



Supplement of

Kinetics and impacting factors of HO₂ uptake onto submicron atmospheric aerosols during the 2019 Air QUALity Study (AQUAS) in Yokohama, Japan

Jun Zhou et al.

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45 [bin/trajtype.pl?runtype=archive](http://ready.arl.noaa.gov/hypub-bin/trajtype.pl?runtype=archive) vi

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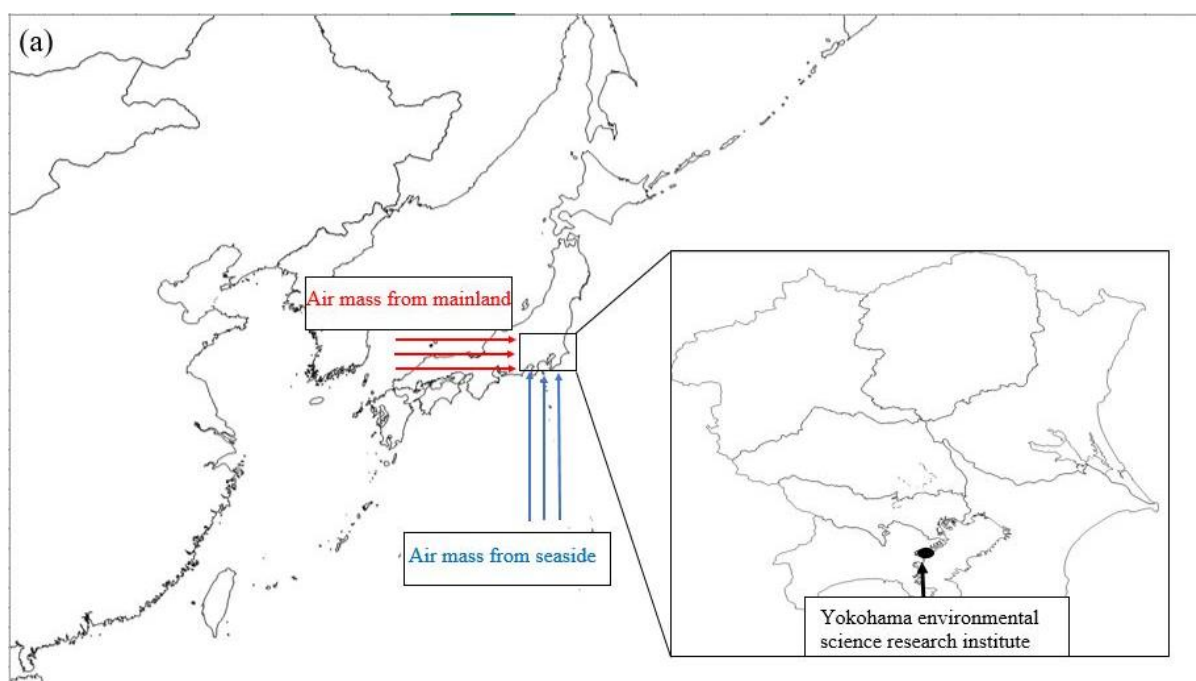
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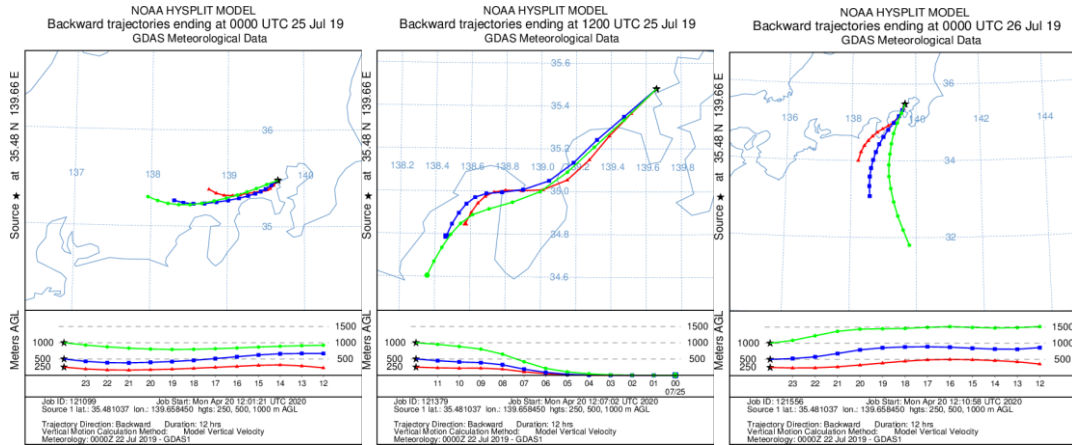
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Air mass directions

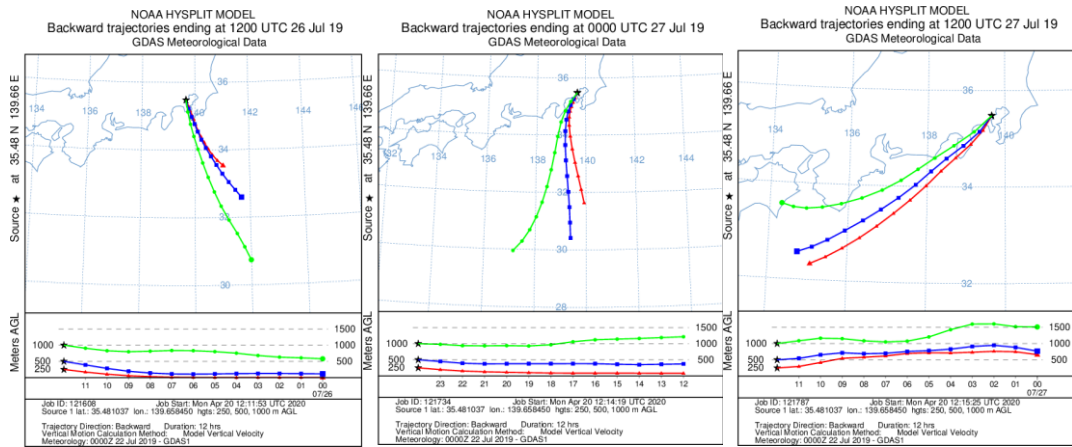
Figure S1a shows air mass direction schematic diagram during the campaign. For each day, the Internet-Based HYSPLIT Trajectory Model and gridded meteorological data (Global Data Assimilation System, GDAS1) from the U.S. National Oceanic and Atmospheric Administration (NOAA) were used during the modeling, the tested results of all experimental days are listed in Fig. S1b. Backward trajectories ended at local time 00:00 am and 12:00 pm after a total run time of 12 h. Results suggesting that arriving air mass can be classified into two categories (i) from the sea to the north direction towards Yokohama City (~19% of the experimental period: from 12:00 pm Jul. 25 to 12:00 Jul. 27, 2019); (ii) from the mainland towards Yokohama City (~81% of the experimental period).



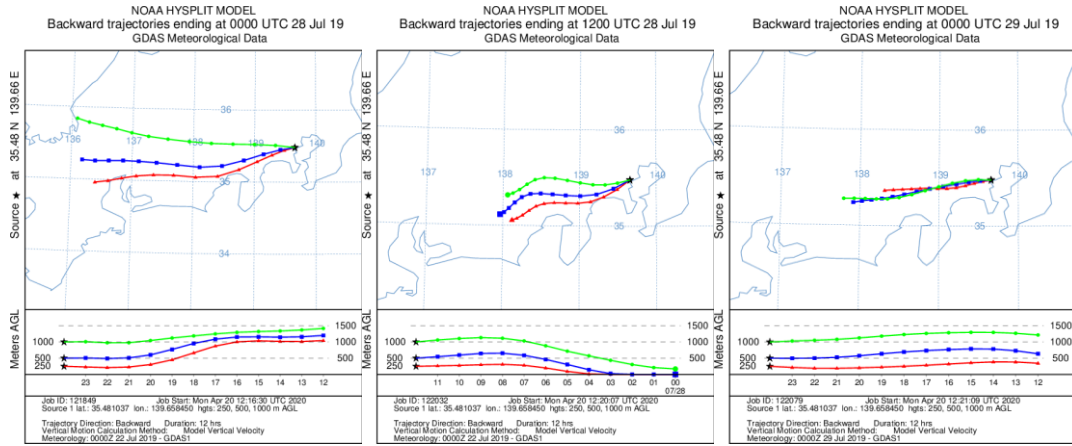
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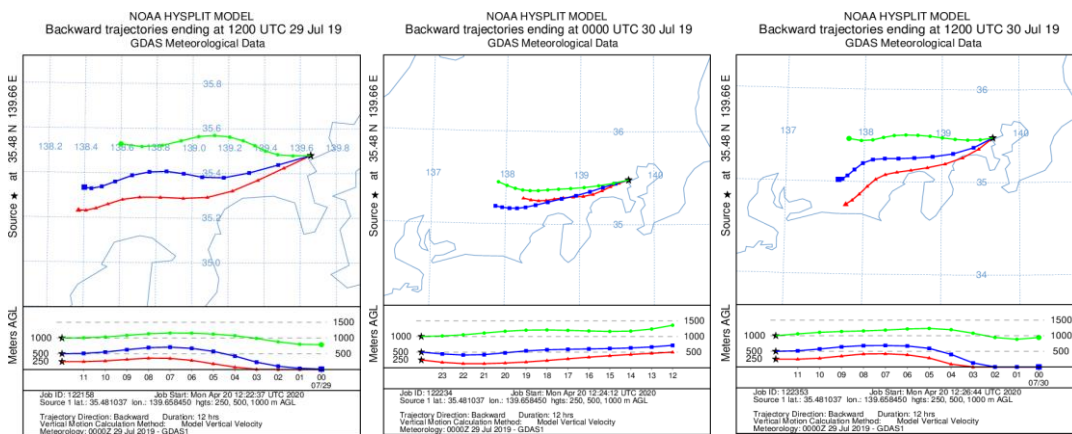
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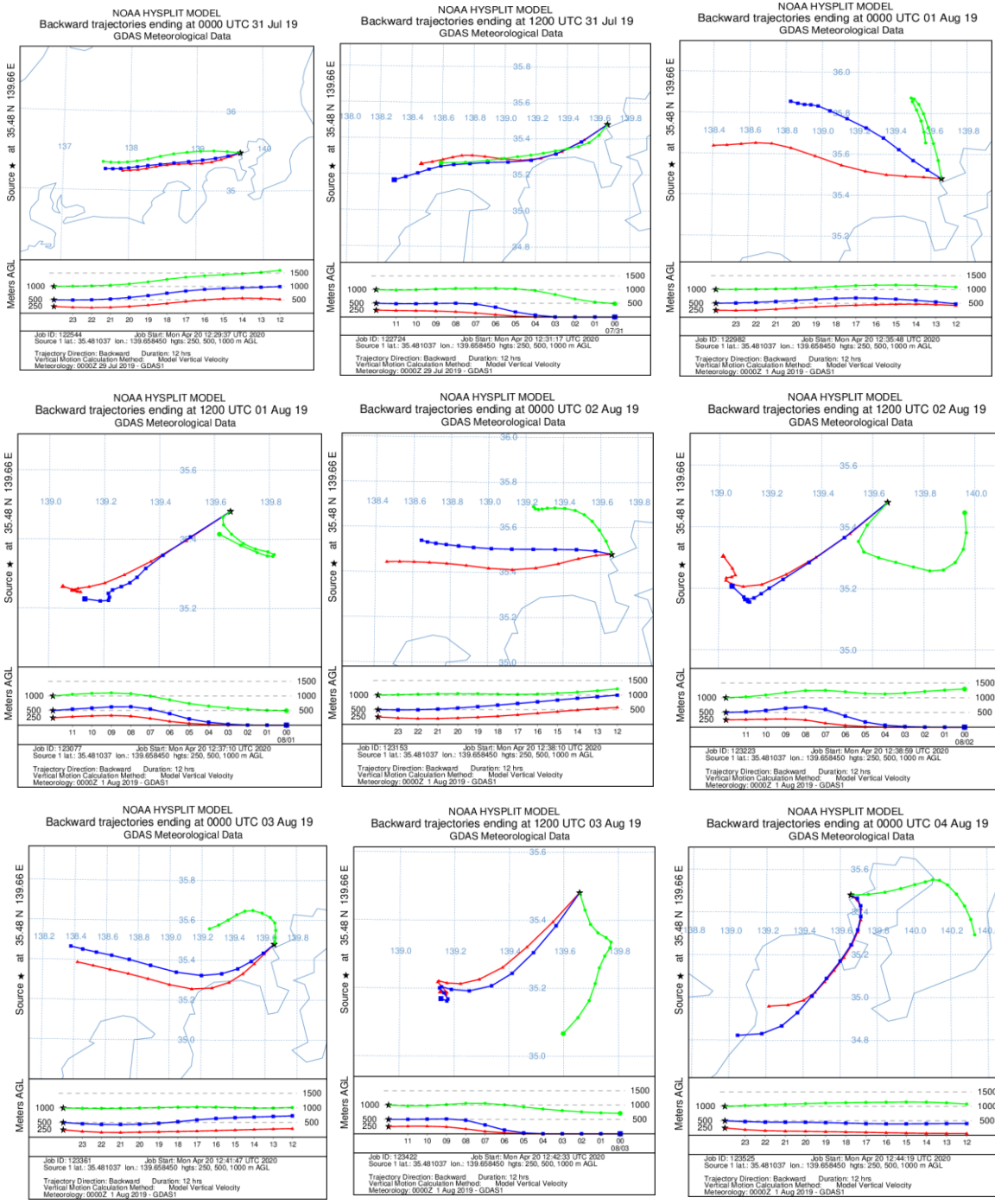
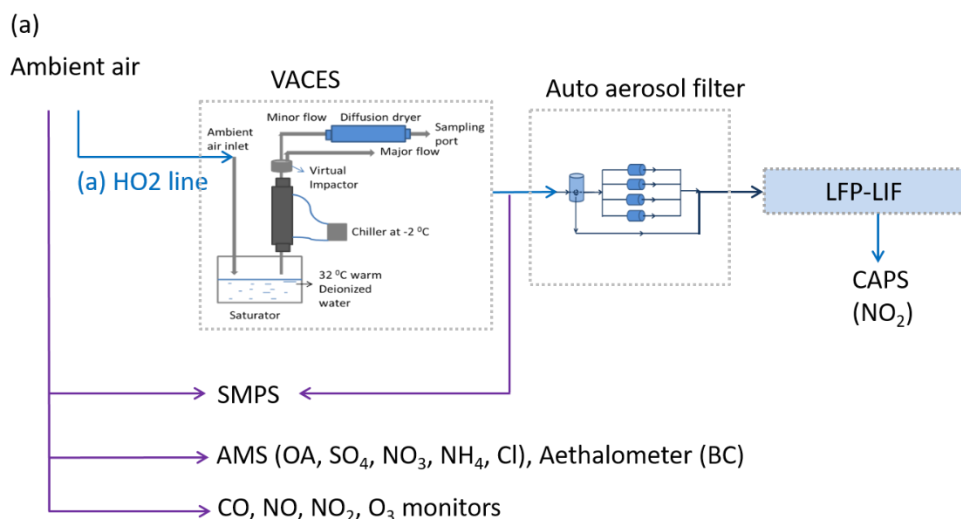


Figure S1: (a) Air mass direction schematic diagram; (b) NOAA-HYSPLIT model showing back trajectories for ~ 11 days sample periods from 12:00 July 24 to 00:00 August 04, 2019 (back trajectories ending 00:00 UTC 25 July to 00:00 August 04, 2019) from the sampling site. Arriving air masses 250 m, 500 m, and 1000 m above ground level (AGL) were calculated using the following website: <http://ready.arl.noaa.gov/hypub-bin/trajtype.pl?runtype=archive>

Measurement strategy

The HO₂ reactivity was measured using LFP–LIF, adapted from a laser-induced pump and probe OH reactivity measurement technique, which has been validated and employed for the total gas phase HO_x (=OH+HO₂) reactivity and HO_x uptake kinetics onto ambient aerosols in field^{1, 2-4}. We further coupled this system with a versatile aerosol concentration enrichment system (VACES) to enrich the ambient aerosols to compensate the relatively low limit of detection (LOD) for the HO₂ reactivity measurement. A schematic of the experimental system is shown in Fig. S2a, and a detailed abstract of the measurement process of the HO₂ reactivity of the ambient aerosol phase is shown in Fig. S2b. The ambient air was drawn into the VACES, where the aerosol concentration was enriched. The ambient air was then sampled using a three-port valve (Bolt, Flon Industry Co., LTD) and injected into the LFP–LIF system at a flow rate of 8 L min⁻¹. The valve was switched automatically between two sampling lines, one with the aerosol filter and the other without the aerosol filter (termed “the auto-switching aerosol filter” hereafter), which enabled alternative measurements of HO₂ reactivity by the gas phase and the gas + enriched aerosol phase of the ambient air, separately.



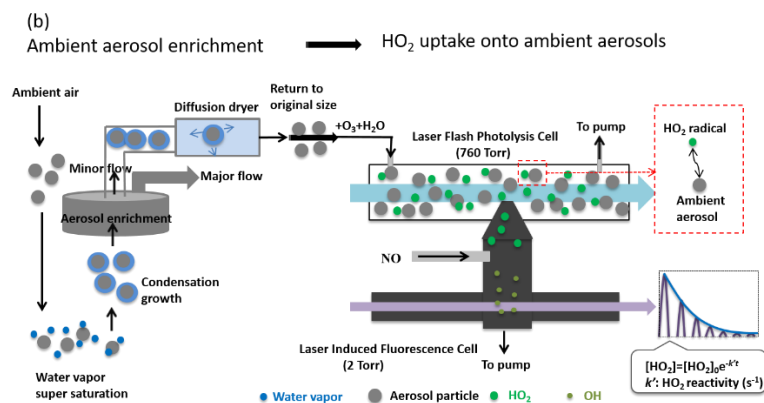


Figure S2: (a) Sampling setup for testing HO_2 reactivity using laser-flash photolysis and laser-induced fluorescence (LFP–LIF) with a versatile aerosol concentration enrichment system (VACES) and auto-switching aerosol filter (SMPS = scanning mobility particle sizer; AMS = aerosol mass spectrometer; CAPS = cavity attenuated phase shift); and (b) Detailed presentation of the measurement process of the HO_2 reactivity of the ambient aerosol phase. Further details concerning the measurement process can be found in our previous publication³.

A technique combined laser-flash photolysis with laser-induced fluorescence (LFP–LIF)

LFP–LIF comprises two cells: the laser-flash photolysis cell (the reaction cell) and the laser-induced fluorescence detection cell (the detection cell). In the HO_2 reaction cell, pure air was supplied by a zero-air generator (Model 111, Thermo Fisher Scientific Inc., USA), and relative humidity was controlled by bubbling water vapor into one part of the zero air. The ambient air was sampled into the reaction cell after mixed with the humidified zero air and O_3 , where O_3 (~100 ppb) was generated by 184.9 nm irradiation of zero air by a low-pressure Hg lamp (pen ray lamp, Sen lights corporation, JP, part number: SP-5-2H (5w)) at 50 sccm (standard cubic centimeter per minute, at 273 K and 1 atm). The reaction cell was made of aluminum, with a length of 1.4 m and an inner diameter of 0.04 m, and the inner wall of the flow tube was coated with Teflon to reduce the heterogeneous losses of HO_2 and the reactants. The sample inlet of the detection cell was located ~0.7 m from the sample injection position. The total flow inside the reaction cell was ~10 L min⁻¹, with a residence time of ~4.8 s. The Reynolds number in the reaction cell was ~354 and (1 atm pressure and 298 K were assumed inside the reaction cell), thus indicating a laminar flow. A pulsed 266-nm Nd:YAG laser (Tempest 300, New Wave Research Inc., USA), with a 1-cm diameter, laser power ranging between 0.4 and 3.0 mJ pulse⁻¹, and a repetition of 1 Hz, was used in the reaction cell to irradiate the sample air to produce OH through reactions SR1–SR2.



176 Meanwhile, excess CO was introduced into the reaction cell to convert all OH radicals to HO₂:



179 The initial HO₂ concentration in the reaction cell was of the order of 10¹⁰ molecules cm⁻³, estimated
 180 from the photolysis power, humidity, and O₃ concentration³. A stream of flow (~ 2 LPM) in the reaction
 181 cell was pumped into the detection cell using a rotary oil pump (D-950, ULVAC) under a pressure of
 182 1.6 Torr through a 0.5-mm pinhole. NO (>99.999%) was injected with a flow rate of 3 sccm between
 183 the reaction cell and the detection cell to convert HO₂ to OH (Eq. SR5, conversion efficiency: ~ 30%).
 184 The second harmonic of a pulsed laser (Sirah Credo, Spectra Physics) pumped by the second harmonic
 185 of a Nd:YVO₄ laser (YHP40-532Q, Spectra Physics) and set at a maximum absorption of Q₁(2) A²Σ⁺(v'
 186 = 0) ← X²Π_{3/2}(v'' = 0) transition of OH at 308 nm was used to irradiate the detection cell with a
 187 repetition rate of 10 kHz. The fluorescence emitted by the OH radical induced by each irradiation was
 188 collected by a photomultiplier tube (R2256P, Hamamatsu Photonics), and a decay file of OH was
 189 obtained after 240 integrations. The HO₂ decay rate was considered the same as the OH decay rate as
 190 we were measuring the relative change in the HO₂ concentration in the detection cell.



192 **The enrichment of the ambient aerosols**

193 The versatile aerosol concentration enrichment system (VACES) was built according to Sioutas
 194 et al. (1999)⁵, which comprises the aerosol growth part and the aerosol enrichment part (as shown in
 195 Fig. S2a). The ambient air sample was drawn into VACES at a flow rate of over 100 L min⁻¹ (Q_{tot}) into
 196 a ultra-pure water tank which was heated to ~32°C, where the ambient air steam was saturated and then
 197 cooled down in a condenser connected immediately above the tank (with a temperature of -2 °C). The
 198 grew ambient aerosol (mostly with a diameter > 2 μm) through condensed water droplets were then

enriched by a virtual impactor with a 50% cutoff point less than 1 μm , with $\sim 92 \text{ L min}^{-1}$ going to the major flow that connected to the exhaust pump and $\sim 8 \text{ L min}^{-1}$ going to the minor flow (q_{min}) that connected to the aerosol instrumentations after passing through a diffusion dryer. In theory, the enrichment factor (EF) of the ambient aerosol concentration can be estimated as:

$$\text{EF} = Q_{\text{tot}}/q_{\text{min}}(1 - \text{WL}) \times \eta_{\text{vi}} \quad (\text{S1})$$

where η_{vi} and WL are its collection efficiency and fractional loss, respectively⁵. The enrichment efficiency (EE) of the impactor was estimated as $\sim 1^3$. In this study, we test the enrichment factor of the surface area of the enriched ambient aerosols (E) by connecting two SMPS before and after VACES separately for ~ 2 hours every day for ~ 6 days, the enrichment factor can be calculated as:

$$E = S_1/S_2 \quad (\text{S2})$$

Where S_1 and S_2 are the surface areas of the enriched ambient aerosols after VACES and the ambient aerosols before VACES, respectively. Obtained E values from all the tests were then averaged and used as the final enrichment factor ($\sim 12.5 \pm 2.5$) for all the experimental days. The surface area of the enriched ambient aerosols with diameters $< 2.5 \mu\text{m}$ (ES) are propagated from S_1 multiply the ratio between mass concentration of $\text{PM}_{2.5}$ and $\text{PM}_{0.74}$ (calculated as ~ 1.1), by assuming the total volume and the total surface area of each size distribution bin (ranged from 0 to $2.5 \mu\text{m}$) of $\text{PM}_{2.5}$ are increased in proportional with mass concentration compared to that of $\text{PM}_{0.75}$ (ranged from 0 to $0.75 \mu\text{m}$):

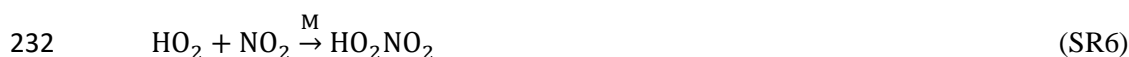
$$ES = \frac{\text{PM}_{2.5}}{\text{PM}_{0.74}} \times S_1 \quad (\text{S3})$$

HO₂ reactivity of ambient air

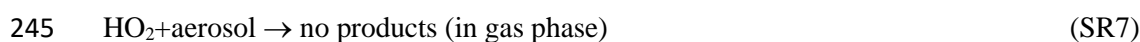
Owing to the excess CO, almost all HO₂ radicals formed in the reaction cell after the photolysis pulse, and the HO₂ and RO₂ radicals in urban ambient air were destroyed, or at least partially, during their intake into the LFP detection cell, thus the self-reaction of HO₂ and the interaction of HO₂ with RO₂ owing to the inherent HO₂/RO₂ concentrations from ambient air was negligible. Due to the large excess reactants over HO₂ radicals produced in the LFP reaction cell, pseudo-first order conditions were achieved, and the HO₂ decay rate k (HO₂ reactivity) can be explained through the following equation²:

$$\frac{d[\text{HO}_2]}{dt} = -(k_{\text{NO}_2}[\text{NO}_2] + k_{\text{NO}}[\text{NO}] + k_{\text{aerosol}}[\text{ambient aerosol}] + k_{\text{wall}}) \times [\text{HO}_2] \quad (\text{S4})$$

where k_i is the rate constant of the HO_2 reaction with different reacting species i , where $i = \text{NO}_2, \text{NO}$ and the ambient aerosols. k_{wall} is the loss rate of the HO_2 radicals onto the wall, and $[i]$ represents the concentration of the reacting species i . Due to the short reaction time, k_{wall} was small and included in the baseline. And the consumption of HO_2 by NO in the reaction cell is immediately compensated by excess CO , converting its product OH back to HO_2 ; therefore, the HO_2 decay in the LFP reaction cell may be mostly attributed to its reaction with NO_2 and aerosol phase. The reaction with NO_2 will produce peroxyntic acid:

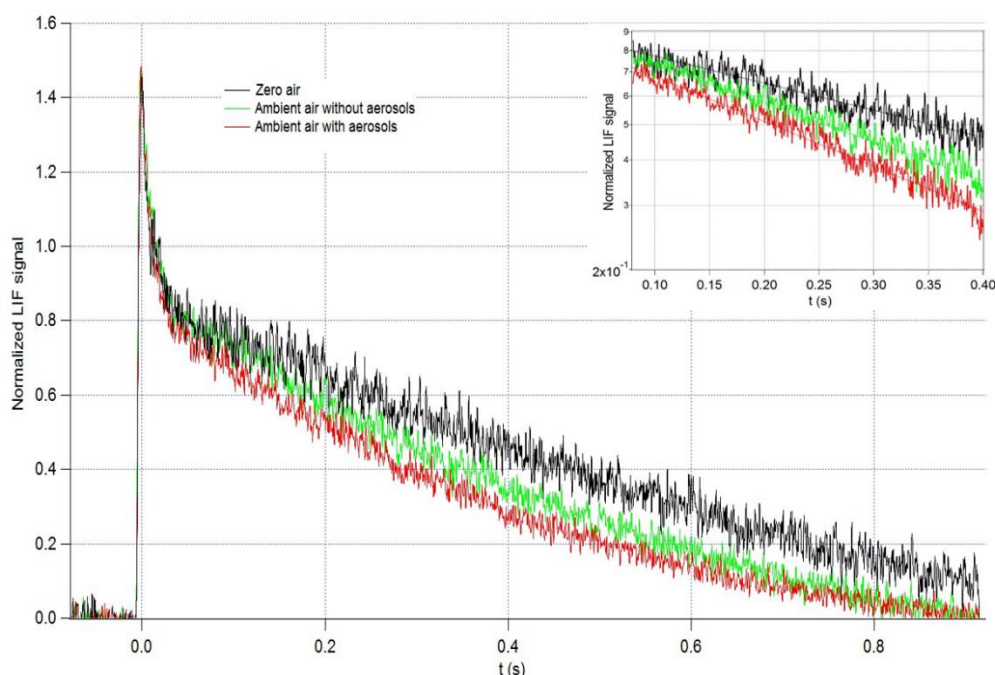


Ideally, the thermal unimolecular decomposition of HO_2NO_2 may occur. However, we didn't consider this reverse reaction, due to (1) The reaction cell (~40 mm diameter) is considerably larger than the reaction-initialized region (the laser beam covered area, ~10 mm diameter). The HO_2 , NO_2 , and HO_2NO_2 that are produced will diffuse to the outside of the reaction-initialized region (~16 times diluted), thus largely reducing the reactant concentrations. Further, reproducing the reaction process is impossible because the sampling port of the deflection cell is located in the center of the reaction-initialized region; (2) The log scale plot of the HO_2 decay profile as a function of time was linear in the fitting range (as illustrated in Fig. S3). 3) As shown in Fig. S4, the HO_2 reactivity exhibited a linear correlation with the wide concentration range of NO_2 . These phenomena indicate the negligible influence of the reverse reaction to the gas phase HO_2 reactivity. We also observed the negligible reverse reaction previously, even in the case of lower HO_2 and NO_2 concentrations². We assume the heterogeneous loss of HO_2 by the aerosol following the single first order reaction step as:



HO_2 was converted to OH in the reaction with NO in the detection cell, according to Eq. SR5. The HO_2 concentrations were then measured by laser-induced fluorescence from OH after each probe laser (266

248 nm) irradiation to obtain a decay curve. Examples of the time series of HO₂ decay files of zero air,
 249 ambient air without aerosols and ambient air with enriched aerosols are shown in Fig. S3.



250
 251 Figure S3: Examples of the measured HO₂ decay profiles in zero air (black lines), ambient air without
 252 aerosol phase (green lines), and ambient air with enriched aerosol phase (red lines) at an RH of ~60%,
 253 301 K, and an initial HO₂ concentration of ~10¹⁰ molecules cm⁻³. The log scale plot in the inserted
 254 figure at the upper right shows linear fitting in the range of 0.08–0.4.

255 Correction of gas-phase

256 for HO₂ uptake coefficient

257 γ_{obs} includes the gas phase diffusion, and as the HO₂ radical is active in aerosol bulk, the resistance
 258 model was usually utilized for explaining the observed uptake coefficients (George et al., 2013;
 259 Davidovits et al., 2006):

$$260 \quad \frac{1}{\gamma_{obs}} = \frac{1}{\gamma_{diffusion}} + \frac{1}{\alpha} + \frac{1}{\gamma_{reaction+partitioning}} \quad (S5)$$

261 where γ_{obs} and $\gamma_{diffusion}$ represent the observed uptake coefficients and the gas transport coefficient,
 262 respectively, α is the mass accommodation, and the third term represents the resistance caused by the
 263 sum of the reactive and partitioning processes within the aerosol. The observed uptake coefficients were
 264 further corrected to take into account gas diffusion contribution, and the final γ can be obtained from
 265 Eq. S6^{6, 7}:

$$\gamma = \frac{\gamma_{\text{obs}}}{1 - \gamma_{\text{obs}} \lambda(r_s)} \quad (\text{S6})$$

where $\lambda(r_s)$ are is obtained from Eq. S7:

$$\lambda(r_s) = \frac{0.75 + 0.283 K_n}{K_n(1 + K_n)} \quad (\text{S7})$$

$$\text{where } K_n = \frac{3D_g}{w_{\text{HO}_2} r_s} \quad (\text{S8})$$

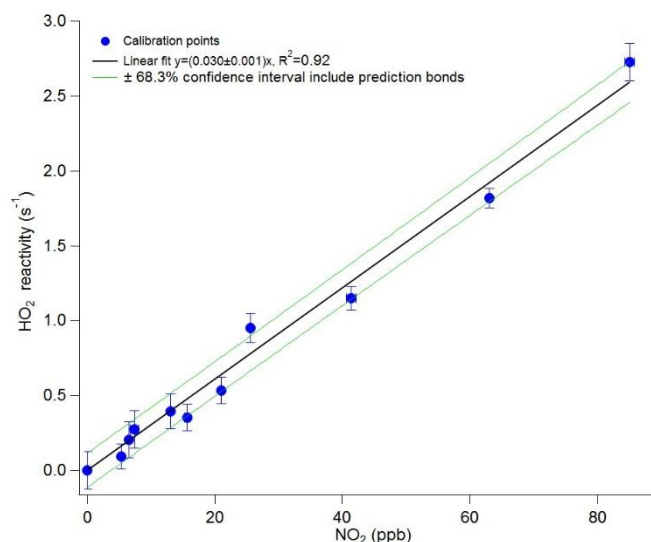
where D_g is the gas phase diffusion coefficient of HO_2 ($0.25 \text{ cm}^2 \text{ s}^{-1}$) at $\sim 298 \text{ K}$, and r_s represents the average radius of the aerosols, defined as follows:

$$r_s^2 = \frac{A_{\text{total}}}{4\pi N_{\text{total}}} \quad (\text{S9})$$

where A_{total} denotes the total surface area measured and N_{total} denotes the total number of particles producing that surface area.

HO_2 reactivity of ambient gas phase (k_g)

Gas phase HO_2 reactivity was directly measured in the reaction cell without aerosol phase. To check the dominant factor of the gas phase HO_2 reactivity, we modeled the HO_2 reactivity by using the NO_2 concentration in the LFP reaction cell, using the calibration factor obtained by plotting the measured HO_2 decay rates as a function of the NO_2 concentration prepared in the laboratory (with the NO_2 concentration in zero air ranging from 0 to 85 ppb at 298 K and 1 atm in the reaction cell, Fig. S4).



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282 Figure S4: Average of HO₂ reactivity calibrations using LFP-LIF with different NO₂ concentrations
 283 supplied by NO₂ gas. The green lines represent the $\pm 68.3\%$ prediction band of the calibration data points
 284 ($1\sigma = 0.1 \text{ s}^{-1}$), i.e., the uncertainty in the estimation of HO₂ reactivity using the calibration curve.

285 The linear fitting coefficient represents the HO₂ reactivity with NO₂ concentrations in the reaction cell,
 286 which was $0.030 \text{ s}^{-1} \text{ ppb}^{-1}$ with a standard deviation of 0.001. This indicates that the instrument accuracy
 287 in determining k_{HO_2} from NO₂ concentration was 3%. This calibration factor was used to simulate HO₂
 288 reactivity (k_{HO_2}) caused by NO₂ from ambient air in the LIF reaction cell as follows:

289
$$k_{\text{HO}_2}(\text{s}^{-1}) = (0.030 \text{ (s}^{-1}/\text{ppb)} \times \Delta\text{NO}_2(\text{ppb})) \times \left(\frac{k_f([M], T)}{k_c([M], T)} \right) \quad (\text{S10})$$

290 where ΔNO_2 denotes the difference between the NO₂ concentrations in ambient air and zero gas (here
 291 NO₂ is $\sim 0.5 \text{ ppb}$ in zero gas, which may be due to the interferences in zero gas), while $k_f([M], T)$ and
 292 $k_c([M], T)$ denote the rate constant calculated from the equations recommended by Sander et al. (2011)⁸
 293 using the temperature in the reaction cell at the ambient air measurement time and calibration time,
 294 respectively.

295 Temperature and pressure influence correction

296 Reaction in SR6 is favored by low-temperature and high-pressure conditions and is believed to play an
 297 important role in the free troposphere and particularly the upper troposphere as it becomes cooler with
 298 higher pressure⁹. The room temperature was maintained at 298 K during the whole campaign. However,
 299 the temperature in the reaction cell ranged from 298 K to 302 K due to the sampled ambient air

temperature. The temperature and pressure correction was done according to the procedure adopted by the National Aeronautics and Space Administration (NASA) data evaluation panel, as follows⁸:

$$k_f([M], T) = \left[\frac{k_0(T)[M]}{1 + \frac{k_0(T)[M]}{k_\infty(T)}} \right] 0.6 \left\{ 1 + \left[\log_{10} \left(\frac{k_0(T)[M]}{k_\infty(T)} \right) \right]^2 \right\}^{-1} \quad (\text{S11})$$

where $k_0(T)$ denotes the low-pressure-limiting rate constants, which can be calculated as:

$$k_0(T) = k_0^{300} \left(\frac{T}{300} \right)^{-n} \text{ cm}^6 \text{ molecule}^{-2} \text{ s}^{-1} \quad (\text{S12})$$

and $k_\infty(T)$ denotes the limiting high-pressure rate constant, which can be calculated similarly:

$$k_\infty(T) = k_\infty^{300} \left(\frac{T}{300} \right)^{-m} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1} \quad (\text{S13})$$

Here, n and m in Eqs. S11&S12 represent the temperature-dependent coefficients, which are recommended as 0.34 ± 0.4 and 1.1 ± 1.4 , respectively. The equilibrium constants at temperature T , $K(T)$, can be expressed as:

$$K(T) = \frac{k_f([M], T)}{k_{-1}(T)} = 2.1 \times 10^{-27} \left(\frac{10900}{T} \right) \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1} \quad (\text{S14})$$

Thus, $k_{-1}(T)$, which is the rate constant of the reverse reaction of SR6, can be calculated from the known $K(T)$ and $k_f([M], T)$.

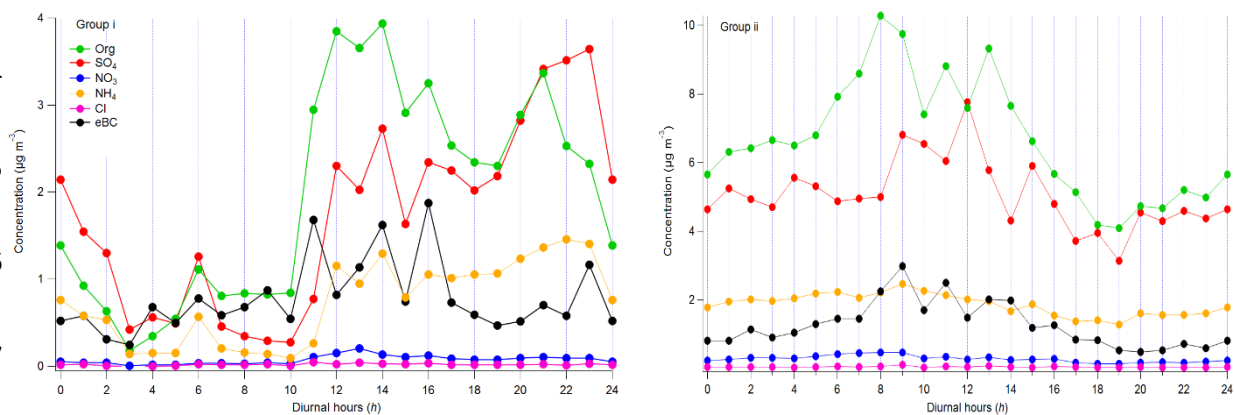


Figure S5: Diurnal trends in non-refractory chemical components plus eBC of group i (left side) and group ii (right side).

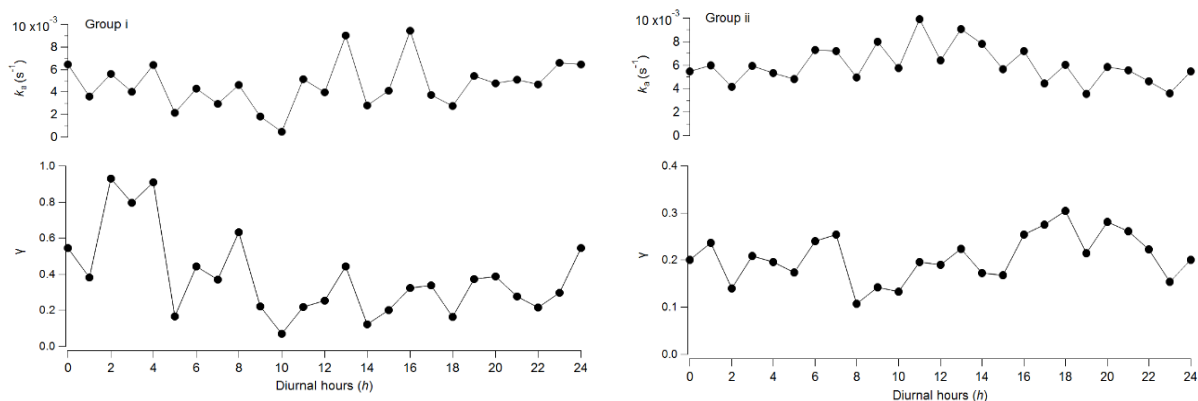


Figure S6: Diurnal trends in total HO_2 reactivity caused by the ambient aerosol phase (k_a , upper panel) and the HO_2 uptake coefficients onto ambient aerosols (γ , lower panel).

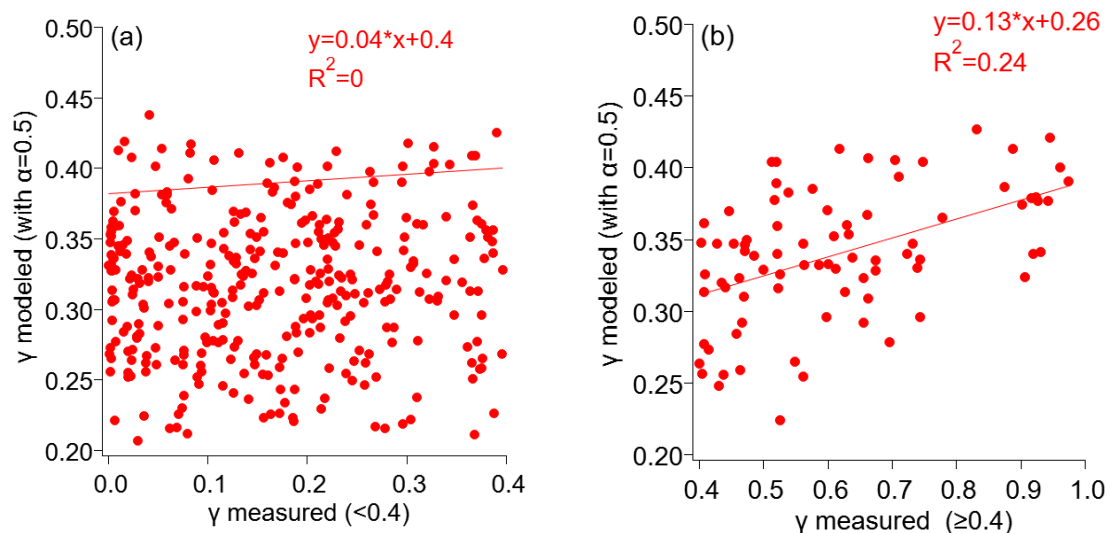


Figure S7: Correlations between measured and modeled γ with (a) $\gamma < 0.4$ and (b) $\gamma \geq 0.4$.

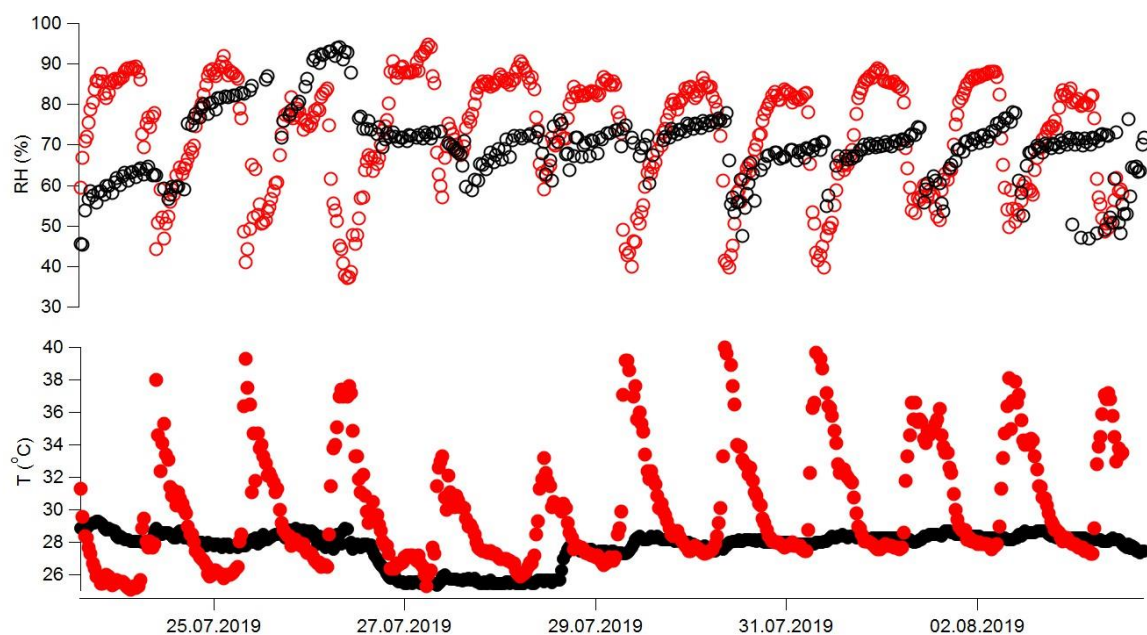


Figure S8: Time series of the half-hour averaged ambient RH (red open cycles in the upper panel) and temperature (red filled cycles in the lower panel) measurements in comparison to the reaction cell RH (black open cycles in the upper panel) and temperature (black filled cycles in the lower panel).

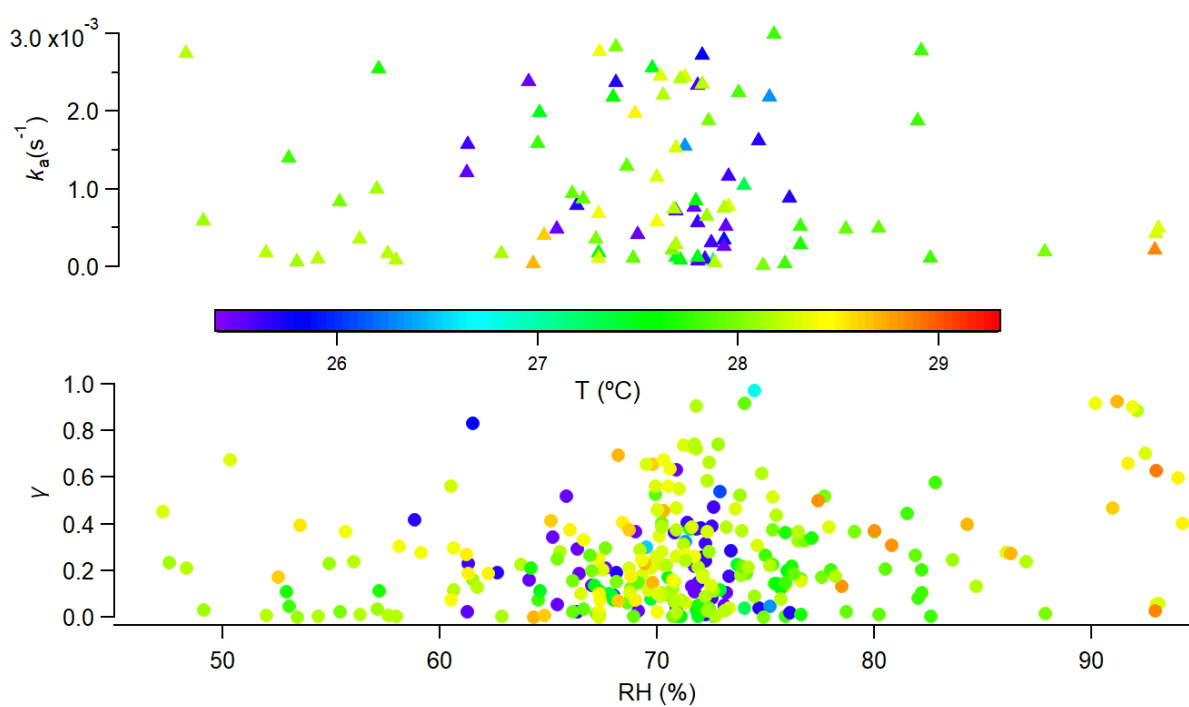


Figure S9: k_a and γ values as a function of RH in the reaction cell, colored coded with T .

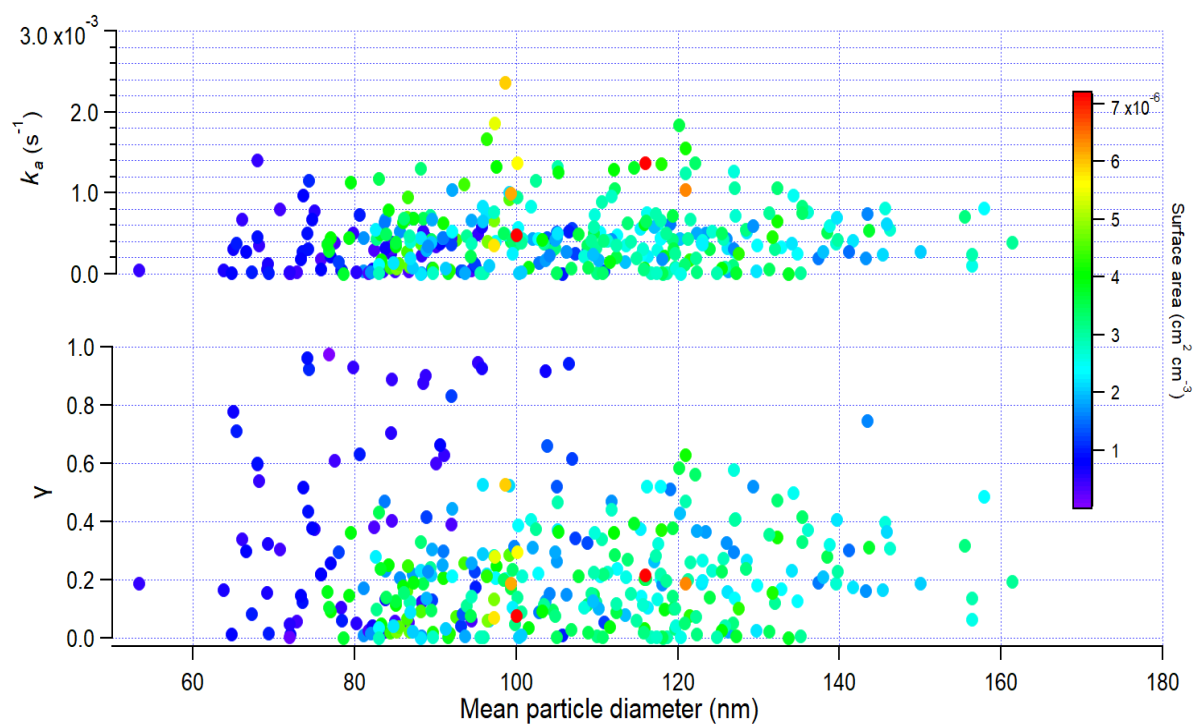


Figure S10: k_a (upper panel) and γ (lower panel) as a function of mean particle diameter, color coded with the surface area concentration.

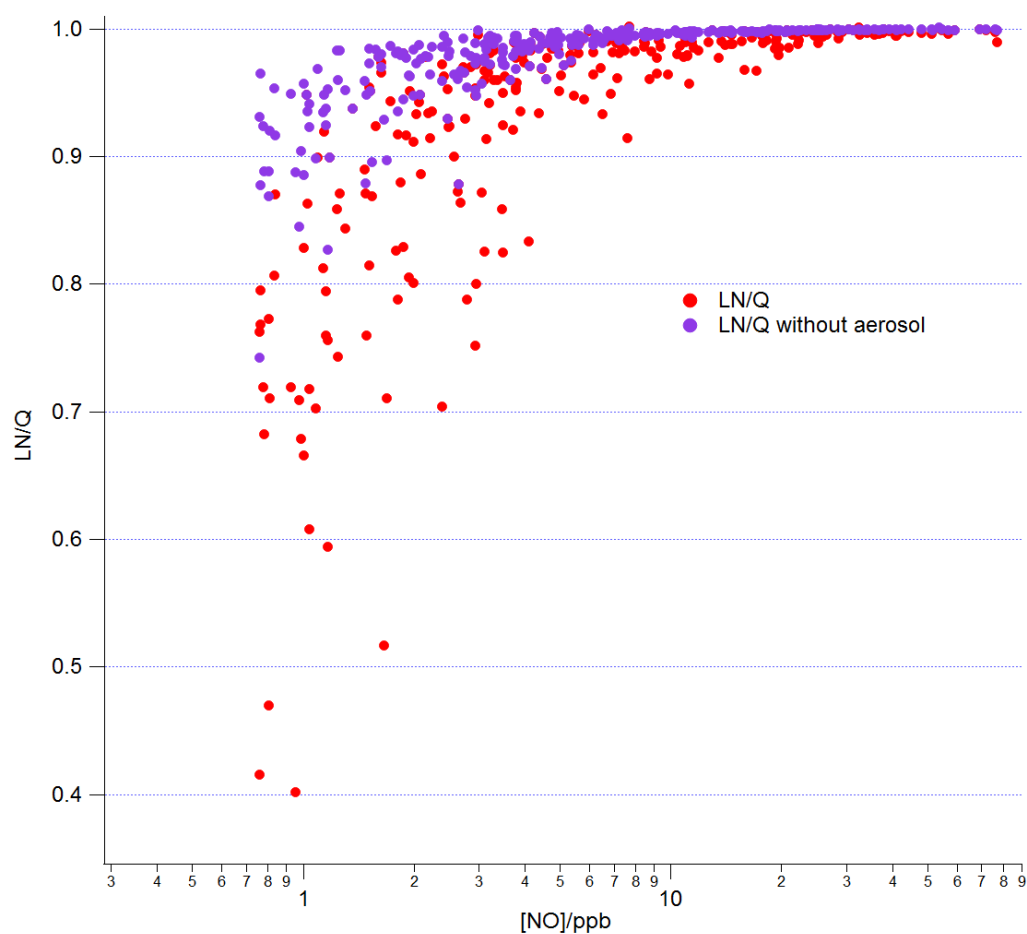


Figure S11: Dependence of day time LN/Q and $LN/Q_{\text{without_aerosol}}$ on $[NO]$.

Profiles of key factors used in Section 3.5:

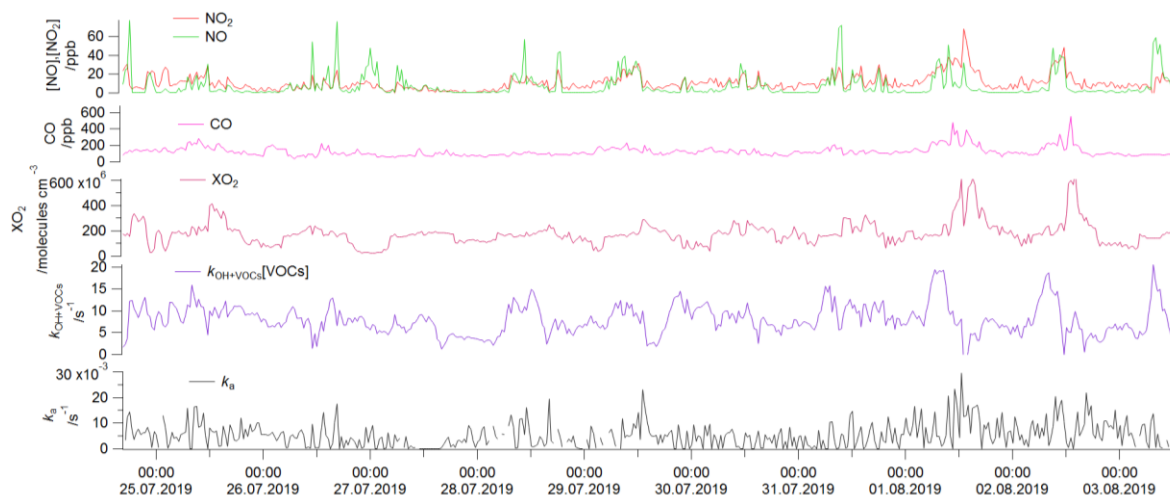


Figure S12: Temporal variations in key factors in ambient air for determining XO_2 loss rates and $P(O_3)$ sensitivity in Sect. 3.6.

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Table S1 Summary of equations and values used in Section 3.4.

Parameters	Equations and values	Ref.
$\omega / \text{cm s}^{-1}$	47376	
α^{HO_2*}	>0.2 (with copper (II)-doped aerosols)	[¹⁰⁻¹⁶]
$H_{eff} / \text{M atm}^{-1}$	$H_{\text{HO}_2} (1 + \frac{k_{eq}}{[H^+]})$	[¹⁷]
$H_{\text{HO}_2} / \text{M atm}^{-1}$	EXP(4.9×4184/(8.314×T))	[¹⁸]
k_{eq}^{**}	2.1×10^{-5}	[¹⁷]
$[H^+] / \text{mol L}^{-1}$	$10^{-\text{pH}}$	
pH	Calculated from the ISORROPIA-II model	
$R / \text{J mol}^{-1} \text{K}^{-1}$	8.314	
$[\text{HO}_2(\text{g})]^{** *}$	1.0×10^{10}	[³]
r_p / cm	Measured by SMPS	
$k_{\text{TMI}}^{\text{II}} / \text{M}^{-1} \text{s}^{-1}$	10^9	[¹⁷]
$[\text{TMI}] / \text{mol L}^{-1}$ (using Cu^{2+} as surrogate) ****	$0.1 \times [\text{Cu}]^{***}$ <i>Liquid content in the aerosol ****</i>	[¹⁹]
D_{aq}	10^{-5}	[¹⁷]

* Due to the aerosol particles collected in Yokohama City containing Cu, a high accommodation coefficient of HO₂ (α^{HO_2}) may lead to HO₂ uptake as an important sink of the HOx radical. According to the current research studies, we select α^{HO_2} as 0.2 (typically for organics) and 0.5 (typically for inorganics) for the model simulation.

** HO₂ acid dissociation constant

***HO₂ concentration in the reaction cell, calculated using the same method as Zhou et al. (2019)³.

**** Measured by off-line method

381 **Table S2** Summary of equations and values used in Section 3.6.

Parameters	Equations and values	Ref.
$k_a=k_{\text{HO}_2}=k_{\text{RO}_2}$	Observed	
$k_{\text{NO}-\text{XO}_2}=k_{\text{NO}-\text{HO}_2}=k_{\text{NO}-\text{RO}_2}$ /cm ³ molecule ⁻¹ s ⁻¹	$3.3 \times 10^{12} \exp\left(\frac{270}{T}\right)$	[²⁰]
[OH] /molecules cm ⁻³	10 ⁶ (we assumed it is constant during the campaign)	
[HO ₂]* /molecules cm ⁻³	Day time (4:30 am – 7 pm): $\exp(8.4171 \times 10^{-13} [\text{O}_3] + 18.081)$ Night-time (7 pm – 4:30 am): $6.042 \times 10^6 + 1.841 \times 10^{-4} [\text{O}_3]$	[²¹]
[XO ₂]/molecules cm ⁻³	[HO ₂] plus [RO ₂]	
[HCHO]**/ppb	2	
$k_{\text{OH}-\text{VOCs}}[\text{VOCs}]/\text{s}^{-1}$	Total OH reactivity (k_{OH}^*) minus $k_{\text{OH}+\text{NO}_2}[\text{NO}_2]$	
$k_{\text{HO}_2-\text{HO}_2}$ /cm ³ molecule ⁻¹ s ⁻¹	1.5×10^{-12}	[²²]
$k_{\text{HO}_2-\text{RO}_2}$ /cm ³ molecule ⁻¹ s ⁻¹	$2.91 \times 10^{-13} \exp\left(\frac{1300}{T}\right) [1 - \exp(-0.245n)]$ (n = 4, assumed from observed VOCs distribution).	[²³]
$k_{\text{OH}-\text{HCHO}}$ /cm ³ molecule ⁻¹ s ⁻¹	$8.2 \times 10^{-12} \times (T/298) \exp(0.33/(8.314 \times T))$	[⁸]
$k_{\text{OH}-\text{CO}}$ /cm ³ molecule ⁻¹ s ⁻¹	2.4×10^{-13}	[²⁰]
$k_{\text{OH}-\text{NO}_2}$ /cm ³ molecule ⁻¹ s ⁻¹	1.21×10^{-11}	[²⁴]

382 *Measured in real time

383 **Average value measured during the campaign

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