac{9.45 \times 10^{17}}{[M]} \sqrt{T(0.03472 + \frac{1}{k_1})}$. LWC is the volume mixing ratio of cloud liquid water. $\Lambda = 1 + (\lambda + 1.3(\frac{1}{k_2} - 1)), \lambda = \frac{0.71 + 1.3\beta}{1 + \beta}, \beta = 4.54 \times 10^{-15} \sqrt{V_g^2 + V_{air}^2}, V_g = \sqrt{\frac{8RT}{\pi k_1}}, V_{air} = \sqrt{\frac{8RT}{28.8\pi}}, R = 8.31 \times 10^7$ is the ideal gas constant (multiplied by a factor to keep V_g and V_{air} in the unit of centimeters per second; hereafter cms⁻¹), *r* is the radius of cloud droplets in centimeters (hereafter cm), and [*M*] is the number density of air in the unit of molecules per cubic centimeter (hereafter molec. cm⁻³). *T* is atmospheric temperature in Kelvin (K). k_1 is the molar mass (grams per mole; hereafter g mol⁻¹). k_2 is the mass accommodation coefficients. All the formulas above refer to Shao et al. (2019) and Liang and Jacobson (1999). ^b Reaction rate constant is $k = \frac{k_{n-1}}{0.082T LWCC}$. The unit is s⁻¹. $C = k_1 \exp(-500k_2(\frac{1}{T} - \frac{1}{298}))$, and k_{n-1} is the rate constant of its reverse reaction with ^a. LWC is as in ^a. k_1 is Henry's law constants (moles per timesphere; hereafter M atm⁻¹) are at 298 K. k_2 is ΔH (joules per mole; hereafter J mol⁻¹)/*R* (joules per mole per Kelvin; hereafter J mol⁻¹ K⁻¹). ΔH is the enthalpy of dissolution. All the formulas above refer to Liang and Jacobson (1999).

 Table 2. Aqueous-phase chemistry.

No.	Reactions	$k_{298}, \mathrm{M}^{-n} \mathrm{s}^{-1} \mathrm{a}$	$E_{\rm a}/R,{\rm K}$	Reference
	Aqueous ionization equilibria			
33	$H_2O_2 \rightarrow H^+ + HO_2^-$	1.26×10^{-2}		De Laat and Le (2005)
34	$H^{+} + HO_{2}^{-} \rightarrow H_{2}O_{2}^{2}$	10 ¹⁰		De Laat and Le (2005)
35	$HO_2 \rightarrow H^{+} + O_2^{-}$	1.14×10^6		Miller et al. (2013)
36	$\mathrm{H^{+}} + \mathrm{O_{2}^{-}} \rightarrow \mathrm{HO_{2}^{-}}$	7.2×10^{10}		Miller et al. (2013)
37	$\rm CO_2 + H_2O \rightarrow H^+ + HCO_3^-$	3.84×10^{4}	9250	Welch et al. (1969);
		10		Graedel and Weschler (1981)
38	$H^+ + HCO_3^- \rightarrow CO_2 + H_2O$	5×10^{10}		Graedel and Weschler (1981)
39	$HCO_3 \rightarrow H^+ + CO_3^-$	2.35	1820	Harned and Owen (1958)
40	$H^+ + CO_3^- \rightarrow HCO_3$	5×10^{10}	5(0)	Graedel and Weschler (1981)
41	$NH_3 + H_2O \rightarrow NH_4 + OH$	6.02×10^{9}	560	Harned and Owen (1958)
42	$NH_4^+ + OH^- \rightarrow NH_3^- + H_2O^-$	3.4×10^{12}	1800	Badlich (1046)
45	$HNO_3 \rightarrow H^+ + NO_3$ $H^+ + NO^- \rightarrow HNO_2$	1.1×10^{10} 5 × 10 ¹⁰	-1800	Graedel and Weschler (1981)
45	$HNO_2 \rightarrow H^+ + NO_2^-$	2.65×10^{7}	1760	Park and Lee (1988)
46	$H^+ + NO_2^- \rightarrow HNO_2$	5×10^{10}	1100	Graedel and Weschler (1981)
47	$HO_2NO_2 \rightarrow H^+ + O_2NO_2^-$	5×10^{5}		Lammel et al. (1990)
48	$H^+ + O_2 NO_2^- \rightarrow HO_2 NO_2$	5×10^{10}		Herrmann et al. (2000)
49	$SO_2 + H_2O \xrightarrow{2} H^+ + HSO_3^-$	6.27×10^4	-1940	Beilke and Gravenhorst (1978);
	- 5			Harned and Owen (1958)
50	$\mathrm{H^{+} + HSO_{3}^{-} \rightarrow SO_{2} + H_{2}O}$	2.0×10^8		Graedel and Weschler (1981)
51	$HSO_3^- \rightarrow H^+ + SO_3^{2-}$	3110	-1960	Beilke and Gravenhorst (1978)
52	$\mathrm{H^{+} + SO_{3}^{2-} \rightarrow HSO_{3}^{-}}$	5×10^{10}		Graedel and Weschler (1981)
53	$HSO_4^- \rightarrow H^+ + SO_4^{2-}$	1.02×10^9	-2700	Redlich (1946)
54	$\mathrm{H^{+} + SO_{4}^{2-} \rightarrow HSO_{4}^{-}}$	1×10^{11}		Graedel and Weschler (1981)
55	$\rm HCOOH \rightarrow H^+ + HCOO^-$	8.85×10^{6}	-12	Harned and Owen (1958)
56	$\rm H^+ + HCOO^- \rightarrow HCOOH$	5×10^{10}		Graedel and Weschler (1981)
57	$CH_3COOH \rightarrow H^+ + CH_3COO^-$	8.75×10^{5}	-46	Harned and Owen (1958)
58	$H^+ + CH_3COO^- \rightarrow CH_3COOH$	5×10^{10}		Graedel and Weschler (1981)
	HO_x chemistry			
59	$H_2O_2 \xrightarrow{hv} 2 OH$	See ref.		Zellner et al. (1990)
60	$O_3 \xrightarrow{H_2O,hv} H_2O_2 + O_2$	See ref.		Graedel and Weschler (1981)
61	$OH + HO_2 \rightarrow H_2O + O_2$	$6.6 imes 10^9$	1500	Sehested et al. (1968); Thomas (1963)
62	$\mathrm{HO}_2 + \mathrm{HO}_2 \rightarrow \mathrm{H}_2\mathrm{O}_2 + \mathrm{O}_2$	8.3×10^5	2700	Bielski et al. (1985)
63	$\mathrm{OH} + \mathrm{H_2O_2} \rightarrow \mathrm{HO_2} + \mathrm{H_2O}$	2.7×10^{7}	1700	Christensen et al. (1982);
				Buxton et al. (1988b)
64	$O_2^- + O_3 \xrightarrow{H_2O} OH + OH^- + 2 O_2$	$1.5 imes 10^9$	1500	Sehested et al. (1983); Bielski et al. (1985)
65	$OH + HSO_{2}^{-} \xrightarrow{O_{2}} SO_{5}^{-} + H_{2}O$	4.5×10^{9}	1500	Huie and Neta (1987)
66	$OH + SO^2 \xrightarrow{O_2} SO^- + OH^-$	5.5×10^9	1500	Huia and Nata (1987).
00	0	5.5 × 10	1500	Adams and Boag (1964); Buxton et al. (1988b)
67	$HCOO^- + OH \xrightarrow{O_2} CO_2 + HO_2 + OH^-$	3.2×10^9	1250	Chin and Wine (1994)
68	$SO_3^{2-} + SO_4^{-} \xrightarrow{O_2} SO_4^{2-} + SO_5^{-}$	$7.5 imes 10^8$	1500	Wine et al. (1989)
69	$HSO_3^- + SO_4^- \xrightarrow{O_2^-} SO_4^{2-} + SO_5^- + H^+$	$7.5 imes 10^8$	1500	Wine et al. (1989)
70	$\mathrm{HSO}_3^- + \mathrm{O}_3 \rightarrow \mathrm{SO}_4^{2-} + \mathrm{H}^+ + \mathrm{O}_2$	3.7×10^5	5530	Hoffmann (1986);
	2	0		Wine et al. (1989)
71	$SO_3^{2-} + O_3 \rightarrow SO_4^{2-} + O_2$	1.5×10^{9}	5280	Hoffmann (1986); Wine et al. (1989)
72	$SO_4^- + OH^- \rightarrow SO_4^{2-} + OH$	8.0×10^7	1500	Maruthamuthu and Neta (1978)
73	$SO_4^- + H_2O_2 \rightarrow H^+ + SO_4^{2-} + HO_2$	1.2×10^{7}	2000	Wine et al. (1989)
74	$\mathrm{SO}_4^- (+\mathrm{H_2O}) \rightarrow \mathrm{SO}_4^{2-} + \mathrm{H^+} + \mathrm{OH}$	440	1850	Bao and Barker (1996)
75	$SO_4^- + HCOO^- \xrightarrow{O_2} SO_4^{2-} + CO_2 + HO_2$	1.1×10^8	1500	Reese et al. (1997); Wine et al. (1989)
76	$HCOOH + OH \rightarrow H_2O + CO_2 + HO_2$	1.1×10^{8}	1000	Chin and Wine (1904)
77	$O_3 + H_2O_2 + OH^- \rightarrow OH + O_2^- + O_2 + H_2O_2$	4.4×10^8	-4000	Staehelin and Hoigne (1982)

Table 2. Continueu.

No.	Reactions	k_{298} , M ⁻ⁿ s ^{-1a}	$E_{\rm a}/R,{\rm K}$	Reference
78	$SO_4^- + HO_2 \rightarrow SO_4^{2-} + H^+ + O_2$	5.0×10^{9}	1500	Jacob (1986)
79	$SO_4^- + O_2^- \rightarrow SO_4^- + O_2$	5.0×10^{9}	1500	Jacob (1986)
80	$HCOO^- + O_3 \rightarrow CO_2 + OH + O_2^-$	1.0×10^2	5500	Hoigne and Bader (1983b)
81	$SO_5^- + HCOO^- \xrightarrow{O_2} HSO_5^- + CO_2 + O_2^-$	1.4×10^4	4000	Jacob (1986)
82	$SO_5^- + HSO_3^- \xrightarrow{O_2} HSO_5^- + SO_5^-$	2.5×10^4	3850	Huie and Neta (1987)
83	$HSO_5^- + OH \rightarrow SO_5^- + H_2O$	1.7×10^{7}	1900	Maruthamuthu and Neta (1977)
84	$HSO_5^{-} + HSO_3^{-} + H^+ \rightarrow 2 SO_4^{2-} + 3 H^+$	1.7×10^7	2000	Mcelroy (1987); Betterton and Hoffmann (1988)
85	$SO_5^- + HSO_3^- \rightarrow SO_4^- + SO_4^{2-} + H^+$	$7.5 imes 10^4$	3500	Huie and Neta (1987)
86	$O_2^- + SO_5^- \xrightarrow{H_2O}O_2 + HSO_5^- + OH^-$	$1.0 imes 10^8$	1050	Jacob (1986)
87	$OH + HSO_3^- \xrightarrow{O_2^-} SO_4^{2-} + H^+ + HO_2$	4.5×10^{9}		Huie and Neta (1987)
88	$OH + O_3 \rightarrow HO_2 + O_2$	2.0×10^9		Buhler et al. (1984)
89	$HO_2 + O_2 \xrightarrow{H} H_2O_2 + O_2$	9.7×10^{7}	1060	Bielski et al. (1985)
90	$\Omega_2^- + \Omega_2^- \rightarrow \Omega_2^- + \Omega_2^-$	1.1×10^{10}	2120	Christensen et al. (1989)
91	$HSO_2^- + OH \rightarrow H_2O + SO_2^-$	2.7×10^{9}		Buxton et al. $(1996b)$
92	$SO_2^{2-} + OH \rightarrow OH^- + SO_2^-$	4.6×10^{9}		Buxton et al. (1996b)
93	$HSO_3^- + H_2O_2 + H^+ \rightarrow SO_4^{2-} + H_2O + 2 H^+$	6.9×10^{7}	4000	Lind et al. (1987)
94	$SO_2 + O_3 \xrightarrow{H_2O} HSO_7 + O_2 + H^+$	2.4×10^{4}		Hoffmann (1986)
95	$SO_2^- + SO_2^- \rightarrow S_2O_2^{2-} + O_2$	1.8×10^{8}	2600	Herrmann et al. (1995)
96	$SO_{5}^{-} + SO_{5}^{-} \rightarrow 2SO_{8}^{-} + O_{2}$	7.2×10^{6}	2600	Herrmann et al. (1995)
97	$SO_5^- + HO_2 \rightarrow HSO_5^- + O_2$	1.2×10^9	2000	Buyton et al. $(1996a)$
98	$SO_5^- + O_2 \rightarrow SO_5^-$	2.5×10^9		Buxton et al. (1996b)
99	$SO_3^- + O_2^- \rightarrow BO_5^- + SO_3^-$ $SO_5^- + HSO_3^- \rightarrow HSO_5^- + SO_3^-$	8.6×10^3		Buxton et al. (1996b)
100	$SO^{-} + SO^{2-} \xrightarrow{H^{+}} HSO^{-} + SO^{-}$	2.13×10^5		Puyton at al. (1006b)
100	$so_5^- + so_3^2 \rightarrow so_5^- + so_3^2$	2.13×10^{5}		Buxton et al. (1996b)
101	$30_5 + 30_3 \rightarrow 30_4 + 30_4$	3.5×10^{5}		Tang et al. (1990b)
102	$OH + HSO_4 \rightarrow H_2O + SO_4$ $SO^- + USO^- \rightarrow SO^{2-} + SO^- + U^+$	3.3×10^{-10}		$\mathbf{P}_{\text{respective}} = \mathbf{r}_{\text{respective}} \left(1988 \right)$
103	$SO_4 + HSO_3 \rightarrow SO_4 + SO_3 + H^2$	3.2×10^{8}	1200	Reese et al. (1997)
104	$SO_4 + SO_3^- \rightarrow SO_4^- + SO_3^-$ $HSO^- + SO^{2-} + H^+ \rightarrow 2SO^{2-} + 2H^+$	3.2×10^{6} 7 14 × 10 ⁶	1200	Reese et al. (1997) Betterton and Hoffmann (1988)
105	$\frac{O_2}{O_2} = \frac{O_2}{O_2} = $	7.14 × 10		Detterion and Hormann (1966)
106	$HCOOH + SO_4 \longrightarrow SO_4^- + H^+ + HO_2 + CO_2$	2.5×10^{6}		Reese et al. (1997)
107	$O_2 + H_2O_2 \rightarrow OH + OH + O_2$	0.13		Bielski et al. (1985)
108	$OH + OH \rightarrow H_2O_2$	5.5×10^{-2}		Miller et al. (2013)
1109	$H_2O_2 + HO_2 \rightarrow H_2O + O_2 + OH$	0.7 × 107		$D_{2} L \text{ act and } L_{2} (2005)$
110	$HO_2 + O_2 \rightarrow HO_2 + O_2$ $O_2^{2-} + U_2^{+} \rightarrow HO_2^{-}$	9.7 × 10		De Laat and Le (2005)
111	$O_2 + H^+ \rightarrow HO_2$ $SO^- + SO^- \rightarrow S^2O^{2-}$	4.5×10^8		De Laat and Le (2005) Buyton et al. $(1996b)$
112	$30_4 + 30_4 \rightarrow 320_8$	4.5 × 10		
113	$OH + O_3 \longrightarrow H_2O_2 + O_2 + OH$	70 2.8106	2500	Staehelin and Hoigne (1982)
114	$HO_2 + O_3 \rightarrow OH + O_2 + O_2$	2.8×10^{-3}	2500	Staenelin and Holgne (1982)
115	$H_2O_2 + O_3 \rightarrow H_2O + 2O_2$ $HCOOH + O_3 \rightarrow CO_2 + HO_2 + OH$	$7.8 \times 10^{-5} [O_3]^{-5.0}$	0	Hoigne and Bader (1983a)
117	$SO_2 + H_2O_2 \xrightarrow{H_2O} SO^{2-} + 2H^+ + H_2O_2$	7.5×10^{7}	4430	Mcardle and Hoffmann (1983)
118	$SO_2^2 + H_2O_2 \rightarrow SO_4^2 + H_2O_2$	7.5×10^7	//30	Meardle and Hoffmann (1983)
119	$SO_3^- + SO_2^{-0_2,H_2O} HSO_5^- + SO_5^- + OH^-$	2.5×10^4	2000	Huie and Neta (1987)
120	$SO_5^- + HCOOH \xrightarrow{O_2} HSO_5^- + CO_2 + HO_2$	200	5300	Jacob (1986)
121	$SO_2 + HO_2 \xrightarrow{H_2O} SO_4^{2-} + OH + 2 H^+$	1.0×10^6	0	Hoffman and Calvert (1985)
122	$HSO_2^- + HO_2 \rightarrow SO_4^{2-} + OH + H^+$	1.0×10^{6}	0	Hoffman and Calvert (1985)
123	$SO_3^2 + HO_2 \rightarrow SO_4^2 + OH$	1.0×10^{6}	0	Hoffman and Calvert (1985)
124	$SO_2 + O^{-} \xrightarrow{H_2O}{H_2O} SO^{2-} + OU + U^+$	1.0×10^{5}	0	Hoffman and Calvert (1985)
124	$HSO_{2}^{-} + O_{2}^{-} \rightarrow SO_{4}^{-} + OH$	1.0×10^{-5}	0	Hoffman and Calvert (1985)
106	$SO_{4}^{2} + O_{4}^{2} + O_{4}^{2} + O_{4}^{2} + O_{4}^{2}$	1.0 105	0	Hoffman and Calvert (1985)
126	$SO_3 + O_2 \longrightarrow SO_4^- + OH + OH$ H ₂ O 2	1.0×10^{-5}	0	Hollman and Calvert (1985)
127	$SO_3^- + SO_3^- \xrightarrow{-} SO_3^{} + H^+ + HSO_4^-$	0.37		Fischer and Warneck (1996)

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Table 2. Continued.
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No.	Reactions		$k_{298}, \mathrm{M}^{-n} \mathrm{s}^{-1} \mathrm{a}$	$E_{\rm a}/R,{\rm K}$	Reference
	Fe chemistry				
128	$FeOH^{2+} \xrightarrow{hv} Fe^{2+} + OH$		See ref.		Benkelberg and Warneck (1995)
129	$\operatorname{FeSO}_4^+ \xrightarrow{hv} \operatorname{Fe}^{2+} + \operatorname{SO}_4^-$		See ref.		Benkelberg and Warneck (1995)
130	$H_2O_2 + Fe^{2+} \rightarrow FeOH^{2+} + OH$	$63 + (3 \times 10^{-10})$	$[\mathrm{H}^+]^{-1} 5.9 \times 10^6)$		Millero and Sotolongo (1989)
131	$Fe^{2+} + O_3 \xrightarrow{H_2O} FeOH^{2+} + OH + O_2$		8.2×10^5		Logager et al. (1992)
132	$\operatorname{FeOH}^{2+} + \operatorname{HSO}_{3}^{-} \xrightarrow{\operatorname{O}_{2}} \operatorname{Fe}^{2+} + \operatorname{SO}_{4}^{2-} + \operatorname{H}_{2}\operatorname{O}$	[FeOH ²⁺]	$\times 1 \times 10^9$		Martin et al. (1991)
133	$O_3 + Fe^{2+} \rightarrow FeO^{2+} + O_2$		8.2×10^5		Logager et al. (1992)
134 135	$H_{2}O_{2} + FeO^{2+} \rightarrow FeOH^{2+} + HO_{2}$ $HO_{2} + FeO^{2+} \rightarrow FeOH^{2+} + O_{2}$		9.5×10^{-5} 2.0 × 10 ⁶	2800	Jacobsen et al. (1997) Jacobsen et al. (1997)
126	$HO_2 + HO_2 + HO_2$		2.0 × 10 ⁷		
150	$OH + FEO + FEOH + H_2O_2$		1.0 × 10		Jacobsen et al. (1992),
137	$FeO^{2+} + H_2O \rightarrow FeOH^{2+} + OH$		1.3×10^{-2}	4100	Jacobsen et al. (1997)
138	$FeO^{2+} + Fe^{2+} \xrightarrow{H_2O} 2 FeOH^{2+}$		7.2×10^4	840	Jacobsen et al. (1997)
139	$FeO^{2+} + Fe^{2+} \xrightarrow{H_2O} Fe(OH)_2Fe^{4+}$		$1.8 imes 10^4$	5050	Jacobsen et al. (1997)
140	$Fe(OH)_2Fe^{4+} \rightarrow 2 FeOH^{2+}$		0.49	8800	Jacobsen et al. (1997)
141	$HNO_2 + FeO^{2+} \rightarrow FeOH^{2+} + NO_2$		1.1×10^{4}	4150	Jacobsen et al. (1998)
142	$NO_2^- + FeO^{2+} \xrightarrow{\Pi^+} FeOH^{2+} + NO_2$		1.0×10^5		Jacobsen et al. (1998)
143	$HSO_3^- + FeO^{2+} \rightarrow FeOH^{2+} + SO_3^-$		2.5×10^{5}		Jacobsen et al. (1998)
144	$HCOOH + FeO^{2+} + FeOH^{2+} + CO_2 + HO_2$		160	2680	Jacobsen et al. (1998)
145	$HCOO^{-} + FeO^{2+} \xrightarrow{H^+,O_2} FeOH^{2+} + CO_2 + HO_2$		3.0×10^{5}		Jacobsen et al. (1998)
146	$\text{FeOH}^{2+} + \text{HSO}_3^- \rightarrow \text{FeSO}_3^+ + \text{H}_2\text{O}$		4.0×10^{6}		Lente and Fabian (2002)
147	$FeSO_3^+ + H^+ \xrightarrow{OH} FeOH^{2+} + HSO_3^-$		2.08×10^3		Lente and Fabian (2002)
148	$\operatorname{FeSO}_3^+ \to \operatorname{Fe}^{2+} + \operatorname{SO}_3^-$		0.19		Lente and Fabian (2002)
149	$\operatorname{Fe}^{2+} + \operatorname{SO}_{3}^{-} \to \operatorname{Fe}\operatorname{SO}_{3}^{+}$	2.0 105 7 6 106	$3.0 \times 10^{\circ}$	5605	Buxton et al. (1999)
150	$\operatorname{FeOH}^2 + \operatorname{SO}_3 \rightarrow \operatorname{Fe}^2 + \operatorname{HSO}_4$	$3.0 \times 10^{5} + 7.6 \times 10^{6}$	$\times 1.64 \times 10^{-5} [H^+]^{-1}$	1100	Warneck (2018) Christenson and Schooted (1081)
151	$H_2\Omega_2 + F_2\Omega H^{2+} \rightarrow H\Omega_2 + H_2\Omega + F_2^{2+}$		4.3×10^{-3}	1100	Walling and Goosen (1973)
152	$O_2^- + FeOH^{2+} \rightarrow O_2 + Fe^{2+} + OH^-$		1.5×10^{8}		Rush and Bielski (1985)
154	$HO_2 + FeOH^{2+} \rightarrow Fe^{2+} + O_2 + H_2O$		1.3×10^5		Ziajka et al. (1994)
155	$O_2^- + Fe^{2+ \frac{H^+, H_2O}{2}}H_2O_2 + FeOH^{2+}$		1.0×10^7		Rush and Bielski (1985)
156	$HO_2 + Fe^{2+} \xrightarrow{H_2O} H_2O_2 + FeOH^{2+}$		1.2×10^6	5050	Jayson et al. (1973)
157	$NO_3 + Fe^{2+} \xrightarrow{OH^-} NO_3^- + FeOH^{2+}$		8×10^6		Pikaev et al. (1974)
158	$\text{FeOH}^{2+} + \text{HSO}_3^- \rightarrow \text{Fe}^{2+} + \text{SO}_3^- + \text{H}_2\text{O}$		39		Ziajka et al. (1994)
159	$Fe^{2+} + SO_5^{-} \xrightarrow{H_2O} FeOH^{2+} + HSO_5^{-}$		4.3×10^7		Herrmann et al. (1996)
160	$Fe^{2+} + HSO_5^- \rightarrow FeOH^{2+} + SO_4^-$		3×10^4		Ziajka et al. (1994)
161	$Fe^{2+} + SO_4^{-} \xrightarrow{H_2O}{H_2O} FeOH^{2+} + SO_4^{2-} + H^+$		$3.5 imes 10^7$		Ziajka et al. (1994)
162	$\operatorname{Fe}^{2+} + \operatorname{S_2O_8^{2-}} \xrightarrow{\operatorname{H_2O}} \operatorname{FeOH}^{2+} + \operatorname{SO_4^{2-}} + \operatorname{SO_4^{-}} + \operatorname{H^+}$		17		Buxton et al. (1997)
163	$SO_4^- + Fe^{2+} \rightarrow FeSO_4^+$		3×10^{8}		Mcelroy and Waygood (1990)
164	$\text{FeOH}^{2+} + \text{SO}_4^{2-} \rightarrow \text{FeSO}_4^+ + \text{OH}^-$		3.2×10^{3}		Brandt and Vaneldik (1995)
165	$\operatorname{FeSO}_4^+ \xrightarrow{\operatorname{OH}} \operatorname{FeOH}^{2+} + \operatorname{SO}_4^{2-}$		1.8×10^5		Brandt and Vaneldik (1995)
166	$Fe^{2+} + O_2 \xrightarrow{OH} FeOH^{2+} + O_2^{-}$		$8.8 imes 10^{-2}$		Santana-Casiano et al. (2005)
167	$Fe^{2+} + O_2^- \xrightarrow{OH} FeOH^{2+} + O_2^{2-}$		107		De Laat and Le (2005)
168	$O_2^- + FeSO_4^+ \rightarrow Fe^{2+} + SO_{4_2}^{2-} + O_2$		1.5×10^{8}		Rush and Bielski (1985)
169	$HO_2 + FeSO_4^+ \rightarrow Fe^{2+} + SO_2^{-+} + O_2 + H^+$ $Fe^{2+} + H_2O_4 \rightarrow FeO^{2+} + H_2O_4$		1.0×10^3		Rush and Bielski (1985)
	$re + r_2O_2 \rightarrow reO + r_2O$		See lei.		
	IN CREMISTRY				
171	$NO_2 \xrightarrow{\text{II} \ \mu \to 0} NO + OH$		See ref.		Zellner et al. (1990)
172	$NO_3 \xrightarrow{\longrightarrow} NO_2 + OH$		See ref.		Zellner et al. (1990)
173	$N_2 \cup 5 + H_2 \cup \rightarrow 2 H^+ + 2 N \cup_3$		5×10^{9}	2700	Herrmann et al. (2000)
174	$NO_3 + OII \rightarrow NO_3 + OII$ $NO_3 + H_2O_2 \rightarrow NO_2^- + H^+ + HO_2$		9.4×10^{7} 4.9×10^{6}	2000	Herrmann et al. (1992)

Table 2.	Continued.
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No.	Reactions	$k_{298}, \mathrm{M}^{-n} \mathrm{s}^{-1} \mathrm{a}$	$E_{\rm a}/R,{\rm K}$	Reference
176	$NO_3 + HSO_3^- \rightarrow NO_3^- + H^+ + SO_3^-$	1.3×10^{9}	2000	Exner et al. (1992)
177	$NO_3 + SO_3^{2-} \rightarrow NO_3^{-} + SO_3^{-}$	3.0×10^8		Exner et al. (1992)
178	$NO_3 + HSO_4^- \rightarrow NO_3^- + H^+ + SO_4^-$	2.6×10^5		Raabe (1996)
179	$NO_3 + SO_4^{2-} \rightarrow NO_3^{-} + SO_4^{-}$	5.6×10^3		Logager et al. (1993)
180	$NO_2 + OH \rightarrow NO_3^- + H^+$	1.2×10^{10}		Wagner et al. (1980)
181	$NO_2 + O_2^- \rightarrow NO_2^- + O_2$	1×10^8		Warneck and Wurzinger (1988)
182	$NO_2 + NO_2 \xrightarrow{H_2O} HNO_2 + NO_3^- + H^+$	8.4×10^7	-2900	Park and Lee (1988)
183	$O_2 NO_2^- \rightarrow NO_2^- + O_2$	4.5×10^{-2}		Lammel et al. (1990)
184	$NO_2^- + NO_3 \rightarrow NO_3^- + NO_2$	1.4×10^{9}	0	Herrmann and Zellner (1998)
185	$SO_4^- + NO_3^- \rightarrow SO_4^{2-} + NO_3$	5.0×10^{4}		Exner et al. (1992)
186	$HCOOH + NO_3 \xrightarrow{O_2} NO_3^- + H^+ + HO_2 + CO_2$	3.8×10^5	3400	Exner et al. (1994)
187	$HCOO^- + NO_3 \xrightarrow{O_2} NO_3^- + HO_2 + CO_2$	5.1×10^7	2200	Exner et al. (1994)
188	$NO_2 + HO_2 \rightarrow HO_2NO_2$	1.0×10^7		Warneck and Wurzinger (1988)
189	$\mathrm{HO_2NO_2} \rightarrow \mathrm{NO_2} + \mathrm{HO_2}$	4.6×10^{-3}		Warneck and Wurzinger (1988)
190	$\mathrm{SO}_4^- + \mathrm{NO}_2^- \rightarrow \mathrm{SO}_4^{2-} + \mathrm{NO}_2$	9.8×10^8	1500	Wine et al. (1989)
191	$NO + NO_2 \xrightarrow{H_2O} 2 NO_2^- + 2 H^+$	2.0×10^{8}	1500	Lee (1984)
192	$NO + OH \rightarrow NO_2^- + H^+$	2.0×10^{10}	1500	Strehlow and Wagner (1982)
193	$HNO_2 + OH \rightarrow \dot{NO}_2 + H_2O$	1.0×10^{9}	1500	Rettich (1978)
194	$NO_2^- + OH \rightarrow NO_2 + OH^-$	1.0×10^{10}	1500	Treinin and Hayon (1970)
195	$HNO_2 + H_2O_2 \xrightarrow{H^+} NO_2^- + 2 H^+ + H_2O_2$	$6.3 \times 10^3 [\text{H}^+]$	6693	Lee and Lind (1986)
196	$NO_2^- + O_3 \rightarrow NO_2^- + O_2$	5.0×10^{5}	6950	Damschen and Martin (1983)
197	$NO_3^2 + HO_2 \rightarrow NO_2^2 + H^+ + O_2$	4.5×10^{9}	1500	Jacob (1986)
198	$NO_3 + O_2^- \rightarrow NO_3^- + O_2$	1.0×10^9	1500	Jacob (1986)
199	$2 \text{ NO}_2 + \text{HSO}_2 \xrightarrow{\text{H}_2\text{O}} \text{SO}_4^{2-} + 3 \text{ H}^+ + 2 \text{ NO}_2^{-}$	2.0×10^{6}	0	Lee and Schwartz (1983) ^c
200	$NO_2 + NO_2 \rightarrow N_2O_4$	4.5×10^{8} b		Graedel and Weschler (1981)
201	$N_2O_4 \xrightarrow{H_2O} 2 H^+ + NO_2^- + NO_2^-$	$1.0 \times 10^3 \text{ b}$		Graedel and Weschler (1981)
202	$NO_3 + H_2O \rightarrow NO_3^- + OH + H^+$	6.0	4500	Rudich et al. (1996)
203	$NO_3^- + OH + H^+ \rightarrow NO_3 + H_2O$	1.4×10^8		Rudich et al. (1996)
204	$HSO_5^- + NO_2^- \rightarrow HSO_4^- + NO_3^-$	0.31	6646	Edwards and Mueller. (1962)
205	$HO_2NO_2 + HSO_3^- \rightarrow HSO_4^- + NO_3$	3.5×10^5		Amels et al. (1996)
	Carbonate chemistry			
206	$\mathrm{HCO}_3^- + \mathrm{O}_2^- \rightarrow \mathrm{HO}_2^- + \mathrm{CO}_3^-$	1.5×10^{6}	0	Schmidt (1972)
207	$\mathrm{CO}_3^- + \mathrm{H}_2\mathrm{O}_2 \to \mathrm{HO}_2 + \mathrm{HCO}_3^-$	8.0×10^{5}	2820	Behar et al. (1970)
208	$\mathrm{CO}_2^- + \mathrm{O}_2 \rightarrow \mathrm{O}_2^- + \mathrm{CO}_2$	2.4×10^{9}		Tan et al. (2009)
209	$\mathrm{CO}_3^- + \mathrm{O}_2^- \to \mathrm{CO}_3^{2-} + \mathrm{O}_2$	6.8×10^{8}		Tan et al. (2009)
210	$\text{CO}_3^- + \text{HCOO}^- \rightarrow \text{HCO}_3^- + \text{CO}_2^-$	1.5×10^{5}		Tan et al. (2009)
211	$NO_2^- + CO_3^- \rightarrow CO_3^{2-} + NO_2$	6.6×10^{5}	850	Huie et al. (1991)
212	$HCOO^- + CO_3^- \xrightarrow{O_2^-} CO_3^{2-} + HO_2 + CO_2$	1.4×10^{5}	3300	Zellner et al. (1996)
213	$HCO_3^- + OH \rightarrow H_2O + CO_3^-$	1.7×10^{7}	1900	Exner (1990)
214	$CO_3^{2-} + OH \rightarrow OH^- + CO_3^-$	3.9×10^{8}	2840	Buxton et al. (1988b, a)
215	$\mathrm{CO}_3^{2-} + \mathrm{SO}_4^{-} \rightarrow \mathrm{SO}_{4_2}^{2-} + \mathrm{CO}_3^{-}$	4.1×10^{7}		Herrmann et al. (2000)
216	$\mathrm{HCO}_{3}^{-} + \mathrm{SO}_{4}^{-} \rightarrow \mathrm{SO}_{4}^{2-} + \mathrm{CO}_{3}^{-} + \mathrm{H}^{+}$	2.8×10^6	2090	Huie and Clifton (1990)
217	$\text{CO}_3^{2-} + \text{NO}_3 \rightarrow \text{NO}_3^- + \text{CO}_3^-$	4.1×10^{7}		Herrmann et al. (2000)
218	$CO_3^- + CO_3^- \xrightarrow{O_2^-} 2 O_2^- + 2 CO_2$	2.2×10^6		Huie and Clifton (1990)
219	$CO_3^- + Fe^{2+} \xrightarrow{OH} CO_3^{2-} + FeOH^{2+}$	2×10^7		Herrmann et al. (2000)
220	$\dot{\text{CO}_3} + \text{HO}_2 \rightarrow \text{HCO}_3 + \text{O}_2$	$6.5 imes 10^8$		Herrmann et al. (2000)
221	$\text{CO}_3^- + \text{HSO}_3^- \rightarrow \text{HCO}_3^- + \text{SO}_3^-$	1×10^7		Herrmann et al. (2000)
222	$CO_3^- + SO_3^{2-} \to CO_3^{2-} + SO_3^{}$	$5.0 imes 10^6$	470	Huie et al. (1991)

^a *n* is the reaction order -1. The units are s⁻¹ for first-order reactions and moles per liter per second (hereafter $M^{-1} s^{-1}$) for second-order reactions. Reaction rate constant is $k = k_{298} \exp(-\frac{E_a}{R}(\frac{1}{T} - \frac{1}{298}))$. ^b The temperature for *k* is 293 K. ^c Referenced from https://www.osti.gov/biblio/6567096 (last access: 27 August 2021).

in Tables 1 and 2, coupled with default gas chemistry. In the non-cloudy part, the calculation is similar to the original case but still without parameterized aqueous-phase reactions. Finally, the concentration in each grid is the average of the cloudy and non-cloudy results weighted by F_{cld} .

The time step used in this study is the default 30 min in CESM2. In the improved case, the lifetime of clouds (i.e., the time between the formation and evaporation of clouds) is set equal to the time step. At t = 0 of each time step, all the cloud droplets are assumed to be instantaneously and simultaneously formed according to the cloud-related variables, such as LWC, F_{cld} , and r, and all the water-soluble species (listed in Table 1) are dissolved into the cloud droplets according to the effective Henry's law constants. The pH value of each grid cell is calculated by the ionization equilibria of ionizable species (listed in Table 2) and the dissociation of CCN (including sulfate, nitrate, and ammonium), assuming that equilibrium and electroneutrality are continuously maintained. Such pH values can directly influence the formation of aqueous-phase sulfate and nitrate of this time step. At the same time, a given initial concentration of soluble Fe³⁺ $(5 \,\mu\text{M})$ is allocated into each cloud droplet. When $t = 30 \,\text{min}$, all the cloud droplets are assumed to instantaneously evaporate. All the species remaining in the aqueous phase are transferred directly back to the gas phase. Low-volatility species such as ammonium, sulfate, and nitrate are released directly back to the atmosphere as inorganic aerosols. Meanwhile, the newly formed sulfate and nitrate will further influence the ionization equilibria and the calculation of pH values in the next step, thus forming a fully coupled feedback system between pH values and concentrations of sulfate and nitrate.

On the basis of the improved case, more sensitivity cases are simulated to explore the influences of different factors (e.g., the concentration of soluble Fe and the pH value) on the capacity for SO_2 oxidation. The process of all these simulations is the same as that of the improved case. The detailed description of all the model simulations used in this study is summarized in Table S1 in the Supplement.

Finally, all the simulations are running for a 2 year period, from 1 January 2014 to 31 December 2015. The first year is used for model spin-up. In this study, we used the information at https://svn-ccsm-inputdata.cgd. ucar.edu/trunk/inputdata/input/atm/cam/inic/fv/ (cami-chem_1990-01-01_0.9x1.25_L30_c080724.nc, last access: 31 December 2021) as the initial data and boundary conditions to provide the initial values of all the physical variables and concentrations of all the chemical species. The output of the simulation is in the form of a daily mean and is then converted to a monthly or seasonal mean for research needs.

2.4 Observations for evaluation of global simulation

For the model evaluation, the observational data used in this study are collected from four monitoring networks. The observations in Europe (EU) are obtained

from the European Monitoring and Evaluation Programme (EMEP, 2020; https://www.emep.int/, last access: 8 August 2020). The observations in the United States of America (USA) are obtained from the U.S. Environmental Protection Agency Air Quality System (United States Environmental Protection Agency, 2020; https://aqs.epa.gov/aqsweb/airdata/download_files.html#Raw, last access: 19 July 2020). The observations in China (CN) are obtained from the China National Environmental Monitoring Center (CNEMC; https://quotsoft.net/air/, last access: 22 December 2020). The observations in Japan and South Korea (JK) are obtained from the Acid Deposition Monitoring Network in East Asia (EANET; https://monitoring.eanet.asia/document/public/index, last access: 2 November 2020). The locations of monitoring stations are shown in Fig. 1. All observational data were collected from 1 January 2015 to 31 December 2015. The monthly averages used for analysis of the results are calculated from raw daily averages or even hourly averages collected from the measurement networks above. For convenience of comparison, the units of simulated concentration of SO₂ are all converted to the forms in corresponding observational data.

3 Effects of in-cloud aqueous-phase chemical mechanisms on the simulation of SO₂

3.1 Simulation of SO₂ in the original case

Figure 2 shows the seasonally averaged surface mixing ratios of SO₂ in the original simulation. There are huge spatial and temporal differences in the global distribution of SO₂. On the one hand, the mixing ratios of SO_2 are no more than 0.1 ppbv in most parts of the world and are basically concentrated in Asia, EU, North America (NA), and southern Africa (SA) and especially in central and eastern CN. The mixing ratios in NA and EU are mainly in the ranges of 0.1– 5 and 1-10 ppbv, respectively. The mixing ratios in EU are slightly higher than those in NA. Meanwhile, the mixing ratios in the eastern USA are evidently higher than those in the western USA. In EA, the mixing ratios in JK range from 0.1 to 5 ppbv throughout the year. The mixing ratios in most of central and eastern CN are in the range of 10-50 ppbv and are even higher than 50 ppbv in some regions, which are much higher than those in other regions. In addition, similar to the USA, the mixing ratios in central and eastern CN are much higher than those in western CN. Such distributions are directly related to the high emissions of SO₂ in these regions of CN (Jo et al., 2020; Xie et al., 2016; Geng et al., 2019).

On the other hand, the mixing ratios of SO_2 are remarkably different in the four seasons. They are highest in winter, followed by spring and autumn, and lowest in summer, especially in Asia and NA. Such seasonal differences are related to both emissions and the capacity for SO_2 oxidation in the



Figure 1. Locations of monitoring sites from various measurement networks in (a) Europe (EU; EMEP), (b) USA (EPA), and (c) East Asia (EA; red points for CNEMC and blue points for EANET).



Figure 2. Global distribution of seasonally averaged surface mixing ratios of SO₂ (in parts per billion by volume; hereafter ppbv) in 2015, simulated by CESM2 with standard configuration (i.e., the original case). DJF, MAM, JJA, and SON represent December–January–February, March–April–May, June–July–August and September–October–November, respectively, with the same below.

gas phase. In winter, due to the increase in heating demand, the combustion of fossil fuels such as coal could significantly increase the emissions of SO₂ (Jo et al., 2020; Xie et al., 2016; Geng et al., 2019; Feng et al., 2020). At the same time, higher temperatures and stronger sunlight could enhance the gas-phase oxidation of SO₂ in summer, which is the opposite in winter. Such phenomena are consistent with multiple studies (Alexander et al., 2009; Huang et al., 2014; Tilgner et al., 2013; Shao et al., 2019).

3.2 Differences between the original and improved simulations

After replacement of default parameterized aqueous-phase reactions with detailed in-cloud aqueous-phase chemistry,

the surface mixing ratios of SO_2 generally decrease markedly, as shown in Fig. 3. The extent of the reduction is distinct in different regions and seasons. In general, reductions in SO_2 mainly occur in Asia, EU, NA, and SA. The mixing ratios of SO_2 decrease the most in CN, followed by EU, and the least in NA and JK. These results are partly due to the relatively high background mixing ratios in these regions in the original simulation. Therefore, all the distribution patterns above are also similar to those in the original simulation. The reductions in SO_2 also differ in various seasons. In NA and EU, the mixing ratios of SO_2 in most regions are reduced by 0.1–5 and 1–10 ppbv in winter, respectively. In spring and autumn, the mixing ratios mainly decrease by 0.1–5 ppbv, which is slightly less than that in winter. How-



Figure 3. The differences in global seasonally averaged surface SO_2 mixing ratios between the improved case and the original case in 2015, after the incorporation of detailed in-cloud aqueous-phase chemical mechanisms (ppbv).

ever, the reduction in SO₂ in summer is very limited. Notably, the mixing ratios in some areas even increase slightly, which is partly due to the replacement of the default parameterized aqueous-phase reactions. Sometimes these simplified and parameterized reactions are even stronger than detailed radical reactions, especially in summer. Similar to Fig. 2, Fig. 3 shows that the decline in SO₂ mixing ratios in the eastern USA is larger than that in the western USA, which is also related to the background mixing ratios in the original case. However, the situation is different in EA. The mixing ratios decrease significantly in all seasons in central and eastern CN. The reduction is always more than 1 ppbv, sometimes even greater than 10 ppbv. Again, the reductions in central and eastern CN are higher than that in western CN. These results are also partly related to the background mixing ratios. The decrease in JK ranges from 0.1 to 5 ppbv throughout the year, without obvious fluctuation.

With regard to the relative differences between the original and improved cases, the results seem slightly different, as shown in Fig. S1 in the Supplement. Although the reduction sequence is winter > autumn > spring > summer in general, which is very similar to the results above, the regional differences are no longer distinct. In winter, the mixing ratios of SO₂ decrease more than 50 % in most regions of EU and NA but no more than 50 % in central and eastern CN. In contrast, the reductions are very small in EU, NA, and JK in summer. However, the decreases exceed 10 % in CN and even 50 % in some regions (e.g., Shanxi, Hebei, Zhejiang, and Fujian provinces).

Such enhancement of the oxidation capacity can also be reflected in the net chemical loss rate of SO₂. Figure S2 shows the ratio of the net chemical loss rates between the improved and original simulations. The net chemical loss rate increases in most parts of the world (ratios > 1). The seasonal differences in the ratios are winter > autumn > spring > summer, which is still similar to the results above. The ratios in NA and JK are all more than 20 times greater and even above 100 times higher in some regions. Those in EU are more than 20 times greater in winter but less than 10 times higher in summer. The multiples in western CN are all more than 20 times greater and even more than 100 times greater in some regions, which are much higher than those in eastern CN, which are only less than 10 times greater.

3.3 Comparison between the simulated and observed SO₂ concentrations

The regional annual average mixing ratios between the simulated and *observed* SO₂ are summarized in Table 3. At the same time, scatterplots of SO₂ over various sites in the four monitoring networks are also shown in Fig. S3. Clearly, the effect of detailed aqueous-phase chemistry on the improvement in the SO₂ simulation is remarkable. The annual average mixing ratios in the original case are 4.3, 1.5, 2.0, and

Table 3. Comparison of regional annual average values among the observed, original-simulated, and improved-simulated SO_2 mixing ratios (ppbv) in EU, USA, CN, and JK in 2015. The observed mixing ratios are calculated by averaging the data from all monitoring stations of various measurement networks. The simulated mixing ratios are calculated by averaging the data from all the grids where the monitoring stations are located.

Region	Monitoring network	Obs	Ori	Imp
EU	EMEP*	0.38	2.0	1.0
US	EPA	1.1	2.7	1.6
CN	CNEMC*	10	30	23
JK	EANET	0.54	1.4	0.78

* The original units of EMEP and CNEMC are in micrograms of sulfur per cubic meter (hereafter μ g S m⁻³) and micrograms per cubic meter (hereafter μ g m⁻³), respectively. To facilitate compari-

son, these two units are converted to ppbv. Units conversion is as follows: $1 \mod \log_{air}^{-1} = 1 \times 10^9 \text{ ppbv} = \frac{64 \times 10^6 P_{air}}{RT_{air}} \, \mu \text{g m}^{-3} = \frac{32 \times 10^6 P_{air}}{RT_{air}} \, \mu \text{g S m}^{-3}$. The values of 64 and 32 are molar masses of SO₂ and S, respectively. The value of 10⁶ is the unit conversion coefficient between grams (hereafter g) and micrograms (hereafter μg). $R = 8.314 \, \text{J} \, \text{mol}^{-1} \, \text{K}^{-1}$ is the ideal gas constant. T_{air} (288 K used here) is atmospheric temperature in K. P_{air} (1.013 × 10⁵ Pa used here) is atmospheric pressure in Pascal (hereafter Pa). The same applies below.

1.6 times overestimated in EU, USA, CN, and JK, respectively. After incorporating the detailed aqueous-phase chemistry, these values are reduced by 46%, 41%, 22%, and 43%, respectively. The slopes of the linear fitting lines are all close to or even approximately equal to 1 in EU, USA, and JK.

The comparison between the simulated and observed monthly average mixing ratios of SO₂ in the four monitoring networks is shown in Fig. 4. The relative differences between the original and improved simulations are also shown in Fig. S4. According to these two figures, compared with the observations, the original simulation is generally overestimated in all regions, especially in winter. Coupling the detailed in-cloud aqueous-phase chemical mechanisms greatly improves the simulation of SO₂. In EU, aqueous-phase reactions significantly improve the simulation of SO₂ from October to February. The simulated mixing ratios decrease by more than 60 % from the original case to the improved case and even by more than 75% in December. The improved mixing ratios for 6 months are within the standard deviation of observations. The results in the USA are even better than those in EU. The mixing ratios of SO₂ decrease more in winter, spring, and autumn (-30% to -70%) than in summer. All improved mixing ratios are within the standard deviation of observations. Although the absolute reduction in SO_2 over CN is the greatest, the relative improvement in CN is the least due to the excessively high original mixing ratios of SO₂. None of the simulated mixing ratios decrease by more than 40 %. None of the improved mixing ratios are within the standard deviation of observations. The aqueous-phase reactions also greatly improve the simulation in JK. The relative differences in the four seasons are all close (approximately -30% to -60%). Almost all the improved mixing ratios are also within the standard deviation of observations.

Overall, the overestimation in winter is more serious than that in summer. At the same time, the improvement from adding aqueous-phase chemistry is much greater in winter than in summer, especially in EU and USA. These results indicate the importance of incorporating detailed aqueousphase chemistry in winter and are highly consistent with the results of some existing studies (Shao et al., 2019; Ma et al., 2018; Huang et al., 2019). Such seasonal differences may be related to the ambient temperature, humidity, and especially sunlight. In summer, both the temperature and sunlight are sufficient to generate a high concentration of •OH (Lakey et al., 2016). Therefore, gas-phase oxidation is strong and dominant (Cheng et al., 2016). However, due to the weak sunlight in winter, the gas-phase concentration of •OH is 2 or 3 orders of magnitude less than that in summer. In addition, the rate constant is also less than one-third to onehalf of that in summer, owing to the decrease in temperature. Therefore, the gas-phase photochemical oxidation of SO₂ induced by •OH is sharply weakened. These changes indicate the greatly increased importance of aqueous-phase reactions (Elser et al., 2016; Ervens, 2015; Harris et al., 2013; Huang et al., 2018). At the same time, higher humidity and more cloud coverage can provide a more sufficient aqueous environment, which is also beneficial to improve the performance of aqueous-phase reactions, such as those that occur during winter in EU and USA and summer in EA.

4 Contributions of different aqueous-phase chemical mechanisms to the oxidation of SO₂

On the basis of the above analysis of the overall detailed aqueous-phase chemistry, it is necessary to discuss the contributions of different aqueous-phase chemical mechanisms in detail. Cases for four different mechanisms are performed with the corresponding reactions in Tables 1 and 2. See Table S1 for details about the configuration of individual cases. Given the fact that the HO_x chemistry involves most of the critical radicals in aqueous-phase chemistry, the cases of Fe, N, and carbonate chemistry also include the HO_x chemistry. The individual contribution of Fe, N, or carbonate chemistry is compared with the HO_x chemistry case alone.

Figure 5 shows the effects of HO_x chemistry, Fe chemistry, N chemistry, and carbonate chemistry on surface SO₂ (case $3 \sim 6$ – case 1). Remarkable differences are clearly seen among these four mechanisms. On the one hand, generally speaking, the contributions from both HO_x chemistry and Fe chemistry to the oxidation of SO₂ are significant. Nonetheless, the seasonal and regional distribution properties of these two chemical mechanisms are obviously different. For HO_x chemistry, the mixing ratios of SO₂ decrease in most parts of the world, and the seasonal differences



Figure 4. Regional monthly average mixing ratios (ppbv) of SO₂ in EU, USA, CN, and JK in 2015. The black, red, and green lines represent the observed, original-simulated, and improved-simulated mixing ratios, respectively. The gray areas represent the standard deviation of observed mixing ratios. The corresponding monitoring networks are (a) EMEP, (b) EPA, (c) CNEMC, and (d) EANET.

are very small. The reductions generally range from 0.01 to 0.1 ppbv over the ocean and 0.1-5 ppbv over land. With regard to Fe chemistry, however, the reduction in SO₂ is mostly concentrated on land only, especially in the Northern Hemisphere. The seasonal properties of the reductions are nearly the same as those described in Sect. 3.2. On the other hand, these two chemical mechanisms contribute much more than N chemistry to the oxidation of SO₂. The decrease in SO₂ exceeds 1 ppbv in many regions of Asia, EU, and NA due to the effects of Fe chemistry or HO_x chemistry. However, the contribution of N chemistry almost never exceeds 1 ppbv. Such a great disparity may be related to the level of Fe concentrations and pH values in cloud water, which are discussed in Sect. 5. With regard to carbonate chemistry, however, it is difficult to see consistent change in either spatial or temporal SO₂ distribution. The mixing ratios of SO₂ decrease in some places and seasons but increase in other places and seasons. Moreover, all the changes are very small, within ± 0.1 ppbv. Therefore, carbonate chemistry has no significant effect on the oxidation of SO₂.

The contributions of the different chemical mechanisms discussed above can also be seen from the relative differences, as shown in Fig. S5. HO_x chemistry contributes the most over the ocean in the Southern Hemisphere. At the same time, Fe chemistry contributes the most over land in the Northern Hemisphere. The mixing ratios of SO₂ decrease by more than 50 % in both mechanisms. Furthermore, note that, although the contribution of carbonate chemistry is quite small, there is an evident decrease over the ocean in the Southern Hemisphere.

5 Factors affecting the capacity for SO₂ oxidation from aqueous-phase reactions

5.1 The concentration of soluble Fe

The concentrations of soluble $[Fe^{3+}]$ are all set to $5 \mu M$ in the improved case. Nevertheless, $[Fe^{3+}]$ varies greatly in different regions, seasons, and ambient conditions. For instance, $[Fe^{3+}]$ is generally no more than 0.1 μM under marine condi-



Figure 5. The differences in global seasonally averaged surface SO_2 mixing ratios (ppbv) in 2015 with the incorporation of HO_x chemistry, Fe chemistry, N chemistry, and carbonate chemistry individually from top to bottom, respectively.

tions and no more than 1 µM under remote continental conditions (Herrmann et al., 2000; Matthijsen et al., 1995; Deguillaume et al., 2005; Mao et al., 2013; Jacob, 2000; Shao et al., 2019; Li et al., 2017). In many polluted cities, [Fe³⁺] is much higher than that in remote regions, usually ranging from 5 to 20 µM and sometimes even exceeding 100 µM (Matthijsen et al., 1995; Deguillaume et al., 2005; Herrmann et al., 2000; Mao et al., 2013; Jacob, 2000; Li et al., 2017). Therefore, in this study, four other levels of initial $[Fe^{3+}]$ (0.1, 1, 20, and 100 µM) are tested with the whole in-cloud aqueousphase reactions to evaluate the influence of soluble Fe concentration on the capacity for SO₂ oxidation. The processing $[Fe^{3+}]$ in these sensitivity cases is identical to the improved case, except for the differences in Fe³⁺ concentrations. All the levels of $[Fe^{3+}]$ are based on the reported values above. See Table S1 for details.

The regional monthly average mixing ratios of SO₂ in four regions are shown in Fig. 6. In all four regions, the simulated SO₂ first still increases in summer when initial [Fe³⁺] is 0.1 μ M and then decreases considerably when initial [Fe³⁺] increases from 0.1 to 5 μ M but declines only slightly when initial [Fe³⁺] increases to 20 μ M. The two lines of [Fe] = 20 μ M and [Fe] = 100 μ M almost overlap and cannot be distinguished clearly in EU, USA, and JK. Only in CN do the mixing ratios of SO₂ further decrease obviously when initial [Fe³⁺] increases from 5 to 100 μ M. There are many steel and coal factories and power plants in CN. These results imply that there may be a strong correlation between high emissions of SO_2 and iron, and that the concentrations of Fe in CN may be higher than those in other regions.

Such an effect on the capacity for SO₂ oxidation by $[Fe^{3+}]$ chemistry can also be seen in Fig. S6. The capacity for SO₂ oxidation is enhanced with increasing $[Fe^{3+}]$ on the whole. When initial $[Fe^{3+}]$ is only 0.1 µM, the effect of Fe chemistry is still quite weak. The effect is rapidly enhanced when initial $[Fe^{3+}]$ increases from 0.1 to 5 µM. However, such enhancement becomes markedly less when initial $[Fe^{3+}]$ is greater than 20 µM. The mixing ratios of SO₂ is almost unchanged when initial $[Fe^{3+}]$ increases to 100 µM. This result indicates that the effect of increasing $[Fe^{3+}]$ on the capacity for SO₂ oxidation has a threshold. Too much $[Fe^{3+}]$ will not further facilitate the oxidation of SO₂. The reason for such a limitation is discussed below.

In any case, a higher concentration of soluble Fe results in an improvement in the SO_2 simulation compared to the observations.

5.2 The pH value

As mentioned in the Introduction, the pH value in cloud water is a key parameter for aqueous-phase chemistry, which could directly affect ionization equilibria and gas–aqueous mass transfer processes. There are expressions for the rate constants of several aqueous-phase reactions, and some expressions include pH values directly. Therefore, the pH value could affect the various aqueous-phase reaction rates, espe-



Figure 6. Regional monthly average mixing ratios (ppbv) of SO₂ in EU, USA, CN, and JK in 2015. The black and red lines represent the observed and original-simulated mixing ratios of SO₂, respectively. Other lines represent SO₂ mixing ratios with different soluble [Fe³⁺]. [Fe³⁺], from top to bottom, is 0.1, 1, and 5 (i.e., the improved case) and 20 and 100 μ M, respectively. The gray areas represent the standard deviation of observed mixing ratios. The corresponding monitoring networks are (**a**) EMEP, (**b**) EPA, (**c**) CNEMC, and (**d**) EANET.

cially that of N chemistry (Shao et al., 2019; Li et al., 2017; Cheng et al., 2016; He et al., 2018; He and He, 2020). Therefore, it is necessary to discuss the influence of the variation in the pH value on the capacity for SO₂ oxidation. In this study, there are four sets of pH values (i.e., 3, 4, 5, and 6) prescribed in the following sensitivity tests (Table S1). All the pH values are referenced from previous studies (Herrmann et al., 2000; Matthijsen et al., 1995; Shao et al., 2019; Guo et al., 2017; Cheng et al., 2016). [Fe³⁺] is set to 5 μ M. However, it is difficult to see obvious differences among these four pH levels in all seasons. Only a small decrease in SO₂ can be seen in most regions from pH 3 to 4. The reduction in SO₂ is almost the same from pH 4 to 6. This result indicates that the effect of increasing the pH value on the capacity for SO₂ oxidation is limited. The global distributions of SO_2 in different seasons, shown in Fig. S7, have similar features. Although the capacity for SO_2 oxidation increases to some extent from pH 3 to 4 in all four regions, the changes from pH 4 to 6 are very small.

Notwithstanding, a higher pH value doubtless enhances the capacity for SO_2 oxidation and results in simulated values that are closer to the observations, which is similar to the influence of the soluble Fe concentration (Shi et al., 2019; Shao et al., 2019; Li et al., 2017; Cheng et al., 2016).

It seems that the influence of the pH value on the aqueousphase chemistry is much weaker than that of the soluble Fe concentration. When further discussing the effect of the pH value on N chemistry, HO_x chemistry, or Fe chemistry individually, however, the situation is quite different, as shown in Table S1 and Figs. S8–S10. When the pH increases from 3 to 6, the capacity for SO₂ oxidation from N chemistry and HO_x chemistry is evidently enhanced at all times. When the pH is 6, the oxidation capacity from N chemistry and HO_x chemistry becomes almost as strong as that from Fe chemistry with a high concentration of soluble Fe. This indicates that the capacity for SO₂ oxidation from N chemistry and HO_x chemistry is greatly affected by the pH value (Wang et al., 2020; Cheng et al., 2016; He et al., 2018; L. Li et al., 2018; He and He, 2020). In contrast, the capacity for SO₂ oxidation from Fe chemistry is the opposite. When [Fe³⁺] is set at the default medium level (5 μ M), regardless of the pH, there are no remarkable changes in the SO₂ mixing ratios, and the capacity for SO₂ oxidation from Fe chemistry is nearly the same, especially when the pH ranges from 4 to 6. This indicates that the Fe chemistry is not significantly affected by pH.

These results explain well why the contribution of N chemistry is much smaller than that of Fe chemistry and HO_x chemistry in Sect. 4. According to the simulation, the pH value in cloud water is generally in the range of 3–5. This pH range is highly consistent with those in previous studies (Herrmann et al., 2000; Matthijsen et al., 1995; Shao et al., 2019; Guo et al., 2017; Cheng et al., 2016). As seen in Fig. 5, the capacity for SO₂ oxidation from N chemistry is between pH 4 and 5, which is still not strong enough. Consequently, the capacity for SO₂ oxidation from N chemistry is largely limited by the relatively low pH values in cloud water.

As analyzed in the sections above, it is worth noting that, regardless of the high soluble Fe concentration or high pH value for different chemical mechanisms, the reduction in SO₂ always seems to reach a very similar limitation, and the global distribution and regional monthly average mixing ratios are also almost the same. This is not only related to soluble Fe concentration, pH value, or the chemical properties of various mechanisms themselves but is also derived from the exhaustion of $SO_2(aq)$ by detailed aqueous-phase chemistry in a finite cloud. The aqueous-phase chemistry cannot affect regions without clouds because the total SO₂ is calculated by weighted averages of cloudy and non-cloudy conditions, according to F_{cld} . The overestimated SO₂ is sometimes caused by a shortage of clouds, especially in CN. Therefore, only more cloud coverage or lower emissions may further reduce the overestimation.

Consequently, it is easy to conclude that the oxidation capacity of Fe chemistry and HO_x chemistry is much higher than that of N chemistry when the pH is less than 5, but evaluating their relative importance at high pH is difficult. The cloud content and substrate concentration become the limiting factors. Therefore, a comprehensive investigation of cloud pH in different seasons and at different places is urgently needed.

5.3 Discussion and uncertainty analysis

Recent studies show that hydroxymethanesulfonate (HMS), formed by aqueous-phase reactions of dissolved HCHO and SO_2 , is an abundant organosulfur compound in aerosols during winter haze episodes and suggest that aqueous clouds act as the major medium for HMS chemistry (Moch et al., 2020; Song et al., 2021). Therefore, it is necessary to further investigate the influence of this organic chemistry on the incloud aqueous-phase chemistry system in CESM2. We tried to incorporate 10 aqueous-phase organic species and 60 related reactions, including the reactions related to CH₃OH, HCHO, CH₃OOH, and HMS, as shown in Table S2a and b. We conducted additional simulations for testing the contribution from this organic chemistry. As shown in Fig. S11, incorporating this organic chemistry has a minor effect on SO₂ concentrations, similar to that of carbonate chemistry.

In addition to the soluble Fe concentration and pH value discussed above, there are some other factors that may also affect the capacity for SO₂ oxidation and increase the uncertainty of the simulation. First, the simulation of variables related to cloud properties (such as LWC, F_{cld} , and r) directly determines the contribution of aqueous-phase chemistry. However, the simulation of these variables is also one of the greatest uncertainties (Zhang et al., 2019; Faloona, 2009). In addition, the initial valence of soluble Fe and the proportion of various valences are related to the capacity of Fe chemistry. The higher the proportion of Fe^{3+} , the stronger the atmospheric oxidizability and the more helpful it is for the oxidation of SO₂ (Jacob, 2000; Deguillaume et al., 2005; Huang et al., 2014; Alexander et al., 2009). Moreover, the emissions and solubility of Fe vary greatly in different regions. For instance, the total concentration of atmospheric Fe is generally measured in the range of $1-1000 \text{ ng m}_{air}^{-3}$, and the solubility of elemental Fe varies from less than 1% to 10 % (Cwiertny et al., 2008; Hsu et al., 2010, 2013; Sedwick et al., 2007; Sholkovitz et al., 2009; Heal et al., 2005; Ingall et al., 2018; Mao et al., 2013; Itahashi et al., 2018; Shelley et al., 2018; Mcdaniel et al., 2019; Conway et al., 2019; Shi et al., 2020; Myriokefalitakis et al., 2018; Wang et al., 2015). Meanwhile, the simulated LWC usually ranges from 10^{-8} to $10^{-5} L_{water} L_{air}^{-1}$ in CESM2 and other model studies (Herrmann et al., 2000, 2015; Jacob, 1986; Matthijsen et al., 1995; J. Liu et al., 2012). In addition, F_{cld} should also be considered. Therefore, the concentration of soluble Fe can be calculated in a range from less than 10^{-3} to $10^3 \mu$ M, involving great uncertainties. It is also the reason why the dust aerosol is simulated but not coupled with soluble Fe in this study. At the same time, the proportions of aerosols containing sulfate, nitrate, and ammonium in the aqueous phase could directly affect the pH of cloud water. The simulated pH value of cloud water itself is one of the sources of uncertainty (Shi et al., 2019; Xue et al., 2016). Finally, some sources of kinetic parameters for the aqueous-phase reactions are outdated. They may also not be accurate enough because measurement conditions in the laboratory are different from the conditions of the real atmosphere. These issues influence the accuracy of the reaction rates and increase the uncertainty of the simulation.



Figure 7. Regional monthly average mixing ratios (ppbv) of SO₂ in EU, USA, CN, and JK in 2015. The black and red lines represent the observed and original-simulated mixing ratios of SO₂, respectively. Other lines represent SO₂ mixing ratios at different pH values. The pH values, from top to bottom, are 3, 4, 5, and 6, respectively. $[Fe^{3+}]$ is set to 5 μ M. The gray areas represent the standard deviation of observed mixing ratios. The corresponding monitoring networks are (**a**) EMEP, (**b**) EPA, (**c**) CNEMC, and (**d**) EANET.

In addition, there are factors that affect the performance of the simulation to a certain degree. First, an accurate emission inventory is the premise for improving the simulation (Im et al., 2018; De Meij et al., 2006; Liu et al., 2018; Buchard et al., 2014). The data sources and resolutions of various emission types could affect the reliability of the inventory. For instance, regardless of how the parameters discussed above are optimized, the concentration of SO₂ in CN is always overestimated, which may be related to the uncertainties in emission inventories. The emissions of SO₂ in CN have decreased considerably in recent years, which may lead to biases in the simulations (Jo et al., 2020; Xie et al., 2016; Geng et al., 2019). Meanwhile, the meteorological data include information on the water content, wind, temperature, and pressure, which all influence the formation and movements of clouds. Therefore, the reliability of meteorological data is also related to the uncertainty of simulations with incloud chemistry (Bei et al., 2017; Liu et al., 2007). At the same time, the simulation of the SO_2 wet deposition process also involves great uncertainty. Furthermore, the selection of monitoring stations determines the quality of observational data. As a global model, CESM2 used in this study has a resolution that is still not fine enough to accurately simulate regions that are too remote or too close to pollution sources. The simulation of each grid can represent only the average level of a region. Therefore, the monitoring stations should also represent the average level of the region. Otherwise, the limitation of the model resolution also increases the deviation of the comparison with observations and the uncertainty of the simulations. Finally, there are slight numerical fluctuations during the calculation of the model itself, but the uncertainty from the fluctuations is very small and can be ignored, especially after the results are averaged.

6 Conclusions

To improve the global simulation of SO_2 in this study, we used CESM2 to evaluate the effects of detailed in-cloud aqueous-phase reaction mechanisms on the capacity for SO₂ oxidation. After the replacement of default simplified and parameterized aqueous-phase reactions with detailed in-cloud aqueous-phase reactions, the overestimation of surface SO₂ generally decreases significantly. The reductions vary in different regions and seasons. Most them are in the range of 0.1– 10 ppbv, and some can be greater than 10 ppbv in some regions of CN. The net chemical loss rate of SO₂ also increases substantially. When compared with the observations, the simulated values that incorporate detailed aqueous-phase chemistry improve greatly, making the simulations much closer to the observations. The biases of annual average simulated mixing ratios decrease by 46%, 41%, 22%, and 43% in EU, USA, CN, and JK, respectively. The mixing ratio even decreases by approximately 70 % in winter in EU, which is very close to the observed value. The mixing ratios of SO₂ in CN are still highly overestimated, although they decrease considerably. Aqueous-phase chemistry contributes more in EU, USA, and JK than in CN, which may be related to cloud coverage and emissions.

The contribution of each aqueous-phase mechanism to the simulation of SO₂ also differs significantly. Fe chemistry and HO_x chemistry contribute more to the capacity for SO₂ oxidation than N chemistry. Carbonate chemistry has no significant effect on the oxidation of SO2. Several factors could influence the capacity for SO₂ oxidation. Higher concentrations of soluble Fe and higher pH values could further enhance the oxidation capacity and improve the simulation of SO₂. In addition, the oxidation capacities from N chemistry and HO_x chemistry are strongly affected by pH values and increase rapidly with increasing pH. The oxidation capacity from Fe chemistry is almost unaffected by pH. Many other factors also affect the aqueous-phase chemistry and the simulation of SO₂. Regardless of which factor changes, there is still a limitation on the improvement in the simulations because of limited cloud coverage in the aqueous phase.

This study emphasizes the importance of aqueous-phase chemical mechanisms for SO₂ oxidation. These mechanisms are helpful to improve the simulation of SO₂ by CESM2, deepening the understanding of SO₂ oxidation and the formation of sulfate, PM2.5, and even hazy days. A better simulation of SO₂ is a prerequisite for better representing sulfate, which further influences cloud microphysics, radiation transfer, and climate change.

However, some aspects still need to be further studied and improved in the future. For instance, there is a high degree of uncertainty in the concentration of soluble Fe owing to the dramatically large variation in the total atmospheric Fe content and Fe solubility in different regions. At the same time, there are few observational data or emission inventories of soluble Fe. Therefore, the contribution of Fe chemistry to the capacity for SO₂ oxidation is uncertain under different atmospheric conditions and difficult to evaluate accurately. Meanwhile, many variables and parameters related to the simulated clouds are also uncertain, such as LWC, F_{cld} , r, pH values in clouds, wet deposition processes, and proportions of inorganic aerosols in the aqueous phase. Therefore, it is urgently necessary to compare these variables with observational data if possible. Moreover, the effect of aqueousphase chemistry on SO₂ at high altitude is not discussed in this study. These issues will be examined in our future work.

Code availability. The Community Earth System Model 2 (CESM2) developed by the National Center for Atmospheric Research can be downloaded (https://www.cesm.ucar.edu/models/ cesm2/, CESM Working Groups of National Center for Atmospheric Research, 2020a). All codes used to generate the results of this study are available from the authors upon request.

Data availability. The CMIP6 emission data sets analyzed during the current study are available at https://svn-ccsm-inputdata.cgd. ucar.edu/trunk/inputdata/atm/cam/chem/ (CESM Working Groups of National Center for Atmospheric Research, 2020b). The MERRA-2 meteorological offline data are publicly available from https://rda.ucar.edu/datasets/ds313.3/ (Data Engineering and Curation Section of the Computational and Information Systems Laboratory at the National Center for Atmospheric Research, 2020).

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